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# N-Heterocyclic Carbene Modified Palladium Catalysts for the Direct Synthesis of Hydrogen Peroxide

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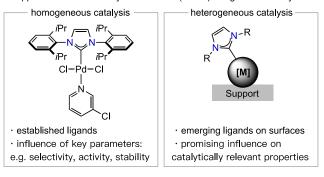
Supporting Information

**ABSTRACT:** Heterogeneous palladium catalysts modified by N-heterocyclic carbenes (NHCs) are shown to be highly effective toward the direct synthesis of hydrogen peroxide  $(H_2O_2)$ , in the absence of the promoters which are typically required to enhance both activity and selectivity. Catalytic evaluation in a batch regime demonstrated that through careful selection of the N-substituent of the NHC it is possible to greatly enhance catalytic performance when compared to the unmodified analogue and reach concentrations of  $H_2O_2$  rivaling that obtained by state-of-the-art catalysts. The enhanced performance of the modified catalyst, which is retained upon reuse, is attributed to the ability of the NHC to electronically modify Pd speciation.

T-Heterocyclic carbenes (NHCs) are well-established compounds in various fields of chemistry and find application as ligands for numerous processes in the field of homogeneous catalysis. 1-3 This is due to their effective and controllable donor capability and highly modular structure. As a result, parameters such as stability, reactivity, and selectivity can be effectively tuned, allowing ligands to be tailored for a wide variety of applications. Well-known precatalysts containing NHCs as ligands include PEPPSI (pyridine-enhanced precatalyst preparation stabilization and initiation) and the second-generation Grubbs (-Hoveyda) catalysts. 4,5 In comparison, the systematic application of NHCs as ligands in heterogeneous catalysis is still in its infancy.<sup>6,7</sup> There is a growing number of reports using NHCs for surface modification, <sup>8–10</sup> with many studies demonstrating their ability to control important catalytic properties (Figure 1A presents an example of both an NHC-based homogeneous catalyst and an NHC-promoted heterogeneous catalyst). 11-20 Building on these fundamental discoveries, the goal of this work is to use NHC-modified heterogeneous catalysts for the production of the commodity chemical hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) from the elements (Figure 1B).

Global demand for H<sub>2</sub>O<sub>2</sub> has risen significantly in recent years, driven largely by its use as an oxidant for a range of chemical transformations, as well as its utilization as a bleaching agent. Currently, industrial production of H<sub>2</sub>O<sub>2</sub> is met almost entirely via the highly efficient anthraquinone oxidation process.<sup>21</sup> However, numerous routes to small-scale H<sub>2</sub>O<sub>2</sub> production have been investigated, including electrochemical,<sup>22</sup> photocatalytic,<sup>23</sup> and thermal catalytic approaches.<sup>24</sup> The thermal catalytic direct synthesis of H<sub>2</sub>O<sub>2</sub> from the elements is considered particularly attractive for onsite production, at desirable concentrations of this powerful oxidant, and theoretically allows for total atom efficiency. The direct route is of particular interest for chemical processes

A. Application of N-heterocyclic carbenes (NHCs) as ligands in catalysis



B. NHCs as ligands for the direct hydrogen peroxide synthesis (this work)

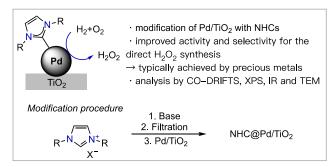


Figure 1. N-Heterocyclic carbenes as ligands in catalysis and their application for the direct synthesis of hydrogen peroxide.

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Table 1. Influence of Structurally Diverse NHCs on the Productivity and Selectivity of 1%Pd/TiO<sub>2</sub> toward the Direct Synthesis of H<sub>2</sub>O<sub>2</sub>

entry	catalyst	$\begin{array}{c} productivity/\\ mol_{H2O2} \ k{g_{cat}}^{-1} \ h^{-1} \end{array}$	H <sub>2</sub> O <sub>2</sub> concn/ wt %	apparent rate of reaction at 30 min/ $\mathrm{mmol}_{\mathrm{H2O2}}$ $\mathrm{mmol}_{\mathrm{Pd}}^{-1}$ $\mathrm{min}^{-1}$	$\begin{array}{c} \operatorname{degradation/} \\ \operatorname{mol}_{\mathrm{H2O2}}  \operatorname{kg}_{\mathrm{cat}}^{-1}  \operatorname{h}^{-1} \end{array}$
1	$1\%Pd/TiO_2$ (unmodified)	80	0.16	$8.73 \times 10^2$	231
2	$1\%Pd\text{-ICy}(1:1)/TiO_2$	110	0.21	$1.19 \times 10^{3}$	208
3	$1\%Pd\text{-IMes}(1:1)/TiO_2$	133	0.27	$1.40 \times 10^{3}$	202
4	1%Pd-IPr(1:1)/TiO <sub>2</sub>	160	0.32	$1.70 \times 10^3$	184
5	$1\%Pd-pPh-IPr(1:1)/TiO_2$	118	0.23	$1.26 \times 10^{3}$	169
6	1%Pd-IPr*(1:1)/TiO <sub>2</sub>	110	0.21	$1.15 \times 10^3$	137
7	$1\%Pd/TiO_2 + IPr-HBF_4$	79	0.16	$8.41 \times 10^2$	237
8	IPr-HBF <sub>4</sub>	0	0	0	0
9	$TiO_2$ (P25)	0	0	0	0

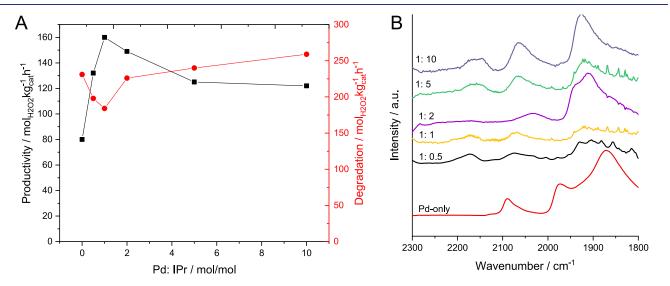


Figure 2. Effect of Pd:IPr ratio on catalytic performance toward the direct synthesis of  $H_2O_2$ . (A) Catalytic activity of NHC-modified  $1\%Pd/TiO_2$  catalysts toward the direct synthesis of  $H_2O_2$  and its subsequent degradation as a function of Pd:IPr molar ratio. (B) CO-DRIFTS spectra of the  $1\%Pd-IPr/TiO_2$  catalysts, as a function of Pd:IPr molar ratio.  $H_2O_2$  direct synthesis reaction conditions: catalyst (0.01 g),  $H_2O$  (2.9 g), MeOH (5.6 g),  $5\%PH_2/CO_2$  (420 psi), 25%  $O_2/CO_2$  (160 psi), 0.5 h, 2 °C, 1200 rpm.  $H_2O_2$  degradation reaction conditions: catalyst (0.01 g),  $H_2O_2$  (50 wt %, 0.68 g)  $H_2O$  (2.22 g), MeOH (5.6 g),  $5\%PH_2/CO_2$  (420 psi), 0.5 h, 2 °C, 1200 rpm.

where the generated  $H_2O_2$  is utilized *in situ* for chemical valorization<sup>25</sup> or pollutant degradation.<sup>26</sup> Pd-based catalysts have been widely studied for the direct synthesis reaction;<sup>27</sup> however, they typically suffer from poor selectivity and require the use of halide<sup>28–30</sup> or acid promoters.<sup>31</sup> While the use of such agents can significantly enhance catalytic performance, their application can have deleterious effects on catalyst and reactor lifetimes and lead to the formation of complex product streams. Indeed, in the case of some catalyst formulations the use of halide additives can lead to a near-total inhibition of catalytic performance;<sup>32</sup> as such, there is a need for alternative approaches to improve catalytic activity and selectivity.

The introduction of secondary metals<sup>33–36</sup> has also been demonstrated to inhibit competitive reaction pathways while avoiding the need for the stabilizing agents typically utilized for Pd-only analogues. Notably, Fischer et al. have reported that combining the stabilizing agents typically utilized for Pd-only catalysts (HBr and  $\rm H_3PO_4$ ) with bimetallic Pd-based formulations exceptionally high concentrations of  $\rm H_2O_2$  can be obtained. It should be emphasized that such concentrations

are far greater than those often reported in the literature and are even more remarkable, given the use of a water-only reaction medium, which avoids the additional process costs associated with the alcohol cosolvents commonly used to promote H<sub>2</sub> solubility.<sup>37</sup> However, the additional costs and often complex synthesis procedures associated with the use of bimetallic catalysts have prompted a focus on alternative means to improve the performance of Pd-only formulations. The encapsulation of supported Pd nanoparticles in organic moieties such as poly(vinyl alcohol) or poly(vinylpyrrolidone) has been shown to enhance performance by selectively tuning the three-dimensional environment of the metal nanoparticle.38-40 Recently, the groups of Pérez-Ramírez and Nikolla have expanded on these studies, with the latter establishing the efficacy of a series of surface-bound ligand modifiers to promote the selectivity of Pd nanoparticles toward H<sub>2</sub>O<sub>2</sub>.41,42

Herein, the effect of a range of NHCs (ICy, IMes, IPr, pPh-IPr, and IPr\*) on the catalytic performance of supported Pd catalysts toward the direct synthesis and subsequent

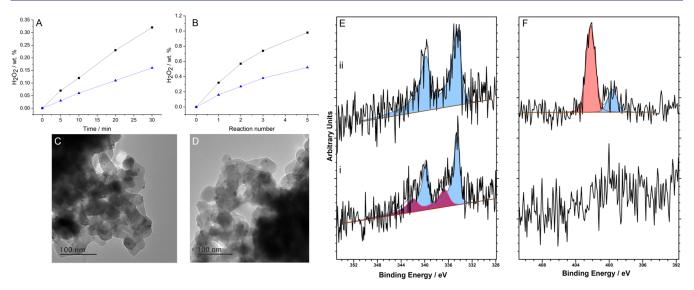


Figure 3. Comparison of catalytic performance toward the direct synthesis of  $H_2O_2$  in addition to a structural and morphological analysis of the 1% Pd/TiO<sub>2</sub> and 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalysts. (A) Catalytic activity as a function of reaction time and (B) over sequential  $H_2O_2$  synthesis reactions. Key: 1%Pd/TiO<sub>2</sub> (blue triangles); 1%Pd-IPr(1:1)/TiO<sub>2</sub> (black squares). TEM micrographs of the (C) 1%Pd/TiO<sub>2</sub> and (D) 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalysts. XPS spectra of (E) Pd(3d) and (F) N(1s) regions for (i) 1%Pd/TiO<sub>2</sub> and (ii) 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalysts. Key: for the Pd 3d spectra Pd<sup>2+</sup> (purple), Pd<sup>0</sup> (blue); for the N 1s spectra, imidazolium salt (peach), NHC-Pd moiety (blue).  $H_2O_2$  direct synthesis reaction conditions: catalyst (0.01g),  $H_2O$  (2.9 g), MeOH (5.6 g), 5%H<sub>2</sub>/CO<sub>2</sub> (420 psi), 25%O<sub>2</sub>/CO<sub>2</sub> (160 psi), 0.5 h, 2%C, 1200 rpm.

degradation of H<sub>2</sub>O<sub>2</sub> was investigated. For this purpose, the free NHCs were prepared via deprotonation of the corresponding imidazolium salts and subsequently immobilized onto a 1%Pd/TiO<sub>2</sub> catalyst. Successful NHC deposition onto the catalyst surface was confirmed using attenuated total reflectance infrared spectroscopy (ATR-IR) (Figure S.1) and corroborated by XPS (Figure S.2; corresponding spectra of the imidazolium salts are reported in Figure S.3). Initial catalytic testing established the activity of the NHC-modified 1%Pd/ TiO<sub>2</sub> catalysts (Table 1). The unmodified 1%Pd/TiO<sub>2</sub> catalyst (entry 1) was found to be highly active toward H<sub>2</sub>O<sub>2</sub> synthesis  $(80 \text{ mol}_{\text{H2O2}} \text{ kg}_{\text{cat}}^{-1} \text{ h}^{-1})$  but also displayed considerable activity toward its subsequent degradation (221  $\text{mol}_{\text{H2O2}}$ kg<sub>cat</sub> - 1 h<sup>-1</sup>). The introduction of the various NHCs (so that the Pd:NHC molar ratio was equal to 1:1) was found to greatly modify catalytic activity toward both the direct synthesis and subsequent degradation of H<sub>2</sub>O<sub>2</sub>. In particular, the optimal 1% Pd-IPr(1:1)/TiO<sub>2</sub> catalyst (entry 4) offered H<sub>2</sub>O<sub>2</sub> synthesis rates (160 mol<sub>H2O2</sub> kg<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>) double that of the unmodified analogue, while degradation rates were reduced (184  $mol_{H2O2}$ kg<sub>cat</sub><sup>-1</sup> h<sup>-1</sup>). Indeed, the catalytic activity of the 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalyst can be considered to rival that achieved by state-of-the-art materials, 33,34 under identical reaction conditions, although it should be noted that the NHCmodified material is unable to attain the high selectivities toward H<sub>2</sub>O<sub>2</sub> such as those reported in earlier works (Table S.1). The improved activity of the 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalyst was also observed under conditions considered less conducive to H<sub>2</sub>O<sub>2</sub> stability (Table S.2). Further studies, comparing the activity of the optimal 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalyst to an equimolar physical mixture of 1%Pd/TiO2 and imidazolium salt (IPr-HBF<sub>4</sub>) (entry 7), indicated that the NHC must be present on the catalytic surface in order to achieve enhanced activity toward H2O2. It should be noted that neither the IPr-HBF4 salt alone nor the titania support exhibited any activity toward H2O2 synthesis or its subsequent degradation (entries 8 and 9, respectively).

The stark improvement in catalytic performance observed over the  $1\%\text{Pd-IPr}(1:1)/\text{TiO}_2$  catalyst, in comparison to the unmodified analogue, motivated us to further investigate the effect of varying the Pd:IPr molar ratio on catalytic performance (Figure 2A). These studies indicated an optimal catalyst composition of  $1\%\text{Pd-IPr}(1:1)/\text{TiO}_2$ . Increasing IPr content further was found to result in a decrease in  $H_2O_2$  production, with a corresponding increase in  $H_2O_2$  degradation, although it is noteworthy that, despite this loss in catalytic selectivity at higher IPr loadings, all IPr-containing catalysts still outperformed the  $1\%\text{Pd/TiO}_2$  analogue.

With NHCs well-known to act as modifiers of metal species, we next set out to determine the means by which the catalytic performance was enhanced through NHC incorporation. The evaluation of the 1%Pd-IPr/TiO<sub>2</sub> catalysts with varying Pd:IPr molar ratio by CO-DRIFTS is shown in Figure 2B (an analysis of the IPr/TiO<sub>2</sub> material (i.e., without Pd present) is reported in Figure S.4). Typically, the CO-DRIFTS spectra of supported Pd catalysts include CO adsorbed in a linear and nonlinear mode at approximately 2050-2100 and 1800-2000 cm<sup>-1</sup>, respectively. 44 The 1%Pd/TiO<sub>2</sub> catalyst was found to exhibit the expected absorption bands, specifically at 2090, 1980, and 1870 cm<sup>-1</sup>. The addition of the IPr moiety results in two major changes to the CO-DRIFTS spectra. This includes a new absorption band, which appears at 2170 cm<sup>-1</sup>, suggesting a new adsorption site associated with the IPr-containing catalysts.

A systematic shift in the wavenumber of the linear CO-Pd band was observed as the IPr:Pd molar ratio increased, from 2090 cm<sup>-1</sup> in the 1%Pd/TiO<sub>2</sub> catalyst to 2060 cm<sup>-1</sup> in the 1% Pd-IPr(1:10)/TiO<sub>2</sub> formulation. Such a shift indicates that the adsorption of CO onto the Pd surface increases in strength, which can be explained by the transfer of charge from the NHC to the Pd surface and the resulting enhanced backdonation to CO. Similar observations have been made by Ouyang et al., who reported a comparable red shift upon the alloying of Au with Pd and an associated enhancement in

catalytic selectivity.<sup>45</sup> It is therefore possible to conclude the enhanced activity that results from the introduction of the NHCs onto the catalyst surface can be attributed to the ability of the carbene moiety to electronically modify Pd species.

Finally, with the evident improved efficacy of the 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalyst in comparison to the unmodified 1% Pd/TiO<sub>2</sub> analogue established, we were motivated to investigate this subset of materials to gain further insight into the underlying cause for the observed differences in performance. An assessment of selectivity toward H<sub>2</sub>O<sub>2</sub> (Table S.3) further demonstrates the improvement that results from the introduction of the carbene onto the catalytic surface, with the 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalyst displaying far greater selectivity toward H<sub>2</sub>O<sub>2</sub> (64%) than the 1%Pd/TiO<sub>2</sub> analogue (22%). In keeping with earlier studies (Table 1, entry 7) an evaluation of fresh and used materials by XPS indicates that the observed promotive effect that results from NHC incorporation cannot be attributed to the presence of residual halide (Table S.4). The enhanced activity of the 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalyst was further highlighted through a comparison of initial reaction rates (Table S.5), where there are assumed to be no limitations associated with reactant availability or contribution from H<sub>2</sub>O<sub>2</sub> degradation pathways.

A comparison of catalytic activity as a function of reaction time can be seen in Figure 3A, with the greater activity of the 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalyst again clear, achieving concentrations of H<sub>2</sub>O<sub>2</sub> (0.32 wt %) double that of the unmodified analogue (0.16 wt %), over a standard 0.5 h reaction. Indeed, the 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalyst displayed rates of H<sub>2</sub>O<sub>2</sub> synthesis comparable to those reported for the current stateof-the-art materials.<sup>33,34</sup> A further evaluation of catalytic performance over sequential H<sub>2</sub>O<sub>2</sub> synthesis reactions (Figure 3B) again demonstrates the enhanced activity of the 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalyst, which was able to achieve H<sub>2</sub>O<sub>2</sub> concentrations (0.98 wt %) comparable to that achieved by state-of-the-art materials.34

Numerous studies have demonstrated the strong relationship between catalytic activity toward H2O2 synthesis and the particle size of Pd-only catalysts. 46 The determination of mean particle size via TEM (Figure 3C,D, with particle size distributions shown in Figure S.5) indicates no significant change as a result of the introduction of the IPr carbene onto the 1%Pd/TiO<sub>2</sub> catalyst (mean particle sizes determined to be 2.0 and 2.4 nm for the 1%Pd/TiO<sub>2</sub> and 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalysts, respectively). As such, it is reasonable to propose that the enhanced activity of the 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalyst is not associated with increased metal dispersion. However, an analysis of the 1%Pd-IPr(1:1)/TiO<sub>2</sub> and 1%Pd/TiO<sub>2</sub> catalysts via XPS indicated that the introduction of the IPr carbene leads to a significant shift in the Pd oxidation state, toward Pd<sup>0</sup> (Figure 3E,F), corroborating our studies via CO-DRIFTS (Figure 2.B).

We further determined the high stability of both the 1%Pd/ TiO<sub>2</sub> and 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalysts. No loss in H<sub>2</sub>O<sub>2</sub> synthesis activity was observed upon reuse of either material in the direct synthesis reaction (Table S.5), while ICP-MS analysis of post-reaction solutions (Table S.6) indicated negligible metal leaching over the course of a standard reaction. An analysis by TEM reveals a minor increase in mean particle size after use (Figure S.6), although such a shift occurs to a lesser extent over the NHC-incorporated material, while XPS (Figure S.7) reveals no significant variation in Pd oxidation state between the fresh and used materials. However,

in the case of the IPr-modified sample, we do observe a substantial loss in the N(1s) signal associated with the residual parent imidazolium salt (centered at 403 eV), while the corresponding signal associated with IPr moiety interacting with Pd nanoparticles is retained, which correlates well with the observed stability of the catalytic material and indicates that the enhanced activity of the 1%Pd-IPr(1:1)/TiO<sub>2</sub> catalyst results from the Pd-IPr interaction.

We have demonstrated the enhanced activity and selectivity of NHC-modified supported palladium nanoparticles toward the direct synthesis of H2O2. Our studies reveal the ability of the NHC ligands to act as electronic modifiers of Pd, in a way similar to that observed previously through the introduction of secondary metals, with the catalytic performance being retained upon reuse. Such results not only demonstrate the efficacy of these materials toward H2O2 formation but also highlight the role that this class of ligand may offer toward a range of heterogeneously catalyzed reaction pathways.

#### ASSOCIATED CONTENT

### Supporting Information

The Supporting Information is available free of charge at https://pubs.acs.org/doi/10.1021/jacs.2c04828.

Experimental procedures, catalytic testing data, and material characterization (ATR-IR, XPS, CO-DRIFTS and TEM) in addition to metal leaching analysis via ICP-MS (PDF)

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#### **Author Contributions**

<sup>⊥</sup>R.J.L. and M.K. contributed equally.

#### Notes

The authors declare no competing financial interest.

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#### DEDICATION

This paper is dedicated to Guy Bertrand on the occasion of his 70th birthday.

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