Sonophotocatalysis with Photoactive Nanomaterials for Wastewater Treatment and Bacteria Disinfection

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**ABSTRACT:** Sonophotocatalysis is described as a combination of two individual processes of photocatalysis and sonocatalysis. It has proven to be highly promising in degrading dissolved contaminants in wastewaters as well as bacteria disinfection applications. It eliminates some of the main disadvantages observed in each individual technique such as high costs, sluggish activity, and prolonged reaction times. The review has accomplished a critical analysis of sonophotocatalytic reaction mechanisms and the effect of the nanostructured catalyst and process modification techniques on the sonophotocatalytic performance. The synergistic effect between the mentioned processes, reactor design, and the electrical energy consumption has been discussed due to their importance when implementing this novel technology in practical applications,



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such as real industrial or municipal wastewater treatment plants. The utilization of sonophotocatalysis in disinfection and inactivation of bacteria has also been reviewed. In addition, we further suggest improvements to promote this technology from the lab-scale to large-scale applications. We hope this up-to-date review will advance future research in this field and push this technology toward widespread adoption and commercialization.

**KEYWORDS:** sonophotocatalysis, nanomaterials, degradation, wastewater treatment, cavitation bubbles, sonoluminescence, sonophotocatalytic mechanisms, bacteria disinfection

# 1. INTRODUCTION

Nowadays, water bodies are being contaminated by a broad range of pollutants at a sky-rocketing pace. Although there is no precise information associated with the amount of wastewater discharged to the environment, the horrible consequences of pollutants existing in the aquatic media have led to great public concerns (i.e., human and animal infections, and destruction of the natural habitats and the wildlife living in those territories).<sup>1,2</sup> There is an array of wastewater treatment approaches that have already been investigated, including biological, physical, and chemical treatments. Despite their cost-effectiveness, conventional methods still suffer from several shortcomings, such as being time-consuming, high cost of waste disposal, forming large amounts of slug, and too much sensitivity of living organisms to operational parameters.<sup>3</sup>

Over the past few decades, photocatalysis has been eliciting considerable interest for several reasons including low-cost, outstanding reusability and recyclability of photocatalysts, its ability to produce a high content of active radicals, negligible sludge generation, and high mineralization rate.<sup>4</sup> The photocatalysis process starts through the excitation of electrons and generation of holes in a semiconductor material (such as ZnS,<sup>5</sup>

 $g-C_3N_{49}^{\phantom{4},6}$  TiO<sub>2</sub>,<sup>7</sup> ZnO,<sup>8</sup> CuO<sup>9</sup>) under the irradiation of a light source. However, the practical applications of conventional photocatalysts have been restricted due to some bottlenecks such as low efficiency, high recombination rate of electron/ hole (e<sup>-</sup>/h<sup>+</sup>) pairs, and agglomeration of nanoparticle catalysts.<sup>10</sup> To overcome these hindrances, the combination of photocatalysis process with other methods, electrochemical and sonolysis techniques, has been proposed.

Sonochemistry refers to the chemical process realized by passing ultrasonic waves through liquid environments. It has been utilized for the degradation of several pollutants.<sup>11,12</sup> Coupling ultrasonic waves of specific frequencies (20–1000 kHz) with photocatalysis is postulated to be one of the most promising techniques for developing complete mineralization of recalcitrant contaminants since it improves the overall contaminant removal efficiency. Figure 1 depicts the growth in

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use of sonocatalysts, sonophotocatalysts, and sonophotocatalyst nanomaterials for wastewater treatment in the recent years.





Acoustic cavitation generated by powerful ultrasonic waves of a liquid can provide unique and unusual reaction sites. This is attributed to extremely small and transient cavitation microbubbles with high pressure and temperature (5000 K, 1000 atm) inside the bubble. Among all the advantages this process can provide, the most critical one is the unique release of an avalanche of reactive radicals, e.g., OH<sup>•</sup> and H<sup>•</sup>, owing to the homolytic cleavage of water molecules.<sup>13</sup> These specific physical and chemical events generated during the cavitation process are often different from those taking place in traditional photochemical reactions. Providing large numbers of hot vapor sites in solution (microbubbles), ultrasonication expels hydrophobic pollutants to the liquid-vapor boundaries where they will be degraded effectively by either produced shock waves or radicals on-site, whereas hydrophilic contaminants can be removed by photocatalysis in liquid.<sup>14</sup> Therefore, both hydrophobic and hydrophilic contaminants can be effectively degraded in water, which is clearly advantageous over the traditional photocatalysis. Moreover, ultrasonication offers several additional benefits, like simple and safe operation and the formation of a large number of hydroxyl radicals (OH<sup>•</sup>) through different mechanisms.<sup>15</sup> Studies of the combination of light with ultrasound (US) irradiation for the removal of organics from wastewater have been reported, and the combined process was found to be significantly more effective than either process separately, showing a great synergistic enhancement effect.<sup>16-20</sup> This association provides an excellent opportunity to decrease the reaction time and the amount of photocatalyst utilized without using extreme physical conditions.

Recently, photocatalysis has been employed for the disinfection of pathogenic bacteria due to its potential to produce reactive oxygen species. It is true that photocatalysis is capable of deactivating water borne enteric bacteria, but there is a number of challenges associated with its implementation,<sup>21,22</sup> for example, prolonged exposure times, reactivation of bacteria after a photocatalytic process due to DNA repair mechanisms, and a decrease in active surface area because of agglomeration of photocatalysts.<sup>23–25</sup> Sonophotocatalysis—a

hybrid disinfection strategy—is proposed as a solution to overcome these limitations of traditional photocatalysis.

Although there are a few review articles in this field, they do not include information related to reaction mechanisms in sonophotocatalysis. In this critical review, mainly focused on metal-oxide nanomaterials, we conducted a thorough analysis of ultrasonic-assisted photocatalytic mechanisms in wastewater treatment, their synergistic effects, and enhancing techniques. For the first time, an electrical energy consumption analysis has been performed, which allowed us to make a comparison between sonophotocatalysis, traditional photocatalysis, and sonocatalysis. In addition to the description of different reactor designs, we reviewed the application of sonophotocatalysis in bacterial disinfection. We hope this review article will contribute to the ongoing research into whether sonophotocatalysis could replace conventional photocatalysis or be used in large-scale wastewater treatment applications.

## 2. SONOPHOTOCATALYSIS MECHANISMS

As the name implies, sonophotocatalytic mechanisms include those of photocatalysis and sonocatalysis. Detailed explanations of each individual process will follow in order to explain the mechanisms clearly.

## 2.1. Photocatalysis Mechanisms

In order to highlight the differences between sonophotocatalysis and photocatalysis, we will first briefly describe the mechanism of traditional photocatalysis. Photocatalytic processes initiate with the exposure of catalytic semiconductor materials to a light source. In this step, photonic energy leads to the excitation of electrons from the valence band (VB) to conduction band (CB), creating positive holes in the VB. The reaction of oxygen molecules and hydrogen peroxide molecules (produced either *in situ* or intentionally introduced) with photoinduced electrons produces superoxide anion radicals  $(O_2^{\bullet-})$  and OH<sup>•</sup> radicals, respectively. Meanwhile, the reaction of water molecules with positive holes produces  $OH^{\bullet}$  radical species (eqs 1-9).<sup>10</sup> These photoactivated systems have the ability to degrade a wide variety of pollutants (e.g., dyes and pharmaceuticals) and completely mineralize contaminants. On the other hand, these systems suffer from a few disadvantages, such as low reaction rate constants, low visible (Vis) light absorption of catalytic materials, and performance reduction over time due to catalytic particle agglomeration. These drawbacks restrict their utilization at an industrial scale.<sup>26,27</sup>

$$\text{catalyst} \xrightarrow{h\nu} \mathbf{h}_{VB}^{\phantom{VB}+} + \mathbf{e}_{CB}^{\phantom{CB}-} \tag{1}$$

$$H_2O + h^+ \to H^+ + OH^{\bullet}$$
(2)

$$O_2 + e^- \to O_2^{\bullet-} \tag{3}$$

$$O_2^{\bullet-} + H^+ \to OOH^{\bullet} \tag{4}$$

$$2OH^{\bullet} \to H_2O_2 \tag{5}$$

$$H_2O_2 + e^- \to OH^- + OH^{\bullet}_{ads}$$
<sup>(6)</sup>

$$2OOH^{\bullet} \rightarrow H_2O_2 + O_2 \tag{7}$$

$$H^{\bullet} + H_2O_2 \rightarrow OH^{\bullet} + H_2O \tag{8}$$

$$OH^{\bullet} + H_2O_2 \rightarrow OOH^{\bullet} + H_2O \tag{9}$$



Figure 2. Illustration of sonophotocatalytic setup and degradation mechanism. The sonophotochemical reactor figure is reproduced with permission from ref 28. Copyright 2020 Elsevier.

#### 2.2. Sonocatalysis Mechanisms

Among all the strategies adopted to overcome the photocatalysis shortcomings, integration with ultrasonic waves ranks top in terms of feasibility and effectiveness. The sonocatalysis mechanism consists in three key processes (see Section 1 in Figure 2).

First, at the phase boundary or solid surface, solid catalytic particles serve as additional nucleation sites for the heterogeneous nucleation of cavitation bubbles. It is notable that this process is different from homogeneous nucleation that occurs in the bulk solution by thermal fluctuations. Accordingly, cavitation bubbles are formed when acoustic cavitations reach rarefaction cycles (expansion) where an acoustic pressure is sufficiently high to dissociate water molecules. Having grown to an unstable and critical size during the rarefaction cycles, bubbles filled with vapor from the liquid and with dissolved gases can collapse violently, creating implosions and cavitations especially for high acoustic pressure amplitudes more than 1 bar.<sup>29,30</sup>



**Figure 3.** (A) Photographic images of SL (left images) and chemiluminescence (right images) in water at various US powers of (a) 10, (b) 30, and (c) 50%. (B) PL spectra of SL detected at three different zones of US reactor (red line, top; black line, middle; and blue line, bottom) with US power of (a) 10, (b) 30, and (c) 50%. Inset spectra are UV to Vis light range only. Reprinted with permission under a Creative Commons CC-BY license from ref 36. Copyright 2020 MDPI.

Sonoluminescence (SL) refers to emission of light by the collapse of cavitation bubbles. The second key step involves the collapse of cavitation bubbles, which results in SL, i.e., emission of light ranging from 200 nm to near-infrared (NIR) zone (longer than 700 nm) with relatively high intensity. This phenomenon happens only if the plasma energy is high enough to generate electronically excited species (ions, molecules radicals, etc.). Obviously, the energy threshold for excited species production during the bubble collapse is much higher than that for radical formation.<sup>31</sup> In this way, since the light energy from SL is greater than that of the semiconductor band gap, it could induce extra e<sup>-</sup>/h<sup>+</sup> pairs, which leads to high reactive species production (eqs 1-4). Previous studies indicated that the excitation of TiO<sub>2</sub> catalyst by SL caused a remarkable decomposition of pollutants, such as methylene blue (MB) and phenol and 2,4-dinitrophenol, just as observed in photocatalytic processes.<sup>32,33</sup> The spectral shapes and intensities of SL rely on several parameters, such as the presence of additives, types of saturated gas, and the frequency and power of US.<sup>31,34</sup> For example, Qui et al.<sup>35</sup> calculated the

SL power at a wavelength of 400 nm during sonocatalysis (energy  $4.9 \times 10^{-19}$  J). Since each flash of SL can last for about 50 ps, emitting approximately  $10^7$  photons, the power of SL for each second was 0.098 W. Choi et al.<sup>36</sup> detected the ultrasonicinduced SL through the sonophotocatalytic degradation of eosin B using commercial TiO<sub>2</sub>, by means of photographic imaging, a radical indicator (luminol, C<sub>8</sub>H<sub>6</sub>N<sub>3</sub>O<sub>2</sub>Na) for detecting radical formation zones, and photoluminescence (PL) spectroscopy for detecting emitted photons in the wavelength range 300-1050 nm. At an US power of 35.4 W/ cm<sup>2</sup>, SL was observed in a standing wave pattern throughout the sonophotocatalytic reactor (Figure 3A). By increasing US intensity, this pattern disappeared and the SL mostly occurred at the ultrasonic horn tip. Authors highlighted that SL occurred mostly in the NIR range, and its intensity increased almost linearly with the US power (Figure 3B). PL measurements revealed that UV irradiations appear only when enough energy input was applied (106.1 and 176.8 W/cm<sup>2</sup>). With the 35.4 W/cm<sup>2</sup> US intensity, band-type chemiluminescence arose at



**Figure 4.** Adsorption/desorption isotherms of  $TiO_2$  (A) before and (B) after  $H_2O_2$ -assisted sonophotocatalysis (model solution contained 13 compounds commonly found in olive mill wastewaters at the concentration of 50 mg/L each, UVA power of 400 W, and US power of 120 W at 80 kHz). SEM images of as-prepared ZnO samples before (C, E, and G) and after sonophotocatalysis (D, F, and H). (C and D) ZnO-R, (E and F) ZnO-F, and (G and H) ZnO-S. (A and B) Reproduced with permission from ref 45. Copyright 2007 Elsevier. (C–H) Reproduced with permission from ref 46. Copyright 2021 Elsevier.

the top and middle zones of the reactor, but as the intensity increased, it appeared around the horn tip.

The third step involved in the degradation process is related to the collapse of cavitation bubbles that produces high local temperature points. This leads to thermal activation of semiconductor surface, enhancing  $e^{-}/h^{+}$  pairs production and formation of active radicals.<sup>28,37</sup> The produced OH<sup>•</sup> radicals can diffuse in the bulk solution and reach the interfacial region of the other cavitation bubbles with high temperature due to the existence of a large gradient of temperature and radical concentration. Notably, through sonocatalytic decontamination processes, hydrophobic organic contaminants tend to move to interfacial regions and to be destroyed by the cavitation bubbles and highly concentrated OH<sup>•</sup> radicals at the gas-bubble region. On the contrary, hydrophilic contaminants could not get oxidized in the bubble boundaries due to their tendency to move to the bulk area and get decontaminated indirectly through the hydroxyl-radicalproducing reactions initiated by the cavitation process or by photocatalysts. The presence of dissolved oxygen can enhance the effect of the third step. Thermal dissociation of dissolved oxygen and water molecules in the cavitation bubbles convert them into active species (including  $OH^{\bullet}$ ,  $O_2^{\bullet-}$ ,  $H^{\bullet}$  and  $OOH^{\bullet}$ radicals) (eqs 10-18). Then, the as-produced reactive species can participate in decontamination processes in the bulk solution and/or at the gas-cavitation-bubble interface. In the case of absence of contaminants, the produced species convert to water molecules (eqs 15–17). The production of  $H_2O_2$ occurs outside of hotspots (implosion of bubbles) or at the

lower temperature gas–liquid interfaces by recombination of OH<sup>•</sup> and OOH<sup>•</sup> radicals in the same way as during the photocatalysis (eqs 6-9).<sup>38-40</sup>

$$H_2O \xrightarrow{US} OH^{\bullet} + H^{\bullet}$$
(10)

$$O_2 \xrightarrow{OS} 2O^{\bullet}$$
 (11)

$$OH^{\bullet} + O^{\bullet} \to OOH^{\bullet}$$
(12)

$$O^{\bullet} + H_2 O \to 2OH^{\bullet}$$
(13)

$$H^{\bullet} + O_2 \to OOH^{\bullet}$$
(14)

$$\mathbf{D}\mathbf{H}^{\bullet} + \mathbf{H}^{\bullet} \to \mathbf{H}_2\mathbf{O} \tag{15}$$

$$2OH^{\bullet} \to H_2O + O^{\bullet} \tag{16}$$

$$OOH^{\bullet} + OH^{\bullet} \to H_2O + O_2 \tag{17}$$

$$2H^{\bullet} \to H_2 \tag{18}$$

#### 2.3. Catalyst Cleaning Effect and Recyclability Studies

There has been evidence that ultrasound shock waves can cause catalyst depoisoning and cleaning. This was reported by Disselkamp et al.<sup>41</sup> investigating the ultrasound impact on hydrogenation vs isomerization of 3-buten-1-ol in the presence of black palladium in water. This study showed that applying ultrasound during the reaction caused a rapid *in situ* cleaning reduction of black Pd. This was caused by the implosion of cavitation bubbles on the surface of Pd, which led to a 5-fold



**Figure 5.** (A) Reusability test of  $TiO_2/CuO/NGP$  (1:0.1 10G) under different modes of light irradiation. (B) Schematic sonophotocatalytic charge transfer mechanism of integrated  $TiO_2/CuO/NGP$ . (C) XRD patterns of the sample (a) before treatment, (b) after photocatalytic treatment, and (c) after sonophotocatalytic treatment of MB. (D) Recyclability of NU@ZIS20 nanocomposite catalyst in sonophotocatalytic tetracycline degradation. (E) XRD patterns and (F) FT-IR spectra of NU@ZIS20 before (I) and after (II) sonophotocatalytic cyclic tests under a 300 W halogen lamp irradiation. TEM image of NU@ZIS20 nanocomposite before (G) and after (H) five runs. (A–C) Reproduced with permission from ref 51. Copyright 2018 Elsevier. (D–H) Reproduced with permission from ref 52 Copyright 2021 American Chemical Society.

increase in the reaction rate. The same phenomenon was observed by Carcenac et al.<sup>42</sup> studying catalytic hydrogenation of fluorinated alkenes using  $PtO_2$ .

In photocatalysis, physically, cavitation bubbles collapsing near the surface of nanoparticles will cause asymmetric shock waves, which consequently leads to deaggregation of particles and continuous surface cleaning, increasing the exposed active sites at the surface of the material.<sup>43,44</sup> Silva et al.<sup>45</sup> reported an improvement in the specific BET surface area of TiO<sub>2</sub> when  $H_2O_2$ -assisted sonophotocatalytic degradation of phenolic compounds in agro-industrial effluent was investigated. Although the pre- and post-treatment catalysts displayed similar type isotherms (Figures 4A,B), the used sample was able to adsorb much more nitrogen than the fresh one. After 180 min of reaction, the BET specific surface area improved from 47.3 to 109.7 m<sup>2</sup>/g, and the average pore diameter increased from 20.1 to 27.7 nm, suggesting that the deaggregation of nanoparticles by ultrasound results in an

enhancement in surface area. The same phenomenon was observed by Yang et al.<sup>46</sup> when three different morphologies of ZnO nanoparticles were synthesized and employed for sonophotocatalytic degradation of methyl orange. Surface areas of rod-like ZnO (ZnO-R) with 2.617 m<sup>2</sup>/g, flower-like ZnO (ZnO-F) with 14.98 m<sup>2</sup>/g, and sheet-like ZnO (ZnO-F) with 47.46 m<sup>2</sup>/g increased after the treatment. According to SEM images (see Figure 4C–H), there was no significant morphological change after the sonophotocatalytic process.

Reusability is one of the most prominent factors, influencing the application of nanomaterials as well as their economic aspects. During conventional photocatalytic reactions, sticking of pollutant molecules or degradation products onto the catalyst surface, in particular porous sites, leads to catalyst poisoning and, thereby, decreased efficiency over continuous use of the photocatalysts.<sup>26</sup> Reusability tests have revealed that photocatalysts can be reutilized generally over three to five consecutive cycles while maintaining approximately over 85% photocatalytic degradation efficiency. This usually depends on the type of nanomaterials used, pollutants and operational parameters. Usually, the catalyst samples were collected, washed with DI water, dried and gathered for next consecutive cycles.<sup>47,48</sup> For instance, Niu et al.<sup>49</sup> showed that boron-doped TiO<sub>2</sub>, as a Vis-light-driven photocatalyst, could be used for five runs in the photocatalytic degradation of rhodamine B (RhB) under optimized conditions. The same number of cycles with about 80% degradation efficiency at the fifth one was obtained for the photocatalytic degradation of MB using WO<sub>3</sub>/SiO<sub>2</sub> monoliths.<sup>50</sup>

Sonophotocatalysis, as an upgraded photocatalytic degradation method with a higher removal potential, enables catalysts to be more effectively reused. The generated acoustic waves, cavitation bubbles and subsequent shock waves can have refreshing and depoisoning effects, leading to better sonophotocatalysts recyclability without a significant decrease in efficiency.<sup>43,44</sup> Taufik et al.<sup>51</sup> examined the photocatalytic and sonophotocatalytic degradation of MB by a TiO<sub>2</sub>/CuO composite incorporated with graphene nanoplates under both Vis and UV light irradiations. As can be seen in Figure 5A, catalysts showed better cyclic performances in both Vis + US and UV+US degradation experiments compared to those solely under Vis and UV illuminations. In the photocatalytic runs, catalysts were reused for four consecutive cycles with approximately 20% decrease in efficiency in both series of experiments. However, when using sonophotocatalysis, the degradation efficiency was maintained at 100% for the first three cycles. This is clear evidence of the beneficial effect of US waves in catalyst cleaning, which increased the number of active sites in the surface of the materials. On these active sites, high-energy photons will be continuously absorbed, giving electrons enough energy to migrate to the CB and initiate sonophotocatalytic oxidation reactions. The schematic sonophotocatalytic charge transfer pathway of TiO<sub>2</sub>/CuO/NGP is also shown in Figure 5B. The intensity and location of XRD peaks remained unchanged after six cycles (Figure  $5C_{a}-c$ )), proving that ultrasonic cleaning has no destructive effect on the crystalline structure of the catalysts. In another study by Abazari et al.,<sup>52</sup> core@shell Zr (IV) metal-organic framework nanorods and ZnIn<sub>2</sub>S<sub>4</sub> nanostars (NU@ZIS20) achieved a sonophotocatalytic activity of 92% for tetracycline degradation after five cycles (Figure 5D). There were not significant structural or morphological changes, as can be seen from the

XRD patterns, Fourier transform infrared spectroscopy (FTIR) spectra, and TEM images in Figure 5E–H.

Hayati et al.<sup>53</sup> revealed that N, Fe codoped TiO<sub>2</sub>@singlewalled carbon nanotubes (CNTs) could be reused for seven cycles for ultra-assisted photocatalytic degradation of sulfathiazole. In a similar investigation by Gholami et al.,<sup>54</sup> Zn– Cu–Mg-mixed metal hydroxide/g-C<sub>3</sub>N<sub>4</sub> (MMH/g-C<sub>3</sub>N<sub>4</sub>) was used for the degradation of sulfadiazine. A negligible decrease of 5% in performance was observed. Additionally, no fracture in the structure or mass loss was detected after 10 cycles.

#### 3. NANOSTRUCTURED SONOPHOTOCATALYST ENHANCEMENT STRATEGIES

#### **3.1. Catalyst Modifications**

It is well-known that both the size and morphology of semiconductors play a crucial role in their properties. Some examples of nanomorphologies are nanoparticles, nanorods, nanoflowers, nanotubes, and nanosheets. Due to the greater surface-to-volume ratio, availability of increased number of accessible active sites, and higher separation efficiency of photogenerated electrons and holes, nanoscaled catalysts tend to have higher performance when compared to non-nano or bulk materials.58 However, limited light absorption, high  $e^{-}/h^{+}$  recombination rate, and low adsorption rate are mostly inevitable in sonophotocatalysis. Thus, researchers have focused their attention in modifying nanoscale semiconductor materials to enhance their catalytic activity. To this end, we have identified three main strategies: (1) addition of metal/nonmetal dopants, (2) use of nanostructured organic/inorganic supports, and (3) the combination with other nanosized semiconductors.

**3.1.1. Doping Strategy.** Doping with metal/nonmetal ions was employed to improve the catalytic activity of nanomaterials through numerous sonophotocatalytic degradation investigations.<sup>20,59,60</sup> Metallic dopants increase catalytic performance by forming impurity energy levels in the band gap. Equations 19 and 20 describe how incorporated metallic ions participate in the photocatalytic process of semiconductors. Mt<sup>n</sup> represents metallic ion-doped nanocatalysts. They help with photocatalysis process mainly on two aspects: (i) increasing photon-absorption from the light source and/or SL and (ii) considerably reducing the  $e^-/h^+$  recombination rate. Additional electron and hole states are formed in the nanostructure, which facilitates the  $e^-$  and  $h^+$  transfer between the metallic dopant and the nanosized semiconductor (see eqs 21 and 22).

$$Mt^{n+} \xrightarrow{SL/h\nu} Mt^{(n+1)} + e_{CB}^{-}$$
(19)

$$\operatorname{Mt}^{n+} \xrightarrow{\operatorname{SL}/h\nu} \operatorname{Mt}^{(n-1)} + \operatorname{h_{VB}}^{+}$$
 (20)

$$Mt^{n+} + h_{VB}^{+} \to Mt^{(n+1)+} (hole trap)$$
(21)

$$Mt^{n+} + e_{CB}^{-} \rightarrow Mt^{(n-1)+}$$
(electron trap) (22)

Tabasideh et al.<sup>20</sup> synthesized Fe-doped TiO<sub>2</sub> pseudospherical nanoparticles for the degradation of diazinon as a persistent organophosphorus pesticide in aquatic media. They achieved considerably greater degradation efficiency (85%) than using pristine TiO<sub>2</sub> (reported to be ~50%) while using a sonophotocatalytic process. Similar results were obtained by Yap et al.<sup>16</sup> They degraded paracetamol by pubs.acs.org/nanoau



**Figure 6.** (A) Addition of dopants to achieve higher sonophotocatalytic potential: Ag-doped h-MoO<sub>3</sub> nanorods for the degradation of MB under diffused sunlight and ultrasonic irradiation. (B) Diffuse reflectance spectra (DRS) of MoO<sub>3</sub> and Ag-doped MoO<sub>3</sub> nanorods. (C) Tauc plots of MoO<sub>3</sub> and Ag-doped h-MoO<sub>3</sub> nanorods. (D) Introduction of nanosubstrates (CNTs) for catalytic performance improvement: WO<sub>3</sub>/CNT nanocatalyst for the decontamination of tetracycline from aquatic solution. (E) EIS patterns of WO<sub>3</sub> and WO<sub>3</sub>/CNT samples. (F) Type II heterojunction, (G) indirect Z-scheme using mediators, and (H) direct Z-scheme (mediator-free) charge transfer mechanisms at the interface. (A–C) Reproduced with permission from ref 61. Copyright 2017 Elsevier (D–E). Reproduced with permission from ref 71. Copyright 2020 Elsevier. (F–H) Reproduced with permission from ref 82. Copyright 2017 Wiley Online Library.

means of sonophotocatalysis using Fe-doped TiO<sub>2</sub> nanoparticles and achieved full 100% degradation efficiency in 30 min. They created trapping sites in the TiO<sub>2</sub> lattice, slowing down the  $e^+/h^-$  recombination rate. The doped catalyst exhibited  $\sim 2$  times improvement compared to pristine TiO<sub>2</sub> in the sonophotocatalytic degradation process. Paul et al.<sup>61</sup> synthesized Ag-doped flower-like hierarchical molybdenum oxide  $(h-MoO_3)$  nanorods and utilized them for the degradation of MB under diffused sunlight and ultrasonic irradiation. As seen in Figure 6A, Ag acts as an electron trap, captures electrons that migrate to the CB of h-MnO<sub>3</sub> and suppress the  $e^-/h^+$  recombination. The captured electrons can then react with oxygen to produce superoxide radicals. Agdoped h-MnO<sub>3</sub> nanorods degraded 98% of MB in 90 min, while nondoped nanorods showed 97.8% degradation efficiency in 150 min. The 40% decrease in the reaction time clearly revealed the advantage of Ag doping. This can be

explained with the reduction of the h-MoO<sub>3</sub> band gap and the dramatically increased absorption in the Vis region (see Figure 6B,C). Rajoriya et al.<sup>62</sup> employed Sm-doped TiO<sub>2</sub> for the acoustic cavitation-assisted photodegradation of 4-acetamidophenol. They reported ~30% enhancement in the 4-acetamidophenol degradation efficiency.

Non-metal dopants can also enlarge the absorption range of Vis light, significantly increase charge carriers' separation, and reduce  $e^-/h^+$  recombination due to the introduction of localized electronic states above semiconductor's VB in the bandgap.<sup>63</sup> Kumawat et al.<sup>64</sup> synthesized an N-doped ZnO nanorod-like structure and employed it in the degradation of nigrosine under simultaneous ultrasonic and Vis light irradiations. The sonophotocatalytic degradation rate constants for N-doped and undoped ZnO were  $7.33 \times 10^{-4}$  and  $4.6 \times 10^{-4} s^{-1}$ , respectively. Rajoriya et al.<sup>62</sup> employed N-doped TiO<sub>2</sub> spherical nanoparticles with a porous structure for

acoustic cavitation assisted photodegradation of 4-acetamidophenol and also achieved a higher degradation efficiency (91%) compared to undoped  $\text{TiO}_2$  (~79%). Additionally, sonophotocatalysis yielded a maximum degradation efficiency in 4-acetamidophenol under optimized conditions of 91% within 180 min. However, when using only photocatalytic oxidation, only 63% of degradation rate was achieved.

An additional strategy that a few groups have adopted is codoping.<sup>17,53,65</sup> This grants important synergic effects, changes both the transfer and recombination dynamics of charge carries, and shifts light adsorption spectra to the Vis light region due to interactions between dopants within the crystalline matrix of nanocatalysts.

3.1.2. Using Nanostructured Substrates. Loading nanoscale semiconductors onto nanostructured supports has been reported to be an effective strategy to improve the sonophotocatalytic performance of nanocatalysts. Nanostructured supports feature a high specific surface area. They can help prevent nanoparticle agglomeration, which is a quite common issue of nanoparticles, during the catalytic processes or washing/redispersion steps between cycles. Moreover, they provide a higher capacity for adsorption of organic pollutants and increase the chance of surface reactions as well as act as an acceptor of sono/photoinduced reactive species, significantly suppressing the e<sup>-</sup>/h<sup>+</sup> recombination in nanoparticle catalysts.<sup>66</sup> Specifically, in sonophotocatalysis, continuous ultrasonic irradiation helps to reduce nanocatalyst agglomeration in solution to a certain extent. But, the negative side is that it may also cause the detachment of integrated nanocatalysts from the support. For example, Zeng et al.<sup>19</sup> reported a higher Mo leaching content of MoS<sub>2</sub> nanosheets grown on carbon layers in sonophotocatalytic elimination of levofloxacin when compared to the photocatalytic treatment employing peroxymonosulfate as an enhancer. Keeping this in mind, the nanocatalyst-substrate bonding should be sufficiently strong to avoid the nanocatalyst loss from the substrate surface to the solution and to increase the beneficial effect of the substrate's introduction. Hayati et al.<sup>10</sup> fabricated mesoporous hexagonal MgO nanocrystals onto CNT using a multistep fabrication method that started with the hydrothermal treatment of Mg(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O and Na<sub>2</sub>CO<sub>3</sub> followed with a calcination step and ultrasonic-assisted hydrothermal treatment. This nanocomposite was employed for the degradation of sulfadiazine (pharmaceutical pollutant) under ultrasonic and UV light irradiation, which exhibited 38.8% higher degradation efficiency than pristine MgO under the same conditions. The authors attributed the improved performance to the increased specific surface area, the reduction of  $e^-/h^+$  recombination rate, and the inhibitory effect of CNTs as a substrate from agglomeration of MgO nanoparticles.

Zeolites are crystalline aluminosilicates with microporous (4–14 Å) structures that have been widely used as hybrid adsorbents and catalysts.<sup>67,68</sup> They possess unique chemical and structural properties including high surface area, high adsorption capabilities, and adjustable surface properties.<sup>67</sup> Having uniform pores and channel sizes, zeolites can serve as hosts for entrapping nanosized semiconductors and preventing the agglomeration of nanocatalysts.<sup>69,70</sup> Jorfi et al.<sup>66</sup> performed a comparative study on a sonophotocatalytic treatment of a textile industrial effluent using nanosized MgO spherical-shaped nanoparticles grafted on zeolite. The MgO@zeolite/UV/US system exhibited a much higher degradation rate (78%) than those of MgO/UV/US and MgO@zeolite/UV

systems, with only 43%, and 49% elimination rates, respectively. These results highlight the importance of the zeolite as well as the binary use of US and UV systems to take advantage of both the sonocatalytic and photocatalytic mechanisms. Also, MgO nanoparticles showed a minimal loss of <0.3 mg/L after the treatment under optimum conditions, confirming the excellent physicochemical stability of MgO@ zeolite in sonophotocatalysis processes.

Isari et al.<sup>71</sup> synthesized WO<sub>3</sub> nanocuboids coupled with CNTs for the decontamination of tetracycline, where CNTs acted as a substrate (see the molecular structure and charge transfer pathway in Figure 6D). They achieved the excellent introduction of CNTs into the WO3 framework. The outstanding activity of this nanocomposite was demonstrated by the total elimination of tetracycline in 60 min, outperforming the individual photocatalytic and sonocatalytic processes with 48.56% and 45.92% degradation efficiencies. The reduced radius of the semicircle in electrochemical impedance spectroscopy (EIS) Nyquist plot revealed the increased interfacial charge transfer in the composite (Figure 6E). The authors believed that the interfacial bonding (W–C or/and W-O-C) formed between WO<sub>3</sub> and CNTs allowed for the photogenerated electrons to be transferred to CNTs with very low resistance. In this case, the substrate contributed to the catalytic performance by reducing the  $e^{-}/h^{+}$ recombination rate.

3.1.3. Coupling with Other Semiconductors. Another promising strategy for increasing photon absorption from light source or SL is coupling a nanoscale semiconductor with another lower band gap semiconductor. When they are in contact with each other, semiconductors with different Fermi levels form heterojunctions at the interface, which leads to the formation of an internal electric field. This electric field can direct the movement of electrons and holes through the interfacial zone.<sup>72,73</sup> The most investigated and desired heterojunction for photocatalysis and sonophotocatalysis is known as type II. In the conventional type II heterojunction, the holes and electrons kinetically flow upward and downward, respectively, which effectively facilitates e<sup>-</sup>/h<sup>+</sup> separation (Figure 6F). Aghaei et al.<sup>74</sup> synthesized ZnO/CuO sphericalshaped nanoparticles with an average particle size of 32 nm by coprecipitating zinc nitrate and copper(II) nitrate for the removal of parathion from wastewater. The total degradation of parathion was achieved after 60 min of simultaneous ultrasonic and light irradiation. They also evaluated the beneficial effect of the addition of CuO to ZnO crystalline nanostructure and found that a ZnO/CuO (90:10) mixture exhibited higher sonophotocatalytic activity than pure ZnO nanoparticles. Under optimized conditions, the sonophotocatalytic reaction rate constant was 1.36 times higher than that from photocatalysis. A similar charge transfer mechanism coupled with synergism between the UV and US processes was also shown by Eshaq et al.<sup>75</sup> in a study on hydrothermally prepared FeVO<sub>4</sub>@BiOCl (nanorods/nanoflowers with a core@shell heterojunction structure) for the efficient sonophotocatalytic degradation of *p*-nitrophenol. Guo et al.<sup>76</sup> fabricated brush-like ZnO nanorod arrays on a stainless-steel mesh and subsequently transformed them into ZnO/ZnS core@shell nanorods and nanotubes to investigate the effectiveness of heterojunction and the sonophotocatalytic degradation capability for the MB removal. For over 50 min of reaction, the removal capability of ZnO/ZnS core@shell nanorods (45.4%) was remarkably higher than that of ZnO



**Figure 7.** (A) Fabrication and (B) charge transfer mechanism of  $N/Ti^{3+}$  codoped biphasic  $TiO_2/Bi_2WO_6$  composite heterojunctions for MB decontamination. (C) Diffuse reflectance spectrum and (D) Tauc plot of  $TiO_2$ ,  $NT-TiO_2$ , and  $NT-TBW_x$  samples. (E) Sonophotocatalytic activities of  $Bi_2WO_6$ ,  $TiO_2$ ,  $NT-TiO_2$ , and different NT-TBW<sub>x</sub> composite samples. (F) Comparative studies of sonophotocatalytic degradation of MB in different modes. Reproduced with permission from ref 17. Copyright 2020 Elsevier.

nanorods (25.1%), suggesting that the interfacial polarization field induced by the ZnO/ZnS heterojunction increased the sonophotocatalytic efficiency. As the nanorods were transformed into nanotubes, they exhibited a higher degradation rate (63.3%) due to the coupling effect of the enhanced piezoelectric field and the reduced migration distance, which suppressed the recombination of photoexcited electron-hole pairs. This study not only shed light on the importance of forming efficient heterojunctions in sonophotocatalysts but also indicated that morphology can play an important role in the performance of sonophotocatalysts.

Another interesting, increasingly explored charge transfer mechanism is indirect Z-scheme type, through which the excited electrons of photocatalyst II (PCII) are transferred downward to recombine with the holes on photocatalyst I (PCI) using an electron mediator (Figure 6G). These mediators can be either conductors (i.e., metal nanoparticles, CNT or graphene), which act as low resistive electron highways or redox pairs (i.e.,  $Co^{3+}/Co^{2+}$  and  $Fe^{3+}/Fe^{2+}$ ).<sup>77,78</sup> In Z-scheme systems, unlike conventional type II hetero-

junction composites, the reduction and oxidation reactions are driven by electrons at the CB of PCI with a higher redox potential and holes located at the VB of PCII with a higher oxidation potential, respectively.<sup>79</sup>

The recently emerged direct Z-scheme catalytic systems, without engaging any mediators, have also been applied to both sonocatalysis and photocatalysis and demonstrated outstanding catalytic properties. The charge transfer mechanism is exactly the same as the above-mentioned indirect Zscheme heterojunction (Figure 6H).<sup>80,81</sup> The electrons left at the CB of PCI and holes at the VB of PCII, with the highest reduction and oxidation potentials, respectively, are capable of participating in radical-producing reactions much more effectively. However, in the direct Z-scheme heterojunction, the shielding effect and the backward reactions are mostly hindered due to the absence of mediators.<sup>82</sup> In spite of all these favorable factors, rational construction of the direct Z-scheme system with an intimate interface and effective charge transfer remains challenging. It should be also mentioned that there are many articles on the Z-scheme sonocatalytic or photocatalytic

processes, but to the best of our knowledge there is no available comprehensive information about the integrated Zscheme sonophotocatalytic systems, which may be worthwhile to be investigated in detail in future studies.

It is common to use the combination of these modification strategies for the fabrication of desirable sonophotocatalysts. Sun et al.<sup>17</sup> fabricated N/Ti<sup>3+</sup> codoped biphasic TiO<sub>2</sub>/Bi<sub>2</sub>WO<sub>6</sub> composite heterojunctions (denoted as NT-TBW<sub>x</sub>) by a single hydrothermal treatment (see Figure 7A), for the decontamination of MB, p-nitrophenol, RhB, and levofloxacin. The nanocomposite was composed of nanoparticles of biphasic TiO<sub>2</sub> (both anatase and rutile phases) and Bi<sub>2</sub>WO<sub>6</sub> nanosheets with a lamellar structure. Although TiO<sub>2</sub> is a UV light responsive photocatalyst, N atoms and Ti<sup>3+</sup> can create impurity levels above the VB and continuous local states below the CB of TiO<sub>2</sub>, respectively (see Figure 7B). Both can result in TiO<sub>2</sub> exhibiting the Vis light response. Results shown in Figure 7C,D confirm that the band gap value of TiO<sub>2</sub> was reduced from 3.10 to 2.47 eV by incorporating  $N/Ti^{3+}$  and that the resulting catalysts absorbed both UV and Vis light. The combined effect of dopants and the charge transfer mechanism at the interface TiO<sub>2</sub>/Bi<sub>2</sub>WO<sub>6</sub> resulted in superior performance compared to other samples. Figure 7E depicts the comparative study that confirmed the synergistic effect among the heterojunctions, heterophase junction (anatase/rutile), and doping level. Since codoped composite samples  $(NT-TBW_r)$  had a higher light response and e<sup>-</sup>/h<sup>+</sup> separation rate, their sonophotocatalytic performance was superior to that of  $N/Ti^{3+}$  codoped  $TiO_2$  and pure TiO<sub>2</sub>. In addition, the improved sonophotocatalytic degradation performance showed a positive synergism between sonocatalysis and photocatalysis (see Figure 7F). Over 50 min of reaction time, the degradation rate of MB by the sonophotocatalytic process is 98%, which is 1.09- and 1.52fold greater than the degradation rates by sonocatalytic and photocatalytic techniques alone.

Babu et al.<sup>83</sup> fabricated CuO-TiO<sub>2</sub>/rGO (rGO: reduced graphene oxide) for ultrasonic-assisted photocatalytic degradation of methyl orange dye. They found that both graphene oxide nanosheets and Cu played a crucial role in the system due to (i) band gap energy shifting from 3.23 to 3.08 eV as a function of Cu loading; (ii) rGO acting as electron acceptor and transfer bridge, improving charge mobility; and (iii) rGO providing a highly active surface area for the effective adsorption of organic pollutants. Similarly, such improvements made by the combination of these strategies have been reported in the literature.<sup>27,53</sup>

#### **3.2. Process Modifications**

Any additional source for generating reactive species can boost sonophotocatalytic activities. In the following, various process enhancement techniques are described.

The sparging of gases  $(N_2, Ar, O_2)$  enhances the performance of the system by generating high-potential bubble formation sites. This increases the rate of cavitation events and greatly influences the amount of produced H<sub>2</sub>O<sub>2</sub>, which can indeed actively participate in and contribute to the photocatalytic degradation process. Therefore, the number of cavitation bubbles will be in a direct relationship with the amount of sparged gas. Previous studies confirmed the positive effect of aeration on ultrasonic-produced degradation mechanisms.<sup>15,84</sup> It has been shown that Ar offers a better performance compared to N<sub>2</sub> thanks to its better solubility in water and a higher heat capacity ratio.<sup>85</sup> Another possible

reason for relatively lower performance is  $N_2$ 's scavenging effect, leading to less reactive species available for the photocatalytic reaction. Moreover, as shown in previous sections,  $O_2$  can act as a scavenger agent for excited electrons on the CB, results in more production of  $O_2^{\bullet-}$  and diminish the rate of  $e^-/h^+$  recombination. Also, by further reacting with other existing species in solution, extra amounts of radicals like  $HO_2^{\bullet}$  will be generated (eqs 23–25).

$$O_2 + e^- \to O_2^{\bullet-}$$
(23)

$$H_2 O \xrightarrow{US} H^{\bullet} + O H^{\bullet}$$
(24)

$$O_2 + H^{\bullet} \to HO_2^{\bullet} \tag{25}$$

The ultrasonic-produced shock waves have a positive effect on boosting the production of reactive agents in the solution and enhancing the influence of aeration as an intensifier (eqs 26-28).<sup>86</sup>

$$O_2 \xrightarrow{US} 2O^{\bullet}$$
 (26)

$$O^{\bullet} + HO_2^{\bullet} \to OH^{\bullet} + O_2$$
(27)

$$O_2 + O^{\bullet} \to O_3 \tag{28}$$

To investigate the effect of gas purging, Dinesh et al.<sup>85</sup> selected a solution of 10 ppm of Basic Brown 1 dye for sonophotocatalytic treatment system using Fe-doped  $Bi_2O_3$ . Each experiment was carried out by bubbling the reaction mixture with Ar, air,  $O_2$ , and  $N_2$ , separately. According to the results, Ar bubbling exhibited the highest decontamination performance of 17% for 37 kHz, 13% for 22 kHz, and 8% for the UV-only case. These efficiencies were higher than those of  $N_2$ , air, and  $O_2$ . The overall positive synergism was also observed in the integrated sonophotocatalytic system.

By using  $H_2O_2$  as an individual enhancer, a large number of free and adsorbed radicals can be released in the medium. Besides, it can act as an electron trap to suppress  $e^-/h^+$  recombination (eqs 29–32).<sup>87</sup>

$$H_2O_2 \xrightarrow{h\nu/SL/US} 2OH^{\bullet}_{free}$$
(29)

$$H_2O_2 + e^- \to OH^- + OH^{\bullet}_{ads}$$
(30)

$$\mathrm{H}_{2}\mathrm{O}_{2} + \mathrm{OH}^{\bullet} \to \mathrm{H}_{2}\mathrm{O} + \mathrm{HO}_{2}^{\bullet} \tag{31}$$

$$H_2O_2 + O_2^{\bullet-} \rightarrow OH^- + OH^{\bullet} + O_2$$
(32)

Rahman et al.<sup>60</sup> explored the effect of  $H_2O_2$  addition on the chemical oxygen demand (COD) removal of palm oil mill effluent using C–N codoped black TiO<sub>2</sub> under Vis light and US irradiations. According to the obtained results, the sonophotocatalytic elimination of COD improved from 67.69% to 75.48% by the addition of 1.0 mM  $H_2O_2$ . When the  $H_2O_2$  concentration was increased to 2.0 mM, the COD removal efficiency rate went up to 84.63%. However, as  $H_2O_2$  increased beyond 2.0 mM, the removal efficiency decreased dramatically, which was attributed to the radical scavenging effect of  $H_2O_2$  molecules.

Owing to the high oxidation potential of  $O_3$  (~2.08 eV), ozonation has been utilized for production of reactive species either alone or as an enhancer in combination with US-activated or/and light-activated degradation systems.<sup>88,89</sup> A series of reactions will be initiated be the presence of  $O_3$  (eqs 33–37).



Figure 8. Schematic illustration of enhancer-enhanced sonophotocatalytic degradation of Azorubine dye using PDS and Fe<sup>2+</sup>. Reproduced with permission from ref 93. Copyright 2017 Elsevier.



Figure 9. Some of the typical (A) batch and (B) continues sonophotocatalytic reactors. Reproduced with permission from ref 89. Copyright 2004 John Wiley and Sons.

$$O_3 + h\nu/u \text{trasonic} \rightarrow O_2 + O$$
 (33)

$$O + H_2 O \to 2OH^{\bullet} \tag{34}$$

$$O_3 + OH^{\bullet} \to HO_2^{\bullet} + O_2 \tag{35}$$

$$\mathrm{HO}_{2}^{\bullet} \to \mathrm{O}_{2}^{\bullet-} + \mathrm{H}^{+}$$
(36)

$$OH^{\bullet} + O_2^{\bullet-} \to OH^- + O_2 \tag{37}$$

Acoustic streaming and turbulence generated by US waves can effectively break the mass transfer boundaries associated with ozonation, leading to further adsorption of  $O_3$  in the solution. It is also notable that the existence of  $H_2O_2$  species enlarges the share of  $O_3$  in production of reactive agents in the solution (eqs 38 and 39).

$$\mathrm{H}_{2}\mathrm{O}_{2} \to \mathrm{HO}^{2^{-}} + \mathrm{H}^{+} \tag{38}$$

$$O_3 + HO^{2-} \rightarrow O_2^{\bullet-} + OH^{\bullet} + O_2$$
(39)

Sulfate radicals with excellent oxidizing potential (2.6-3.1 V) can be released in the solution by activation of peroxydisulfate (PDS) and peroxymonosulfate (PMS) enhancers.<sup>90,91</sup> Both of them release sulfate radicals (with higher oxidation potentials than OH<sup>•</sup> (1.8–2.7 V)) and react with other ions in the solutions to produce OH<sup>•.54</sup> Ultrasonication waves can also degrade persulfate species into sulfate radicals according to eqs 40–47.

$$S_2 O_8^{2-} \xrightarrow{US}{\rightarrow} 2SO_4^{\bullet-}$$
 (40)

$$S_2 O_8^{2-} + O_2^{\bullet-} \to S O_4^{2-} + S O_4^{\bullet-} + O_2$$
 (41)

$$HSO_5^{-} \xrightarrow{h\nu/SL} SO_4^{\bullet-} + O_2$$
(42)

$$HSO_5^- + e^- \to OH^{\bullet} + SO_4^{2-}$$
(43)

$$HSO_5^- + e^- \to OH^- + SO_4^{\bullet-}$$
(44)

$$\mathrm{HSO}_{5}^{-} + \mathrm{h}^{+} \to \mathrm{SO}_{5}^{\bullet-} + \mathrm{H}^{+}$$
(45)

$$2SO_5^{\bullet-} + h^+ \rightarrow 2SO_4^{\bullet-} + O_2 \tag{46}$$

$$\mathrm{SO}_4^{\bullet-} + \mathrm{OH}^- \to \mathrm{OH}^{\bullet} + \mathrm{SO}_4^{2-}$$
 (47)

Fenton-like reactions could provide the reaction media with extra numbers of radical species. Ferrous ions react with *in situ*produced H<sub>2</sub>O<sub>2</sub> during sonophotocatalytic reactions to provide additional free radicals and facilitate the degradation of dissolved organics. An optimum amount of Fe<sup>2+</sup> could be converted to Fe<sup>3+</sup> by reacting with H<sub>2</sub>O<sub>2</sub> in the presence of UV or/and US to produce OH<sup>•</sup> (eqs 48–52).<sup>38</sup>

$$Fe^{3+} + H_2O_2 \rightarrow Fe(OOH)^{2+} + H^+$$
 (48)

$$\operatorname{Fe(OOH)}^{2+} \xrightarrow{h\nu/\operatorname{SL}} \operatorname{Fe}^{2+} + \operatorname{OH}^{\bullet}$$
 (49)

$$Fe(OOH)^{2+} \rightarrow Fe^{2+} + HO_2^{\bullet}$$
(50)

$$Fe^{2+} + O_2 \to Fe^{3+} + O_2^{\bullet-}$$
 (51)

$$\mathrm{Fe}^{2+} + \mathrm{H}_2\mathrm{O}_2 \to \mathrm{Fe}^{3+} + \mathrm{OH}^{\bullet} + \mathrm{OH}^{-}$$
(52)

However, the excessive amount of  $Fe^{2+}$  could diminish catalytic activity due to its competition with organic materials, which tend to react with radical species in the solution.<sup>92</sup> It can

also quench radicals when used simultaneously with PDS or PMS. For example, Chakma et al.<sup>93</sup> reported a clear schematic synergy function of Fe<sup>2+</sup> and PDS enhancers when used in the degradation of Azorubine dye (Figure 8). They also confirmed that  $SO_4^{\bullet}$  can be scavenged by Fe<sup>2+</sup> ions.

## 3.3. Reactor Design

Reactor design is considered one of the main factors in developing sonophotocatalytic treatment systems, influencing both process efficiency and overall cost of a system. Parts A and B of Figure 9 show some of the batch and continuous sonophotocatalytic reactors reported so far.<sup>28,89</sup> Some key features should be taken into account in their design to reach maximum efficiency.<sup>15,89,94</sup> The first one is the light source mode. It is notable that the type of light irradiation (indirect or direct) does not influence the synergism, giving considerable flexibility in their design. However, two other points must be taken into consideration: (i) uniform irradiation must be delivered to all the particles inside the reaction solution and (ii) light and US must be applied simultaneously rather than sequentially. Second, in terms of reactor type, continuous- or/ and recirculation-equipped reactors are preferred in wastewater treatment compared to batch reactors due to higher treatment capacity, feasibility, and scale-up potential. Nevertheless, in terms of instrument cost, continuous reactors are more expensive than batch reactors in general, because they involve more system components. When lower doses of photocatalysts are used or/and photocatalyst separation is easy, slurry reactors can be used; otherwise, supported or immobilized catalyst reactors are preferred.<sup>94</sup> Multiple-frequency sonophotocatalytic reactors achieve higher efficient decontamination of wastewaters compared to single transducer or/and frequency operation, given their more uniform and intense energy transfer. Ye et al.95 found that cavitation bubbles are much easier to collapse in dual-frequency ultrasonic field than those operated in the single-frequency mode.

#### 4. SYNERGY

Employing the above-mentioned photo- and sono-activated mechanisms by combining photocatalysis and sonocatalysis lead to excellent synergistic effects on pollutant removal, which would not be achieved by applying them individually. As a quantitative measurement to evaluate the enhancement factor of integrated systems, the synergism between the processes can be calculated by the following equations:<sup>38</sup>

synergy index = 
$$\frac{K_{(X+UV+US)}}{K_{(X+UV)} + K_{(X+US)}}$$
(53)

synergy (%) = 
$$\frac{K_{(X+UV+US)} - (K_{(X+UV)} + K_{(X+US)})}{K_{(X+UV+US)}} \times 100$$
(54)

where  $K_{(X+UV)}$ ,  $K_{(X+US)}$ , and  $K_{(X+UV+US)}$  denote the reaction rate constants of photocatalytic, sonocatalytic, and sonophotocatalytic reactions and X is the type of catalyst. It should be noted that, to avoid any possible false conclusions, all formulas should be calculated by reaction rate constants instead of degradation percentages. Accordingly, by addition of additives and enhancers, the above-mentioned formula would be converted to eq 55.<sup>19</sup>



**Figure 10.** (A) SEM and (B) TEM images of CZ0.75 M. (C) Tauc plots of  $ZrO_2$ ,  $CeO_2$ ,  $MoS_2$ ,  $CeO_2-ZrO_2$ , and CZ0.75 M. (D) Pseudo-firstorder reaction rate constants of naproxen sonophotocatalytic degradation reactions in controlled experiments under optimum experimental conditions (catalyst dosage, 0.5 g/L, pH = 5.8; initial naproxen concentration, 10 mg/L; US frequency, 970 kHz; US power, 300 W; and light intensity, 0.17 mW/cm<sup>2</sup>. ESR spectra of (E) DMPO-OOH and (F) DMPO-OH spin adducts under Vis (blue), US (red), and US/Vis (black) irradiations. (G) Schematic charge transfer mechanism of CZ0.75 M and sonophotocatalytic degradation of naproxen. Reproduced with permission from ref 98. Copyright 2021 Elsevier.

synergy index = 
$$\frac{K_{(X+Y+UV+US)}}{K_{(X+Y+UV)} + K_{(X+Y+US)}}$$
(55)

Eshaq et al.<sup>96</sup> reported a great synergism between binary irradiation of UV and US leading to complete decontamination of 4-nitrophenol (20 mg/L) using FeVO<sub>4</sub>@CeO<sub>2</sub> (0.1 g/L) as the catalyst and H<sub>2</sub>O<sub>2</sub> (10 mM) as an enhancer at pH = 7. Clearly, combining sonolysis with photocatalytic technique coupled with H<sub>2</sub>O<sub>2</sub> and heterogeneous Fenton reaction shortened the reaction time to 30 min with excellent synergy percentage of 28.9% (using eq 54). A study by Lops et al.<sup>58</sup> shows that coupling sunlight and ultrasonic irradiation in a sonophotocatalytic approach resulted in complete removal of

RhB in just 10 min by using micro- and nanosized ZnO as catalysts, demonstrating an excellent synergy between the two individual processes. This impact was shown by the great increase in the kinetic rate constant of about 56 and 13 times. In addition, there was a notable decrease of the half-lifetime (the required time to eliminate the 50% of the initial RhB concentration) of about 98% and 92%, compared to sole sonocatalytic and photocatalytic systems, respectively. Selvamani et al.<sup>97</sup> reported a synergy value of 3.83 and 1.71 for sonophotocatalytic degradation of tetracycline and ciprofloxacin antibiotics when using a  $Cu_2O/MoS_2/rGO$  nanocomposite within short times of 10 and 75 min, respectively.

			Reaction rate constant (min <sup>-1</sup> )			Energy power (W)			E <sub>EO</sub> (kWh/m <sup>3</sup> * order)			Costs (S)						
Power source	Enhancer	Catalyst	Contaminant	V solution (L)	K UV/cat	K US/Cat	K (UV/US/Cat)	P <sub>UV</sub>	Pus	P (UV/US/Cat)	E <sub>EO</sub> UV/Cat	E <sub>EO</sub> US/cat	E <sub>EO</sub> (UV/US/Cat)	Cost UV/Cat	Cost US/Cat	Cost (UV/US/Cat)	Synergy index	Ref
Halogen lamp + 40 kHz US bath	-	Cu <sub>2</sub> O/MoS <sub>2</sub> /rGO	Tetracycline	0.1	0.03	0.018	0.184	150	120	270	1920	2560	563.479	184.3	245.8	54.1	3.83	[97]
160 Hg 420 nm lamp + 20 kHz titanium probe sonicator		ZnO/CNT	МВ	0.1 for UV/ 0.2 for US	0.015	0.0171	0.0198	160	60	220	4096	673.684	2133.333	393.2	64.7	204.8	0.617	[105]
160 W Hg lamp 420 nm filter	H <sub>2</sub> O <sub>2</sub> assisted	ZnO/CNT	4- nitrophenol	0.1 for UV/ 0.2 for US	0.06	0.15	0.3	160	60	220	1024	76.8	140.8	98.3	7.4	13.5	1.429	[106]
High-pressure Xe lamp+ bottom US generator (40 kHz) MoS	$MoS_2$	Levofloxacin	0.1	0.0239	0.0022	0.0389	2.4	70	72.4	38.561	12218.182	714.694	3.7	1172.9	68.6	1.49	[19]	
	MoS <sub>2</sub> /C	Levofloxacin	0.1	0.0247	0.0021	0.0702	2.4	70	72.4	37.312	12800	396.034	3.6	1228.8	38	2.62		
16w UVC lamp + bottom US transducer	-	P25	Bisphenol A	1.1	0.006	0.007	0.028	16	50	66	93.090	249.351	82.286	8.9	23.9	7.9	2.154	[107]
8W UVC lamp +13 mm titanium probe	Fenton assisted	FeVO4@BiOCl	p-nitrophenol	0.11	0.0403	0.031	0.112	8	125	133	69.298	1407.625	414.545	6.7	135.1	39.8	1.571	[75]
6W UVC lamp +125 W US wave 13 mm titanium prob		FeOCl (I)		ene 0.11	0.0479	0.0217	0.0892	6	125	131	43.727	2010.8923	512.678	4.2	193	49.2	1.28	[103]
	Fenton	CuOCl (II)	Nitrahamana		0.0373	0.0161	0.0635				56.154	2710.333	720.172	5.4	260.2	69.1	1.189	
	assisted	BiOCl (IV)	Nitrobenzene		0.03	0.0141	0.0484				69.818	3094.778	944.853	6.7	297.1	90.7	1.091	
		ZnOCl (III)	1		0.0259	0.0115	0.0426				80.870	3794.466	1073.495	7.8	364.3	103.1	1.139	
25 W UVC lamp +4 cm in diameter pizo-electeriz disk as US irradiation source	-	FePO <sub>4</sub>	Methyl violet 2B	0.5	0.0229	0.0068	0.0397	25	80	105	83.843	903.529	203.123	8.1	86.7	19.5	1.33	[109]
14.4 W/m blue LED light+95 W US bath	-	Ce:Cu-1,4-BDO AH2	Diazinon	0.05	0.138	0.059	0.279	14.4	95	109.4	80.139	1236.610	301.144	7.7	118.8	28.9	1.41	[14]
240 W LED lamp US bath (Ultech, 40 and 970 kHz, 300 W)	-	CeO <sub>2</sub> - ZrO2@MOS <sub>2</sub>	Naproxen	0.05	0.007	0.014	0.077	250	30 <b>0</b>	550	27428.571	16457.143	5485.714	2633.1	1579.9	526.6	3.67	[58]

Table 1. Summary of Cost Estimation of Photocatalytic, Sonocatalytic, and Sonophotocatalytic Degradation of Contaminants<sup>14,19,75,97,98,105–109</sup>, *a* 

<sup>a</sup>Electricity rate was assumed to be \$0.096 per kWh according to average electricity price for businesses in Canada, March 22. Source: www. globalpetrolprices.com. Materials' costs are not included.

Talukdar et al.<sup>98</sup> constructed CeO<sub>2</sub>-ZrO<sub>2</sub>@MoS<sub>2</sub> (CZ0.75 M) nanoflowers for naproxen sonophotocatalytic degradation. The morphological characteristics of the hybrid nanostructure CZ0.75 M were validated by field emission scanning electron microscopy (FESEM) micrographs and TEM images (Figure 10A,B).  $CeO_2$ -ZrO<sub>2</sub> hybrids were grown uniformly between and on the exterior of the  $MoS_2$  nanosheets in the CZ0.75 M. The CZ0.75 M ternary composite has a band gap of 1.60 eV lower, when compared to ZrO<sub>2</sub>, CeO<sub>2</sub>, and CeO<sub>2</sub>-ZrO<sub>2</sub> (Figure 10C). The low band gap energy of  $MoS_2$  (1.30 eV) shortened the overall band gap of the hybrid material by interaction with CeO<sub>2</sub>-ZrO<sub>2</sub> and defect energy states. The presence of these defects and oxygen vacancies from Ce<sup>3+</sup> formation not only promoted a rapid charge carrier migration but also maximized the solar spectrum utilization. The sonophotocatalytic degradation of naproxen by the CZ0.75 M achieved 96% degradation efficiency within 40 min. It had a synergistic effect of 72.7%, resulting in 11- and 5.5-times greater degradation efficiencies than the individual sonocatalytic and photocatalytic experiments, respectively (Figure 10D). According to the electron spin resonance (ESR) results shown in Figure 10E,F, in the US/Vis/CZ0.75 M system, DMPO-OOH (DMPO: 5,5-dimethylpyrroline-N-oxide) and DMPO-OH spin adduct signals were stronger than in the Vis and US alone system. US irradiation of the solution resulted in SL and the conversion of microbubble cavitation energy into optical energy, which enhanced the production of radical species. Figure 10G shows the schematic charge transfer mechanism of the CZ0.75 M and sonophotocatalytic degradation of naproxen. As seen, by forming an efficient ternary heterojunction among CeO<sub>2</sub>, ZrO<sub>2</sub>, and MoS<sub>2</sub>, electrons can easily migrate through the interfaces, reducing charge recombination. Electrons on the CB of MOS<sub>2</sub> can easily react with O<sub>2</sub> to produce radical species and holes at the VB of ZrO<sub>2</sub> can form OH<sup>•</sup> species by reacting with water molecules.

## 5. ELECTRICAL ENERGY CONSUMPTION

In full-scale applications, the available resources and economic considerations are of high importance. Only a limited number of articles have been published on the sonophotocatalysis for wastewater treatment.<sup>13,64</sup> Little is known about the economic aspects of this technique. In advanced oxidation processes (AOPs), the amount of electrical energy consumed is responsible for the major fraction of operating expenses. Using an extra electrical-energy-consuming source-ultrasonic device-in addition to the traditional photocatalytic system may raise questions about the performance and costeffectiveness. Defined by Bolton et al.99 and approved by IUPAC, the figures-of-merit of AOPs can be calculated for electrical-energy-driven systems numerically. These calculations are divided into two types: (i) electrical energy per mass  $(E_{\rm EM})$  and (ii) electrical energy per order of magnitude  $(E_{\rm EO})$ , which are suitable for situations where pollutant concentration is high and low, respectively.  $E_{\rm EO}$  is the electric energy in kilowatt hours [kWh] required to remove a pollutant by 1 order of magnitude (90%) in a unit volume [e.g., 1 m<sup>3</sup>] of polluted air or water. Low concentrations of contaminants and first-order degradation reactions are the prerequisites for using  $E_{\rm EO}$  to determine the electrical energy consumption of an AOP system. The pseudo-first order kinetics of a sonophotocatalytic reaction system can be described according to eq 56. Also, the  $E_{\rm EO}$  (kWh/m<sup>3</sup>·order) for an AOP can be calculated by eq 57.<sup>60</sup>

$$\log\left(\frac{[C_0]}{[C]}\right) = 0.4343K_{app}t$$

$$(56)$$

$$1000 \times P_a \times t$$

$$E_{\rm EO} = \frac{1000 \times T_{\rm e} \times T}{60 \times V \times \log\left(\frac{[C_0]}{[C]}\right)}$$
(57)

where  $K_{app}$  (min<sup>-1</sup>) is the pseudo-first order rate constant,  $P_e$  denotes the input power of electrical-energy-consuming source



**Figure 11.** (A) Different types of disinfection mechanisms under the combined effects of ultrasonication and photocatalysis. (B) Schematic mechanisms of disinfection of bacteria and different types of cell membrane perforation caused by acoustic cavitation. The numbers represent the following processes: (1) formation and collapse of cavitation bubbles; (2) production of reactive oxidative species by sonochemistry; (3) reactive species formation by sonoluminescence; (4) membrane perforation; (5) promote penetration of antibacterial agents; (6) transmembrane protein inactivation; (7) intracellular protein and enzyme inactivation; (8) DNA breakage; and (9) metabolism inhibition. Adapted with permission from ref 39. Copyright 2020 Elsevier.

(kW), V is the volume of the reaction solution (L), t represents time (s), and C and  $C_0$  are the concentrations of pollutant at time t and 0, respectively. The 1000 and 60 values are converting constants for kW to W and s to min conversion, respectively. For a pseudo-first reaction model reaction in a batch reactor, the above-mentioned equations can be simplified as it is described in eq 58.<sup>100</sup>

$$E_{\rm EO} = \frac{P_{\rm e} \times 38.4}{V \times K_{\rm app}} \tag{58}$$

There are plenty of studies that conducted electrical energy consumption analysis for photocatalytic and sonocatalytic degradation systems.<sup>101–103</sup> But, to the best of our knowledge, there are no review studies analyzing the electrical energy consumption of sonophotocatalytic systems. Using experimentally available data from the literature, the electrical energy consumption calculations were carried out for some of previous investigations. Table 1 summarizes key parameters and data, including all energy consumption data translated into cost values. It can be noticed that, in all cases, the  $E_{\rm EO}$  of sonophotocatalytic system is lower than the sum of photocatalytic and sonocatalytic systems cost ( $E_{\rm EO(UV/US/Cat)}$  <

 $E_{\rm EO(UV/Cat)} + E_{\rm EO(US/Cat)})$ , confirming the efficacy and cost-effectiveness of the integrated system. This reduction in  $E_{\rm EO}$  can be attributed to the synergistic effect between these two radical-producing processes, resulting in an increase in the number of degradation events and shortening the reaction time.

Using enhancers could be another cost-effective approach to reduce the overall costs by enhancing process efficiency. Excellent contribution of enhancers in the production of radical species as well as shortening the reaction time outweigh their costs. Asgari et al.<sup>104</sup> performed an economic assessment on the ZnO/persulfate (PS) system for the degradation of AB113 dye through a sonophotocatalytic process. The spherical ZnO nanoparticles with sizes mostly in the range 30-90 nm were synthesized using a sol-gel method. The authors reported that the ZnO/PS/UV/US system exhibited the best removal performance under the optimized conditions, with about 98% degradation rate in 25 min. The economic analysis was performed for UV only, US only, ZnO, PS, and the integrated ZnO/PS/US/UV system. The costs of US and UV systems were calculated using  $E_{\rm EO}$  for each process, with values of 214.2 and 43.8 \$/m<sup>3</sup>, respectively. Also, the removal capacities of ZnO and PS were calculated as the number of milligrams of contaminant removed by one gram of ZnO or PS and were found to be 11.2 and 16.1 mg/g, respectively. According to the amounts of ZnO and PS required, the costs of ZnO and PS for the treatment of 1 m<sup>3</sup> of wastewater containing 200 mg/L AB113 were \$1690.5 and \$1064, respectively. In the case of integrated system (ZnO/PS/UV/ US), the energy cost was \$7.1 and material cost were \$92.4 and \$55.1 for ZnO and PS used, respectively, clearly showing the efficacy of the PS-assisted sonophotocatalytic system.

There are other factors influencing overall costs. For example, sonophotocatalysts can be reused over several cycles, lowering material consumption. The use of natural sunlight irradiation as a reactions' driving force instead of energyconsuming lamps could also be a promising way of reducing costs. Ahmad et al.<sup>18</sup> examined the degradation of RhB using ZnO-decorated multiwall CNTs through photocatalytic, sonocatalytic, and sonophotocatalytic processes. Their sonophotocatalytic reactor consisted of an open 200 mL cylindrical stainless glass vessel, covered with a transparent sheet to avoid evaporation and a 200 W rectangular shaped ultrasonic bath, as the source of US waves, operating in a fixed frequency (35 kHz). The whole setup was exposed to sun light between 10 a.m. and 4 p.m. with an average intensity of  $1.213 \times 10^5$  Lux unit during this period. Relatively lower reaction time and higher reaction rate constant were obtained in the sonophotocatalytic processes, when compared to the individual ones. The use of electricity from renewable resources (i.e., solar cells) is expected to be able to further reduce the operation costs of a sonophotocatalytic system in the future.

## 6. APPLICATION OF SONOPHOTOCATALYSIS IN BACTERIAL INACTIVATION AND DISINFECTION

We have mainly focused on the application of sonophotocatalysis in the pollutant degradation while describing and discussing various aspects of sonophotocatalysis, such as enhancement strategies, reactors, and energy consumption. In the following, we would like to specifically deal with an important application, bacterial inactivation and disinfection, where sonophotocatalysis also shows a high potential. Recently, semiconductor nanocatalysts have been used to

disinfect microbes and Gram-negative bacteria by means of photocatalysis.<sup>110</sup> The combination of ultrasonication and photocatalysis has also become a powerful technique for disinfecting hard-to-kill antibiotic resistant bacteria. Gramnegative bacterial membranes are characterized by an outer membrane that is made up of lipopolysaccharides (LPS), proteins, and phospholipids.<sup>111</sup> Although they possess a thinner peptidoglycan layer compared to Gram-positive bacteria, they are well-equipped to handle a variety of environmental stresses and mechanical loads.<sup>112</sup> It is also worth mentioning that the shape of the bacterium can have a considerable impact on the disinfection effectiveness of the ultrasonic system.<sup>113</sup> Compared to bacilli/rod-shaped bacteria, cocci/spherical bacteria are more resistant to sonication treatment.<sup>114</sup> There are commonly three steps involved in the disinfection of bacteria by sonophotocatalysis. The first stage begins gradually due to the bacteria's resistance to oxidative stress caused by the reactive species. This self-defense mechanism involves an important antioxidant enzyme, named superoxide dismutase (SOD). However, the constant mechanical shear and extended radical species production breaks the bacterial cell membrane and exposes their inner cellular components, causing rapid disinfection (second step). During the final step, the impact of reactive species is diminished due to the presence of intracellular components and cellular debris resulting in a reduced level of disinfection.<sup>115</sup>

Figure 11A illustrates different kinds of disinfection mechanisms involved under the combined effects of ultrasonication and photocatalysis. The physical or mechanical consequences of ultrasound cavitation (such as shock waves, shear pressures, microjets) cause the mechanical rupturing of cell membranes and lead to cellular lysis.<sup>43,118</sup> Additionally, a large number of reactive radical species can be produced from both sonocatalytic and photoinduced chemical reactions (photocatalysis). As a result, DNA and intercellular nucleic acids are ejected from the cell due to cytoplasmic material leakage (see Figure 11B). This can be explained by pressure and pressure gradients during the collapse of cavitation bubbles near or inside the cells. It was also reported that a lower frequency acoustic cavitation has greater mechanical effects than chemical effects related to the produced oxidative species.<sup>119</sup> In the following section, we will present three examples of how sonophotocatalysis can be applied to bacterial disinfection and explain how they confirm cell damage and the release of intercellular components caused by sonophotocatalytic disinfection mechanisms. Mukherjee et al.<sup>120</sup> reported the complete disinfection of the

multidrug resistant Klebsiella pneumonia bacteria under blue light irradiation from a LED source in combination with lowfrequency ultrasonication using CdS nanorods synthesized via hydrothermal reaction. The minimum inhibitory concentration (MIC) was defined as the lowest concentration of the nanomaterial to prevent the growth of bacteria.<sup>121</sup> The integrated disinfection technique was able to eradicate 106 CFU/mL (CFU: colony-forming units) of Gram-negative Klebsiella pneumonia efficiently in 20 min. This bacterium has a peptidoglycan layer containing cross-linked sugar and amino acids and has high permeability, making it easy for nanoparticles and oxidative species to pass through. The cell membrane's LPS and phospholipid bilayer are the main targets of oxidative radical attacks generated by sonophotocatalysis.<sup>1</sup> The mechanism of integrated system in disinfection of Klebsiella pneumonia is depicted in Figure 12A. The



Figure 12. (A) Expulsion of 260 nm absorbing material of *Klebsiella pneumonia* after ultrasonication, photocatalysis, and a combination of ultrasonication and photocatalysis (Son, ultrasonication; photo, photocatalysis (at MIC: 250 mg/L)). (B) Schematic sonophotocatalytic disinfection mechanism of *Klebsiella pneumonia* using CdS nanorods. (C) Effect of catalyst dosage on the sonophotocatalytic disinfection of *Klebsiella pneumonia* (MIC of CdS nanorod, 250 mg/L; light intensity, 15 mW/cm<sup>2</sup>). (D) Stability of CdS nanorods after multiple cycles of disinfection. XRD patterns of CdS nanorods (E) before and (F) after cyclic sonophotocatalytic tests. Reproduced with permission from ref 120. Copyright 2022 Elsevier.

effectiveness of ultrasonication-produced shockwaves combined with photocatalysis in disrupting the pathogen's cell membrane was also assessed. These two processes together caused leakage and discharge of compounds, that mainly have absorption around 260 nm, into the supernatant. As seen in Figure 12B, the optical density at 260 nm  $(OD_{260 \text{ nm}})$  for the separate photocatalytic and ultrasonication systems was significantly higher than the control without any treatment. When the two treatments were combined, the discharge of intracellular components was remarkably larger than when only ultrasonication or photocatalysis was applied. Compared to sonolysis, photocatalysis resulted in a slower rupture of the cell wall and release of intracellular components. Benefiting from the synergy index of 1.817 for sonophotocatalytic process (CdS-1xMIC: 250 mg/L; Figure 12C), the combined technique exhibited complementary and additive efficiency. A similar performance was also achieved using 0.5xMIC CdS

nanorods, which successfully managed to reduce the use of the nanomaterial below its MIC by coupling it with sonication (Figure 12C). Thus, the combination of these two processes allowed for the use of nanoparticles at much lower concentrations, which facilitates the practical application of sonophotocatalysis. Also, the electrical energy consumption values were 2.840, 0.8235, and 0.4709 kWh/L for sonolytic, photocatalytic, and sonophotocatalytic (CdS 1xMIC) treatment methods, respectively. The stability test results showed that the catalytic activity of the nanomaterial remained over 92% after nine cycles, confirming the high structural and functional stability of nanocatalysts under disinfection conditions (Figure 12D). As seen in Figure 12E,F, XRD patterns confirmed no significant structural crystalline changes of the CdS nanorods before and after the disinfection reactions, which demonstrates that ultrasonic waves did not damage the catalyst.

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**Figure 13.** (A) Synthesis flowchart of Fe/ZnO. (B) Different controlled experiments for *Shigella dysenteriae* disinfection (SPC, sonophotocatalysis; SC, sonocatalysis; PC, photocatalysis; SPL, sonophotolysis; PL, photolysis; SL, sonolysis; CL, catalysis). (C) Effect of different catalysts on the solar-sonophotocatalytic activity of *S. typhimurium*. (D) Comparative study and (E) proposed mechanism for sonophotocatalytic disinfection of *S. typhimurium*. (F) (a) and (b) the FESEM images of *S. typhimurium* without the presence of light and ultrasound at t = 0 and t = 30 min, respectively, (c–f) FESEM images of *S. typhimurium* that was subjected to solar-sonophotocatalysis at 10, 20, 30, and 45 min treatment, respectively (ZnO/Fe loading = 200 ppm, bacterial loading  $\approx 10^7$  CFU/mL, intensity of sunlight 55,000 lx). (A and B) Reproduced with permission from ref 123. Copyright 2020 Elsevier. (C–F) Reproduced with permission from ref 124. Copyright 2018 Elsevier.

Rahman et al.<sup>123</sup> developed Fe-doped ZnO (Fe/ZnO) nanoparticles for the Vis light-assisted sonophotocatalytic disinfection of *Shigella dysenteriae*. The ZnO nanoparticles were synthesized through colloidal and precipitation routes using zinc nitrate hexahydrate as precursor (Figure 13A). This work compared the effectiveness of sonophotocatalysis, sonocatalysis, and photocatalysis on the removal of the aforementioned bacteria. The results showed in Figure 13B concluded that sonophotocatalysis outperformed any other

processes. Excluding the 30 min of initial dark phase, the sonophotocatalysis method achieved a full log reduction of  $10^7$  CFU/mL *Shigella dysenteriae* in 60 min. In contrast, photocatalysis functioned similarly to sonocatalysis, both of which were unable to entirely disinfect bacteria load even after 1.5 h of reaction, leaving  $\approx 2.1$  log CFU/mL bacteria unaffected. However, sonophotocatalysis affected the metabolic processes of *Shigella dysenteriae*. It effectively multiplied reactive species production, primarily containing h<sup>+</sup> and O<sub>2</sub><sup>•-</sup> radicals, along

## Table 2. Summary of Sonophotocatalytic Degradation Experiments Reviewed in This Article

Nanocatalyst	Light source	Ultrasonic source	Model pollutant	Reaction time	Catalytic performance	Reference
TiO <sub>2</sub>	UV light, 400 W	80 kHz, 120 W	Olive mill wastewater	120 min	100% toxicity removal	45
Sheet-like ZnO	UV light, 300W	40 kHz, 200 W	Methyl orange	100 min	~80%	46
TiO <sub>2</sub> /CuO/graphene	UV–C, 80 W	40 kHz, 150 W	Methylene blue	60 min	100%	51
TiO <sub>2</sub> /CuO/graphene	Xe lamp, 40 W	40 kHz, 150 W	Methylene blue	80 min	100%	51
ZnIn <sub>2</sub> S <sub>4</sub> nanostars (NU@ZIS20)	300 W halogen lamp	20 kHz, 200 W	Tetracycline	35 min	99%	52
N, Cu, codoped TiO <sub>2</sub> functionalized CNT	Xe lamp, 200 W	400W	Sulfamethoxazole	60 min	100%	53
$Zn-Cu-Mg$ -mixed metal hydroxide/ $g$ - $C_3N_4$	Visible LED lamp, 15 W	40 kHz, 300 W	Sulfadiazine	200 min	93% COD removal	54
Fe-doped TiO <sub>2</sub>	Mercury lamp, 30 W	37 kHz, 100 W	Diazinon	100 min	85%	20
Fe-doped TiO <sub>2</sub> , H <sub>2</sub> O <sub>2</sub> assisted reaction	UV light, 24 W	50 kHz, 296 W	Paracetamol	30 min	100%	16
Ag-doped <i>h</i> -MoO <sub>3</sub> nanorods	Sunlight, 1205 W	100 W	Methylene blue	90 min	98.8%	61
N-doped TiO <sub>2</sub>	UV lamp, 300 W	20 kHz, 750 W	4-acetamidophenol	180 min	91%	62
Sm-doped TiO <sub>2</sub>	UV lamp, 300 W	20 kHz, 750 W	4-acetamidophenol	180 min	87%	62
N-doped ZnO	N/A	40 kHz, 200 W	Nigrosine	90 min	92%	64
MoS <sub>2</sub> /C peroxymonosulfate assisted reaction	Visible light, high-pressure Xe-lamp	40 kHz	Levofloxacin	80 min	100%	19
MgO@CNT	UV lamp, 150 W	24 kHz	Sulfadiazine	80 min	100%	10
MgO@zeolite	UVA, 24 W	24 W/cm <sup>2</sup>	Textile wastewater sample	240 min	78% COD removal	66
WO <sub>3</sub> /CNT	Visible light, 300 W/m <sup>2</sup>	24 kHz	Tetracycline	60 min	100%	71
ZnO/CuO	400 W solar simulator	80 kHz, 60 W	Parathion	60 min	100%	74
FeVO <sub>4</sub> @BiOCl, H <sub>2</sub> O <sub>2</sub> assisted reaction	UV lamp, 8 W	20 kHz, 125 W	p-nitrophenol	50 min	100%	75
ZnO/ZnS nanotube	500 W Hg-lamp	N/A	Methylene blue	50 min	63.3%	76
N/Ti <sup>3+</sup> codoped TiO <sub>2</sub> /Bi <sub>2</sub> WO <sub>6</sub>	500 W xenon lamp	35 kHz, 180 W	Methylene blue	50 min	98%	17
CuO-TiO <sub>2</sub> /rGO	UV light	40 kHz	Methyl orange	90 min	99%	83
Fe-doped Bi <sub>2</sub> O <sub>3</sub> + Ar bubbling assisted reaction	UV–C lamp, 4 W	37 kHz	Basic brown 1	42 min	99%	85
C–N codoped black TiO <sub>2</sub> H <sub>2</sub> O <sub>2</sub> assisted reaction	Visible light, 500 W	30 kHz	Palm oil mill effluent	60 min	75.48%	60
FeVO <sub>4</sub> @CeO <sub>2</sub> H <sub>2</sub> O <sub>2</sub> assisted reaction	UV light	20 kHz, 125 W	4-nitrophenol	30 min	100%	96
ZnO nanoparticle	150 W/m <sup>2</sup>	59 kHz	Rhodamine B	10 min	100%	58
Cu <sub>2</sub> O/MoS <sub>2</sub> /rGO	150 W, halogen lamp	40 kHz, 120 W	Tetracycline	10 min	100%	97
			Ciprofloxacin	75 min	94%	
$CeO_2$ -ZrO <sub>2</sub> @MoS <sub>2</sub>	Visible light, 250 W	40 and 970 kHz, 0–600 W	Naproxen	40 min	96%	98
CdS nanorods	Blue LED light, 150 $W/m^2$	700 W	Klebsiella pneumonia bacteria	20 min	100% (10 <sup>6</sup> CFU/mL)	120
ZnO	Visible light	40 kHz bath sonicator	Shigella bacteria	120 min	100% (10 <sup>7</sup> CFU/ mL)	123
Fe-doped ZnO				90 min	100% (10 <sup>7</sup> CFU/mL)	
Fe-doped ZnO	Sun light	40 kHz bath sonicator	Salmonella bacteria	90 min	100% (10 <sup>7</sup> CFU/ mL)	124

with acoustic cavitation. It perturbed the membrane and resulted in internal DNA damage and the release of intracellular components. In a similar study performed also by the same group, Fe-doped ZnO (ZnO/Fe) nanoparticles were utilized in the disinfection of *Salmonella typhimurium* (*S. typhimurium*) by sunlight-assisted sonophotocatalysis.<sup>124</sup> As seen in Figure 13C, the ZnO/Fe nanoparticles presented higher disinfection efficiency compared to bare ZnO nanoparticles for sonophotocatalytic disinfection. Even so, TiO<sub>2</sub> nanoparticles did not yield a complete disinfection when tested under the same conditions. Due to Fe doping, the  $e^-/h^+$  recombination rate in ZnO/Fe was reduced, unlike in ZnO and TiO<sub>2</sub>. Further, the transfer of the charges generated as a result of photoexcitation of Fe led to the generation of oxidative radicals. The DNA, protein, and ion leakage assay

provided proof that sonophotocatalysis had damaged the cells. The comparative study showed that the order of disinfection efficiencies followed the order of sonophotocatalysis > photocatalysis > sonocatalysis > sonolysis > photolysis> sonophotolysis (see Figure 13D). In the case of sonophotocatalysis, a complete 7 log (CFU/mL) reduction was achieved within only 45 min. The combined effect of sunlight irradiation, ultrasonic waves as well as presence of the catalyst, was proven to reduce the treatment time compared to control experiments. Figure 13E represents the schematic solar-sonophotocatalytic disinfection mechanism of *S. typhimurium* including the cell's membrane rupture and release of intercellular components into the environment. The complete disintegration and collapse of *S. typhimurium* cells during sonophotocatalysis was further confirmed by FESEM images.

As seen in Figure 13F, it is quite likely that internal elements including DNA, proteins, and ions have leaked into the environment. All these evidence confirmed the severe damages on the cell membrane of *S. typhimurium* during the sonophotocatalytic disinfection process and the subsequent leakage of chromosomal DNA into the environment.

A summary of sonophotocatalytic degradation experiments is shown in Table 2, including all the pertinent studies published to date. For better comparison among the examples, important parameters such as catalysts, light sources, ultrasonic sources, model pollutants, reaction time, and degradation efficiencies are provided in this table.

## CONCLUSIONS AND PERSPECTIVES

Employing nanocatalyst-based sonophotocatalysis for wastewater treatment and bacterial inactivation and disinfection requires a thorough multidisciplinary (chemical, physical, and engineering) understanding of liquid, solid, and interfacial properties as well as ultrasound parameters. Several chemical and physical events such as radical-producing reactions, cavitations, SL, increased mass transport, surface cleaning, and surface adsorption capacity variation are likely to happen simultaneously and result in considerable improvement in the efficiency. Hence, main limitations of photocatalytic process can possibly be eliminated when using sonophotocatalysis for degradation and disinfection processes (such as resistance in mass transfer and catalyst fouling) without having any significant impact on the structure, crystallinity, or morphology of the nanocatalyst. It is also important to mention that the efficient design of sonophotocatalytic reactors is essential to maintain high efficiency and provide a flexible, sustainable, and cost-effective alternative to conventional photocatalytic and sonocatalytic treatment methods. The sonophotocatalytic system activity can be enhanced by means of nanocatalyst modification techniques (incorporating dopants, using nanosubstrates, and forming efficient heterojunctions) aimed at improving mainly light absorption, optimizing charge transfer pathways, and reducing e<sup>-</sup>/h<sup>+</sup> recombination rates. Furthermore, process modification techniques primarily influence sonocatalytic mechanisms such as the nucleation and formation and collapse of cavitation bubbles, and promote the proliferation of radical species in the environment. Acoustic cavitations coupled with photocatalysis showed excellent synergism, affecting energy consumption of the integrated system. Sonophotocatalysis allows researchers to find new ways to improve the efficiency of ultrasound or even search for new strategies to generate cavitation that could be more efficient and of lower treatment costs (for example, by using renewable electricity) in the future.

Due to the lack of standardized data, the presence of various contaminants, and the different operational parameters of each experiment, it is not always possible to reach straightforward conclusions relating nanomaterial's morphology to sonophotocatalytic activity. However, looking at some of the examples described in this manuscript, we will give the reader some insights to help to better rationally design novel nanomaterials, heterojunctions, and composites in the future. Sheet-like and flower-like morphologies usually have higher sonophotocatalytic activity, such as for the case of ZnO nanocatalysts, when compared to rod-like ZnO in the degradation of methyl orange.<sup>46</sup> Furthermore, desert rose morphology of ZnO with 50 nm nanosheet petals outperformed other ZnO morphologies, such as nanospheres, nanowires, and microwires in the

RhB sonophotocatalytic removal.<sup>58</sup> For the degradation of MB, ZnS/ZnO nanotubes showed greater degradation rate than their nanorods counterpait.<sup>76</sup> Looking at these examples, we can conclude that nanosheets and nanotubes usually outperformed other nanostructures. In general, nanomaterials possess high specific surface areas, high porosity, and optimal interfacial charge transfer. Low-dimensional nanoscaled materials (2D, 1D, 0D) exhibit a more uniform size distribution compared to bulk materials, allowing for better control of their properties. Their larger surface area allows them to come into contact with a greater portion of photons and pollutants in the solution. Additionally, the energy levels of nanomaterials can also be tuned by modifying their size, doping and creating defects.<sup>125</sup> In particular, 2D nanomaterials benefit from having a high surface area and the possibility of being host materials to form heterojunctions and composites and thereby improved charge transfer.<sup>126,127</sup> Furthermore, in some cases, the charge transfer is favored in one specific direction due to the orientation of the nanostructures such as nanotubes, thereby reducing charge recombination,<sup>128,129</sup> as it could be seen in the previous ZnS/ZnO example. Additionally, nanotubes are generally preferred to nanorods due to their increased surface area with more exposed catalytic active sites to light and adsorbed molecules, with their tendency to form a packed interconnected network and reduced charge recombination rate.<sup>13</sup>

There are several factors that must be considered for future investigations in order to improve its efficiency and extend its application to other fields:

- The simultaneous degradation of multiple contaminants should be investigated. Contrary to the cases reported in most articles, where artificial wastewaters only contain a single contaminant, real effluents always include more than one type of contaminants. The performance of sonophotocatalysis through degradation of multiple contaminants must be explored, as well as possible new phenomena, extra synergism, or better removal capability of semiconductors. To really assess the efficiency of sonophotocatalysis and promote its practical application, the analysis of real wastewater samples should be performed.
- It is highly needed to standardize the experimental conditions and characterization tests in the field of sonophotocatalysis if we want to fairly compare different materials. Since a broad range of catalysts, pollutants, catalyst dosages, pollutant concentrations, reaction times, light and US power sources, and different reactor sizes have been employed in the literature, progress cannot be assessed in a rational way. For example, a specific dye or pollutant can be selected as standard contaminant for future investigations. Also, reaction kinetic constants must always be provided for all processes and controlled experiments. With all these, researchers in this field will be able to compare the catalyst activities and rationally design new nanomaterials and heterojunction-enhanced nanocatalysts.
- Deeper study of mechanisms and pathways is of high necessity. Because of the short time interval in which the sonophotocatalytic reaction pathways take place, deeper mechanism and pathway analysis are hard but necessary. Future research could also focus on exploring possible effects of ultrasound on nanomaterial properties (such as

band structure and Fermi energy) and its impacts on the thermodynamics and kinetics of reactions. Sonophotocatalytic disinfection of bacteria is also not understood to its full extent. Particularly, a systematic investigation is needed to understand how sonophotocatalysis differs from other oxidation processes in terms of disinfection pathways at the molecular level. Along with theoretical simulations, *in situ* characterization techniques (e.g., *in situ* FTIR, *in situ* Raman) are promising tools in achieving this goal.

- Fabricating integrated Z-scheme sonophotocatalytic systems requires further research and should be one of the main focuses of future research to promote the optimization of redox and oxidation potentials in sonophotocatalysts and boost the degradation efficiency in such systems.
- Precise investigation of attenuation of photons and US in large-scale usage should be taken into consideration. Although there are a lot of studies concerning sonophotocatalytic degradation of pollutants in at the laboratory scale, little is known about reactor parameters optimization, the effective penetration distance of photons and US at the larger scale. Attenuation of ultrasonic waves and light irradiation caused by various parameters such as solvent and dissolved organics and catalyst particles is one of the fundamental phenomena that must be taken into consideration in order to bring this technique into large-scale applications.
- The stability of nanomaterials is related to several factors. One of them is correlated with their stability in acid or basic media. Additionally, their stability under light (especially UV light) and ultrasonic waves needs also to be considered and studied. Sonophotocatalysis should not damage the catalyst's physical and/or chemical structure to avoid its structural or morphological changes. Also, in the case of binary or ternary composites, ultrasonic waves should not adversely affect their integrity. To achieve this goal, rational morphology design (e.g., core@shell structures) or formation of strong covalent bonds instead of simple van der Waals interactions among the nanocomponents can be used to strengthen their junctions and interfaces.<sup>131</sup> Performing leaching tests, TEM, XRD, and FTIR analysis before and after the experiments is highly recommended for future investigations to study the integrity and structural and morphological features of the fabricated nanocatalysts.
- A more in-depth economic assessment will be required to use this technique for scale-up processes. Electrical energy consumption accounts for part of the sonophotocatalytic degradation of wastewaters. Other expenses (such as costs of reactors, piping, valves, site work, engineering, part replacement, labor, chemicals, characterizations, sampling, operation, and maintenance) need to be considered and optimized to lowest without compromising the performance.
- The majority of published articles on sonophotocatalysis employed UV-active materials. Other photocatalysts with absorption in the Vis and NIR regions of the spectra should be considered to increase the sunlight and SL utilization and the overall efficacy of sonophotocatalysis.
- In this interdisciplinary field, computational modeling/ calculations are necessary to support all critical elements

and operational parameters such as the design of catalysts, reactors, etc.

• "Self propelled nanorobotics are holding outstanding applications in biosensing, biomedicine, environment, and chemistry fields, which is a new application of cutting-edge multidisciplinary field in nanotechnology.<sup>132-135</sup> Catalytic micro/nano robots are nanomaterials that can effectively convert external forces such as magnetic field, light source (photocatalytic), ultrasonic waves (sonocatalytic), and chemical fuels to mechanical motion for desired applications. For example, Ussia et al.<sup>133</sup> used self propelled black titania/silver nanorobots under light irradiation for treatment of bacterial biofilm. The molecular motion of light propelled micro/nano motors could be controlled by adjusting the light intensity. Photocatalytic nanorobots could give rise to the concentration of reactive oxygen species that affectively degrade bacteria.<sup>132,133</sup> Also, it has been reported that ultrasonic waves can increase the motion of micromotors due to the production of microbubbles.<sup>135</sup> As a new subject, the simultaneous usage of light and ultrasonic sources as driving forces could be investigated in the future to improve the performance of nanomaterial for micro/nano robot preparation for biomedical applications.

Overall, due to the combination of physical, sonochemical, and photochemical processes, sonophotocatalysis has indisputable advantages over classic photocatalysis, allowing for researchers to build enhanced systems with larger degradation potentials. We hope that we have been able to grant a comprehensive overview of the research progress in this area and shed some light on the advantages, its limitations, and future directions to promote its use in general, and ultimately, in industrial applications.

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