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Article

# Property and Reactivity Relationships of Co<sub>3</sub>O<sub>4</sub> with Diverse Nanostructures for Soot Oxidation

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**ABSTRACT:** Cobalt oxide  $(Co_3O_4)$  nanostructures with different morphologies (nanocubes, nanoplates, and nanoflowers) were synthesized by a simple hydrothermal method and used for catalytic oxidation of soot particles. Through the study of the physicochemical properties of the catalysts, the key factors affecting the performance of soot oxidation were investigated. The results showed that all three kinds of  $Co_3O_4$  nanocrystals exhibited excellent low-temperature activity in catalytic oxidation of soot, and the  $Co_3O_4$  nanoflowers showed higher oxidation activity of soot compared with  $Co_3O_4$  nanocubes and  $Co_3O_4$  nanoplates, whose  $T_m$  was only 370 °C. The excellent activity of  $Co_3O_4$  nanoflowers was due to the large amount of  $Co^{3+}$  and lattice oxygen on their surface and highly defective structure, which promoted the adsorption and activation of oxygen species. The large crystallite size and few surface defects were the main reasons for the poor catalytic performance of  $Co_3O_4$  nanocubes. During soot oxidation, the crystallite size of the catalysts and the contact between the catalysts and soot played a significant role in the catalytic performance.



# **1. INTRODUCTION**

Diesel exhaust contains many pollutants, such as particulate matter, nitrogen oxides  $(NO_x)$ , and unburned hydrocarbons, which are harmful to human health and severely pollute the environment.<sup>1</sup> Owing to their small size, soot particles can be inhaled by the human body, causing asthma, bronchitis, lung cancer, and other diseases.<sup>2</sup> Soot particles are produced on burning hydrocarbon fuels. They are mainly carbon particles, containing a mixture of graphite sp<sup>2</sup>-bonded carbon and other mixed particles of organic and inorganic matter.<sup>3,4</sup> Soot particles appear as necklace-like agglomerates.<sup>5</sup>

Recently, diesel particulate filters (DPFs) have become the most economical, safe, and reliable exhaust aftertreatment technology for removing soot particles. However, soot particles accumulate on the filter, affording decreased filtration efficiency and increased engine backpressure. The spontaneous combustion temperature of soot particles is above 600 °C, and the engine exhaust temperature is between 200 and 500 °C.<sup>6</sup> It is an effective way to achieve active regeneration of DPFs by strategically injecting fuel to burn soot. However, this approach causes a high-temperature increase, which may damage DPFs and not be conducive to the fuel economy. Currently, catalytic combustion and DPFs are the most commonly used post-treatment technology. In this technology, the DPF traps soot particles in tail gas, reduces the spontaneous combustion temperature of soot using a catalyst, and makes soot burn at the diesel engine's exhaust temperature to realize the periodic passive regeneration of the filter.<sup>8,9</sup>

A suitable catalytic system is the key to lowering the soot oxidation temperature. Recently, a range of highly efficient catalysts such as noble metals, alkali metals, transition metal oxides, perovskite oxides, and rare earth oxides have shown good performances for removing soot particles.<sup>10</sup> To reduce the cost, several studies have focused on developing non-noble metal catalysts. Transition metal oxides exhibit an excellent redox performance owing to the change in valence in the oxidation reaction. Thus, they are widely used in catalytic chemistry in the fields of electrochemistry, formaldehyde catalytic oxidation, CO oxidation, and soot oxidation.<sup>11–14</sup>

Among them, cobalt oxides are inexpensive and have gained increasing attention, owing to their excellent catalytic activity in volatile organic compound (VOC) sensors, electrochemistry, high alcohol synthesis, phenol oxidation, methane, toluene combustion, soot catalytic oxidation, and many other fields.<sup>15</sup> Co<sub>3</sub>O<sub>4</sub> nanorods exhibited good stability, high sensitivity, and fast response and recovery time to detect VOCs.<sup>16</sup> Co<sub>3</sub>O<sub>4</sub> cube nanoelectrodes exhibited better sensitivity and lower limit of detection through the comparative study of the Co<sub>3</sub>O<sub>4</sub> spheres and cubes for H<sub>2</sub>O<sub>2</sub> electrochemical detection.<sup>17</sup> Furthermore, Co<sub>3</sub>O<sub>4</sub> nanooctahedrons had a strong long cycle and rate performance, good structural durability, and low charge transfer resistance,

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showing excellent electrochemical performance, through the study of the lithium storage properties.<sup>18,19</sup> The Co<sub>3</sub>O<sub>4</sub> hollow octahedral cage showed low initial irreversible loss and very high reversible capacity.<sup>20</sup> Ouyang et al. found that  $Co_3O_4$ (nanorods and nanowires)-supported Pt catalysts had stable CO<sub>2</sub> conversion and alcohol selectivity within 50 h, and some oxygen vacancies on the active surface of the Pt-Co<sub>3</sub>O<sub>4</sub>-p catalyst made it easier to be reduced.<sup>21</sup> Moreover, Co<sub>3</sub>O<sub>4</sub> nanorods exhibited excellent catalytic activity in the oxidation of phenol by the sulfate group, and they had good stability and small inactivation in several studies.<sup>22</sup> Furthermore, Co<sub>3</sub>O<sub>4</sub> exhibits excellent activity in catalytic combustion. Hu et al. found that in the catalytic combustion of methane, the catalytic activity follows the order  $Co_3O_4$  nanowires >  $Co_3O_4$  nanoribbons >  $Co_3O_4$  nanocubes.^{23} Ren et al. found that 3D-Co<sub>3</sub>O<sub>4</sub> nanoflowers had a large specific surface area and rich surface active oxygen, which improved their oxidation ability. Furthermore, the catalytic activity of 3D-Co<sub>3</sub>O<sub>4</sub> nanoflowers did not considerably decrease within 120 h, suggesting that the nanoflowers had long-term stability for toluene combustion.<sup>24</sup> In terms of CO oxidation, Wang et al. found that Co<sub>3</sub>O<sub>4</sub> nanorods showed excellent CO catalytic activity and durability owing to many oxygen defects on their surface.<sup>25</sup> Hu et al. reported that Co<sub>3</sub>O<sub>4</sub> nanoribbons had higher catalytic activity than Co<sub>3</sub>O<sub>4</sub> nanocubes in CO oxidation because the  $Co^{3+}$  sites on the (011) plane were more active than those on the (001) plane.<sup>26</sup> The importance of the shape and crystal plane effect has been proved, which is important for developing shape-controllable nanocrystal model catalysts. Given the soot catalytic combustion of Co<sub>3</sub>O<sub>4</sub>, Zhai et al. showed that  $Co_3O_4$  nanocubes with exposed (001) surfaces had more active Co<sup>3+</sup> and enhanced redox properties and surface lattice oxygen mobility, showing improved soot catalytic efficiency.<sup>27</sup> Meanwhile, Co<sub>3</sub>O<sub>4</sub> nanocubes had a clear shape, stable crystal phase, and strong stability to structural collapse.

The catalytic oxidation of soot is a typical heterogeneous catalytic reaction, which occurs at the three-phase boundary between the solid catalyst, soot particles, and the gas reaction (solid-solid-gas).<sup>28</sup> There are two main factors affecting the catalytic activity of soot: the contact efficiency between the soot and catalyst and the intrinsic activity of the catalyst.<sup>27</sup> To improve the catalytic oxidation activity of soot, the catalyst must be modified in the following two ways. First, the surface characteristics of catalysts play a key role in determining the combustion efficiency of soot.<sup>29</sup> Second, the role of catalysts is to transfer active oxygen species to the surface of soot to enable soot oxidation.<sup>30</sup> Therefore, it is necessary to design catalysts with an acceptable structure to expand the contact efficiency between soot and catalysts. Finding catalytic materials with high intrinsic activity is the main research task. Although many efforts have been made in the aspect of the facet-dependent reactivity of Co<sub>3</sub>O<sub>4</sub> nanocrystals, the essential correlation between the physicochemical properties of Co<sub>3</sub>O<sub>4</sub> and its performance in catalyzing soot oxidation is unclear. Herein, Co<sub>3</sub>O<sub>4</sub> with various nanostructures (nanotubes, nanoplates, and nanoflowers) is expected to produce a new and more efficient catalyst for soot particle oxidation. Three types of Co<sub>3</sub>O<sub>4</sub> nanocrystals with different facets were synthesized using a simple hydrothermal method. The structural morphology and physicochemical properties of the catalyst were studied using X-ray diffraction (XRD), Raman spectroscopy, Fourier transform infrared spectroscopy (FTIR),

and scanning electron microscopy (SEM).<sup>31,32</sup> The redox properties of the samples were studied via hydrogen– temperature-programmed reduction ( $H_2$ –TPR) and oxygen– temperature-programmed desorption ( $O_2$ –TPD),<sup>33</sup> The structure and electronic properties of the catalyst were studied using X-ray photoelectron spectroscopy (XPS).<sup>34</sup> Through the study of Co<sub>3</sub>O<sub>4</sub> nanocrystals with different facets, the oxidation efficiency of catalysts with different facet shapes of the same element is explored. This is expected to prepare more efficient catalysts in the field of soot catalysis.

#### 2. EXPERIMENTAL SECTION

**2.1. Catalyst Preparation.**  $Co_3O_4$  nanocrystals with diverse nanostructures, including nanocubes, nanoplates, and nanoflowers, were synthesized using a template-free hydro-thermal synthesis method. Certain amounts of  $Co(NO_3)_2$ .  $6H_2O$  and 0.02 mol NaOH were dissolved in 80 mL of deionized water via magnetic stirring for 30 min. The resulting solution was transferred to a stainless-steel autoclave lined with polytetrafluoroethylene (PTFE) and reacted at 180 °C for 5 h. The reaction was centrifuged five times with deionized water after cooling to room temperature (25 °C), dried at 80 °C for 24 h, and finally calcined at 500 °C for 4 h in air. The resulting  $Co_3O_4$  nanocubes were labeled Co-c.

 $Co_3O_4$  nanoplates were synthesized using the following procedure. A certain amount of  $Co(NO_3)_2 \cdot 6H_2O$  was dissolved in a mixture containing 10 mL of ethanol and 10 mL of deionized water and stirred to form a clear solution. Subsequently, 0.8 g of NaOH was dissolved in 50 mL of deionized water and added to the abovementioned solution. The resulting solution was stirred for 30 min, transferred to a stainless-steel autoclave lined with PTFE, sealed, and heated to 100 °C for 12 h. The synthesized product was centrifuged five times with deionized water after cooling to room temperature, dried at 80 °C overnight, and finally calcined at 300 °C for 3 h in air. The  $Co_3O_4$  nanoplates obtained were called Co-p.

 $Co_3O_4$  nanoflowers were synthesized using the following procedure. A certain amount of  $Co(NO_3)_2 \cdot 6H_2O$  was dissolved in 20 mL of deionized water, mixed with 4 g of urea, and stirred for 30 min. The resulting mixture was transferred to a stainless-steel autoclave lined with PTFE and kept in an oven at 110 °C for 12 h. After cooling to 25 °C, the synthesized product was centrifuged five times with deionized water and dried overnight in an oven at 50 °C. Finally, it was calcined at 300 °C for 3 h in air. The resulting  $Co_3O_4$  nanoflowers were labeled Co-f.

**2.2. Catalyst Characterizations.** The crystallographic information of  $Co_3O_4$  with various nanostructures was obtained by the XRD method and compared with the diffraction peak of the standard card to determine the crystalline phases of the samples. XRD analysis of the catalysts was carried out using an Ultima IV X-ray diffractometer from Japan. Copper target Ka radiation, power 3 KW, scan speed  $10^{\circ}$  min<sup>-1</sup>, and scan angle  $10-80^{\circ}$ .

The specific surface areas and pore size distributions of the catalyst samples were measured by nitrogen adsorption at liquid nitrogen temperature using a surface area analyzer (ASAP 2460, Micromeritics).

The micromorphology and grain size of the catalyst samples were measured using a Zeiss Sigma 300 scanning electron microscope. The field emission was 15 kV acceleration voltage. Before the test, gold was sprayed on the sample for 30 s to enhance the conductivity of the samples.



Figure 1. (A) Catalytic performance of Co<sub>3</sub>O<sub>4</sub> on soot oxidation and (B) stability tests of catalyst Co-f.

H<sub>2</sub>-TPR and O<sub>2</sub>-TPD were performed using a PCA-1200 chemisorption analyzer. The 30 mg samples were pretreated in a nitrogen atmosphere at 100 °C for 10 min. After dropping to room temperature, the samples were purged with a mixture of nitrogen and hydrogen/argon oxygen, and the TCD was turned on. After the baseline was stabilized, the temperature was increased to 900 °C with 10 °C min<sup>-1</sup> program.

Raman spectroscopy is an important way to detect the surface defects of catalysts. The Raman spectrum analysis was carried out on the Thermo Fisher DXR2 explicit differential spectrometer with an excitation wavelength of 532 nm and a laser power of 3 MW.

FTIR adopted the Fourier transform infrared spectrometer Tensor 27 of Bruker company in Germany, with a resolution of  $4 \text{ cm}^{-1}$  and a scanning range of  $400-4000 \text{ cm}^{-1}$ . First, potassium bromide was ground into fine particles; then, the catalyst sample and potassium bromide were mixed and ground for 5 min according to a mass ratio of 1 to 100 MPa, the mixture was fully refined to prevent the effect of scattering on the spectrum, the tablets were pressed under a pressure of 10 MPa in the tablet press, and the samples with good permeability were put into the instrument for testing.

The element composition and main valence state of the catalyst were tested by XPS. The photoelectric spectrometer Thermo Scientific K-Alpha was used in the experiment, the Al Ka ray ( $h\nu = 1486.6$  eV) was used as the X-ray source, the voltage was 12 kV, and the C 1s = 284.80 eV binding energy (BE) was used as the energy standard for charge correction.

**2.3. Catalyst Activity Evaluation.** This experiment used Printex-U carbon black (Degussa, Germany) with a particle size of 25 nm to substitute the soot particles in exhaust. The catalyst activity was evaluated via thermogravimetric analysis (TGA, TGA-Q500). Briefly, 5 mg of soot particles and 50 mg of the catalyst were mixed well in a mass ratio of 1:10. The mixed samples were placed on an aluminum crucible and heated from room temperature to 800 °C at a heating rate of  $10 \text{ °C min}^{-1}$  in air (100 mL/min). The catalytic activity of the catalysts for soot oxidation was evaluated by measuring the mass change in soot particles before and after the reaction and by calculating the conversion rate of soot particles. 1-1 presents the formula for calculating the soot conversion rate.

$$\eta = \frac{[\text{Soot}]_{A} - [\text{Soot}]_{B}}{[\text{Soot}]_{A}} \times 100\%$$
(1-1)

where  $\eta$  is the soot conversion rate,  $[\text{Soot}]_A$  is the soot quality before the reaction, and  $[\text{Soot}]_B$  is the soot quality after the reaction. The catalyst activity associated with the catalytic oxidation process of soot particles was evaluated based on the soot-particle conversion temperatures.  $T_{50}$  and  $T_{90}$  represented the temperatures when the soot particle conversion rates were 50 and 90%, respectively, and  $T_m$  is the maximum oxidation rate temperature. When the conversion rate is the same, a smaller value means the catalyst has a better catalytic effect on soot particles.

## 3. RESULTS AND DISCUSSION

3.1. Catalytic Performances of  $Co_3O_4$  for Soot Oxidation. Figure 1 shows the conversion curve of the

Table 1. Comparative Activity Evaluation of Some Co<sub>3</sub>O<sub>4</sub> Catalysts Reported in the Literature for Soot Oxidation

catalysts	$T_{50}/^{\circ}\mathrm{C}$	$T_{90}/^{\circ}\mathrm{C}$	$T_{\rm m}/^{\circ}{\rm C}$	Reference
without catalyst	609	638	620	this work
Co-c	438	535	442	this work
Со-р	382	513	386	this work
Co-f	369	474	370	this work
Co <sub>3</sub> O <sub>4</sub> spherical flower	437	474	482	35
Co <sub>3</sub> O <sub>4</sub> urchin	406	439	440	35
Co <sub>3</sub> O <sub>4</sub> sheet	377	412	405	35
Co <sub>3</sub> O <sub>4</sub> pyramid	361	396	385	35
Co <sub>3</sub> O <sub>4</sub> nanocubes			423	27
Co <sub>3</sub> O <sub>4</sub> truncated octahedrons			435	27
Co <sub>3</sub> O <sub>4</sub> octahedrons			448	27
Co <sub>3</sub> O <sub>4</sub>	387.3	428.7		7
Co <sub>3</sub> O <sub>4</sub>	580	621	600	33
Co <sub>3</sub> O <sub>4</sub>	545			36
<i>.</i>				

oxidation process of soot particles catalyzed by  $Co_3O_4$  and the stability tests of catalyst Co-f. Table 1 summarizes the  $T_{50}$ ,  $T_{90}$ , and  $T_m$  of the catalyst samples and compares the activity of some  $Co_3O_4$  catalysts reported for soot oxidation. Soot begins to oxidize at 500 °C without a catalyst, and  $T_m$  is 620 °C, as shown in Figure 1. Using the catalyst, the soot was oxidized at 300 °C, and  $T_m$  was reduced by 178–250 °C, indicating that the prepared catalysts with different facet shapes exhibited high catalytic activity at low temperatures. Among them, the nanoflower-shaped Co-f exhibited the best low-temperature oxidation activity, followed by the nanoplate-shaped Co-p and



Figure 2. XRD patterns of Co<sub>3</sub>O<sub>4</sub> with different nanostructures.

Table 2. Grain Diameter and Textural Properties of  $Co_3O_4$  with Different Nanostructures

sample	peak position (°)	FWHM (°)	D (nm)	$surface \\ area \\ (m^2 g^{-1})$	average pore size (nm)	pore volume (cm <sup>3</sup> g <sup>-1</sup> )
Co-c	36.8	0.1966	42.12	5.389	10.07	0.0119
Co-p	36.8	0.6705	12.35	51.52	16.45	0.2038
Co-f	36.8	0.6662	12.43	57.09	11.50	0.1621



Figure 3.  $N_2$  adsorption-desorption isotherms and pore size distributions (inset).

the nanocube-shaped Co-c. The  $T_{\rm m}$  of these three catalysts was in the order Co-f < Co-p < Co-c, which is much lower than that of soot  $T_{\rm m} = 620$  °C. Co-f exhibited a high oxidation activity at low temperatures; its  $T_{50}$ ,  $T_{90}$ , and  $T_{\rm m}$  were only 369, 474, and 370 °C, respectively. The results show that the soot oxidation activity of Co-f was higher than that of Co-p and Coc at low temperatures. After three cycles of experiments, the activity of Co-f oxidized soot remained stable. The activity of Co-c was the poorest.

**3.2.** Characterization of the Catalysts. 3.2.1. XRD Analysis. The crystal structures of the  $Co_3O_4$  materials were examined using XRD. Figure 2 displays the XRD patterns of  $Co_3O_4$  with different nanostructures. The three catalysts are

spinel cubic Co<sub>3</sub>O<sub>4</sub> phases. The characteristic peaks of the  $Co_3O_4$  catalysts at  $2\theta$  values of 19.0, 31.3, 36.8, 38.5, 44.8, 55.6, 59.4, and 65.2°, respectively, correspond to the crystal plane parameters of spinel Co<sub>3</sub>O<sub>4</sub> (111), (220), (311), (222), (400), (422), (511), and (440) (JCPDS NO.43-1003);<sup>24,37</sup> no other impurities were observed, and the XRD peaks of the three catalysts were strong and narrow. The catalysts exhibited high purity, and they all exhibited a high degree of crystallization. The Scherrer equation was used to calculate the crystallite size of Co<sub>3</sub>O<sub>4</sub> using the main XRD peak of (311), as shown in Table 2. The grain sizes of Co-p, Co-f, and Co-c were 12.35, 12.43, and 42.12 nm, respectively. Co-c exhibited the largest grain diameter and the lowest catalytic activity combined with the performance test results of the catalysts, while Co-f and Co-p exhibited high soot catalytic activity because of their small grain diameters. Furthermore, there was little difference between the activities of Co-f and Co-p when the grain diameter was small. The catalytic activity varied with the particle size, crystallinity, and crystal shape of the catalyst. A smaller catalyst particle size indicated better carbon soot oxidation activity.

Figure 3 shows the N<sub>2</sub> adsorption–desorption isotherms and the pore size distributions of the three catalysts. The curves for all the catalysts exhibited classical type-IV isotherms with a hysteresis loop, showing a characteristic mesoporous structure.<sup>38</sup>Table 2 lists the textural properties in terms of the average pore size, Brunauer–Emmett–Teller (BET) surface area, and pore volume. The BET surface areas of Co-c, Co-p, and Co-f were 5.389, 51.52 and 57.09 m<sup>2</sup> g<sup>-1</sup>, respectively. The pore volumes of Co-c, Co-p, and Co-f were 0.0119, 0.2038, and 0.1621 cm<sup>3</sup> g<sup>-1</sup>, respectively. Co-f had the largest specific surface area and good pore volume, which is one of the main reasons for its superior catalytic activity. However, the smallest specific surface area, average pore size, and pore volume of Coc are one of the main reasons for its poorest catalytic activity.

3.2.2. Scanning Electron Microscopy. The micromorphologies of the Co<sub>3</sub>O<sub>4</sub> catalysts with different nanostructures were studied using SEM, as shown in Figure 4. Co-c, Co-p, and Co-f exist as nanocubes, nanoplates, and nanoflowers, respectively. Figure 4a shows a smooth  $Co_3O_4$  nanocube structure with four exposed surfaces with a mean size of ~400 nm; Figure 4b shows a rough round  $Co_3O_4$  nanoplate structure, ~100 nm in diameter. The material comprises irregular nanosheets with a Co<sub>3</sub>O<sub>4</sub> nanoflower shape and voids of various sizes inside the nanoflower (Figure 4c). The three catalysts have good crystallinity and an unmistakable shape, which concurred with the XRD results. Co-f exhibits the best soot oxidation activity at low temperatures owing to the unique nanoflower structure, which improves the contact efficiency with soot particles and oxygen. Figure 4d shows SEM of Co-f after the reaction with soot, and its flower-like structure remains stable before and after the reaction, which is the main reason why it maintains stable catalytic activity.

3.2.3.  $H_2$ -TPR Analysis. The reducibility of Co<sub>3</sub>O<sub>4</sub> catalysts with different nanostructures was investigated using H<sub>2</sub>-TPR, which was mainly used to study the reduction ability of the catalyst samples. Figure 5 shows the H<sub>2</sub>-TPR profiles of the three shapes of Co<sub>3</sub>O<sub>4</sub> nanocrystals. All the catalysts exhibited two reduction peaks below 406 °C, suggesting that the reduction process of Co<sub>3</sub>O<sub>4</sub> included two processes: from Co<sup>3+</sup> to Co<sup>2+</sup> and from Co<sup>2+</sup> to metal Co<sup>0.24</sup> For the first reduction peak of Co<sup>3+</sup> to Co<sup>2+</sup>, the reduction peak temperatures of Co-f and Co-p were 299 and 290 °C, respectively, which were much



Figure 4. SEM images of different morphologies of  $Co_3O_4$ : [(a1,a2) Co-c; (b1,b2) Co-p; (c1,c2) Co-f; (d1) Co-f after the first reaction with soot; and (d2) Co-f after the third reaction with soot].



Figure 5.  $H_2$ -TPR profiles of  $Co_3O_4$  with different nanostructures.



Figure 6.  $O_2$ -TPD profiles of  $Co_3O_4$  with different nanostructures.

lower than the reduction peak temperature of Co-c (345 °C). The second reduction peak was due to the double electron reduction process from  $\text{Co}^{2+}$  to metal  $\text{Co}^{0}$ . The second reduction peak of Co-f was observed at 347 °C, which was 35 and 59 °C lower than that of Co-p and Co-c, respectively. Therefore, the low-temperature reducibility of Co-f was better



Figure 7. Raman spectra of  $Co_3O_4$  with different nanostructures.



Figure 8. FTIR spectra of  $Co_3O_4$  with different nanostructures.

than that of the other two samples. Figure 5 shows that the reduction peak of Co-f shifted the most toward the low temperature. Co-f had better low-temperature reducibility than the other two samples. The Co-f reduction peak shifted toward the low-temperature portion, whereas the Co-c peak exhibited the widest temperature range. The low-temperature reducibility of the catalysts was in the order Co-f > Co-p > Co-c.



Figure 9. XPS spectra of Co 2p over  $Co_3O_4$  with different nanostructures.



Figure 10. XPS spectra of O 1s over  $\text{Co}_3\text{O}_4$  with different nanostructures.

This suggests that Co-f has stronger reducibility related to the catalytic activity, so the catalytic activity of Co-f for soot oxidation is the highest; this is consistent with the test results of catalyst performance.

3.2.4.  $O_2$ -TPD Analysis. Figure 6 shows the  $O_2$ -TPD diagram of the catalysts, which shows how well the catalysts can adsorb and activate oxygen. Generally, the order of oxygen desorption in metal oxides is as follows: oxygen  $(O_2) >$  oxygen molecular anion  $(O_2^-) >$  oxygen ion  $(O^-) >$  lattice oxygen  $(O^{2-})$ .<sup>39</sup>  $O_2^-$  and  $O^-$  are due to the molecular adsorption oxygen and chemisorption, respectively. Surface-active oxygen desorbs easily from metal oxide catalysts, whereas lattice

oxygen is more challenging.<sup>39</sup>Figure 6 shows a desorption peak at ~800 °C owing to the large amount of lattice oxygen precipitated during the thermal decomposition of  $Co_3O_4$ . The lowest desorption peak temperature of Co-f was 783 °C, followed by Co-p (800 °C). The highest desorption peak temperature of Co-c was 831 °C. Co-f can decompose a large amount of lattice oxygen at lower temperatures, showing better activation performance. Co-f had the largest desorption peak area and the highest concentration of surface-decomposed lattice oxygen, exhibiting the best catalytic capacity for soot oxidation; the results are consistent with those of H<sub>2</sub>–TPR.

3.2.5. Raman Analysis. Figure 7 shows the Raman spectra of all the catalysts. Four obvious peaks were observed at 486 cm<sup>-1</sup> (E<sub>g</sub>), 524 cm<sup>-1</sup> (F<sub>2g</sub><sup>2</sup>), 622 cm<sup>-1</sup> (F<sub>2g</sub><sup>3</sup>), and 692 cm<sup>-1</sup>  $(A_{1g})$ , which are consistent with the characteristics of the spinel Co<sub>3</sub>O<sub>4</sub> phase.<sup>27</sup> No other impurity peaks are found, which is consistent with the results of XRD. The XRD peak of the catalyst shifts to a low wavenumber, and the FWHM increases in the order Co-f > Co-p > Co-c, which may be related to the high-defect structure of the spinel. The increase in the surface defect structure of the catalyst was beneficial to the formation of oxygen vacancies, which promoted the adsorption and activation of oxygen species and subsequently promoted soot oxidation. Among them, the defect structure of Co-f was more than that of Co-p and Co-c, so it exhibited higher soot oxidation activity. This is consistent with the abovementioned results of H<sub>2</sub>-TPR and O<sub>2</sub>-TPD.

3.2.6. Fourier Transform Infrared Spectroscopy. The FTIR spectra of the catalysts showed four absorption peaks in the  $400-4000 \text{ cm}^{-1}$  range (Figure 8), in which the absorption peak at 3450 cm<sup>-1</sup> corresponds to the characteristic peak of the stretching vibration of the OH group in  $Co(OH)_2$ . The absorption peak at 1630 cm<sup>-1</sup> was caused by the stretching vibration of NO3<sup>-</sup>, and the absorption peaks at 667 and 590 cm<sup>-1</sup> were caused by the stretching vibration of Co–O in the metal oxide lattice.<sup>40</sup> A characteristic peak of NO3<sup>-</sup> was observed in the spectrum, but NO<sub>3</sub><sup>-</sup> was not detected by XRD because NO3<sup>-</sup> entered the structure and did not form a chemical bond with  $Co(OH)_2$ , which explains why there was no hydrogen bonding in the structure. No characteristic peak of stretching vibration of Co-OH was observed in the spectra (Figure 8), indicating that all the final products had transformed to a pure phase  $Co_3O_4$ . The change in the abovementioned stretching vibration absorption peak reflected the change in the phase structure of the catalysts during the synthesis process, which was consistent with the XRD results.

3.2.7. X-ray Photoelectron Spectroscopy Analysis. The surface element composition and valence state of  $Co_3O_4$  nanocrystals were measured using XPS, including Co 2p and O 1s photoelectron spectroscopy. Figure 9 shows the Co 2p spectra of the catalysts. The Co 2p spectra of  $Co_3O_4$  nanocrystals have two main peaks near 780 and 795 eV, which were assigned to Co  $2p_{3/2}$  and Co  $2p_{1/2}$  orbitals, respectively. The difference in BE between Co  $2p_{3/2}$  and Co

Table 3. BE of the Co 2p and O 1s Core Levels and the Ratio of  $Co^{3+}/Co^{2+}$  and  $O_{ads}/O_{latt}$  for the As-Prepared Catalysts

	Co 2p			O 1s		
catalysts	Co <sup>2+</sup> (eV)	Co <sup>3+</sup> (eV)	$Co^{3+}/(Co^{2+} + Co^{3+})$	O <sub>ads</sub> (eV)	O <sub>latt</sub> (eV)	$O_{ads} / (O_{ads} + O_{latt})$
Co-c	781.3/796.5	779.6/794.6	0.527	530.9	529.5	0.479
Co-p	781.4/796.6	779.3/794.4	0.551	531.1	529.4	0.506
Co-f	781.4/796.3	779.2/794.3	0.592	530.8	529.4	0.603

 $2p_{1/2}$  peaks was 15 eV, showing that cobalt oxides existed in the form of  $Co_3O_4$ , which is in accordance with a previous report.<sup>24</sup> Both Co  $2p_{3/2}$  (~779.3 eV) and Co  $2p_{1/2}$  (~794.7 eV) were attributed to the characteristic peaks of  $Co^{3+}$  cations, while the characteristic peaks in Co  $2p_{3/2}$  (near 781.6 eV) and Co  $2p_{1/2}$  (near 796.5 eV) generally belonged to  $Co^{2+}$  in the catalysts.<sup>27</sup> The characteristic peak intensity of  $Co^{2+}$  cations was small, indicating only a small part of  $Co^{2+}$  in  $Co_3O_4$ nanocrystals, mainly in the form of  $Co^{3+}$ . The ratio of  $Co^{3+}/$ ( $Co^{2+} + Co^{3+}$ ) of Co-f was considerably higher than that of Co-c and Co-p, indicating more exposed  $Co^{3+}$  on the surface of Co-f because of its unique nanoflower structure and small particle size. More  $Co^{3+}$  on the catalyst surface affords higher catalytic activity.

Figure 10 shows the O 1s XPS spectra of the  $Co_3O_4$  nanocrystals. The spectra of O 1s can be deconvoluted into three peaks with their BE near 529.4, 530.9, and 533.1 eV, belonging to the surface lattice oxygen  $(O_{latt}: O^{2-})$ , surface chemisorbed oxygen  $(O_{ads}: O_2^{2-} \text{ and } O_2^{-})$ , and chemisorbed water  $(O_w)$ , respectively.<sup>41</sup> Typically, the  $O_{ads}/(O_{ads} + O_{latt})$  ratio represents the active oxygen content on the catalyst surface. The active oxygen content and catalytic activity increase with increasing molar ratio.<sup>42</sup> The  $O_{ads}/(O_{ads} + O_{latt})$  ratio decreased in the following order (Figure 10 and Table 3): Co-f > Co-c, which was consistent with the sequence of catalytic activity. Co-f, possessing more  $Co^{3+}$  and  $O_{ads}$  species, exhibited better catalytic performance.

## 4. CONCLUSIONS

A series of  $Co_3O_4$  materials with various nanostructures, including nanocubes, nanoplates, and nanoflowers, were synthesized using a simple template-free hydrothermal method and showed excellent catalytic activity for the oxidation of soot particles. The three types of nanostructured Co<sub>3</sub>O<sub>4</sub> crystals produced had exceptional purity and crystallinity, which exhibited clear cubic, plate-like, and floral morphologies. The Co<sub>3</sub>O<sub>4</sub> nanoflowers showed better soot oxidation activity than the Co<sub>3</sub>O<sub>4</sub> nanocubes and nanoplates because of the presence of a large number of Co<sup>3+</sup> cations and a large amount of lattice oxygen on the surface of Co<sub>3</sub>O<sub>4</sub> nanoflowers prone to lowtemperature redox reactions. The Co<sub>3</sub>O<sub>4</sub> nanoflowers have highly defective structures, which are favorable for the formation of oxygen vacancies, promoting the adsorption and activation of oxygen species for soot oxidation. Furthermore, Co<sub>3</sub>O<sub>4</sub> nanoflowers have a good shape and spatial structure, increasing the contact area with soot particles and yielding improved soot catalytic efficiency. However, Co<sub>3</sub>O<sub>4</sub> nanocubes had the poorest catalytic performance. This is mostly because of their large grain size and less defective surface structure, affording poor redox ability and less lattice oxygen. One of the key factors to achieve improved catalytic activity is increasing the contact area between the catalysts and soot particles.

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#### Notes

The authors declare no competing financial interest.

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