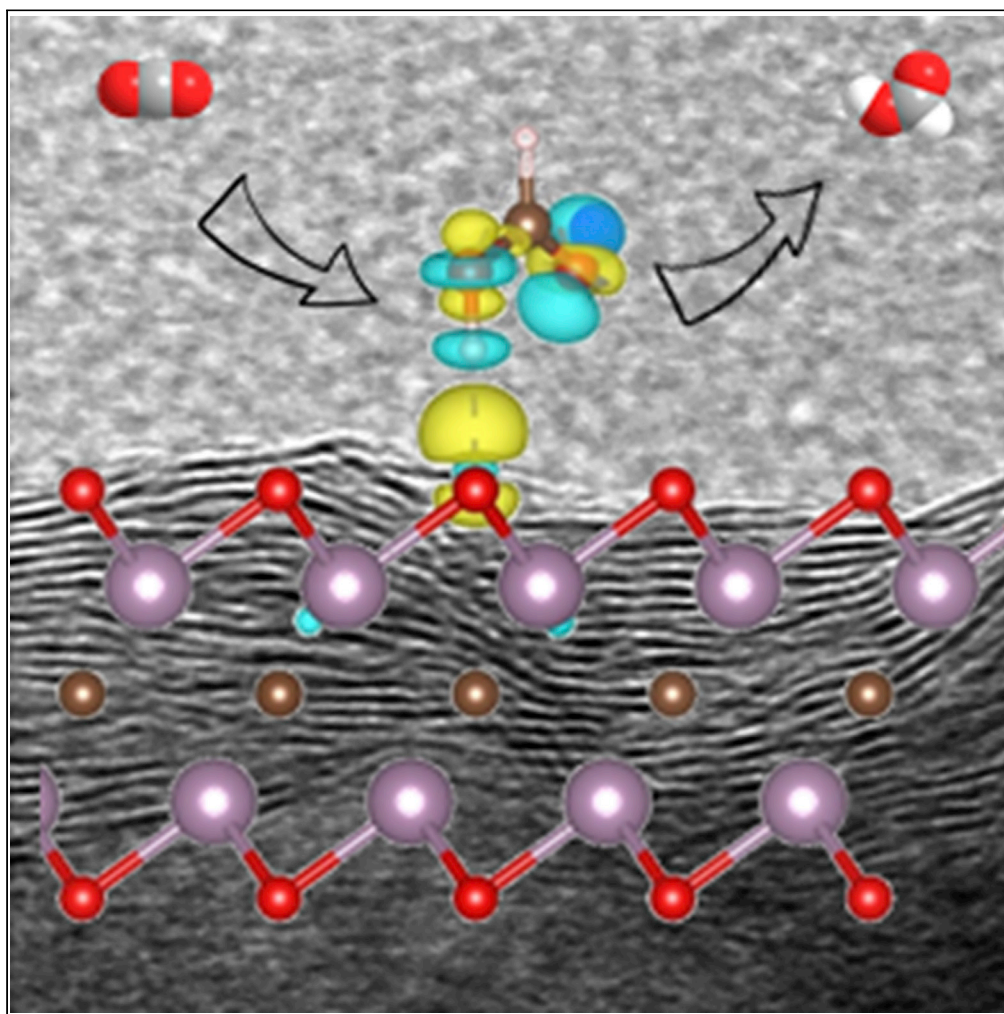


## Article

Two-Dimensional Titanium and Molybdenum Carbide MXenes as Electrocatalysts for CO<sub>2</sub> Reduction

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**HIGHLIGHTS**

Combined experimental  
and theoretical CO<sub>2</sub>RR  
investigation on MXenes

T<sub>x</sub> group stabilizes \*H-  
coordinated  
intermediates and breaks  
scaling relations

Formic acid is the main  
CO<sub>2</sub>RR product on Ti<sub>2</sub>CT<sub>x</sub>  
and Mo<sub>2</sub>CT<sub>x</sub> MXenes

Lower degree of -F  
termination in T<sub>x</sub> group  
results in smaller  
overpotential

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## Article

Two-Dimensional Titanium and Molybdenum Carbide MXenes as Electrocatalysts for CO<sub>2</sub> ReductionAlbertus D. Handoko,<sup>1</sup> Hetian Chen,<sup>2</sup> Yanwei Lum,<sup>1</sup> Qianfan Zhang,<sup>2,\*</sup> Babak Anasori,<sup>3,4,\*</sup> and Zhi Wei Seh<sup>1,5,\*</sup>

## SUMMARY

**Electrocatalytic CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) is an attractive way to produce renewable fuel and chemical feedstock, especially when coupled with efficient CO<sub>2</sub> capture and clean energy sources. On the fundamental side, research on improving CO<sub>2</sub>RR activity still revolves around late transition metal-based catalysts, which are limited by unfavorable scaling relations despite intense investigation. Here, we report a combined experimental and theoretical investigation into electrocatalytic CO<sub>2</sub>RR on Ti- and Mo-based MXene catalysts. Formic acid is found as the main product on Ti<sub>2</sub>CT<sub>x</sub> and Mo<sub>2</sub>CT<sub>x</sub> MXenes, with peak Faradaic efficiency of over 56% on Ti<sub>2</sub>CT<sub>x</sub> and partial current density of up to  $-2.5 \text{ mA cm}^{-2}$  on Mo<sub>2</sub>CT<sub>x</sub>. Furthermore, simulations reveal the critical role of the T<sub>x</sub> group: a smaller overpotential is found to occur at lower amounts of -F termination. This work represents an important step toward experimental demonstration of MXenes for more complex electrocatalytic reactions in the future.**

## INTRODUCTION

Efforts to tackle rising CO<sub>2</sub> concentration in the atmosphere have been primarily focused on carbon capture and sequestration, as well as decarbonization of the energy and land use sectors (Walsh et al., 2017). However, an equally pressing issue of depleting fossil energy and chemical raw materials is looming. Electrocatalytic CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) presents an attractive pathway to achieve both decarbonization of energy economy and production of renewable fuel/chemical feedstock (De Luna et al., 2019; Seh et al., 2017), especially when coupled with increasingly affordable clean electricity (Obama, 2017).

To realize industrial-scale CO<sub>2</sub>RR, substantial challenges on both the fundamental (i.e., catalyst activity and selectivity) and system levels (i.e., mass transport, conversion rate, and energy efficiency) need to be addressed (Jouny et al., 2018; De Luna et al., 2019; Handoko et al., 2018c; Higgins et al., 2019). On the fundamental side, there has been some progress in understanding CO<sub>2</sub>RR in liquid electrolytes, with emphasis on late transition metals, particularly copper, owing to its unusual ability to convert CO<sub>2</sub> to multi-carbon products (Hori, 2008; Huang et al., 2017). However, despite intense optimization of these transition metal catalysts (Saber Safaei et al., 2016; Handoko et al., 2016; Mistry et al., 2016; Li et al., 2017b; Ren et al., 2016), their activity and selectivity seem to be limited. One of the most significant barriers limiting fundamental CO<sub>2</sub>RR on transition metal catalysts appears to be the linear scaling relations between the binding energies of reaction intermediates (Liu et al., 2017). These unfavorable scaling relations due to similarly bound reaction intermediates (e.g., \*COOH, \*CO, \*CHO, "\*" refers to a site on the catalyst surface) limit the CO<sub>2</sub>RR overpotential that can be achieved on pure transition metal surfaces.

One of the most promising ways to improve CO<sub>2</sub>RR activity is to explore new catalyst material systems that allow stabilization of intermediates with different scaling relations. MXenes, a family of two-dimensional transition metal carbide/nitride materials with metallic-like conductivity (Anasori et al., 2017), present a viable solution. MXenes have a general formula of M<sub>n+1</sub>X<sub>n</sub>T<sub>x</sub>, where M represents an early transition metal, X is carbon and/or nitrogen, with n in the range of 1–4 (Anasori and Gogotsi, 2019; Deysher et al., 2020). T<sub>x</sub> represents surface termination groups, which can include -O, -F, etc. (Hope et al., 2016). The tunable surface and internal configuration of MXenes, including the possibility of mixed surface terminations, as well as mixed metal atoms in solid solution (Yang et al., 2016) or ordered structure (Anasori et al., 2015; Anasori and Gogotsi, 2019), allow for tailoring of intermediates' binding configuration and strength (Hart et al., 2019; Anasori et al., 2016; Handoko et al., 2018a; Chen et al., 2019), making it an ideal platform to search for active and selective CO<sub>2</sub>RR catalysts (Handoko et al., 2019). To date, investigations of MXenes for

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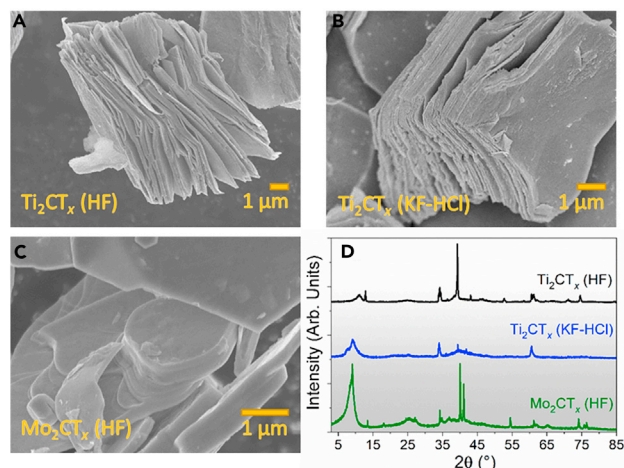
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**Figure 1. Morphology and Phase Characterization of  $Ti_2CT_x$  and  $Mo_2CT_x$  MXenes**

Scanning electron micrographs of as-synthesized (A)  $Ti_2CT_x$  (HF), (B)  $Ti_2CT_x$  (KF-HCl), and (C)  $Mo_2CT_x$  (HF) and (D) the corresponding X-ray diffraction data.

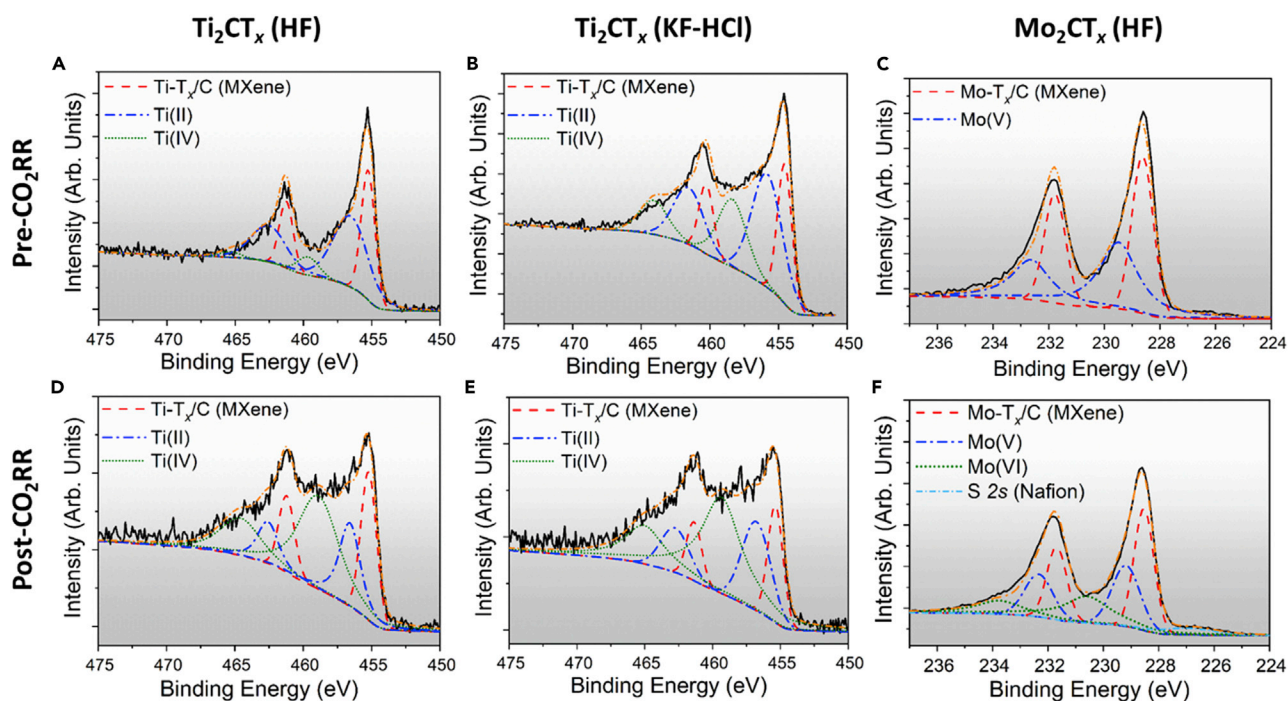
electrocatalytic  $CO_2RR$  have been primarily based on theoretical calculations (Li et al., 2017a; Handoko et al., 2018b; Chen et al., 2019; Zhang et al., 2017b), although some works on photocatalytic  $CO_2RR$  have indicated that MXenes may enhance charge separation or act as co-catalyst (Cao et al., 2018; Ye et al., 2018).

Here, we investigate the electrocatalytic  $CO_2RR$  activity on  $Ti_2CT_x$  and  $Mo_2CT_x$  MXenes using a combination of experiment and theory. These MXenes were chosen as they have Ti and Mo metal sites with opposing hydrogen binding behavior (Laursen et al., 2012). The  $CO_2RR$  experiments are carried out in mixtures of acetonitrile, water, and 3-butyl-1-methyl-1H-imidazol-3-ium tetra-fluoroborate ( $BMIMBF_4$ ) electrolyte. Formic acid is found to be the main  $CO_2RR$  product on these MXenes with Faradaic efficiency of 56.1% at  $-1.8$  V (all potentials in this work are expressed with respect to the standard hydrogen electrode, SHE).  $H_2$  is the main side product, alongside trace amounts of CO,  $CH_4$ , and other hydrocarbons. More importantly, we demonstrate that the nature of surface terminating group appears to control the  $CO_2RR$  activity. Specifically, the presence of  $-F$  termination group, commonly adsorbed onto MXene surface during synthesis (Hope et al., 2016), was found to alter the binding strength of intermediates and the corresponding  $CO_2RR$  limiting potential compared to fully  $-O$  terminated MXenes, as supported by density functional theory (DFT). Overall, this work provides insights on MXene electrocatalysts that circumvent traditional scaling relations in  $CO_2RR$ , which can potentially be extended to other promising reactions of interest.

## RESULTS

We first investigate the effect of surface termination group  $T_x$  on the  $CO_2RR$  activity of  $Ti_2CT_x$  MXenes. To achieve this, we synthesized two variants of  $Ti_2CT_x$  with different surface termination compositions using different etching procedures, namely, 18 h in 10% HF and 48 h in 4 M KF-HCl mixture (refer to the Transparent Methods in the Supplemental Information). These MXenes will be referred to as  $Ti_2CT_x$  (HF) and  $Ti_2CT_x$  (KF-HCl), respectively. Previous works suggest that the use of fluoride salt etching solution in place of HF can reduce the amounts of  $-F$  terminations (Hope et al., 2016; Handoko et al., 2018a). The scanning electron micrographs of both  $Ti_2CT_x$  (HF) and  $Ti_2CT_x$  (KF-HCl) show layered structures after the etching procedure (Figures 1A and 1B), consistent with previously reported morphologies (Anasori et al., 2017). X-ray diffraction (XRD) shows that most of the  $Ti_2AlC$  precursors are successfully converted to  $Ti_2CT_x$ , with the appearance of the characteristic (002) broad peaks of MXenes around  $2\theta = 11.1^\circ$  and  $9.2^\circ$  for HF and KF-HCl etched  $Ti_2CT_x$ , respectively (Figure 1D; see Figure S1 and Table S1 for characterization of precursors). These peaks correspond to MXene interlayer distances of around 8.0 and 9.6 Å, consistent with previous reports on smaller interlayer distance for HF-etched samples Naguib et al., 2012.

X-ray photoelectron spectroscopy (XPS) of the as-synthesized  $Ti_2CT_x$  samples in the Ti 2p range detects a mix of Ti species, including Ti- $T_x/C$ , Ti(II), and more oxidized Ti(IV) species (Figures 2A and 2B; see Tables



**Figure 2. Analysis of the "M" Elements of  $Ti_2CT_x$  and  $Mo_2CT_x$  MXenes**

X-ray photoelectron spectroscopy measurements of MXenes before and after  $CO_2RR$ : (A and D) Ti 2p spectra of  $Ti_2CT_x$  (HF), (B and E) Ti 2p spectra of  $Ti_2CT_x$  (KF-HCl), (C and F) Mo 3d spectra of  $Mo_2CT_x$  (HF).

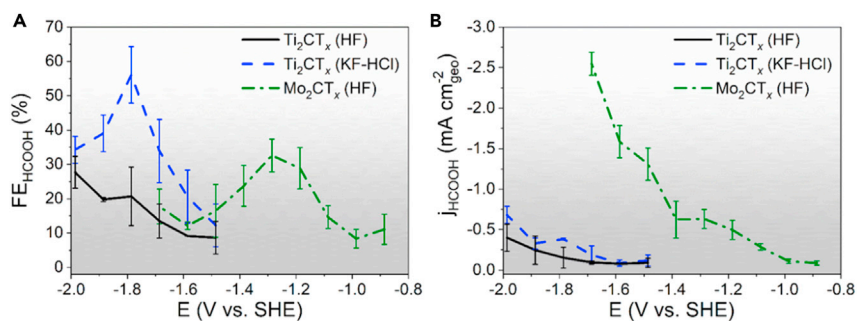
S2–S5 for more details). Some degree of Ti(IV) formation is unavoidable in  $Ti_2CT_x$  as it is less stable against oxidation compared with other MXenes with higher  $n$  such as  $Ti_3C_2T_x$  (Zhang et al., 2017a). A comparison of the F to Ti atomic ratio (Tables S3 and S4) shows that  $Ti_2CT_x$  (HF) has significantly more –F surface terminations ( $F/Ti = 0.36$ ) than  $Ti_2CT_x$  (KF-HCl) ( $F/Ti = 0.21$ ). We have previously shown that the electrocatalytic activities of MXenes are very sensitive to the surface termination (Handoko et al., 2018a), thus we posit that the variation in –F termination content on  $Ti_2CT_x$  samples will alter their  $CO_2RR$  activity.

As an initial  $CO_2RR$  activity assessment, we first compared the linear scanning voltammetry (LSV) profile of  $Ti_2CT_x$  (HF) and  $Ti_2CT_x$  (KF-HCl) in the presence and absence of  $CO_2$  in a mixture of 80:15:5 mol fraction of acetonitrile:water:BMIMBF<sub>4</sub> electrolyte (Figure S2). The electrolyte mixture is used in this study owing to prevalent HER in aqueous electrolyte systems like 0.1 M KHCO<sub>3</sub> (Figure S3). Dipolar aprotic solvents like acetonitrile have enhanced  $CO_2$  solubility compared with aqueous systems (Gennaro et al., 1990). Furthermore, imidazolium-based ionic liquid has been shown to enhance  $CO_2RR$  (Asadi et al., 2016), possibly by forming complexes with  $CO_2$  molecules at moderately cathodic potentials (–0.1 V versus SHE) (Matsubara et al., 2015; Rosen et al., 2011).

Under  $N_2$  purging, both  $Ti_2CT_x$  samples display sharp onset potential at around –1.8 V (Figures S2A and S2B), which can be attributed to the hydrogen evolution reaction (HER). The introduction of  $CO_2$  into the reaction environment changes the LSV profile for both  $Ti_2CT_x$  samples significantly. Most notably, some cathodic features are observed around –1.4 to –1.8 V. These features were especially clear on  $Ti_2CT_x$  (KF-HCl), indicating more significant  $*CO_2$  (or related intermediates) adsorption and interaction (Salehi-Khojin et al., 2013) compared with  $Ti_2CT_x$  (HF). Additionally, the HER onset potentials on both  $Ti_2CT_x$  samples are delayed by about –0.1 to –0.2 V with reduced current density. As the electrolyte pH (~1.24) and reference electrode are unaffected by  $CO_2$  purging (Figure S4), this HER “poisoning” effect can be attributed to  $*CO_2$  (or related intermediates) adsorption that competes with  $*H$ . Such an effect is expected on transition metal surfaces that show weak  $*H$  binding strength like Ti (Huang et al., 2017; Zhang et al., 2014).

To quantify their  $CO_2RR$  activity, both  $Ti_2CT_x$  samples are subjected to chronoamperometric (constant voltage) measurement for 100 min under continuous  $CO_2$  gas purging in a two-compartment cell





**Figure 3. CO<sub>2</sub>RR Selectivity and Activity on Ti<sub>2</sub>CT<sub>x</sub> and Mo<sub>2</sub>CT<sub>x</sub> MXenes**

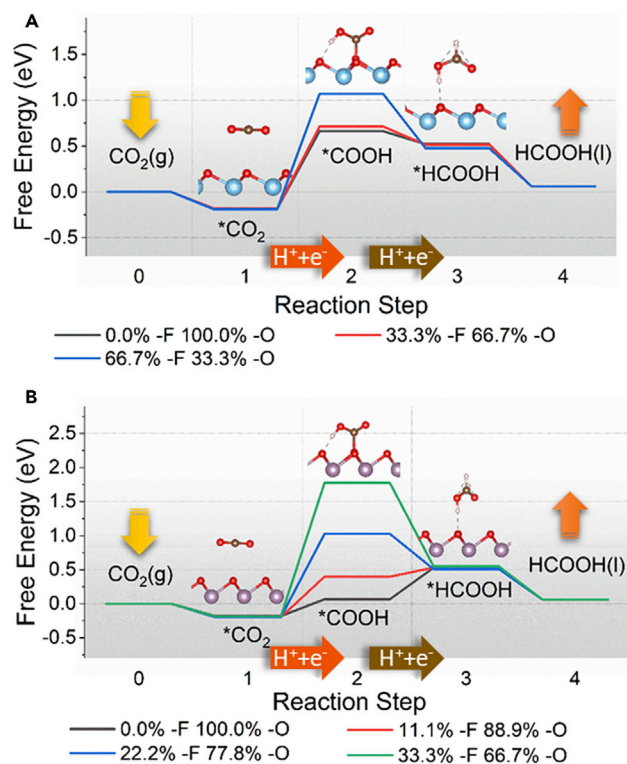
Comparison of (A) Faradaic efficiency and (B) partial current density normalized by geometric surface area for CO<sub>2</sub>RR to formic acid on Ti<sub>2</sub>CT<sub>x</sub> and Mo<sub>2</sub>CT<sub>x</sub> MXenes. Error bars represent one standard deviation of three independent measurements.

(Figure S5). Both Ti<sub>2</sub>CT<sub>x</sub> samples retain most of their characteristic XPS peaks after CO<sub>2</sub>RR, with slight increase in the more oxidized Ti(IV) signals due to ambient exposure during testing (Figures 2D and 2E). Online gas chromatography (GC) and nuclear magnetic resonance (NMR) were used to quantify gaseous and liquid products from CO<sub>2</sub>RR, revealing formic acid and H<sub>2</sub> to be the main products on both Ti<sub>2</sub>CT<sub>x</sub> samples (Figures 3 and S6). It is clear from the Faradaic efficiency (FE) plot (Figure 3A) and partial current density (j) plot (Figure 3B) that Ti<sub>2</sub>CT<sub>x</sub> (KF-HCl) shows enhanced selectivity and turnover for CO<sub>2</sub>RR to formic acid compared with Ti<sub>2</sub>CT<sub>x</sub> (HF), although the CO<sub>2</sub>RR onset potentials are similar for both samples at -1.5 V. At a potential of -1.8 V, Ti<sub>2</sub>CT<sub>x</sub> (KF-HCl) displays 56.1% FE<sub>HCOOH</sub> compared with 20.7% on Ti<sub>2</sub>CT<sub>x</sub> (HF), with a corresponding 2.5 times higher j<sub>HCOOH</sub> normalized to geometric surface area. Plots of j<sub>HCOOH</sub> normalized to electrochemical surface area are also shown in Figure S7 and Table S6.

To gain insight on the experimental results, we turn to DFT calculations to systematically investigate the effect of varying amounts of -F termination group on the theoretical CO<sub>2</sub>RR overpotential on Ti<sub>2</sub>CT<sub>x</sub> samples. In particular, three different Ti<sub>2</sub>CT<sub>x</sub> structures were modeled with T<sub>x</sub> groups comprising (1) 0.0% -F, 100.0% -O, (2) 33.3% -F, 66.7% -O, and (3) 66.7% -F, 33.3% -O (Figure S8). The T<sub>x</sub> compositions were selected based on the range of -F termination previously studied on Ti-based MXenes (Handoko et al., 2018a). On fully -O terminated Ti<sub>2</sub>CT<sub>x</sub> surface, CO<sub>2</sub>RR to formic acid is completed in four steps, including a CO<sub>2</sub> adsorption step, two consecutive proton-coupled electron transfer (PCET) steps, and finally an HCOOH (l) desorption step (Figure 4A). In this case, only the \*COOH pathway was considered, as the alternative route through HCOO intermediate was found to be unfavorable (Figure S9), consistent with the literature (Li et al., 2017a). The \*CO<sub>2</sub> + H<sup>+</sup> + e<sup>-</sup> → \*COOH step (PCET-1) is predicted to be potential limiting with a free energy change (ΔG<sub>elem</sub>, at 0 V applied potential) of 0.85 eV. Hence, the theoretical CO<sub>2</sub>RR limiting potential (UL<sub>CO<sub>2</sub></sub> = -ΔG<sub>elem</sub>/e) can be calculated to be -0.85 V.

Gradual -F substitution of the -O T<sub>x</sub> group in Ti<sub>2</sub>CT<sub>x</sub> results in significant variation of reaction free energy (Figure 4A). Specifically, the PCET-1 potential limiting step becomes more endergonic (larger ΔG<sub>elem</sub>) at a higher fraction of -F substitution. As a result, the UL<sub>CO<sub>2</sub></sub> becomes more negative at -0.89 and -1.26 V for 33.3% and 66.7% -F, respectively, possibly due to increasingly unstable \*COOH conformations (Figure S8). As \*HCOOH adsorption energy does not change substantially with -F substitution, we observe that the PCET-1 reaction step remains potential limiting throughout. This means that the least negative UL<sub>CO<sub>2</sub></sub> can only be achieved on fully -O terminated Ti<sub>2</sub>CT<sub>x</sub>. These simulation results explain the higher FE<sub>HCOOH</sub> and j<sub>HCOOH</sub> observed on Ti<sub>2</sub>CT<sub>x</sub> (KF-HCl) as it has significantly lower -F surface termination compared with Ti<sub>2</sub>CT<sub>x</sub> (HF).

To study if the effect of -F substitution is common to other MXenes, we expand the investigation to Mo<sub>2</sub>CT<sub>x</sub>. In this case, only HF etching is used, as milder KF-HCl etchant is not able to etch Mo<sub>2</sub>Ga<sub>2</sub>C precursor. Nonetheless, Mo<sub>2</sub>CT<sub>x</sub> could potentially be a better CO<sub>2</sub>RR catalyst as it tends to have fewer -F terminations than Ti<sub>2</sub>CT<sub>x</sub> even when a harsher etching condition using 48% HF is used (Halim et al., 2016). The morphology of Mo<sub>2</sub>CT<sub>x</sub> is slightly different than Ti<sub>2</sub>CT<sub>x</sub> with less obvious delamination between the layers (Figure 1C), consistent with previous studies (Halim et al., 2016). XRD analyses also indicate successful etching of most Mo<sub>2</sub>Ga<sub>2</sub>C precursor, with a broad peak at 2θ = 9.0° indicative of a (002) interlayer distance of around 9.8 Å (Figure 1D; see Figure S1 and Table S1 for characterization of precursors). XPS shows a



**Figure 4. Density Functional Theory Calculations for CO<sub>2</sub>RR to Formic Acid on Ti<sub>2</sub>CT<sub>x</sub> and Mo<sub>2</sub>CT<sub>x</sub> MXenes**

Calculated free energy diagram at 0 V applied potential for CO<sub>2</sub>RR to formic acid on (A) Ti<sub>2</sub>CT<sub>x</sub> and (B) Mo<sub>2</sub>CT<sub>x</sub> MXenes with varying fractions of -F and -O surface terminating groups. Blue, purple, red, brown, and white spheres represent Ti, Mo, O, C, and H atoms, respectively.

relatively large Mo-T<sub>x</sub>/C component with no signs of Mo(VI) (Figure 2C). The F/Mo atomic ratio is estimated to be 0.03 (Table S5).

Initial LSV assessments under N<sub>2</sub> purging show earlier HER onset potential on Mo<sub>2</sub>CT<sub>x</sub> around -1.3 V (Figure S2C), which is consistent with its superior HER activity (Handoko et al., 2018a; Seh et al., 2016). However, it is unusual that Mo<sub>2</sub>CT<sub>x</sub> also displayed a similar HER poisoning effect under CO<sub>2</sub> purging since, unlike Ti, Mo should bind to \*H strongly (Laurson et al., 2012). The observation of HER poisoning on both MXenes suggests that the interaction of \*CO<sub>2</sub> or other intermediates with the T<sub>x</sub> groups is possibly more critical than that with the base metal sites.

GC and NMR analysis during chronoamperometric measurements revealed that Mo<sub>2</sub>CT<sub>x</sub> starts forming formic acid at much less negative potential (-0.9 V) than both types of Ti<sub>2</sub>CT<sub>x</sub> (-1.5 V). This is consistent with the cathodic features observed in LSV under CO<sub>2</sub> purging (Figure S2C). Although the maximum FE<sub>HCOOH</sub> of Mo<sub>2</sub>CT<sub>x</sub> (32.6% at -1.3 V, Figure 3A) is lower compared with Ti<sub>2</sub>CT<sub>x</sub> (KF-HCl, 56.1% at -1.8 V), the former shows significantly higher j<sub>HCOOH</sub> up to -2.5 mA cm<sup>-2</sup><sub>geo</sub> at less negative potentials (Figure 3B), suggesting that it is quite active in reducing CO<sub>2</sub> to formic acid. The stability of CO<sub>2</sub>RR on Mo<sub>2</sub>CT<sub>x</sub> is assessed by conducting continuous electrolysis for 500 min. Some fluctuation in FE<sub>HCOOH</sub> from 39.9% in the 100<sup>th</sup> minute to 25.7% in the 500<sup>th</sup> minute was observed (Figure S10A). We attribute the apparent FE<sub>HCOOH</sub> instability to the loss of volatile acetonitrile in the electrolyte during continuous purging rather than catalyst deactivation, as no degradation of j<sub>HCOOH</sub> is observed (Figure S10B). Gradual evaporation of acetonitrile would alter the electrolyte composition and increase the water proportion, leading to higher HER turnover that dominates the total current density (Figure S10B). Loss of volatile electrolyte component is a common issue for analytical electrochemical systems that require continuous sampling (Lazouski et al., 2020).

Mo<sub>2</sub>CT<sub>x</sub> was found to retain most of its characteristic XPS peaks after CO<sub>2</sub>RRR as well (Figure 2F). The earlier onset and higher turnover for CO<sub>2</sub>RR to formic acid on Mo<sub>2</sub>CT<sub>x</sub> is unexpected owing to its predisposition

for catalyzing HER (Seh et al., 2016; Pan, 2016; Handoko et al., 2018a). As such, Mo-based MXenes have not been considered active for CO<sub>2</sub>RR in previous computational studies (Handoko et al., 2018b; Morales-García et al., 2018; Chen et al., 2019), with the exception of a hypothetical Mo<sub>3</sub>C<sub>2</sub>(OH)<sub>2</sub> structure (Li et al., 2017a).

To explain the experimental finding on Mo<sub>2</sub>CT<sub>x</sub>, we turn back to DFT calculations to examine CO<sub>2</sub>RR steps on this surface. Similar to Ti<sub>2</sub>CT<sub>x</sub>, we construct fully –O terminated Mo<sub>2</sub>CT<sub>x</sub> and gradually replace the T<sub>x</sub> with –F, but this time at lower fractions of 11.1%, 22.2%, and 33.3% (Figure S11) owing to fewer –F terminations detected experimentally. On fully –O terminated Mo<sub>2</sub>CT<sub>x</sub>, the reaction step \*COOH + H<sup>+</sup> + e<sup>–</sup> → \*HCOOH (PCET-2) with ΔG<sub>elem</sub> of 0.47 eV (and UL<sub>CO<sub>2</sub></sub> of –0.47 V) is found to be potential limiting. Here, –F substitution on Mo<sub>2</sub>CT<sub>x</sub> appears to affect CO<sub>2</sub>RR intermediates more significantly than on Ti<sub>2</sub>CT<sub>x</sub> (Figure 4B). We observe on Mo<sub>2</sub>CT<sub>x</sub> that the ΔG<sub>elem</sub> of PCET-1 increases significantly by 0.35 eV after substitution of only 11.1% of the –O termination to –F. This is in contrast to the 0.05 eV change observed on Ti<sub>2</sub>CT<sub>x</sub> when 33.3% of the –O T<sub>x</sub> group is replaced by –F (Figure 4A).

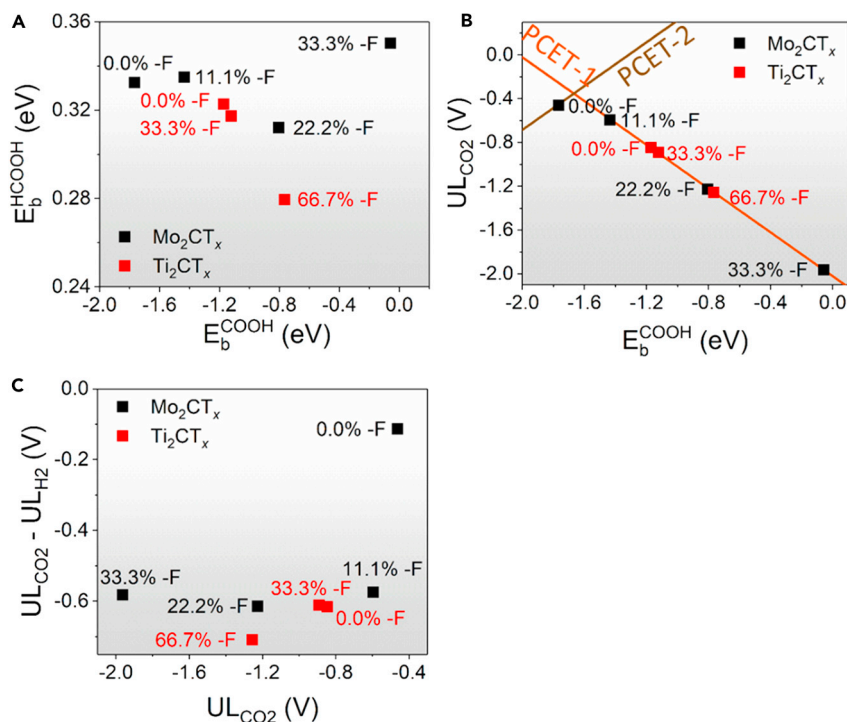
More interestingly, we note that the presence of –F T<sub>x</sub> group on Mo<sub>2</sub>CT<sub>x</sub> changes the potential limiting step from PCET-2 on fully –O terminated surface to PCET-1 after 11.1% –F substitution. This means that the lowest UL<sub>CO<sub>2</sub></sub> can be found at low fraction of –F substitution, between 0% and 11.1%, that equalize the ΔG<sub>elem</sub> of PCET-1 and PCET-2. Quadratic functions fitting of the \*COOH free energy and the respective limiting potential at different fractions of –F substitution suggest that such a minimum can be found at around 4.2% –F (Figure S12A).

One possible reason for the unique CO<sub>2</sub>RR behavior on Ti<sub>2</sub>CT<sub>x</sub> and Mo<sub>2</sub>CT<sub>x</sub> MXenes could lie in the preference toward the \*HCOOH pathway. Unlike late transition metal catalysts, where a majority of CO<sub>2</sub>RR goes through the ubiquitous \*CO intermediate (Peterson and Nørskov, 2012), the reaction path through \*HCOOH intermediate is favorable on MXenes owing to the hydrogen-bond interaction between \*HCOOH and the T<sub>x</sub> groups, particularly –O (Figure S13). The preference toward the \*HCOOH pathway results in non-linear scaling with \*COOH in terms of their binding energies, as these two intermediates are coordinated differently on the MXene surfaces (Figure 5A). In general, \*COOH binds to the –O T<sub>x</sub> groups on MXene surfaces through C atom, whereas \*HCOOH binds through the H atom (Figures S8, S11, and S13). A volcano-like plot of limiting potentials can then be constructed, with boundaries drawn to mark the neutral potential of PCET-1 (orange line) and PCET-2 (brown line) reaction steps with respect to \*COOH binding energy (Figure 5B). A majority of the catalysts are governed by the PCET-1 step, where less negative UL<sub>CO<sub>2</sub></sub> is achieved at stronger \*COOH binding energy, up to a point where protonation of \*COOH to \*HCOOH becomes difficult. It can be seen that fully –O terminated Mo<sub>2</sub>CT<sub>x</sub> sits atop the volcano, near to the ideal case where both PCET-1 and PCET-2 can proceed at the same limiting potential.

We also examined the HER reaction steps on both Ti<sub>2</sub>CT<sub>x</sub> and Mo<sub>2</sub>CT<sub>x</sub> surfaces at various –F substitution using DFT calculation (Figure S14). This is important as HER is the main competition to CO<sub>2</sub>RR on these surfaces. Compared with CO<sub>2</sub>RR, HER is a simpler reaction, which can be represented by: \* + H<sup>+</sup> + e<sup>–</sup> → \*H → 1/2 H<sub>2</sub> (g) + \*. It is found that –F substitution generally destabilizes \*H adsorption due to much weaker H-F interaction. The weaker \*H results in a more negative HER limiting potential (UL<sub>H<sub>2</sub></sub>) nearly on all cases, except on Mo<sub>2</sub>CT<sub>x</sub> with 11.1% –F substitution where the limiting potential is close to the ideal value (–0.02 V, Figure S12B).

The difference between the limiting potentials of CO<sub>2</sub>RR and HER (UL<sub>CO<sub>2</sub></sub>–UL<sub>H<sub>2</sub></sub>) could then be used to gauge the selectivity of the catalysts toward CO<sub>2</sub>RR (Hong et al., 2016; Shi et al., 2014). In addition to having the least negative UL<sub>CO<sub>2</sub></sub> value, we found that –O terminated Mo<sub>2</sub>CT<sub>x</sub> also possesses the least negative UL<sub>CO<sub>2</sub></sub>–UL<sub>H<sub>2</sub></sub> difference of –0.1 V (Figure 5C). Quadratic functions fitting of UL<sub>CO<sub>2</sub></sub>–UL<sub>H<sub>2</sub></sub> on Mo<sub>2</sub>CT<sub>x</sub> identifies a minimum at 3.8% –F substitution (Figure S12B), indicating that low amounts of –F T<sub>x</sub> presence may be beneficial to CO<sub>2</sub>RR.

Although the UL<sub>CO<sub>2</sub></sub>–UL<sub>H<sub>2</sub></sub> values on all variants of Ti<sub>2</sub>CT<sub>x</sub> and Mo<sub>2</sub>CT<sub>x</sub> are still generally negative across all fractions of –F substitutions, we recognize that the kinetics of both HER and CO<sub>2</sub>RR can be significantly altered by the reaction environment (König et al., 2019). In addition to the enhanced CO<sub>2</sub> solubility in acetonitrile, the formation of BMIM-CO<sub>2</sub> complex has been shown to enhance CO<sub>2</sub> mass transport and significantly boost CO<sub>2</sub>RR activity (Rosen et al., 2011). Furthermore, the hydrophobic BMIM cation has been



**Figure 5. Relations between Binding Energies of Different CO<sub>2</sub>RR Reaction Intermediates on Ti<sub>2</sub>CT<sub>x</sub> and Mo<sub>2</sub>CT<sub>x</sub> MXenes**

(A) \*HCOOH binding energy plot against \*COOH binding energy showing deviation from linear scaling relations. (B) Limiting CO<sub>2</sub>RR potentials for elementary steps. The lines represent the calculated potential where the most negative reaction steps are neutral as a function of \*COOH binding energy (PCET-1: \*CO<sub>2</sub> + H<sup>+</sup> + e<sup>-</sup> → \*COOH; PCET-2: \*COOH + H<sup>+</sup> + e<sup>-</sup> → \*HCOOH). (C) Calculated UL<sub>CO2</sub>-UL<sub>H2</sub> plot with respect to UL<sub>CO2</sub> on all variants of Ti<sub>2</sub>CT<sub>x</sub> and Mo<sub>2</sub>CT<sub>x</sub> theoretical models with different -F T<sub>x</sub> termination fractions in this study.

proposed to populate near the catalyst surface and suppress HER upon application of CO<sub>2</sub>RR-relevant cathodic potentials (Rosen et al., 2012).

Apart from formic acid, we also detected up to 1.1% FE of CO and trace amounts of CH<sub>4</sub> and multi-carbon products (Figures S15–S17). Our finding partially validates the CO<sub>2</sub>RR route via a \*HCOOH intermediate (Li et al., 2017a; Handoko et al., 2018b; Chen et al., 2019), although further optimization of MXene surface terminations (Table S7 and S8 and Figures S18–S22) is necessary to enhance the \*HCOOH intermediate stability for the production of more reduced moieties like CH<sub>4</sub> and multi-carbon products.

## DISCUSSION

In this work, we report a combined experimental and theoretical CO<sub>2</sub>RR investigation on Ti<sub>2</sub>CT<sub>x</sub> and Mo<sub>2</sub>CT<sub>x</sub> MXenes. Formic acid is found to be the main CO<sub>2</sub>RR product with maximum FE exceeding 56% at -1.8 V versus SHE on Ti<sub>2</sub>CT<sub>x</sub> (KF-HCl). In addition, CO, trace amounts of CH<sub>4</sub>, and other multi-carbon products are also detected. More importantly, we found that the CO<sub>2</sub>RR activity appears to be correlated with the fraction of -F and -O surface termination groups (T<sub>x</sub>). Ti<sub>2</sub>CT<sub>x</sub> (HF) with large amounts of -F (less -O) shows poorer CO<sub>2</sub>RR activity and selectivity than Ti<sub>2</sub>CT<sub>x</sub> (KF-HCl) with lower -F (more -O). Even higher CO<sub>2</sub>RR activity, up to -2.5 mA cm<sup>-2</sup><sub>geo</sub> is observed on Mo<sub>2</sub>CT<sub>x</sub> catalysts with minimal -F fraction.

DFT simulations indicate that the presence of -F destabilizes \*COOH and \*H, thus causing the limiting potential of both CO<sub>2</sub>RR and HER to become more negative. An exception is found on Mo<sub>2</sub>CT<sub>x</sub> where small amounts of -F substitution is predicted to balance the individual limiting potentials for PCET-1 and PCET-2 steps and yield the smallest overpotential for CO<sub>2</sub>RR to formic acid. The CO<sub>2</sub>RR activity on MXene surfaces could be attributed to unique intermediate-T<sub>x</sub> interaction, which results in stabilization of differently



coordinated \*COOH and \*HCOOH intermediates. The dissimilar binding coordination leads to deviation in linear scaling relations typically observed on late transition metal-based CO<sub>2</sub>RR catalysts like copper.

Although the activity and selectivity toward formic acid can be further improved, this work represents an important step toward experimental demonstration of MXenes for electrocatalytic CO<sub>2</sub>RR. The detection of trace amounts of CH<sub>4</sub> and other hydrocarbon products indicate that CO<sub>2</sub>RR to more complex moieties on MXenes is possible as well. Work is ongoing to further enhance the activity and selectivity of MXene catalysts through material design strategies including surface engineering (Hart et al., 2019), doping (Yu et al., 2019; Li et al., 2018; Gao et al., 2019), and formation of composite/hybrid structures (Handoko et al., 2019; Chi et al., 2018). In addition, we believe that MXenes could be extended to other technologically important electrocatalytic reactions such as nitrogen reduction or methane oxidation, via surface/composition tailoring and catalytic reaction engineering in the future.

### Limitations of the Study

This study investigates Ti- and Mo-based MXenes for CO<sub>2</sub>RR to HCOOH and demonstrates different reaction pathways that can break the scaling relations seen in pure transition metal catalysts. However, the prevalent HER activity on MXenes requires the use of non-aqueous electrolyte, which can be challenging for reaction scale up. Gradual loss of volatile component of the non-aqueous electrolyte also causes fluctuation in the HCOOH selectivity. Further optimization of MXene surface terminations is necessary to enhance the intermediate stability for the production of more reduced moieties like CH<sub>4</sub> and multi-carbon products. The DFT computational methods employed here only lend insight from the thermodynamic point of view. The actual experimental result also depends on reaction kinetics that is challenging to probe in complicated systems with multiple intermediates like CO<sub>2</sub>RR.

### Resource Availability

#### Lead Contact

Further information and requests for resources and reagents should be directed to and will be fulfilled by the Lead Contact, Zhi Wei Seh ([sehzw@imre.a-star.edu.sg](mailto:sehzw@imre.a-star.edu.sg)).

#### Materials Availability

This study did not generate new unique reagents.

#### Data and Code Availability

This study did not generate/analyze datasets/code.

## METHODS

All methods can be found in the accompanying [Transparent Methods supplemental file](#).

## SUPPLEMENTAL INFORMATION

Supplemental Information can be found online at <https://doi.org/10.1016/j.isci.2020.101181>.

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## AUTHOR CONTRIBUTIONS

A.D.H. and Z.W.S. conceived the idea and wrote the manuscript. A.D.H. and B.A. performed materials synthesis. A.D.H. carried out materials characterization and electrochemical testing. H.C. and Q.Z. performed DFT calculations. All the authors discussed the results and commented on the manuscript.

## DECLARATION OF INTERESTS

The authors declare no competing interests.

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## **Supplemental Information**

### **Two-Dimensional Titanium and Molybdenum Carbide**

### **MXenes as Electrocatalysts for CO<sub>2</sub> Reduction**

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## Supplemental figures and data

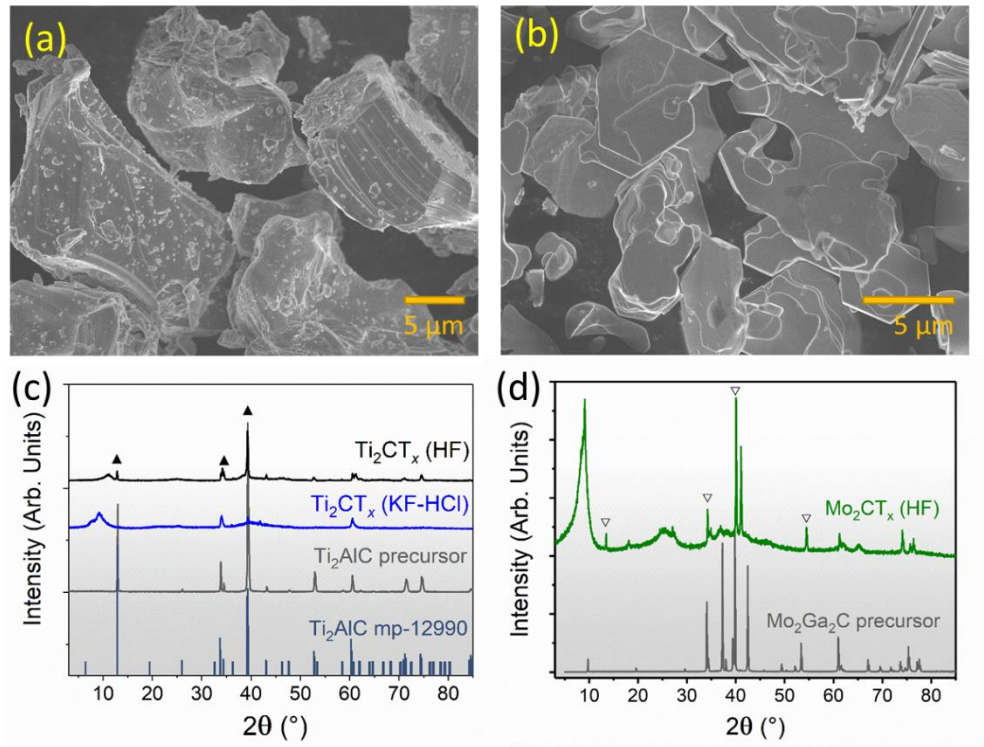


Figure S1: Characterisation of the precursor phases before etching: (a, c) Ti<sub>2</sub>AlC and (b, d) Mo<sub>2</sub>Ga<sub>2</sub>C.

The resulting MXene phase is inserted in (c and d) to check for presence of precursor phase. A standard Ti<sub>2</sub>AlC pattern generated from CIF file from materials project (structure mp-12990) is included in (c). Small amounts of Ti<sub>2</sub>AlC (▲) and Mo<sub>2</sub>Ga<sub>2</sub>C (▽) precursor residues were observed.

Related to Figure 1.

Table S1: XPS analysis to quantify precursor residues. Related to Figure 1.

Element	Ti <sub>2</sub> CT <sub>x</sub> (HF)	Element	Ti <sub>2</sub> CT <sub>x</sub> (KF-HCl)	Element	Mo <sub>2</sub> CT <sub>x</sub> (HF)
Ti	50.24%	Ti	40.91%	Mo	69.53%
C	8.49%	C	24.11%	C	7.61%
O	16.43%	O	18.18%	O	15.69%
F	17.81%	F	16.79%	F	2.90%
Al	7.03%	Al	N. Q.	Ga	4.28%

N.Q.: not quantified due to very low signal to noise ratio.

Table S2: Oxidation state fraction of “M” elements in M<sub>2</sub>CT<sub>x</sub> MXenes. Related to Figure 2.

	Ti <sub>2</sub> CT <sub>x</sub> (HF)		Ti <sub>2</sub> CT <sub>x</sub> (KF-HCl)		Mo <sub>2</sub> CT <sub>x</sub> (HF)	
	pre-CO <sub>2</sub> RR	post-CO <sub>2</sub> RR	pre-CO <sub>2</sub> RR	post-CO <sub>2</sub> RR	pre-CO <sub>2</sub> RR	post-CO <sub>2</sub> RR
M-T <sub>x</sub> /C (MXene)	37.7%	27.3%	26.8%	19.6%	49.4%	21.5%
Ti(II)	55.9%	47.6%	46.6%	28.0%	n.a.	n.a.
Ti(IV)	6.4%	25.1%	26.6%	52.4%	n.a.	n.a.
Mo(V)	n.a.	n.a.	n.a.	n.a.	50.6%	48.6%
Mo(VI)	n.a.	n.a.	n.a.	n.a.	n.a.	29.9%

Table S3: XPS details for Ti<sub>2</sub>CT<sub>x</sub> (HF) before CO<sub>2</sub>RR. Related to Figure 2.

Element	Samples						Average	Stdev
	1	2	3	4	5	6		
Ti	44.77%	37.15%	48.98%	39.04%	39.49%	50.17%	43.27%	5.52%
C	10.98%	3.46%	14.78%	9.96%	10.65%	11.04%	10.15%	3.69%
O	21.24%	39.24%	25.58%	37.15%	35.17%	27.43%	30.97%	7.22%
F	23.01%	20.16%	10.66%	13.85%	14.69%	11.35%	15.62%	4.94%

Average F/Ti = 0.36

Table S4: XPS details for Ti<sub>2</sub>CT<sub>x</sub> (KF-HCl) before CO<sub>2</sub>RR. Related to Figure 2.

Element	Samples					Average	Stdev
	1	2	3	4	5		
Ti	36.00%	35.04%	33.22%	28.70%	31.51%	32.89%	2.91%
C	26.97%	26.66%	26.56%	33.41%	29.39%	28.60%	2.93%
O	30.97%	31.09%	33.87%	30.81%	31.00%	31.55%	1.30%
F	6.07%	7.21%	6.34%	7.09%	8.09%	6.96%	0.80%

Average F/Ti = 0.21

Table S5: XPS details for Mo<sub>2</sub>CT<sub>x</sub> (HF) before CO<sub>2</sub>RR. Related to Figure 2.

Element	Samples					Average	Stdev
	1	2	3	4	5		
Mo	54.82%	72.64%	64.47%	65.76%	66.98%	64.93%	6.45%
C	12.69%	7.95%	9.61%	5.71%	6.11%	8.41%	2.85%
O	29.83%	16.39%	24.11%	27.08%	25.71%	24.63%	5.06%
F	2.65%	3.03%	1.81%	1.44%	1.20%	2.03%	0.79%

Average F/Mo = 0.03

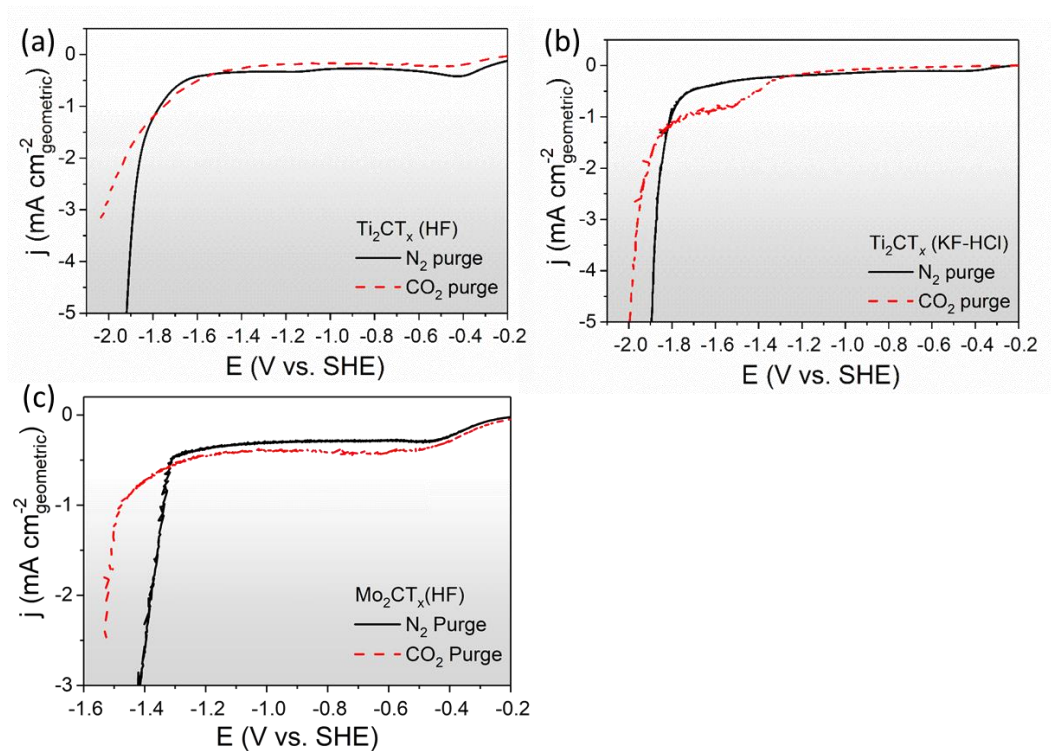


Figure S2: Linear scanning voltammetry (LSV) scans of MXenes in the presence and absence of  $\text{CO}_2$ : (a)  $\text{Ti}_2\text{CT}_x$  (HF), (b)  $\text{Ti}_2\text{CT}_x$  (KF-HCl), and (c)  $\text{Mo}_2\text{CT}_x$  (HF). Electrolyte: acetonitrile- $\text{H}_2\text{O}$ -BMIMBF<sub>4</sub> mixture. Gas purging:  $\text{N}_2$  and  $\text{CO}_2$  purged as marked.  $iR$  drop is compensated via positive feedback correction at 85% of estimated  $R_u$  obtained by electrochemical impedance spectroscopy (EIS) measurement. Related to Figure 3.



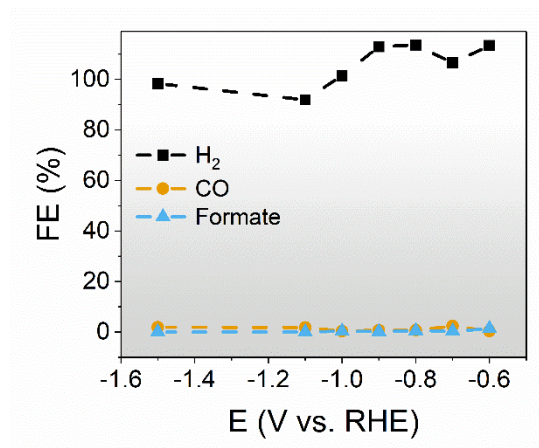


Figure S3: CO<sub>2</sub>RR on Ti<sub>2</sub>CT<sub>x</sub> (KF-HCl) in 0.1 M KHCO<sub>3</sub> aqueous electrolyte. All conditions identical except that the electrolyte in both anodic and cathodic compartments is replaced with CO<sub>2</sub> purged 0.1 M KHCO<sub>3</sub> aqueous solution. Related to Figure 3.

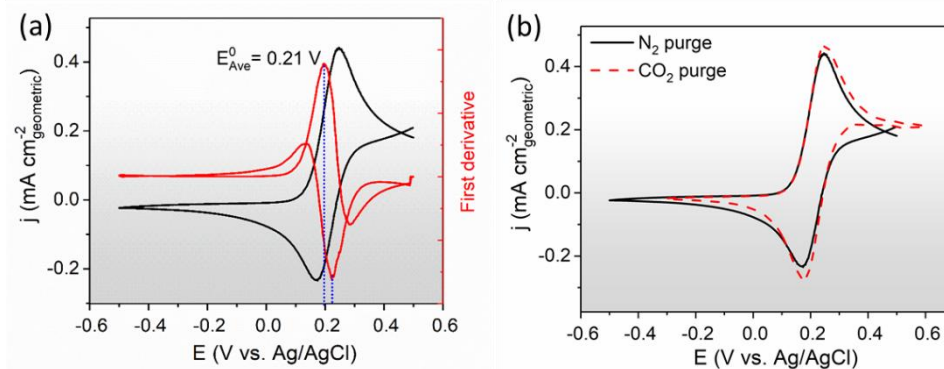


Figure S4: Cyclic voltammetry (CV) of glassy carbon electrode in acetonitrile-H<sub>2</sub>O-BMIMBF<sub>4</sub> electrolyte with 5 mM of ferrocene. (b) Comparison of N<sub>2</sub> and CO<sub>2</sub> purged electrolyte. The reference electrode used in this work is calibrated by conducting CV scans in acetonitrile-H<sub>2</sub>O-BMIMBF<sub>4</sub> electrolyte mixture in the presence of 5 mM ferrocene. Average of anodic going and cathodic going first derivative of the CV cycle is determined to be 0.21 V. Fc/Fc<sup>+</sup> redox potential in acetonitrile solution is taken at 0.624 V vs. SHE, (Pavlishchuk and Addison, 2000) thus the conversion value of Ag/AgCl in acetonitrile-H<sub>2</sub>O-BMIMBF<sub>4</sub> electrolyte mixture is determined to be 0.414 V. We further determine that the Fc/Fc<sup>+</sup> reaction and reference electrode is unchanged in presence of CO<sub>2</sub> purging, indicating that the bicarbonate buffer system is insignificant in our electrolyte system. Related to Figure 3.

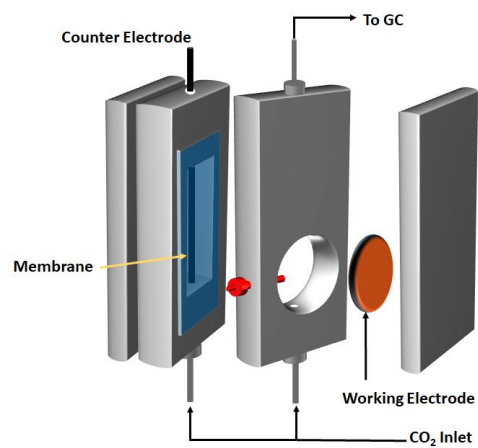


Figure S5: Schematic of two-compartment electrochemical cell used for CO<sub>2</sub>RR in this work. Related to Figure 3.

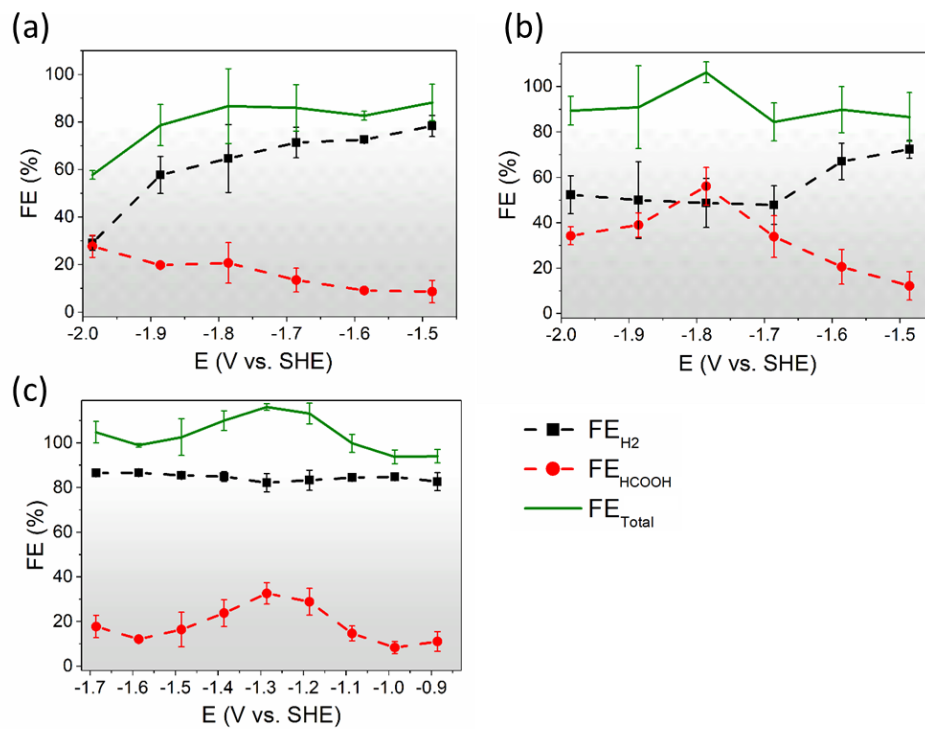


Figure S6: FE of CO<sub>2</sub>RR major products for (a) Ti<sub>2</sub>CT<sub>x</sub> (HF); (b) Ti<sub>2</sub>CT<sub>x</sub> (KF-HCl); and (c) Mo<sub>2</sub>CT<sub>x</sub> (HF). Related to Figure 3.



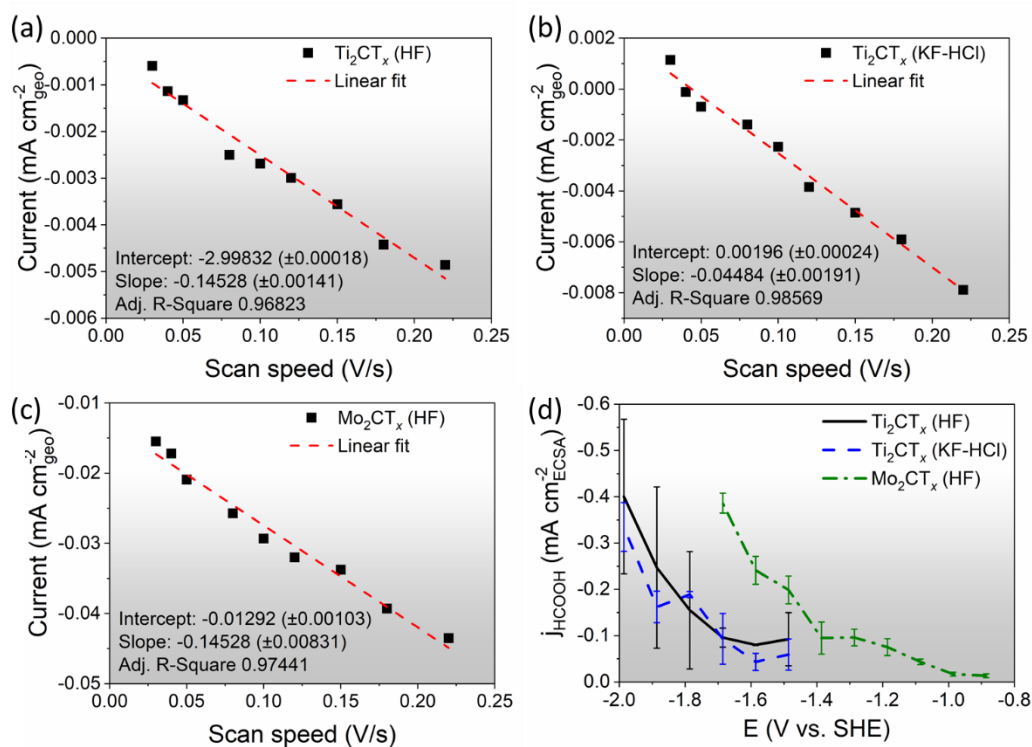


Figure S7: Plot of geometric current density in consecutive CV measurements at varying scan speeds to estimate double layer capacitance in (a) Ti<sub>2</sub>CT<sub>x</sub> (HF), (b) Ti<sub>2</sub>CT<sub>x</sub> (KF-HCl), and (c) Mo<sub>2</sub>CT<sub>x</sub> (HF). (d) Relative electrochemical surface area (ECSA) normalised partial current density of CO<sub>2</sub>RR to formic acid on Ti<sub>2</sub>CT<sub>x</sub> and Mo<sub>2</sub>CT<sub>x</sub> MXenes. Error bars represent one standard deviation of three independent measurements. Related to Figure 3.

Table S6: Tabulation of measured double layer capacitance value and the respective normalised surface area of MXenes. Related to Figure 3.

	Ti <sub>2</sub> CT <sub>x</sub> (HF)	Ti <sub>2</sub> CT <sub>x</sub> (KF-HCl)	Mo <sub>2</sub> CT <sub>x</sub> (HF)
Capacitance value (μF)	29.2	59.5	192.8
Normalised	1	2.03	6.59

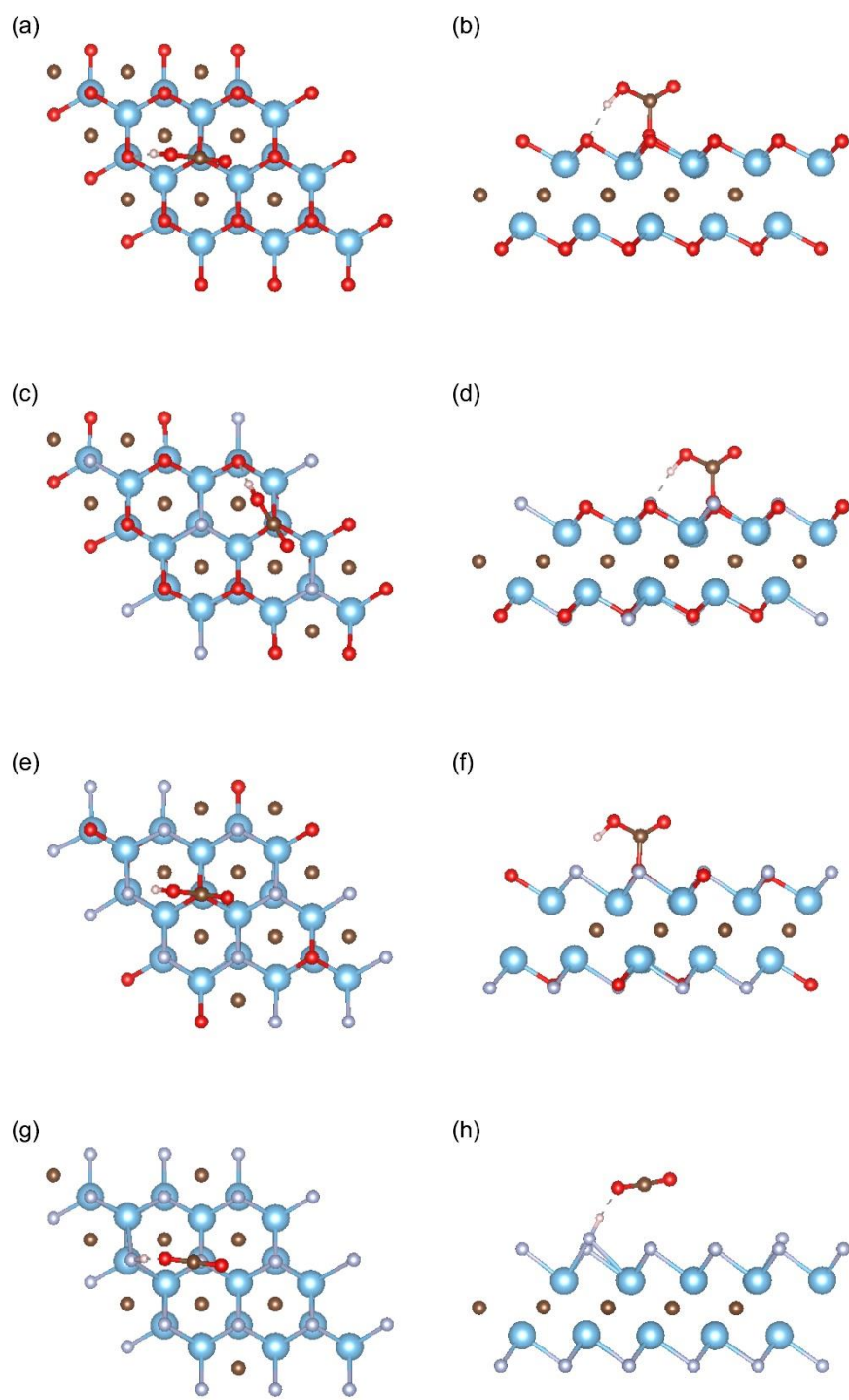


Figure S8: Top and side view of  $^*COOH$  intermediate conformation on  $Ti_2CT_x$  surface with different  $T_x$  groups: (a-b) fully  $-O$  terminated, (c-d) 33.3%  $-F$  66.7%  $-O$  terminated, (e-f) 66.7%  $-F$  33.3%  $-O$  terminated, (g-h) fully  $-F$  terminated. Related to Figure 4.

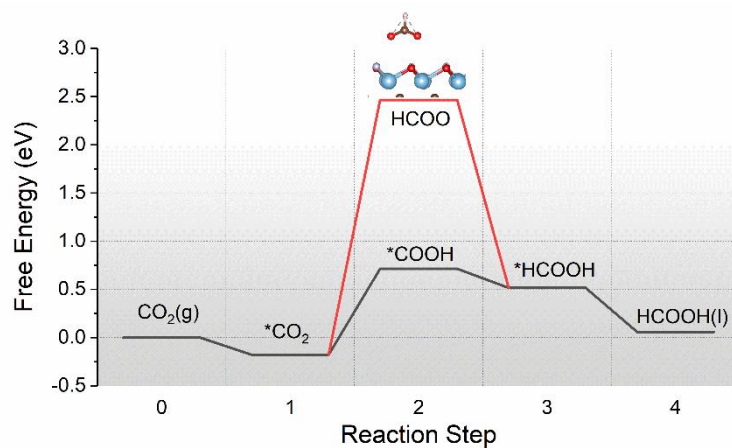


Figure S9: Calculated free energy diagram at 0 V applied potential for CO<sub>2</sub>RR to formic acid through an alternative HCOO pathway compared to the \*COOH pathway on Ti<sub>2</sub>CT<sub>x</sub> (33.3% -F, 66.7% -O). Related to Figure 4.

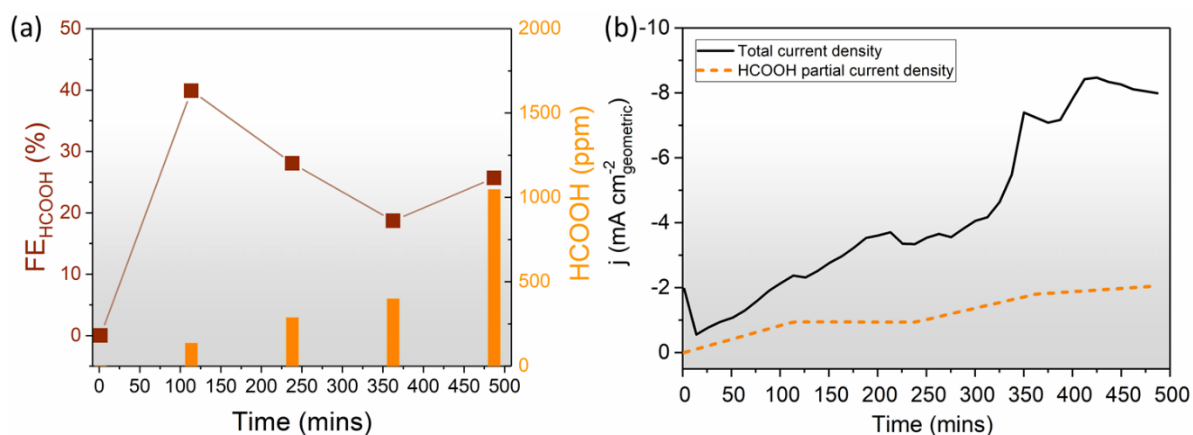


Figure S10: (a) Periodic sampling of HCOOH concentration during 500 mins CO<sub>2</sub>RR on Mo<sub>2</sub>CT<sub>x</sub> showing the Faradaic efficiency (squares, left axis) and the measured HCOOH concentration (orange bars, right axis), as well as (b) total current density and HCOOH partial current density. The apparent Faradaic efficiency instability is attributed to change in electrolyte composition due to loss of acetonitrile, resulting in a significant increase in hydrogen evolution activity while maintaining CO<sub>2</sub>RR to HCOOH. This is reflected in the increased total current density and relatively stable HCOOH partial current density. Related to Figure 3.

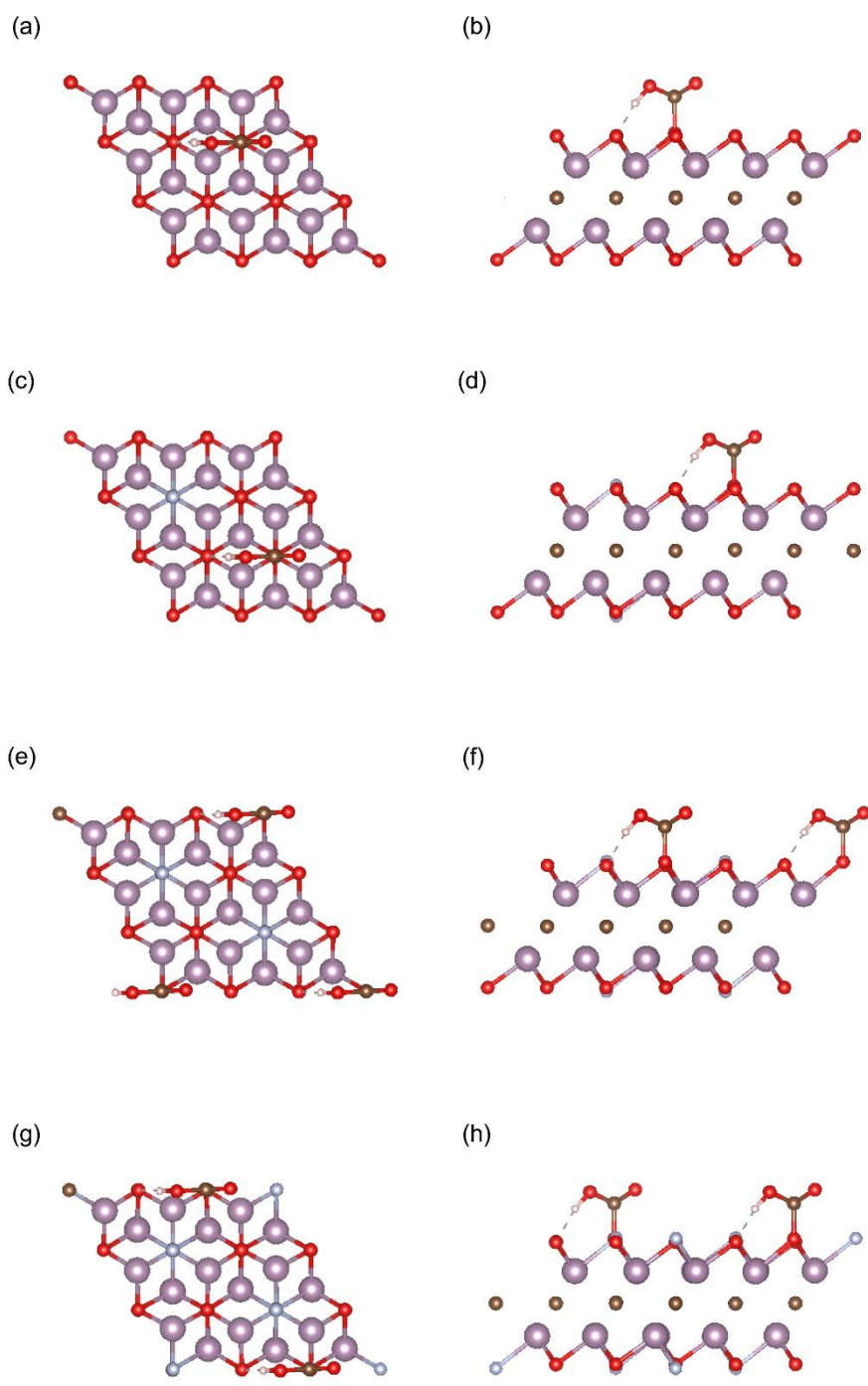


Figure S11: Top and side view of \*COOH intermediate conformation on Mo<sub>2</sub>CT<sub>x</sub> surface with different T<sub>x</sub> groups: (a-b) fully -O terminated, (c-d) 11.1% -F 88.9% -O terminated, (e-f) 22.2% -F 77.8% -O terminated, and (g-h) 33.3% -F 66.7% -O terminated. Related to Figure 4.

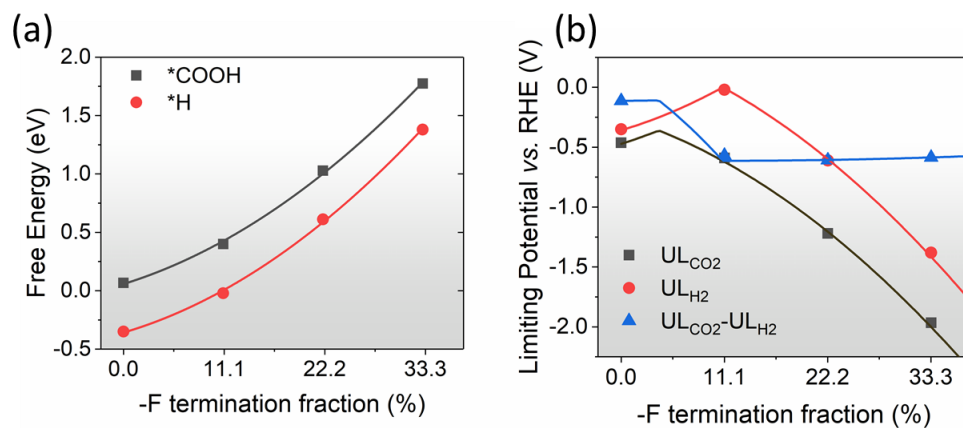


Figure S12: Fitting function diagram of the (a) \*COOH and \*H free energy and (b) the corresponding limiting potentials for CO<sub>2</sub>RR, HER and the difference between the two ( $UL_{CO_2}-UL_{H_2}$ ) on Mo<sub>2</sub>CT<sub>x</sub> MXene at varying -F T<sub>x</sub> fraction. Related to Figure 5.

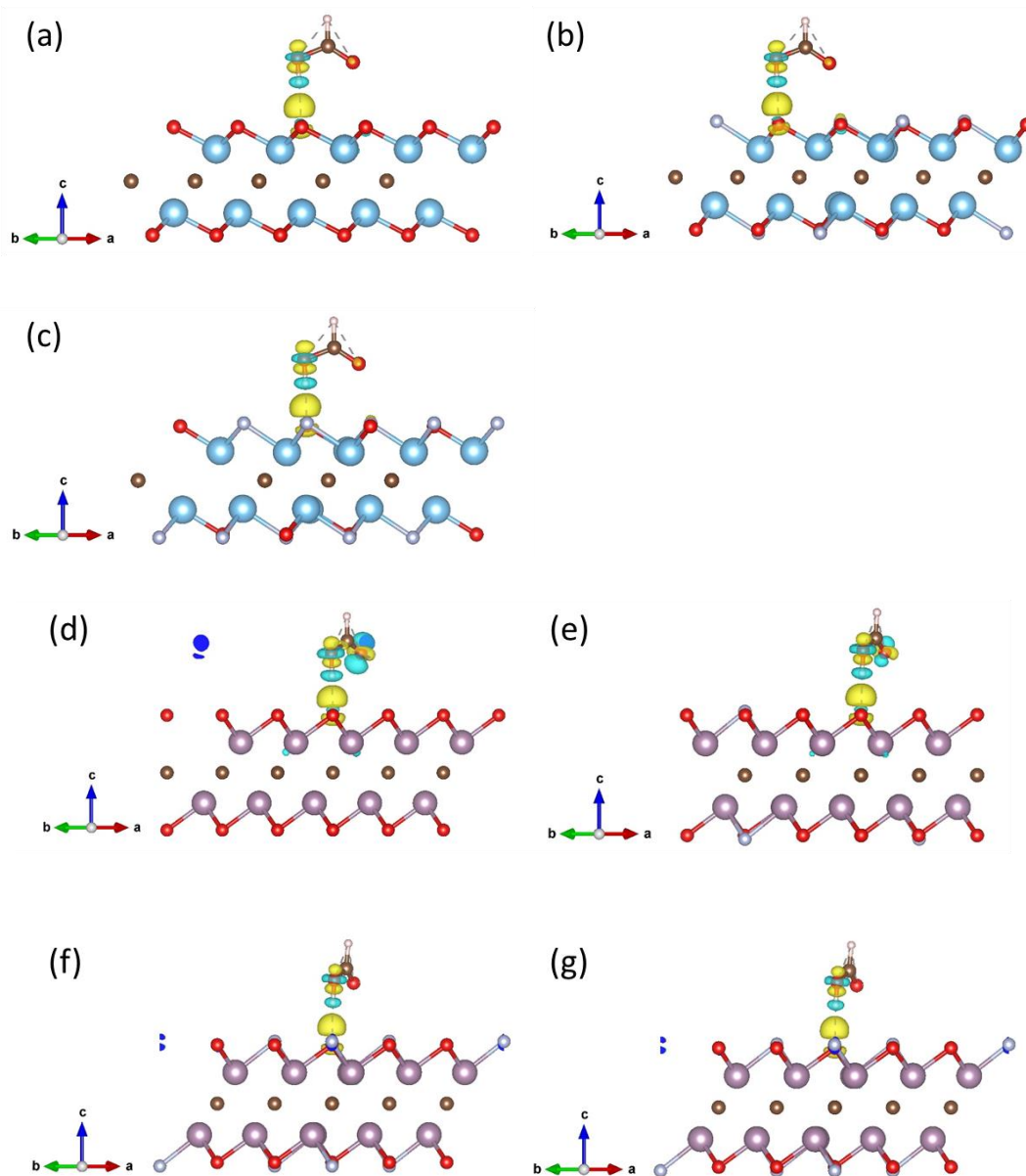


Figure S13: Charge deformation density of adsorbed  $^*\text{HCOOH}$  intermediates on  $\text{Ti}_2\text{CT}_x$  (a) fully  $-\text{O}$  terminated, (b) 33.3%  $-\text{F}$  66.7%  $-\text{O}$  terminated, (c) 66.7%  $-\text{F}$  33.3%  $-\text{O}$  terminated, and  $\text{Mo}_2\text{CT}_x$  (d) fully  $-\text{O}$  terminated, (e) 11.1%  $-\text{F}$  88.9%  $-\text{O}$  terminated, (f) 22.2%  $-\text{F}$  77.8%  $-\text{O}$  terminated, and (g) 33.3%  $-\text{F}$  66.7%  $-\text{O}$  terminated. Iso-surfaces drawn represent  $0.002 \text{ e bohr}^{-3}$ . Charges flow out from blue areas to yellow areas. Related to Figure 5.



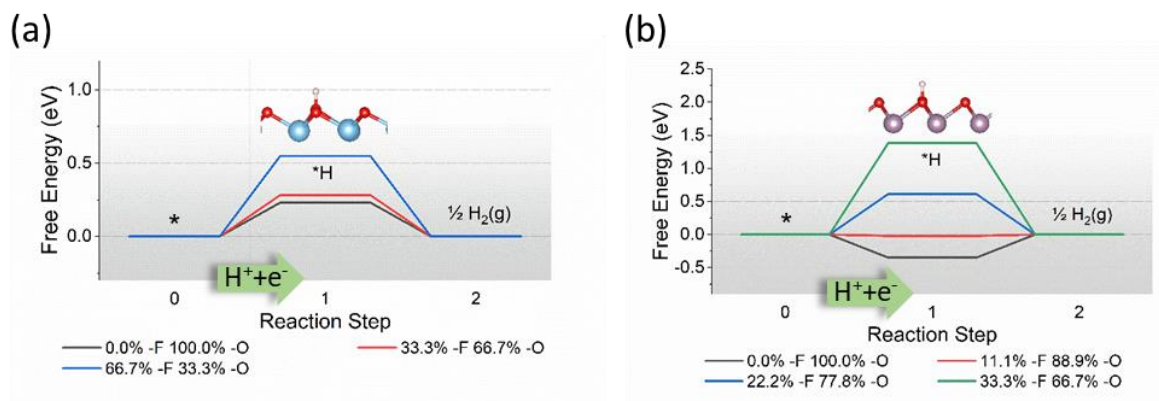


Figure S14: Calculated free energy diagram of HER at 0 V applied potential on (a) Ti<sub>2</sub>CT<sub>x</sub> and (b) Mo<sub>2</sub>CT<sub>x</sub> at varying -F T<sub>x</sub> fraction. Related to Figure 5.

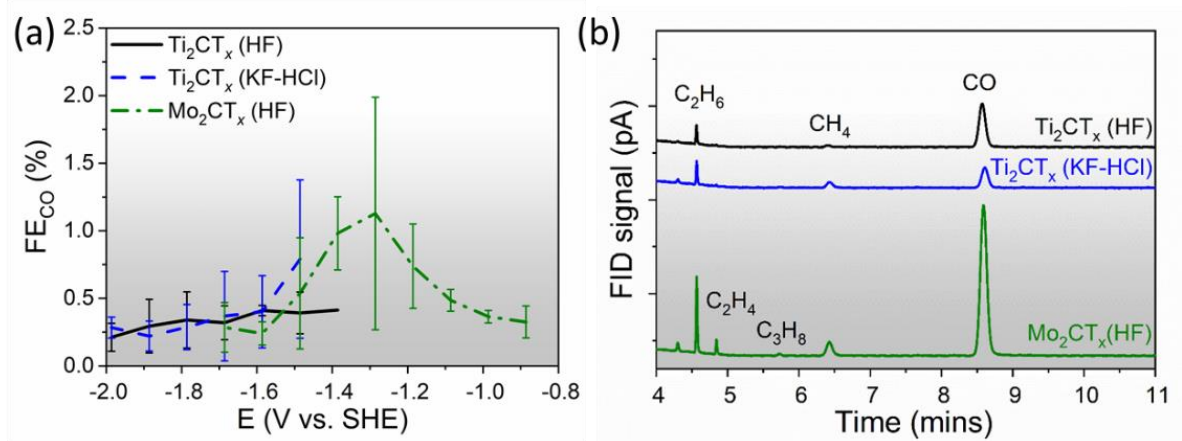


Figure S15: (a) FE data for minor product (CO) and (b) representative gas chromatogram FID of  $Ti_2CT_x$  and  $Mo_2CT_x$  at -1.5 V showing trace levels of CO and  $CH_4$ . Other products  $C_2H_4$ ,  $C_2H_6$  and  $C_3H_8$  are not quantified due to low amounts. Related to Figure 3.

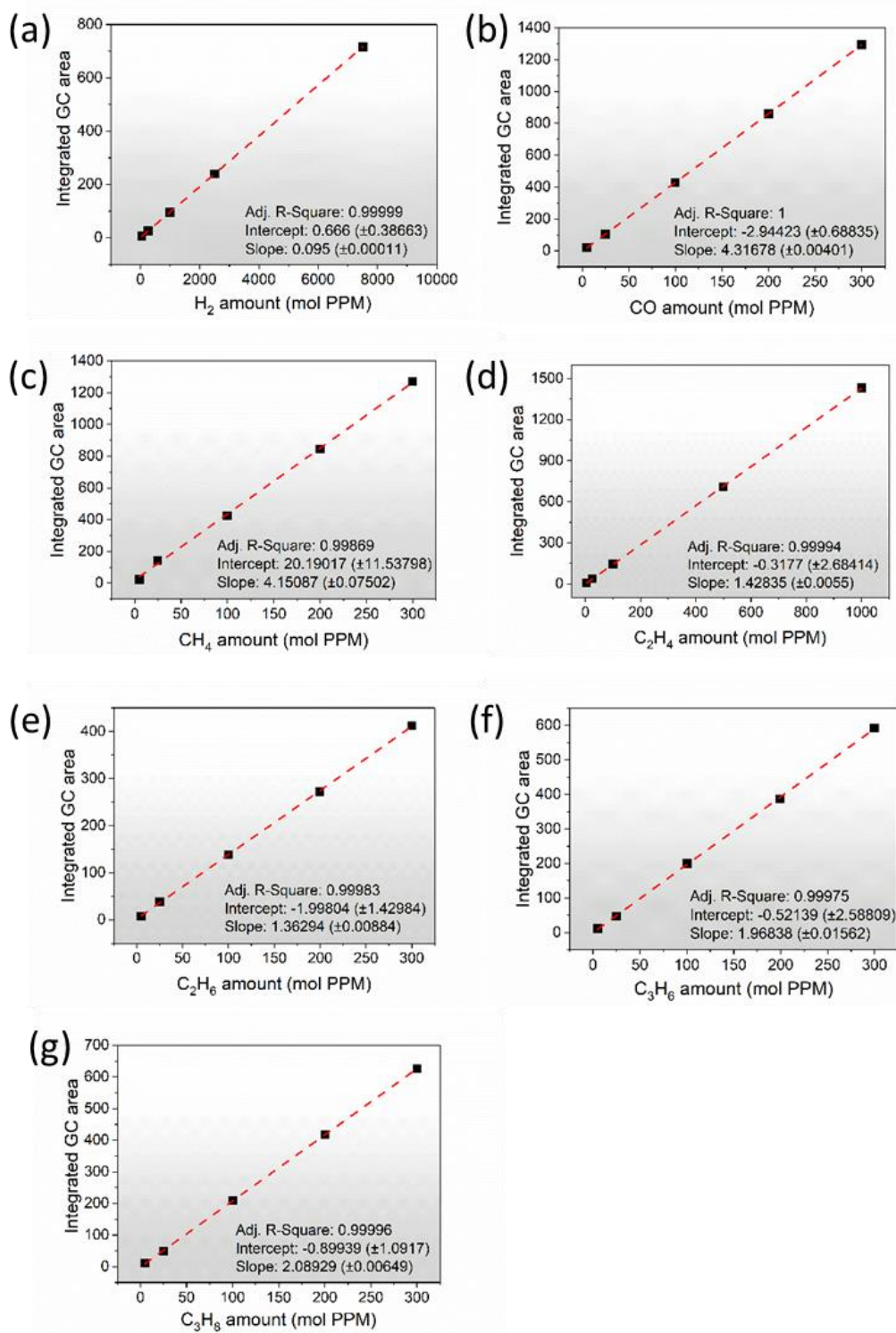


Figure S16: GC calibration plot for (a)  $H_2$  (b) CO (c)  $CH_4$  (d)  $C_2H_4$  (e)  $C_2H_6$  (f)  $C_3H_6$  and (g)  $C_3H_8$ . Calibrations were performed at 20 sccm flowrate. The balance gas for all calibration gases is  $CO_2$ .

Related to Figure 3.

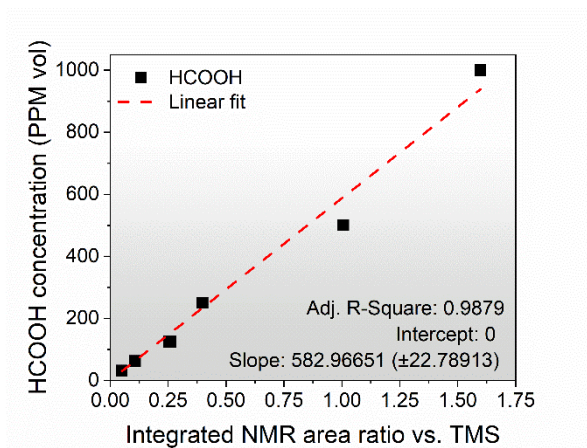


Figure S17: NMR calibration plot for formic acid. Mixtures of different concentrations of formic acid are prepared in the same composition of acetonitrile-H<sub>2</sub>O-BMIMBF<sub>4</sub> mixture as the electrolyte used in this study. Integrated NMR area ratio is calculated with respect to the internal standard (50 mM tetramethyl silane in acetonitrile) area. Related to Figure 3.

Table S7: Surface energy of different types of  $Ti_2CT_x$ . The most favourable  $T_x$  surface termination sites (*fcc* or *hcp*) with lowest surface energy are marked in red. Related to Figure 4.

	Surface energy (eV)			
-F Substitution	0.0%	33.3%	66.7%	100.0%
<i>fcc</i>	-405.35	-390.44	-374.67	-357.66
<i>hcp</i>	-388.96	-377.74	-366.44	-352.73

Table S8: Surface energy of different types of  $Mo_2CT_x$ . The most favourable  $T_x$  surface termination sites (*fcc* or *hcp*) with lowest surface energy are marked in red. Related to Figure 4.

	Surface energy (eV)					
-F Substitution	0.0%	11.1%	22.2%	33.3%	66.7%	100.0%
<i>fcc</i>	-405.21	-402.96	-398.20	-394.17	-377.34	-358.09
<i>hcp</i>	-414.71	-409.59	-403.96	-397.10	-375.26	-355.50

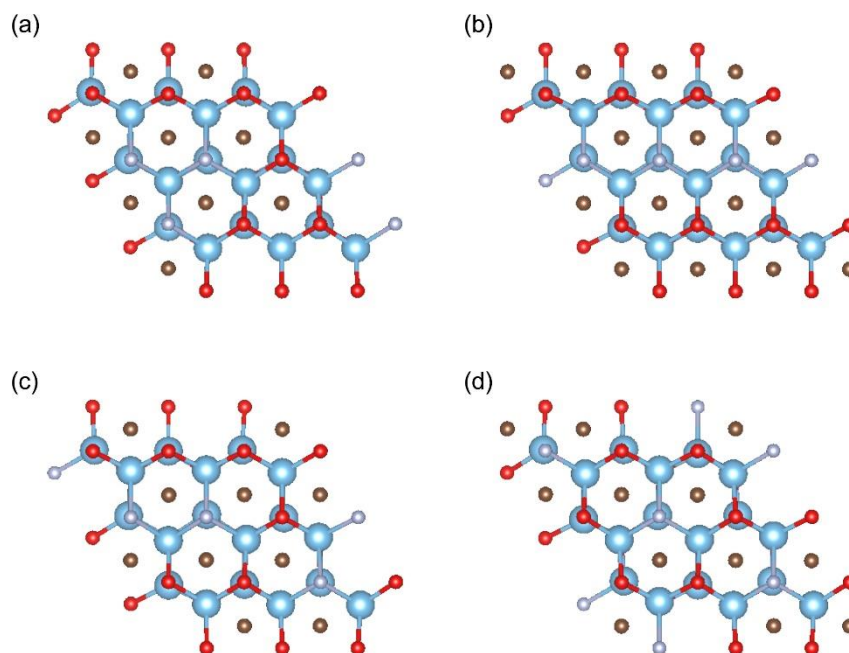


Figure S18: -F termination distribution pattern for 33.3% -F substituted  $\text{Ti}_2\text{CT}_x$ . The calculated energies are (a) -389.88 eV, (b) -389.95 eV, (c) -390.03 eV, and (d) -390.44 eV. Related to Figure 4.

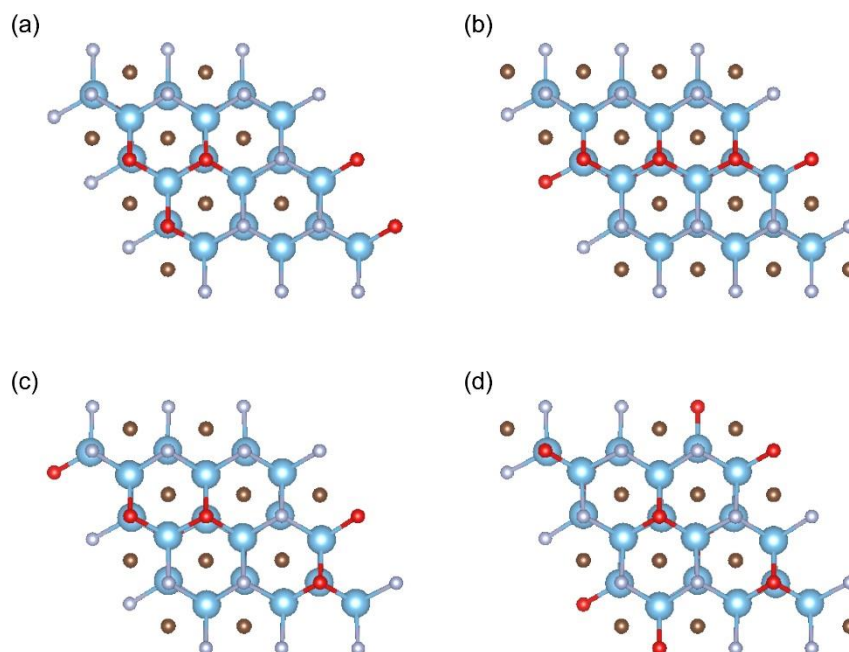


Figure S19: -F termination distribution pattern for 66.7% -F  $\text{Ti}_2\text{CT}_x$ . The calculated energies are (a) -374.11 eV, (b) -374.21 eV, (c) -374.31 eV, (d) -374.67 eV. Related to Figure 4.

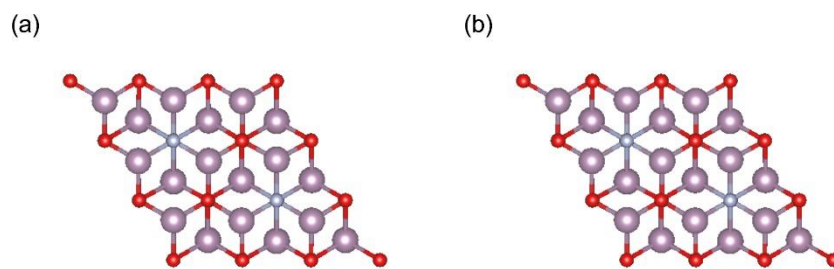


Figure S20: -F termination distribution pattern for 22.2% -F Mo<sub>2</sub>CT<sub>x</sub>. The calculated energies are (a) -403.66 eV, (b) -403.96 eV. Related to Figure 4.

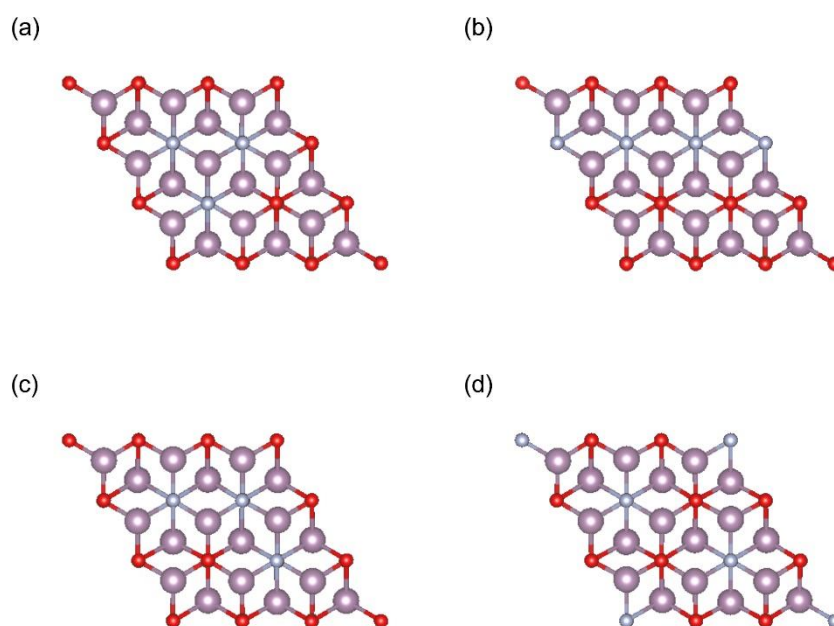


Figure S21: -F termination distribution pattern for 33.3% -F Mo<sub>2</sub>CT<sub>x</sub>. The calculated energies are (a) -396.26 eV (b) -396.32 eV (c) -396.46 eV (d) -397.10 eV. Related to Figure 4.



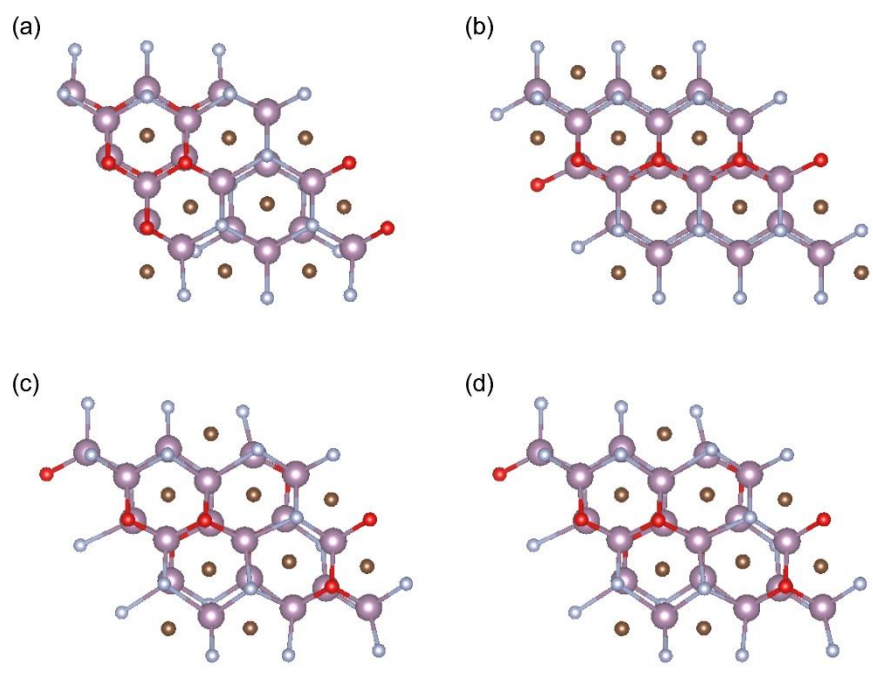


Figure S22:  $-F$  termination distribution pattern for  $66.7\%$   $-F$   $Mo_2CT_x$ . The calculated energies are (a)  $-377.15$  eV, (b)  $-376.65$  eV, (c)  $-376.26$  eV, (d)  $-377.34$  eV. Related to Figure 4.

## Transparent Methods

### Synthesis

Ti<sub>2</sub>AlC was synthesised following previously reported procedure (Handoko et al., 2018). Typically, TiC, Ti, and Al powders (Alfa Aesar) with average particle sizes of 2 μm, <44 μm and <44 μm, respectively, were ball milled for 24 h using zirconia balls in a plastic jar. The TiC : Ti : Al molar ratio was 0.85 : 1.15 : 1.05. The powder mixture was heated in an alumina crucible at 5 °C min<sup>-1</sup> to 1400 °C and held for 4 h under flowing Ar. After furnace cooling, the porous compact was milled using a TiN-coated milling bit and sieved through a 400 mesh sieve to make Ti<sub>2</sub>AlC powder with particle size <37 μm.

Mo<sub>2</sub>Ga<sub>2</sub>C synthesis methods were described previously (Hu et al., 2015). In brief, 2:1 molar ratio of Mo and C powders (Alfa Aesar) were first heated at 1000 °C for 12 h in Ar environment. The resulting Mo<sub>2</sub>C solid was crushed into a powder and homogeneously mixed with melted Ga (at 45 °C) in mortar and pestle with 1:8 molar ratio. The solidified mixture was then vacuum sealed inside quartz tube. The quartz tube then heated at a rate of 10 °C min<sup>-1</sup> to 850 °C, and held at that temperature for 48 h. The resulting powder was immersed in a 37 wt% HCl after cooling for 3 days to dissolve possible residual Ga or Ga<sub>2</sub>O<sub>3</sub>. The final Mo<sub>2</sub>Ga<sub>2</sub>C powders were sieved to achieve particle size of <37 μm and kept under argon filled glovebox until further use.

HF etched Ti<sub>2</sub>CT<sub>x</sub> and Mo<sub>2</sub>CT<sub>x</sub> MXenes were prepared as reported previously (Anasori et al., 2017). Typically, 2 g of Ti<sub>2</sub>AlC or Mo<sub>2</sub>Ga<sub>2</sub>C powders were added slowly (over ≈2 min) onto 20 mL of 10 wt% (or 48 wt% for Mo<sub>2</sub>Ga<sub>2</sub>C) HF solution (Merck) and held for 18 h (or 7 days for Mo<sub>2</sub>Ga<sub>2</sub>C) at ambient temperature (or 55 °C for Mo<sub>2</sub>Ga<sub>2</sub>C) inside a Teflon container while stirring at 200 rpm. After that the mixtures were washed at least 5 times by adding deionized (DI) water (18.2 MΩ•cm, Purelab Option Q), shaken for 1 min using a vortex shaker and centrifuging for 5 min at 5000 rpm until a pH of >6. The powders were then dried under vacuum at 50 °C and kept under argon filled glovebox until further use.

To make fluoride salt etched Ti<sub>2</sub>CT<sub>x</sub> (Liu et al., 2017), solution containing 4.70 g of KF (99%, Merck) is slowly mixed into 20 mL HCl (36-38%, electronic grade, Duksan Reagents) under magnetic stirring (200 rpm) for 10 minutes inside a Teflon container. Afterwards, 2 g of Ti<sub>2</sub>AlC is poured slowly over 2 mins to the solution, and kept under stirring (200 rpm) for 48 h at 40 °C. The samples were then washed with DI water 5 times and ethanol 2 times until pH of supernatant is around 7. The powders were then dried under vacuum at 50 °C and kept under argon filled glovebox until further use.

### Characterisation

Morphology of the materials are characterised using JEOL JSM-7600F Schottky Field Emission Scanning Electron Microscope (SEM) operating at 5 kV and 116 μA emission power. Gentle beam

mode is applied at a reduced 1 kV emission voltage to minimise surface charging on non-conductive precursor phases.

Phase composition of the materials was characterised using X-ray diffraction (XRD) using Bruker Advance D8 diffractometer (Cu K $\alpha$ ,  $\lambda = 1.541058 \text{ \AA}$ ) fitted with Ni filter and LynxEye XE energy dispersive 1-D detector at 40 kV 40 mA operating power. Coupled  $\theta$ - $2\theta$  scans were performed from 3 to 85°  $2\theta$  range with 0.02° step size and 0.3 s time per step. A motorised variable aperture was programmed to provide a fixed 10 mm sample irradiation length to enhance signals at higher  $2\theta$  angles. A beam knife is fitted about 1 mm above the sample to minimise air scattering signal at low  $2\theta$  angles. Powders were packed into a zero background diffraction plate with  $\varnothing 10 \text{ mm} \times 0.2 \text{ mm}$  cavity depth (off-cut Si, MTI Corporation) to reduce background contribution.

Elemental analyses is done using X-ray photoelectron spectroscopy (XPS) using a Thermo ThetaProbe or Kratos Axis Supra with a monochromatic Al K $\alpha$  X-ray source (1486.7 eV). Two consecutive measurements were conducted. The first is to obtain energy calibration signal from adventitious C  $1s$  peak at 284.8 eV. The second measurement was performed after sputtering the sample with Ar<sup>+</sup> ion gun for ~600 s to remove surface contamination and better identify C  $1s$ , Ti  $2p$  or Mo  $3d$  components belonging to MXene. XPS fitting was done using Avantage software (V6.01, Thermo Scientific), with fitting assignment following the literature (Mashtalir et al., 2013, Halim et al., 2016).

### Electrochemical CO<sub>2</sub> reduction

All CO<sub>2</sub>RR were performed inside a custom made, two-compartment PTFE electrochemical cell at room temperature (23-25 °C). Each compartment is of 11 mL volume, and separated by 7×2 cm<sup>2</sup> Nafion 117 membrane (Chemours). The cathodic compartment is filled with 8 mL mixture of acetonitrile (80 mol%, HPLC grade, VWR Chemicals) and DI water (15 mol%, 18.2 M $\Omega$ •cm, Purelab Option-Q) as solvent, with 3-butyl-1-methyl-1H-imidazol-3-ium tetra-fluoroborate ionic liquid (5 mol%, BMIMBF<sub>4</sub>, 98%, Combi Blocks) added in as supporting electrolyte. The pH of the electrolyte is 1.24. The addition of water is essential as a proton source and to manage the solution viscosity. (Rosen et al., 2013, Yang et al., 2019) The anodic compartment is filled with 8 mL of 0.5 M H<sub>2</sub>SO<sub>4</sub> (Merck Ultrapur) as proton reservoir (Lu et al., 2018).

A leakless Ag/AgCl (eDAQ) was used as reference electrode, placed 2 mm above the working electrode. The reference was calibrated with ferrocene and the potential in this work is reported against SHE, by taking the average redox potential of Fc/Fc<sup>+</sup> to be 0.624 V vs. SHE in acetonitrile solution at 25 °C (Pavlishchuk and Addison, 2000). Electrochemical measurements were done using a calibrated potentiostat (Gamry 600+ or Gamry 3000). Electrolyte resistance was measured each time using high frequency electrochemical impedance spectroscopy and compensated using positive feedback correction at 85% level. The typical R<sub>u</sub> compensation applied is around 8.5-9.5  $\Omega$ .

The working electrode substrate is  $\varnothing$ 15 mm x 1 mm vitreous carbon discs (Goodfellow), polished to mirror finish with 1  $\mu$ m alumina slurry followed by 0.3  $\mu$ m alumina slurry (Buehler). After each polishing steps, the substrate is ultrasonicated in DI water twice for 5 minutes each. To prepare the catalyst ink, 5 mg of MXene is added into 0.6 mL DI water and 0.4 mL ethanol (absolute grade, VWR Chemicals) and 40  $\mu$ L of Nafion solution (5% mixture in lower aliphatic alcohol and water, Sigma Aldrich). The ink is then homogenised in an ice bath (*approx.* 0-4 °C) inside an ultrasonicator for 15 minutes, vortex shaken (2400 rpm) for 1 minute and deposited volumetrically onto the polished glassy carbon to achieve 0.5 mg cm<sup>-2</sup> loading per vitreous carbon substrate. The catalyst ink is then dried under table lamp (100 W lightbulb). The exposed geometric surface area is 1.327 cm<sup>2</sup>. Spectroscopically pure graphite rod (Ted Pella) was used as the counter electrode.

CO<sub>2</sub> gas (99.999%, Linde Gas) was delivered to both compartments of the electrochemical cell using calibrated mass flow controller (MC 100SCCM-D, Alicat Scientific) at 20 sccm flowrate. The samples were subjected to chronoamperometric (constant voltage) measurement for 100 mins under continuous CO<sub>2</sub> gas purging. Periodic sampling every 12.45 minutes was done by an online custom valve gas chromatograph (GC; Wasson-ECE) for gas products quantification. The GC is equipped with a thermal conductivity detector (N<sub>2</sub> carrier gas, 99.9995%, Leeden National Oxygen) for detecting H<sub>2</sub> and flame ionization detectors (He carrier gas, 99.9995%, Leeden National Oxygen) with a methaniser for detecting C<sub>1</sub> to C<sub>3</sub> hydrocarbons and CO. Chromatograms were processed using Openlab CDS (Chemstation edition, rev. C.01.08, Agilent Technologies). Gaseous products were calibrated with 6 standard gas mixtures in CO<sub>2</sub> balance gas. (AG Gases Ltd., mixtures traceable to standards at the National Physical Laboratory, UK).

Liquid products were analysed using 500 MHz nuclear magnetic resonance (NMR; JEOL JNM-ECA500II), operated with DANTE selective excitation sequence (Morris and Freeman, 1978) (2  $\mu$ s pulse, 0.1 ms interval, 40 dB RF output) to suppress high concentration solvent signals. Each spectra is an average of 64-128 consecutive scans. Data was processed using JEOL Delta V5.2. To prepare sample for NMR analysis, 1 mL of sample is mixed with 50  $\mu$ L of internal standard (50 mM tetramethyl silane in acetonitrile, Cambridge Isotope Lab, 99.9%). 0.5 mL of this mixture is then mixed with 0.1 mL of acetonitrile-D<sub>3</sub> (Cambridge Isotope Lab, 99% D). NMR calibration is performed using variable concentrations of formic acid in acetonitrile-H<sub>2</sub>O-BMIMBF<sub>4</sub> electrolyte in the presence of internal standard and acetonitrile-D<sub>3</sub>. The Faradaic efficiency was calculated by comparing the number of electrons required for the amounts of detected products and the recorded number of electrons measured by the potentiostat (Ren et al., 2015).

#### DFT calculation details

First-principle calculation in the framework of density functional theory (DFT) was applied for all the simulations by using the Vienna ab-initio Simulation Package (VASP) (Kresse and Furthmüller, 1996).

The projector-augmented-wave (PAW) pseudopotential was adopted to treat the core electrons (Blöchl, 1994). Perdew-Burker-Ernzerhof (PBE) formulation based on the generalized gradient approximation (GGA) exchange-correlation was utilized to simulate the electron interactions (Perdew et al., 1996). To take Van der Waals force into consideration, correction using DFT-D3 formalism is adopted (Grimme et al., 2010, Grimme et al., 2011). A cut-off energy 450 eV was applied for all computations. Geometry optimization process were fully carried out, and the energy convergence criteria on each atom was 0.03 eV Å<sup>-1</sup>. The thickness of vacuum is at least 20 Å to avoid artificial interactions amongst the periodic slabs. The 3×3×1 Monkhorst-Pack *k*-point mesh sampled Brillouin zone was used for 3×3 supercells.

The computational hydrogen electrode (CHE) was employed, avoiding the explicit treatment of solvated protons (Nørskov et al., 2005). The change of free energy at 0 V (*vs.* RHE) can be calculated by the following equation:

$$\Delta G = \Delta E_{elec} + \Delta E_{ZPE} - T \times \Delta S$$

Where  $\Delta E_{elec}$  is the electronic energy difference between two contiguous reaction steps,  $\Delta E_{ZPE}$  is the difference of the zero-point energy,  $T$  is the temperature and assumed as 298.15 K, while  $\Delta S$  is the difference of the entropy. *ZPE* and vibrational entropy of adsorbates are calculated from vibrations by standard methods, which is treated in the harmonic oscillator approximation (Cramer and Bickelhaupt, 2003). As for the gas-phase molecule, the thermal corrections of translations and rotations is also included.

Prior to calculating CO<sub>2</sub>RR intermediates, the most preferred T<sub>x</sub> sites with lowest energy for four Ti<sub>2</sub>CT<sub>x</sub> and five Mo<sub>2</sub>CT<sub>x</sub> models with varying –F substitution levels are first determined. The different distributions of –F atoms at various substitution levels to –O T<sub>x</sub> groups are also taken into consideration. Mo<sub>2</sub>CT<sub>x</sub> models with 66.7% and 100% –F substitution are excluded from further calculations due to significant structure distortion. Ti<sub>2</sub>CT<sub>x</sub> with 100% –F substitution is also excluded due to unstable intermediate adsorption.

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