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Effect of short- and medium-chain fatty acid mixture on polyhydroxyalkanoate production by *Pseudomonas* strains grown under different culture conditions

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Short- and medium-chain fatty acids (SMCFAs) derived from the acidogenic anaerobic mixed culture fermentation of acid whey obtained from a crude cheese production line and their synthetic mixture that simulates a real SMCFArich stream were evaluated for polyhydroxyalkanoate (PHA) production. Three individual Pseudomonas sp. strains showed different capabilities of growing and producing PHAs in the presence of a synthetic mixture of SMCFAs. Pseudomonas sp. GL06 exhibited the highest SMCFA tolerance and produced PHAs with the highest productivity (2.7 mg/L h). Based on these observations, this strain was selected for further investigations on PHA production in a fed-batch bioreactor with a SMCFA-rich stream extracted from the effluent. The results showed that PHA productivity reached up to 4.5 mg/L h at 24 h of fermentation together with the ammonium exhaustion in the growth medium. Moreover, the PHA monomeric composition varied with the bacterial strain and the type of the growth medium used. Furthermore, a differential scanning calorimetric and thermogravimetric analysis showed that a short- and medium-chain-length PHA copolymer made of 3-hydroxybutyric, -hexanoic, -octanoic, -decanoic, and -dodecanoic has promising properties. The ability of Pseudomonas sp. to produce tailored PHA copolymers together with the range of possible applications opens new perspectives in the development of PHA bioproduction as a part of an integrated valorization process of SMCFAs derived from waste streams.

KEYWORDS

biopolymers, medium-chain fatty acids, polyhydroxyalkanoates, *Pseudomonas* sp., short-chain fatty acids

1 Introduction

The negative impact of petrochemical plastics on the environment has prompted a growing interest in environmentally friendly alternative materials. Polyhydroxyalkanoates (PHAs) are especially attractive because of their unique material properties such as biodegradability, non-toxicity, and biocompatibility and the similarity of their physical properties to those of synthetic polymers (Zubairi et al., 2016). Moreover, PHAs have many advantages over petrochemical-derived polymers, such as hydrophobicity, thermoplastic processability, relatively high melting point, and optical purity. They are natural polyesters synthesized by various microorganisms under unbalanced growth conditions as intracellular energy compounds in the form of granules in the cytoplasm (Akaraonye et al., 2010). Generally, PHAs are classified according to the carbon-chainlength of the constituent monomers into short-chain-length (PHA_{SCL}) containing 3-5 carbon atoms in the molecule, medium-chain-length (PHA_{MCL}) with 6-14 carbon atoms in the molecule, and long-chain-length (PHA_{LCL}) which contains more than 15 carbon atoms (Tan et al., 2014). It is known that the monomeric composition of PHAs depend mainly on the carbon source used for bacterial culture and the bacterium that is able to synthesize and accumulate PHAs (Koller and Braunegg, 2015). The applicability of bacterial PHAs is directly related to their properties. PHA_{SCL}, such as poly-3-hydroxybutyrate [P(3HB)], shows high crystallinity, stiffness, and brittleness with poor elastic properties, limiting its use as a stable material. PHA_{MCL} shows more favorable and useful properties. They are elastomers with a low degree of crystallinity, melting point, and tensile strength as well as high elongation to break. They are synthesized mainly by bacteria of the Pseudomonas genus. Due to their useful properties, PHAs have great potential in biomedical, agricultural, and industrial applications (Tan et al., 2021). Nevertheless, the commercialization of PHAs in the world market is currently limited, mainly due to the high production costs compared to synthetic polymers. Despite the fact that the fermentation technology and polymer extraction process have considerably improved over the past decade, the cost of the carbon source still accounts for half of the cost of producing PHAs. Consequently, there is a growing need to develop novel microbial processes using renewable and inexpensive carbon sources. Short and medium chain fatty acids (SMCFAs) generated by acidogenic anaerobic mixed culture fermentation (MCF) are an interesting alternative to the expensive substrates. Recycling waste into desirable and valuable products is a revolutionary path in waste management and an environmentally friendly process (Martinez et al., 2015). Various renewable wastes converted into SMCFAs such as sugarcane molasses (Albuquerque et al., 2007), paper mill wastewater (Bengtsson et al., 2008), olive oil wastewater (Beccari et al., 2009), food waste (Venkateswar Reddy and Venkata Mohan, 2012; Aremu et al., 2021; Thomas et al., 2022), and pea shells (Patel et al., 2012) have been used to produce environmentally friendly PHAs. In contrast, few scientific publications have evaluated the potential of pure bacterial cultures to convert SMCFA-rich streams from MCF using organic waste into PHAs (Venkateswar Reddy et al., 2012; Cerrone et al., 2014; Martinez et al., 2015; Vu et al., 2021). It should also be mentioned that none of these studies evaluated, in detail, the properties of the extracted PHAs.

An important aspect in the cost-effective production of PHAs is also the selection of a microorganism that has the ability to efficiently intracellularly accumulate this biopolymer using renewable carbon sources. Bacteria belonging to the Pseudomonas genus meet these criteria by transforming postfermentative carbon sources into multipurpose biopolymers. They are also characterized by fast biomass growth, low production requirements, easy adaptation, and tolerance to oxidative stress (Mozejko-Ciesielska et al., 2019). Pseudomonas sp. Have been characterized as the producers, usually producing mcl-PHA rather than scl-PHA (Solaiman and Ashby, 2005). The synthesis of PHAs from SMCFAs has been described for several Pseudomonas spp., including: Pseudomonas sp. ST2 (Reddy et al., 2008; Munir and Jamil, 2018), Pseudomonas sp. H9 (Liu et al., 2021), P. putida KT2440 (Kourmentza et al., 2009; Cerrone et al., 2014; Yang et al., 2019), P. otitidis (Venkateswar Reddy et al., 2012), P. pseudoflava (Venkateswar Reddy et al., 2017), P. palleronii (Venkateswar Reddy et al., 2017), and P. oleovorans (Aremu et al., 2021). To the best of our knowledge, none of these studies described the properties of the extracted scl-mcl-PHA copolymers.

In recent years, the amount of organic and biomass waste has been steadily increasing. Currently, sewage sludge is a burden for municipal wastewater treatment plants (Lad et al., 2022). Moreover, acid whey, a by-product of Greek yoghurt, cottage cheese production, and the like, poses a risk to the ecosystem and its disposal is associated with a fee (Erickson, 2017). Therefore, SMCFAs derived from sludge and acid whey are attractive raw materials for biopolymer synthesis by microorganisms, and this makes the bioprocess more environmentally friendly. This is the first study that reports about SMCFAs from the anaerobic mixed culture fermentation of acid whey, which is available worldwide, to produce unique scl-mcl PHAs. Three strains belonging to Pseudomonas genera were first evaluated to study their capability of producing PHAs while they grew on different media supplemented with a synthetic mixture of SMCFAs, that simulates a real SMCFA-rich stream, as the only carbon sources. Then, the most effective Pseudomonas sp. strain was cultured with SMCFAs derived from whey wastewater fermentation effluent. The extracted PHAs were characterized using GC/MS, FTIR, DSC, and TG to assess the application potential of these materials.

2 Materials and methods

2.1 Microorganisms and inoculum preparation

Pseudomonas sp. Gl01 and *Pseudomonas* sp. Gl06 strains were isolated from mixed microbial communities and belong to the Culture Collection of the Department of Microbiology and Mycology, University of Warmia and Mazury in Olsztyn. They were previously described as strains capable of synthesizing and accumulating PHA_{MCL} (Ciesielski et al., 2010). The *Pseudomonas antarctica* (DSM 15318) used in the study was purchased from the German Collection of Microorganisms and Cell Cultures GmbH at the Leibniz Institute.

2.2 Culture condition and carbon sources

Seed cultures were grown in lysogeny broth (10 g/L tryptone, 5 g/L yeast extract, 10 g/L NaCl) at 30°C, shaking at 150 rpm for 16 h. Then, the precultures were transferred to three different non-limited and nitrogen-limited mineral salt media (MSM): (MSM 1) 12.8 g/L Na₂HPO₄·7H₂O, 3 g/L KH₂PO₄, 10 g/L NH₄Cl, 0.5 g/L NaCl (Poblete-Castro et al., 2012); (MSM 2) 12.8 g/L Na₂HPO₄, 3 g/L KH₂PO₄, 10 g/L (NH₄)₂SO₄; (MSM 3) 3.5 g/L Na₂HPO₄, 5 g/L KH₂PO₄, 10 g/L (NH₄)SO₄. Nitrogenlimited MSM consisted of 1 g/L of nitrogen source in each media. The media were supplemented with 1 g/L of MgSO₄·7H₂O and 2.5 ml/L of trace element solution consisting of (per liter): 20 g FeCl₃·6H₂O, 10 g CaCl₂·H₂O, 0.03 g CuSO₄·5H₂O, 0.05 g MnCl₂·4H₂O, and 0.1 g ZnSO₄·7H₂O dissolved in 0.5N HCl. The pH of each culture was adjusted to 7.0 by adding 1N NaOH and 1N HCl. All MSM components were dissolved in water and then autoclaved at 121°C. An MgSO4.7H2O solution was sterilized and added separately. The MSM were supplemented with 20% (v/v) of a mixture of synthetic SMCFAs (SMCFA_{synthetic}-rich stream) or 20% (v/v) of SMCFAs extracted from mixed culture fermentation of acid whey (SMCFA_{extracted}-rich stream). SMCFA_{synthetic}-rich stream is a mixture of synthetic carboxylic acids composed of 2.85 g/L of acetic acid, 9.86 g/L of butyric acid, 0.16 g/L of valeric acid, and 3.05 g/L of caproic acid. The effluent for PHA production was taken from the acidogenic anaerobic mixed culture fermentation of acid whey obtained from a crude cheese production line (Duber et al., 2018). It was taken from a steady-state phase and contained (except for organic acids mentioned previously) 9.31 g/L lactic acid and 1.64 g/L ethanol.

The *Pseudomonas* spp. strains were cultured in 250-ml Erlenmeyer flasks in a rotary shaker at 150 rpm, at 30° C for 48 h. Fermentation shake flasks were inoculated with 5% v/v of the precultures. The carbon source was added at the beginning of the cultivations. Three replicate cultivations were carried out.

The bacterial cells were harvested at 48 h to determine the cell dry mass, PHA concentration, and composition.

2.3 Bioreactor fermentation

The preliminary cultivations in shake flasks led to the selection of MSM, consisting of $12.8 \text{ g/L} \text{ Na}_2\text{HPO}_4$, $3 \text{ g/L} \text{ KH}_2\text{PO}_4$, $1 \text{ g/L} (\text{NH}_4)_2\text{SO}_4$ that supported the best PHA productivity, and *Pseudomonas* sp. GL06 as the most effective PHA producer.

The PHA production of the selected Pseudomonas sp. strain was conducted at 30°C with an aeration rate of 4 L/min in a 7 L bioreactor (Biostat A, Sartorius, Germany) equipped with a pH controller. The pH-value was maintained at seven through the modulated addition of concentrated 1N NaOH and 1N HCl. The temperature was maintained by a thermostatic jacket. The dissolved oxygen was monitored during the whole cycle with an O2 electrode (InPro 6800, Mettler Toledo GmbH, Switzerland) and was maintained at 50% air saturation by adjusting the agitation rate from 300 to 1,000 rpm automatically. Total fermentation time was 48 h. The inoculation size was 10% (v/ v). The mineral salt medium was supplemented with a total of 20% (v/v) SMCFAs-extracted. The substrate was added in two portions: first at the beginning of the cultivation and then after 8 h of fermentation. A concentrate solution (Sigma Aldrich) was used as an antifoam in response to the antifoam controller. The samples of the culture broth were removed at several time intervals for analysis of biomass concentration, ammonium and phosphate concentration, PHA yield, the composition, and concentration of PHA monomers.

2.4 Analytical procedures

To measure cell dry mass (CDM), 100 ml of culture broth was centrifuged at $11.200 \times g$ for 10 min and then lyophilized for 24 h using a Lyovac GT2 System (SRK Systemtechnik GmbH). Ammonium and phosphorus concentration were determined spectrophotometrically using a Hach Lange DR 2800 spectrophotometer (Hach Lange, Düsseldorf, Germany) as well as the LCK338 and LCK350 kits according to the manufacturer's instructions, respectively. Quantitative and qualitative analysis of the obtained biopolymers was performed. Biopolyesters were extracted by shaking lyophilized cells in chloroform at 50°C for 3 h. Then the mixture was filtered through No. 1 Whatman filter paper to remove the cellular debris. Biopolymers dissolved in chloroform were purified by precipitation with a 70% cold methanol solution and then allowed to evaporate at room temperature. The PHA content (% of CDM) was defined as the percentage of the ratio of biopolymer concentration to total cell concentration.

2.5 PHA analyses

2.5.1 Gas chromatography coupled with mass spectrometry

To evaluate the PHA composition, the lyophilized cells were analyzed by gas chromatography coupled with mass spectrometry (GC-MS QP2010 PLUS, Shimadzu, Japan) according to the method described by Możejko-Ciesielska and Pokój (2018). As a first step, analyzed samples were suspended in a chloroform-methanol-sulfuric acid mixture (100/97/3, v/v/v), and the methylation process was performed by heating the vials at 100°C for 20 h. After that, the sulfuric acid was neutralized with Na₂CO₃ and the resulting mixture was dried with anhydrous Na₂SO₄. After filtration, the methyl esters were analyzed using a BPX70 (25 m \times 0.22 mm \times 0.25 mm) capillary column (SGE Analytical Science, Victoria, Australia) with helium as a carrier gas at a flow rate of 1.38 ml/min. The column was heated from 80 to 240°C at a rate of 10°C/min. The interface and ion source temperatures of GC-MS were set at 240°C, and the electron energy was set at 70 eV. The total ion current (TIC) mode was used in 45-500 m/z range. Pure standards of methyl 3hydroxybutyrate, 3-hydroxyvalerate, 3-hydroxyhexanoate, -undecanoate, -octanoate, -nonanoate. -decanoate, -dodecanoate, -tetradecanoate, and -hexadecanoate were purchased from Larodan Fine Chemicals (Sweden) to generate calibration curves for the methanolysis assay.

2.5.2 Fourier-transform infrared spectroscopy

The infrared spectra were recorded in the range from 4,000 to 650 cm⁻¹ with a Fourier Transform Spectrophotometer (FTIR) Nicolet iS10 (ThermoScientific, United States) by the attenuated total reflection method (ATR-FTIR) on samples without prior preparation. Each spectrum analyzed was the average of 16 recorded measurements.

2.5.3 Differential scanning calorimetry and thermogravimetry

Differential scanning calorimetry (DSC) tests were carried out in a nitrogen atmosphere with a Q200 differential scanning calorimeter (TA Instruments, United States). The temperature ranged from -70 to 230°C with a heating/cooling rate of 10°C/ min. Samples of approximately 1 mg were first rapidly heated to 230°C and conditioned for 1 min to remove the thermal history of the material. The samples were then cooled to -70°C and reheated to 230°C. Thermal analysis of polymers was based on the second heating curve, where the glass transition temperature (T_g), melting point (T_m), and change in enthalpy of the melting process (Δ H_m) were recorded.

Thermogravimetry (TG) tests were performed in a nitrogen atmosphere with a Q500 thermobalance (TA Instruments, United States). The temperature ranged from 25 to 700° C with a heating rate of 10° C/min. The mass of the analyzed samples was approximately 1 mg. From the thermogravimetric curve, 5% mass loss temperature (T_{5%}) was determined and used as a parameter determining the onset of thermal degradation of the material, taken as the thermal resistance of the material (T_d). The differential thermogravimetric curve (DTG) (first derivative of the TG curve) was also presented, and the T_{max} values determining the temperature of the fastest mass loss were also presented.

3 Results and discussion

3.1 Capability of *Pseudomonas* sp. strains to grow and produce PHAs in mineral salt media containing SMCFA_{synthetic}-rich stream

A preliminary study of the *Pseudomonas* sp. GL01, *Pseudomonas* sp. GL06, and *P. antarctica* was conducted to determine their ability to grow and synthesize PHAs in the presence of a mixture of SMCFAs (SMCFA_{synthetic}-rich stream) that mimicked the effluent from whey wastewater anaerobic fermentation as the carbon source.

As can be seen in Figure 1 all tested bacteria could grow in the medium supplemented with SMCFA_{synthetic}-rich stream under all culture conditions used. In particular, the Pseudomonas sp. GL06 showed the highest biomass concentration among all tested MSM media, achieving the maximum biomass value in MSM 1 (1.8 g/L of CDM). A slightly lower amount of CDM (1.7 g/L) was achieved in the cultivation of Pseudomonas sp. GL01 grown on MSM 2 under non-limited conditions. A 3-fold lower CDM of all Pseudomonas putida strains (KT2440, CA-3, and GO16) was determined by Cerrone et al. (2014) ,who cultured them using fatty acids derived from anaerobic digestion of grass. In our study, low growth was detected in the cultivation of P. antarctica in culture media under non-limited as well as nitrogen-limited conditions, that could suggest the inhibitory effect of the SMCFA_{synthetic}-rich stream used. However, higher CDM values were observed in the cultures under non-limited conditions.

In general, adequate nitrogen source is essential for bacterial cell growth. On the other hand, PHA synthesis and accumulation by bacteria belonging to *Pseudomonas* genera is induced by nitrogen limitation in the culture medium (Hoffmann and Rehm, 2005). Our results showed that PHA concentration and productivity increased under nitrogen starvation and depended on the type of MSM used. Only in the case of *P. antarctica* grown on MSM 3, PHA yield was not triggered by nitrogen limitation (Figures 2A,B). The best PHA concentration was achieved in the culture with *Pseudomonas* sp. GL06 grown on MSM 2 under N-limitation (0.13 g/L) at the PHA productivity level of 2.7 mg/L h. Aremu et al. (2021) reported a similar PHA value (0.12 g/L) in *Pseudomonas oleovorans* culture supplemented with acetic acid as the carbon source in a nitrogen-limited medium.



FIGURE 1

Biomass concentration (g/L) of *Pseudomonas* sp. Gl01, *Pseudomonas* sp. Gl06, and *P. antarctica* at 48 h cultured on three different growth media (MSM 1, MSM 2, and MSM 3) in shake flask experiments under non-limited and N-limited conditions using SMCFA_{synthetic}-rich stream.



FIGURE 2

PHA production from SMCFA_{synthetic}-rich stream by *Pseudomonas* sp. GL01, *Pseudomonas* sp. GL06, and *P. antarctica* at 48 h cultured on three different growth media (MSM 1, MSM 2, and MSM 3) in shake flask experiments under non-limited and N-limited conditions. (A) PHA concentration (g/L) and (B) PHA productivity (mg/L h).



Furthermore, our results suggests that PHA production could be enhanced by controlling the nitrogen source. In all tested *Pseudomonas* strains, higher PHA efficiency was observed when MSM 2 [contained $(NH_4)_2SO_4$] was used under both growth conditions compared to MSM 1 (consisted of NH₄Cl). Moreover, our data revealed that when phosphate sources $(Na_2HPO_4\cdot7H_2O$ and KH_2PO_4) were used in a higher concentration (MSM 2 compared to MSM 3), PHAs were synthesized and accumulated at higher yields, in particular by *Pseudomonas* sp. GL06 and *P. antarctica.* It could be concluded that the PHA concentration and productivity were dependent on the culture conditions used.

3.2 SMCFA_{extracted}-rich stream derived from anaerobic fermentation as the carbon source for biomass growth and PHA production

On the basis of the previously described results that *Pseudomonas* sp. GL06 produced PHAs with the highest efficiency, it was selected for further investigations into PHA production with SMCFA_{extracted}-rich stream from the acidogenic anaerobic mixed culture fermentation of acid whey obtained from a cheese production line. The fermentation process in a bioreactor led us to precisely monitor the bioprocess due to larger volume for sampling. As may be observed from the data reported in Figure 3, biomass concentration had been increasing for up to 32 h, and then reached 1.03 g/L at the end of the bioprocess. Comparable biomass data (1.03 g/L) were reported in *P. oleovorans* culture supplemented with volatile fatty acid



streams from chicken manure where acetate was the predominant acid (Aremu et al., 2021). Higher biomass concentration was determined by our research group by supplementation of the culture medium with the same SMCFA_{extracted}-rich stream in the cultivation of Paracoccus homiensis (Szacherska et al., 2021). Moreover, our results confirmed that PHA productivity increased under nitrogen limitation, reaching a maximum value of 4.5 mg/L h at 24 h of the fermentation after ammonium exhaustion in the growth medium was reached. Similar results (4.4 mg/L h) were achieved by Kourmentza et al. (2009), who cultivated Pseudomonas sp. on a mixture of acetic, propionic, and butyric acids under nitrogen-limiting conditions. Goh and Tan (2012), by feeding of glucose and glycerol in the cultivation of arctic Pseudomonas sp. UMAB-40, determined a much lower productivity, i.e., 2.6 mg/L h and 1.6 mg/L h, respectively. Exponential nonanoic acid-limited growth of P. putida KT2440 resulted in a PHA content of 75.4%, giving a high cumulative PHA productivity of 1.11 g/L h (Sun et al., 2007). It should be emphasized that in our study, the PHA yield did not increase more after 24 h. The observed reduction in PHA synthesis can be explained by the consumption of the accumulated PHAs as energy reserves to extend the survival of bacteria after depletion of the carbon and nitrogen sources (Kourmentza et al., 2017). The same observation was made by Venkateswar Reddy et al. (2012) who reported that after reaching the maximum PHA concentration, the production capacity of *Pseudomonas otitidis* decreased up to the end of the experiment. The authors suggested that due to the famine phase, the stored PHAs were consumed by the bacteria to maintain their cell activity in the absence of essential nutrients. Furthermore, the PHA productivity was about 60% higher than that determined in the shake flask experiments using the same culture medium. It should be noted that the difference between SMCFA_{synthetic}-rich stream and SMCFA_{extracted}-rich stream was the presence of lactic acid and ethanol in the latter. Thus, our data suggested that neither lactic acid nor ethanol affected the PHA productivity negatively.

Furthermore, quite low PHA productivity was reported in the cultivation of *P. homiensis* grown on the same (as in our study) SMCFA_{extracted}-rich stream, suggesting that the presence of butyric acid as the dominant component had more inhibitory effect due to the fact that a single short-chain-fatty acid in the medium resulted in the lowest PHA production efficiency compared with others (Szacherska et al., 2021).

3.3 The characterization of PHAs

3.3.1 GC-MS

As shown in Figure 4, the PHA monomeric composition varied with the bacterial strain and the type of the growth medium used. Our results proved that in the cultivations supplemented with SMCFA_{synthetic}-rich stream that simulated a real SMCFA-rich stream, Pseudomonas sp. GL01 and GL06 showed the tendency to produce high amounts of 3hydroxyhexanoate (3HHx) and 3-hydroxydodecanoate (3HDD) as the main monomers and lower content of 3-hydroxybutyrate (3HB), 3-hydroxyoctanoate (3HO), and 3-hydroxydecaonate (3HD). Interestingly, only in the cultivations of Pseudomonas sp. GL01 performed under non-limited growth conditions a trace amounts of 3-hydroxynonanoate was detected. This monomer was found mainly at the end of the fermentation of the same bacterial strain using saponified waste palm oil (Możejko and Ciesielski, 2013). The level of 3HB in the extracted PHAs seems to be strain dependent. Our results indicated that P. antarctica is able to synthesize P(3HB) homopolymer grown on MSM1 and MSM2 under non-limited conditions, whereas this bacterium cultured on MSM 3 under both conditions applied was capable of producing scl-mcl copolymers. P. otitidis also prefers to produce copolymers, however, consisting of 3HB and 3HV monomers (Venkateswar Reddy et al., 2012). The authors reported that the copolymer showed higher 3HB monomer content (91 mol%) when the bacteria were cultured on synthetic acids (acetate, propionate, and butyrate) compared to acidogenic effluent from the biohydrogen reactor. Furthermore, it was observed that P. putida KT2440 grown in the medium supplemented with acetate as the sole carbon source produced P(3HO-co-3HD-co-3HDD) terpolymer with 3HD as the principal monomer (Yang et al., 2019).



The GC/MS analysis confirmed that at the beginning of the cultivations of Pseudomonas sp. GL06 in the bioreactor, no PHAs were detected. The repeat-unit composition of the purified biopolymers extracted from the bioreactor at 8 h of the fermentation was found to consist mainly of 3HD and 3HDD and lesser amounts of 3HB, 3HHx, and 3HO. From 24 to 48 h of the cultivation higher content of 3HHx fraction was observed from 38.5 mol% to 22.1 mol%, respectively. 3HB and 3HO monomers were detected as minor components in extracted biomaterials. Similarly, when glucose, glycerol, and fructose were supplied as carbon sources to Pseudomonas sp. B14-6 by Choi et al. (2021), scl-mcl copolymer was detected. However, P. putida KT2440 and CA-3 synthesized mcl-copolymers cultured on the concentrated fatty acid mixture derived from the anaerobic digestion leachate. Cerrone et al. (2014) showed that these strains produced 3HD as the main constituent and 3HO and 3HDD as minor components.

3.3.2 FTIR

The FTIR spectra of the polymer produced is presented in Figure 5. The spectrum displays the typical bands for PHAs (Shamala et al., 2009; Rebocho et al., 2020; Meneses et al., 2021). Peaks at 2,956, 2,923, and 2,853 cm⁻¹ can be assigned to the stretching vibration of C-H bonds of methyl (CH₃) and methylene (CH₂) groups of the PHA molecule. The high intensity of the 3,000–2,700 band (the highest in the entire spectrum) results from the presence of a large amount of medium chain length monomers in the tested polymer. The absorbance band located at 1740 cm⁻¹ is attributed to the stretching vibration of the C=O group (ester carbonyl) in the



PHA polyester. The bands between 1,022 and 1,260 cm⁻¹ are related to the crystallinity of the material, with the 1,082 cm⁻¹ peak attributed to C–O bonds. The band appearing at 802 cm⁻¹ represents the C-C stretching bond and is also characteristic of PHA.

3.3.3 Thermal analysis

As can be shown in Figure 6A, DSC studies proved that glass transition temperature (T_g) of P(3HB-co-3HHx-co-3HO-co-3HDD) produced by *Pseudomonas* sp. GL01 reached -45.4°C. Furthermore, a small melting peak with a melting temperature (T_m) of 11.7°C and enthalpy change (Δ H_m) of 6.6 J/g was observed. The recorded T_g value is typical for mcl-PHAs and corresponds to the values reported in the literature (Simon-Colin et al., 2012; Basnett et al., 2017). The obtained melting point (11.7°C) is low and unusual, as in most cases the recorded T_m mcl-PHA values are in the range from 40 to 55°C. Lower

 T_m values are related to the low degree of crystallinity of this polymer and the predominance of the amorphous phase. The low content of the crystalline phase in the tested material is confirmed by the FTIR tests (low absorbance of peaks related to the crystalline phase) and the very low ΔH_m value obtained in the DSC tests. Nevertheless a P(3HO-*co*-3HDD-*co*-3HDD*co*-3HTD) copolymer produced by *Yarrowia lipolytica* ThYl_1,166 also possess low T_g (-39°C) and T_m (19°C) values indicating its amorphous behavior and flexibility at ambient temperature (Rigouin et al., 2019).

Moreover, the degradation temperature (T_d) of the tested scl-mcl copolymer was observed at 174.1°C (Figure 6B) and was lower than the typical T_d values recorded for mcl-PHAs (above 200°C) (Simon-Colin et al., 2012; Basnett et al., 2017) due to its low degree of crystallinity. Additionally, TG analysis showed that the beginning of the degradation process already started just above 100°C and proceeded over a fairly large temperature range with the maximum intensity (T_{max}) at 287.0°C (Figure 6B). The course of the degradation process may have been caused by a large number of macromolecules of shorter length (lower molecular weight), which are characterized by lower degradation temperatures. The fact that 3HB monomer was present in the extracted copolymer could be the reason for its lower thermal resistance.

4 Conclusion

Supplementation of synthetic SMCFAs in bacterial cultures would be expensive. Therefore using SMCFA-rich stream from the fermentation of agro-industrial waste to produce PHAs can significantly reduce the cost of the process. In this study, both variants of SMCFAs were proved to be potential substrates for PHA production by Pseudomonas strains. The highest PHA productivity was achieved in Pseudomonas sp. Gl06 cultivation in the bioreactor under N-limited with MSM 2 using SMCFA_{extracted}-rich stream derived from MCF using food waste. The structure and thermal properties of the PHAs were analytically verified and we proved that the extracted scl-mcl copolymers possess lower melting point and degradation temperature compared to the PHAs described in the literature. These findings indicate the possibility of feeding the Pseudomonas sp. GL06 with cheap SMCFA_{extracted}-rich stream to produce PHA copolymers with improved properties.

Data availability statement

The original contributions presented in the study are included in the article; further inquiries can be directed to the corresponding author.

Author contributions

KS participated in the design of the study and performed the cultivations and PHA extractions. KM performed and interpreted FTIR and differential scanning calorimetric and thermogravimetric analyses. SC performed and interpreted gas chromatography coupled with mass spectrometry analysis. PO-P performed waste-derived SMCFA analysis and participated in the design of the study. JM-C participated in the design of the study and supervised in study coordination. KS and JM-C wrote the manuscript with input from all the authors.

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Conflict of interest

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