materials ISSN 1996-1944 www.mdpi.com/journal/materials

OPEN ACCESS

Review

Sorbate Transport in Carbon Molecular Sieve Membranes and FAU/EMT Intergrowth by Diffusion NMR

Robert Mueller¹, Rohit Kanungo¹, Amrish Menjoge¹, Mayumi Kiyono-Shimobe², William J. Koros², Steven A. Bradley³, Douglas B. Galloway³, John J. Low³, Sesh Prabhakar³ and Sergey Vasenkov^{1,*}

- ¹ Department of Chemical Engineering, University of Florida, Gainesville, FL 32611, USA; E-Mails: silveram@ufl.edu (R.M.); rohit.kanungo@ufl.edu (R.K.); amrishm@ufl.edu (A.M.);
- ² School of Chemical & Biomolecular Engineering, Georgia Institute of Technology, Atlanta, GA 30332, USA; E-Mails: mayumi.marbury@gmail.com (M.K.-S.); bill.koros@chbe.gatech.edu (W.J.K.)
- ³ UOP LLC, A Honeywell Company, 25 E. Algonquin Road, Des Plaines, IL 60017-5017, USA; E-Mails: steven.bradley@uop.com (S.A.B.); douglas.galloway@uop.com (D.B.G.); jlow@mcs.anl.gov (J.J.L.); sesh.prabhakar@uop.com (S.P.)
- * Author to whom correspondence should be addressed; E-Mail: svasenkov@che.ufl.edu; Tel.: +1-352-392-0315; Fax: +1-352-392-9513.

Received: 19 January 2012; in revised form: 9 February 2012 / Accepted: 10 February 2012 / Published: 14 February 2012

Abstract: In this paper we present and discuss selected results of our recent studies of sorbate self-diffusion in microporous materials. The main focus is given to transport properties of carbon molecular sieve (CMS) membranes as well as of the intergrowth of FAU-type and EMT-type zeolites. CMS membranes show promise for applications in separations of mixtures of small gas molecules, while FAU/EMT intergrowth can be used as an active and selective cracking catalyst. For both types of applications diffusion of guest molecules in the micropore networks of these materials is expected to play an important role. Diffusion studies were performed by a pulsed field gradient (PFG) NMR technique that combines advantages of high field (17.6 T) NMR and high magnetic field gradients (up to 30 T/m). This technique has been recently introduced at the University of Florida in collaboration with the National Magnet Lab. In addition to a more conventional proton PFG NMR, also carbon-13 PFG NMR was used.

Keywords: carbon molecular sieve; zeolite; FAU/EMT intergrowth; diffusion; NMR

1. Introduction

Detailed understanding of diffusion of guest molecules in microporous materials is important for numerous industrial applications, which include separations, catalysis, and detection of chemically or biologically important species. In this work we review results of our recent studies of sorbate self-diffusion in two types of microporous materials, *viz.* carbon molecular sieve (CMS) membranes and the intergrowth of FAU-type and EMT-type zeolites.

CMS membranes are amorphous microporous carbon materials formed by pyrolysis of polymer precursors. The pore system of CMS membranes consists of selective ultra-micropores (<6 Å) and slightly larger micropores (6–20 Å) [1,2]. Carbon molecular sieve membranes represent a promising class of materials for energy efficient separations of gas mixtures consisting of similarly sized molecules such as N_2/O_2 and CO_2/CH_4 due to the diffusion dominant process [3,4]. Selectivities of CMS membranes for such difficult separations approach those of zeolite and metal organic framework (MOF) membranes. At the same time, costs of large-scale fabrication of defect-free CMS membranes are expected to be much lower than those of zeolite and MOF membranes. CMS membranes are also less brittle than most zeolite and MOF membranes.

Previous experimental investigations of sorbate transport in CMS membranes have been performed using macroscopic techniques, which for the most part are based on membrane permeability measurements [2,5–7]. To our knowledge, until now microscopic studies of diffusion of light gases in a broad range of length scales inside CMS membranes were not reported. To fill this gap, we review our first data on sorbate self-diffusion on the micrometer and sub-micrometer length scales inside CMS membranes.

The other focus of this work is to review our recent results on sorbate self-diffusion in the intergrowth of FAU and EMT-type zeolites. Molecular transport in FAU-type zeolites has been extensively investigated using a number of experimental techniques. As a result, detailed data on intracrystalline diffusivities of different types of sorbate molecules are available for this zeolite [8,9]. At the same time, much less is known about diffusion properties of FAU/EMT intergrowth. The origin of the structural differences between FAU and EMT zeolites is related to the type of stacking of sodalite layers. In the FAU-type zeolite the stacking occurs in a ABCABC sequence, while in the EMT-type zeolite it occurs in a ABABAB sequence [10]. Figure 1 shows SEM image of a typical particle of FAU/EMT intergrowth used for diffusion studies. This particle can be described as a sandwich of several EMT-type blocks, which resemble thin hexagonal plates, and FAU-type blocks, which have a typical for this zeolite can be slowed down by reduced transport rates through the interfaces between FAU and EMT blocks. References [13–17] provide examples of the observation of a similar decrease of the effective diffusivities inside zeolite crystals due to the existence of intracrystalline defects and the resulting transport barriers.



Figure 1. SEM image of a representative particle of FAU/EMT intergrowth.

Microscopic diffusion studies in CMS membranes and FAU/EMT intergrowth were carried out by high field and high gradient PFG NMR. The diffusion measurements were performed at different temperatures and for different diffusion times corresponding to different mean square displacements (MSDs) of sorbate molecules. The results reported below demonstrate that these measurements show high potential for uncovering the relationship between structural properties and transport in materials with a complex micropore structure.

2. Details of PFG NMR Measurements and Data Processing

Diffusion studies were performed by proton and carbon-13 PFG NMR using a wide-bore 17.6 T Bruker BioSpin spectrometer. Magnetic field gradients with the amplitude up to 30 T/m were generated using Diff60 diffusion probe and Great60 gradient amplifier (Bruker BioSpin). The use of high field affords high sensitivity and the ability to apply high gradients allows the possibility to measure self-diffusion coefficients of sorbate molecules in micropores on small (*i.e.*, sub-micrometer) length scales of molecular displacements.

Diffusion measurements were carried out using the 13-interval PFG NMR sequence with bipolar gradients [18] and the PFG NMR stimulated echo sequence with the longitudinal eddy current delay (PGSTE LED) [19]. The former sequence allows reducing or even completely eliminating the disturbing influence of magnetic susceptibility effects. Susceptibility effects are expected for heterogeneous porous materials such as stacks of membrane pieces and zeolite beds studied in this work. The advantage of the latter sequence is related to the possibility of reducing influence of the transverse (T_2) NMR relaxation on the measured signal. Such reduction is achieved by keeping short the sequence time intervals during which this relaxation process reduces the measured signal. For PGSTE LED sequence the absence of disturbing susceptibility effects and other measurement artifacts was confirmed by using the following two strategies: (i) it was verified that proton and carbon-13 PFG NMR diffusion data measured for the same diffusing species in the same samples and under the same conditions

coincide within the experimental uncertainty, and (ii) it was checked that an increase of the time interval between the first and second $\pi/2$ radiofrequency pulses of PGSTE LED sequence (while keeping the effective diffusion time constant) does not change the measured diffusivities.

¹³C PFG NMR was employed in addition to the more traditional ¹H PFG NMR to take advantage of the longer ¹³C longitudinal (T_1) and transverse (T_2) relaxation times than those typically observed for protons of guest molecules confined in nanopores. An increase in the former relaxation time allows measurements in a broader range of diffusion times and hence broader range of MSDs, while an increase in the later significantly improves the strength of the measured PFG NMR signal. Due to the small gyromagnetic ratio (γ) of carbon-13 (about ¹/₄ of proton), the advantages of using high field and high gradients are especially important because a reduction in γ is expected to lead to reductions in the signal-to-noise ratio of an NMR signal as well as in the smallest length scale of molecular displacements for which PFG NMR diffusion measurements are still possible.

The 13-interval and PGSTE LED sequences were used to measure PFG NMR attenuation curves, *i.e.*, dependencies of the intensity of PFG NMR signal (A) on the amplitude of the magnetic field gradient (g). The signal intensity was obtained by measuring amplitude of NMR lines of the sorbate molecules or area under these lines. The proton and carbon-13 NMR spectra of each type of sorbate consisted of a single line. It was verified that within the experimental uncertainty the line shape does not depend on the gradient amplitude. The PFG NMR attenuation curves provide direct information on effective diffusivities. Effective diffusivities D_i were obtained from monoexponential or biexponential fit of the PFG NMR attenuation curves using:

$$\Psi = \frac{A(g)}{A(g=0)} = \sum_{i=1}^{n=10r^2} p_i \exp\left(-\frac{1}{6}q^2 \langle r_i^2(t) \rangle\right) = \sum_{i=1}^{n=10r^2} p_i \exp\left(-q^2 t D_i\right)$$
(1)

where $q = \gamma \delta g$ for PGSTE LED sequence and $q = 2\gamma \delta g$ for the 13-interval sequence, γ is the gyromagnetic ratio, δ denotes the duration of the field gradient pulses, and t_{eff} is the effective diffusion time which corresponds to the diffusion time (or observation time) in a PFG NMR experiment. $\langle r_i^2(t) \rangle$

and p_i denote, respectively, the mean square displacement (MSD) and fraction of sorbate molecules diffusing with a diffusivity D_i . Monoexponential behavior (n = 1 in Equation (1)) corresponds to the situation when all molecules under study diffuse with a single effective diffusivity. In the case of biexponential behavior (n = 2 in Equation (1)) there are two ensembles of molecules diffusing with two different diffusivities. The expression in the right-hand part of Equation (1) was obtained using the Einstein relation:

$$\left\langle r_i^2(t) \right\rangle = 6D_i t. \tag{2}$$

values of δ and t_{eff} were kept constant for measurement of each attenuation curve.

3. Results and Discussion

3.1. Methane Self-Diffusion in CMS Membranes

Methane self-diffusion was investigated by PFG NMR in the following three carbon molecular sieve membrane samples: 6FDA/BPDA(1:1)-DAM CMS pyrolized in an inert gas (6FDA/BPDA),

Matrimid[®] CMS pyrolized in an inert gas (Matrimid Sample 1), and Matrimid[®] CMS pyrolized under vacuum (Matrimid Sample 2). Diffusion data was obtained using combined application of proton and carbon-13 PFG NMR. It was observed that in all cases the PFG NMR attenuation curves show monoexponential behavior in agreement with Equation (1), n = 1 (Figure 2). This indicates that under any given measurement conditions used there is no significant distribution over methane self-diffusion coefficient inside membrane pieces of each studied membrane sample. It is important to note that under our experimental conditions the diffusivity of methane in the gas phase of the samples is expected to be at least four orders of magnitude larger than that inside the membranes. This estimate was confirmed by our direct PFG NMR measurements. As a result, the PFG NMR signal from methane in the gas phase was completely attenuated when the smallest (non-zero) gradient was used in the measurements of the PFG NMR attenuation curves shown in Figure 2. It was also observed that the diffusion data for methane measured under the same conditions by ¹H and ¹³C PFG NMR were identical within the experimental uncertainty. Figure 2 shows an example of such data. In the presentation of this figure the proton and carbon-13 PFG NMR attenuation curves measured for diffusion of ¹³C-labeled CH₄ have to coincide to reveal the same diffusion behavior. Such coincidence is evident in the figure. The observed agreement between the diffusivities measured at very different resonance frequencies of 750 and 188.6 MHz corresponding, respectively, to ¹H and ¹³C nuclei provide strong evidence that the reported diffusion data are not distorted by magnetic susceptibility effects or by any other disturbing effects.

Figure 2. Examples of PFG NMR attenuation curves measured for methane diffusion in 6FDA/BPDA using proton (**■**) and carbon-13 (**●**) PFG NMR. The measurements were performed for the effective diffusion time of 9 ms at T = 321 K. The 13-interval and PGSTE LED PFG NMR pulse sequences were used for proton and carbon-13 measurements, respectively. The line shows the result of fitting both attenuation curves by Equation (1) with n = 1.



Table 1 shows the methane diffusivities and the corresponding values of root MSD obtained by fitting the measured PFG NMR attenuation curves by Equation (1) (n = 1) and Equation (2). The diffusion data are reported for the broad range of temperatures and effective diffusion times used in this study. In all cases the reported values of root MSD were at least 5 times smaller than the smallest

dimension (*i.e.*, thickness) of the membrane pieces. Hence, the measured diffusivities correspond to intra-membrane diffusion under conditions when the boundaries of the membrane pieces are not expected to influence the diffusion behavior. In this case it is not expected to observe any measurable fraction of methane molecules performing long-range diffusion, *i.e.*, diffusion under conditions of fast exchange of methane molecules between the membrane pieces and the surrounding gas phase. It is seen in Table 1 that within the experimental uncertainty the intra-membrane diffusivities of methane do not change with increasing values of the root MSD. This is illustrated in Figure 3 which presents examples of the measured dependencies of the studied membranes remain homogeneous over a broad range of length scales starting with the length scales as small as 600 nm to as large as 14 μ m which is comparable with the membrane thickness of 60 ± 10 μ m.

Table 1. Data for methane self-diffusion in: (a) 6FDA/BPDA, and (b) Matrimid Samples 1 and 2. Self-diffusion coefficients and the corresponding values of the root MSD were obtained from fitting PFG NMR attenuation curves measured for methane diffusion at different temperatures (*T*) and effective diffusion times (t_{eff}) by Equation (1) with n = 1 and Equation (2). The data obtained by ¹³C PFG NMR is labeled by (*). All other data was obtained by ¹H PFG NMR.

Sample	<i>T</i> (K)	t_{eff} (ms)	$D (m^2 \cdot s^{-1})$	Root MSD (µm)
		9	$(1.4 \pm 0.2) \times 10^{-10}$	2.7 ± 0.2
		9	$(1.2 \pm 0.2) \times 10^{-10} *$	2.6 ± 0.2
		19	$(1.3 \pm 0.2) \times 10^{-10}$	3.8 ± 0.3
		19	$(1.3 \pm 0.2) \times 10^{-10}$ *	3.8 ± 0.3
	207	29	$(1.4 \pm 0.2) \times 10^{-10}$ *	4.9 ± 0.3
	297	39	$(1.2\pm0.2) imes10^{-10}$	5.3 ± 0.4
		39	$(1.2 \pm 0.2) \times 10^{-10}$ *	5.3 ± 0.4
		79	$(9.5 \pm 1.3) \times 10^{-11} *$	6.7 ± 0.5
		159	$(9.8 \pm 1.4) \times 10^{-11} *$	9.7 ± 0.7
		319	$(1.1 \pm 0.1) \times 10^{-10} *$	14.0 ± 1.0
(EDA/DDDA loaded	319	9	$(1.7\pm0.2) imes10^{-10}$	3.0 ± 0.2
orDA/BPDA loaded		9	$(1.7 \pm 0.2) \times 10^{-10}$ *	3.0 ± 0.2
with methane		19	$(1.5 \pm 0.2) \times 10^{-10}$	4.1 ± 0.3
		39	$(1.4 \pm 0.2) \times 10^{-10}$	5.7 ± 0.4
		39	$(1.5 \pm 0.2) \times 10^{-10}$ *	5.9 ± 0.4
	340	9	$(2.2\pm0.3) imes10^{-10}$	3.4 ± 0.2
		9	$(2.1 \pm 0.3) \times 10^{-10}$	3.4 ± 0.2
		19	$(2.2\pm0.3) imes10^{-10}$	5.0 ± 0.3
		39	$(2\pm0.3) imes10^{-10}$ *	6.8 ± 0.5
	252	9	$(2.7\pm0.4) imes10^{-10}$	3.8 ± 0.3
		9	$(2.8\pm0.4) imes10^{-10}$ *	3.9 ± 0.3
	333	19	$(2.6\pm0.4) imes10^{-10}$	5.4 ± 0.4
		39	$(2.4\pm0.3) imes10^{-10}$	7.5 ± 0.5

(a)

(D)						
Sample	<i>T</i> (K)	t_{eff} (ms)	$D (m^2 \cdot s^{-1})$	Root MSD (µm)		
	297	9	$(6.5 \pm 1.3) \times 10^{-12}$	0.6 ± 0.06		
		19	$(4.6 \pm 0.9) \times 10^{-12}$	0.7 ± 0.1		
Matuinid		39	$(6.2 \pm 1.2) \times 10^{-12}$	1.2 ± 0.1		
Sample 1 loaded with methane		79	$(4.7 \pm 1) \times 10^{-12}$	1.5 ± 0.2		
		159	$(4 \pm 0.9) \times 10^{-12}$	2.0 ± 0.2		
		359	$(4 \pm 1) \times 10^{-12}$	2.9 ± 0.4		
	339	9	$(9.4 \pm 2) \times 10^{-12}$	0.7 ± 0.07		
	356	9	$(1.2 \pm 0.2) \times 10^{-11}$	0.8 ± 0.05		
Matrimid Sample 2 loaded with methane	297	9	$(7.5 \pm 1.5) \times 10^{-12}$	0.6 ± 0.1		
		39	$(6.4 \pm 1.3) \times 10^{-12}$	1.2 ± 0.1		
	336	9	$(8.5 \pm 1.5) \times 10^{-12}$	0.7 ± 0.1		
	356	9	$(1.3 \pm 0.2) \times 10^{-11}$	0.8 ± 0.1		

Table 1. Cont.

- 1	L \	
•	\mathbf{v}_{i}	

Figure 3. Dependences of the methane self-diffusion coefficient on the root MSD at T = 297 K for 6FDA/BPDA (\blacksquare), Matrimid Sample 1 (\bullet), and Matrimid Sample 2 (\checkmark). The data was obtained using Equation (1) with n = 1 and Equation (2).



The temperature dependence of the methane self-diffusivities in the three membrane samples is shown in Figure 4. For each sample, the temperature dependence was found to be in agreement with an Arrhenius law

$$D(T) = D_0 \exp\left(-E_a / RT\right) \tag{3}$$

where E_a is the apparent activation energy of diffusion. Application of Equation (3) to the measured data yields the following activation energies: 8 kJ/mol for 6FDA/BPDA and 10 kJ/mol for Matrimid Sample 1 and Matrimid Sample 2. The experimental uncertainty of these values was estimated to be in the range of a factor of 2.

It is seen in Table 1 and Figure 4 that under the same or similar measurement conditions the methane self-diffusivity in 6FDA/BPDA is about an order of magnitude larger than that in both Matrimid samples. At the same time, in all three samples the activation energy for methane diffusion was found to be the same within the experimental uncertainty. This observation can be explained by assuming that 6FDA/BPDA has a higher relative abundance of sufficiently large pores permeable to methane than the Matrimid samples. This is in agreement with the data on permeation experiments conducted on these membrane types and with the data analysis reported in references [5,20]. In a qualitative agreement with the self-diffusion data reported in Table 1 the permeation experiments yielded the effective transport diffusivities of methane that are much lower in Matrimid[®] type CMS than in 6FDA/BPDA type CMS [5]. The quantitative comparison of the transport diffusivities with the self-diffusivities reported in this work cannot be done easily because the transport diffusivities represent the effective (average) values over a broad range of methane loadings in the membranes corresponding to a large methane pressure difference (around 50 psia) between the feed side and the permeate side of the membranes. Hence, both the thermodynamic factor and loading dependence of diffusivity are expected to contribute to the difference between the transport and self-diffusivity values [8,9].

Figure 4. Temperature dependences of the methane self-diffusion coefficient measured by PFG NMR for the effective diffusion time 9 ms in 6FDA/BPDA (■), Matrimid Sample 1 (●), and Matrimid Sample 2 (▼). Lines show the fit to the Arrehenius law (Equation (3)).



3.2. Self-Diffusion of Isooctane in FAU/EMT Intergrowth

Figure 5a shows examples of the PFG NMR attenuation curves measured for isooctane diffusion in the FAU/EMT intergrowth for different effective diffusion times at 264 K. In the presentation of this figure the initial parts of the attenuation curves measured for different effective diffusion times have to coincide if the effective diffusion time. The data in Figure 5a show that the initial slope of the attenuation curves decreases with increasing effective diffusion time. This indicates that the effective diffusivity of isooctane decreases as the diffusion time increases. The shape of the attenuation curves in the figure is relatively close to mono-exponential in agreement with Equation (1), n = 1. The results of fitting of the initial parts of the attenuation curves in Figure 5a by this equation are shown in the figure and also given in Table 2. It is important to note that while the effective diffusivity continuously decreases with increasing diffusion time, the values of the root MSD remain independent of diffusion time within the experimental uncertainty (Table 2). The latter values are much smaller than the characteristic size of the particles of the FAU/EMT intergrowth (around 2.8 microns). At the same

time, the root MSD values are comparable with the sizes of the individual FAU and EMT blocks forming these particles. Figure 1 shows that the block sizes are between around 0.1 and 1 micron.

Figure 5. (a) Proton PFG NMR attenuation curves measured by the 13-interval PFG NMR sequence for diffusion of isooctane in the FAU/EMT intergrowth at T = 264 K for the following effective diffusion times: 6.0 ms (**•**), 10.5 ms (**•**), 20.5 ms (**▲**), and 40.5 ms (**▼**). The lines show the initial slopes of the attenuation curves; (**b**) Proton PFG NMR attenuation curves measured by the 13-interval PFG NMR sequence for diffusion of isooctane in the FAU/EMT intergrowth at T = 289 K for the following effective diffusion times: 5.7 ms (**•**), 10.2 ms (**•**), 40.1 ms (**▼**), 80.1 ms (**□**), and 120.1 ms (**○**). The lines show the best fit curves of the measured data by Equation (1) with n = 2.



Table 2. Results of fitting of the initial parts of the attenuation curves in Figure 5a by Equation (1), n = 1 and the corresponding effective diameters of the particle components surrounded by transport barriers (d_{eff}) . The values of d_{eff} were obtained by using Equation (4).

Sample	<i>T</i> (K)	$t_{\rm eff}$ (ms)	$D_{eff} (\mathrm{m}^2 \cdot \mathrm{s}^{-1})$	Root MSD (µm)	d_{eff} (µm)
FAU/EMT		6.0	$(1.6 \pm 0.2) \times 10^{-12}$	0.24 ± 0.2	0.44 ± 0.4
intergrowth	264	10.5	$(9.0 \pm 1.4) \times 10^{-13}$	0.24 ± 0.2	0.44 ± 0.4
loaded with	204	20.5	$(5.7 \pm 0.9) \times 10^{-13}$	0.26 ± 0.2	0.48 ± 0.5
isooctane		40.5	$(2.7 \pm 0.4) \times 10^{-13}$	0.26 ± 0.2	0.48 ± 0.5

These results can be explained by assuming transport barriers at the interfaces between intergrowth components in the particles of the FAU/EMT intergrowth. These barriers are essentially impermeable for isooctane molecules for diffusion times up to 41 ms at 264 K, as indicated by the unchanging values of the root MSD in Table 2. An existence of a distribution over the sizes of the particle components surrounded by the transport barriers explains small deviations of the PFG NMR attenuation curves in Figure 5a from the monoexponential behavior [8]. Assuming that all particle components separated by the transport barriers can be approximated by spheres with the diameter d_{eff} , the following expression can be used to estimate the value of d_{eff} [8,21,22].

$$D_{eff} = \frac{\left\langle r(t)^2 \right\rangle}{6t} = \frac{d_{eff}^2}{20t} \tag{4}$$

Table 2 presents the values of d_{eff} that were obtained using Equation (4). It is seen that these values obtained for different diffusion times are all the same within the experimental uncertainty. The values of d_{eff} characterize the mean size of the particle components surrounded by the transport barriers. This size is found to be within the range of the observed sizes of the intergrowth components (Figure 1). Hence, these data indicate that the intergrowth components are surrounded by the observed transport barriers.

Figure 5b shows examples of the measured PFG NMR attenuation curves for isooctane in the FAU/EMT intergrowth at a higher temperature of 289 K. It is seen in Figure 5b that the attenuation curves at large diffusion times show fast initial decay, which is followed by much slower signal attenuation at larger gradient strengths. The onset of the slow attenuation of the diffusion process from the intraparticle to long-range regimes as diffusion time increases [8]. In the former regime sorbate displacements are smaller than or comparable with the particle sizes, while in the latter regime these displacements are larger than the particle sizes. As a result, with increasing diffusion time the fraction of molecules corresponding to intraparticle diffusion is expected to decrease, while that corresponding to intraparticle diffusion is expected to decrease, while that corresponding to intraparticle (slow attenuation) and long-range (fast attenuation) diffusion can be obtained from the biexponential fit of the attenuation curves (Equation (1) with n = 2). Table 3 presents the resulting diffusivities and molecular fractions for intraparticle diffusion (D_2 and p_2) and for long-range diffusion (D_1 and p_1).

Table 3. Results of fitting of the PFG NMR attenuation curves measured for isooctane diffusion in the FAU/EMT intergrowth at T = 289 K by Equation (2) with n = 2. The intraparticle diffusivities (D_2) were obtained from the attenuation curves measured at the extended gradient range (not shown in Figure 5). Star (*) indicates values with a large (in the range of a factor of 2–4) experimental uncertainty.

Sample	<i>T</i> (K)	t_{eff} (ms)	$D_1 (\mathbf{m}^2 \cdot \mathbf{s}^{-1})$	<i>p</i> ₁	Root MSD 1 (µm)	$D_2 (\mathbf{m}^2 \cdot \mathbf{s}^{-1})$	P_2	Root MSD 2 (µm)
		5.7	4×10^{-9} *	0.1 ± 0.07	11 *	$(3.5\pm 0.5)\times 10^{-12}$	0.9 ± 0.07	0.34 ± 0.02
FAU/EMT		10.2	2×10^{-9} *	0.1 ± 0.07	11 *	$(2.5\pm 0.4)\times 10^{-12}$	0.9 ± 0.07	0.39 ± 0.03
intergrowth	289	40.1	$(6 \pm 3) \times 10^{-9}$	0.5 ± 0.1	39 ± 10	$(1.5\pm 0.2)\times 10^{-12}$	0.5 ± 0.1	0.43 ± 0.03
loaded with		80.1	$(1.1 \pm 0.3) \times 10^{-8}$	0.7 ± 0.1	74 ± 11	$(4.0\pm 0.6)\times 10^{-13}$	0.3 ± 0.1	0.44 ± 0.04
isooctane		120.1	$(1.3 \pm 0.5) \times 10^{-8}$	0.8 ± 0.1	96 ± 20	$(3.5\pm 0.5)\times 10^{-13}$	0.2 ± 0.1	0.34 ± 0.02

It is seen in the table that within the experimental uncertainty the values of long-range diffusivities (D_1) do not depend on diffusion time. At the same time, the fraction of molecules (p_1) corresponding to long-range diffusion increases significantly with increasing diffusion time. This is an expected behavior for the transition from the intraparticle to long-range diffusion regime with increasing diffusion time [8]. Also, in agreement with the assignment of the ensemble 1 to molecules exhibiting long-range diffusion, the values of the root MSD for this ensemble (Table 3) are larger than the

characteristic size of the particles of the FAU/EMT intergrowth (~2.8 µm). For diffusion in zeolite beds the long-range diffusivity often can be estimated (in the first approximation) as the diffusivity in the gas phase of the bed multiplied by the fraction of diffusing molecules located in the gas phase of the bed at any particular point of time. As a result, the values of long-range diffusivities can be several orders of magnitude larger than those for diffusion inside zeolite particles [8]. It is seen in Table 3 that the effective intraparticle diffusivities continuously decrease with increasing diffusion time. This shows that also at a higher temperature of 289 K the intraparticle diffusion of isooctane has a mostly restricted character. The values of the root MSD obtained for this diffusion process increase slowly with increasing diffusion time. Hence, in contrast to the behavior observed at 264 K, under our measurement conditions at 289 K isooctane molecules show an ability to gradually penetrate through the intraparticle transport barriers. The latter is also manifested by the existence of the molecular fraction exhibiting long-range diffusion. The dependence of this fraction on diffusion time shown in Table 3 allows estimating the permeability can be obtained in the framework of the tracer desorption technique [8] by estimating the value of the intraparticle mean life time (τ_{intra}):

$$\tau_{intra} = \int_{0}^{\infty} (1 - p_1(t_{eff})) dt_{eff}, \qquad (5)$$

where, in addition to the values of p_1 given in Table 3, one can use that $p_1(0) = 0$ and $p_1(\infty) = 1$. The value of τ_{intra} can be estimated using Equation (5) and taking into account that for the tracer exchange processes strongly influenced by the penetration through the transport barriers $p_1(t_{eff}) \approx 1 - \exp\left(-\frac{t_{eff}}{\tau_{intra}}\right)$

[8]. Using this expression it was found that $\tau_{intra} = 104 \pm 10$ ms at 289 K. The intraparticle mean life time is related to the corresponding permeability (k_p) of the transport barriers [8], which separate the particle components with the characteristic diameters equal to d_{eff}

$$\tau_{intra} \ge \frac{d_{eff}}{6k_p} \tag{6}$$

This relation is justified by the expectation that on their way out of the zeolite particles isooctane molecules have to cross over at least one of the transport barriers separating the particle components with the characteristic diameter d_{eff} . Using Equation (6) we find $k_p \ge 0.8 \times 10^{-6}$ m/s at 289 K.

It is of interest to compare intraparticle diffusivities of isooctane in the FAU/EMT intergrowth with the corresponding diffusivities in the pure FAU and pure EMT zeolites. Clearly, in the particles of the pure zeolites there is no intergrowth of different zeolite types and no corresponding transport barriers at the interfaces between alternating FAU and EMT blocks. PFG NMR diffusion measurements of isooctane diffusion in the pure zeolites were performed using the 13-interval PFG NMR. The results of these measurements are shown in Table 4. These values were obtained in the same way as discussed above by fitting the measured PFG NMR curves using Equation (1) with n = 2 for a transition range between the intraparticle and long-range diffusion. The data for the pure zeolites were obtained at the same or comparable temperatures as those used in the studies of the FAU/EMT intergrowth. In all cases no dependence of the intraparticle diffusivities on diffusion time was observed for the pure zeolite samples. The lack of such dependence indicates that for the measured range of the root MSDs

there are no significant diffusion restrictions by transport barriers inside the particles of the pure zeolite samples. The isooctane diffusivity in the FAU-type zeolite was found to be in a good agreement with the previously reported data [23]. The effective intraparticle diffusivities of isooctane in the FAU and EMT samples were found to be significantly higher than that in the FAU/EMT intergrowth for large diffusion times at 264 K (compare data in Tables 2 and 4). Clearly, this is in agreement with the conclusion that the isooctane diffusion in the FAU/EMT intergrowth at 264 K is strongly influenced by the intraparticle transport resistances resulting in lower effective intraparticle diffusivities in the intergrowth in comparison to those in the pure zeolites.

Table 4. Intracrystalline diffusivities of isooctane in the FAU and EMT zeolites. The diffusivities were obtained for the shown range of the effective diffusion times and the corresponding values of the root MSD by fitting the measured PFG NMR attenuation curves using Equation (1) with n = 2.

Sample	<i>T</i> (K)	$D (\mathrm{m}^2 \cdot \mathrm{s}^{-1})$	t_{eff} (ms)	Root MSD (µm)
FAU loaded with isooctane	266	$(3.7\pm0.7)\times10^{-12}$	9.5-39.5	0.5-0.9
EMT loaded with isooctane	264	$(1.7 \pm 0.3) \times 10^{-12}$	9.2-39.2	0.3-0.6

It is quite likely that the intraparticle transport barriers, which are reported in this paper, are located at the interfaces between intergrowth components of the FAU/EMT intergrowth. Similar intracrystalline transport barriers were observed previously in other zeolite types [13–16]. It can be assumed that the reason for the existence of the barriers is a partial blockage of the channel openings at the interfaces. Such assumption is in agreement with the observed reduction of the influence of the transport barriers on the overall diffusion process due to temperature increase. In the opposite case of temperature independent transport barriers a few channel or pore openings are expected to be free of any defects, while the remaining openings are completely blocked for diffusing molecules [24,25].

The data in Table 4 show that the value of the intraparticle diffusivity of isooctane in the FAU zeolite is approximately a factor of two higher than that in the EMT zeolite. This observation correlates with the fact that the size of the channels connecting cages is somewhat smaller in the latter zeolite than in the former [10]. For relatively bulky molecules, including isooctane, such difference in the channel sizes can be a reason of a slower diffusion in the EMT zeolite in comparison to that in the FAU zeolite.

4. Samples

4.1. CMS Membranes

The carbon molecular sieve membranes used in this study were synthesized as described in references [1,5,20]. To briefly summarize, the CMS membranes were formed by synthesis of precursor polymer films and subsequent pyrolysis of the films under carefully controlled conditions. The precursor copolymers used were 6FDA/BPDA-DAM, synthesized in house, with a ratio of 6FDA to BPDA of 1:1 and commercially available Matrimid[®] (Huntsman). Both are high molecular weight polyimides and have relatively high glass transition temperatures of over 500 K [5,26]. All membranes were pyrolyzed at 823 K in the following prescribed pyrolysis atmospheres: inert Ar atmosphere with <1 ppm of O_2 for 6FDA/BPDA and Matrimid Sample 1, and under vacuum for Matrimid Sample 2.

It was recently demonstrated that the presence of oxygen in the pyrolysis atmosphere can lead to more selective and less permeable ultra-micropores to form in the resulting CMS membranes [1,5,20,26].

4.2. Zeolite Samples

The EMT-type zeolite was synthesized as described in [27] using 18-Crown-6 as template. The FAU-type zeolite was formed using a procedure similar to that reported in [28]. The starting materials in the synthesis of the latter zeolite were sodium silicate, sodium aluminate, sodium hydroxide, and water. Synthesis of the FAU/EMT intergrowth was performed using mixed templates of 18-crown-6 and 15-crown-5. The Si-to-Al-ratio calculated from the inductively coupled plasma mass spectrometry (ICP) data ranged from 3 to 6. Powder XRD was used to confirm the formation of the zeolites.

4.3. Preparation of Samples for PFG NMR Studies

PFG NMR samples were prepared as follows. Around 200 mg of zeolite, or between 20 and 40 mg of membrane pieces were introduced into 5 mm NMR tubes. The NMR tubes were connected to a custom-made vacuum system and the samples were activated (*i.e.*, made sorbate-free) by applying a high vacuum at an elevated temperature for at least 24 hours. Sorbate loading was performed after sample activation by exposing the microporous samples to the desired sorbate pressure for at least 4 hours at 298 K. Upon loading, the NMR tube was flame sealed and separated from the vacuum system.

For all CMS membrane samples, high purity methane (99+%, Sigma-Aldrich) was loaded at a pressure of 0.5 bar. To increase the signal to noise ratio in the ¹³C PFG NMR measurements, methane with 99% carbon-13 isotopic enrichment was used.

For all zeolite samples the loading pressure of isooctane was equal to 50 mbar. This resulted in the following sorbate concentrations at 298 K: 182 mg/g for the FAU/EMT intergrowth, 229 mg/g for the FAU zeolite, and 207 mg/g for the EMT zeolite. These loadings were estimated by using the isooctane adsorption isotherms (not shown) measured for the three zeolites at 298 K.

5. Conclusions

This review demonstrates the high potential of multinuclear PFG NMR at high field and high gradients for obtaining detailed understanding of sorbate transport in microporous materials relevant for applications in separations and catalysis. In particular, comparison of self-diffusion coefficients and activation energies of diffusion observed for the same sorbate in the three carbon molecular sieve membrane samples allowed a deeper understanding of the differences in the pore structure of these samples. The reported PFG NMR data also shows a high degree of uniformity of the membrane transport properties and the related structural properties in a broad range of length scales between a fraction of a micrometer and more than 10 microns. Diffusion studies of FAU/EMT intergrowth and the comparison of the results of these studies with the corresponding transport properties of the pure FAU- and EMT-type zeolites revealed the existence of strong transport barriers inside particles of the intergrowth. These barriers can be formed as a result of a partial blockage of the channel openings at the interfaces between the intergrowth components of the FAU/EMT particles.

Acknowledgments

We are grateful for the financial support of the work related to studies of CMS membranes by the NSF CAREER award (CBET No. 0951812). We are also grateful to UOP for the financial support of the reported studies of zeolites. NMR data was obtained at the Advanced Magnetic Resonance Imaging and Spectroscopy (AMRIS) facility in the McKnight Brain Institute of the University of Florida. The NMR measurement time provided in the framework of the external user program of the National High Magnetic Field laboratory, AMRIS is gratefully acknowledged. Members of the Vasenkov Group would especially like to thank Dan Plant at AMRIS for his help with NMR measurements.

References

- 1. Kiyono, M.; Williams, P.J.; Koros, W.J. Effect of pyrolysis atmosphere on separation performance of carbon molecular sieve membranes. *J. Membr. Sci.* **2010**, *359*, 2–10.
- Suda, H.; Haraya, K. Gas permeation through micropores of carbon molecular sieve membranes derived from kapton polyimide. J. Phys. Chem. B 1997, 101, 3988–3994.
- 3. Ismail, A.F.; David, L.I.B. A review on the latest development of carbon membranes for gas separation. *J. Membr. Sci.* 2001, *193*, 1–18.
- 4. Bernardo, P.; Drioli, E.; Golemme, G. Membrane gas separation: A review/state of the art. *Ind. Eng. Chem. Res.* **2009**, *48*, 4638–4663.
- 5. Kiyono, M.; Williams, P.J.; Koros, W.J. Effect of polymer precursors on carbon molecular sieve structure and separation performance properties. *Carbon* **2010**, *48*, 4432–4441.
- Koresh, J.E.; Soffer, A. Mechanism of permeation through molecular-sieve carbon membrane. Part 1—The effect of adsorption and the dependence on pressure. J. Chem. Soc. Faraday Trans. I 1986, 82, 2057–2063.
- Tin, P.S.; Chung, T.S.; Liu, Y.; Wang, R. Separation of CO₂/CH₄ through carbon molecular sieve membranes derived from P84 polyimide. *Carbon* 2004, *42*, 3123–3131.
- 8. Kärger, J.; Ruthven, D.M. *Diffusion in Zeolites and Other Microporous Solids*; Wiley & Sons: New York, NY, USA, 1992.
- 9. Auerbach, S.M.; Carrado, K.A.; Dutta, P.K. *Handbook of Zeolite Science and Technology*; Marcel Dekker, Inc.: New York, NY, USA; Basel, Switzerland, 2003; pp. 341–423.
- 10. Baerlocher, C.; McCusker, L.B.; Olson, D.H. *Atlas of Zeolite Framework Types*, 6th ed.; Elsevier: Amsterdam, The Netherlands, 2007; p. 404.
- Slater, B.; Ohsuna, T.; Liube, Z.; Terasaki, O. Insights into the crystal growth mechanisms of zeolites from combined experimental imaging and theoretical studies. *Faraday Discuss.* 2007, 136, 125–141.
- 12. Belandria, L.N.; Gonzalez, C.S.; Aguirre, F.; Sosa, E.; Uzcategui, A.; Gonzalez, G.; Brito, J.; Gonzalez-Cortes, S.L.; Imbert, F.E. Synthesis, characterization of FAU/EMT intergrowths and its catalytic performance in n-pentane hydroisomerization reaction. *J. Mol. Catal. A* **2008**, *281*, 164–172.
- Geier, O.; Vasenkov, S.; Lehmann, E.; Kärger, J.; Schemmert, U.; Rakoczy, R.A.; Weitkamp, J. Interference microscopy investigation of the influence of regular intergrowth effects in MFI-type zeolites on molecular uptake. *J. Phys. Chem. B* 2001, *105*, 10217–10222.

- Vasenkov, S.; Karger, J. Evidence for the existence of intracrystalline transport barriers in MFI-type zeolites: A model consistency check using MC simulations. *Microporous Mesoporous Mater.* 2002, 55, 139–145.
- Takaba, H.; Yamamoto, A.; Hayamizu, K.; Oumi, Y.; Sano, T.; Akiba, E.; Nakao, S.-I. Dependence of the diffusion coefficients of methane in silicalite on diffusion distance as investigated by 1H PFG NMR. *Chem. Phys. Lett.* **2004**, *393*, 87–91.
- Adem, Z.; Guenneau, F.; Springuel-Huet, M.A.; Gedeon, A. PFG NMR investigation of hydrocarbon diffusion in large NaX zeolite crystals: Effect of internal field gradients on diffusion data. *Microporous Mesoporous Mater.* 2008, 114, 337–342.
- 17. Feldhoff, A.; Caro, J.; Jobic, H.; Ollivier, J.; Krause, C.B.; Galvosas, P.; Kärger, J. Intracrystalline transport resistances in nanoporous zeolite X. *ChemPhysChem* **2009**, *10*, 2429–2433.
- Cotts, R.M.; Hoch, M.J.R.; Sun, T.; Markert, J.T. Pulsed field gradient stimulated echo methods for improved NMR diffusion measurements in heterogeneous systems. *J. Magn. Reson.* 1989, *83*, 252–266.
- 19. Gibbs, S.J.; Johnson, C.S., Jr. A PFG NMR experiment for accurate diffusion and flow studies in the presence of eddy currents. *J. Magn. Reson.* **1991**, *93*, 395–402.
- 20. Kiyono, M.; Williams, P.J.; Koros, W.J. Generalization of effect of oxygen exposure on formation and performance of carbon molecular sieve membranes. *Carbon* **2010**, *48*, 4442–4449.
- 21. Callaghan, P.T. Principles of NMR Microscopy; Clarendon Press: Oxford, UK, 1991; p. 492.
- 22. Stallmach, F.; Kärger, J. The potentials of pulsed field gradient NMR for investigation of porous media. *Adsorption* **1999**, *5*, 117–133.
- 23. Karger, J.; Ruthven, D.M. Diffusion in zeolites. Comparison of sorption and nuclear magnetic resonance diffusivities. *J. Chem. Soc. Faraday Trans. 1* **1981**, 77, 1485–1496.
- Hibbe, F.; Chmelik, C.; Heinke, L.; Pramanik, S.; Li, J.; Ruthven, D.M.; Tzoulaki, D.; Karger, J.R. The nature of surface barriers on nanoporous solids explored by microimaging of transient guest distributions. J. Am. Chem. Soc. 2011, 133, 2804–2807.
- 25. Heinke, L.; Kärger, J. Correlating surface permeability with intracrystalline diffusivity in nanoporous solids. *Phys. Rev. Lett.* **2011**, *106*, 074501.
- Kiyono, M.; Koros, W.J.; Williams, P.J. Correlation between pyrolysis atmosphere and carbon molecular sieve membrane performance properties. In *Inorganic, Polymeric and Composite Membranes: Structure, Function and Other Correlations*, 1st ed.; Oyama, S.T., Stagg-Williams, S.M., Eds.; Elsevier: Amsterdam, The Netherlands, 2011; Volume 14, pp. 138–174.
- 27. Delprato, F.; Delmotte, L.; Guth, J.L.; Huve, L. Synthesis of new silica-rich cubic and hexagonal faujasites using crown-etherbased supramolecules as templates. *Zeolites* **1990**, *10*, 546–552.
- Ginter, D.M.; Bell, A.T.; Radke, C.J. Synthesis of Microporous Materials: Molecular Sieves; Occelli, M.L., Robson, H.E., Eds.; Van Nostrand Reinhold: New York, NY, USA, 1992; Volume 1, p. 6.

© 2012 by the authors; licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution license (http://creativecommons.org/licenses/by/3.0/).