

# Optimizing the Lattice Nitrogen Coordination to Break the Performance Limitation of Metal Nitrides for Electrocatalytic Nitrogen Reduction

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**ABSTRACT:** Metal nitrides (MNs) are attracting enormous attention in the electrocatalytic nitrogen reduction reaction (NRR) because of their rich lattice nitrogen (N<sub>lat</sub>) and the unique ability of N<sub>lat</sub> vacancies to activate N<sub>2</sub>. However, continuing controversy exists on whether MNs are catalytically active for NRR or produce NH<sub>3</sub> via the reductive decomposition of N<sub>lat</sub> without N<sub>2</sub> activation in the in situ electrochemical conditions, let alone the rational design of high-performance MN catalysts. Herein, we focus on the common rocksalt-type MN(100) catalysts and establish a quantitative theoretical framework based on the first-principles microkinetic simulations to resolve these puzzles. The results show that the Mars-van Krevelen mechanism is kinetically more favorable to drive the NRR on a majority of MNs, in which N<sub>lat</sub> plays a pivotal role in achieving the Volmer process and N<sub>2</sub> activation. In terms of stability, activity, and selectivity, we find that MN(100) with moderate formation energy of N<sub>lat</sub> vacancy ( $E_{vac}$ ) can achieve maximum activity and maintain electrochemical stability, while low- or high- $E_{vac}$  ones are either unstable or catalytically less active. Unfortunately, owing to



the five-coordinate structural feature of  $N_{lat}$  on rocksalt-type MN(100), this maximum activity is limited to a yield of NH<sub>3</sub> of only  $\sim 10^{-15}$  mol s<sup>-1</sup> cm<sup>-2</sup>. Intriguingly, we identify a volcano-type activity-regulating role of the local structural features of  $N_{lat}$  and show that the four-coordinate  $N_{lat}$  can exhibit optimal activity and overcome the performance limitation, while less coordinated  $N_{lat}$  fails. This work provides, arguably for the first time, an in-depth theoretical insight into the activity and stability paradox of MNs for NRR and underlines the importance of reaction kinetic assessment in comparison with the prevailing simple thermodynamic analysis.

**KEYWORDS**: electrocatalytic nitrogen reduction, metal nitrides, activity limitation, surface topology, density functional theory calculation, microkinetic

# INTRODUCTION

The ammonia synthesis is one of the most critical reactions in modern industry.<sup>1–5</sup> The Haber-Bosch process as the primary route to produce NH<sub>3</sub> is energy-intensive.<sup>6,7</sup> The electrosynthesis offers a promising strategy to produce NH<sub>3</sub> at mild conditions, such as lithium-mediated ammonia synthesis, nitrate/NO<sub>x</sub> reduction and direct N<sub>2</sub> reduction reaction [nitrogen reduction reaction (NRR)],<sup>8–12</sup> in which the direct NRR is the most attractive technology.<sup>13</sup> Unfortunately, although much effort has been made to develop superior catalysts for NRR,<sup>13–30</sup> many of them are demonstrated to produce only tiny amounts of NH<sub>3</sub> or even do not produce NH<sub>3</sub> under the protocols with rigorous isotope labeling experiments.<sup>9,31–33</sup> Therefore, there is a strong desire to design and prepare advanced catalysts for NRR or at least provide a relatively explicit direction for optimizing catalysts.

Metal nitrides (MNs), which can provide rich lattice nitrogens ( $N_{lat}$ ) to form NH<sub>3</sub> and abundant  $N_{lat}$  vacancies to activate N<sub>2</sub>, have been widely tested in experiments for nitrogen reduction.<sup>17–26,34,35</sup> In electrocatalytic NRR, one of the most significant ambiguities for MNs is where NH<sub>3</sub> comes from, i.e., the decomposition of N<sub>lat</sub> or the catalytic reduction

of  $N_2$ .<sup>36–39</sup> Whether MNs are suitable for electrocatalytic NRR has been confused. For example, VN, which possesses good conductivity and has been used for oxygen electroreduction,<sup>40,41</sup> was synthesized by some research groups and demonstrated to be efficient in the electrosynthesis of NH<sub>3</sub> with high selectivity (vs H<sub>2</sub> evolution reaction, HER).<sup>22,23</sup> However, under the rigorous testing protocols, some studies found that the inability of VN to catalyze the electrosynthesis of NH<sub>3</sub> from N<sub>2</sub> and VN could release N<sub>lat</sub> in a noncatalytic process, leading to the formation of NH<sub>3</sub>.<sup>36–38</sup> A similar controversy exists for Mo<sub>2</sub>N catalyst.<sup>26,39</sup> These different observations could be due to different fine structures exposed under different preparation conditions;<sup>36</sup> for example, all facets of VN except (100) were predicted to show a faster migration

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Figure 1. Major scientific problem and the key findings of this work. The fine structure of the lattice  $N_{lat}$  is an important factor determining the activity and ability of MNs for NRR. The four-coordinate  $N_{lat}$  ( $N_{4c}$ ) can exhibit optimal activity and overcome the performance limitation.



Figure 2. (a) Structure of rocksalt-VN(100) surface. (b) Routes of aqueous H<sup>+</sup> attack the reactant. Route i, the proton transfers to the catalyst surface via the Volmer process (H<sup>+</sup> + e<sup>-</sup>  $\rightarrow$  H<sub>ads</sub>) first, and then the adsorbed H<sub>ads</sub> species reacts with the adsorbed reactant (H<sub>ads</sub> + \*R  $\rightarrow$  \*RH, where R represents reactant); Route ii, the proton directly attacks reactant adsorbed on the catalyst surface by the proton-coupled electron transfer process (PCET, H<sup>+</sup> + e<sup>-</sup> + R  $\rightarrow$  RH). (c) Potential energy variation from AIMD simulation for water(H<sub>3</sub>O<sup>+</sup>)/VN(100) system as a function of time. IM1-IM3 are the key states of proton transfer to N<sub>lat</sub> at 3.100, 3.160, and 3.165 ps, respectively, and the dynamic trajectories can be seen in Figure S2. (d) Relationships of the potential dependent effective barriers of \*N<sub>2</sub>  $\rightarrow$  \*NNH and N<sub>lat</sub>H  $\rightarrow$  N<sub>lat</sub>H<sub>2</sub> following Route i (E<sup>l</sup><sub>ef</sub>) and Route ii (E<sup>l</sup><sub>ef</sub>) and Route ii (e<sup>2</sup><sub>ef</sub>). (e,f) Energy profiles for \*N<sub>2</sub>  $\rightarrow$  \*NNH and N<sub>lat</sub>H  $\rightarrow$  N<sub>lat</sub>H<sub>2</sub> following Route i (blue line) and Route ii (red line) at U = 0 V vs SHE, respectively.

than replenishment of  $N_{lat}$  vacancies and trend to decompose,<sup>24,38</sup> which may result from the different  $N_{lat}$  local structures (Figure 1). One may ask: could the lattice  $N_{lat}$  site be essentially active and stable to catalyze the entire cycle of electrocatalytic NRR? Are these conflicting experimental observations structure-dependent? What fine structure could be suitable for electrocatalytic NRR? In terms of these tasks, it is time-consuming and too costly to controllably prepare and measure the NRR performance of each MN individually under the rigorous isotope experimental protocols. Several theoretical studies investigated a series of MN-based materials for NRR and suggested a number of MNs with potential NRR activity

by assessing the reaction thermodynamics, such as VN, ZrN, and CrN; these materials potentially exhibit limited HER activity but significantly facilitate N<sub>2</sub> electroreduction due to the presence of N<sub>lat</sub> vacancies.<sup>24,42–51</sup> However, there appears to be a discrepancy between the theoretical results and the existing experimental results when assessing the catalytic ability of a given MN.<sup>9,31–33,36,37</sup> Therefore, it is crucial to theoretically elucidate the underlying abilities of MNs built on the complete NRR kinetic information and establish the relation between the structural feature and activity/stability based on the kinetic steady-state description. However, the Scheme 1. L-H (a) and MvK (b) Pathways on VN(100), in which the Related Transition State and Intermediate Structures Are Shown in Figures  $S4-S7^a$ 



<sup>a</sup>The red and orange lines represent the favored L–H and MvK pathways, respectively (see the detailed energy profiles in Figure S8).

related kinetic analysis was generally ignored in the electrocatalytic NRR simulation.

Toward these challenges, in this work we focused on the most stable (100) surfaces of rocksalt-type MNs (e.g., VN, CrN, TiN, and ZrN) as case catalysts inspired by recent theoretical and experimental studies,  $^{20-24,36,37}$  aiming to understand the reaction mode of N<sub>lat</sub> (decomposition or catalysis) in NRR by the first-principles microkinetic analysis. The variation rules of activity and stability of different MNs for NRR were revealed, which shows the optimum activity of rocksalt-type MN(100) at typical working potential at an order of only  $\sim 10^{-15}$  mol s<sup>-1</sup> cm<sup>-2</sup>, and we further determined the structural origin of this low NRR performance. Importantly, a possible structural feature of N<sub>lat</sub> on MNs was proposed, i.e., the four-coordinate  $N_{lat}$  (denoted as  $N_{4c}$ , Figure 1), which may achieve the win-win activity-stability for NRR; the optimal NH<sub>3</sub> yield could be up to  $\sim 10^{-11}$  mol s<sup>-1</sup> cm<sup>-2</sup>. This work goes beyond the traditional thermodynamic analysis, and the obtained kinetic insight could provide a fundamental direction for MN catalyst optimization.

## RESULTS AND DISCUSSION

## Electrocatalytic NRR Mechanism on VN Catalyst

To begin with, we took rocksalt-type VN as a case catalyst to gain mechanistic insight into NRR, which is one of the experimentally most attractive and debated MNs.<sup>20–23</sup> The most exposed facet of VN, (100), can be demonstrated by its largest  $N_{lat}$  formation energy and lowest surface energy (Table S1), and is terminated by two types of active sites, i.e., the five-coordinate  $V_{cus}$  and  $N_{lat}$  sites (hereinafter denoted as \* and #N, respectively, where # represents the  $N_{lat}$  vacancy; Figure 2a). The  $V_{cus}$  and  $N_{lat}$  sites constitute the basic active sites for NRR,

corresponding to two different reaction pathways, respectively: (i)  $N_2$  is activated on the  $V_{cus}$  site and completes the Langmuir–Hinshelwood (L–H) pathway; (ii) the  $N_{lat}$  is converted into  $NH_3$ , followed by  $N_2$  activation in the  $N_{lat}$  vacancy, which obeys the so-called Mars-van Krevelen (MvK) pathway involving the removal/refilling of  $N_{lat}$ .

## Langmuir-Hinshelwood Pathway

As shown in Scheme 1a,  $N_2$  can be activated to some extent at the  $V_{cus}$  site with an adsorption energy of -0.43 eV but is difficult to dissociate with a barrier as high as 3.97 eV. Thus, H-mediated  $N_2$  activation is necessary. In this regard, a key issue on the hydrogenating species needs to first be solved, that is how the aqueous proton attacks the reactant (R). Two general routes are illustrated in Figure 2b: (i) the proton transfers to the catalyst surface via the one-electron reduction (Volmer process,  $H^+ + e^- \rightarrow H_{ads}$ ), and then couples with reactant R ( $H_{ads} + R \rightarrow RH$ ); (ii) the aqueous proton directly attacks R obeying the proton-coupled electron transfer process (PCET,  $H^+ + e^- + R \rightarrow RH$ ).

It was found that the Volmer process at the V<sub>cus</sub> or N<sub>lat</sub> site corresponds to a free energy change of 0.33 and -0.08 eV at U = 0 V (vs the standard hydrogen electrode, SHE), respectively, indicating that the proton prefers to bind to N<sub>lat</sub> rather than V<sub>cus</sub>. The ab initio molecular dynamics simulation with the explicit solvation model at T = 300 K shows that H<sub>2</sub>O can spontaneously dissociate at the water/VN(100) interface with a H released on N<sub>lat</sub> and a hydroxyl left on V<sub>cus</sub>, and then the solvated proton readily transfers to the as-formed hydroxyl through a water molecule chain by the Grotthuss-type mechanism,<sup>52</sup> corresponding to an IM1  $\rightarrow$  IM2  $\rightarrow$  IM3 conversion (Figure 2c; see the dynamic trajectories in Figure S2). This indicates that the proton transfer to the VN(100)



**Figure 3.** (a) Activity map of NRR following the L–H and MvK pathways as a function of  $E_{vac}$  and potential U (vs SHE), where the black dashed line represents the optimal activity trend. (b) Activity curves of NRR at the potential U = -0.3 V, where the red and blue lines represent the L–H and MvK pathways, respectively. (c) Degree of rate control ( $X_{RC}$ ) change trends of the rate-determining steps in the MvK pathway at the potential U = -0.3 V. (d) Coverage change trends of some important species on MNs at the potential U = -0.3 V.

surface to form  $N_{lat}H$  species is a straightforward process. Further, we calculated the reaction barrier of  $H^+/e^- + N_{lat} \rightarrow N_{lat}H$  at U = 0 V, and it gives a low energy barrier of only 0.27 eV, implying the kinetic feasibility of this Volmer process.

Below, the reaction kinetics of \*NNH formation (\*N<sub>2</sub>  $\rightarrow$  \*NNH) via Routes i and ii were explored, respectively, where the effect of electrode potential U was included using the charge-extrapolation method (details in Note S1). Figure 2d shows the potential-dependent effective barriers (see details in Note S2), which demonstrate that \*N<sub>2</sub>  $\rightarrow$  \*NNH via Route i gives an overall lower effective barrier than route ii over a wide range of potentials, indicating the feasibility of Route i. Specifically, as shown in Figure 2e, the effective barrier in Route i is  $E_{\rm ef}^1 = 1.51$  eV at U = 0 V, while the PCET process in Route ii is more difficult with a higher barrier  $E_{\rm ef}^2 = 2.19$  eV. Therefore, it is expected that the N<sub>lat</sub>H can act as a primary hydrogenating species to complete the subsequent N<sub>2</sub> reduction process.

Based on the above results, we then systematically explored the \*N<sub>2</sub> hydrogenation to NH<sub>3</sub> by the L-H pathway (see the detailed discussions in Note S3). As Scheme 1a depicts, the conversion of \*N<sub>2</sub> preferentially obeys the associative alternating mechanism, i.e., \*N<sub>2</sub>  $\rightarrow$  \*NNH  $\rightarrow$  \*NHNH  $\rightarrow$ \*NHNH<sub>2</sub>  $\rightarrow$  \*NH<sub>2</sub>NH<sub>2</sub>. Once \*NH<sub>2</sub>NH<sub>2</sub> forms, the N-N bond can be split with a low barrier of 0.55 eV, and formed \*NH<sub>2</sub> can be easily hydrogenated to release NH<sub>3</sub> and finish the whole catalytic cycle. From Figure S8a, one can see that the first two steps of \*N<sub>2</sub> hydrogenating into \*NHNH constitute the highest point in the whole energy profile, corresponding to an effective barrier of  $E_{ef} = 1.74$  eV. This implies that the \*N<sub>2</sub> hydrogenation could be rate-limiting in the L-H pathway on VN(100).

#### Mars-van Krevelen Pathway

For comparison, the MvK pathways on the VN(100) catalyst were also systematically examined. For N<sub>lat</sub>H hydrogenation to N<sub>lat</sub>H<sub>2</sub> (N<sub>lat</sub>H  $\rightarrow$  N<sub>lat</sub>H<sub>2</sub>), we first compared the proton attacking routes discussed above. Similarly, Route i, i.e., N<sub>lat</sub>H resulting from the Volmer process couples with each other, is more favored than Route ii at the typical working potential (Figure 2d,f; see details in Note S2). This further demonstrates that N<sub>lat</sub>H (#NH) is the main hydrogenating species to participate in NRR. Further hydrogenation of N<sub>lat</sub>H<sub>2</sub> to N<sub>lat</sub>H<sub>3</sub> gives a barrier of 0.44 eV ( $\Delta H = -0.37$  eV) and the subsequent release of N<sub>lat</sub>H<sub>3</sub> costs 0.97 eV of energy, leaving an N<sub>lat</sub> vacancy (N<sub>vac</sub>).

Remarkably, in comparison with the V<sub>cus</sub> site, the formed N<sub>vac</sub> shows a better activation ability toward N<sub>2</sub> with a larger adsorption energy of -0.96 eV (vs -0.46 eV). As Scheme 1b shows (see more details in Note S3), the optimal MvK pathway consists mainly of three key subprocesses: (i) N<sub>lat</sub>H is hydrogenated to release NH<sub>3</sub> with N<sub>vac</sub> left, (ii) N<sub>2</sub> adsorbs in the N<sub>vac</sub> and is hydrogenated to #NNH<sub>2</sub>, which then breaks the N–N bond to form \*NH<sub>2</sub> and refill the N<sub>vac</sub> easily ( $E_a = 0.30$  eV), and (iii) \*NH<sub>2</sub> is hydrogenated to NH<sub>3</sub>, in which the subprocesses i is rate-limiting with an effective barrier of 1.54 eV (Figure S8b). Comparing the L–H and MvK pathways, one can preliminarily judge that the MvK pathway is more feasible with a lower effective barrier on VN(100). A detailed kinetic discussion is given later.

## Activity and Stability Analysis of MNs for NRR

To understand the activity and stability trend, we extended the L–H and MvK pathways to other MNs such as CrN, TiN, and ZrN, and calculated the barriers and enthalpy changes of the relevant elementary steps. As the previous studies have shown that the formation energy of oxygen vacancy on metal oxides is



**Figure 4.** (a) Distribution diagram of main species on the surfaces of different MNs with change of  $E_{vac}$  and U, and the relative detailed coverage changes are shown in Figure S13. (b) Decomposition diagram of  $N_{lat}$  as a function of  $E_{vac}$  and applied potential U (vs SHE), where  $\Delta G(U)$  is the Gibbs free energy change of  $N_{lat}$  leaching out at the potential U.  $E_{ads}(N_2@N_{vac})$  is the adsorption energy of  $N_2$  on  $N_{vac}$  of MN (100) surface.

a reliable descriptor for assessing their catalytic performance, <sup>53–55</sup> here we tested the formation energy of  $N_{vac}$  ( $E_{vac}$ ) as a descriptor to express the energy information on each elementary step in NRR on different MNs.

From Figure S9a, one can find that the adsorption energies of N<sub>2</sub> on the metal site (M<sub>cus</sub>) or N<sub>vac</sub>, as well as the H adsorption energies on N<sub>lat</sub>, have good linear correlations with  $E_{vac}$ 

$$E_{\rm ads}(N_2@M_{\rm cus}) = -0.20E_{\rm vac} + 0.03 \tag{1}$$

$$E_{\rm ads}(N_2 @N_{\rm vac}) = -1.21E_{\rm vac} + 1.58$$
<sup>(2)</sup>

$$E_{\rm ads}({\rm H}@{\rm N}_{\rm lat}) = 0.72E_{\rm vac} - 1.76$$
 (3)

Significantly, a large  $E_{vac}$  is conducive to N<sub>2</sub> adsorption on both the  $M_{cus}$  and  $N_{vac}$  sites. Quantitatively,  $E_{ads}(N_2 @ N_{vac})$ becomes more negative than  $E_{ads}(N_2@M_{cus})$  when  $E_{vac} > 1.50$ eV, demonstrating the superior  $N_2$  activation ability of  $N_{vac}$  on the MNs with relatively high  $E_{\rm vac}$ . In addition, it is noteworthy that  $N_2$  and H species show the opposite variation trends; the larger  $E_{vac}$  enhances the adsorption ability toward N<sub>2</sub> but weakens the binding strength of H species on N<sub>lat</sub>. As depicted in Figure S9b-e, the barriers and enthalpy changes of all elementary steps in either the L-H or MvK pathways exhibit linear scaling with  $E_{\rm vac}$ . Almost all of these correlations have negative slopes, indicating that these steps become easier to proceed as  $E_{vac}$  increases. The primary cause of this phenomenon is the weaker H binding at N<sub>lat</sub> and the stronger binding of the  $M_{cus}$  sites as  $E_{vac}$  increases. This facilitates the hydrogenation steps and N-N bond cleavage. Overall, an increase in  $E_{vac}$  is beneficial for activating the N<sub>2</sub> molecule, promoting the  $N_{\text{lat}}/N_2$  hydrogenation and the N–N bond cleavage, while simultaneously weakening the H binding at the surface  $N_{lat}$  site. Therefore,  $E_{vac}$  proved to be an efficient indicator.

## NRR Activity of MNs

Based on these scaling relations, we constructed the microkinetic model to inspect the NRR activity and stability trends at different working potentials and T = 300 K (see the microkinetic details in Note S4). In the microkinetic simulation, we also probed the NRR selectivity by incorporating the competitive HER (details in Note S5). Figure 3a illustrates the activity trend of different MNs for NRR by plotting the logarithms of turnover frequency (TOF) as a function of  $E_{vac}$  and working potential U (vs SHE). The NH<sub>3</sub> formation rates are proportional to  $E_{\rm vac}$  and U. Specifically, MNs with a low  $E_{vac}$  (i.e., the highly reactive  $N_{lat}$ ) consistently exhibit low catalytic activities. As  $E_{vac}$  increases, the corresponding catalytic activities gradually increase. However, when  $E_{\rm vac}$  increases to a certain extent,  $N_{\rm lat}$  becomes inert and the catalytic activity is severely limited; only when a high potential is applied can these MNs catalyze NRR again. Unfortunately, as demonstrated in Figure S11, the HER is progressively promoted at high potentials and yields a comparable rate of  $NH_3$  formation on these high- $E_{vac}$  MNs. This suggests a low selectivity of NRR at this stage, which is not desirable for the experiment. Therefore, to ensure the more favored formation of NH<sub>3</sub> rather than H<sub>2</sub>, the optimal potential U for MNs should be controlled within a range of low potential (>-0.5 V). However, in such a situation, it corresponds to a very low maximum NH<sub>3</sub> formation rate of only  $\sim 10^{-6}$  s<sup>-1</sup> site<sup>-1</sup> ( $\sim 10^{-15}$  mol s<sup>-1</sup> cm<sup>-2</sup>) on MN(100).

To inspect the activity analysis of MN catalysts for NRR, a microkinetic simulation was conducted at the typical voltage U = -0.3 V (vs SHE). Two volcano-type activity curves following the L–H or MvK pathways were obtained. Figure 3b shows that the MvK pathway is generally more favored than the L–H pathway over a wide range, as evidenced by the fact that the MvK activity curve is overall higher than the L–H one and reaches a much higher maximum point. The L–H pathway becomes active only when  $E_{\rm vac}$  increases to a certain extent (>3.20 eV), where N<sub>lat</sub> is too inert to be reduced. For instance, NRR on CrN(100), VN(100), and TiN(100) predominantly follows the MvK pathway, while on ZrN(100) it follows the L–H pathway. This suggests that the MvK pathway is the primary route for NRR on MNs, which accords with the experimental reports.<sup>17–26</sup>

On analyzing the activity curve (Figure 3b), it is evident that it rises significantly from a low  $E_{\rm vac}$  and reaches an inflection point at  $E_{\rm vac} = 1.30$  eV. In the range of  $E_{\rm vac} < 1.30$  eV, the ratelimiting step is the hydrogenation of  $\#N_2$  ( $\#N_2 \rightarrow \#NNH$ ), as indicated by the higher rate control sensitivity  $X_{\rm RC}$  (Figure 3c). Combining with the coverage change (Figure 3d), the increased activity in this range is attributed to the decreased energy barrier and the rapidly increased coverage of N<sub>2</sub> on N<sub>vac</sub> [ $\theta(\#N_2)$ ] and H species on N<sub>lat</sub> [ $\theta(\#NH)$ ] with the increase of  $E_{\rm vac}$ . After  $E_{\rm vac} = 1.30$  eV, the activity curve becomes flat and gradually reaches the maximum point at  $E_{\rm vac} = 2.10$  eV, which corresponds to an optimal NRR activity (but only ~10<sup>-6</sup> s<sup>-1</sup> site<sup>-1</sup>). In the range 1.30 eV <  $E_{\rm vac} < 2.10$  eV, the rate-limiting



Figure 5. (a) Schematic diagram for rationally screening/designing the appropriate MN catalysts for NNR by  $E_{vac}$  at the low working potential.  $E_{vac}(opt)$  is the location of MNs with the optimum activity. (b) Schematic illustration of the influence of the scaling relation for the rate-limiting step  $\#NH \rightarrow \#NH_2$  on different structural  $N_{lat}$  on the peak height of the volcano-shaped activity curve.  $N_{5\sigma} N_{4\sigma}$  and  $N_{3c}$  represent the five-, fourand three-coordinate  $N_{lav}$  respectively. (c) Slopes ( $\alpha$ ) and intercepts ( $\beta$ ) of the relation for the rate-limiting step RLS-1 as a function of  $E_{vac}$  on different coordinate  $N_{lav}$  respectively. (d) Structural features of  $N_{5\sigma} N_{4\sigma}$  and  $N_{3\sigma}$  and the corresponding activity changing trend. The white, blue, and gray balls represent the hydrogen, nitrogen and metal atoms, respectively. (e) Relationships of adsorption energies of H species on  $N_{5\sigma} N_{4\sigma}$ and  $N_{3\sigma}$  respectively. (f) Decomposition diagram of  $N_{lat}$  as a function of  $E_{vac}$  and applied potential U (vs SHE), where  $\Delta G(U)$  is the Gibbs free energy change of  $N_{lat}$  leaching out at the potential U (vs SHE).  $E_{ads}(N_2@N_{vac})$  is the adsorption energy of  $N_2$  on  $N_{vac}$  of  $N_{4c}$ .

step changes from  $\#N_2$  hydrogenation to  $N_{lat}H$  hydrogenation ( $\#NH \rightarrow \#NH_2$ , Figure 3c). When  $E_{vac} > 2.10$  eV, the activity begins to decline rapidly, primarily due to the inert  $N_{lat}$  evidenced by  $\theta(\#N) \approx 1$  ML (Figure 3d). Specifically, CrN(100) and VN(100) were previously predicted to be efficient for NRR based on a simplified thermodynamic assessment;<sup>24</sup> however, despite being located around the optimal point of the activity curve, they exhibit a low reaction rate of only about  $10^{-10}$  s<sup>-1</sup> site<sup>-1</sup> ( $\sim 10^{-19}$  mol s<sup>-1</sup> cm<sup>-2</sup>) under the quantitative microkinetic simulation. As can be seen from the activity curves, for MNs(100) with too reactive or too inert N<sub>lat</sub>, adjusting  $E_{vac}$  to a moderate degree ( $\sim 2.10$  eV) can improve their catalytic activities for NNR; however, even at this optimal point, the catalytic activity remains limited, with a NH<sub>3</sub> formation rate of only  $\sim 10^{-6}$  s<sup>-1</sup> site<sup>-1</sup> ( $\sim 10^{-15}$  mol s<sup>-1</sup> cm<sup>-2</sup> site<sup>-1</sup>, see the detailed discussions in the latter).

# **Electrochemical Stability of MNs**

It is worth discussing that if consumed  $N_{lat}$  in the MvK pathway cannot be replenished in time, MNs would eventually decompose and lose catalytic activity. In other words, the competition between  $N_{lat}$  dissolution in the form of  $NH_3$  and  $N_2$  adsorption in  $N_{vac}$  could determine the stability of MNs in the realistic NRR environment. Quantitatively, the distribution

diagram of the key species on different MNs(100) at the kinetic steady state was plotted as a function of  $E_{vac}$  and potential *U* by virtue of microkinetic simulation (Figure 4a), which can provide an explicit description of the surface environment.

Figure 4a shows that on MNs with low  $E_{\text{vac}}$  (<1.30 eV), the coverage of  $N_{vac}$  [ $\theta(\#)$ ] is almost 1 ML at typical potentials, demonstrating that the surface N<sub>lat</sub> has been leached out at the steady state. Therefore, these MNs tend to decompose and are unsuitable for catalyzing NRR. The electrochemical phase diagram of MN(100) surfaces (Figure 4b), which describes the Gibbs free energy change  $[\Delta G(U)]$  of the N<sub>lat</sub> leaching-out process (details in Note S6), can rationalize the origin of the low stability of these MNs. As Figure 4b shows, when MN(100) has low  $E_{vac}$  (<1.00 eV), the dissolution U is larger than 0 eV, indicating that this surface N<sub>lat</sub> would be reduced to NH<sub>3</sub> and released easily even at the very small reduction potential. At the same time, the low  $E_{\rm vac}$  means the weak N<sub>2</sub> adsorption on  $N_{vac}$  (Figure S9a), and  $\textit{E}_{ads}(N_2 @ N_{vac})$  is even positive (>0.55 eV), implying the difficult supply of  $N_2$  on  $N_{vac}$ . As  $E_{\text{vac}} > 1.00$  eV, although the dissolution U begins to become negative,  $E_{ads}(N_2 @ N_{vac})$  is still larger than 0 eV until  $E_{vac}$  = 1.30 eV, and therefore the MNs would still be unstable at the usual low reduction potential due to the difficult supply of N<sub>2</sub> to fill N<sub>vac</sub>. When  $E_{vac}$  is above 1.30 eV, the microkinetic results show that the N<sub>vac</sub> coverage gradually decreases, and the surface N<sub>lat</sub> coverage increases at the steady state; at this time, the N<sub>2</sub> supply also becomes thermodynamically favored and can compete with the decomposition of N<sub>lat</sub>, as illustrated in Figure 4a,b.

In general, for MNs with low  $E_{vac}$ , the insufficient adsorption of N<sub>2</sub> cannot balance the N<sub>lat</sub> release, leading to abundant N<sub>vac</sub> on these metal-nitride surfaces and catalyst deactivation. This explains the phenomenon that NH<sub>3</sub> formation occurs only at the preliminary stage on some MNs and decreases quickly or is even undetectable over time.<sup>36,37</sup> The electrochemical stability of MNs can be improved as  $E_{\rm vac}$  becomes higher. Based on these findings, it is worthwhile at this point to discuss the controversy on the stability of VN catalyst. (100) as the most stable surface of VN catalyst has an  $E_{\rm vac}$  of 2.29 eV (>1.30 eV) and  $E_{ads}(N_2 @ N_{vac})$  is strong (-0.96 eV), indicating its relative stability in the electrochemical NRR condition. In contrast, the VN(311) surface (taken as an example of secondarily exposed surfaces of VN catalyst) corresponds to an  $E_{vac}$  of only 0.73 eV and  $E_{ads}(N_2 @ N_{vac})$  is limited by -0.33 eV, which implies that  $N_{lat}$  on the (311) surface could be easily reduced to  $NH_3$  and released even at the low reduction potential based on the decomposition diagram of  $N_{lat}$  (Figure 4b), and thus, VN(311)is less stable. Therefore, the electrochemical stability of the VN catalyst in NRR could be critically determined by the exposed morphology during catalyst preparation, which may rationalize the different experimental observations on the stability of VN catalyst.<sup>20–24,37</sup>

## Further Discussion on Designing MN for NRR

Overall, by integrating the above stability and activity analysis, a quantitative rule can be provided to assess the suitability of MNs for NRR. As illustrated in Figure 5a, MN(100) with low  $E_{\rm vac}$  (<1.30 eV) is always unstable due to the easy reduction of N<sub>lat</sub> and poor N<sub>2</sub> supply on N<sub>vac</sub>, resulting in very low catalytic ability for NRR. When  $E_{\rm vac} > 1.30$  eV, MN(100) gradually favors the N<sub>2</sub> supply on N<sub>vac</sub> and leads to improved catalytic activities and electrochemical stabilities. However, beyond a specific  $E_{\rm vac}$  threshold, the catalytic activities decrease quickly due to the inert N<sub>lat</sub>, despite excellent stabilities of these MNs at this time.

Nonetheless, it is essential to note that such a maximum reaction rate ( $\sim 10^{-6} \text{ s}^{-1} \text{ site}^{-1}$ ) on the (100) surface of rocksalt-type MNs falls below the demand for industrial application. To further improve the catalytic activity, increasing the electrode potential U could certainly be a possible strategy. As Figure 3a shows, the optimal NRR rate can reach  $10^{-1}$  to  $10^{\circ} \text{ s}^{-1}$  site<sup>-1</sup> on high- $E_{\text{vac}}$  rocksalt-type MNs (around  $E_{\text{vac}}$  = 2.80 eV) at the higher potential U = -0.8 V; however, at this time, HER would be improved even more and leads to a low NRR selectivity (Figure S11b). Therefore, elevating the electrode potential could not be a good method to improve the catalytic activity of MNs for NRR; increasing the intrinsic catalytic activity of MNs is crucial to overcome the limitations of the peak height of the volcano activity curve. To this end, it is a requisite to understand the inherent constraint on rocksalt-MN(100) catalysts. From the microkinetic analysis above, it can be seen that the peak position  $[E_{vac}(opt)]$  of the activity curve for rocksalt-MN(100) is largely determined by the intersection of two rate-limiting steps (RLS-1:  $\#NH \rightarrow \#NH_2$ )

and RLS-2:  $\#NH_2 \rightarrow \#NH_3$ ). Quantitatively, the peak height  $(r_{max})$  can be expressed with reference to RLS-1

$$r_{\max} = \frac{k_{\rm B}T}{h} \exp\left(\frac{-\alpha E_{\rm vac}({\rm opt}) - \beta}{k_{\rm B}T}\right) \times \theta(\#{\rm NH})^2 \tag{4}$$

where  $\alpha$  and  $\beta$  are the slope and intercept, respectively, of the linear correlation of the barrier of RLS-1 as a function of  $E_{\text{vac}}$ .  $E_{\text{vac}}(\text{opt})$  is the peak position of the activity curve, around 2.10 eV.  $\theta(\#\text{NH})$  is the coverage of H species on N<sub>lat</sub>, which is nearly 1 ML at  $E_{\text{vac}}(\text{opt})$  (Figure 3d). Hence,  $r_{\text{max}}$  can be simplified as being directly proportional to  $\alpha$  and  $\beta$ 

$$\ln r_{\rm max} \propto -\alpha E_{\rm vac}({\rm opt}) - \beta \tag{5}$$

Accordingly, slope  $\alpha$  and intercept  $\beta$  are the critical factors influencing  $r_{\text{max}}$ . Since these two parameters are constant for the catalysts of the same structural type, <sup>56,57</sup> it can be speculated that breaking the scaling relationship limit of  $\alpha$  and  $\beta$  on the five-coordinate N<sub>lat</sub> (denoted as N<sub>5c</sub>) of MNs(100) may be an effective strategy to enhance their intrinsic catalytic activity.

To verify this hypothesis, we explored the barriers of RLS-1 on the four- (or three-) coordinate  $N_{lat}$  (denoted as  $N_{4c}$  and  $N_{3 \ensuremath{\mathcal{C}}\xspace}$  respectively), on the other low Miller index (110) and (111) surfaces of rock-salt-type MNs as a proof of concept. After scaling these barriers and enthalpy changes on N<sub>4c</sub> and  $N_{3c}$  with  $E_{vac}$ , we can establish new relations (Figure S14) and the higher  $r_{\text{max}}$  can be obtained around  $E_{\text{vac}} = 2.10 \text{ eV} (r_{\text{max}})$  $N_{4c} > N_{3c} > N_{5c}$ ; especially, there is a  $r_{max}$  as high as  $10^{-2} \text{ s}^{-1}$ site<sup>-1</sup> on  $N_{4c}$  (~10<sup>-11</sup> mol s<sup>-1</sup> cm<sup>-2</sup>, Figure 5b), which is about  $10^4$  times larger than that on N<sub>5c</sub>. Compared with N<sub>5c</sub> (Figure 5c), the slope  $\alpha$  on N<sub>4c</sub> and N<sub>3c</sub> decreases but the difference in lpha values is relatively small; by comparison, the eta term on  $\mathrm{N_{4c}}$ and  $N_{3c}$  is much lower than that on  $N_{5c} \, (1.28/1.39 \mbox{ eV vs } 2.58$ eV). In other words, the larger  $r_{\rm max}$  on  $N_{4c}$  and  $N_{3c}$  can be attributed to the much smaller  $\beta$  term, which can decrease the overall energy barrier of N<sub>lat</sub> hydrogenation and facilitate NRR.

The intercept  $\beta$  is determined by the local structural features of active sites.<sup>56–58</sup> In terms of the rate-determining  $\#NH_2$ formation step  $(N_{lat}H + N_{lat}H \rightarrow N_{lat}H_2 + N_{lat})$ , there are two main factors affecting this H transfer process: (i) the cleavage of H-N<sub>lat</sub> bond and (ii) the formation of new H-N<sub>lat</sub>H bond with the possible cleavage of metal-nitrogen  $(M-N_{lat})$  bonds accompanied on the catalyst surface. As shown in Figure 5d, one can see that the lattice N<sub>5c</sub> is relatively saturated, which will become oversaturated as #NH<sub>2</sub> forms; thus, three M-N<sub>lat</sub> bonds around  $N_{5c}$  are necessary to be broken and the  $N_{5c}$  is pulled out in NH<sub>2</sub> formation. Although the H adsorption on  $N_{5c}$  is relatively weaker compared with that on  $N_{4c}$  and  $N_{3c}$ (Figure 5e), these three  $M-N_{lat}$  bonds are relatively difficult to break, thus leading to higher  $\beta$ ; the higher  $\beta$  indicates that the rate-determining #NH2 formation on N5c is more difficult. By comparison, on the tapered N<sub>3c</sub>, the lattice N<sub>lat</sub> becomes fivecoordinated as #NH<sub>2</sub> forms, which is still relatively unsaturated compared to the most stable six-coordinate N<sub>lat</sub> in the bulk phase. Thus, #NH2 can be stabilized without breaking any M-N<sub>lat</sub> bond. However, the H adsorption on N<sub>3c</sub> is much stronger than that on  $N_{5c}$  (Figure 5e), which limits the H transfer to some extent. For the most promoted N<sub>4c</sub>, it can basically stay at the original lattice position with a stable six-coordination configuration during the #NH<sub>2</sub> formation process, which is the most stable structure for N<sub>lat</sub> in MN and does not need to break any M-N<sub>lat</sub> bond. In addition, N<sub>4c</sub> exhibits an edge

structure and has a moderate H adsorption strength that is relatively weaker than that of the tapered N<sub>3c</sub> (Figure 5e). Thus, the H transfer between N<sub>4c</sub> is more favorable compared with that between N<sub>3c</sub>, resulting in the lowest  $\beta$  and contributing to the largest  $r_{\text{max}}$  for NRR (Figure 5b).

Noteworthily, according to the decomposition diagram of  $N_{lat}$  (as a function of  $E_{vac}$  and applied potential U; see Figure 5f), one can see that for  $N_{lat}$  at  $E_{vac}(opt) \approx 2.10$  eV, the tolerate potential U can reach -0.4 V vs SHE, implying that only when the reduction potential U is more negative than -0.4 V, these  $N_{4c}$  would tend to decompose in the form of NH<sub>3</sub> energetically. In addition, in the  $N_{4c}$  vacancy site at  $E_{vac}(opt) \approx 2.10$  eV, the  $N_2$  adsorption is strong with  $E_{ads}(N_2@N_{vac})$  being -1.0 eV. It is therefore expected that the  $N_{4c}$  configuration is stable under the reaction condition of NRR with a relatively small applied potential (U > -0.4 V) that is generally used in the experiment. In other words,  $N_{4c}$  could be an important topology of  $N_{lat}$  for NRR, which can achieve a win–win in terms of activity and stability.

## CONCLUSIONS

In summary, this work reported a systematic investigation into the electrocatalytic NRR on MNs, in which the molecular-level mechanism of NRR was identified, and structure-activitystability maps of NRR on different metal-nitrides were established by the microkinetic simulations. Mechanically, we verified that the MvK pathway is kinetically more favorable to drive NRR on a majority of MNs, where N<sub>lat</sub> plays a pivotal role in achieving the Volmer process and N2 activation; only on MNs with inert Nlat the L-H pathway works. More importantly, we quantitatively revealed the stability, activity, and selectivity trends of MNs for NRR, which closely depend on  $E_{\rm vac}$ . MNs with low  $E_{\rm vac}$  are unstable and easily decompose, and are incapable of activating  $N_2$  efficiently. The high- $E_{vac}$ ones give low catalytic activities despite superior electrochemical stabilities; only at the elevated potential, they could achieve improved NRR activities but encounter low selectivity (vs HER). The moderate- $E_{vac}$  MNs can give the maximum activity and keep good electrochemical stability; this activity maximum is, however, largely limited with the NH<sub>3</sub> yield of only  $\sim 10^{-6} \text{ s}^{-1} \text{ site}^{-1}$  ( $\sim 10^{-15} \text{ mol s}^{-1} \text{ cm}^{-2}$ ) owing to the structural feature of five-coordinate N<sub>lat</sub> on rocksalt-type MN(100). To break through this activity limitation, we explored the activity-regulating role of the local structural features of  $N_{\text{lat}\prime}$  and we proposed that surface engineering by adopting the fine local structures of  $N_{lat}$  (e.g., four-coordinate  $N_{lat} E_{vac}(opt) \approx 2.10 \text{ eV}$  on MNs could potentially improve the NH<sub>3</sub> yield up to an anticipated  $\sim 10^{-2} \text{ s}^{-1}$  site<sup>-1</sup> in experiments. We believe that this work provides an in-depth insight into NRR on MNs and theoretically illustrates whether/how MNs can be suitable for NRR. These fundamental understandings offer direction to design or optimize metal-nitride catalysts.

# METHODS

#### **Calculation Method**

All spin-polarized density functional theory (DFT) calculations were performed by VASP,<sup>59</sup> using the Perdew–Burke–Ernzerhof functional within the generalized gradient approximation.<sup>60</sup> The core– valence electron interaction was described by the project-augmented wave method,<sup>61</sup> and the valence electronic states were expanded in the plane wave basis sets with an energy cutoff of 450 eV. Van der Waals dispersion (DFT-D3) was included, and the DFT + U

approach with the on-site coulomb correction included was used to describe the localized 3d-orbital of V element ( $U_{\text{eff}} = 3.0 \text{ eV}$ ).<sup>62,63</sup> The geometries were optimized by using the Broyden method until the maximal force on each relaxed atom was less than 0.05 eV/Å. The rocksalt-type MN (100) surface was described with a  $p(2 \times 2)$  slab with five atomic layers. During structural optimization, the bottom two layers of the slab were fixed, the top three layers and adsorbates were fully relaxed, and the vacuum between slabs was set to 15 Å; a 3  $\times$  3  $\times$  1 k-point mesh was used. The constrained optimization method was used to search the transition state, which has been widely verified.<sup>64,65</sup> The microkinetic simulation was carried out with the CATKINAS package.<sup>66–69</sup> The formation energy  $(E_{\rm vac})$  of the nitrogen vacancy was calculated with the following equation:  $E_{\rm vac}$  =  $(E_{sur_vac} + 1/2E_{N_2}) - E_{sur}$ , where  $E_{sur}$  and  $E_{sur_vac}$  are the total energies of the pristine surface and surface with one nitrogen vacancy, and  $E_{N_2}$ is the total energy of N2 molecule, respectively.

# EFFECT OF POTENTIAL AND SOLVENT

For the process involving the proton–electron pair  $(H^+/e^-)$ , the reaction free energy was calculated by using the computational hydrogen electrode model (CHE). In this approach, the chemical potential of  $H^+/e^-$  is equilibrated with half the free energy of an  $H_2$  molecule at 0 V (vs SHE), while the effect of external potential U was accounted for by including the -eU correction.<sup>70,71</sup> The potential dependent reaction barrier at a constant potential was calculated by the charge-extrapolation method (see the details in Note S1).<sup>72-</sup> Notably, with respect to the solvent-induced stabilization effect toward the NRR-related adsorbates, it has been estimated to be comparatively small, and contributes little to the tendency judgment.<sup>50,51</sup> To further illustrate the influence of solvation energy in our system, we chose the N<sub>2</sub> and N<sub>lat</sub> hydrogenation steps (\*N<sub>2</sub> + N<sub>lat</sub>H  $\rightarrow$  \*NNH + N<sub>lat</sub> and N<sub>lat</sub>H  $\rightarrow$  N<sub>lat</sub>H<sub>2</sub>) at the water/VN(100) interface as examples and calculated its energy barrier and reaction energy in explicit water by performing the multipoint averaging molecular dynamics (MPA-MD).<sup>52</sup> It shows that the difference with and without a water environment is reliably small (Table S2), ~0.20 eV, demonstrating again a relatively small effect on judging the activity trend. Herein, our DFT calculations were mainly conducted on the bare surfaces by balancing the too-heavy ab Initio molecular dynamics simulations for each elementary step occurring on the catalyst surface.

## ASSOCIATED CONTENT

## Supporting Information

The Supporting Information is available free of charge at https://pubs.acs.org/doi/10.1021/jacsau.4c00377.

Detailed reaction pathway of the L–H and MvK mechanisms on VN(100),  $H_2$  evolution reaction information on VN(100), and TS or intermediate structures, and microkinetic details and some related kinetic data (PDF)

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## **Author Contributions**

H. W. directed this project. H. Y. performed the DFT calculations, data analyses, and wrote the manuscript. C. Z. gave the assistance with some DFT calculations and data analyses. Y. H. and H. G. Y. gave helpful suggestions for the research. All the authors participated in writing and editing the manuscript and contributed their efforts to the discussion. CRediT: Haiyang Yuan conceptualization, data curation, formal analysis, funding acquisition, investigation, writing-original draft, writing-review & editing; Chen Zhu data curation, formal analysis, investigation; Yu Hou writing-review & editing; Hua Gui Yang writing-review & editing; Haifeng Wang conceptualization, formal analysis, funding acquisition, methodology, project administration, supervision, writing-review & editing.

#### Notes

The authors declare no competing financial interest.

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