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Data Article

Electrocoagulation process to Chemical and Biological Oxygen Demand treatment from carwash grey water in Ahvaz megacity, Iran

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ABSTRACT

In this work, we present the result of an electric coagulation process with iron and aluminum electrodes for removal of chemical and biological oxygen demand (COD and BOD) from grey water in different car washes of Ahvaz, Iran. Nowadays, one of the important dangerous that can contaminate water resources for drinking, agriculture and industrial is Car wash effluent [1,2]. In this study, initial COD and BOD concentration, pH of the solution, voltage power and reaction time was investigated. The concentration level

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COD removal
BOD removal

of remaining COD and BOD in samples was measured, using DR/5000 UV-vis HACH spectrophotometer [3,4]. The effects of contact time, initial pH, electrical potential and voltage data on removal of COD and BOD were presented. Statistical analysis of the data was carried out using Special Package for Social Sciences (SPSS 16).

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Specifications Table

<i>Subject area</i>	<i>Environment</i>
<i>More specific subject area</i>	<i>Chemical and biological oxygen demand</i>
<i>Type of data</i>	<i>Table, figure</i>
<i>How data was acquired</i>	<i>DR/5000 UV-vis HACH spectrophotometer</i>
<i>Data format</i>	<i>Raw, analyzed</i>
<i>Experimental factors</i>	<ul style="list-style-type: none"> - For samples collection from different grey water of Ahvaz, a glass tank was used with a volume of 2–4 l, containing 3 electrode-plate iron and aluminum (Al-Al, Al-Fe, Fe-Fe) was used for Electro-coagulation removal. - After collection of wastewater along the car washes, added Sulfuric acid (H_2SO_4), potassium dichromate ($K_2Cr_2O_7$), mercury sulfate ($HgSO_4$), silver sulfate (Ag_2SO_4), potassium hydrogen phthalate ($C_8H_5KO_4$) and 3-methyl-2-benzothiazoline, then it was stored in a dark place at 4 °C temperature until the metals analysis - The effects of contact times, initial pH, electrical potential and voltage were examined.
<i>Experimental features</i>	<i>Electrocoagulation between many treatment processes having to be cost-effective for wastewater treatment with pollutant wide range.</i>
<i>Data source location</i>	<i>Ahvaz, Iran</i>
<i>Data accessibility</i>	<i>Data is with this article.</i>

Value of the data

- These data describe changes in COD and BOD removal from grey water by electrocoagulation process.
- Data show that electrocoagulation can be used as cost-effective for removal of other pollutant from wastewater.
- Data of this study can be used to design the electrocoagulation experiments for removal of wide range of pollutant in wastewater.
- Data are important for discharge environment especially resource water, aqueous and agriculture.

1. Data

In this article the data in Table 1 present the measured parameters and characteristics of the raw grey water that used for description of experiments. Calculated values of K (1/min) and kWh/m³ in the grey water effluent are reported in Table 2. Figs. 1 and 2 show data of different arrangements under optimal conditions applied in this study. The maximum removal efficiency (90.18%) of COD and

Table 1

Parameters measured and characteristics of the raw carwash wastewater used for this study.

Parameter	Range	Unit	Raw wastewater Mean \pm S.D
pH	3, 7, 11	–	7.08 \pm 0.03
Steering time	30, 60, 90	min	–
Voltage	10, 20, 30	Volt	–
Electrode type	Al–Al, Fe–Fe, Al–Fe	–	–
BOD	–	(mg/L)	(102–246) \pm 207.3
COD	–	(mg/L)	(480–1560) \pm 207.3

Table 2Electrode type, voltage, pH, K (1/min) and kWh/m³ values in the removal of COD and BOD in the present study.

Electrode type	Voltage	pH	K (1/min)	kWh/m ³
Fe–Fe	30	7	14.15	787.5
		3	11.61	1575
		11	8.73	2362.5
	20	7	10.29	450
		3	9.76	900
		11	9.24	1350
	10	7	8.53	189
		3	4.43	378
		11	3.62	567
Al–Al	30	7	18.24	675
		3	13.92	1350
		11	15.10	2025
	20	7	14.58	330
		3	10.80	660
		11	10.51	990
	10	7	12.23	159
		3	8.27	318
		11	8.91	477
Al–Fe	30	7	13.99	900
		3	13.89	1800
		11	11.42	2700
	20	7	11.79	540
		3	9.77	1080
		11	11.30	1620
	10	7	9.76	240
		3	8.17	480
		11	6.21	720

K (1/min) is the rate constant of removal (1/min) related to the removal of COD and BOD.

BOD was obtained at optimum pH=7, level of 30 voltage, and contact time of 90 min. The effects of optimum parameters on removal efficiency of COD and BOD are shown in Fig. 3.

2. Experimental design, materials and methods

2.1. Sample collection and analytical procedures

Our data set was obtained from All Car washes. The raw grey water was obtained along the Ahvaz in Iran. The initial concentration of samples has been tested for determination of COD and BOD. To

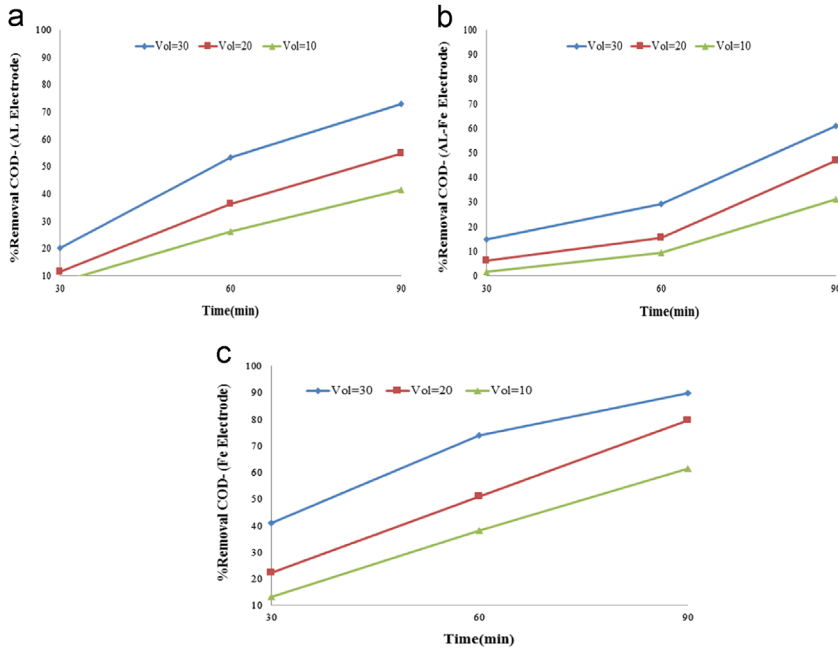


Fig. 1. (a) Aluminum electrode, (b) Aluminum – Iron electrode, and (c) Iron electrode applied in the different Voltage on COD removal efficiency .

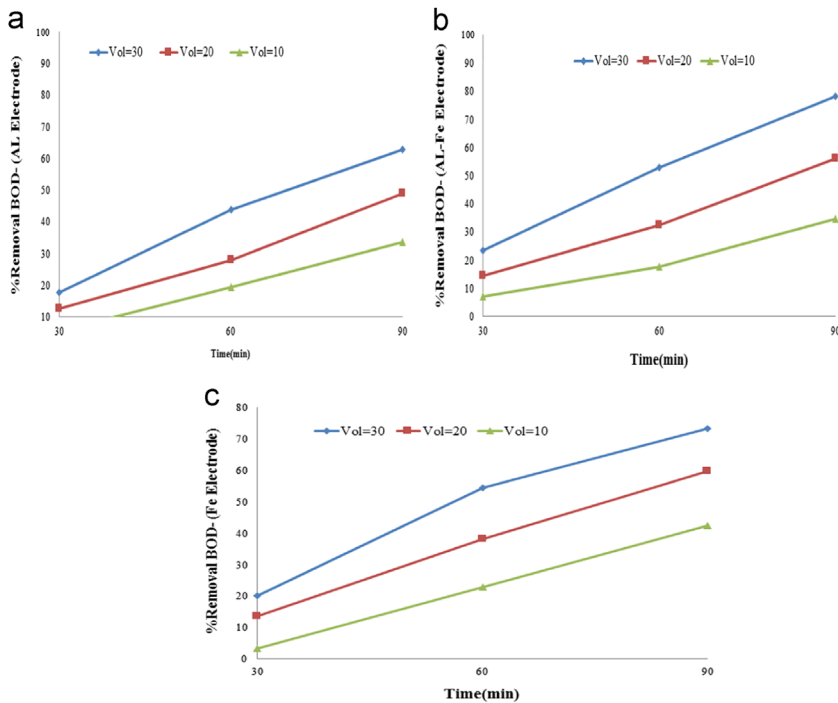


Fig. 2. (a) Aluminum electrode, (b) Aluminum – Iron electrode, and (c) Iron electrode applied in the different Voltage on BOD removal efficiency .

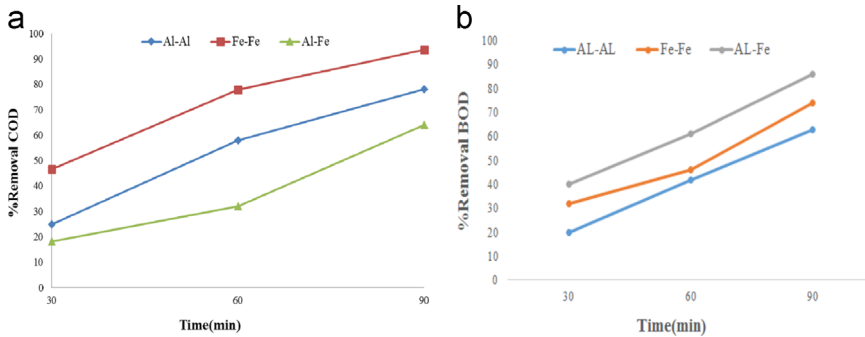


Fig. 3. (a) Aluminum electrode, (b) Aluminum – Iron electrode, and (c) Iron electrode applied in the optimum pH=7 and voltage=30 on COD and BOD removal efficiency.

adjust the primary pH of the solution, the sulfuric acid and one-tenth normal sodium hydroxide were used. A lab-scale reactor with diameters of 15 cm × 15 cm × 15cm was used for performing experiments. Sulfuric acid (H₂SO₄), potassium dichromate (K₂Cr₂O₇), mercury sulfate (HgSO₄), silver sulfate (Ag₂SO₄), potassium hydrogen phthalate (C₈H₅KO₄), 3-methyl-2-benzothiazoline hydrazine were used for preparing COD and BOD solutions in grey water. Steering time of 30, 60 and 90 min, voltage values of 10, 20 and 30 v were used in this study. At each experiment, removal efficiency of COD and BOD in grey water with special Al–Al, Al–Fe, Fe–Fe electrode was investigated. Spectrophotometer (DR/5000 UV–vis HACH) was used to investigate the remaining concentration level of COD and BOD in the grey water effluent [5]. Following equation was applied to calculate the electrocoagulation electrical energy consumption during experiments [4,5].

$$\frac{EE}{V} = \frac{U \times I \times t}{V_r}$$

where: U is voltage used in the process (V), I is intensity of the applied current (A), t is reaction time (min) and V_r is reactor volume (Lit).

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Transparency document. Supporting information

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