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Optimizing radionuclide sequestration in anion nanotraps with record pertechnetate sorption

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The elimination of specific contaminants from competitors poses a significant challenge. Rather than relying on a single direct interaction, the cooperation of multiple functionalities is an emerging strategy for adsorbents design to achieve the required affinity. Here, we describe that the interaction with the target species can be altered by modifying the local environment of the direct contact site, as demonstrated by manipulating the affinity of pyridinium-based anion nanotraps toward pertechnetate. Systematic control of the substituent effect allows the resulting anion nanotraps to combine multiple features, overcoming the long-term challenge of TcO_4^- segregation under extreme conditions of super acidity and basicity, strong irradiation field, and high ionic strength. The top material exhibits the highest sorption capacity together with record-high extraction efficiencies after a single treatment from conditions relevant to the used nuclear fuel (Hanford tank wastes, 95%) and legacy nuclear wastes (Savannah River Sites, 80%) among materials reported thus far.

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Nuclear fission is a mature technology that can make a vital contribution toward global low-carbon energy needs^{1–6}. However, opposition over the safety and security of nuclear facilities and materials still remains and needs to be addressed if new nuclear facilities are to gain widespread acceptance. Much of the controversy surrounding nuclear power stems from the early days of industrial development and the Cold War arms race, which has left a legacy of contaminated sites that must be cleaned up^{7–9}. In addition, the development of nuclear technologies has led to many cases of accidental and intentional release, with the accumulation of significant levels of radionuclides in the environment^{10–12}. One potentially troublesome radionuclide is technetium-99 (⁹⁹Tc), a considerable fraction of which occurs as pertechnetate, TcO_4^- . This species, with a long half-life of 213,000 years, is highly mobile in groundwater and biological systems, leading to possible problematic spread of radiotoxic material following containment breaches^{13–16}. In addition, the volatile nature of some ⁹⁹Tc compounds (e.g., Tc_2O_7), generated during high-temperature vitrification of the nuclear waste, makes ⁹⁹Tc problematic in the off-gas system design for vitrification facilities¹⁷. To this end, ⁹⁹Tc management is important both in terms of ensuring safe disposal of radioactive waste from power generation, minimizing the off-site migration of the contaminated groundwater, and assisting in cleanup efforts of legacy waste sites, yet it remains an unmet challenge^{17,18}.

To address this need, recent efforts have focused on developing ion-exchange sorbents given their ease of implementation and high ⁹⁹Tc recovery rate^{19–24}. While elegant examples of materials embodying this strategy are now known, the battle to ameliorate ⁹⁹Tc contamination is far from finished. Current industrial extraction technologies suffer from relatively low affinity and kinetics, as well as limited capacity for TcO_4^- . Given this, proper remediation of the legacy tank wastes is still pending. These facts underscore the need for material innovation capable of extracting radionuclides from complex media for environmental remediation and in order to close the nuclear fuel cycle.

Nature has been subject to millions of years of evolutionary experimentation to recognize specific metal ions with high sensitivity, whereby multiple functionalities are assisted with the direct binding sites. Chemical efforts to mimic such partnership have led to numerous advances in control of binding affinity. As a sophisticated example, supramolecular techniques have been utilized to engineer cations with intriguing properties that display particular innovation and hold promise as potential game-changing technologies in the field of target ion extraction. The selectivity emerges from the concerted efforts of the binding partners^{25–27}. Thus, it is well conceivable that some structural modifications to a site separate from the place of direct contact of the association partners may well affect their binding strength, thereby providing the needed ability to recognize target anions under highly competitive conditions. While success was encountered using these receptors in the context of a classic liquid–liquid extraction approach, to meet the challenges posed by the immense volumes of wastewater, sorbent materials would allow for an increase in operational ability^{28–34}. With these in mind, we envisioned that if distinct functionalities can be incorporated into a highly porous cationic framework, this may enable a new level of control over ion pair recognition and extraction efficiency within a sorbent material with a high density of readily accessible ion-exchange sites. This is also anticipated to afford new anion receptors with fast kinetics together with high uptakes, which surmount the prime issues of low efficiency encountered by commercial resins as a result of low surface area and low density of accessible ion-exchange groups.

To explore the validity of this hypothesis, we were motivated by the exploration of porous organic polymers (POPs) for this

ambitious task. This class of porous material has moved to the forefront of materials research due to their modular nature. POPs exhibit tailorable porosity and tunable functionality, and are well-suited for a wide range of applications including gas storage/separation, catalysis, hazard contaminants removal, and sensing, to name a few^{35–41}. The potential to deploy POPs as solid extractors is related to the ease of tunability with regard to their composition^{42–44}. In this contribution, we chose pyridinium as the cation building unit to demonstrate the proof-of-concept, given its chemical stability, amenable synthesis, together with easy-to-get properties⁴⁵. To optimize the anion exchange performance and to establish the structure-property relationships, different anchor groups were de novo introduced (Fig. 1). In addition, to improve the uptake capacity and efficiency of the resultant anion nanotraps, porous sorbent materials were constructed by the functional pyridinium moieties alone, to conserve a sufficiently high density of accessible exchange sites. Therefore, the resultant materials combine the advantages of high uptake capacity, selectivity, and removal rate of $\text{TcO}_4^-/\text{ReO}_4^-$ ions, making them promising for decontamination of polluted water and remediation of nuclear waste. Through detailed studies, we showed that the adsorbent constructed with a dimethylamino group in the para position relative to pyridinium displayed extraordinary affinity for TcO_4^- with a record-breaking uptake capacity and selectivity under extreme conditions of super acidity and basicity, as well as high concentrations of competitors. These insights are meant to guide further research, which should be devoted to increasing the binding affinity of adsorbents toward target ions.

Results

Material synthesis. To target the desired materials, our initial step was to construct pyridine moieties with various anchor groups into porous frameworks, due to the low solubility of pyridinium in organic solvents, which is detrimental to yield highly porous polymers. To construct these moieties into porous polymers, we decided to use free radical induced polymerization with the following considerations: (i) the resultant highly cross-linked polymer chains and thus the rigidity of the matrix, reduce the ability of the pyridinium to congregate in hydrated domains, which decrease the affinity for more hydrated anions and thereby enhance the selectivity for less hydrated anions such as TcO_4^- ⁴⁶; and (ii) the adapted synthesis allows for the introduction of hierarchical porosity in the resultant polymers, which is expected to enhance the kinetics, thereby offering an opportunity to meet the challenges posed by the vast volumes of wastewater^{47,48}. To this end, we further functionalized the pyridine moieties with vinyl groups, affording V-Py, V-*p*NH₂Py, and V-*p*N(Me)₂Py, respectively (Table 1). Under solvothermal conditions in dimethylformamide (DMF) at 100 °C, polymerization of these monomers in the presence of azobisisobutyronitrile (AIBN) gave rise to the porous pyridine-based polymers in quantitative yields, which were denoted as POP-Py, POP-*p*NH₂Py, and POP-*p*N(Me)₂Py, respectively. To introduce ion-exchange sites, the pyridine moieties in the resultant materials underwent a quaternization reaction with methyl iodide (CH_3I), yielding the porous ionic organic polymer of polymerized quaternary ammonium (PQA) salt PQA-Py-I, PQA-*p*NH₂Py-I, and PQA-*p*N(Me)₂Py-I, respectively.

Among the synthesized porous materials, POP-*p*N(Me)₂Py and corresponding quaternization product PQA-*p*N(Me)₂Py-I were chosen as representative samples for thorough illustration. As probed by scanning electron microscopy (SEM) and transmission electron microscopy (TEM), it is revealed that no noticeable morphological changes occurred after quaternization, both

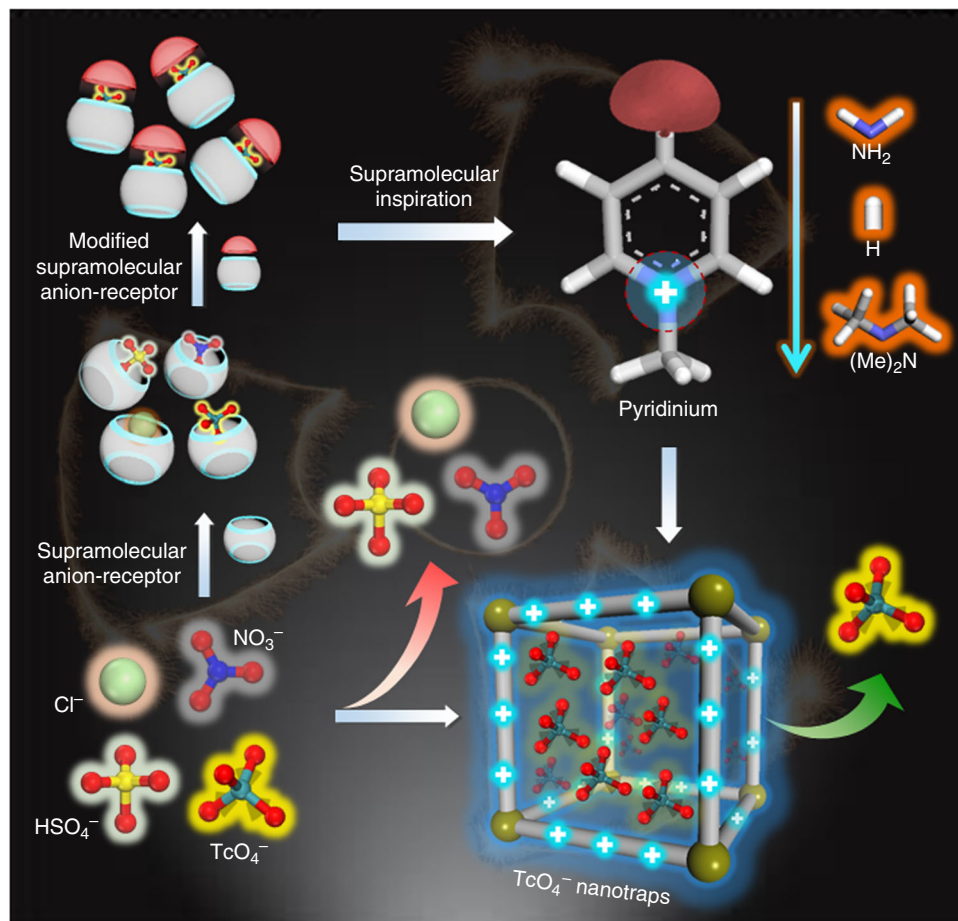


Fig. 1 Anion nanotraps for TcO_4^- removal. Illustration of optimizing pyridinium based anion nanotraps for TcO_4^- recognition inspired by supramolecular technology

Table 1 Structure of building units and textural parameters of various pyridinium functionalized hierarchical porous polymers

PQA	BET surface area (m^2g^{-1})	Pore volume (cm^3g^{-1})
PQA-Py-I	465	0.645
PQA- <i>p</i> NH ₂ Py-I	344	0.238
PQA- <i>p</i> N(Me) ₂ Py-I	223	0.15

POP-*p*N(Me)₂Py and PQA-*p*N(Me)₂Py-I feature aggregates comprising interconnected nanoparticles with sizes of 50–100 nm (Supplementary Fig. 1 and 2). Structural details of these materials were elaborated by solid-state ¹³C NMR spectroscopy. As seen in Supplementary Fig. 3, the characteristic vinyl ¹³C resonance located in the range of 100.0–110.0 ppm in the monomers disappears with the concomitant appearance of the polymerized vinyl group peak at 31.8 ppm, confirming the

conversion of the monomer into the respective polymer⁴⁸. In addition, the increased relative intensity of the peak at 44.9 ppm, ascribed to the methyl group from iodomethane (CH₃I), verified the occurrence of the quaternization reaction between the pyridine moiety on POP-*p*N(Me)₂Py and CH₃I. To provide additional proof, we employed X-ray photoelectron spectroscopy (XPS). The appearance of strong signals of iodine species at 629.3 and 617.8 eV for I3d_{5/2} and I3d_{7/2}, respectively, confirmed the success of this transformation (Supplementary Fig. 4). To quantify the degree of quaternization, we evaluated the content of iodine species in PQA-*p*N(Me)₂Py-I by elemental analysis. The results showed that the weight percentage of iodine species in PQA-*p*N(Me)₂Py-I was 38.3 wt% (Supplementary Table 1), which means about 95% of the pyridine moieties were involved in the quaternization reaction, revealing the high throughput of this reaction. The details of the pore properties of the resultant materials were investigated by N₂ sorption isotherms collected at 77 K. It is shown that both samples exhibit type-I plus type-IV sorption curves, suggesting the retention of the pore structure (Supplementary Fig. 5). A steep step in the curve at relative pressure (*P*/*P*₀) less than 0.01 is due to the filling of micropores, whereas a hysteresis loop at *P*/*P*₀ in the range of 0.45–0.95 is mainly from the contribution of the sample mesoporosity, which was also verified by the pore size distribution⁴⁹. The calculated specific surface areas were 535 and 223 m²g⁻¹ for POP-*p*N(Me)₂Py and PQA-*p*N(Me)₂Py-I, respectively. The decreased surface area can be reasonably attributed to the increased mass after the functionality addition. The details of the characterization

of POP-Py and POP-*p*N(Me)₂Py, as well as their corresponding quaternization products are provided in the Supplementary Information (Supplementary Figs. 6–13).

Sorption isotherms. The full availability of ion exchange sites within the pores of these materials is indicated by a complete anion-exchange process between I[−] and Cl[−], which was verified by TEM-EDS mapping and XPS analyses (Supplementary Figs. 14–17). This feature spurred their exploration for radionuclide polluted water treatment. Sorption experiments were first performed to evaluate the working capacities of these materials. Due to the limited availability and the rarity of the purified isotope ⁹⁹Tc, combined with its highly radioactive nature, perchrenate (ReO₄[−]) was first used as a nonradioactive surrogate for pertechnetate (⁹⁹TcO₄[−]) given their similarities in both magnitude and trend between the solubilities⁵⁰. The amounts of rhenium species enriched by these materials as a function of its concentration in the supernatant at the equilibrium state were determined by varying the initial concentrations from 25 to 800 ppm with a material-to-solution ratio of 0.5 mg mL^{−1}. An overnight reaction time was used to ensure that the ion exchange reached equilibrium. Results indicate that the equilibrium adsorption data of ReO₄[−] appeared to follow the Langmuir isotherm model (Fig. 2a); sorption increases rapidly at low ReO₄[−] concentrations and slows appreciably as the sorption capacity of the adsorbent is approached, yielding high correlation coefficients (R² > 0.99). Exchange capacities up to 936, 806, and 1127 mg of ReO₄[−] per gram of polymer were observed for PQA-Py-Cl, PQA-*p*NH₂Py-Cl, and PQA-*p*N(Me)₂Py-Cl, respectively, almost 20 times that observed for the unmodified counterparts (POP-Py, POP-*p*NH₂Py, and POP-*p*N(Me)₂Py), affording 53, 46, and 37 mg g^{−1}, respectively. Given the greatly enhanced performances after quaternization, we establish that the high density of the ion exchange sites on the polymer backbone is the fundamental contributor to their high working capacities and the mechanism for uptake of ReO₄[−] is thus believed to be predominantly ion exchange.

The high extraction capacities for these materials prompted us to evaluate their ion exchange kinetics, which were determined from distilled water samples spiked with 50 ppm of rhenium in the form of ReO₄[−]. Remarkably, when the solutions were treated with these materials at a phase ratio of 25000 mL g^{−1}, extremely rapid ion exchange and high uptake were recognized. All three materials reached their equilibrium exchange capacities within 60 min and in particular, 95.3% removal was achieved after 5 min for PQA-*p*N(Me)₂Py-Cl (Fig. 2b). This is in stark contrast to the lengthy contact times required for many sorbent materials, which

routinely range from several hours to as much as several days⁵¹. The fast kinetics should be an advantage for the continuous treatment of relatively large volumes of slightly contaminated water. We surmise that the impressive uptake capacity along with the fast removal rate is due to the high density of ion-exchange sites and intrinsic porosities allowing for rapid diffusion of ReO₄[−] throughout the materials. Notably, in addition to rapid saturation, PQA-*p*N(Me)₂Py-Cl also possessed a higher capacity, yielding an equilibrium value of 997 mg g^{−1}, in comparison with 849 and 642 mg g^{−1} afforded by PQA-Py-Cl and PQA-*p*NH₂Py-Cl, respectively, positioning PQA-*p*N(Me)₂Py-Cl as the material with the highest ReO₄[−] uptake among all adsorbents reported so far (Fig. 2b and Supplementary Table 2). Intriguingly, the increase in gravimetric capacity in going from PQA-*p*N(Me)₂Py-Cl to PQA-Py-Cl and PQA-*p*NH₂Py-Cl is opposite to what would be expected from the density of ion-exchange sites. For instance, on the basis of elemental analysis, it was found to have a Cl[−] species content of 10.3, 11.1, and 12.5 wt%, for PQA-*p*N(Me)₂Py-Cl, PQA-Py-Cl, and PQA-*p*NH₂Py-Cl, respectively (Supplementary Table 3). We therefore attribute this anomalous increase in ReO₄[−] uptake capacity for PQA-*p*N(Me)₂Py-Cl to the higher electrostatic ion-pairing attraction energies between the cationic polymer backbone of PQA-*p*N(Me)₂Py-Cl and ReO₄[−] ions. To rationalize this assumption, we measured the distribution coefficient values (*K_d*, for definition, see the Experimental Section) of these materials toward ReO₄[−]. Under the conditions of 10 ppm rhenium with a V/m of 1000 mL g^{−1}, the *K_d* values were calculated and found to equal 1.13 × 10⁶ (8.82 ppb), 5.44 × 10⁵ (18.35 ppb), and 1.00 × 10⁷ (1.00 ppb) for PQA-Py-Cl, PQA-*p*NH₂Py-Cl, and PQA-*p*N(Me)₂Py-Cl, respectively (number given in parentheses is the residual rhenium concentration), with PQA-*p*N(Me)₂Py-Cl showing almost more than an order of magnitude improvement in performance over the other two, indicative of its stronger affinity toward ReO₄[−] and thereby facilitating the ion exchange between Cl[−] and ReO₄[−].

Next, we assessed selectivity over common anions. The material's ability to competitively maintain efficiencies and rapid extraction rates at sub ppm levels, more typical of exposure cases, is one of the most important factors when evaluating a material for water treatment applications. Given the high environmental mobility, any accidental leaching of TcO₄[−] poses a real threat to groundwater contamination and aquatic life forms. As such, to access the ion-exchange properties associated with these materials, treatability studies were carried out using groundwater spiked with 1000 ppb of rhenium to simulate the contaminated water from on-site and off-site wells. PQA-*p*N(Me)₂Py-Cl was shown to remove >99.8% of ReO₄[−] from the groundwater, bringing rhenium concentrations to 1.2 ppb, implying that the

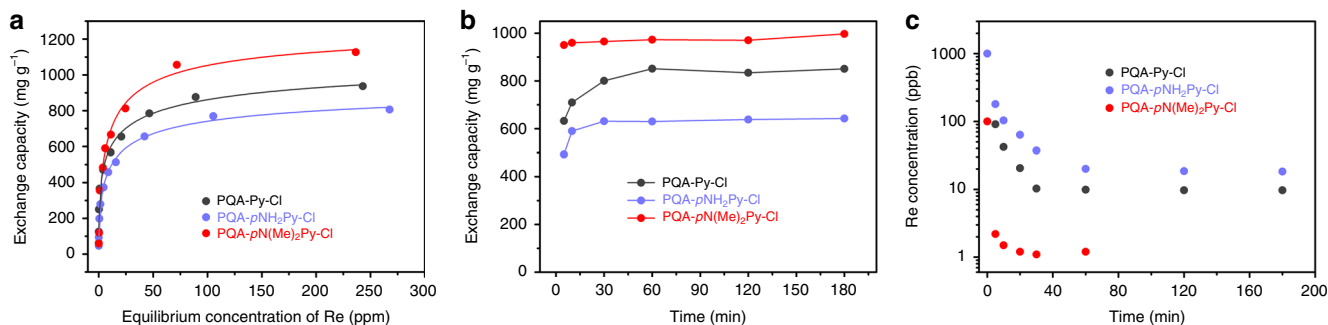


Fig. 2 ReO₄[−] adsorption isotherms and kinetics investigations. **a** ReO₄[−] sorption isotherms for various adsorbents. The lines are fit with the Langmuir model; all the fits have R² values higher than 0.99. **b** The kinetics of ReO₄[−] adsorption from aqueous solution with an initial concentration of 50 ppm, at a phase ratio (V/m) of 25000 mL g^{−1}. **c** ReO₄[−] removal kinetics with an initial concentration of 1000 ppb at a V/m ratio of 5000 mL g^{−1}. Source data are provided as a Source Data file

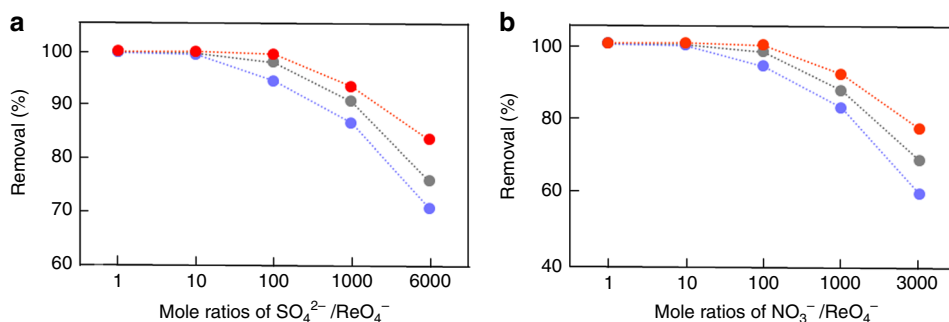


Fig. 3 Selectivity evaluation. Effect of competing (a) SO_4^{2-} and (b) NO_3^- anions on the anion-exchange of ReO_4^- by (gray) PQA-Py-Cl, (blue) PQA- $p\text{NH}_2\text{Py-Cl}$, and (red) PQA- $p\text{N}(\text{Me})_2\text{Py-Cl}$ (lines are guidelines for the eyes). Source data are provided as a Source Data file

interferences commonly found in surface waters have a minimal effect on its performance. It is worth mentioning that the residual rhenium concentrations treated by PQA- $p\text{N}(\text{Me})_2\text{Py-Cl}$ are 8 and 15 times lower than that of PQA-Py-Cl and PQA- $p\text{NH}_2\text{Py-Cl}$, respectively (Fig. 2c). In addition to the impressive removal efficiency, it is outstanding from the viewpoint of kinetic efficiency, reaching the equilibrium exchange capacity within 20 min and over 99.7% of the rhenium species removed within 5 min. These results highlight the vast potential of PQA- $p\text{N}(\text{Me})_2\text{Py-Cl}$ in accomplishing radionuclide removal from groundwater.

Encouraged by the results above, we then evaluated wastewater samples. Compared to surface water samples, wastewater is often comprised of fewer competing ions but significantly higher concentrations. Given this, to evaluate the sorption selectivity of ReO_4^- against the major anions NO_3^- or SO_4^{2-} , we performed binary exchange reactions by varying the equivalent ionic fractions of these anions in reactant solutions. A plot of the removal efficiencies of ReO_4^- against mole fractions of NO_3^- or SO_4^{2-} to ReO_4^- clearly indicated that PQA- $p\text{N}(\text{Me})_2\text{Py-Cl}$ showed a remarkably high tolerance to ReO_4^- sorption ability in the presence of SO_4^{2-} and NO_3^- competition with very high removal efficiencies and excellent $K_d(\text{Re})$ values (Fig. 3). Specifically, at $\text{SO}_4^{2-}/\text{NO}_3^-$: ReO_4^- molar ratios of 1 to 100, >99.9% of ReO_4^- ions were sequestered with $K_d(\text{Re})$ values in the range of 1.5×10^5 – 6.6×10^6 mL g^{-1} . It is interesting that even with a tremendous excess of Na_2SO_4 (SO_4^{2-} : ReO_4^- molar ratio at 6000), PQA- $p\text{N}(\text{Me})_2\text{Py-Cl}$ still retained a very good ReO_4^- removal efficiency (83.4%) and high $K_d(\text{Re})$ value (5034 mL g^{-1}), indicative of an exceptional selectivity of PQA- $p\text{N}(\text{Me})_2\text{Py-Cl}$ for ReO_4^- against SO_4^{2-} . This feature makes it an extremely attractive candidate to selectively remove $\text{ReO}_4^-/\text{TcO}_4^-$ from waste solutions with high ionic strengths. By contrast, under identical conditions, PQA-Py-Cl and PQA- $p\text{NH}_2\text{Py-Cl}$ afforded ReO_4^- removal efficiencies of 75.7% and 70.6%, with corresponding $K_d(\text{Re})$ values of 3123 and 2402 mL g^{-1} , respectively, inferior to those for PQA- $p\text{N}(\text{Me})_2\text{Py-Cl}$ (Supplementary Fig. 19).

Under all conditions tested, the preference of these pyridinium-based sorbents towards ReO_4^- complexation follows the same order: PQA- $p\text{N}(\text{Me})_2\text{Py-Cl}$ > PQA-Py-Cl > PQA- $p\text{NH}_2\text{Py-Cl}$. This trend may not be pinpointed to a single property change of the adsorbents but rather as a consequence of a complex interplay of several factors. For example, an increase in surface area may play a key role in the uptake capacity by providing a greater number of exposed exchangeable sites. However, in the present case, only a very weak correlation with the surface area of these materials could be established, thus suggesting that surface area is not the central factor determining the sorption performance; rather, the interaction strength between binding sites and guest species is a more important factor for determining guest uptake. To understand the lack of

dependence on the materials' textural parameters, we investigated the distribution of ReO_4^- in solid samples. Elemental distribution mapping was performed by SEM. We found homogeneously and densely distributed rhenium species throughout each sample (Supplementary Fig. 20). To examine the binding behavior of ReO_4^- in these adsorbents, XPS and IR spectroscopy were carried out. Comparison of $\text{Re}4f$ signals in the reacted samples (Re@PQA-Py-Cl, Re@PQA- $p\text{NH}_2\text{Py-Cl}$, and Re@PQA- $p\text{N}(\text{Me})_2\text{Py-Cl}$), Re@PQA- $p\text{NH}_2\text{Py-Cl}$ and Re@PQA- $p\text{N}(\text{Me})_2\text{Py-Cl}$ displayed very similar binding energies, giving $\text{Re}4f_{7/2}$ signals at 45.1 and 45.0 eV, respectively (Supplementary Fig. 21), which are lower than those in Re@PQA-Py-Cl (45.6 eV) and KReO_4 (46.1 eV). This presumably arises from the electron donating groups present in PQA- $p\text{NH}_2\text{Py-Cl}$ and PQA- $p\text{N}(\text{Me})_2\text{Py-Cl}$, which weakens the partial positive charge on the cations and thereby that on the rhenium species. These observations were further corroborated by the IR spectra (Supplementary Fig. 22), a slight red-shift of the ReO_4^- antisymmetric vibration was detected in Re@PQA- $p\text{NH}_2\text{Py-Cl}$ and Re@PQA- $p\text{N}(\text{Me})_2\text{Py-Cl}$ (893.8 cm^{-1}) compared to that in Re@PQA-Py-Cl (901.6 cm^{-1}) and KReO_4 samples (906.8 cm^{-1}). Regarding electronic factors, the introduction of electron donating groups facilitates the formation of kinetically labile complexes, which allows for rapid guest exchange. However, the relevant explanations cannot correlate with the observed trend, wherein the introduction of the amino group gave adverse results, with the lowest performance of the three materials. To explain this, we reasoned that, different from the dimethylamino group, the amino group acts both as a hydrogen bond donor and a hydrogen bond acceptor. Anions, such as Cl^- , are inclined to interact with it via hydrogen bonding, thereby compromising the ion-exchange capability for ReO_4^- ions. Such an interaction between the amino group and the Cl^- ion is expected considering the successful Cl^- extraction solely on an amine-based neutral anion receptor²⁷.

Density functional theory calculation studies. We carried out quantum density functional theory (DFT) computations to understand the chemical basis of the binding selectivities toward $\text{ReO}_4^-/\text{TcO}_4^-$. Calculations on the truncated fragments shown in Fig. 4 were performed using M06 exchange and correlation functions with fine grid spacing as implemented in NWChem. A 6-311++G(2d,2p) basis was used for all atoms except technetium, which was treated with the def2-tzvp basis and associated empirical core potential. This combination of functional and basis set was shown to reproduce experimental geometries of TcO_4^- ^{52,53}, providing more confidence in the results than could have been obtained with calculations on ReO_4^- . Full details of the quantum mechanical calculation are provided in the Supplementary Information.

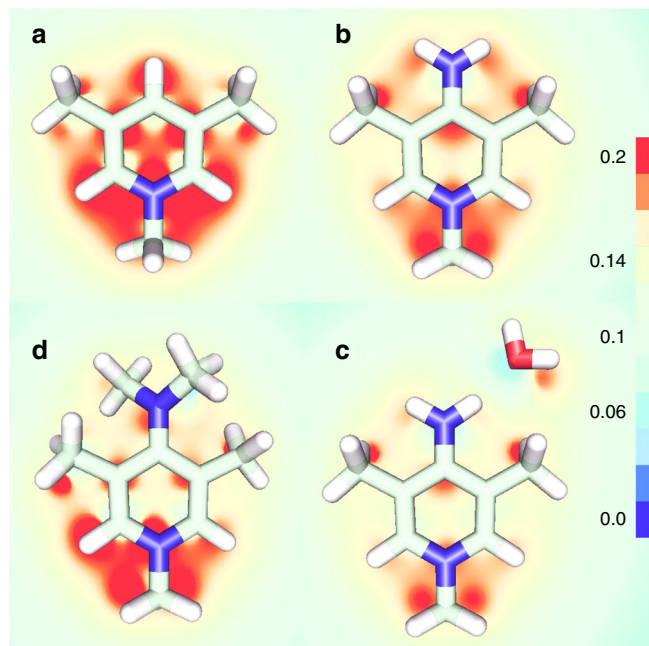


Fig. 4 Electrostatic potential surface. Distribution of the charge density around the aromatic ring is shown by a plot of the electrostatic potential surface just below the molecule. The most favorable binding geometry for a triangular face of an anion has opposite orientations between the cationic building blocks of **a** PQA-Py-Cl, **b**, **c** PQA-*p*NH₂Py-Cl, and **d** PQA-*p*N(Me)₂Py-Cl. Methyl groups have been introduced to take the electrostatic effects of the polymer chain into account. Comparison of **b** and **c** shows some negative charge is donated to the ring system during formation of a hydrogen bond

In all molecules, the pyridinium nitrogen forms a center of positive potential. Concentration of the positive charges at meta-positions would suggest that the triangular faces of NO₃⁻, HSO₄⁻, and TcO₄⁻ should orient directly overtop (Supplementary Fig. 23). Instead, the minimum energy geometries of a show that two of the anion oxygens seek to overlap with the lobes of positive potential on either side of the ring nitrogen closer to its attached methyl. These differences in geometry are significant, since all geometry optimizations started from anion positions containing an oxygen pointing toward the ring nitrogen. For **d**, the tertiary amine also has a large positive partial charge, and pulls anion oxygens toward itself. The resulting competition between these sites results in the smaller nitrate and sulfate anions stretching one oxygen toward each site, and not effectively using their third binding oxygen. In contrast, the longer bond length of TcO₄⁻ allows it to simultaneously occupy positions next to the dimethylamino group and close to the ring nitrogen. This explains the opposite binding orientation to what would be expected based on placing oxygens over both meta- sites. **b** is interesting and in its place, we see a strong positive charge at the para- location with nearly zero charges meta- to the ring nitrogen. Structure **c** was included to understand the effect of electron donation to the ring system due to a hydrogen bonding of water to the side-chain amine. It can be seen that the overall potential of the binding site decreases slightly, which will result in less favorable anion binding.

Binding free energies were computed for Cl⁻, TcO₄⁻, NO₃⁻, and HSO₄⁻ to all four structures in Fig. 4 using the quasi-chemical method (see details in Computational Methods Section and Supplementary Table 4 and Fig. 23). The anion HSO₄⁻ was used in place of SO₄²⁻ because the computational results are

more reliable when comparing ions of equal valence. The difference in binding free energies between HSO₄⁻ and SO₄²⁻ is the same as the difference between the pK_as of HSO₄⁻ in bulk solution compared to HSO₄⁻ bound to the polymer.

A large portion of the binding free energies is due to solvation effects. These increase polymer binding affinity of the larger (less hydrophilic) TcO₄⁻ over the smaller Cl⁻ and NO₃⁻. Although our solvation free energy calculations were carried out for liquid water, the polymer environment is expected to be slightly more hydrophobic. This will give TcO₄⁻ and additional boost relative to other ions that is not reflected in our final calculated selectivities. Entropic effects also contribute additional uncertainty to the calculations because it is difficult to predict the change in volume or rigidity of the surrounding polymer environment upon ion binding. Because of this, our free energy computations include only ligand translational and rotational entropy contributions (treating both binding partners as rigid bodies). Relative to Cl⁻ (which has no rotational entropy), the entropy contributions decrease the overall affinity for all ions by 2.5–6 kcalmol⁻¹ (Supplementary Table 4).

The chemical portion of the binding free energies is provided by energy differences in minimum energy configurations. The energy difference itself favors binding of NO₃⁻ and HSO₄⁻ over TcO₄⁻ by 7, 5, and 4 kcalmol⁻¹ for **a**, **b**, and **d**, respectively. This is not surprising, given that partial charges on NO₃⁻ are most negative, followed by HSO₄⁻ over TcO₄⁻ in that order. When energetic and free energy differences are added together, Cl⁻ is still the most favored binding partner in gas phase. However, the relatively hydrophobic environment of the polymer combined with the stronger affinity of water for Cl⁻ results in the opposite trend of binding free energies in solution. Just as seen in experiments, the final order of ion exchange affinity in solution is TcO₄⁻ > HSO₄⁻ > NO₃⁻ > Cl⁻ for all polymers. **d** has the strongest relative affinity for TcO₄⁻, at -6.1 kcal mol⁻¹ relative to Cl⁻, while its affinity for HSO₄⁻ is -3.9 and for NO₃⁻ is -3.8 kcalmol⁻¹, which is in accordance with our experiment results (Supplementary Table 4).

Stability test. Considering the superior performance of PQA-*p*N(Me)₂Py-Cl to extract ReO₄⁻ with good affinity and selectivity in the aforementioned situations, it was therefore the sample of choice for more detailed studies. The ability to regenerate and recycle the material would afford great advantages in reducing the overall cost and hence facilitating practical applications. To this end, the possibility of regeneration and reusing of PQA-*p*N(Me)₂Py-Cl were evaluated. Significantly, the ion exchange processes were fully reversible as reflected by the fact that the loaded ReO₄⁻ ions can be washed off by saturated NaCl aqueous solutions with maintained ion-exchange capacity for at least three cycles, affording 990, 1003, and 987 mg g⁻¹, respectively (Fig. 5a). These results suggest the adequate chemical and structural stability of PQA-*p*N(Me)₂Py-Cl, which was further established by the following experiments. The ReO₄⁻ uptake capacities and the pore structure of PQA-*p*N(Me)₂Py-Cl remained almost unchanged after being soaked in 12 M HCl or 2 M NaOH in saturated NaCl aqueous solution for one week (Fig. 5b and Supplementary Fig. 24). More impressively, PQA-*p*N(Me)₂Py-Cl was able to maintain its performance in extraction of ReO₄⁻ from 3 M HNO₃ solution for more than three times with approximately 70% of ReO₄⁻ from the HNO₃ solution containing 1.6 mM of ReO₄⁻ (NO₃⁻: ReO₄⁻ molar ratio = 1875) at a phase ratio of 50 mLg⁻¹ after a single treatment (Fig. 5c). Notably, a removal efficiency of 97% can be reached at a phase ratio of 20 mLg⁻¹ (a number that is nearly half that used for the chromatographic column application, 11 mLg⁻¹). These features clearly represent a priority in

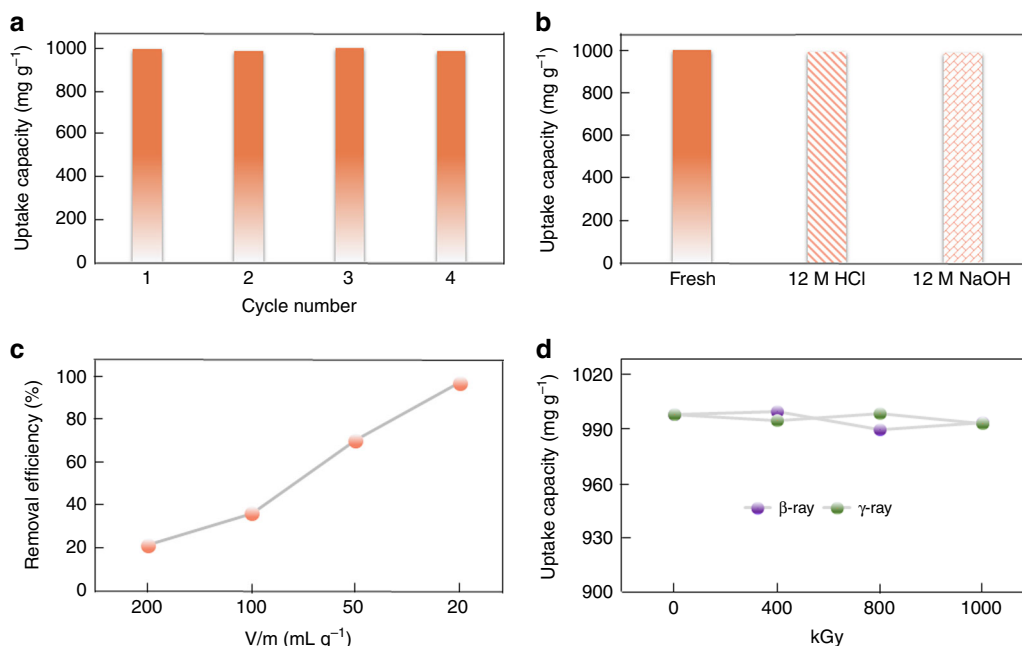


Fig. 5 Stability evaluation. **a** Reversibility of PQA-*p*N(Me)₂Py-Cl for removing ReO₄⁻. **b** ReO₄⁻ uptake capacities of PQA-*p*N(Me)₂Py-Cl after being soaked in 12 M HCl or 2 M NaOH in saturated NaCl aqueous solution for one week. **c** Removal of ReO₄⁻ by PQA-*p*N(Me)₂Py-Cl as a function of phase ratio (V/m) in 3 M HNO₃ aqueous solution. **d** Sorption capacities of ReO₄⁻ by PQA-*p*N(Me)₂Py-Cl after being irradiated with varied doses of β-rays or γ-rays. Source data are provided as a Source Data file

uptake for ReO₄⁻/TcO₄⁻ over NO₃⁻, thereby showing its potential for removing TcO₄⁻ from reprocessed used fuel prior to the plutonium uranium redox extraction (PUREX) process.

Given that the above studies were done with non-radioactive elements, how radiation interacts with the materials was not taken into account⁵⁴. Therefore, to rationalize results obtained from simulants, external radiation sources were exerted. Very impressively, PQA-*p*N(Me)₂Py-Cl exhibits outstanding resistance toward high-energy ionizing radiation of both β- and γ-rays, indicative by no noticeable change in the IR spectra, morphology, surface areas, as well as the sorption performance measurements on the irradiated samples in relation to the pristine material, thereby providing a substantial prerequisite for application in used nuclear fuel reprocessing and waste management (Supplementary Figs. 25–27). Remarkably, even after irradiation with extremely large doses of 1000 kGy of β- or γ-rays, the sorption rate and capacity for ReO₄⁻ by PQA-*p*N(Me)₂Py-Cl remained unaffected (Fig. 5d). PQA-*p*N(Me)₂Py-Cl combines the attributes of high capacity, reusability, and resistance against radiation, providing an extended lifetime that is sought after for long-term use in nuclear waste water treatment applications.

Removal from simulated nuclear wastes. To further validate the results, TcO₄⁻ uptake experiments were performed by contacting PQA-*p*N(Me)₂Py-Cl with an aqueous solution of TcO₄⁻. The concentration of TcO₄⁻ was monitored by liquid scintillation counting measurements. As shown in Supplementary Fig. 28, PQA-*p*N(Me)₂Py-Cl was kinetically favored, 99% of TcO₄⁻ could be removed within 5 min

With this success, it promoted us to investigate performance of PQA-*p*N(Me)₂Py-Cl in legacy nuclear waste. Previous estimates of Hanford tank waste inventories indicated that the amount of technetium in the waste needed to be reduced substantially to prepare immobilized low activity waste (ILAW) glass that meets performance assessment requirements. To investigate the removal of TcO₄⁻ for this application, we prepared a simulated Hanford

LAW melter recycle stream, where the amounts of NO₃⁻, NO₂⁻, and Cl⁻ are more than 300 times that of TcO₄⁻, as listed in Supplementary Table 5, resulting in an enormous challenge to selectively remove TcO₄⁻. Following similar experimental conditions as the established procedures (see details in the Supplementary Information), PQA-*p*N(Me)₂Py-Cl was found to remove about 95% of available TcO₄⁻ from the waste at a phase ratio of 200 mL g⁻¹, placing it within striking distance of the all-time TcO₄⁻ removal record (Supplementary Table 6). To further extend the potential application of PQA-*p*N(Me)₂Py-Cl in nuclear waste remediation, we tested its capability for the decontamination of TcO₄⁻ in Savannah River Sites. It was shown to be effective for the segregation of TcO₄⁻ from simplified simulants, a strong basic TcO₄⁻ solution with the strength of other anions over 70 000 times that of TcO₄⁻ (Supplementary Table 7). Approximately 80% of available TcO₄⁻ was extracted from the waste at a phase ratio of 100 mL g⁻¹, which to date, we have found no materials in the literature with comparable selectivity under similar conditions. Although applicable to pertechnetate-containing waste streams in general, these two examples discussed here were directed at two specific potential applications at the U.S. Department of Energy's legacy site: i) the removal of dilute pertechnetate from near-neutral solutions, typical of the eluent streams from pretreated Hanford tank wastes, and ii) the direct removal of pertechnetate from highly alkaline solutions, typical of those found in Savannah River Sites.

Discussion

In summary, based on the results above, we can now formulate clear design rules to achieve ideal ReO₄⁻/TcO₄⁻ scavengers with optimal uptake capacity and selectivity. The presented case shows that a subtle interplay between various functions in the adsorbent—in this case incorporation of a distinct functionality on a cation moiety—would be used to obtain an optimally performing adsorbent. Given the fact that ion exchange often follows a similar

mechanism, we expect that the trends discovered here will also be of high relevance for many other sequestration processes, such as coordinative binding. We conceptually showed the potential for tuning binding sites in selective capture to a greater degree of complexity. Given the demonstrated easy tunability, regeneration, and separation combined with radioactive resistance, long-term stability, and high performance in application relevant conditions, these new materials presented here could become highly influential for nuclear wastewater treatment technologies, particularly in the event of an impending water crisis. Also, potential cost savings and schedule acceleration could be anticipated based on consequent improvements in vitrification processing, reduction in waste form volumes, and higher waste-package performance.

Methods

Materials and measurements. Commercially available reagents were purchased in high purity and used without purification. The purity and structure of the compounds synthesized in this manuscript were determined by NMR technique (Supplementary Fig. 29). Nitrogen sorption isotherms at the temperature of liquid nitrogen were measured using Micromeritics ASAP 2020M and Tristar system. ^1H NMR spectra were recorded on a Bruker Avance-400 (400 MHz) spectrometer. Chemical shifts are expressed in ppm downfield from TMS at $\delta = 0$ ppm, and J values are given in Hz. ^{13}C (100.5 MHz) cross-polarization magic-angle spinning (CP-MAS) NMR experiments were recorded on a Varian infinity plus 400 spectrometer equipped with a magic-angle spin probe in a 4-mm ZrO_2 rotor. The samples were outgassed for 1000 min at 80 °C before the measurements. Scanning electron microscopy (SEM) and energy dispersive X-ray spectroscopy (EDX) mapping were performed on a Hitachi SU 8000. Transmission electron microscope (TEM) image was performed using a Hitachi HT-7700 or JEM-2100F field emission electron microscope (JEOL, Japan) with an acceleration voltage of 110 kV. High-angle-annular-dark-field (HAADF) scanning, STEM imaging, and energy dispersive X-ray spectroscopy (EDX) mapping were carried out by Titan ChemiSTEM operated at 200 kV. XPS spectra were performed on a Thermo ESCALAB 250 with Al K α irradiation at $\theta = 90^\circ$ for X-ray sources, and the binding energies were calibrated using the C1s peak at 284.9 eV. IR spectra were recorded on a Nicolet Impact 410 FTIR spectrometer. The concentrations of TcO_4^- in solution were measured using a UV-vis spectrometer (Varian Cary 6000i) by monitoring the characteristic absorption peak at 290 nm and the activity of $^{99}\text{TcO}_4^-$ was also analyzed by a liquid scintillation counting (LSC) system (Perkin Elmer Quantulus 1220). ICP-OES was performed on a Perkin-Elmer Elan DRC II Quadrupole. ICP-MS was performed on a Perkin-Elmer Elan DRC II Quadrupole Inductively Coupled Plasma Mass Spectrometer. Elemental analyses were performed via flask combustion followed by ion chromatography.

Data availability

The authors declare that all the data supporting the findings of this study are available within the article (and Supplementary Information files), or available from the corresponding author on reasonable request. The source data underlying Figs. 2, 3, and 5 are provided as a Source Data file.

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Author contributions

Q.S. and S.M. conceived and designed the research. Q.S. and B.A. performed the synthesis. Q.S., L.Z., P.K.T., and B.A. carried out the adsorption tests. C.X., J.C., and S.W. conducted the radiation stability tests. D. R. contributed to DFT calculation. All authors participated in drafting the paper, and gave approval to the final version of the manuscript.

Additional information

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