



Data Article

Raw data of silver extraction from sodium-silver jarosite using three different lixiviants in alkaline medium



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ABSTRACT

This article presents the raw data of silver concentration ([Ag]) obtained as a function of time (t) from silver leaching experiments, which were conducted using a synthetic sodium-silver jarosite and different complexing agents: thio-sulfate, thiocyanate, and cyanide. Leaching experiments were performed under different conditions of temperature, pH and lixiviant concentration. The data refer to the article “Silver leaching from jarosite-type compounds using cyanide and non-cyanide lixiviants: a kinetic approach” (Islas et al., 2021), in which they were used to determine the leaching kinetics of jarosite-type compounds. The datasets were obtained experimentally from batch experiments. Concentration of silver, [Ag], was determined in each experiment as a function of time by atomic absorption spectroscopy. The information presented in this article can be useful for engineering stu-

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dents interested in mineral processing; particularly, for the calculation of kinetic parameters of silver leaching process. The data could also help in the formulation, implementation, or optimization of strategies for extraction of valuable metals from residues generated by the hydrometallurgical industry.

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Specifications Table

Subject	Engineering
Specific subject area	Mineral Processing; Hydrometallurgy
Type of data	Table
How the data were acquired	[Ag] in leaching samples was determined by atomic absorption spectroscopy (AAS), in a PerkinElmer Spectrometer model AAnalyst 200 AA (Waltham, MA, USA).
Data format	Raw
Description of data collection	Silver leaching from jarosite samples was evaluated by monitoring the variation of silver extraction with temperature (T), concentration and type of complex ($S_2O_3^{2-}$, SCN^- or CN^-), and initial pH. For each experiment, one parameter was modified, while the other three were kept constant. To follow the progress of the leaching reaction in each experiment, the concentration of silver, [Ag], was determined by AAS in samples of 5 ml, which were taken from the leaching solution at different times (t).
Data source location	Institution: Autonomous University of San Luis Potosí City/Town/Region: San Luis Potosí, S.L.P. Country: Mexico
Data accessibility	The datasets are deposited on Mendeley Data and can be accessed via the following link: https://doi.org/10.17632/wj8w88
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Value of the Data

- The datasets presented can be useful for scientists to develop comparative studies of silver leaching from ores using alternatives to cyanide such as thiosulfate and thiocyanate, aiming to increase the silver extraction and to minimize the reagent consumption.
- The datasets can be useful for engineering students as case study of leaching process to calculate reaction rates and kinetic parameters.
- The datasets can help scientists and engineers in the formulation, implementation, or optimization of strategies to recover valuable metals from residues produced by the hydrometallurgical industry.

1. Data Description

The datasets presented in this article show the results (silver concentration vs. time) regarding the leaching of a synthetic sodium-silver jarosite sample with three different lixivants: thiosulfate, thiocyanate, and cyanide. [Table 1](#) shows the results of the silver leaching from the sodium jarosite sample with thiosulfate. It shows the effects of temperature, pH, and concentration of complexing agent. The range in which these variables were evaluated during the experiments is also shown in [Table 1](#). The results of [Ag] against time for the silver leaching with

Table 1Datasets of [Ag] vs. time for silver leaching evaluation in alkaline medium from sodium-silver jarosite using $S_2O_3^{2-}$ as complexing agent. [Ag] in $mg L^{-1}$ and t in min.

NaS ₂ O ₃ (mol L ⁻¹)/pH _i ^a																				
0.1	t	0	2	6	10	15	20	25	30	40	60	80	120	-	-	-	-	-	-	
11.84	[Ag]	0	0.045	0.32	1.382	2.268	2.955	3.375	3.631	3.762	3.754	3.608	3.684	-	-	-	-	-	-	

0.04081	t	0	1	2	4	6	8	10	15	20	25	30	40	60	90	-	-	-	-	
11.80	[Ag]	0	0	0	0.001	0.094	0.304	1.03	3.079	4.639	5.636	6.338	6.788	6.777	6.671	-	-	-	-	

0.02857	t	0	2	6	10	15	20	30	40	60	80	110	150	-	-	-	-	-	-	
11.80	[Ag]	0	0.103	0.162	0.351	0.898	2.079	3.953	4.924	5.598	5.706	5.708	5.589	-	-	-	-	-	-	

0.01224	t	0	1	2	4	6	8	10	15	20	25	30	35	40	50	60	80	120	-	
11.77	[Ag]	0	0.004	0	0.001	0.001	0.001	0.001	0.01	0.122	0.744	1.098	1.414	1.628	2.014	2.252	2.366	2.386	-	

0.00408	t	0	2	6	10	15	20	30	40	60	90	120	150	225	-	-	-	-	-	
11.85	[Ag]	0	0.125	0.184	0.23	0.405	0.445	1.018	2.113	3.983	4.844	4.962	5.008	5.016	-	-	-	-	-	

0.00245	t	0	2	6	10	15	20	30	40	60	80	120	180	-	-	-	-	-	-	
11.88	[Ag]	0	0	0.035	0.044	0.062	0.123	0.265	0.81	2.088	2.981	3.854	4.083	-	-	-	-	-	-	

0.000408	t	0	2	6	10	15	20	30	40	60	80	120	180	240	300	-	-	-	-	
11.89	[Ag]	0	0	0	0	0	0	0.066	0.26	0.974	1.638	2.576	2.897	2.955	2.985	-	-	-	-	

NaOH (mol L ⁻¹) /pH _i																				
0.06	t	0	0.5	1	1.5	2	2.5	3	4	5	6	8	10	12	15	20	25	30	40	60
12.73	[Ag]	0	0.11	0.132	0.17	0.5	1.073	1.852	2.994	4.027	4.968	6.526	7.754	8.274	8.687	8.519	8.594	8.669	8.813	8.658

0.03	t	0	1	2	3	4	5	6	8	10	12	14	16	18	20	25	30	40	60	-
12.39	[Ag]	0	0.069	0.131	0.256	0.356	0.706	1.285	2.575	3.544	4.402	4.952	5.359	5.664	5.778	5.689	5.7	5.319	5.213	-

0.01	t	0	1	2	4	6	8	10	15	20	25	30	40	60	90	-	-	-	-	-
12.03	[Ag]	0	0	0	0.001	0.094	0.304	0.871	2.779	4.139	5.436	6.178	6.658	6.777	6.671	-	-	-	-	-

(continued on next page)

Table 1 (continued)

0.0066 11.80	t [Ag]	0 0	2 0	6 0.016	8 0.095	10 0.225	15 1.109	20 2.387	25 3.548	30 4.417	40 5.782	50 6.431	60 6.655	90 6.571	120 6.437	- -	- -	- -	- -	- -
0.0011 11.08	t [Ag]	0 0	2 0	4 0	6 0.002	10 0.013	15 0.042	20 0.101	25 0.23	30 0.593	40 1.112	50 2.471	60 3.565	80 5.067	100 6.016	120 6.531	150 6.707	240 6.345	- -	- -
0.00055 10.32	t [Ag]	0 0	5 0.023	10 0.034	15 0.06	20 0.081	30 0.189	40 0.309	50 0.445	60 0.577	80 1.773	100 2.971	120 4.143	150 5.379	180 6.206	220 6.899	300 6.942	- -	- -	- -
0.000275 9.98	t [Ag]	0 0	5 0.005	10 0	15 0.003	20 0.01	30 0.013	40 0.009	60 0.179	80 0.482	100 1.171	120 1.968	150 2.958	180 3.891	220 5.068	300 6.216	380 6.452	480 6.632	- -	- -
T (°C) /pH _i																				
70 10.59	t [Ag]	0 0	0.25 0.024	0.5 0.064	0.75 0.307	1 0.571	1.25 1.045	1.5 1.366	1.75 1.978	2 2.354	2.5 3.215	3 3.773	3.5 4.381	4 5.128	5 6.02	6 6.837	8 7.333	10 7.414	- -	- -
60 10.92	t [Ag]	0 0	0.25 0.002	0.5 0.024	0.75 0.113	1 0.222	1.25 0.49	1.5 0.656	1.75 1.066	2 1.522	3 2.663	3.5 3.308	4 4.109	5 5.024	6 6.13	8 7.683	10 8.645	12 9.307	15 9.239	20 9.358
50 11.31	t [Ag]	0 0	0.25 0.001	0.5 0.015	0.75 0.025	1 0.045	1.25 0.096	1.5 0.144	1.75 0.213	2 0.499	2.5 0.704	3 1.56	4 3.216	6 4.246	8 5.446	12 5.99	15 6.348	20 6.41	- -	- -
45 11.57	t [Ag]	0 0	0.5 0.003	1 0	1.5 0.054	2 0.08	3 0.32	4 0.993	6 2.195	8 3.364	10 4.272	15 5.509	20 6.164	25 6.309	30 6.45	- -	- -	- -	- -	- -
40 11.83	t [Ag]	0 0	0.5 0.002	1 0.001	1.5 0.052	2 0.051	3 0.193	4 0.416	6 1.609	8 2.723	10 3.779	15 5.313	20 6.357	25 6.793	30 6.98	40 7.053	50 7.025	60 6.635	- -	- -
35 12.04	t [Ag]	0 0	1 0.002	2 0.028	4 0.089	6 0.31	8 0.732	10 1.621	15 3.321	20 4.476	25 5.069	30 5.49	40 5.653	50 5.759	60 5.518	80 5.748	- -	- -	- -	- -
30 12.33	t [Ag]	0 0	1 0	2 0	4 0.001	6 0.094	8 0.304	10 0.871	15 2.779	20 4.139	25 5.436	30 6.178	40 6.658	60 6.777	90 6.671	- -	- -	- -	- -	- -

^a pH_i = initial pH, kept constant in all experiments.

thiocyanate are shown in Table 2. Table 3 shows the results of [Ag] vs. time for silver leaching with cyanide.

2. Experimental Design, Materials and Methods

2.1. Standards and reagents

Sodium cyanide, sodium thiocyanate, and sodium thiosulfate were used for the silver (Ag) leaching experiments; sodium hydroxide was used to adjust pH. All reagents were acquired from Sigma-Aldrich in ACS grade. For monitoring of Ag leaching by atomic absorption spectrometry (AAS), PerkinElmer Pure brand standard of Ag was used. All experiments were conducted using ultra-pure water with a resistivity of 18 M Ω cm.

2.2. Sample of synthetic sodium-silver jarosite

The sodium-silver jarosite sample was previously synthesized and fully characterized in a previous work [1]; details for the synthesis can be found in references [2,3]. The solid sample was sieved using Tyler sieves in the range $-325/+400$ mesh for the leaching experiments. The result of the sample elemental composition analysis was: Na 4.59%, Ag 0.89%, Fe 32.3 %, SO₄²⁻ 40.4% and H + O 21.82% (obtained by difference). The chemical approximate formula corresponds to Na_{0.96}Ag_{0.04}Fe_{2.82}(SO₄)_{2.01}(OH)_{5.36}(H₂O)_{0.86}.

2.3. Silver leaching experiments

The evaluation of the silver leaching from the sodium-silver jarosite was performed following an experimental method employed in previous works related to the alkaline decomposition of jarosite type compounds, silver leaching from mining tailings and silver metallic studies with some modifications [4–6].

All silver leaching experiments were carried out in a Pyrex glass reactor of 500 mL placed over a heating plate with an automatic external probe of temperature (Thermo Fisher Scientific, model SuperNuova+), and coupled to a digital mechanical stirrer with a three-blade propeller (IKA model RW20). The pH of the leaching solution was constantly measured with a pH-meter Orion 3 Star equipped with an Orion Ultra Sure Flow electrode and an automatic temperature compensation probe (Thermo Scientific). For the experiments, 500 mL of the leaching solution prepared according to the conditions of sodium hydroxide and the complexing agent (Tables 1–3), were decanted in the reaction vessel, and adjusted to a desired temperature. The stirring rate employed was 750 rpm. When the required temperature was reached, a sample of the leaching solution was taken corresponding to the condition $t = 0$ (blank). To start the reaction, 0.2 g of sodium-silver jarosite with an initial particle size of 38 μ m were added; at this point, the reaction time begins to be measured. The progress of the silver leaching was carried out taken samples at different times (t). These aqueous samples were previously filtered to remove solid residues and the [Ag] was determined by AAS. The initial pH (pH_i) in all leaching experiments was kept constant adding small volumes of a concentrated NaOH solution (1.0 mol L⁻¹). To evaluate the effect of NaOH concentration on the silver concentration, temperature and concentration of the leaching agent were kept constant at 30 °C (303 K) and 0.1 mol L⁻¹, respectively, varying the concentration of NaOH accordingly. To evaluate the effect of the leaching agent on the silver concentration in the leaching solution, the concentration of the lixiviant agent was varied maintaining constant the NaOH concentration and temperature (0.01 mol L⁻¹, 30 °C). To evaluate the effect of temperature, the concentrations of NaOH and complexing agent were kept constant (0.01 and 0.1 mol L⁻¹ respectively), varying the reaction temperature in each experiment.

Table 2Datasets of [Ag] vs. time for silver leaching evaluation in alkaline medium from sodium-silver jarosite using SCN^- as complexing agent. [Ag] in mg L^{-1} and t in min.

NaSCN (mol L^{-1})/pH _i																			
0.1	t	0	2	4	6	10	15	20	25	30	40	50	60	90	-	-	-	-	-
11.77	[Ag]	0	0.011	0.173	0.478	1.008	1.622	2.208	2.623	2.914	3.188	3.194	3.277	3.337	-	-	-	-	-
0.04081																			
11.95	t	0	1	2	4	6	8	10	15	20	25	30	40	50	60	80	100	-	-
11.95	[Ag]	0	0.01	0.012	0.013	0.041	0.095	0.173	0.379	0.537	0.653	0.762	0.91	0.993	0.963	0.883	0.916	-	-
0.02857																			
11.82	t	0	2	4	6	10	15	20	25	30	40	50	60	80	120	-	-	-	-
11.82	[Ag]	0	0.008	0.011	0.019	0.043	0.162	0.286	0.396	0.498	0.659	0.768	0.854	0.917	0.945	-	-	-	-
0.01224																			
11.83	t	0	1	2	3	4	6	8	10	15	20	25	30	40	50	60	80	100	120
11.83	[Ag]	0	0	0	0	0	0	0.002	0.007	0.023	0.042	0.068	0.087	0.119	0.145	0.171	0.206	0.226	0.237
0.00408																			
11.85	t	0	3	6	10	15	20	30	40	60	80	120	180	-	-	-	-	-	-
11.85	[Ag]	0	0.001	0.004	0.006	0.016	0.028	0.058	0.086	0.141	0.182	0.211	0.218	-	-	-	-	-	-
0.00245																			
11.86	t	0	2	4	6	10	15	20	30	40	60	80	120	180	-	-	-	-	-
11.86	[Ag]	0	-0.013	-0.029	-0.029	-0.025	-0.033	0.002	-0.009	-0.007	-0.011	0.019	0.03	0.04	-	-	-	-	-
0.000408																			
11.86	t	0	3	6	10	15	20	30	40	60	80	120	180	240	-	-	-	-	-
11.86	[Ag]	0	0.019	-0.003	-0.021	-0.032	-0.031	-0.048	-0.051	-0.041	0.015	0.045	0.056	0.051	-	-	-	-	-
NaOH (mol L^{-1}) /pH _i																			
0.06	t	0	0.5	1	1.5	2	3	4	6	8	10	12	15	20	40	-	-	-	-
12.56	[Ag]	0	0.005	0.019	0.028	0.037	0.098	0.228	0.497	0.696	0.839	0.928	1.018	0.978	1.118	-	-	-	-
0.03																			
12.33	t	0	1	2	3	4	6	8	10	12	16	20	25	30	40	50	-	-	-
12.33	[Ag]	0	0.002	0.016	0.024	0.032	0.114	0.232	0.35	0.478	0.748	0.902	1.057	1.157	1.118	1.176	-	-	-
0.01																			
11.95	t	0	1	2	4	6	8	10	15	20	25	30	40	50	60	80	100	-	-
11.95	[Ag]	0	0.01	0.012	0.013	0.015	0.055	0.193	0.329	0.537	0.683	0.762	0.88	0.993	0.963	0.883	0.916	-	-
0.0066																			
11.64	t	0	1	2	4	6	10	15	20	25	30	40	50	60	80	120	180	240	-
11.64	[Ag]	0	0.002	0.004	0.005	0.006	0.008	0.043	0.222	0.341	0.494	0.742	0.937	1.131	1.351	1.478	1.521	1.429	-

(continued on next page)

Table 2 (continued)

0.00275 11.34	t [Ag]	0 0	2 0.002	4 0.004	8 0.006	12 0.008	16 0.011	20 0.016	25 0.093	30 0.153	40 0.346	50 0.596	60 0.726	80 0.905	100 1.026	120 1.112	150 1.179	180 1.199	220 1.219	280 1.242
0.0011 10.88	t [Ag]	0 0	2 0.003	4 0.008	6 0.011	10 0.017	15 0.022	20 0.029	30 0.139	40 0.234	60 0.463	80 0.787	120 1.119	180 1.477	240 1.581	280 1.603	420 1.577	-	-	-
0.00055 10.38	t [Ag]	0 0	4 0	10 0.001	15 0.002	20 0.004	25 0.006	30 0.009	40 0.018	50 0.027	60 0.114	80 0.23	110 0.503	140 0.754	180 0.994	220 1.117	340 1.358	400 1.34	-	-
T (°C) /pH _i																				
70 10.59	t [Ag]	0 0	0.25 0.043	0.5 0.088	0.75 0.174	1 0.224	1.25 0.31	1.5 0.416	2 0.586	2.5 0.74	3 0.864	3.5 0.976	4 1.067	5 1.286	6 1.484	8 1.737	10 1.884	15 1.99	20 1.868	-
60 10.92	t [Ag]	0 0	0.25 0.007	0.5 0.034	0.75 0.07	1 0.116	1.25 0.185	1.5 0.245	2 0.406	2.3 0.516	3 0.677	3.5 0.771	4 0.875	5 1.045	6 1.275	8 1.552	10 1.732	15 1.875	20 1.829	-
50 11.31	t [Ag]	0 0	0.25 0	0.5 0.001	0.75 0.028	1 0.049	1.5 0.073	2 0.112	2.5 0.167	3 0.234	4 0.328	5 0.443	6 0.555	8 0.72	10 0.879	15 1.122	20 1.252	25 1.321	30 1.295	-
45 11.57	t [Ag]	0 0	0.5 0.015	1 0.026	1.5 0.052	2 0.066	2.5 0.13	3 0.197	4 0.3	5 0.384	6 0.474	8 0.686	10 0.862	15 1.308	20 1.567	25 1.728	30 1.83	40 1.817	-	-
40 11.83	t [Ag]	0 0	0.5 0.021	1 0.029	1.5 0.047	2 0.077	3 0.117	4 0.16	6 0.281	8 0.437	10 0.585	15 0.887	20 1.171	25 1.299	30 1.413	40 1.456	50 1.454	-	-	-
35 11.66	t [Ag]	0 0	1 0.009	2 0.023	4 0.053	6 0.138	10 0.354	15 0.611	20 0.792	25 0.94	30 1.014	40 1.082	50 1.108	60 1.108	-	-	-	-	-	-
30 11.95	t [Ag]	0 0	1 0.01	2 0.012	4 0.013	6 0.015	8 0.055	10 0.193	15 0.329	20 0.537	25 0.653	30 0.762	40 0.88	50 0.993	60 0.963	80 0.883	100 0.916	-	-	-

Table 3Datasets of [Ag] vs. time for silver leaching evaluation in alkaline medium from sodium-silver jarosite using CN^- as complexing agent. [Ag] in mg L^{-1} and t in min.

[NaCN] (mol L^{-1}) /pH _i																					
0.1	t	0	1	2	4	6	8	10	15	20	25	30	40	50	60	70	80	100	-	-	-
11.27	[Ag]	0	0.022	0.034	0.061	0.076	0.166	0.408	1.154	2.196	3.387	4.483	6.28	7.307	7.948	8.228	8.488	8.612	-	-	-
0.04087	t	0	0.5	1	2	4	6	8	10	15	20	25	30	40	50	60	80	100	120	140	233
11.19	[Ag]	0	0.026	0.034	0.056	0.086	0.099	0.122	0.135	0.392	0.922	1.376	2.085	3.101	4.146	4.896	5.973	6.579	6.718	6.858	7.155
0.0286	t	0	2	4	8	12	16	20	25	30	35	40	45	50	60	70	80	100	120	140	160
11.19	[Ag]	0	0.007	0.013	0.021	0.029	0.093	0.26	0.575	1.138	1.825	2.831	3.595	4.739	5.81	6.691	7.442	8.314	8.775	9.07	9.106
0.01224	t	0	3	6	9	15	20	25	30	40	50	60	80	100	120	150	180	-	-	-	-
11.13	[Ag]	0	0.015	0.021	0.035	0.153	0.271	0.417	0.623	1.155	2.847	4.099	6.15	7.555	8.598	9.138	9.368	-	-	-	-
0.00408	t	0	5	10	15	20	25	30	40	50	60	70	80	100	130	160	200	240	300	-	-
11.13	[Ag]	0	0.007	0.019	0.02	0.03	0.065	0.091	0.31	0.609	1.074	2.215	2.875	4.226	6.194	7.791	8.836	9.28	9.505	-	-
0.00254	t	0	5	10	20	30	40	60	80	100	130	160	200	240	300	420	-	-	-	-	-
11.09	[Ag]	0	0.02	0.033	0.036	0.054	0.077	0.201	0.462	1.476	3.293	4.774	6.37	7.384	8.402	8.665	-	-	-	-	-
0.000408	t	0	5	10	20	30	40	60	80	100	130	160	200	240	300	360	420	480	-	-	-
11.09	[Ag]	0	0.005	0.006	0.009	0.018	0.078	0.185	0.417	0.583	2.059	3.509	5.082	6.175	7.061	7.655	7.904	8.007	-	-	-
[NaOH] (mol L^{-1}) /pH _i																					
0.03	t	0	0.5	1	1.5	2	3	4	6	8	10	15	20	25	30	40	50	70	-	-	-
12.50	[Ag]	0	0.089	0.129	0.238	0.571	1.141	1.705	3.131	4.65	6.025	7.548	8.076	7.674	7.747	7.747	7.498	7.687	-	-	-
0.01	t	0	0.5	1	1.5	2	4	6	8	10	12	15	20	25	30	40	50	70	110	-	-
11.99	[Ag]	0	0.013	0.028	0.046	0.093	0.192	0.392	0.71	1.241	2.373	3.515	4.659	5.792	6.354	6.737	6.631	6.756	6.666	-	-
0.0066	t	0	0.5	1	1.5	2	3	4	6	8	10	15	20	25	30	40	50	60	80	-	-
11.83	[Ag]	0	0	0.005	0.005	0.026	0.015	0.022	0.044	0.095	0.363	1.335	2.388	3.48	4.555	5.453	5.841	6.048	6.181	-	-

(continued on next page)

Table 3 (continued)

0.0011 11.19	t [Ag]	0 0	0.5 0.026	1 0.034	2 0.056	4 0.086	6 0.099	8 0.122	10 0.135	15 0.392	20 0.922	25 1.376	30 2.085	40 3.101	50 4.146	60 4.896	80 5.973	100 6.579	120 6.718	140 6.858	233 7.155
0.00055 11.07	t [Ag]	0 0	5 0.012	10 0.021	15 0.12	20 0.306	30 1.019	40 1.953	60 3.729	80 4.948	100 5.711	120 6.113	150 6.516	200 6.571	- -	- -	- -	- -	- -	- -	- -
0.000275 11.00	t [Ag]	0 0	5 0.015	10 0.042	20 0.202	30 0.502	40 1.118	50 1.879	60 2.869	80 4.095	100 4.913	120 5.38	150 5.811	200 6.054	240 6.119	- -	- -	- -	- -	- -	- -
0.00006 10.93	t [Ag]	0 0	5 0.01	10 0.024	15 0.033	20 0.07	30 0.285	40 0.715	50 1.182	60 1.881	80 3.295	100 4.462	120 5.172	150 5.995	180 6.575	240 6.814	300 6.927	- -	- -	- -	- -
T (°C) /pH _i																					
70 10.33	t [Ag]	0 0	0.25 0.099	0.5 0.214	0.75 0.411	1 0.668	1.25 1.013	1.5 1.414	2 2.074	2.5 2.791	3 3.734	3.5 4.443	4 5.13	5 6.144	6 7.097	8 8.327	10 9.408	15 9.966	20 9.846	- -	- -
60 10.46	t [Ag]	0 0	0.25 0.024	0.5 0.137	0.75 0.24	1 0.324	1.25 0.458	1.5 0.528	2 1.255	2.5 1.605	3 2.081	4 3.519	6 5.719	8 7.609	10 9.296	15 11.114	20 11.744	25 11.494	30 11.614	- -	- -
50 10.65	t [Ag]	0 0	0.25 0.003	0.5 0.01	0.75 0.015	1 0.025	1.5 0.047	2 0.066	3 0.15	4 0.297	6 1.154	8 2.033	10 2.973	15 4.499	20 5.453	30 5.834	40 5.508	- -	- -	- -	- -
45 10.80	t [Ag]	0 0	0.5 0.007	1 0.005	2 0.005	3 0.051	4 0.114	5 0.181	6 0.323	8 0.723	10 1.374	12 1.788	15 2.588	20 3.731	25 4.596	30 5.148	40 5.604	60 5.577	- -	- -	- -
40 10.91	t [Ag]	0 0	1 0.007	2 0.016	3 0.027	4 0.036	5 0.062	6 0.111	8 0.228	10 0.398	12 0.765	15 1.353	20 2.435	25 3.393	30 4.014	40 4.854	50 5.331	60 5.499	80 5.572	- -	- -
35 11.04	t [Ag]	0 0	1 0.013	2 0.025	4 0.047	6 0.071	8 0.145	10 0.179	15 0.531	20 1.315	25 1.883	30 2.506	40 3.639	50 4.575	60 5.108	80 5.745	100 5.911	140 6.025	- -	- -	- -
30 11.27	t [Ag]	0 0	0.5 0.026	1 0.034	2 0.056	4 0.086	6 0.099	8 0.122	10 0.135	15 0.392	20 0.922	25 1.376	30 2.085	40 3.101	50 4.146	60 4.896	80 5.973	100 6.579	120 6.718	140 6.858	233 7.155

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships which have, or could be perceived to have, influenced the work reported in this article.

Data Availability

[Dataset of Ag concentration against time \(Original data\)](#) (Mendeley Data).

CRedit Author Statement

Hernán Islas: Investigation, Conceptualization, Validation; **Mizraim U. Flores:** Investigation, Validation; **Julio C. Juárez:** Investigation; **Martín Reyes:** Investigation; **Alien Blanco:** Investigation; **Emmanuel J. Gutiérrez:** Writing – review & editing; **Javier Aguilar:** Data curation; **Mary C. Nolasco:** Investigation; **Israel Rodríguez:** Data curation; **Iván A. Reyes:** Writing – original draft, Supervision.

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