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Silica-supported isolated gallium sites as highly active, selective and stable propane dehydrogenation catalysts†

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Single-site gallium centers on the surface of silica are prepared via grafting of $[Ga/OSi(OtBu)_{3}]_{3}$ (THF)] on SiO_{2-700} followed by a thermolysis step. The resulting surface species corresponds to well-defined tetracoordinate gallium single-sites, $[(\equiv \text{SiO})_3Ga(XOS\equiv)]$ $(X = -H$ or \equiv Si) according to IR, X-ray absorption near-edge structure and extended X-ray absorption fine structure analysis. These gallium sites show high activity, selectivity and stability for propane dehydrogenation with an initial turnover frequency of 20 per h per gallium center, propylene selectivity of ≥93% and remarkable stability over 20 h. The stability of the catalyst probably results from site-isolation of the active site on a non-reducible support such as silica, diminishing facile reduction typical of Ga_2O_3 -based catalysts. EDGE ARTICLE

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Introduction

The increasing propylene demand combined with the use of alternative feedstocks such as shale gas has amplified the pressure towards propene production and the development of light alkane dehydrogenation processes.¹ In particular, the recent conversion of cracking plants from naphtha to ethane, the second largest component of shale gas, has resulted in a decline in annual propylene production while demand continues to increase. As a result, on-site propane dehydrogenation (PDH) is of particular interest for current and future propylene production. $1a, c, 2$ While the two principal industrial processes for PDH utilize Cr–Al₂O₃ (CATOFIN) and PtSn–Al₂O₃ (Oleflex) supported catalysts,^{1c,2} other materials such as galliumbased catalysts are receiving considerable attention as alternative catalysts.

Gallium-based zeolites have already been implemented for the conversion of lightweight alkanes to aromatics and H_2 , a process proposed to involve a tandem dehydrogenation–aromatization process.³ Ga₂O₃ and related materials have also been investigated as catalysts for alkane conversion, specifically PDH due to the high selectivity for propylene.⁴ In this regard it is proposed that tetra-coordinate surface sites of $Ga₂O₃$ are the active sites for propane dehydrogenation. However, due to the reducibility of $Ga₂O₃$, these active sites typically suffer from facile reduction,

ultimately resulting in catalyst deactivation.^{1c,5} This is supported by advantageous effects of co-feeding $CO₂$ or $H₂O$ during PDH, which have been attributed to the re-oxidation of inactive $Ga(i)$ sites and removal of coke from the surface.^{5a,6} Several computational and experimental studies have aimed at identifying these active sites, $4f, h, i, 7$ which so far remains a topic of debate. Silicasupported gallium species have been recently prepared by electrostatic adsorption methods.⁷^a While showing promising results, the structure of the active sites is unknown.

Surface organometallic chemistry (SOMC) allows for the generation of well-defined surface species on a variety of supports via grafting of tailored molecular precursors on supports with isolated -OH sites.⁸ Thus, we reasoned that the development of an appropriate molecular precursor would allow for generating well-defined isolated active sites of gallium outside of bulk $Ga₂O₃$. This would result in a material with high catalytic activity with respect to total metal loading, as inactive bulk $Ga₂O₃$ would not be present. Additionally, generating isolated gallium sites on a non-reducible support such as silica could diminish reduction processes and allow for the development of a catalyst with enhanced stability under PDH conditions. A two-step approach, involving both SOMC and the thermolytic molecular precursor approach has previously been implemented to generate isolated surface sites with controlled oxidation state and nuclearity.⁹ Herein we describe the synthesis, structural characterization of the molecular complex $\left[{\rm Ga(OSi(OtBu)_{3}})_{3}({\rm THF})\right](1)^{\rm 10}$ and its utilization as a precursor for generating gallium single-sites on silica. These isolated gallium sites were achieved through grafting of 1 on silica followed by a thermolysis step at 500 $^{\circ}\textrm{C}$ under high vacuum. The presented gallium species display unprecedented catalytic performances, combining high activity, selectivity and stability in the dehydrogenation of propane.

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Results and discussion

First, we developed the synthesis of $[Ga(OSi(OtBu)_{3})_{3}(THF)]$ (1) by reacting GaCl₃ with Na $\left($ OSi $\left($ OtBu $\right)$ ₃ $\right)$ in THF.¹⁰ A high-quality X-ray diffraction experiment provides reliable bond distances and angles for this precursor (Fig. 1). Opaque single crystals were grown from a saturated pentane solution cooled to $-40\,^{\circ}$ C. This analysis reveals a distorted trigonal pyramidal geometry around the Ga(III) center ($\tau_4 = 0.86$).¹¹ The THF ligand occupies the axial position (Ga1–O1_{THF}, 1.963(2) \AA) rendering the three siloxide ligands in the equatorial plane (Ga1–O2 $_{siloxide}$, 1.780(2) Å). This unusual geometry about the gallium metal center is attributed to the steric repulsion of the bulky siloxide ligands.

The next step was the reaction of a benzene solution of 1 with SiO₂₋₇₀₀ (0.31 mmol -OH per g)¹² (Fig. 1). After 12 hours and subsequent washings of the material with benzene, ${}^{1}H$ NMR spectroscopy revealed complete consumption of 1 and formation of isobutene, tert-butanol and THF in ratios of 4.3, 1.9, and 1.0 equivalents per consumed gallium complex. No detectable amount of $HOSi(OtBu)$ ₃ was released after the grafting process, which is in sharp contrast to what was observed for similar $Cr(m)$ or $Fe(m)$ analogues.^{9b,h} The aforementioned ratios indicate release of THF and thermal transformation of two $-OSi(OtBu)$ ₃ ligands of 1 when contacted with the silica surface over the duration of 12 hours. The material was dried under high vacuum $(10^{-5}$ mbar) for 12 hours and subsequent analysis by IR spectroscopy revealed Openical Seince
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Fig. 1 (a) Molecular structure of 1 obtained from X-ray diffraction studies. Ellipsoids are at the 50% probability and all H atoms and all $-CH₃$ groups of the $-OSi(OtBu)_{3}$ ligand have been omitted for clarity. (b) Synthesis of $[(\equiv$ SiO)₃Ga(HOR)], (2, R = $-Si(OtBu)$ ₃ or –tBu) and thermal transformation under high vacuum yielding thermal transformation under $[(\equiv$ SiO)₃Ga(XOSi \equiv)] (**3**, X = H or \equiv Si).

two v_{OH} bands in the range of 3800–3100 cm⁻¹ that are attributed to regenerated surface –OH sites and HOR $(R = -Si(OtBu)_{3}$ or –tBu) remaining on the surface (see ESI†). Additional v_{CH} bands of an alkoxide ligand are observed in the range of 3050–2860 and 1550–1360 cm^{-1} . ¹³C MAS SSNMR also revealed chemical shifts consistent with the presence of a remaining alcohol ligand on the surface of the material (see ESI†). Elemental analysis of the new material indicated a gallium loading of 1.53 weight% and 9.12 C atoms per Ga on the surface. These findings are consistent with a material possessing a remaining alcohol ligand per gallium immobilized on the support, specifically $[(\equiv \text{SiO})_3\text{Ga(HOR)}]$, $(2, R = -Si(OtBu)$ ₃ or $-tBu$).

The material 2 was then subjected to thermal treatment up to 500 °C for 10 hours under high vacuum (10⁻⁵ mbar). Analysis of the volatile components from thermolysis revealed 2.5 equivalents of isobutene per gallium on the surface gauged by $^1{\rm H}$ NMR spectroscopy. Quantification of $ca. 3 C₄$ fragments per gallium, the absence of v_{CH} and the regeneration of \equiv SiOH in the IR of the new material indicates that thermal elimination of aliphatics from 2 was achieved yielding $[(\equiv \text{SiO})_3\text{Ga(XOSi})]$ (3, X = H or \equiv Si)] along with the regeneration of \equiv SiOH groups (Fig. 1).

To understand the coordination environment of gallium on the silica surface, we performed X-ray absorption spectroscopy (XAS) measurements at Ga K-edge on materials 1–3. The edge position in the X-ray absorption near-edge structure (XANES) spectra of 2 and 3 was similar (10 374.8 and 10374.2 eV, respectively) as well as the position of a shoulder at higher energies (10 380.8 and 10 381.2 eV, respectively), which is consistent with tetra-coordinate $Ga(m)$ sites on the surface $(Fig. 2).^{7a,13}$

Fits of the extended X-ray absorption fine structure (EXAFS) data for complexes $1-3$ were fitted in R-space $(1.0-3.5 \text{ Å})$ after a Fourier transform (1 and 3, $k = 3.0$ –12.0 \AA^{-1} ; 2, $k = 3.0$ – 11.0 \AA^{-1}). The data are summarized in Table 1. For the molecular

Fig. 2 XANES spectra of $[Ga(OSi(OtBu)_{3})_{3}(THF)]$ (1), $[(\equiv SiO)_{3}Ga(HOR)]$, $(2, R = -Si(OtBu)_{3}$ or $-tBu$) and $[(\equiv SiO)_{3}Ga(XOS\equiv)]$ (3, X = H or \equiv Si).

Table 1 EXAFS fit parameters for $[Ga(OSi(OtBu)_{3})_{3}(THF)]$ (1) $[(\equiv$ SiO)₃Ga(HOR)], (2, R = -Si(OtBu)₃ or –tBu) and $[(\equiv$ SiO)₃Ga(XOSi \equiv)] $(3, X = H \text{ or } \equiv Si)^{a}$

Sample	Neighbor	N^b	r^c [Å]	σ^{2d} $\left[\AA^2\right]$
1	О	$3*$	1.788(3)	0.0035(2)
	О	$1*$	2.01(1)	0.0035(2)
	Si	$3*$	3.15(2)	0.007(2)
	O-Si	$6*$	3.25(3)	0.007(2)
	О	$3*$	3.50(2)	0.007(2)
2	О	4.1(4)	1.81(2)	0.008(1)
	Si	2.0(1.2)	3.17(1)	0.011(6)
3	О	3.6(5)	1.80(1)	0.008(1)
	Si	1.4(6)	3.08(3)	$0.011*$

 a^a Samples were measured at 295 K in transmission mode. b^b Number of neighbors. c Distance between Ga and neighbor. d Debye–Waller factor. Set parameters are indicated by (*).

complex 1, two Ga–O scattering paths at distances of 1.79 Å ($N =$ 3) and 2.01 Å ($N = 1$) were used for modeling of the 1st shell; a longer scattering path for Ga–Si of 3.15 Å $(N = 3)$ was also employed for modeling of the $2nd$ shell. An additional multiscattering path for Ga–O–Si of 3.25 Å ($N = 6$) and a long scattering path for Ga–O of 3.50 Å ($N = 3$) were required to produce a good fit. These distances match well with the X-ray single-crystal diffraction data obtained for 1. For the grafted complex 2 and the thermally treated complex 3, only Ga–O and Ga–Si scattering paths were used for fitting the experimental data. The fit for 2 indicates that Ga has 4.1 oxygen neighbors at 1.81 \AA and 2.0 silicon neighbors at 3.17 Å. Similarly, the best fit for 3 is consistent with 3.6 oxygen neighbors at 1.80 \AA and 1.4 silicon atoms at $3.08 \text{ Å}.$

Given the possibility of generating gallium dimers upon grafting on the surface of silica, 14 we have also probed the contribution of a Ga–Ga scattering path by performing a wavelet transform (WT) analysis¹⁵ on the EXAFS data for thermally treated 3 (Fig. 3). This analysis provides a correlation of R and k-space and ultimately aids in the distinction between two different atoms positioned at similar distances from the gallium metal center. The WT analysis of 3 shows a predominant feature with the maximum intensity in the range of $R =$ 1.2–1.6 Å and $k = 4.5$ –6.2 Å⁻¹, which is ascribed to the Ga–O scattering path. Scattering paths for Ga–Si and Ga–O–Si produce features in the range of $R = 2.6 - 2.8$ Å and $k = 6.0 - 8.0$ Å⁻¹ for complex 3; no Ga-Ga path could be identified. Fig. 3 also shows the WT analysis of EXAFS data of a $Ga₂O₃$ reference sample. This was done to evaluate the presence of a Ga–Ga scattering path in 3. The WT analysis performed on the EXAFS data of $Ga₂O₃$ shows a similar feature for a Ga–O scattering path described for 3 and an additional intense feature for a Ga–Ga scattering path in the range of $R = 2.5$ –3.0 Å and $k = 9.0$ –10.0 Å⁻¹. This later feature is not observed for complex 3, implying that a Ga–Ga scattering path is not significant for fitting of the EXAFS data, indicating that $Ga₂O₃$ domains are not present at the surface. Analysis of the XAS measurements for 1–3 strongly supports the formation of well-defined and dispersed tetra-coordinate gallium single-sites on the silica surface.

Fig. 3 Wavelet transform (WT) analysis of EXAFS data for Ga_2O_3 (top) and $[(\equiv \text{SiO})_3\text{Ga}(\text{XOSi})]$ (3, X = H or \equiv Si) (bottom).

To chemically probe the presence and accessibility of the gallium sites on the surface, pyridine adsorption studies were performed on 3 revealing three vibrational bands at 1621, 1493, 1458 cm^{-1} (see ESI†). These vibrational bands were retained upon heating to 500 $^{\circ}$ C under high vacuum indicating the presence of strong Lewis acid sites on the surface.^{7a,16} Additionally, no vibrational bands characteristic of the pyridinium ion were observed, indicating the absence of Brønsted acid surface sites.

We then investigated the catalytic performance of 3 towards PDH at 550 °C. Using a flow (10 mL per min; WHSV, 2.1 per h) consisting of 20% C_3H_8 in Ar, selectivity for propylene after 30 min was 94.3% with a TOF of 20.4 mol C_3H_6 per mol Ga per h and conversion of 9.3% (Fig. 4). After 20 hours of catalytic performance selectivity remained nearly constant $(\geq 93\%)$ with a TOF of 14.2 per h and conversion of 6.5%. The only other hydrocarbons detected during the duration of the experiment were methane and ethylene, determined to be secondary products of the reaction (see ESI†). After PDH only minimal darkening of the catalyst, as well as elemental analysis (0.18% C), suggests that coke formation is a negligible contribution to propane conversion. The initial TOF for 3 is ca. 11 times higher than recently reviewed $Ga₂O₃$ based materials (highest reported TOF of 1.8 per h; WHSV, 0.97 per h)^{1c} and five times greater than isolated Ga sites prepared by electrostatic adsorption (TOF of 3.8 per h), which were tested at significantly lower space velocities.^{7a} The higher activity of 3, with respect to the total metal loading of the catalysts, is attributed to negligible amounts of inactive bulk gallium-material being present in 3. Over the 20 hour experiment, 3 experiences a slow deactivation process (k_d of 0.02 per h) which is an order of magnitude slower

Fig. 4 Catalytic performance of $[(\equiv S_i O)_3Ga(XOS\equiv)]$ (3, X = H or \equiv Si) for propane dehydrogenation at 550 °C with conversions in the range of 9.3–6.5%. Propylene selectivity (circles) and turnover frequency per hour (triangles), over a period of 20 hours.

than that observed for Ga_2O_3 (k_d of 0.67 per h) and β - Ga_2O_3 $(k_d$ of 0.21 per h) which have a catalyst life of 4 and 6 hours, respectively.^{1c,17} An industrial-like $C\Gamma O_X-Na/Al_2O_3$ (20 wt% Cr, 1 wt% Na) catalyst displays an initial TOF of 0.027 per h and slightly lower selectivity (80%) for propylene at 550 $^{\circ}{\rm C}$ with a WHSV of 0.12 per h.^{1c} The considerably lower initial TOF in comparison to 3 highlights the effect of having signicant amounts of inactive bulk metal in the catalyst. These catalytic comparisons are summarized in the ESI.†

Fig. 5 XANES spectra of $[(\equiv \text{SiO})_3\text{Ga}(\text{XOSi})]$ (3, X = H or \equiv Si) before (bottom) and after (top) propane dehydrogenation at 550 \degree C for 20 hours.

In an effort to understand the stability of 3 under PDH conditions, XAS measurements at Ga K-edge of the spent catalyst were performed. This analysis revealed a partial reduction of the catalyst as evident by a new feature with an edge position at 10 370.6 eV in the XANES spectrum (Fig. 5). This shift to lower energies is attributed to partial formation of $Ga(I)$ surface sites as no vibrational bands characteristic of surface Ga–H species were observed in the IR spectrum of the spent catalyst (see ESI†). Analysis of the EXAFS data after catalysis displayed no intense feature at higher R-values $(2.2-3.5 \text{ Å})$ indicating that site-isolation of the gallium sites is retained after PDH. The partial reduction of the catalyst could explain the decrease in activity $(ca. 30\%)$ after 20 hours. The high TOF and selectivity $(\geq 93\%)$ maintained over 20 hours exemplifies the ability of SOMC methods to generate a stable material possessing highly active sites on the surface. It also indicates that site isolation and immobilization on a non-reducible support can diminish reduction processes that contribute to deactivation of other $Ga₂O₃$ -based materials.

Conclusions

In summary, we have synthesized silica-supported isolated tetra-coordinated gallium sites from a well-defined gallium-siloxide molecular precursor employing to a two-step process involving the grafting of a bulky siloxide molecular precursor 1 on highly dehydroxylated silica followed by thermolysis. XANES and EXAFS data, including a wavelet transform analysis, allowed for assignment of well-defined isolated gallium sites on the surface. Such material combines high activity towards propane dehydrogenation with high selectivity for propylene and stability over a 20 hour period. We attribute the prolonged stability of the catalyst to the generation of isolated Ga sites on a non-reducible support, thus diminishing facile reduction typical of Ga_2O_3 . This study has thus opened new avenues to generate more efficient and rationally designed dehydrogenation catalysts, and we are currently exploring this area.

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References

1 (a) Z. Nawaz, Rev. Chem. Eng., 2015, 31, 413–436; (b) D. Malakoff, Science, 2014, 344, 1464–1467; (c) J. J. H. B. Sattler, J. Ruiz-Martinez, E. Santillan-Jimenez and B. M. Weckhuysen, Chem. Rev., 2014, 114, 10613– 10653; (d) P. C. A. Bruijnincx and B. M. Weckhuysen, Angew. Chem., Int. Ed., 2013, 52, 11980–11987; (e) J. M. Thomas and W. J. Thomas, Principles and Practice of Heterogeneous Catalysis, Wiley-VCH, New York, 2nd edn, 2015; (f) G. Ertl, H. Knözinger, F. Schüth and J. Weitkamp, Handbook of Heterogeneous Catalysis, Wiley-VCH, Weinheim, 2nd edn, 2008; (g) K. Weisermel and H. J. Arpe, Industrial Organic Chemistry, Wiley-VCH, Weinheim, 4th edn, 2003.

- 2 D. Sanfilippo and I. Miracca, Catal. Today, 2006, 111, 133-139.
- 3 (a) R. Fricke, H. Kosslick, G. Lischke and M. Richter, Chem. Rev., 2000, 100, 2303–2406; (b) G. L. Price and V. Kanazirev, J. Catal., 1990, 126, 267–278; (c) P. Meriaudeau and C. Naccache, J. Mol. Catal., 1989, 50, L7–L10; (d) N. S. Gnep, J. Y. Doyemet, A. M. Seco, F. R. Ribeiro and M. Guisnet, Appl. Catal., 1988, 43, 155–166; (e) H. Kitagawa, Y. Sendoda and Y. Ono, J. Catal., 1986, 101, 12–18; (f) J. M. Thomas and X. S. Liu, J. Phys. Chem., 1986, 90, 4843–4847; (g) G. D. Meitzner, E. Iglesia, J. E. Baumgartner and E. S. Huang, J. Catal., 1993, 140, 209–225.
- 4 (a) S. Tan, S.-J. Kim, J. S. Moore, Y. Liu, R. S. Dixit, J. G. Pendergast, D. S. Sholl, S. Nair and C. W. Jones, ChemCatChem, 2016, 8, 214–221; (b) S. Tan, L. B. Gil, N. Subramanian, D. S. Sholl, S. Nair, C. W. Jones, J. S. Moore, Y. Liu, R. S. Dixit and J. G. Pendergast, Appl. Catal., A, 2015, 498, 167–175; (c) J. J. H. B. Sattler, I. D. Gonzalez-Jimenez, L. Luo, B. A. Stears, A. Malek, D. G. Barton, B. A. Kilos, M. P. Kaminsky, T. W. G. M. Verhoeven, E. J. Koers, M. Baldus and B. M. Weckhuysen, Angew. Chem., Int. Ed., 2014, 53, 9251– 9256; (d) J.-L. Wu, M. Chen, Y.-M. Liu, Y. Cao, H.-Y. He and K.-N. Fan, Catal. Commun., 2013, 30, 61–65; (e) P. Michorczyk, P. Ku´strowski, A. Kolak and M. Zimowska, Catal. Commun., 2013, 35, 95–100; (f) M. Chen, J. Xu, F.-Z. Su, Y.-M. Liu, Y. Cao, H.-Y. He and K.-N. Fan, J. Catal., 2008, 256, 293–300; (g) H. Li, Y. Yue, C. Miao, Z. Xie, W. Hua and Z. Gao, Catal. Commun., 2007, 8, 1317–1322; (h) B. Xu, B. Zheng, W. Hua, Y. Yue and Z. Gao, J. Catal., 2006, 239, 470–477; (i) B. Zheng, W. Hua, Y. Yue and Z. Gao, J. Catal., 2005, 232, 143–151; (j) N. S. Nesterenko, O. A. Ponomoreva, V. V. Yuschenko, I. I. Ivanova, F. Testa, F. Di Renzo and F. Fajula, Appl. Catal., A, 2003, 254, 261– 272; (k) K. Nakagawa, C. Kajita, K. Okumura, N.-O. Ikenaga, M. Nishitani-Gamo, T. Ando, T. Kobayashi and T. Suzuki, J. Catal., 2001, 203, 87-93; (l) K. Nakagawa, C. Kajita, Y. Ide, M. Okamura, S. Kato, H. Kasuya, N. O. Ikenaga, T. Kobayashi and T. Suzuki, Catal. Lett., 2000, 64, 215–221; (m) K. Nakagawa, M. Okamura, N. Ikenaga, T. Suzuki, K. Nakagawa, M. Okamura, T. Suzuki, T. Kobayashi and T. Kobayashi, Chem. Commun., 1998, 1025–1026; (n) H. Xiao, J. Zhang, P. Wang, X. Wang, F. Pang, Z. Zhang and Y. Tan, Catal. Sci. Technol., 2016, 6, 5183–5195; (o) M. Saito, S. Watanabe, I. Takahara, M. Inaba and K. Murata, Catal. Lett., 2003, 89, 213–217. Edge Article

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	- 5 (a) C. Copéret, Chem. Rev., 2010, 110, 656-680; (b) C. Copéret, D. P. Estes, K. Larmier and K. Searles, Chem. Rev., 2016, 116, 8463–8505.
- 6 (a) E. A. Pidko and R. A. van Santen, J. Phys. Chem. C, 2009, 113, 4246–4249; (b) E. J. M. Hensen, E. A. Pidko, N. Rane and R. A. van Santen, Angew. Chem., Int. Ed., 2007, 46, 7273–7276; (c) E. A. Pidko, R. A. van Santen and E. J. M. Hensen, Phys. Chem. Chem. Phys., 2009, 11, 2893– 2902.
- 7 (a) A. B. Getsoian, U. Das, J. Camacho-Bunquin, G. Zhang, J. R. Gallagher, B. Hu, S. Cheah, J. A. Schaidle, D. A. Ruddy, J. E. Hensley, T. R. Krause, L. A. Curtiss, J. T. Miller and A. S. Hock, Catal. Sci. Technol., 2016, 6, 6339–6353; (b) Y. Liu, Z. H. Li, J. Lu and K.-N. Fan, J. Phys. Chem. C, 2008, 112, 20382–20392; (c) I. Takahara, M. Saito, M. Inaba and K. Murata, *Catal. Lett.*, 2004, 96, 29-32; (d) P. Michorczyk and J. Ogonowski, Appl. Catal., A, 2003, 251, 425–433; (e) A. A. Gabrienko, S. S. Arzumanov, A. V. Toktarev and A. G. Stepanov, Chem. Phys. Lett., 2010, 496; (f) V. B. Kazansky, I. R. Subbotina, A. A. Pronin, R. Schlögl and F. C. Jentoft, J. Phys. Chem. B, 2006, 110, 7975–7978; (g) U. Das, G. Zhang, B. Hu, A. S. Hock, P. C. Redfern, J. T. Miller and L. A. Curtiss, ACS Catal., 2015, 5, 7177–7185.
- 8 (a) C. Copéret, A. Comas-Vives, M. P. Conley, D. P. Estes, A. Fedorov, V. Mougel, H. Nagae, F. Núñez-Zarur and P. A. Zhizhko, Chem. Rev., 2016, 116, 323–421; (b) C. Copéret, M. Chabanas, R. Petroff Saint-Arroman and J.-M. Basset, Angew. Chem., Int. Ed., 2003, 42, 156–181; (c) S. L. Wegener, T. J. Marks and P. C. Stair, Acc. Chem. Res., 2012, 45, 206–214; (d) J. D. A. Pelletier and J.-M. Basset, Acc. Chem. Res., 2016, 49, 664–677.
- 9 (a) T. D. Tilley, J. Mol. Catal. A: Chem., 2002, 182–183, 17–24; (b) C. Nozaki, C. G. Lugmair, A. T. Bell and T. D. Tilley, *J. Am.* Chem. Soc., 2002, 124, 13194–13203; (c) J. Jarupatrakorn and T. D. Tilley, J. Am. Chem. Soc., 2002, 124, 8380–8388; (d) K. L. Fujdala and T. D. Tilley, J. Catal., 2003, 216, 265–275; (e) K. L. Fujdala, R. L. Brutchey and T. D. Tilley, Surface and Interfacial Organometallic Chemistry and Catalysis, Springer, Berlin, Heidelberg, 2005; (f) A. W. Holland, G. Li, A. M. Shahin, G. J. Long, A. T. Bell and T. D. Tilley, J. Catal., 2005, 235, 150–163; (g) M. P. Conley, M. F. Delley, G. Siddiqi, G. Lapadula, S. Norsic, V. Monteil, O. V. Safonova and C. Copéret, Angew. Chem., Int. Ed., 2014, 53, 1872-1876; (h) M. F. Delley, F. Núñez-Zarur, M. P. Conley, A. Comas-Vives, G. Siddiqi, S. Norsic, V. Monteil, O. V. Safonova and C. Copéret, Proc. Natl. Acad. Sci. U. S. A., 2014, 111, 11624-11629; (i) V. Mougel, K.-W. Chan, G. Siddiqi, K. Kawakita, H. Nagae, H. Tsurugi, K. Mashima, O. Safonova and C. Copéret, ACS Cent. Sci., 2016, 138, 14987–14997; (j) D. P. Estes, G. Siddiqi, F. Allouche, K. V. Kovtunov, O. V. Safonova, A. L. Trigub, I. V. Koptyug and C. Copéret, J. Am. Chem. Soc., 2016, 2, 569–576; (k) R. L. Brutchey, C. G. Lugmair, L. O. Schebaum and T. D. Tilley, J. Catal., 2005, 229, 72–81.
- 10 $[Ga(OSi(Okba)]_3(THF)]$ was disclosed during the course of this study; J. P. Dombrowski, G. R. Johnson, A. T. Bell and T. D. Tilley, Dalton Trans., 2016, 11025–11034.
- 11 M. H. Reineke, M. D. Sampson, A. L. Rheingold and C. P. Kubiak, Inorg. Chem., 2015, 54, 3211–3217.
- 12 Silica (Degauss Aerosol, 204 $\mathrm{m^2\,g^{-1}}$) thermally treated at 700 $^{\circ} \mathrm{C}$ with a temperature ramp of 5 $^{\circ} \mathrm{C}$ per min under high vacuum (10⁻⁵ mbar) yielded 0.31 mmol OH per g of $SiO₂$ corresponding to 0.92 accessible OH groups per nm^2 . The slightly higher –OH density in comparison to that reported in literature for $SiO₂₋₇₀₀$ is attributed to the slightly higher temperature ramp used during dehydroxylation (see ref. 8a). Openical Science

12. Silvin (Degrade on 03 January 2017) 13: The minimaler Mole 11:40:25. The minimale Common Commo
	- 13 (a) K. Nishi, K.-i. Shimizu, M. Takamatsu, H. Yoshida, A. Satsuma, T. Tanaka, S. Yoshida and T. Hattori, J. Phys. Chem. B, 1998, 102, 10190–10195; (b) P. Behrens, H. Kosslick, T. Vu Anh, M. Fröba and F. Neissendorfer, Microporous Mater., 1995, 3, 433–441; (c) K. A. Al-majnouni, N. D. Hould, W. W. Lonergan, D. G. Vlachos and R. F. Lobo, J. Phys. Chem. C, 2010, 114, 19395–19405; (d)

R. I. Walton and D. O'Hare, J. Phys. Chem. Solids, 2001, 62, 1469–1479.

- 14 (a) Z. A. Taha, E. W. Deguns, S. Chattopadhyay and S. L. Scott, Organometallics, 2006, 25, 1891–1899; (b) S. D. Fleischman and S. L. Scott, J. Am. Chem. Soc., 2011, 133, 4847–4855.
- 15 H. Funke, M. Chukalina and A. C. Scheinost, J. Synchrotron Radiat., 2007, 14, 426–432.
- 16 (a) A. Vimont, J. C. Lavalley, A. Sahibed-Dine, C. Otero Areán, M. Rodríguez Delgado and M. Daturi, J. Phys. Chem. B, 2005, 109, 9656–9664; (b) E. P. Parry, J. Catal., 1963, 2, 371–379.
- 17 k_d is defined as $ln(1 conv_{end}/conv_{end}) ln(1 conv_{start}/$ $conv_{start}$)/t, where conv_{start} is the conversion at start of experiment, convend is the conversion at end of experiment, and t is the duration of experiment in hours.