

Combining Source Rock Kinetics and Vitrinite Reflectance in Source Rock Evaluation of the Bakken Formation, Williston Basin, USA

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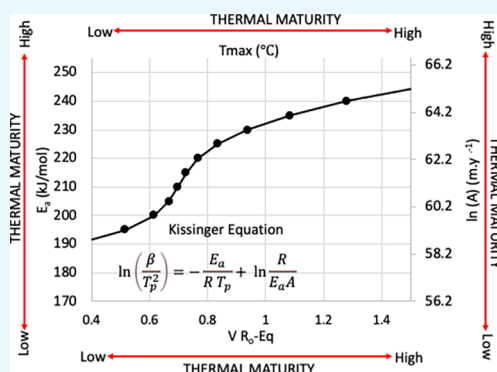
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ABSTRACT: The elements of Bakken Petroleum System consist of two source rocks with high underlying burial depths for significant hydrocarbon generation. However, this deep hydrocarbon generation process is dependent on its kinetic properties, thermal maturity, and geochemical properties. The statistical compensation effect is a complicating factor in the kinetic analyses of the Bakken Formation. In this study, we experimentally determined the kinetics of the Bakken formation source beds, observed the presence of the residual compensation effect, and numerically established a correlation between the kinetic parameters, thermal maturity indices (T_{max}), and the vitrinite reflectance (VR_o) and bitumen reflectance (BR_o). First, we conducted source rock analysis to determine kinetic properties and the organic geochemical assays of reactive kerogen in the Bakken source beds. Finally, we incorporated previous established studies to generate numerical correlation for T_{max} in terms of VR_o and BR_o reflectance. Our kinetic results show evidence of the residual compensation effect in the Bakken Formation when samples are repeatedly analyzed. The simultaneous linear expression of the residual compensation effect and the regression analysis of the solutions to the Kissinger equation for heating rate, yielded a kinetic parameter solution that correlates with T_{max} . Furthermore, recalculated T_{max} values established a correlation between the kinetic parameters, T_{max} , VR_o , and BR_o . The application of state-of-the-art numerical correlations to measure subsurface kinetics, source rock richness, and burial-depth temperatures will enhance the accuracy of reservoir exploration and hydrocarbon production within the Bakken Formation.



INTRODUCTION

The Bakken Formation (Late Devonian to Early Mississippian) in the Williston Basin underlies parts of Montana, North Dakota, and the Canadian provinces of Saskatchewan and Manitoba (Figure 1). The Bakken Formation is subdivided into four members consisting of the Upper and Lower shale members, an intervening mixed siliciclastic and carbonate member (Figure 2). The fourth Pronghorn (or Bakken silt member) is a discontinuous unit that occasionally in places contains thin limestone as well as basal sandstone. The Bakken Formation lies on a regional unconformity with the underlying Three Forks Formation and is conformably overlain by the thick Lodgepole Limestone.

The upper and lower shale within the Bakken are the core source rocks of the Bakken Petroleum System. Currently, over 12-million barrels of oil are being produced daily from reservoirs in the Middle and Pronghorn members of the Bakken Formation and the Upper Three Forks Formation. Based on the horizontal drilling and hydrofracture stimulation technology available in 2006, the U.S. Geological Survey estimated that there are 4.2 billion barrels of technically recoverable oil within the Bakken Formation.¹ In 2014, an additional 3.73 billion barrels of technically recoverable Bakken

sourced oil were identified in the underlying Three Forks Formation.²

The most unique aspect of the Bakken Petroleum System is that it is the first regional-scale example of oil production from a Basin-Centered Petroleum System.³ To illustrate, the basic component of these systems is the presence of an oil generating source bed that is encased in porous, though poorly permeable reservoir rocks that have interfacial capillary pore pressures preventing the escape and free migration of the generated oil. These ideal features resulted in accumulations that are largely independent of conventional structural and stratigraphic controls. This leads to a petroleum system that is dictated by buoyancy and attendant density contrasts between oil and formation waters. Consequently, basin-centered petroleum systems have the capability of efficiently retaining expelled oil in reservoirs that are immediately adjacent to the

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Figure 1. Location of the study area (dark fill) within the Williston Basin (light fill).

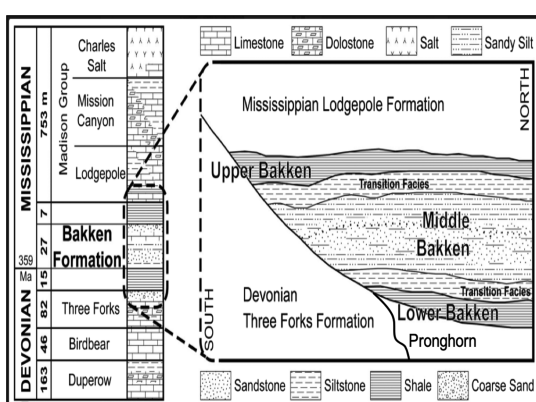


Figure 2. Generalized stratigraphic column for the Bakken petroleum system in the Williston Basin, Modified from Webster,²⁰ Kuhn et al.,²¹ and Johnson.²²

source beds. Therefore, understanding the oil generation process should be the key in defining where extractable oil is likely to be found.

The amount of Bakken exploration has immensely increased discoveries of reservoir zones within the Middle Bakken Member and underlying Three Forks. According to Dow;⁴ Schmoker and Hester;⁵ Webster;⁶ Meissner;⁷ and Price and LeFever,⁸ the estimated calculated basin-centered petroleum system for the Bakken source rocks may have expelled between 10 to 413 billion barrels of oil, charging both unconventional and conventional reservoirs. As Bakken reservoir zones are realized, an effort to understand the sub-basin petroleum systems requires modern techniques to evaluate the oil generation process and determine future production. The objective of this study is to experimentally determine the kinetics of the source beds within the Bakken Formation, in particular, in a sub-basin within the Williston Basin by demonstrating the equivalence between the following: kinetics, thermal maturity indices (T_{max}), and vitrinite reflectance (VR_o) (bitumen reflectance (BR_o)).

■ GEOLOGIC SETTING OF THE BAKKEN FORMATION

The Bakken Formation was deposited in the Williston Basin during the Late Devonian to Early Mississippian age. The Basin occupies a paleoposition at the center of a vast epicontinental sea, covering what is now the interior of western North America.^{9,10} During the Late Devonian in the Williston Basin, block fault movement along a basement structure accompanied by uplift along the Sweetgrass Arch established a restricted seaway connection to the western craton margin.^{11,12} At that time, uplift of the Transcontinental, Severn, and Wisconsin Arches redefined the eastern and northeastern margins of the basin. Structural deformation in the Devonian period of the Williston Basin was affected by tectonic forces arising from the Acadian orogeny. Furthermore, changes in the relative sea level (transgression and regression) influenced the depositional environment during sediment accommodation and accumulation.^{13–19} More importantly, the relative sea levels during the deposition of the Bakken Formation is an important aspect in determining the type of marine depositional environment that dominated the Williston Basin.

Organic material within source rocks consists of extremely complex macromolecules made largely of hydrogen, carbon structures, and a host of other minor components. The process of oil generation involves breaking bonds within these macromolecules to form mobile and soluble (in organic solvents) hydrocarbon fragments that together mix to form mobile crude oil and natural gas or immobile bitumen. Even though the processes and mechanisms of oil generation are exceedingly complex, there is general agreement that overall reaction rates are in agreement with the Arrhenius equation (eq 1).²³ Additionally, in this expression, time, temperature and the kinetic properties of the reacting kerogen are capable of approximating rates of natural oil generation and conversely kerogen degradation.^{24,25} Furthermore, Connan²⁶ described the Arrhenius equation as a theoretical expression of exponential temperature that defines the chemical reaction rate through the frequency factor, A , and activation energy, E .

Previous studies have used the Arrhenius equation to model the rate constants for oil generation.^{23,27–30} Additionally, these studies also show that high quality kinetic analysis is vital for

Table 1. Summary of Kinetic Analyses^a

well code	NDIC well number	E_{aa} (kJ/mol)	$\ln(A_a)$ -m.y	T_H	C	No.	E_{ac} (kJ/mol)	$\ln(A_c)$ -m.y	E_{ac1} (kJ/mol)	$\ln(A_{c1})$ -m.y
A	17,043	206.77	60.77	721.29	-157.64	7	204.42	60.38	213.08	61.82
B	16,160	227.48	63.20	741.61	-162.20	8	226.66	63.07	218.97	61.82
C	17,023	215.21	61.68	730.20	-159.27	4	215.15	61.68	216.03	61.82
D	16,532	214.93	61.81	727.92	-159.12	14	211.36	61.22	215.02	61.82
E	16,862	204.28	60.14	723.98	-157.70	1	209.18	60.95	214.40	61.82
F	21,668	219.33	61.32	751.19	-163.61	1	241.43	64.85	222.48	61.82
G	22,572	231.63	64.30	733.81	-160.64	1	216.99	61.90	216.52	61.82
H	17,434	203.95	59.71	731.51	-159.20	1	217.95	62.01	216.77	61.82
I	5088	216.89	61.59	736.98	-160.47	4	223.96	62.74	218.32	61.82
J	13,098	237.32	64.36	736.97	-157.01	14	237.31	64.36	221.77	61.82
K	8177	218.92	62.78	721.33	-157.59	1	204.71	60.41	213.16	61.82

^a E_{aa} and $\ln(A_a)$ are solutions to the Kissinger equation found by including all experiments for each well combined into a single analysis. Each analysis contains seven experiments using 2, 2, 5, 10, 20, 50, and 50 °C/min. Heating Rates. The harmonic mean of the peak reaction temperatures (T_H) for each set of analyses is used in eq 3 to “correct” E_{aa} and $\ln(A_a)$ to E_{ac} and $\ln(A_c)$ with eqs 5 and 7, respectively.

these models based on the need to extrapolate from rapid heating rates at high temperatures to slow heating rates in the laboratory setting, and imitate relatively low temperatures found in nature.³¹ This study is focused on applying the Arrhenius equation (eq 1) to the problem of thermal maturity and oil generation rates in the Bakken Formation

$$K = Ae^{-E_a/RT} \quad (1)$$

Where:

K = rate constant (m.y.⁻¹)

A = frequency factor (m.y.⁻¹)

E_a = activation energy (kJ/mol)

T = temperature (K)

R = gas constant (kJ/mol·K)

Kissinger³² provided an exact solution to the Arrhenius equation for first order reactions under constant rates of nonisothermal heating. His method equates the shift in peak reaction temperature (T_p) at different heating rates (β) to the activation energy and frequency resulting in the following linear expression:

$$\ln\left(\frac{\beta}{T_p^2}\right) = -\frac{E_a}{R} \frac{1}{T_p} + \ln\left(\frac{R}{E_a} A\right) \quad (2)$$

T_p = temperature corresponding to the maximum reaction rate (K).

β = heating rate (K/sec).

R = gas constant (kJ/mol·K).

Peak reaction temperatures found using different rates of constantly increasing temperatures when plotted as $\ln(\beta/T_p^2)$ against T_p^{-1} produce lines with a slope equal to the ratio between the activation energy and the gas constant. The intercept of this line ($\ln(R/E_a A)$) provides the corresponding value for the frequency factor.

Experimental errors in measuring T_p complicate the direct use of these variables in the Arrhenius equation, resulting in compensating errors in E_a and A . In general, kinetic parameters exhibit a strong linear relationship between E_a and the $\ln(A)$ (e.g.,^{28,30,33–37}). This relationship is caused by small errors in experimental temperatures^{34,38,39} that produce solutions for E_a and $\ln(A)$ that fall within an extremely elongated error ellipse. Barrie³⁸ suggested using the term statistical compensation effect for this behavior. At the temperatures used for source rock kinetics, the error ellipse enclosing the statistical compensation effect for some level of confidence is elongated,

almost to the point of being a line.³⁸ This permits with little error, replacement of the error ellipse by a line that coincides with its principal axis. This line describes the distribution of other solutions for all equivalent but error encumbered solutions to E_a and $\ln(A)$. Nielsen and Dahl,³⁴ Barrie,³⁸ and Nordeng³⁹ show that the slope of the principal axis of the error ellipse in the $E_a - \ln(A_a)$ plane is equivalent to the product of the harmonic mean (T_H) of the peak reaction temperatures (T_p) and the gas constant (R). The slope when combined with a given solution of E_a and $\ln(A_a)$ provides an expression (eq 3) for a line that contains other equivalent solutions with error as well as the “true” solution

$$E_{aa} = RT_H \ln A_a + C \quad (3)$$

E_{aa} = apparent activation energy

A_a = apparent A

This expression, however, cannot provide a unique, “true” solution for either E_a or A without first constraining one or both of these parameters.

■ STUDY AREA AND METHODS

Eleven wells were used in this study based on the availability of cores and temperature profile control. The wells are centered in and around an apparent depocenter that lies along the eastern margin of the north–south trending Nesson anticline in Mountrail County North Dakota (Table 1).

To estimate modern oil generations rates in the Bakken Formation and avoid poorly constrained variables, at a particular temperature, four parameters are required to use the Arrhenius equation: the kinetic properties of the kerogen, activation energy and frequency factor, together with the total reactive kerogen mass and temperature.

Kinetic Analysis. Values of activation energy (E_{aa}) and the corresponding frequency factor (A_a) were obtained by programmed pyrolysis using the University of North Dakota’s Source Rock Analyzer (Weatherford Labs). Each determination used seven heating rates (2, 2, 5, 10, 25, 50, 50 °C/min) that ran from 250 °C to 650 °C. During each experiment, the mass of evolved hydrocarbon vapor was measured with a flame ionization detector and recorded with time and temperature. Nonlinear interpolation of these data refined the peak generation temperature, T_p , to within 0.1 °C. Linear regression of the time–temperature data was used to validate and refine

the experimental heating rates. Linear regression of $\ln\left(\frac{\beta}{T_p^2}\right)$

against $\frac{1}{T_p}$ provides the slope and intercept terms that, from eq 2, yield the apparent activation energies (E_{aa}) and frequency factors (A_a) shown in Table 1.

VR_o and BR_o. VR_o measures the percentage of incident light reflected from the surface of vitrinite particles in a sedimentary rock often referred to as %R_o (percentage of light reflected by oil). Vitrinite reflectance is a major maturity parameter, because of its persistence throughout the maturation process at any stage in geological time. Moreover, vitrinite is a standard method that has recognizable features and is homogenous when viewed under an incident light microscope. When vitrinite has been absent in particular shale formations, the relationship between the pyrolysis T_{max} and vitrinite or BR_o has been used. Shale is unique and has varying reflectance in relationship with T_{max} . On the other hand, solid bitumen is not a kerogen component but exists as a secondary reaction product that is not present throughout the entire maturation process. For example, Thompson-Rizer⁴⁰ and Jacob⁴¹ show that solid bitumen is a product of generation from kerogen which moves into pore spaces within mineral grains.

Prior authors have proposed an equation relating vitrinite reflectance to T_{max} in the following shales: the Bakken Shale,⁴² the Barnett Shale,⁴³ Duvernay Formation,⁴⁴ and the Woodford Formation.⁴⁵ For example, in the study of Abarghani et al.⁴² (Bakken Shale), where vitrinite was absent, the reflectance from particles of bitumen was converted to equivalent Vitrinite Ro % using an equation proposed by Liu et al.⁴⁶ who originally applied this equation to the Coeval New Albany Shale. The results were compared to the Barnett shale in the United States and Devonian Duvernay shale in Canada, which indicates discrepancies between the Bakken vitrinite reflectance and T_{max} relationship. While a number of equations have been published for correlating BR_o and T_{max} ,^{46–50} no unified method has been established. As a result, Gentzis and Goodarzi,⁵¹ and Dembicki⁵² discuss in their prior research that these kinds of equations should be applied cautiously. In this study, we showed that VR_o and BR_o equations from Liu et al.⁴⁶ and Abarghani et al.,⁴² respectively, are directly related to the kinetic parameters (E_a and A) and T_{max} .

Mass of Reactive Kerogen. This calculation estimates the total mass of reactive kerogen in a prism with a cross-sectional area of 1 cm² that extends through the Upper and Lower Shale of Bakken Formation. This is done by analyzing the upper and lower source rocks for reactive kerogen mass per mass sample using the University of North Dakota's Source Rock Analyzer (SRA), a Rock-Eval equivalent (technique is described in detail by Peters⁵³) and converting this to a reactive mass per cm³ volume using bulk density logs (Table 2). The total mass of kerogen within the cm² prism is found by multiplying the mass per volume term by the combined thickness of both source beds (Table 2).

$$X \left(\frac{\text{mg HC}}{\text{cm}^2} \right) = S_2 \left(\frac{\text{mg HC}}{\text{g}} \right) \times \rho_B \left(\frac{\text{g}}{\text{cm}^3} \right) \times \text{Thickness (cm)} \quad (4)$$

X = mass of reactive kerogen (mg/cm²)
 S_2 = mass thermally active kerogen (mg HC/g)

ρ_B = bulk density (g/cm³).

The total mass of reactive kerogen was found using programmed pyrolysis using samples collected at one-foot

Table 2. The Thickness Column Is the Combined Thickness of the Upper and Lower Bakken Shale^a

well code	thickness (m)	bulk density		number of samples	kerogen mass (g/cm ²)
		average (g/cm ³)	variance		
A	12.5	2.12	0.009	19	263.52
B	18.0	2.25	0.004	107	183.90
C	14.9	2.16	0.003	96	253.80
D	15.4	2.19	0.015	47	375.34
E	12.5	2.20	0.007	36	322.81
F	14.0	2.30	0.004	88	54.33
G	11.9	2.15	0.003	76	228.63
H	12.8	2.14	0.005	92	219.87
J	23.5	2.25	0.004	23	71.36
K	24.0	2.24	0.008	21	76.00

^aThe average densities of the Bakken Shales are bulk density logs that are correlated to the sharp and distinct gamma ray excursions that mark the top and bottom of both shales. The kerogen mass is the product of the thickness, Average Density, and S_2 mass from Table 2. This mass represents the total kerogen mass of a 1 cm² prism that extends through both the Upper and Lower Shale.

intervals throughout the upper and lower source beds. Small (60 to 80 mg) samples were pyrolyzed in an inert (He) atmosphere at ambient pressures in an SRA. The heating schedule emulates the two-heating stage Rock Eval method that involves three minutes of isothermal heating at 300 °C followed by ramping the temperature from 300 to 650 °C at a constant rate of 25° C/min. Hydrocarbons released during the course of each experiment were measured with a flame ionization detector (FID).

The total hydrocarbon mass recorded during the initial isothermal phase is considered "free" hydrocarbons and defined as S_1 . The total mass of hydrocarbons released during the second nonisothermal phase is considered reactive kerogen with the mass recorded in Table 3 as S_2 . The temperature that corresponds to the maximum rate of hydrocarbon generation during this phase is recorded, after conversion to the established Rock Eval convention, as T_{max} . The difference between the two is that T_{max} is approximately 40 degrees lower than the recorded peak reaction temperature.

Density and Thickness. The measured mass of reactive kerogen per mass sample is converted into a volumetric term by multiplication with the bulk density of the rock. This was done using bulk density logs that were run through the source rock interval shortly after drilling or just prior to drilling of the horizontal lateral.

The bulk density and gamma ray logs used in this study are from LASer (LAS) files available through the North Dakota Industrial Commission. Data in these logs are typically tabulated at 0.5 ft. (15.24 cm) intervals. The logs were depth corrected to match the cores by correlating the sharp change in gamma ray and density-neutron porosity logs to the corresponding visible contacts present in the core between the Lodgepole Formation, middle Bakken member, and Three Forks Formation. The bulk density through both shale members for each well was reduced to a simple mean and variance (Table 2) for calculation purposes. The total thickness of both members was also taken from these log-core correlations.

Bakken Formation Temperature. The North Dakota Geological Survey has temperature logged 19 temporarily

Table 3. Summary of the Organic Richness and Quantity^a

well code	HI		TOC (wt %)		T_{\max} (°C)		S_2 (mg HC/g sample)		number of samples
	average	variance	average	variance	average	variance	average	variance	
A	622	3760.42	15.75	13.07	424.39	3.60	99.63	773.01	24
B	391	18147.50	11.59	8.66	441.18	5.32	45.43	365.50	47
C	533.768	3267.09	14.42	10.10	430.34	1.70	78.50	417.71	51
D	758.04	5360.07	14.72	13.74	433.68	4.37	75.74	755.08	71
E	804.43	23591.17	14.20	16.98	432.15	6.09	80.68	1606.81	51
F	146	325.10	11.43	3.97	449.21	7.97	16.82	16.40	43
G	566	3026.37	15.59	11.43	435.78	1.68	89.58	568.71	20
H	513.4706	3304.68	15.32	7.85	429.05	2.00	80.10	375.88	34
I	298.1429	3608.06	11.25	16.68	443.90	8.78	34.99	259.10	107

^aHI is the hydrogen index ($S_2/TOC \times 100$). TOC is the total organic carbon content in terms of weight percent and S_2 is the mass of hydrocarbons per mass of sample released during programmed pyrolysis between 300 and 650 °C at a heating rate of 25 °C/min. T_{\max} is a thermal maturity indicator that is approximately 39.5 °C lower than the oven temperature that coincides with the maximum release of hydrocarbons during programmed pyrolysis at a heating rate of 25 °C/min.

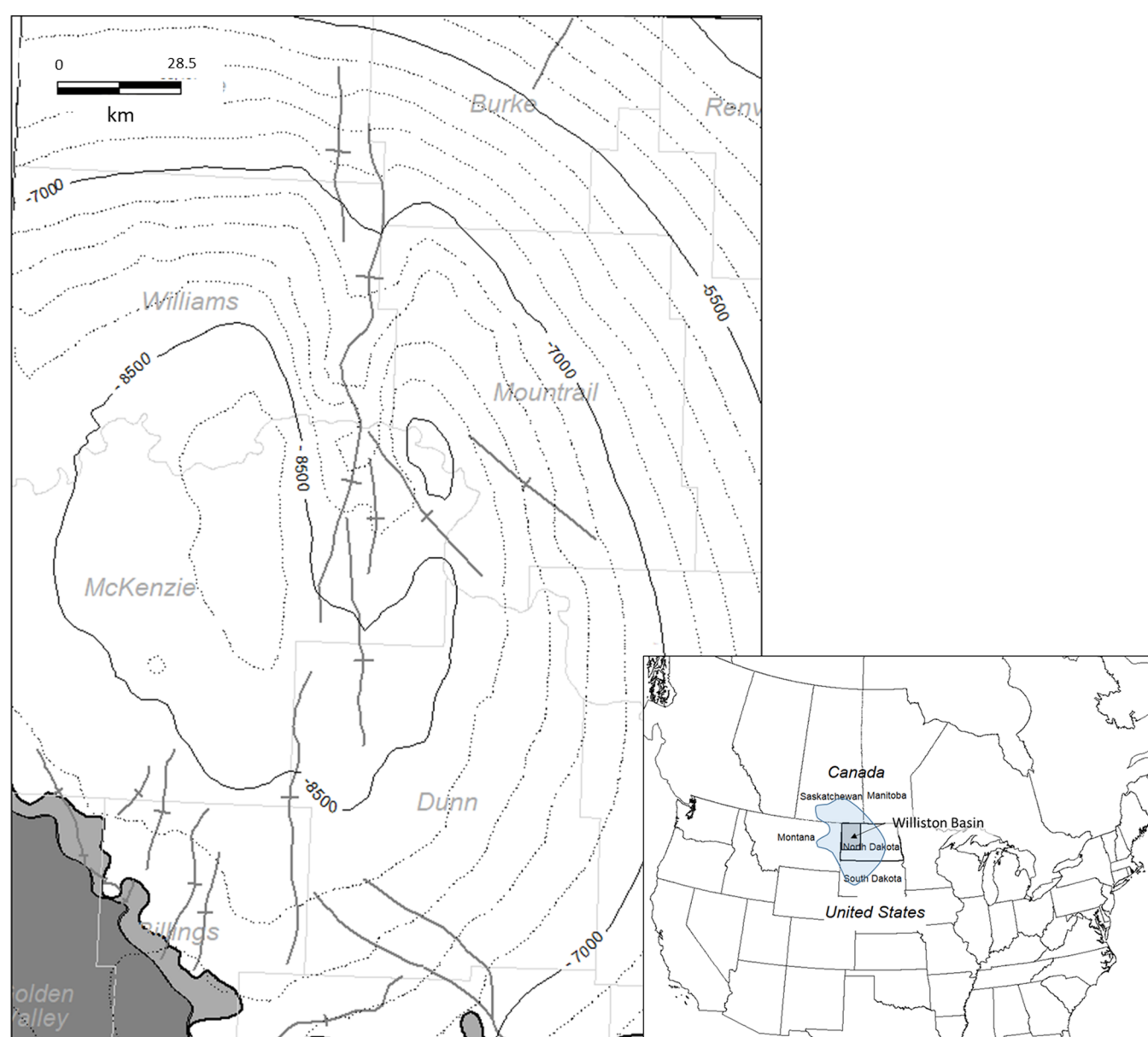


Figure 3. Index map of the study area situated near the center of the Williston Basin in North Dakota, USA. Contour lines represent subsea depths in feet with anticline structures approximated with the heavy gray lines.

Table 4. Estimated Temperature Values and the Calculated Reaction Rate Index of the Bakken Formation

well code	temperature	kinetics			kinetics 2		
		K c	rate c	my/cm	K c	rate c	my/cm
A	81	1.17E-04	0.0375	26.67	2.63E-05	0.0084	119.13
B	111	3.70E-04	0.0825	12.12	1.18E-03	0.2635	3.80
C	103	8.06E-04	0.2480	4.03	7.03E-04	0.2164	4.62
D	95	3.95E-04	0.1795	5.57	2.19E-04	0.0995	10.05
E	96	7.43E-04	0.2907	3.44	3.23E-04	0.1263	7.92
F	127	4.45E-04	0.0293	34.09	6.38E-03	0.4205	2.38
G	103	5.59E-04	0.1550	6.45	6.02E-04	0.1669	5.99
H	93	6.89E-05	0.0184	54.43	8.36E-05	0.0223	44.88

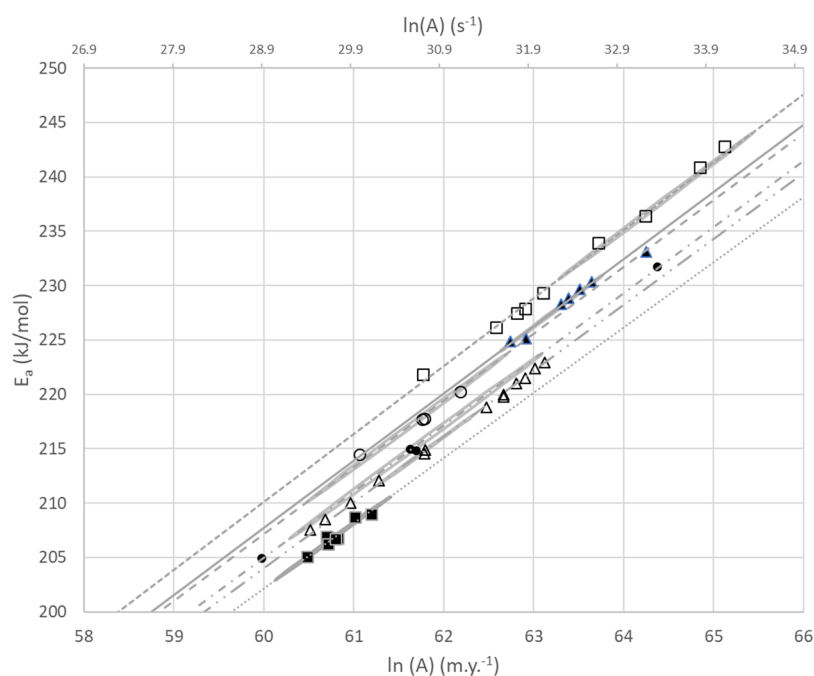


Figure 5. Diagram illustrating the statistical compensation effect present within individual wells and the corresponding 2σ error ellipse for each well where all analyses for a particular well are used to find a single solution for E_a and $\ln(A)$ with the Kissinger equation. Well A, open triangle; Well B, filled triangle; Well C, open circle; Well D, filled circle; Well J, open square; Well I, filled square.

Table 5. Linear Regression Variables from the Lines that Relate Specific Values of T_{\max} to E_a and $\ln(a)$ at the Point of Intersection with the Residual Compensation Effect Shown in Figure 6

T_{\max}	regression coefficients		kinetic parameters	
	slope	intercept	$\ln(A)$ -m.y	E_a (kJ/mol)
385	2.610170267	-145.762	55.84402	166.9629
415	2.373399229	-140.028	58.99878	193.0354
435	2.215835989	-136.223	61.47683	213.5152
455	2.058499472	-132.432	64.33404	237.1287
475	1.901389188	-128.654	67.66342	264.6443
495	1.744504651	-124.891	71.59111	297.1047

constant frequency factor beyond the point consistent with a residual compensation effect will result in errors. These errors arise in E_a and A for both less mature and more mature source rocks.

The residual compensation effect when simultaneously solved with the linear expression for the statistical compensation effect provides a unique solution for both effects (Eq 3). This allows reduction of the raw kinetic analyses to a common, though in part empirical basis. Solutions for E_a

and $\ln(A)$ at the intersection of the two compensation effects are shown in Table 4 and will be used to estimate the production rate index.

The regression analysis shown in Figure 6 provides the following empirical relationship (eq 5) between the activation energy $E_{a, \text{comp}}$ and the natural logarithm of the frequency factor $\ln(A_{\text{comp}})$ from a composite analysis using all available analyses from a single core.

$$E_{a, \text{comp}} = 8.2645 \ln(A_{\text{comp}}) - 294.56 \text{ kJ} \quad (5)$$

Setting the expression for the statistical compensation effect (eq 3) equal to the residual compensation effect in eq 5 provides a unique solution that satisfies both. These solutions will be referred to as E_{ac} for “corrected activation energy” and $\ln(A_c)$ for the “corrected natural logarithm of the frequency factor”. The corrected values are found by rearranging eq 3 to solve for the intercept C as shown in eq 6 and inserting experimental values for E_{aa} , $\ln(A_a)$, T_{Hj} , and the gas constant R . C , when inserted into eq 7 along with T_{Hj} , gives $\ln(A_c)$ and the corresponding E_{ac} is found by inserting $\ln(A_c)$ into eq 5.

$$C = E_{aa} - RT_{Hj} \ln(A_a) \quad (6)$$

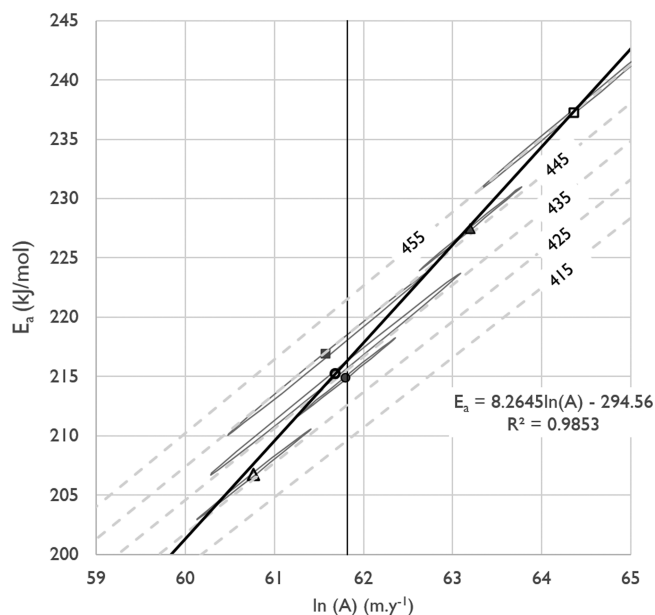


Figure 6. Diagram illustrating the distribution of kinetic solutions (symbols) from multiple analyses of single samples or samples from a single core. The light gray ellipses represent the statistical compensation effect with three standard deviation error bounds about the best fit solution (symbol). The dashed gray lines reflect the relationship between the Rock Eval T_{\max} and the kinetic parameters E_a and $\ln(A)$.

$$\ln(A_c) = \frac{(-294.56 - C)}{(RT_H - 8.2645)} \text{ kJ} \quad (7)$$

The values of E_{ac} and $\ln(A_c)$ presented in Table 1, lie at the intersection of the statistical compensation effect and the empirical relationship shown in Figure 5.

Regression analysis of the solutions to the Kissinger equation for the heating rate used to find T_{\max} shows these solutions to be linear ($R^2 = 1$). The linear coefficients, shown in Table 5, when solved simultaneously with the linear expression for the residual compensation effect yields the solutions for both E_a and $\ln(A)$ that correspond with T_{\max} .

Regression of T_{\max} versus E_a shown in Figure 7 provides the relationship between T_{\max} and E_a (eq 8) and with the relationship between E_a and $\ln(A)$ (eq 9), a solution for $\ln(A)$ as well.

The approximate relationship between E_a and T_{\max} is:

$$E_a = 22.195e^{0.00528 T_{\max}} \quad (8)$$

And the relationship between E_a and $\ln(A)$ from Figure 6 is:

$$E_a = 8.2645 \ln(A) - 294.56 \text{ kJ} \quad (9)$$

The residual compensation effect in samples of the Bakken Formation appears to be a function of differences in the distribution of kinetic parameters that progress with thermal maturity (Figure 6). This provides the solution that shows that E_a and A are directly related to T_{\max} , which is related to VR_o and BR_o using the equation from Abarghani et al.⁴²

$$X = T_{\max} = 188.679 \ln \left[\frac{E_a}{21.646} \right] \quad (10)$$

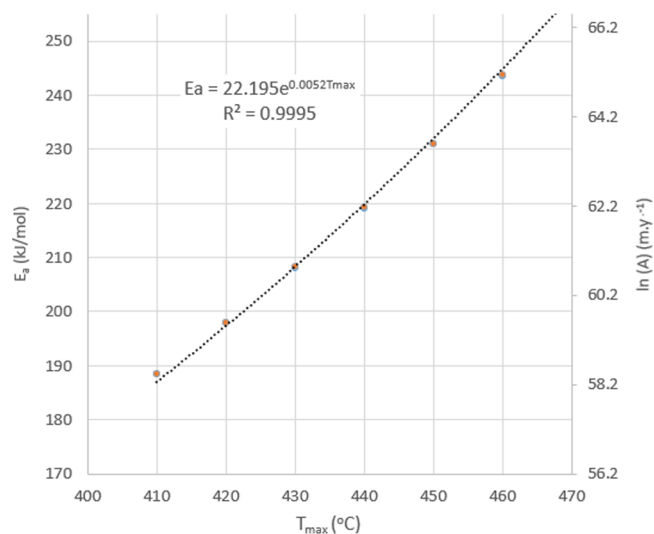


Figure 7. Regression (dotted line) of E_a and T_{\max} from the data shown in Table 5 (circles) using the residual compensation effect shown in Figure 6 and eq 8 provides a close approximation to the kinetic parameter E_a that corresponds to a given value of T_{\max} .

$$VR_o Eq = -1.30004e^{-7} X^4 + .000255242 X^3 - 0.185271 X^2 + 59.1015 X - 7005.3 \quad (11)$$

Setting X equal to the function of E_a that estimates T_{\max} and inserting it into the expression from Abarghani et al.⁴² yields the relationship between bitumen, equivalent vitrinite reflectance ($VR_o Eq$), E_a , and $\ln(A)$ (Figure 8).

Total Reactive Kerogen. Kerogen at elevated temperatures and pressures generates petroleum. The mass of kerogen is derived by the thickness of the source rock multiplied by the density of the source rock and S_2 (mg HC/g of rock) from pyrolysis. The results presented in the Table 2 are an average of the calculated densities, thickness, and kerogen mass. Higher masses are dependent on the amount of crackable hydrocarbon present in the rock sample.

The data obtained from pyrolysis (Table 3) show that total organic carbon (TOC) content values are between 11 and 15 wt %, implying that they are excellent source rock. According to Peters and Cassa,⁵⁶ rocks containing <0.5% TOC content are considered as poor source rocks. A TOC% value between 0.5 and 1% indicates fair source rock. A TOC% value between 1 and 2% indicates good source rocks. TOC% values above 2% often indicate a highly oxygen reducing environment and are excellent source rocks. The values from our analysis are confirmed from the plot of TOC (wt %) versus S_2 (mg/HC) shown in Figure 9. Hydrogen index (HI) values indicate the hydrocarbon generation potential and can be used to differentiate between the types of organic matter.⁵⁷ Kerogen with HI above 600 mg HC/g usually consists of type I or type II kerogen and has excellent potential to generate oil. Kerogen with HI between 300 and 600 mg HC/g contains a substantial amount of type II kerogen and has good potential for generating oil and minor gas. Kerogen with HI between 150 and 300 mg HC/g contains type III kerogen more than type II and can generate mixed gas and oil but mainly gas. HI <150 mg HC/g indicates a potential source for generating gas (mainly type III kerogen).

The HI values within the sampled locations ranged between 146 and 621 mg HC/g OC. HI <150 mg HC/g OC indicates a

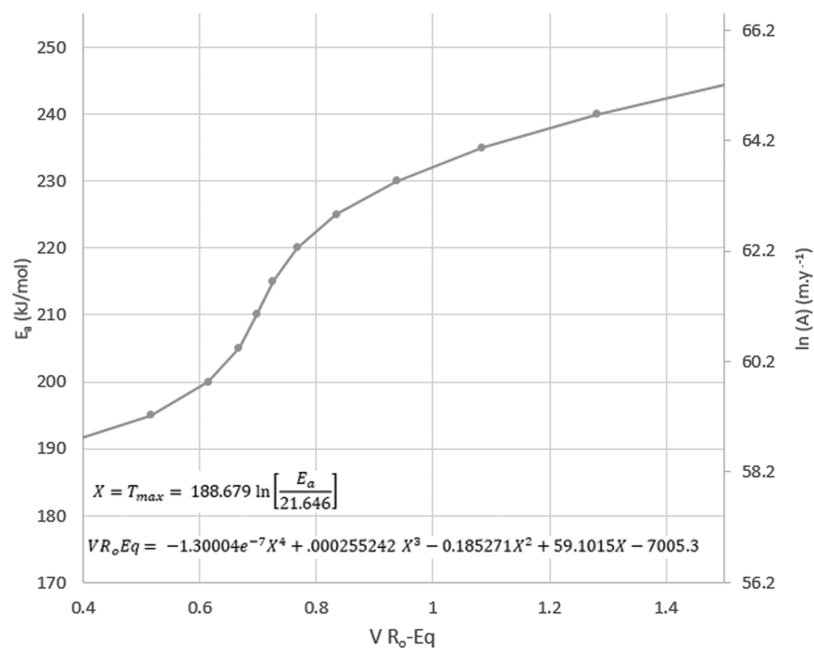


Figure 8. Curve relating the kinetic parameters of activation energy and frequency factor defined by the residual compensation effect to the BR_o ⁴² fourth order polynomial fit to VR_oEq ⁴⁶ for the Bakken Shale.

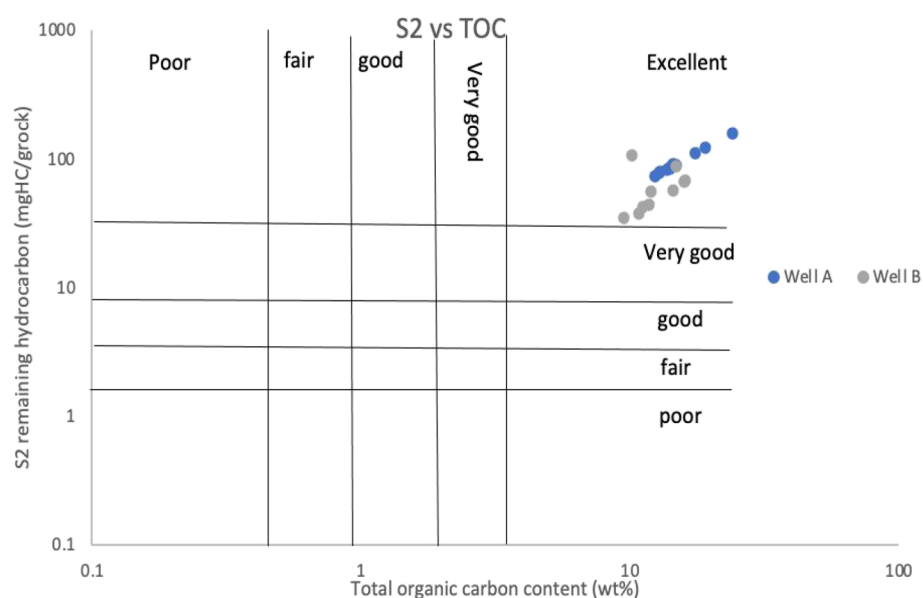


Figure 9. Plot of S2 versus TOC. Well no A is immature well while well no B is mature. This shows that the study wells both immature and mature have an excellent TOC.

source is generating type III kerogen (gas prone). This is as a result of intense generation within the sampled location and HI has been consumed (found within the wells in the central basin showing highly mature to overmature). Samples with HI >300 contain a significant amount of type II kerogen and have the capability of producing oil and lesser gas primarily. Samples with HI >600 contain roughly type II kerogen and are an excellent source of oil. This is due to the immaturity of Bakken Shales in the sampled location; hence HI is preserved (found at the outer portion of the basin). Based on the discussion above, HI is higher in areas that are thermally matured showing production. The map (Figure 10) shows that there is no production at the basin margin where we have low pressure. Areas of high pressure correspond to high reaction rates.

Production Rate Index. The rate at which kerogen mass converts into oil was calculated using the Arrhenius equation. It combines all the variables involving the frequency factor (A_e), minimum energy required for the reaction to take place (E_a), the gas constant (R), temperature at the depth of formation (T), and the mass of reactive kerogen(X) into an index for comparison with the formation pressure map and the results are shown in Table 4.

In the mature areas, high T_{max} and lower HI values compared with the results from the production rate calculation shows that wells at the interior basin have the highest reaction rate forty times ($30.84 \text{ mol-mg-cm}^2/\text{M.Y}$) higher than the immature areas. The higher rate is consistent with overpressure. Wells in the immature areas have the least reaction

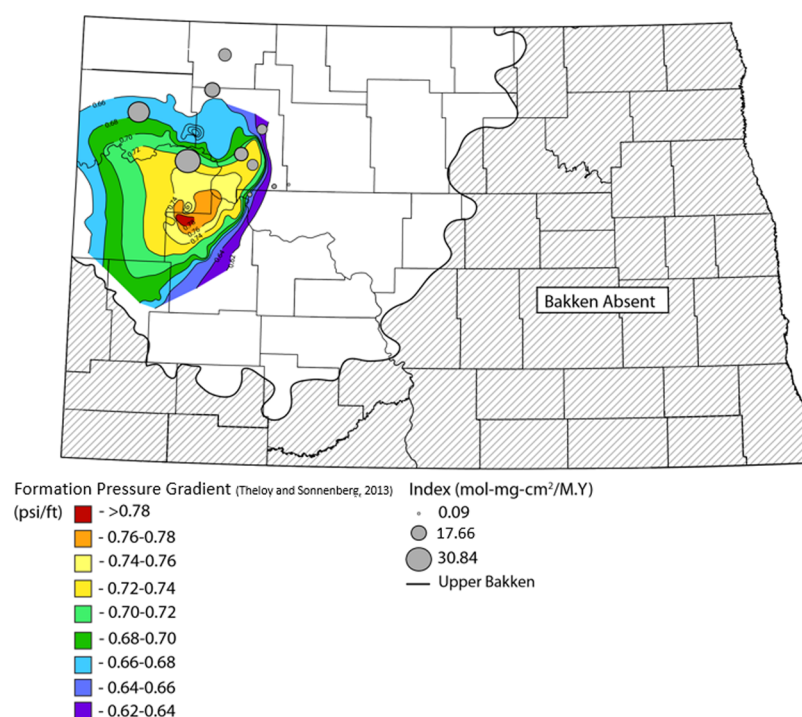


Figure 10. Map of formation pressure with the reaction rate bubble map placed on it. Formation pressure map modified from Theloy and Sonnenberg.⁵⁸ Hydrostatic gradient indicating a normal pressure gradient ≈ 0.46 psi/ft.

rate of $0.09 \text{ mol-mg-cm}^2/\text{M.Y.}$ The mechanism causing overpressure might be intense hydrocarbon generation from thermally matured and excellent quality source rock. The reaction rate calculated is consistent with current oil generation that may maintain overpressure. The map of reaction rate was placed on the overpressure map which was produced by Theloy and Sonnenberg⁵⁸ showing that wells with the highest reaction rate are found within areas of overpressure.

CONCLUSIONS

The wells in this study range from immature to thermally mature. Breakdown of kerogen increases in the Bakken shales at the deeper portion of the Williston Basin. The maturity of Bakken is not uniform across the basin, and thus the areas of high hydrocarbon generation lie within the interior basin where the heat flow is deeper and hotter. Additionally, the immature and mature areas contain excellent TOC, which provides only semiquantitative scale of petroleum generation, supporting quantity and not the quality of the organic matter. These organic-rich source rocks could generate hydrocarbon in the presence of higher temperatures. Temperature and pressure are factors that drive the conversion of organic matter to oil and may be tied to production. Evaluating oil generation rate could better define the limits of resource play, and it will aid in the search for new resources. The thickness, thermal maturity, TOC contents, and source rock kinetics controlled the amount of oil generated and expelled from the shales. Data from the kinetic analysis suggest that when Bakken samples are repeatedly analyzed the “best” solutions to these data form a residual compensation effect that is distinct from the statistical compensation effect. This appears to be a function of differences in the distribution of kinetic parameters that progress with thermal maturity. The linear expression of the residual compensation effect when solved simultaneously with

the regression analysis of the solutions to the Kissinger equation for the heating rate, yielded the solution for E_a and $\ln(A)$ that corresponds with T_{\max} . Finally, the values of T_{\max} recalculated in terms of VR_o and BR_o provided a relationship between the kinetic parameters (E_a and A), T_{\max} , VR_o , and BR_o . T_{\max} values measured within the Bakken Shale can be used to evaluate the “average” value of the kinetics as well as an estimate of the level of maturation roughly provided by VR_o and BR_o . Thus, of these different measures of maturity, E_a and $\ln(A)$ are the most capable of giving some measures as to how much observed reaction is occurring.

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Notes

The authors declare no competing financial interest.

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