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Effect of thiol-containing monomer on the preparation of temperature-sensitive hydrogel microspheres

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Abstract The main objective of this study is to prepare, thermally, sensitive microgel particles bearing thiol groups via precipitation polymerization of *N*-isopropylacrylamide (NIPAM), methylenebisacrylamide (MBA) and vinylbenzylisothiouronium chloride (VBIC) using 2-2'-azobis(2-amidinopropane)-dihydrochloride (V50) as initiator. The influence of various parameters has been investigated as a systematic study to point out the role of each reactant on polymerization conver-

sion, and consequently, on particles and water-soluble polymer formation. The final microgel particles were characterized with respect to particle size and swelling ability. The aim of this paper is to complete our first short communication; *Macromolecular symposia*, 2000. 150: p. 283–290.

Keywords Precipitation polymerization · Functionalized hydrogel · *N*-isopropylacrylamide · Polymerization kinetics · Thiol monomer

Introduction

The preparation and the use of stimuli responsive materials have attracted the attention of various application areas. Regarding the elaboration of temperature-responsive microgels, the first work in this direction has been reported by Pelton and Chibante [1] and by Kawaguchi et al. [2] by investigating precipitation polymerization of *N*-isopropylacrylamide (NIPAM) as main monomer, methylenebisacrylamide (MBA) as a cross-linker and potassium persulfate (KPS) as the initiator. In addition, the effect of charged surfactant [sodium dodecyl sulfate (SDS)] on the precipitation polymerization has been examined and discussed by Pelton et al. [3]. The principal results have been discussed on the basis of the polymerization above the lower critical solution temperature (LCST) of the corresponding linear polymer, the uses of the cross-linker agent and charged initiator. Then, during the precipitation polymerization at a high temperature (above the LCST of the corresponding linear polymer), the precipitated macromolecule chains are cross-linked, leading to the formation of hydrogel particles. The main problem in the elaboration of thermally sensitive microgel is related to high production of water-soluble

polymer [4, 5]. Various works have been also investigated to prepare core shell-like particles such as polystyrene core and poly(NIPAM) shell [6–9]. The effect of the used *N*-alkylacrylamide or *N*-alkylmethacrylamide on surfactant-free radical emulsion polymerization of styrene has been examined, and the polymerization and the final colloidal properties reported have to be related to the amount of water-soluble monomer in the used recipe [9].

Regarding the colloidal and physico-chemical properties of such thermally sensitive particles, several authors have reported various works. To some extent, swelling ability [8], electrokinetic properties [10, 11], colloidal stability [12] have been systematically investigated as a function of temperature, pH of the medium, ionic strength and solvent nature. As expected, the reported results principally demonstrate the drastic effect of temperature on the investigated colloidal properties.

The great interest of functionalized thermally sensitive particles is based on the possible control of adsorption/desorption by motoring the incubation temperature, and consequently, the covalent binding efficiency of proteic materials [13]. Then, various functional thermally sensitive microgels have been reported. Whereas, few systematic

studies have been dedicated to the elaboration of functionalized thermally sensitive latexes such as carboxylic [14], amine [15], boronic acid [15, 16]. Concerning the elaboration of thiol-containing thermally sensitive particles, the first preliminary work has been reported by Meunier et al. [17]. Colloidal particles bearing a thiol group is of great importance in biomedical diagnostic for specific and orientation of antibody fragments via disulfur bridging [18].

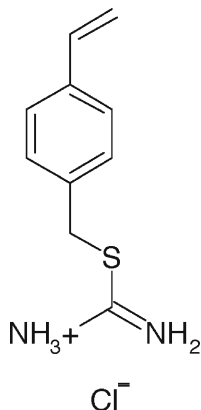
For a better understanding of the mechanistic approach of precipitation polymerization using NIPAM, MBA and protected thiol-containing monomer and colloidal properties of obtained latexes, a systematic polymerization study was of good interest.

The aim of the presented work is to investigate a systematic study to point out the role of each reactant and principally this related to the vinylbenzylisothiuronium chloride (VBIC) monomer on the precipitation polymerization process (of NIPAM, MBA, VBIC). In addition, the final latex particles such as particle size, size distribution, swelling ability and water-soluble polymer formation are addressed.

Experimental

Materials

N-isopropylacrylamide (NIPAM) from Kodak was recrystallized from toluene/hexane mixture. MBA from Amilabo was used without further purification. 2-2'-Azobis(2-amidinopropane) di-hydrochloride (V50) was provided kindly by Wako Chemical GmbH (Germany) and was recrystallized from water/acetone mixture. The VBIC monomer was synthesized according to Yamaguchi's method [19] and was recrystallized from diethylether/ethanol mixture. Water is of Milli-Q grade (Millipore S. A., France) and was boiled for 2 h under a nitrogen stream before use. ¹⁴C-labeled iodoacetamide was from Amersham (France).



Preparation of latexes

The polymerizations were performed under batch condition and were carried out in a 250-ml thermostated reactor, round-bottomed four-necked flask, equipped with a glass anchor-shaped stirrer, condenser, thermocouple and nitrogen inlet. The stirrer, in all cases, was 300 rpm. Well-boiled deoxygenated water was introduced under a constant stream of nitrogen. The reaction temperature was controlled at 70 °C into the reactor. Water, NIPAM, MBA and VBIC were added and the temperature was checked to be constant at 70 °C; after equilibrium, V50, dissolved in water, was introduced. The overall conversions were determined gravimetrically. When opalescence appeared in the reactor, the stirrer was lowered to 100 rpm to avoid the flocculation of the latex particles. The duration of the polymerization was about 4 h.

Polymerization kinetics

NIPAM conversion was determined by Gas Chromatography (9000 Perkin). The column was a 10% carbowax, 20 M, onto chromosorb WAW 80 400, 2-m length. The detection was performed with flame ionization and the amount of NIPAM was referred to dimethylformamide used as external standard. The overall conversion and the water-soluble polymer (WSP) were determined gravimetrically.

Characterization of water-soluble polymer (WSP)

Average molecular weights, M_w , were determined using statistical light scattering. In addition, ¹H NMR technique (Bruker AC 200 spectrometer, 200 MHz) was used to analyze the microstructure and to quantify the amount of functional groups in the water-soluble polymer.

Volume phase transition temperature (T_{VPT}) and lower critical solubility temperature (LCST) of microgels and water-soluble polymer were measured using UV-spectrophotometer Uvikon 941. The optical density (*OD*) was measured at a 540-nm wavelength as a function of temperature in a highly diluted concentration.

Colloidal characterization of latexes

Particle size was measured by quasi-elastic light scattering (QELS, using a N4MD from Coultronics). The temperature dependency of the hydrodynamic particle diameter was determined for all latexes by measuring the particle size as a function of temperature from 25 to 50 °C.

The VBIC concentration on the particles was examined using ^{14}C -labeled iodoacetamide (from Amersham, France) [18] and Ellmann's reagent [20]. ^1H NMR technique was also used to examine the chemical composition of the water-soluble polymer.

Results and discussion

Batch polymerizations were investigated to point out the influence of each parameter on the polymerization kinetic, particle size, water-soluble polymer formation. Then, the influence of MBA, V50 and VBIC concentration were systematically studied.

Influence of cross-link concentration

At first, the influence of MBA concentration on the polymerization was investigated. The results of a series of latex preparation at 70°C using a NIPAM concentration of 194.04 mmol/l , an initiator concentration of 1.2 mmol/l and an isothiuronium salt concentration of 0.1924 mmol/l are discussed below. The latexes prepared using high MBA concentration (36 mmol/l) show aggregation after 2-min polymerization only. The latexes prepared using MBA concentration below (36 mmol/l) remained stable during and after the polymerization reaction.

The diameter particle size was investigated by QELS (below and above the LCST of polyNIPAM) and by TEM analysis as a function of initial MBA concentration. The effect of MBA concentration revealed the existence of a maximum MBA limit that leads to unstable particles during the polymerization process as aforementioned. This phenomenon can be attributed to the high reactivity of such water-soluble cross-linker agent and to the possible bridging flocculation of particles via a chemical cross-linking process. As a general tendency, the hydrodynamic particle size increases with increasing amount of MBA as shown in Fig. 1. The swelling ability of the final particles decreases as the MBA amount increases in the polymerization recipe. This reflects the enhancement of the cross-linking density of the final particles vs MBA concentration.

The polymerization kinetic was studied as a function of initial MBA concentration by investigating the conversion vs time. The obtained results are reported in Fig. 2. The initial polymerization slope of polymer conversion vs time increases with increasing MBA concentration in the polymerization medium. The observed behavior is attributed to the reactivity of MBA, which acts as a water-soluble comonomer, whereas, the final conversion is found to reach a plateau value above 10 min polymerization time.

The influence of MBA amount on water-soluble polymer formation was also studied. As expected, the amount of water-soluble polymer decreases when increasing the initial MBA concentration in the polymerization recipe.

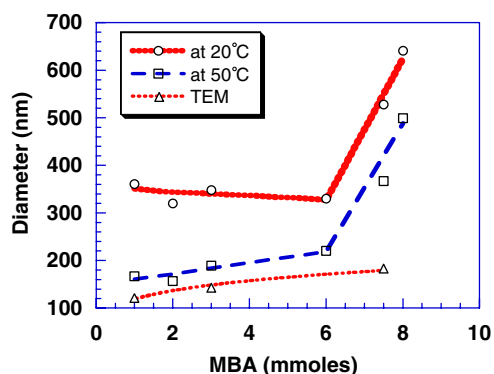


Fig. 1 Effect of MBA concentration on the final particle size using light scattering and TEM analysis. 48.51×10^3 mol of NIPAM, 0.30×10^3 mol of V50, 0.0481×10^3 mol of VBIC

The effect of BA concentration on conversion vs. time curves

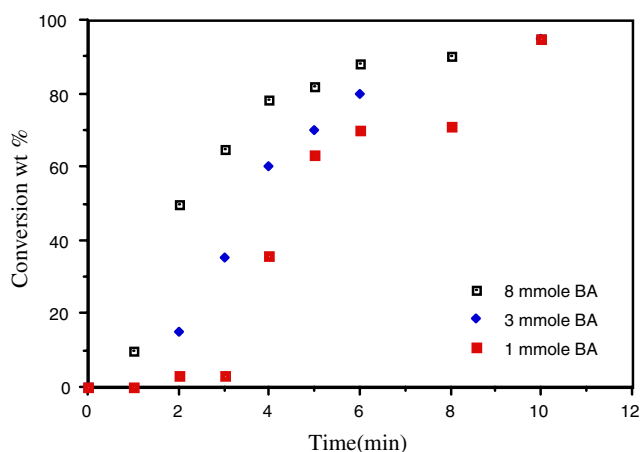


Fig. 2 Effect of MBA concentration on polymerization kinetics. 48.51×10^3 mol of NIPAM, 0.30×10^3 mol of V50, 0.0481×10^3 mol

This can be attributed to the effectiveness of MBA to cross-link the polymer chains (or nanoparticles) during the formation or nucleation step. Surprisingly, the amount of water-soluble polymer was found to be at less around 5 wt% in the investigated MBA range Fig. 3.

Influence of initiator concentration

The effect of the used water-soluble radical initiator (V50) on the final particle size was studied and the results obtained are reported in Fig. 4. In the investigated V50 concentration domain, the particle size (hydrodynamic diameters and TEM analysis) increases as the initiator amount increases in the polymerization medium. Compared to classical radical emulsion polymerization, the opposite effect was generally observed in low or moderate initiator concentration range. In such dispersion polymerization of water-soluble monomers, this can be attributed to the effect of salt induced by the initiator, which may affect

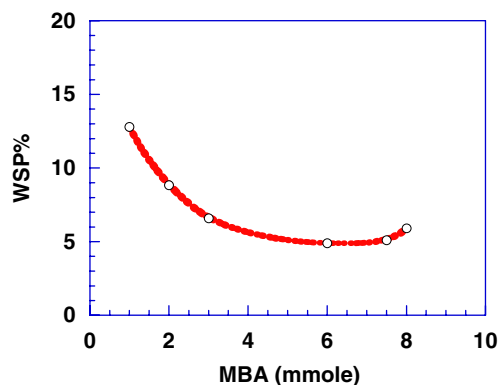


Fig. 3 Effect of MBA concentration on water-soluble polymer. 48.51×10^3 mol of NIPAM, 0.30×10^3 mol of V50, 0.0481×10^3 mol of VBIC

the colloidal stability of the formed nanoparticles during the nucleation step, and leads to the enhancement of the final particle size.

The used radical initiator affects not only the final particle size, but also the swelling ability. In fact, the swelling capability increases as the amount of V50 initiator increases. This demonstrates the drastic influence of V50 on the microstructure of the microgels as also observed when the effect of MBA was investigated.

The influence of initiator concentration on the polymerization rate (data not shown) and on the water-soluble polymer formation (Fig. 5) was investigated. As expected, the polymerization rate (i.e., the initial slope of polymer conversion vs time) increases as the initiator amount increases in the polymerization recipe. With regard to the amount of water-soluble polymer formation, the increase of V50 amount leads to the enhancement of free-chain formation. This can be attributed to short chain formation, which are hard to precipitate on one hand and to incorporate on the formed particles, on the second hand. Consequently, in such precipitation polymerization, the increase of initiator concentration (in the presence of VBIC

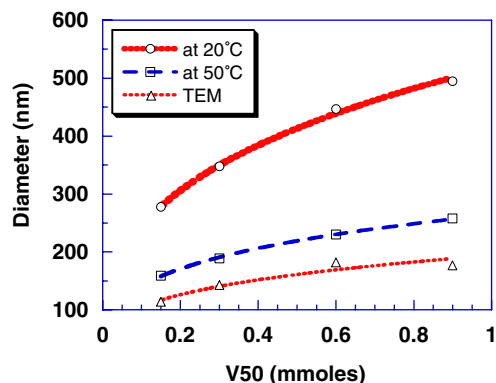


Fig. 4 The influence of V50 on the final particle size measured using light scattering. 48.51×10^3 mol of NIPAM, 3.00×10^3 mol of MBA, 0.0481×10^3 mol of VBIC

monomer) leads to a large particle size and to water-soluble polymer enhancement.

Influence of VBIC monomer concentration

The effect of VBIC comonomer concentration on the polymerization yield was examined and the results obtained are presented in Fig. 6 in which particles yield is reported as a function of polymerization time for various VBIC amounts ranging from 0 to 9.63 mmol/l.

The VBIC was found to have great influence on the polymerization kinetic (i.e. conversion vs time). For high VBIC amount, the crude final samples (i.e. prepared with 0.4815- or 2.4075-mmol VBIC) are transparent rather than turbid as for classical polymer latex particles. Rapid analysis by QELS reveals the absence of particles formation. ^1H NMR and gas chromatography analysis pointed out that NIPAM monomer was totally consumed. Consequently, a high amount of VBIC monomer leads principally to the linear polymer rather than to the particles or nanogels and to a high polymerization conversion.

The analysis of water-soluble polymer by GPC analysis (after particles removal) revealed the formation of short polymer chains (i.e. short oligomers). The GPC traces were found to be well defined and symmetrical as for the monomer. The increase in VBIC concentration in the polymerization recipe leads drastically to a high water-soluble polymer formation (Fig. 7). Such behaviour has already been observed in the case of aminoethylmethacrylate hydrochloride (AEMH) comonomer used in a similar condition [5] and attributed to the transferring role of the protected amine compound. Then, the increase of water-soluble formation as a function of VBIC concentration can be attributed to the transferring character of this monomer even under the protected form.

The influence of VBIC monomer concentration of final particles size was also examined (Fig. 8). The particle size

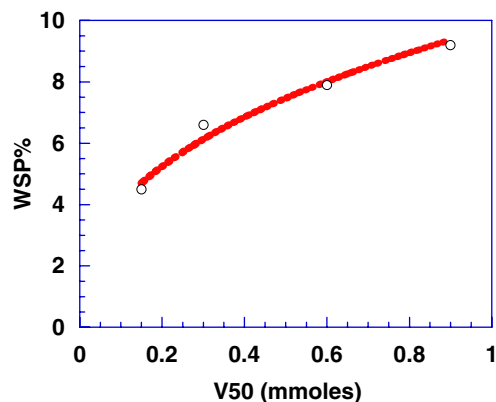


Fig. 5 Influence of initiator concentration on water-soluble polymer formation. 48.51×10^3 mol of NIPAM, 3.00×10^3 mol of BA, 0.0481×10^3 mol of VBIC

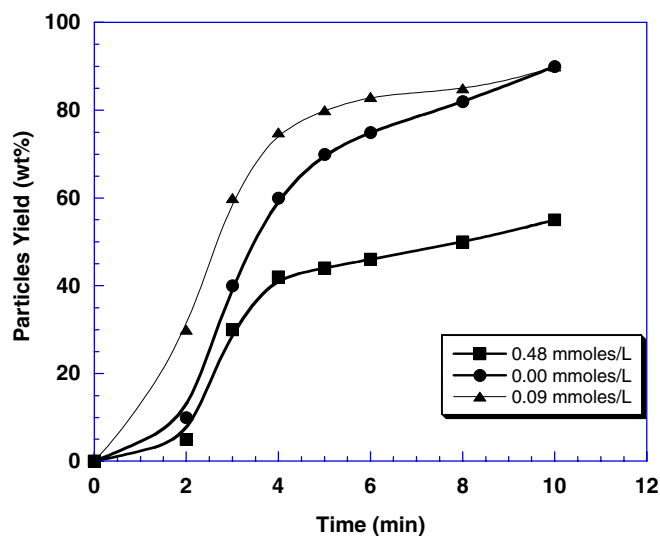


Fig. 6 The effect of VBIC on particle-formation kinetics. 48.51×10^3 mol of NIPAM, 0.30×10^3 mol of V50, 3.00×10^3 mol of MBA

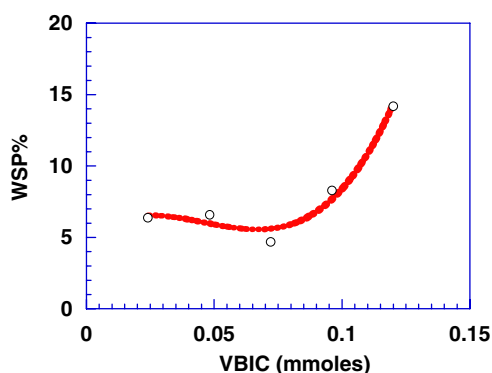


Fig. 7 The effect of VBIC monomer on water-soluble polymer formation. 48.51×10^3 mol of NIPAM, 0.30×10^3 mol of V50, 3.00×10^3 mol of MBA

was found to be highly sensitive to VBIC amount in the recipe. A similar tendency has been observed when a water-soluble charged comonomer (such as amino-containing) was used in a similar batch precipitation polymerization [5]. This can be attributed principally to the influence of VBIC on the nucleation step by contributing to a high number of particle formation.

The swelling ability (*i.e.* $swelling\ ratio = D_{20^\circ C}/D_{50^\circ C}$)³ of the elaborated microgel particles decreases as the VBIC amount increases in the polymerization recipe. This can be attributed to a reduction of the final particle size and also to the enhancement of the cross-linking density of the formed particles. The rapid analysis of the molecular weight of the formed water-soluble polymer revealed interesting results. In fact, the molecular weight (M_w) decreases drastically from 67,800 g/mol for free VBIC to 31,600 g/mol for

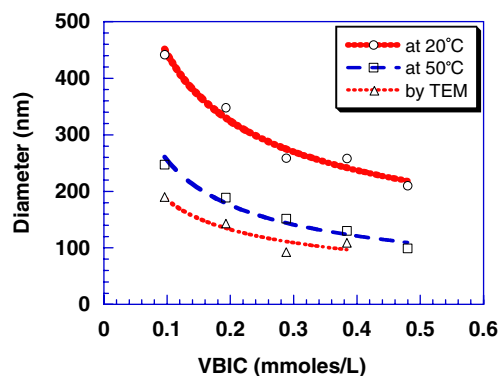


Fig. 8 Influence of VBIC monomer concentration on final particle size measured at 20 and 50 °C. 48.51×10^3 mol of NIPAM, 0.30×10^3 mol of V50, 3.00×10^3 mol of MBA

0.0481-mmol VBIC, which confirms the formation of low polymer chains vs VBIC amount.

Conclusions

The preparation of thiol containing poly(*N*-isopropylacrylamide)-based particles was examined by investigating various parameters as a systematic study.

The polymerization kinetic was marginally affected by VBIC monomer in the investigated concentration range. The tendency shows that the polymerization kinetic slightly increases with increasing VBIC amount in the polymerization recipe as evidenced by the initial slope of polymer conversion vs time. The VBIC monomer affects, principally, the particle yield and water-soluble formation. In fact, a low amount of VBIC monomer affects drastically the particle formation, and consequently, the final particle size. The water-soluble polymer was found to be related to various parameters. The increase of water-soluble polymer amount is associated to the use of a low concentration of the cross-linker agent, increasing the initiator amount and VBIC comonomer ratio over NIPAM.

It is interesting to notice that a weak amount of VBIC comonomer leads to a decrease in the average particle diameter, as generally observed in a radical surfactant-free emulsion polymerization when charged comonomer was used. The used monomer (VBIC) had a protected thiol function; then, we can assume that at the beginning of the polymerization reaction, the protected thiol was deprotected, and consequently, the resulting thiol acts as a good transfer agent. The formed oligomers during the first minutes of polymerization should have sufficient size to self-precipitate or to be cross-linked to form primary particles.

If this comonomer (VBIC) affects the polymerization, where is it located at the end of the polymerization? Three methods were used to detect the functional monomer on the particle surface. Even the isothiuronium salt was intro-

duced in moderate concentration and whatever the explored analysis method, it was not detected on the particle surface. This phenomenon confirms that the salt was a transfer agent, and the monomer was mainly incorporated in the polymer chain and contributes to the polymer core formation and consequently, not accessible and detectable using classical techniques.

The volume phase transition temperature (T_{VPT}) of the elaborated microgels was examined as a function of initial

polymerization recipe. The T_{VPT} temperature was not affected and found to be in the same range as for VBIC free microgels. Whereas, the LCST of the formed water-soluble polymer formed in the presence of VBIC comonomer was around 36 °C, slightly higher than that temperature that was generally observed in the case of linear homopoly(NIPAM) (32 °C).

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