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# Introduction

The emission control of volatile organic compounds (VOCs) has aroused great attention, due to their toxicity, carcinogenesis, and/or mutagenicity. Many techniques, such as catalytic oxidation,<sup>1,2</sup> adsorption<sup>3,4</sup> and biological methods,<sup>5,6</sup> have been explored for the removal of VOCs, of which adsorption was regarded as the most promising method for pollution control owe to its high efficiency, low cost and ease of regeneration.<sup>7–9</sup> Currently, a large quantity of waste biomass is generated from both living and industrial activities, which accounts for about 62.1% of the total amount of solid waste produced each year in China.<sup>10</sup> Among them, plant-based

# Preparation of high-yield N-doped biochar from nitrogen-containing phosphate and its effective adsorption for toluene<sup>+</sup>

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Novel biochar was prepared from plant-based biomass by the addition of nitrogen-containing phosphates (NCPs), including ammonia phosphate (AP), ammonia polyphosphate (APP) and urea phosphate (UP). The results demonstrated that with the addition of NCPs, the yield of biochar could be significantly increased from about 30% to up to about 60%. The pore structure of the biochar was significantly improved, and the AP-prepared biochar obtained a higher  $S_{BET}$  and  $V_{tot}$  of 798 m<sup>2</sup> g<sup>-1</sup> and 0.464 cm<sup>3</sup> g<sup>-1</sup>, respectively. Moreover, the surface chemistry of the NCP-prepared biochar was affected, and N heteroatoms could be successfully doped on the surface of biochar, up to 4.16%. Furthermore, through TG-FTIR and XPS analysis, some possible interactions between plant-based biomass and NCPs during the pyrolysis process were proposed to explore the mechanisms of the preparation process, including the P route and N route, in which the H<sub>3</sub>PO<sub>4</sub> and NH<sub>3</sub> gradually generated during the heating process played the dominant roles for the high yield N-doped biochar. All the NCP-prepared biochar presented good toluene adsorption capacities from 175.9 to 496.2 mg g<sup>-1</sup>, which were significantly higher than that of blank char (6.5 mg g<sup>-1</sup>).

biomass (PBB) is considered as the most promising carbon precursor for the preparation of biochar, because of its relatively high carbon content (>35%), high volatiles content (55–80.4%), abundant functional groups, low ash content, extensive source and low cost.<sup>11,12</sup> Biochar is a kind of suitable adsorbent for the control of pollutants as it possesses an abundant pore structure and surface functional groups.<sup>13,14</sup>

Biochar from PBB is generally prepared through chemical activation methods, in which KOH is the most common activation agent reported in previous studies.<sup>12,15,16</sup> It can help to form pores *via* its reactions with the carbon substrate and the resultant biochar usually possessed a high specific surface area ( $S_{BET}$ ).<sup>12,17</sup> However, the carbon yield from PBB using KOH as the activation agent was very low (10–20%),<sup>12,15,17</sup> and strong base of KOH has a serious corrosion on instruments and safety problem, which inhibited greatly the wide application of the basic agents.<sup>18</sup>

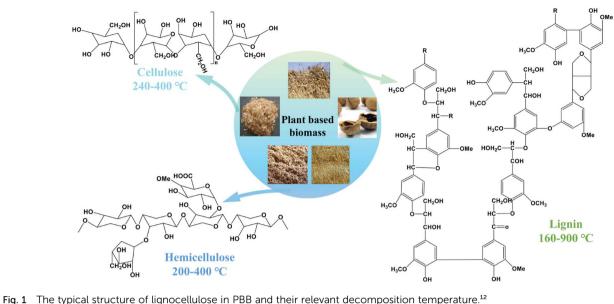
Moreover, it has been reported that the surface functionalization with some heteroatoms such as N atoms could change significantly the surface chemical properties of porous carbon, which could enhance its adsorption performance and catalytic activity for some specific pollutants, like VOCs, CO<sub>2</sub> and SO<sub>2</sub>, *etc.*<sup>15,19–24</sup> Generally, the post-treatment method has been widely investigated for N-doped biochar with nitrogencontaining agents, like urea, melamine and NH<sub>3</sub>, *etc.*<sup>25</sup> However, the low N-doping content, high corrosivity, complex technical process and high consumption severely inhibited its practical application.<sup>25</sup> Thus, it is significantly important to

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<sup>†</sup> Electronic supplementary information (ESI) available: Fig. S1 presented the schematic of the fixed bed system for toluene adsorption. Fig. S2 exhibits the yields of prepared carbon. Fig. S3 shows the SEM images of C-600, and AP-600. Fig. S4 and S5 respectively displays the N<sub>2</sub> adsorption isotherms and pore size distribution of the prepared carbon. Fig. S6–S8 respectively presents the high resolution XPS spectra for C 1s, N 1s and P 2p of the prepared carbon. Fig. S9 shows the TG analysis of pristine stillage, mixture of tillage and APP and UP. Table S1 summarized the characteristics of nitrogen-containing phosphates. And Table S2 presents the bulk density of prepared carbon. See DOI: 10.1039/c8ra05714a



**rg. 1** The typical structure of light cellulose in Fbb and their felevant decomposition temperature

develop a simple and effective method to prepare the N-doped biochar with low cost, together with high yield.

Nitrogen-containing phosphates (NCPs) might be a kind of promising additive for the preparation of N-doped biochar. First, NCPs can gradually generate H<sub>3</sub>PO<sub>4</sub> during the heating process, which could help the dehydration and crosslinking of biopolymers like cellulose, hemicellulose and lignin in PBB (Fig. 1)<sup>12</sup> with the decrease of burn off, resulting in high yield of resultant biochar. Meanwhile, the generated H<sub>3</sub>PO<sub>4</sub> can react with carbon to form pores during heating process.<sup>26</sup> On the other hand, the NCPs with high content of nitrogen can also be progressively decomposed to escape nitrogen species during the heating process, which can react with the carbon substances to form nitrogen-containing functional groups. Thus, based on the characteristics of PBB and NCPs, the NCPs exhibited a great potential as a novel additive for the preparation of biochar with high yield, abundant pores and nitrogen-containing functional groups. However, few studies have been found on using the NCPs as the additives for the preparation of biochar, and the effects of the NCPs addition on the pyrolysis process of PBB is not clear yet.

Therefore, in this study, three kinds of NCPs with different P contents and N formation were used as the additives for the preparation of biochar, including ammonia phosphate (AP), ammonia polyphosphate (APP) and urea phosphate (UP). Stillage, a common waste PBB generated from the wine-making process, was adopted as the carbon precursor. The effects of NCPs addition on the yield, pore structure and surface chemistry of the prepared biochar were investigated. Moreover, the possible interactions between NCPs and PBB was proposed to explore the preparation process of N-doped biochar. Finally, the toluene adsorption behaviours of the prepared biochar were evaluated.

# Experiment

#### Materials

Stillage used in this study was obtained from a local winery, Sichuan, China, whose main elemental contents were as follows (%): C 58.72, H 7.41, O 30.49 and N 3.38. Three kinds of NCPs, including AP, APP and UP were purchased from Chengdu Kelong Chemical Factory, whose properties are tabulated in Table S1.<sup>†</sup>

#### Preparation of biochar

After drying at 105 °C for 8 h, stillage was ground and sieved to particle size below 200 mesh, and then mixed with each NCP by a pulverizer at a weight ratio of 1:1. The pyrolysis of the mixture was performed in a tubular furnace under N<sub>2</sub> flow with a heating rate of 10 °C min<sup>-1</sup> to the target temperature and maintained for 1 h. After pyrolysis, the obtained carbon was washed with diluted HCl (1.2 mol L<sup>-1</sup>) at a ratio of 1 g carbon/ 10 mL HCl, followed by an extensively washing by hot distilled water until a neutral pH of washing liquor. The required biochar could be finally obtained after drying, which was denoted as AP/APP/UP-*x*, where *x* represented its pyrolysis temperature (°C).

#### Characterization

The pore structure of the prepared carbon was studied by  $N_2$  adsorption–desorption method using a surface area analyser (ASAP 2460, Micromeritics, USA) at 77 K. Prior to measurement, the samples were outgassed under vacuum at 250 °C for 8 h. Their  $S_{\text{BET}}$  was calculated from their isotherms data with the relative pressure ranging from 0.01 to 0.3. The micropore volume ( $V_{\text{mic}}$ ) and total pore volume ( $V_{\text{tot}}$ ) were derived from the  $N_2$  uptake when the relative pressure was at 0.1 and 0.95,

respectively. The mesopore volume ( $V_{meso}$ ) was calculated from BJH model, while the micropore size distribution was obtained by using DFT model.

The chemical composition of the prepared carbon was determined by X-ray photoelectron spectroscopy (ESCALAB250, Thermo, USA) with Al K $\alpha$  X-rays radiation. The high resolution XPS spectra for each element was measured at a 0.2 eV step size and their signals were fitted using mixed Lorentzian–Gaussian curves with a Shirley function as background. Fourier transform infrared (FTIR) spectra was obtained on a spectrometer (Nicolet 6700, Thermo, USA) in the wave number in the ranging of 4000–400 cm<sup>-1</sup>.

The pyrolysis process of stillage, AP and their mixture were investigated *via* TG-FTIR method with following protocol. Samples were loaded in a platinum pan of the TG analyzer (TG 209 C, NETZSCH, Germany) and heated with a heating rate of 10 °C min<sup>-1</sup> from room temperature to 1000 °C under N<sub>2</sub> atmosphere. The generated gas was recorded every 15 seconds by an FTIR analyser (Tensor 27, Bruker, Germany) with a resolution of 2 cm<sup>-1</sup>.

#### Toluene adsorption test

The toluene adsorption behavior of the prepared biochar was estimated by a fixed bed reactor system, whose schematic is depicted in Fig. S1.<sup>†</sup> Two lines of  $N_2$  gas was controlled by two mass flow meters, respectively, in which one was bubbled through a pure toluene solution to bring out the toluene vapor and the other line was adopted as the balance gas to make the inlet toluene concentration maintained at 600 ppmv and the total flow rate of gas at 400 mL min<sup>-1</sup>. The prepared biochar was filled into a glass-made fixed bed (inner diameter: 10 mm), with the packing height at 20 mm. The reaction temperature was controlled at 30 °C and the outlet content of toluene was online monitored every 10 min by a GC-FID (Agilent, 7892B, USA) analyzer equipped with a six-way valve. The toluene adsorption capacity was calculated from the integration of the break-through curve.

### **Results and discussion**

#### Yield of biochar

Fig. S2<sup>†</sup> shows the yields of prepared biochar obtained with different NCPs (AP, APP and UP) and at different temperature (500–900 °C). The yields of the biochar from pristine stillage were in the range of 26.5–31.5 and slightly decreased with the increase of pyrolysis temperature. Compared with the pristine stillage, the yields of the NCPs-treated biochar was evidently higher with the temperature range from 500 to 800 °C (over 45%), demonstrating that the addition of NCPs could effectively increase the yield of biochar. When the pyrolysis temperature was raised to 900 °C, the yields of all the NCPs-treated biochar decreased dramatically and were close to the blank sample.

#### Characterization of biochar

**Pore structure.** The SEM images of the blank biochar and the NCPs- treated biochar (*i.e.* C-600 and AP-600) are presented in

Fig. S3.<sup>†</sup> It can be seen that the fiber structure of pristine stillage was still remained for blank biochar and its surface was relatively smooth. The morphology of AP-600 was quite different, and the fiber structure of stillage was evidently damaged and much more pores could be found on the surface of AP-600. This suggests that the addition of AP greatly changed the surface morphology and improved the porous structure of biochar.

The N<sub>2</sub> adsorption-desorption isotherms of the prepared biochar is plotted in Fig. S4.† It can be seen that a small amount of N<sub>2</sub> could be adsorbed by blank biochar (*i.e.* C-600 and C-900) during the whole relative pressure, while all the biochar with the addition of NCPs presented significantly higher N2 adsorption capacities. For the samples prepared at 600 °C, the NCPs-treated biochar presented evidently higher N2 adsorption uptake (from 100 to 150 cm<sup>3</sup> g<sup>-1</sup>) at low relative pressure, suggesting that the NCPs-treated biochar had abundant micropores. Furthermore, the isotherm of the biochar with NCPs presented distinct hysteresis loops, demonstrating the existence of some mesopores in the biochar. The NCPs-treated biochar prepared at 900 °C exhibited evidently better N<sub>2</sub> adsorption performance at low relative pressure and more evident hysteresis loops, compared with those at 600 °C. This indicates that more micropores and mesopores could be generated at high temperature.

The textural properties of the samples calculated from the N<sub>2</sub> adsorption isotherms are summarized in Table 1. The blank biochar (*i.e.* C-600 and C-900) had very low  $S_{\text{BET}}$  and  $V_{\text{tot}}$ , at about 40 m<sup>2</sup> g<sup>-1</sup> and 0.08 cm<sup>3</sup> g<sup>-1</sup>, respectively, demonstrating their poor pore structure. After the addition of NCPs, the  $S_{\text{BET}}$ ,  $V_{\text{tot}}$  and  $V_{\text{mic}}$  of the NCPs-treated biochar were dramatically increased. For the samples prepared at 600 °C, their  $S_{\text{BET}}$  and  $V_{\text{tot}}$  were at 388–481 m<sup>2</sup> g<sup>-1</sup> and 0.265–0.303 cm<sup>3</sup> g<sup>-1</sup>, respectively, and the  $V_{\text{mic}}/V_{\text{tot}}$  ratios were in the range of 59.2–69.4%, with the highest for AP-600, indicating that AP might help to generate more micropores. Compared with the samples prepared at 600 °C presented higher  $S_{\text{BET}}$ ,  $V_{\text{tot}}$ ,  $V_{\text{meso}}$  and  $V_{\text{mic}}$ , especially for  $V_{\text{meso}}$ , while the  $V_{\text{mic}}/V_{\text{tot}}$  ratios were in the range of 45.5–50.9%, indicating that high temperature helps to develop mesopores.

The pore size distribution of the prepared biochar is presented in Fig. S5.† Little pores with the diameter lower than 3 nm could be found in the C-600, while all the biochar with the NCPs exhibited several evident peaks and the peak located at

Table 1	Textural properties of prepared biochar	
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		Pore vo	lume (cm		
Sample	$S_{\rm BET} \left( {{m}^2 {\ g^{ - 1}}}  ight)$	$V_{\rm tot}$	V <sub>mic</sub>	V <sub>meso</sub>	$V_{ m mic}/V_{ m tot}$ (%)
C-600	37	0.073	0.017	0.056	23.3
AP-600	481	0.291	0.202	0.087	69.4
APP-600	388	0.265	0.157	0.108	59.2
UP-600	443	0.303	0.182	0.119	60.0
C-900	40	0.081	0.018	0.063	22.2
AP-900	798	0.464	0.211	0.253	45.5
APP-900	831	0.468	0.223	0.245	47.6
UP-900	666	0.428	0.218	0.210	50.9

0.6–0.7 nm presented the highest intensity. Such micropores are beneficial for the adsorption of pollutants with small sizes, like CO<sub>2</sub>, SO<sub>2</sub>, and H<sub>2</sub>S *etc.*<sup>15,20,24</sup> On the other hand, the peak located at 1.0–2.0 nm for all the NCPs prepared biochar at 900 °C presented higher intensity than those at 600 °C, indicating that high temperature helps the formation of more micropores with larger size. The biochar prepared in our study was different from that prepared by H<sub>3</sub>PO<sub>4</sub>, which was likely with more mesopores<sup>26</sup>. This suggests that the biochar treated with NCPs might be preferred for preparing the adsorbates with more micropores.

**Elemental analysis.** The elemental contents of prepared biochar obtained from XPS analysis are listed in Table 2. The blank biochar (C-600) exhibited evidently higher C content (82.81%), compared with NCPs-treated biochar prepared at 600 °C (70.78–73.61%), indicating that more non-carbon substances were introduced on the carbon surface with the addition of NCP. Furthermore, the NCP-treated biochar exhibited distinctively higher N contents (3.26–4.16%) than C-600 (1.54%), suggesting that N atoms were successfully doped by the addition of NCP.

For the samples prepared at 900 °C, their carbon contents were approximately similar, *i.e.* about 79%, and the relative contents of C in all NCP-treated biochar were dramatically increased, compared with those at 600 °C. This indicates that more non-carbon species were released at high temperature. Both N and P contents dramatically decreased, compared with those prepared at 600 °C, suggesting that part of N and P species with lower thermal stability was decomposed. However, the N and P contents of the NCP-treated biochar were higher than those of C-900, indicating that some N and P species still maintained on the surface of carbon after high temperature, which might be existed in more stable forms. In addition, AP-treated biochar had relatively higher contents of N than the other samples, possibly due to higher contents of N existed in AP (Table S1<sup>†</sup>).

Surface functional groups. The FTIR spectra of the prepared biochar are plotted in Fig. 2. The broad band located at 3000–3500 cm<sup>-1</sup> and the peak at about 1580 cm<sup>-1</sup> could be found in all prepared samples, which are attributed to the secondary amines and C=O, respectively.<sup>27</sup> The C-600 had the signal appearing at 1091 cm<sup>-1</sup> that was ascribed to the tertiary amines,<sup>28</sup> which might be derived from the N atoms existing in pristine stillage, while the NCP-treated biochar didn't show this peak, which might be due to the interference from other species

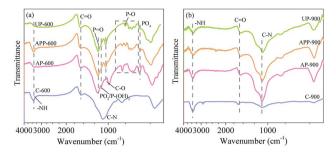


Fig. 2 FTIR spectra of prepared biochar at 600 °C (a) and 900 °C (b).

in the samples, such as P species. AP-600, APP-600 and UP-600 presented approximately same bands at 1190, 1100, 1040 and 597 cm<sup>-1</sup>, which were assigned to the stretching vibration of hydrogen-bonded P=O groups of phosphates,<sup>26</sup> symmetric stretching vibration of PO<sub>2</sub> or the asymmetric stretching vibration of P-(OH)<sub>2</sub> in phosphate, stretching vibration of the C-O in P-O-R and the asymmetric deformation vibration of PO<sub>4</sub> in phosphate, respectively. Furthermore, a series of peaks located at 1000–750 cm<sup>-1</sup> were due to the asymmetric stretching vibrations of C-O-P and P-O-P.<sup>29</sup> All the bands are the characteristics of the presence of phosphate esters in the prepared biochar due to the addition of NCPs.

For the samples prepared at 900 °C, much less functional groups could be detected compared with those at 600 °C. Only the peaks ascribed to NH, C=O and C-N presented, indicating that some N species were remained on the surface of carbon. However, the bands belonging to P species were in absence, indicating that most of the phosphorus compounds were decomposed or the P species existing on the carbon surface might be in non-IR active, like elemental P, *etc.* 

The relative contents of each functional group obtained from the high resolution XPS spectra (Fig. S6–S8†) are given in Table 3. It could be seen that four kinds of functional groups could be detected in C 1s spectra in all samples, *i.e.* C–C, C–O, C=O and COOR.<sup>30</sup> It can be seen that for the samples prepared at 600 °C, NCPs-treated biochar presented similar contents of C–O and C=O, while evidently higher COOR content (10.47–19.82%), compared with blank biochar (5.11%). This demonstrates that more esters were generated in the carbon with NCPs addition. For the samples prepared at 900 °C, the contents of esters and C=O dramatically decreased (<5%), indicating that they were decomposed at higher temperature. Based on the FTIR analysis

Table 2         Elemental analysis of prepared biochar							
Sample	C 1s (%)	O 1s (%)	N 1s (%)	P 2p (%)	O 1s/C 1s	N 1s/C 1s	
C-600	82.81	15.43	1.54	0.22	0.186	0.019	
AP-600	73.61	19.66	4.16	2.58	0.267	0.057	
APP-600	75.08	19.17	3.45	2.30	0.255	0.046	
UP-600	70.78	23.56	3.26	2.39	0.333	0.046	
C-900	79.91	19.46	0.47	0.16	0.244	0.005	
AP-900	79.31	18.01	1.60	0.88	0.227	0.023	
APP-900	79.79	17.82	1.54	0.85	0.223	0.019	
UP-900	78.13	20.61	0.76	0.50	0.263	0.010	

Table 3 Relative contents of functional groups in prepared biochar calculated from XPS spectra

Sample	600-C	600-AP	600-APP	600-UP	900-С	900-AP	900-APP	900-UF
C-C	64.23	54.89	61.63	44.60	77.19	67.28	64.24	71.88
С-О	18.98	20.30	18.60	23.86	14.04	24.17	27.15	19.13
C=O	11.68	10.53	9.30	9.85	3.86	4.48	3.66	6.68
COOR	5.11	14.29	10.47	19.82	4.91	4.68	4.94	2.29
Pyridinic	28.57	30.29	47.25	29.45		28.13	12.99	21.05
Pyrrolic	47.40	47.36	35.65	70.55		25.00	22.08	30.26
Graphitic	14.94	18.03	9.28	_		26.88	35.06	38.16
Oxidized	9.09	4.33	7.83	_		20.00	29.87	10.53
Р	_	_	_	_	_	26.14	16.47	48.00
$PO_{4}^{3-}$		33.72	51.30	22.33		73.86	83.53	52.00
$PO_3^-$		_	11.30	7.57		_	_	_
$P_2O_5$		66.28	37.39	70.10		_	_	_

(Fig. 2), it can be assumed that the esters might be phosphorus esters.

As shown in Table 3, all samples prepared at 600 °C had four kinds of N species, including pyridinic N, pyrrolic N, graphitic N and oxidized N.<sup>31</sup> It can be seen that pyridinic N and pyrrolic N were the main forms of N atoms. However, for the samples prepared at 900 °C, the relative contents of pyridinic N and pyrrolic N decreased significantly, while the contents of graphitic N and oxidized N increased evidently. This indicates that more N species were transferred into the inner of graphitic structure and some N groups were oxidized at higher temperature.32 In this study, the oxidants might be the generated gases during biomass decomposition process, like CO2 and H2O, etc. This result is corresponded to previous studies that used NH<sub>3</sub> post heating treatment for carbon surface modification.<sup>32</sup> They reported that much more graphitic N and oxidized N were generated with high temperature (i.e. 800 °C). It can be assumed that the NCPs can be decomposed into NH<sub>3</sub>, which could modify the carbon surface during pyrolysis process.

XPS results show that the P 2p peaks for blank biochar (C-600 and C-900) were not detected, due to the low content of P in pristine stillage, while the resolution of the NCPs-treated biochar was evident. As shown in Table 3, all NCPs-treated biochar prepared at 600 °C had the peaks ascribed to  $PO_4^{3-}$  and  $P_2O_5^{,33}$ which might be the  $H_3PO_4$  generated from the NCPs or/and derived from the partial decomposition of phosphate esters (Fig. 2). Furthermore, the APP-600 and UP-600 showed a small amount of P existing as the form of  $PO_3^{-},^{33}$  which might be also generated from the decomposition of phosphate compounds. When the temperature increased to 900 °C, both  $P_2O_5$  and  $PO_3^{-}$ on the carbon surface were diminished, while the peak ascribing to elemental P appeared.<sup>33</sup> This indicates that these phosphorus oxides were reduced by carbon to elemental P under high temperature.<sup>34</sup>

The results of both FTIR and XPS analysis demonstrated that N heteroatoms could be successfully introduced to the surface of the biochar with the treatment of NCPs, which was quite different with those prepared from conventional additives, like  $H_3PO_4$  and KOH. On the one hand, when  $H_3PO_4$  or KOH were used for the additives, post treatment is necessary for the introduction of N to the carbon surface,<sup>35</sup> while the NCPs

used in our study presented a high content of N (Table S1†), which could provide abundant N atoms with resultant biochar. On the other hand, the conventional additives could release N atoms that existed in biomass, especially for KOH, which caused a further decrease of N content in resultant biochar.<sup>36</sup>

#### TG-FTIR analysis during pyrolysis process

TG analysis. As shown in Fig. 3, the TG curve of the mixture of stillage and AP with the weight ratio of 1 : 1 were also plotted, together with the simulated curve calculated from the respective TG curves of stillage and AP. It can be seen that the two TG curves were not coincided, indicating that there were some interactions happened between stillage and AP during the pyrolysis process. From 100 °C to 340 °C, the mixture presented a higher weight loss compared with the fitting curve, indicating that the addition of AP might help the decomposition of stillage or vice versa. With the temperature growing from 340 to 600 °C, the weight loss of the mixture was clearly lower than that of fitting curve, suggesting that more substances remained on the surface of carbon. According to both FTIR (Fig. 2) and XPS analysis (Table 3), we can find that some phosphate esters existing on the surface of carbon after the pyrolysis of the mixture at 600 °C. This suggests that the NCPs could be

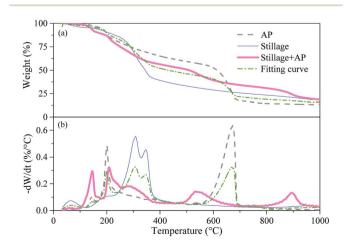


Fig. 3 TG (a) and DTG (b) analysis of AP, pristine stillage and their mixture with the weight ratio of 1: 1.

decomposed to H<sub>3</sub>PO<sub>4</sub> firstly, which subsequently react with the lignocellulose in biomass to form phosphate esters to inhibit the decomposition of carbon substances and decrease the weight loss of biomass.<sup>12</sup> As a result, the biochar yields were higher for the samples with the NCPs, compared with blank biochar (Fig. S1<sup>†</sup>). Notably, an evident weight loss of the mixture could be observed from 500 °C, with the DTG peak at about 537 °C, while the fitting curve was at about 672 °C. This phenomenon might indicate that the generated phosphorus esters started to decompose from 500 °C,33 resulting in the appearance of  $P_2O_5$  on the surface of AP-600 (Table 3). Finally, a distinct decomposition peak was detected for the mixture from 800 °C, with the DTG peak at about 893 °C, while no evident weight loss could be found in the fitting curve. As a result, the weight loss caused the decrease of yield for biochar prepared at 900 °C (Fig. S2<sup>†</sup>). As shown in Table 3, both N and P contents declined dramatically for the samples prepared at 900 °C. This suggests that some reactions involving nitrogen, phosphate compounds and carbon happened within this temperature range, resulting in the change of C, N and P species existing on carbon surface (Table 3).

In addition, the TG curves of the APP mixture (APP + stillage) and UP mixture (UP + stillage) were not coincided with their relevant fitting curves (Fig. S9†), either, demonstrating that the two NCPs also took part in the activation process of stillage. Furthermore, the weight loss profile of the APP mixture and UP mixture were parallel to that of AP mixture, which suggests that the reactions occurred between carbon with the APP or UP were similar to those with AP.

TG-FTIR analysis. To understand better the preparation process of biochar with AP addition, the gaseous products generated from the pyrolysis of stillage, AP and their mixture were monitored by FTIR spectrometer, along with the TG analysis, as shown in Fig. 4. In Fig. 4(a) (<270 °C), for stillage, when the temperature were higher than 180 °C, two peaks located at 1798 and 1128 cm<sup>-1</sup> appeared, which were ascribed to the stretch vibration of C=O in fatty groups and C-O-C in saccharides, respectively.<sup>12</sup> This suggests that the decomposition of lignin in stillage started.12 Furthermore, the peaks at 2359 and 2338 cm<sup>-1</sup> could also be detected when temperature were higher than 210 °C, which were the R and P branches of the asymmetric stretch vibration of CO2 molecules, respectively.37 With the increase of temperature, the intensities of all the peaks got higher, indicating that the decomposition process became more vigorous.

For AP, two series of peaks could be detected when temperature was higher than 120 °C, which were due to the stretch and deformation vibration of  $NH_3$ , demonstrating that AP began to decompose and the  $NH_3$  molecules could be released gradually. Their intensities were increased first when temperature was lower than 210 °C, and then gradually decreased.

For the spectra of the mixture, when the temperature was about 120  $^{\circ}$ C, the vibration of NH<sub>3</sub> could be detected. And the intensities of NH<sub>3</sub> were increased when temperature were lower than 150  $^{\circ}$ C, while decreased over 150  $^{\circ}$ C. The phenomena were different from that of AP, indicating that the stillage might promote the decomposition of AP at lower temperature. In

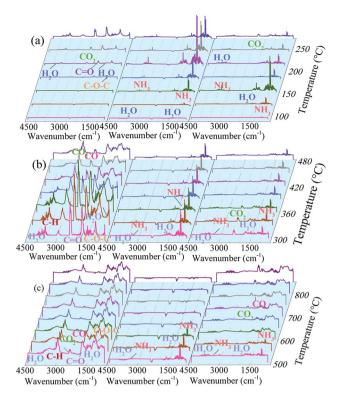


Fig. 4 Typical FTIR spectra for the gaseous products of stillage (left), AP (middle) and their mixture (right) at different temperature. (90– 270  $^{\circ}$ C (a), 300–480  $^{\circ}$ C (b), 500–850  $^{\circ}$ C (c)).

addition, the intensities of  $H_2O$  were higher in the mixture sample when temperature were higher than 120 °C, suggesting that the addition of AP could help the dehydration of stillage. Meanwhile, no peaks ascribed to C=O and C-O-C could be found in the spectra of the mixture, while only a small amount of  $CO_2$  could be detected when temperature were higher than 180 °C. This suggests that the decomposition pathway of biomass was severely changed with the presence of AP. It was reported that the ethers in PBB could be dehydrated to ketone with the catalysis of  $H_3PO_4$  when temperature were higher than 50 °C.<sup>27</sup> This suggests that the dehydration might occur for ethers in PBB once the AP was decomposed, instead of being liberated, avoiding the reduction of carbon species.

As illustrated in Fig. 4(b), from 300 to 500 °C, the peaks ascribed to H<sub>2</sub>O, C=O, C–O–C and CO<sub>2</sub> could be detected in all spectra of stillage. Furthermore, the absorption bands ranging from 3030–2800 cm<sup>-1</sup> appeared, which were assigned to the stretch vibration of CH, CH<sub>2</sub> and CH<sub>3</sub>, suggesting the generation of some light alkanes, such as methane, ethane or propane.<sup>37</sup> The products were generated from the decomposition of hemicellulose and cellulose in stillage.<sup>12</sup> For AP, H<sub>2</sub>O and NH<sub>3</sub> were still the main gaseous products at this temperature range, especially the NH<sub>3</sub> was generated drastically with similar intensities. This indicates that NH<sub>3</sub> could be released gradually from the AP during pyrolysis process. For the mixture of stillage and AP, H<sub>2</sub>O, CO<sub>2</sub> and NH<sub>3</sub> were the main products at this period. No bands belonging to the light hydrocarbons could be detected and the peak intensities of both CO<sub>2</sub> and NH<sub>3</sub> were relatively lower than

those of the stillage and AP, respectively, especially for  $CO_2$ , suggesting that the loss of carbon species were suppressed.

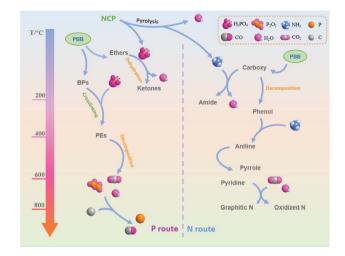
When the temperature was higher than 500  $^{\circ}$ C (Fig. 4(c)), for the stillage, the intensity of peaks belonging to light alkanes was higher than that of CO<sub>2</sub>, and with temperature growing, less CO<sub>2</sub> could be generated. For AP, even though the contents of generated NH<sub>3</sub> kept decrease, there was still NH<sub>3</sub> released below 700 °C. This indicates that N source existed within 700 °C. For the mixture, from 500 to 550 °C, H<sub>2</sub>O and NH<sub>3</sub> were its main products, while no more NH3 molecule could be detected and more CO<sub>2</sub>, CO and H<sub>2</sub>O were generated when temperature were higher than 600 °C. It is possible that there are four types of processes occurred at this temperature range. First, the generated NH<sub>3</sub> was evolved in the decomposition of stillage, which lead to the formation of N-containing groups on the surface of carbon (Table 3) and meanwhile help to develop pores. Second, the contents of CO<sub>2</sub> and C-O-C in gas phase increased significantly after 750 °C, which was corresponded with an evident weight loss in TG curve (Fig. 3). Third, the gradually increased CO content from 750 °C demonstrating the reactions of carbon substrate with some oxidants, like CO2, H2O and P2O5, etc. Furthermore, as shown in Table 2, the P contents decreased dramatically from 600 to 900 °C, while no P species could be found in FTIR patterns at this temperature range (Fig. 2). It can be assumed that the elemental P, which is in non-IR activity, was released from the reactions between P2O5 and carbon matrix.<sup>34</sup> In the preparation process, we found that some red substances precipitated on the inner wall of the furnace when the pyrolysis temperature were beyond 800 °C, which must be the condensed elemental P.

#### Possible interactions between PBB and NCP

Based on the above results, the possible interactions between PBB and NCP during the preparation process of biochar was proposed, which could be classified into two aspects, including P route and N route, as illustrated in Fig. 5.

For P route, when temperature were higher than 120 °C, AP might be firstly decomposed into  $H_3PO_4$  (eqn (1)-(3)). At lower temperature (<340 °C), in the presence of  $H_2O$  (Fig. 4(a)), the generated H<sub>3</sub>PO<sub>4</sub> could act as a Brønsted acid to catalyze the dehydration of ethers in PBB, like lignin, cellulose and hemicellulose, etc., into ketones and H<sub>2</sub>O.<sup>38,39</sup> As a result, the O and H species were volatilized and the weight loss was higher within the temperature range (Fig. 4). With temperature growing (340-500 °C), phosphate esters (PE) were formed from the crosslinking of H<sub>3</sub>PO<sub>4</sub> and biopolymers (BPs) in PBB (eqn (4)), which could keep stable during this period and avoid the escape of C atoms. Furthermore, when temperature was higher than 500 °C, part of the generated phosphate esters started to decompose into  $P_2O_5$  (Table 3),  $H_2O$  and  $CO_2$  (Fig. 4). With temperature higher than 800 °C, the generated P<sub>2</sub>O<sub>5</sub> might play as an oxidant for carbon species to produce CO<sub>2</sub> and elemental P. At the same time, the generated elemental P could be evaporated and diffused through the carbon layers, leading into a further pore forming.

Decomposition



**Fig. 5** Possible reactions between PBB and NCP during the pyrolysis process (PBB: plant-based biomass, NCP: nitrogen containing phosphate, BPs: biopolymers, PEs: phosphate esters).

$$(\mathrm{NH}_4)_3\mathrm{PO}_4 \to (\mathrm{NH}_4)_2\mathrm{HPO}_4 + \mathrm{NH}_3\uparrow \tag{1}$$

$$(\mathrm{NH}_4)_2\mathrm{HPO}_4 \to \mathrm{NH}_4\mathrm{H}_2\mathrm{PO}_4 + \mathrm{NH}_3\uparrow \tag{2}$$

$$\mathrm{NH}_4\mathrm{H}_2\mathrm{PO}_4 \to \mathrm{H}_3\mathrm{PO}_4 + \mathrm{NH}_3\uparrow \tag{3}$$

Crosslinking

For N-route, NH<sub>3</sub> was the main product released from the NCP during the pyrolysis process (Fig. 4). The generated NH<sub>3</sub> could be decomposed to free radicals such as NH2 and NH, etc., which could attack carbon substrate to form N-containing functional groups on the surface of resultant biochar (Table 3). Meanwhile, the generated NH<sub>3</sub> could produce pores through NH<sub>3</sub> diffusing through the carbon layers. It was reported that at lower temperature, the NH<sub>3</sub> molecule would react with carboxy in PBB to form amide. With temperature growing (from about 300 °C), carboxy started to be decomposed to phenolic compounds,40 resulting in the generation of anilines with the presence of NH<sub>3</sub>. When the temperature was higher (beyond 600 °C), more N species could be transformed to the functional groups with higher thermal stability like pyridinic N and pyrrolic N (Table 3). Furthermore, partial N atoms could enter into the internal structure of carbon to form graphitic N, or be oxidized by the generated P2O5, CO2 or/and H2O produced from the decomposition of phosphoric acid to form oxidized N,<sup>32</sup> when the temperature was about 900 °C (Table 3).

Furthermore, the  $CO_2$  and  $H_2O$  generated from the pyrolysis process could also act as the activators for biochar when temperature were higher than 700 °C. This further created pores for biochar, resulting in high porous structure for the samples prepared at high temperature, *i.e.* 900 °C in this study (Table 1).

Furthermore, the  $CO_2$  and  $H_2O$  generated from the pyrolysis process could also act as the activators for biochar when temperature were higher than 700 °C. This further created pores for biochar, resulting in high porous structure for the samples prepared at high temperature, *i.e.* 900 °C in this study (Table 1).

#### **Toluene adsorption**

The breakthrough curve, along with the adsorption capacity, of toluene by prepared biochar is shown in Fig. 6. Blank biochar (C-600 and C-900) presented poor toluene adsorption performance, with the adsorption capacity at 6.5 and 8.0 mg  $g^$ respectively. Compared with C-600 and C-900, the samples with NCPs addition took much longer time to approach breakthrough and exhibited higher adsorption capacities. For the biochar prepared at 600 °C, its breakthrough time of the NCPtreated biochar was in the order of AP-600 > UP-600 > APP-600, with their corresponding volumetric adsorption capacities as 144.0, 104.0 and 89.8 g L<sup>-1</sup>, respectively and mass adsorption capacity at 296.4, 175.9 and 245.8 mg  $g^{-1}$ , respectively. The biochar prepared at 900 °C presented higher toluene uptake compared with those at 600 °C, with volumetric adsorption capacities ranging from 122.5 to 164.5 g  $L^{-1}$  and mass adsorption capacities ranging from 364.1 to 496.2 mg  $g^{-1}$ . Notably, it can be seen that AP-treated biochar presented higher mass adsorption capacity, while UP-treated biochar showed higher volumetric adsorption capacity. This might be ascribed to their different bulk density and UP had higher bulk density than AP (Table S2<sup>†</sup>).

The results show that the toluene adsorption capacity of AP-900 (496.2 mg g<sup>-1</sup>) was markedly higher than those biochar reported in previous studies using biomass as carbon precursors.<sup>41,42</sup> Martinez de Yuso, *et al.*<sup>42</sup> reported that the highest toluene uptake was 2.75 mmol L<sup>-1</sup> (*i.e.* 25.3 mg g<sup>-1</sup>) for almond shell based activated carbon with  $S_{\text{BET}}$  at 1128 m<sup>2</sup> g<sup>-1</sup> and microporosity at 77.8%. Lillo-Ródenas *et al.*<sup>41</sup> found that wood based carbon using H<sub>3</sub>PO<sub>4</sub> as activation agent had the highest toluene uptake at 310 mg g<sup>-1</sup>, with  $S_{\text{BET}}$  at 1757 m<sup>2</sup> g<sup>-1</sup>. This demonstrated that the carbons prepared with NCPs in our study are desirable for toluene adsorption. Moreover, pore structure is

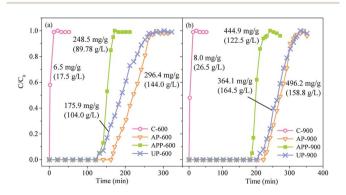


Fig. 6 The breakthrough curves of toluene by prepared biochar. (The numbers labelled beside the curve represented the toluene adsorption capacity of the relevant carbon).

not the only one factor contributing to such excellent adsorption behavior.

As shown in Table 3, there were some N-containing functional groups on the surface of the NCPs-treated biochar, which might lead to the desirable adsorption capability of toluene. On one hand, the NH<sub>3</sub> generated from NCPs could enhance the hydrophobicity of carbon during the pyrolysis of stillages, promoting its affinity to volatile organic compounds.<sup>15</sup> One the other hand, the addition of NCPs could help increase the content of basic functional groups, like pyridinic N, and pyrrolic N, on the carbon surface (Table 3), which could significantly increase the basicity of the carbon. The interaction of aromatic ring  $\pi$  electron of toluene with carbon could be enhanced by the increase of carbon basicity, due to the donoracceptor mechanism, resulting in higher toluene uptake.43,44 In addition, the empty bed residence time (EBRT) of the adsorption reactor in our study was 0.24 s, which was quite shorter than those for biological reactors (usually >5s).5,6 Thus, compared with biological method, adsorption exhibited extremely higher removal rate for toluene and could effectively decrease the volume of reactor, resulting in a lower area occupation.

## Conclusions

The results show that a novel N-doped biochar was prepared successfully using the stillage as the carbon precursor and different NCPs as the additives. The addition of NCPs could evidently increase the yield of biochar. All NCPs-treated biochar presented better pore structure than blank carbon, with higher  $S_{\text{BET}}$  for AP-added carbon, at 481 and 798 m<sup>2</sup> g<sup>-1</sup> for AP-600 and AP-900, respectively. Furthermore, the N atoms could be successfully doped on the surface of prepared biochar, with relatively high contents of N for AP-600, up to 4.16%. The pyridinic N and pyrrolic N were the main N species at 600 °C and partial N species was transformed to graphitic N and oxidized N at 900 °C. The interactions between plant-based biomass and NCPs could be divided into P route and N route, in which the generated H<sub>3</sub>PO<sub>4</sub> and NH<sub>3</sub> from NCPs played the dominant roles for the high yield N doped biochar. Moreover, the prepared biochar presented a desirable toluene adsorption behaviour, with the highest adsorption capacity at 496.2 mg  $g^{-1}$ for AP-900, which was ascribed to both abundant porous structure and N modified surface chemistry of the prepared biochar.

# Conflicts of interest

There are no conflicts to declare.

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**RSC** Advances

## References

- 1 H. Nigar, I. Julián, R. Mallada and J. Santamaría, *Environ. Sci. Technol.*, 2018, **52**, 5892–5901.
- 2 Y. Shu, Y. Xu, H. Huang, J. Ji, S. Liang, M. Wu and D. Y. C. Leung, *Chemosphere*, 2018, **208**, 550–558.
- 3 W. K. Pui, R. Yusoff and M. K. Aroua, *Rev. Chem. Eng.*, 2018, DOI: 10.1515/revce-2017-0057.
- 4 H. Wang, T. Wang, L. Han, M. Tang, J. Zhong, W. Huang and R. Chen, *J. Mater. Res.*, 2016, **31**, 516–525.
- 5 H. Chen, C. Yang, G. Zeng, S. Luo and G. Yu, *Bioresour. Technol.*, 2012, **121**, 199–204.
- 6 C. Yang, H. Qian, X. Li, Y. Cheng, H. He, G. Zeng and J. Xi, *Trends Biotechnol.*, 2018, **36**, 673–685.
- 7 J. Wang and C. Chen, Biotechnol. Adv., 2006, 24, 427-451.
- 8 J. Wang and C. Chen, Biotechnol. Adv., 2009, 27, 195.
- 9 S. Wu, H. He, X. Inthapanya, C. Yang, L. Lu, G. Zeng and Z. Han, *Environ. Sci. Pollut. Res. Int.*, 2017, 24, 1–18.
- 10 Y. Luo, Doctoral thesis, Tsinghua University, 2010.
- 11 J. Chen, J. Yang, G. Hu, X. Hu, Z. Li, S. Shen, M. Radosz and M. Fan, *ACS Sustainable Chem. Eng.*, 2016, **4**, 1439–1445.
- 12 A. R. Mohamed, M. Mohammadi and G. N. Darzi, *Renewable Sustainable Energy Rev.*, 2010, 14, 1591–1599.
- 13 J. H. Park, Y. S. Ok, S. H. Kim, J. S. Cho, J. S. Heo, R. D. Delaune and D. C. Seo, *Chemosphere*, 2016, **142**, 77–83.
- 14 N. Zhu, T. Yan, J. Qiao and H. Cao, *Chemosphere*, 2016, **164**, 32–40.
- 15 J. Mohammed, N. S. Nasri, M. A. Ahmad Zaini, U. D. Hamza and F. N. Ani, *Int. Biodeterior. Biodegrad.*, 2015, **102**, 245–255.
- 16 Y. Kan, Q. Yue, J. Kong, B. Gao and Q. Li, *Chem. Eng. J.*, 2015, 260, 541–549.
- 17 K. C. Bedin, A. C. Martins, A. L. Cazetta, O. Pezoti and V. C. Almeida, *Chem. Eng. J.*, 2016, **286**, 476–484.
- 18 M. A. Yahya, Z. Al-Qodah and C. W. Z. Ngah, Renewable Sustainable Energy Rev., 2015, 46, 218–235.
- 19 M. Seredych and T. J. Bandosz, *Energy Fuels*, 2008, 22, 850–859.
- 20 J. Song, W. Shen, J. Wang and W. Fan, *Carbon*, 2014, **69**, 255–263.
- 21 L. Fan, J. Chen, J. X. Guo, X. Jiang and W. J. Jiang, *J. Anal. Appl. Pyrolysis*, 2013, **104**, 353–360.
- 22 C. J. Zhang, D. N. Yang, X. Jiang and W. J. Jiang, *Environ. Technol.*, 2016, **37**, 1895–1905.
- 23 W. Xing, C. Liu, Z. Zhou, L. Zhang, J. Zhou, S. Zhuo, Z. Yan, H. Gao, G. Wang and S. Z. Qiao, *Energy Environ. Sci.*, 2012, 5, 7323–7327.

- 24 F. Sun, J. Gao, X. Liu, Y. Yang and S. Wu, *Chem. Eng. J.*, 2016, **290**, 116–124.
- 25 M. S. Shafeeyan, W. M. A. W. Daud, A. Houshmand and A. Shamiri, *J. Anal. Appl. Pyrolysis*, 2010, **89**, 143–151.
- 26 M. Myglovets, O. I. Poddubnaya, O. Sevastyanova, M. E. Lindström, B. Gawdzik, M. Sobiesiak, M. M. Tsyba, V. I. Sapsay, D. O. Klymchuk and A. M. Puziy, *Carbon*, 2014, 80, 771–783.
- 27 K. Li, Y. Li and Z. Zheng, J. Hazard. Mater., 2010, 178, 553–559.
- 28 W. Shen, S. Zhang, Y. He, J. Li and W. Fan, *J. Mater. Chem.*, 2011, **21**, 14036–14040.
- 29 R. Huang, H. Y. Liu, B. S. Zhang, X. Y. Sun, C. H. Liang, D. S. Su, B. N. Zong and J. F. Rong, *ChemSusChem*, 2014, 7, 3476–3482.
- 30 H. Guedidi, L. Reinert, J.-M. Lévêque, Y. Soneda, N. Bellakhal and L. Duclaux, *Carbon*, 2013, 54, 432–443.
- 31 F. Sun, J. Liu, H. Chen, Z. Zhang, W. Qiao, D. Long and L. Ling, ACS Catal., 2013, 3, 862–870.
- 32 C. L. Mangun, K. R. Benak, J. Economy and K. L. Foster, *Carbon*, 2001, **39**, 1809–1820.
- 33 A. M. Puziy, O. I. Poddubnaya, R. P. Socha, J. Gurgul and M. Wisniewski, *Carbon*, 2008, 46, 2113–2123.
- 34 H. Li, Master thesis, Inner Mongolia University of Science & Technology, 2013.
- 35 M. Saleh, J. N. Tiwari, K. C. Kemp, M. Yousuf and K. S. Kim, *Environ. Sci. Technol.*, 2013, **47**, 5467–5473.
- 36 X. Tian, M. Zhou, C. Tan, M. Li, L. Liang, K. Li and P. Su, *Chem. Eng. J.*, 2018, 775–785.
- 37 L. Tao, G.-B. Zhao, J. Qian and Y.-k. Qin, *J. Hazard. Mater.*, 2010, **175**, 754–761.
- 38 M. Jagtoyen and F. Derbyshire, Carbon, 1998, 36, 1085-1097.
- 39 M. A. Nahil and P. T. Williams, *Biomass Bioenergy*, 2012, 37, 142–149.
- 40 Y. Long, L. Ruan, X. Lv, Y. Lv, J. Su and Y. Wen, *Chin. J. Chem. Eng.*, 2015, 23, 1691–1697.
- 41 M. A. Lillo-Ródenas, A. J. Fletcher, K. M. Thomas, D. Cazorla-Amorós and A. Linares-Solano, *Carbon*, 2006, 44, 1455–1463.
- 42 A. Martinez de Yuso, M. T. Izquierdo, R. Valenciano and B. Rubio, *Fuel Process. Technol.*, 2013, **110**, 1–7.
- 43 Y. J. Tham, P. A. Latif, A. M. Abdullah, A. Shamala-Devi and Y. H. Taufiq-Yap, *Bioresour. Technol.*, 2011, **102**, 724–728.
- 44 N. Wibowo, L. Setyadhi, D. Wibowo, J. Setiawan and S. Ismadji, *J. Hazard. Mater.*, 2007, **146**, 237–242.