

Adsorption characteristics of a clinoptilolite-rich zeolite compound for Sr and Cs

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Abstract

The Sr and Cs adsorption capacities of LithoFillTM, LithoGranTM and a competing clinoptilolite containing zeolite product were investigated by radioanalytical methods (⁸⁵Sr and ¹³⁴Cs gamma spectroscopy). The dependence of adsorption and adsorption rate on physical factors including temperature, available ions and time were assessed. In addition, the reversibility of adsorption under high ionic strength conditions was also examined. In general, cesium is more strongly adsorbed than strontium, adsorption yields are generally independent of temperature (from room temperature to 65 °C) and adsorption is relatively rapid (identical results for 2 or 5 day adsorption times). As expected, increasing the concentration of other ions in solution tends to reduce adsorption of cesium and strontium. In general, Cs adsorption ranges between 54.5 and 45.2 mg/g for LitoFill and LitoGran samples and between 36.9 and 24.4 mg/g for the competing product. For Sr adsorption, ranges are 30–21 mg/g and 7.3–6.7 mg/g respectively, leading to the conclusion that the higher content of clinoptilolite in the LitoFill/LitoGran samples results in better adsorption characteristics.

Keywords Zeolite · Clinoptilolite · Strontium · Cesium · Ion exchange

Introduction

Zeolites, specifically in the form of clinoptilolite $((Na,K,Ca)_{2-3}Al_3(Al,Si)_2Si_{13}O_{36}\cdot 12(H_2O))$ are well known as natural inorganic ion-exchangers [1–5] with applications in geochemical [6–8], agricultural [9] and decontamination/waste disposal [10–19] operations. The authors received three samples from the company Lithos Natural who have several zeolite mining operations in Lower Austria. Due to the unusually high content of clinoptilolite ($\sim 90\%$) in their zeolite, the company claimed exceptionally high ion adsorption capabilities and was interested in the specific properties of their product with respect to the adsorption of cesium and strontium. For comparison, a zeolite with lower clinoptilolite content ($\sim 60\%$) was also provided.

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Experimental

To test the adsorption capabilities of the samples for Sr²⁺ and Cs⁺ ions, 500 mg of sample were mixed with 500 µl of stock solutions of CsCl or Sr(NO₃)₂ that contained ¹³⁴Cs or ⁸⁵Sr as tracer (see below). If required, additional ions (NaCl or HCl) were added to the mixture. The sample vials were then filled to 10 ml with distilled water and the zeolite powder suspended in the liquid by vortexing. After the planned adsorption time during which the samples were repeatedly vortexed and kept at the desired temperature, liquid and zeolite were separated by centrifugation. The supernatant liquid was decanted, taking care to decant only clear liquid. The decanted liquid was then weighed and measured on a gamma spectrometer to measure the remaining concentration of Cs or Sr in the liquid for comparison to the initial stock solution. From these measurements, the total absorbed Cs or Sr on the zeolite could be calculated.

Samples

Four samples were provided. Samples A (LithofillTM 100T) and B (LithofillTM 100) were composed of particles of



Atominstitut, TU Wien, Stadionallee 2, 1020 Vienna, Austria

 $<125\,$ and $<100~\mu m,\,$ respectively. Sample C (Lithogran TM) had a particle size of 0.5–2 mm. The three samples A, B, and C each have a clinoptiolite content of approximately 90%. The fourth sample (D) composed of particles sized similarly to sample A was provided for comparison and had a clinoptiolite content of approximately 60%.

Stock solutions

Stock solutions were prepared by irradiating a small amount of CsCl (10 mg) or $Sr(NO_3)_2$ (30 mg) at a neutron flux density of approximately $2\times 10^{12}~cm^{-2}~s^{-1}$ for 8 h in the dry irradiation tube of the TRIGA Mk II reactor of the Atominstitut. The irradiated powders were then dissolved in distilled water and inactive CsCl or $Sr(NO_3)_2$ was added to reach concentrations of approximately 50 mg/ml. The final cesium stock solution had a Cs concentration of 49.43 mg/ml (372 mmol/L). For the strontium experiments, two stock solutions had to be prepared due to the shorter half-life of ^{85}Sr . The two solutions had final Sr concentrations of 61.16 mg/ml (698 mmol/L) and 59.99 mg/ml (685 mmol/L).

Adsorption times

In an initial experiment, different adsorption times were tested for the adsorption of Cs on the zeolite samples. Adsorption times of 2, 4, 10, and 20 min at room temperature (~ 20 °C) were applied. From these initial experiments, it was clear that adsorption reached saturation after 10 min. This time was then used for all further Cs adsorption experiments.

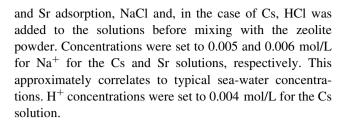
A similar experiment with the Sr stock solution showed that the adsorption was still increasing after 20 min. Thus, adsorption times of 48 and 120 h were applied. After 48 h, the increase in adsorption was only minimal, so 120 h was considered to be a sufficient time for full adsorption.

Adsorption temperature

To examine the influence of temperature on the adsorption of Cs and Sr, the samples were kept in a water bath at temperatures of 55–65 °C during the adsorption time. The zeolite was kept in suspension by vortexing while maintaining the desired adsorption temperature in the sample. For the Cs and Sr experiments, adsorption time was kept to 5 min.

Competing ions

It stands to reason that if ions other than Sr or Cs are available in the solution, adsorption behavior will change. To understand how availability of other ions influences Cs



Results and discussion

In general, it was observed that the adsorption capacities for the three samples A, B, and C are consistently better than for sample D for both Cs⁺ and Sr²⁺ ions. The adsorption capacity for Cs in samples A and B (small particle size) was about 50 mg of Cs per 1 g of sample. For the larger particles in sample C, the adsorption was only slightly smaller at 45 mg/g. For sample D, adsorption of Cs was about 30 mg/g.

The adsorption capabilities of all products for Sr²⁺ ions were approximately half of the capabilities for Cs⁺ and the adsorption process was much slower. We believe this is due to the monovalent versus divalent nature of the cations.

Detailed results are provided in Tables 1 (Cs) and 2 (Sr) as well as in Figs. 1–6 in the supplemental material. An increase in temperature reduced the time necessary to reach saturation. While saturation was reached for Cs adsorption in samples A–C within minutes already at low temperatures, the lower clinoplilotite content of sample D caused slower uptake of Cs, leading to a measureable increase in adsorption at higher temperatures. A similar situation can be seen for the adsorption of Sr, however on a much slower timescale.

The experiments with additional, competing ions show that in the case of Cs adsorption, saturation was reached since a significant decrease in Cs adsorption was observed. This indicates that the competing ions may displace the Cs ions. The situation is similar for the uptake of Sr.

Conclusion and outlook

From the data collected during this study it can be concluded that the major factor influencing for the adsorption of Cs and Sr on zeolites is the content of clinoptilolite. Higher temperature increases the rate of uptake to saturation of the zeolite. Under the conditions used, for Cs, adsorption is very fast (on the order of minutes) whereas for Sr several hours are needed to reach saturation. Also, in general, adsorption capacity for Cs is about double the capacity for Sr. Both, the longer adsorption time as well as the lower adsorption capacity are most probably due to the divalent nature of Sr. Ionic radius and the nature of



Cs uptake (mg/g)

Err%

Table 1 Cs adsorption on samples under different conditions

Time (min)

Sample

Sample	Time (min)	Cs uptake (mg/g)	EIT%
A	1	49.1	3*
A	2	54.4	3*
A	5	49.8	2.2
A	10	50.4	3*
В	1	54.5	3*
В	2	51.4	3*
В	5	47.8	4.1
В	10	50.2	3*
C	1	40.1	3*
C	2	43.8	3*
C	5	45.2	6.6
C	10	43.0	3*
D	1	24.4	3*
D	2	25.2	3*
D	5	36.9	17.8
D	10	28.9	3*
Sample	Temperature (°C)	Cs uptake (mg/g)	Err%
A	22	50.4	3*
A	55	48.6	3*
A	65	50.5	3*
В	22	50.1	3*
В	55	46.5	3*
В	65	46.9	3*
C	22	46.5	3*
C	55	41.7	3*
C	65	47.2	3*
D	22	30.6	3*
D	55	36.4	3*
D	65	43.7	3*
Sample	Ion concentration (mo	I/L) Cs uptake (mg/g)	Err%
A	0	50.4	3*
A	0.004	46.2	0.7
A	0.005	38.9	3*
В	0	50.1	3*
В	0.004	47.8	0.8
В	0.005	41.2	3*
C	0	46.5	3*
C	0.004	41.9	6.4
C	0.005	31.9	3*
D	0	30.6	3*
D	0.004	24.1	3.2
D	0.005	23.7	3*

Since not all adsorption experiments were repeated, error is estimated from counting statistics at 3% as indicated by "*". All other errors were calculated as the standard deviation of repeat experiments

Table 2 Sr adsorption on samples under different conditions

Sample	Time (h)	Sr uptake (mg/g)	Err%
A	0.08	13	46
A	48	23	3.4
A	120	30	2.8
В	0.08	21	27
В	48	26	4.3
В	120	26	5.9
C	0.08	11	26
C	48	19	3.3
C	120	21	7.4
D	0.08	6.7	22
D	48	6.7	10
D	120	7.3	24
Sample	temperature (°C)	Sr uptake (mg/g)	Err%
A	22	8.1	21
A	60	19	6.2
В	22	17	12
В	60	27	5.1
C	22	9.3	6.2
C	60	15	10
D	22	4.9	16
D	60	6.7	25
Sample	ion concentration (mo	nl/L) Sr uptake (mg/g)	Err%
A	0	30	2.8
A	0.006	16	1.7
В	0	26	5.9
В	0.006	9.3	29
C	0	21	7.4
C	0.006	7.5	17
D	0	7.3	24
D	0.006	4.1	46
All error	s were calculated as th	ne standard deviation of 4	repeat

All errors were calculated as the standard deviation of 4 repeat experiments

exchanges sites within the zeolite structure are also likely to influence capacity and adsorption rate. Finally, smaller particle sizes speed adsorption, which might be expected due to the larger surface area available.

Further studies of the Cs and Sr adsorption under the influence of several different concentrations of competing ions, including divalent species, up to similar concentrations as in the stock solution would be useful. While this would most probably not be a case in a practical application as a remediation medium, more detailed information on the selectivity of clinoptilolite could be gained. Furthermore, the adsorption kinetics for the Sr²⁺ ions should be studied further, hopefully gaining insight into the



structural properties of the clinoptilolite that enable monoand divalent ion absorption.

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References

- Ames LL Jr (1964) Some zeolite equilibriums with alkaline earth metal cations. Am Miner 49:1099–1110
- Ames LL Jr (1964) Some zeolite equilibriums with alkali metal cations. Am Miner 49:127–145
- Howery DG (1964) Ion exchange properties of the zeolite, clinoptilolite. Thesis submitted to the faculty of the University of North Carolina
- Ames LL Jr (1963) Mass action relations of some zeolites in the region of high competing cation concentrations. Am Miner 48:868–882
- Ames LL (1960) The cation sieve properties of clinoptilolite. Am Mineral 45:689–800
- Howery DG, Thomas HC (1965) Ion exchange on the mineral clinoptilolite. J Phys Chem 69(2):531–537
- Deist J, Talibudeen O (1967) Thermoldynamics of K–Ca ion exchange in soils. J Soil Sci 18(1):138–148. https://doi.org/10. 1111/j.1365-2389.1967.tb01495.x

- Avakyan GS (1973) Zeolitic rocks of the Noemberyansk region of the Armenian SSR and their prospects for industrial use. Izv Akad Nauk Arm SSR Nauki Zemle 26(6):48–60
- Nishita H, Hamilton M, Hamilton M (1968) Influence of minerals on strontium-90 and cesium-137 uptake by bean plants. Soil Sci 105(4):237–243. https://doi.org/10.1097/00010694-196804000-00006
- Mercer BW Jr (1960) The removal of cesium and strontium from condensate wastes with clinoptilolite, vol HW-66276. General Electric Company, Richland
- Mercer BW Jr, Ames LL, Touhill CJ (1968) Ammonia removal from waste water by selective ion exchange. Amer Chem Soc Div Water Air Waste Chem Gen Pap 8(1):97–102
- Mercer BW Jr, Ames LL, Touhill CJ, Van Slyke WJ, Dean RB (1970) Ammonia removal from secondary effluents by selective ion exchange. J Water Pollut Control Fed 2(Pt. 2):R95–R107
- Nelson JL, Alkire GJ, Mercer BW (1964) Inorganic ion-exchange separation of cesium from Purex-type high-level radioactive wastes. Ind Eng Chem Process Des Dev 3(2):143–148. https:// doi.org/10.1021/i260010a009
- Mathers WG, Watson IC (1962) Waste disposal experiment using mineral exchange on clinoptilolite. At Energy Can Ltd, [Rep] AECL AECL-1521:33
- Katz H, Rothbart M, Schreiner T (1964) Decontamination of Savannah River waste supernate by ion exchange. U S A E C BNL 853 (T-339):19
- Frost CR (1963) The fixation of cesium on Australian minerals.
 II. Zeolite minerals. vol AAEC/TM206. At. Energy Comm. Res. Estab..
- 17. Dyer A (1984) Uses of natural zeolites. Chem Ind 7:241-245
- Dyer A (2007) Ion-exchange properties of zeolites and related materials. In: Cejka J, van Bekkum H, Corma A, Schüth F (eds) Introduction to zeolite science and practice, 3rd edn. Elsevier, New York
- Lihareva N, Dimowa L, Petrov O, Tzvetanova Y (2018) Evaluation of Bulgarian clinoptilolite as ion-exchanger for Cs + removal from water solutions. J Radioanal Nucl Chem 316(1):37–47

