

http://pubs.acs.org/journal/acsodf

<u>⊷</u>©()()()()()

Article

Microscopic Insights and Optimization of the CH₄–CO₂ Replacement in Natural Gas Hydrates

Yinglong Zhang, Mao Cui, Dexiang Li, and Gongming Xin*



benefit from both the deep diffusion of CO_2 in the higher temperature stage and the rapid rebuilding of CO_2 hydrate within just nanoseconds caused by the memory effects in the lower temperature stage. The results also reveal that the optimal lower temperature duration and frequency should be moderate. Decreasing the lower temperature value can distinctly enhance CO_2 capture and hydrate stability. This study can help understand the mechanisms of CH_4-CO_2 replacement under different temperature and pressure conditions, especially at temperature transitions, and proposes a potentially effective method to achieve large-scale carbon sequestration in the hydrate.

1. INTRODUCTION

The lack of energy has been drawing increasing attention due to the rapid development of industry and society.^{1,2} Meanwhile, there is an obvious conflict that traditional fossil fuels have caused serious pollution after utilization for several decades.^{3,4} In view of the immaturity and instability of new energy sources,^{5–7} increasing attention is being paid to natural gas,⁸ a kind of clean energy that has been proven to be widely stored in natural gas hydrates (NGH). Nowadays, three kinds of hydrates have been found: type I, type II, and type H.⁹ For NGH, it is mainly CH₄ hydrate, which belongs to type I.^{10,11} In the standard case, each cubic meter of NGH can produce 164 cubic meters of methane gas after decomposition, which is why NGH is a kind of significant energy source.¹²

oscillations can achieve comprehensive improvements, which

The main extraction methods of NGH are depressurization, thermal stimulation, hydrate inhibitor injection, and the CO_2 replacement method.^{9,10} The principle of the first three methods is to make NGH out of the conditions, where it can stay stable. The principle of the gas exchange method is to replace methane in the NGH by using CO_2 .¹¹ Among the four methods mentioned above, depressurization is the most popular, and the other three are often used as auxiliary methods. However, due to the imperfect production technology and complex reservoir characteristics, the first three methods may lead to large-scale uncontrollable decomposition of NGH and further

loss and damage.^{13–15} First, NGH play an indispensable role in geological stability. Hydrate and sand support each other to ensure a stable geologic structure.^{16,17} Without hydrate, geological disasters are inevitable.¹⁸ More seriously, it can set off a series of chain reactions. For instance, undiscovered hydrate reservoirs can be destroyed and release much CH4, causing greenhouse effects, sea level rise, climate deterioration, and ecological unbalance.^{19,20} Second, the uncontrollable decomposition of NGH produces much gas and water. When they flow out, a lot of sand can be carried out, resulting in the breakdown of facilities and even the shutdown of the whole hydrate exploitation project.^{21,22} In consideration of the risks mentioned above, more and more researchers have begun to realize the significance of the gas exchange method.^{23–25} Different gases can be utilized to replace the CH_4 in hydrate, among which CO_2 is the most widely used gas.^{26,27} For one thing, due to the higher stability of CO₂ hydrate than CH₄ hydrate, the newly formed

10000 ps

15000 ps

20000 ps

Received:October 9, 2022Accepted:November 30, 2022Published:December 12, 2022

5000 10000 15000 20000 Time (ps)







Figure 1. (a) Initial configuration of the simulation system (black arrows: CH_4 molecules at different depths); (b) simulation conditions and phase diagrams of CH_4 hydrate and CO_2 hydrate.

CO₂ hydrate reduces the risk of uncontrollable decomposition of hydrates, sand production, and other secondary disasters mentioned above.^{28,29} For another, the CO₂ replacement method can help not only extract CH₄ from NGH but also realize CO₂ storage and reduce the greenhouse effects. Therefore, a recycle without carbon emissions can be formed, which is supported by the policies of many countries.^{30,31} In addition, the development of the carbon trading market also provides extra benefits for the gas exchange method.^{32,33} At present, many experimental and computational investigations have been performed to verify the feasibility of the CO₂ replacement method in aspects of thermodynamics and kinetics.^{34–38} However, it cannot be ignored that the low replacement efficiency of the gas exchange method limits its application and promotion.^{37,39,40} Possible improving methods mainly include extending the soaking time,⁴¹ using smallmolecule gases, 27,42 changing the phase of CO_2 , 43,44 using hydrate promoters or inhibitors,^{45,46} and selecting the proper temperature and pressure. Therein, selecting the proper temperature and pressure is closest to the field test because it is easy to realize with the assistance of the thermal stimulation method and depressurization method.

Zhang et al.⁴⁷ conducted experiments at different pressures (3.6, 4.0, and 4.5 MPa) and different temperatures (below and above the freezing point) to study how pressure and temperature affect the replacement process. The results indicated that higher pressure and temperature are conducive to improving the average replacement rate and efficiency. Xu et al.⁴⁸ investigated the effects of pressure on the replacement process by in situ Raman analysis. It was found that the replacement rate is positively influenced by the operating pressure. Gambelli and Rossi⁴⁹ carried out eight experimental tests to compare the effects of two different thermal stimulations on the replacement process. They found that increasing the temperature first and then introducing CO₂ required much less thermal energy to finish the replacement process than introducing CO₂ first and then increasing the temperature. Zhang et al.⁵⁰ combined thermal stimulation and gas exchange methods, and the CH₄ replacement percentage of an upper limit of 64.63% was achieved. Li et al.⁵¹ injected mixed CO₂ and N₂ into gas hydrates and found that there was decomposition and replacement in this process at the same time. The results indicated that higher temperature and lower pressure can promote the decomposition and improve the gas recovery efficiency. Mok et al.⁵ investigated the effects of different pressures (10.0–18.5 MPa) and temperatures (274.2-277.2 K) on the CH₄-CO₂ + N₂ replacement process. It was shown that at 274.2 K, the extent of replacement increased with the injection pressure of CO_2 and N_2 . Meanwhile, at a higher temperature, the extent of replacement did not change. Chen et al.⁵³ studied the behavior of methane hydrate during depressurization-assisted CO_2 replacement. They found that depressurization assistance can enhance the CO_2 utilization efficiency. Although many works have been done to test different temperature and pressure conditions, there are still no definite principles and related explanations. Some previous studies have even presented contrary research conclusions, especially on the influencing pattern of pressure.⁵⁴ In addition, most previous researchers focused on experimental studies and observed the macroscopic phenomenon. Few have focused on the micro-mechanisms of the replacement process under different conditions and their differences. This may lead to unclarities on some key issues, such

To monitor and explain the microscopic process, the molecular dynamics (MD) simulation is regarded as an effective method, which can provide more general and fundamental insights. Nowadays, MD simulation has been widely utilized in studying various behaviors of NGH.^{55–58} For CO₂ hydrate and CO₂/CH₄ mixed hydrate, MD simulation has also shown satisfying applicability and provided valuable insights.^{59–61} In this work, the MD method is used to analyze and evaluate the CH₄–CO₂ replacement at different constant temperatures (270–290 K) and pressures (1–10 MPa). As a novel optimization strategy, various temperature oscillations are introduced. The effects of the lower temperature duration, the lower temperature value, and the frequency of oscillations are investigated and explained.

as whether the CO_2 is firmly trapped by the hydrate, or silted in

the pore space, or just dissolved in the liquid.

2. METHODOLOGY

2.1. Model and Simulation Details. At first, the initial type I hydrate structure is constructed according to previous X-ray analysis,⁶² based on which a $3 \times 3 \times 3$ supercell is built. Then, 200 CO₂ molecules are added to the surfaces of CH₄ hydrate. The total amount of CO₂ molecules is 400 due to the fact that there are two surfaces of CH₄ hydrate. Subsequently, energy minimization is carried out based on the steepest descent, ABNR, and quasi-Newton methods. Finally, the whole model of the simulations is shown in Figure 1a, containing 1242 H₂O molecules, 216 CH₄ molecules, and 400 CO₂ molecules. The simulation model is divided into three regions: region I, region II, and region III. At the initial time, all the CO₂ molecules are in the fluid phase (region I and region III). Meanwhile, the CH₄



Figure 2. (a) Changes in the amounts of escaped CH_4 molecules over time at different temperatures; (b) RDF curves between CH_4 molecules and H_2O molecules at different temperatures; (c) changes in the amounts of captured CO_2 molecules over time at different temperatures; (d) RDF curves between CO_2 molecules and H_2O molecules at different temperatures; (e) changes in the amounts of hydrated H_2O molecules over time at different temperatures; (f) RDF curves between H_2O molecules at different temperatures.

molecules are arranged at different depths of the hydrate phase (region II).

For MD simulation, it is vital to ensure the accuracy of the potential energy functions. In this work, the TIP4P/Ice model⁶³ is used for H₂O, which is more accurate to simulate the solid water phase than the previous TIP4P model.⁶⁴ The OPLS-AA model⁶⁵ is utilized for CH₄, which considers five points of methane molecules rather than a single point. In this way, more accurate results can be obtained than using single-point models such as OPLS-UA.^{64,66} The EPM2 model⁶⁷ is applied to CO₂. Previous investigations have been conducted to verify that the models used in this work are almost the most superior models to reproduce the real properties of hydrate.^{66,68,69} For atoms in different molecules, the Lorentz-Berthelot mixing rule is used to determine their parameters of Lennard-Jones potentials. MD simulations of 20,000 ps under the NPT ensemble are carried out with a time step of 1 fs. The rigid bonds and angles are fixed by the SHAKE algorithm.⁷⁰ The velocity-Verlet algorithm is used to calculate Newton's equation of motion. The cutoff for short-ranged interactions is set to 15 Å, and the long-ranged Coulomb interactions are calculated by the PPPM algorithm. Periodic boundary conditions are applied in all directions. The simulation conditions and typical phase equilibrium diagrams of CH_4 hydrate and CO_2 hydrate⁷¹ are shown in Figure 1b. All the MD simulations are carried out by LAMMPS, an open-source program."

2.2. Evaluation and Description of CH_4-CO_2 Replacement. Evaluation metrics need to be determined first to evaluate the CH_4-CO_2 replacement. According to the unique significance of the CO_2 replacement method, in this work, the performances of the CH_4-CO_2 replacement processes are evaluated in three aspects: CH_4 production, CO_2 sequestration, and hydrate stability. Correspondingly, the escape of CH_4

molecules, the capture of CO_2 molecules, and the maintenance of the hydrate cage structure need to be monitored and evaluated on the microscale. It is worth mentioning that the better the hydrate cage structure is maintained, the better the hydrate stability is maintained, and the better the formation can be cemented and supported by hydrate.⁵⁴ In order to achieve the evaluation and elucidate the micro-mechanisms, the dynamic position distributions of different molecules, the radial distribution functions (RDFs), the Chill+ structure identification algorithm,³⁹ and the hydrate configurations are selected to characterize the replacement processes.

Article

Depending on the degree of the CH_4-CO_2 replacement, CH_4 molecules at different depths are replaced by CO_2 molecules. In accordance with the literature, ⁶⁹ in this work, the CH_4 molecules that spread into region I and region III are regarded to have escaped. And the CO_2 molecules that spread into region II are considered to have been captured. The position of different molecules is determined by a self-made code.

The RDFs can describe the relative spatial distribution between two types of particles, and they can be calculated as eq 1.

$$g(r) = \frac{V}{N_{\rm A}N_{\rm B}} \left(\sum_{i=1}^{N_{\rm A}} \frac{n_i b(r)}{4\pi r^2 \Delta r} \right) \tag{1}$$

where N_A and N_B represent the total numbers of particles A and B, respectively. V stands for the total volume of the simulation box. $n_i b(r)$ denotes the number of particle B in the space between concentric spheres that is r far from particle A.

The Chill+ structure identification algorithm³⁹ distinguishes water structures such as free water, ice, and NGH through the topological relation between H_2O molecules. It can identify the type of water structure to which a single H_2O molecule belongs to and count the amount of hydrated H_2O molecules that form gas hydrate in the whole simulation system. Combined with the configurations of hydrate, the structural changes of hydrate can be monitored intuitively.

3. RESULTS AND DISCUSSION

3.1. CH₄-CO₂ Replacement Process at Different **Temperatures.** At different temperatures, the changes in the amount of escaped CH₄ molecules over time are shown in Figure 2a. The semitransparent and thin lines represent raw data obtained by a self-made code. For clearer expression, the raw data are fitted based on a power function, and the fitting curves are presented by solid dots. The power function has a similar trend to the Avrami model and the shrinking core model, which are well-known physical models for crystallization kinetics and the CH_4 - CO_2 replacement process.⁷³ It can be seen that the amount of escaped CH₄ molecules increases with temperature. Moreover, the RDFs between CH4 molecules and H2O molecules at different temperatures are calculated and exhibited in Figure 2b. It shows that the RDF peaks at 4 Å (from 6.618 to 5.547) become lower with the increase in the temperature, which indicates that more CH4 molecules escape from the center of hydrate cages.

At different temperatures, the changes in the amounts of captured CO_2 molecules over time are presented in Figure 2c. Same to the escape of CH_4 molecules, the results show that the amounts of captured CO_2 molecules also increase with temperature. And it is worth noting that two different variation trends are observed in both Figure 2a,c. With regard to 270 and 280 K, the amounts of escaped CH_4 molecules and captured CO_2 molecules increase at first and then tend to level off. Taking the case at 270 K as an example, Figure 3a displays the



Figure 3. (a) Configuration after 20,000 ps at 270 K; (b) configuration after 20,000 ps at 290 K.

configuration of the simulation system at the last moment. It can be seen that the replacement process stops at the surface of CH_4 hydrate even though 20,000 ps has been spent. This phenomenon can be attributed to that the CO_2 hydrate formed on the surface is very stable at 270 and 280 K, which leads to the termination of the replacement process. On the one hand, the possibility of the further decomposition of internal CH_4 hydrate is reduced by the stable CO_2 hydrate because the decomposition of hydrate must start from the surface.⁷⁴ Therefore, lots of CH_4 molecules in the deeper cannot be released. On the other hand, stable CO_2 hydrate plays a role as a mass transfer barrier, which stops the replacement process. The CH_4 molecules in the deeper cannot be replaced by the CO_2 molecules. As a result, both the escape of CH_4 and the capture of CO_2 stop after a period of time.

In terms of 283, 285, and 290 K, however, it is demonstrated that the changing curves of escaped CH₄ molecules and captured CO₂ molecules still keep increasing rather than level off after a period of time. Taking the case at 290 K as an example, the final configuration in Figure 3b reveals that the replacement process does not stop at the surface of the CH₄ hydrate but proceeds to the deeper part. The reason can be that the CO_2 hydrate becomes relatively unstable at 283, 285, and 290 K. For one thing, therefore, internal CH₄ hydrate has opportunities to further decompose and release amounts of CH₄ molecules. For another, the unstable CO2 hydrate leads to a weaker mass transfer barrier, which makes it easier for CH₄ molecules in the deep to escape. Meanwhile, the CO_2 molecules in the region I and region III can diffuse into the deeper of hydrate phase to easily replace the CH₄ molecules. However, it needs to be noted that the relative instability of CO₂ hydrate caused by higher temperatures can also bring about negative effects on the capture of CO_2 . Much of the newly formed CO_2 hydrate decomposes after a period of time and releases CO₂ molecules. Some of the released CO₂ molecules return to the region I and region III again, which can be inferred from the sudden drops of the changing curves circled in Figure 2c. Additionally, based on the Chill+ structure identification algorithm,³⁹ the yellow circles in Figure 3b mark a few CO₂ molecules captured by amorphous H₂O molecules rather than more stable hydrate cages, though these CO₂ molecules still stay in region II. Moreover, Figure 2d exhibits the RDFs between CO₂ molecules and H₂O molecules at different temperatures. It can be seen that the peaks at 4 Å become higher (from 0.577 to 0.642) with the temperature between 270 and 285 K, but the peak at 290 K is lower than the peak at 285 K. All these results show that excessive temperature is not conducive to CO₂ storage in the form of standard CO₂ hydrate, meaning that the capture of CO_2 may be temporary.

In order to evaluate the maintenance of the hydrate cage structure, the changes in the amounts of hydrated H₂O molecules over time at different temperatures are calculated by the Chill+ algorithm³⁹ and shown in Figure 2e. It is demonstrated that the amount of hydrated H₂O molecules becomes less with the rising temperature. Moreover, the RDFs between H₂O molecules at different temperatures are displayed in Figure 2f. It is indicated that the RDF peaks at 2.5 Å (the distance between H₂O molecules in hydrate) become lower (from 11.206 to 10.206) with temperature. The decrease of this feature peak means that the H₂O molecules tend not to be arranged in the form of gas hydrate. The reasons for the above results could be twofold. On the one hand, it is supposed that higher temperatures make CH4 molecules leave the hydrate cages very rapidly, but the CO₂ molecules cannot occupy the empty hydrate cages in a timely manner. Then, the empty hydrate cages get broken without the support of CO₂ molecules. On the other hand, the CO_2 hydrate is relatively unstable at higher temperatures. Therefore, some of the newly formed CO_2 hydrate decomposes after a period of time, and the hydrate cages are broken. In short, it is detrimental to the maintenance of hydrate stability before and after the replacement process.

Overall, the amounts of CH_4 production and CO_2 capture can be improved at higher temperatures, where CO_2 hydrate



Figure 4. (a) Changes in the amounts of escaped CH_4 molecules over time at different pressures; (b) RDF curves between CH_4 molecules and H_2O molecules at different pressures; (c) changes in the amounts of captured CO_2 molecules over time at different pressures; (d) RDF curves between CO_2 molecules and H_2O molecules at different pressures; (e) changes in the amounts of hydrated H_2O molecules over time at different pressures; (f) RDF curves between CO_2 molecules at different pressures; (f) RDF curves between H_2O molecules at different pressures; (f) RDF curves between H_2O molecules at different pressures.

becomes relatively unstable and forms a weaker mass transfer barrier. In this work, however, an unlimited increase in temperature is not regarded as a perfect way to facilitate the CH_4-CO_2 replacement process. At higher temperatures, the sequestration of CO_2 tends to be unstable, which means that the observed CO_2 capture may be temporary. Also, the hydrate's stability will decrease, leading to a weaker ability to ensure geological stability. Briefly, there is a conflict in selecting the proper temperature. In order to handle this conflict, choosing a middle temperature as a compromise can be feasible.

3.2. CH₄-CO₂ Replacement Process at Different Pressures. At the same temperature of 280 K and different pressures, the changes in the amounts of escaped CH₄ molecules captured CO₂ molecules, and hydrated H₂O molecules with time are shown in Figure 4a,c,e. Furthermore, the RDF curves between different particles at different pressures are calculated and shown in Figure 4b,d,f. It can be seen that the various curves intersect and overlap with each other, and the differences are not obvious. It is indicated that the effect of pressure on the replacement process is not as significant as that of temperature, and the conclusion is also consistent with previous computational and experimental studies.^{64,75,76} However, it is worth emphasizing that the insignificance is relative to the effects of temperature but not absolute. On a larger and longer scale than that of this work, pressure is still an important and non-negligible factor.54

Figure 5 exhibits the average amounts of escaped CH_4 molecules, captured CO_2 molecules, and hydrated H_2O molecules from 19,500 to 20,000 ps at different pressures to evaluate the final performance. In terms of the differences that can be observed, the effect of pressure appears to be not monotonic but fluctuating. There are no definite principles detected. A possible reason might be that pressure plays a role in



Article

Figure 5. Average amounts of escaped CH_4 molecules, captured CO_2 molecules, and hydrated H_2O molecules from 19,500 to 20,000 ps at different pressures.

the replacement process in two different ways between 1 and 10 MPa. For one aspect, higher pressure can increase the local concentration of CO_2 molecules according to the ideal gas state equation, promoting the diffusion of CO_2 molecules into the solid phase (CH₄ hydrate) based on Fick's law. Then, these CO_2 molecules can replace CH₄ molecules in the hydrate more easily. For another aspect, it is supposed that lower pressure has a similar but weaker effect with higher temperature. At low pressure, both CH₄ hydrate and CO₂ dioxide hydrate become relatively unstable. Subsequently, the mass transfer barrier becomes weaker, improving the replacement process. As the pressure changes, however, it is difficult to determine which of the above aspects plays a dominant role, so the effects of pressure do not show a clear pattern.

3.3. Mechanisms and Evaluation of Temperature Oscillation Cases. Considering the unclear and weaker effects of pressures mentioned above, temperature conditions are hoped to be further optimized. For constant temperatures, no



Figure 6. Temperature changes of different temperature oscillation cases.



Figure 7. Changes in the amounts of escaped CH_4 molecules over time for (a) oscillation case 1, (b) oscillation case 2, (c) oscillation case 3, (d) oscillation case 4, (e) oscillation case 5, and (f) oscillation case 6.

matter higher or lower temperature has unacceptable drawbacks. And choosing a compromise temperature just avoids these disadvantages, but there seem to be no advantages to be gained. Meanwhile, choosing a constant compromise temperature is passive so that active adjustments cannot be made during the replacement process but only a long wait for its proceeding. Faced with the above issues, inspired by the idea of pressure oscillation,⁷⁷ temperature oscillation as a potential optimization strategy is first proposed and investigated in this work. The philosophy of temperature oscillation is that the advantages and disadvantages possessed by the lower and higher temperatures are inherently complementary. Therefore, it is speculated that the temperature oscillations can fully utilize the advantages of both higher and lower temperatures, compensating for the

defects of each other at the same time. It transfers the contradiction of temperature selection within the same space to be solved at a different time.

Six kinds of temperature oscillations are introduced as shown in Figure 6. The higher temperatures are set at 300 K, and the lower temperatures are not higher than 280 K. Based on the results achieved above, a temperature of 300 K can help break up the mass transfer barrier, and a temperature below 280 K can help hydrate cages stay stable. The pressure is still fixed at 4 MPa.

Compared with the case at 290 K, the changes in the amounts of escaped CH_4 molecules over time of different oscillation cases are shown in Figure 7. It can be observed that the variation trend of the amount of escaped CH_4 molecules is sensitive to temperature changes. The amount of escaped CH_4 molecules



Figure 8. Changes in the amounts of captured CO_2 molecules over time for (a) oscillation case 1, (b) oscillation case 2, (c) oscillation case 3, (d) oscillation case 4, (e) oscillation case 5, and (f) oscillation case 6.



Figure 9. Rapid rebuilding of CO₂ hydrate in the lower temperature stage of temperature oscillations.

increases when the temperature is 300 K. And it stops almost immediately when the temperature becomes lower. According to the previous results in this work, the reason is that the mass transfer barrier formed by CO_2 hydrate becomes very stable when the temperature becomes lower than 280 K. An internal CH_4 hydrate cannot decompose, which immediately prevents the escape of CH_4 molecules. It is worth mentioning that the amount of escaped CH_4 molecules may decrease slightly during the lower temperature stage. This is because some of the escaped CH_4 molecules could be captured again by the hydrate cages.

As for the capture of CO_2 , it can be seen in Figure 8 that the amount of captured CO_2 molecules increases at the initial higher temperature stage. Similar to the cases at constant temperatures, the increase in this stage is mainly caused by the diffusion of CO_2 molecules into the hydrate phase. Interestingly, at the lower temperature stage, as marked by the light-yellow rectangles in Figure 8, the amount of captured CO_2 molecules continues to rise for a period of time, showing a delayed response to

temperature changes. It is supposed that the increase in this stage is mainly caused by the rebuilding of CO_2 hydrate. Figure 9 illustrates parts of the rebuilding process of CO₂ hydrate under different temperature oscillation cases. It can be seen that the intact hydrate cages are broken and produce incomplete hydrate cage structures after the higher temperature stage. When the temperature reduces to the lower, CO₂ hydrate can stay stable. Because of the memory effects of hydrate,⁷⁴ it is easy for CO₂ molecules and these incomplete hydrate cage structures to rebuild CO₂ hydrate rapidly within only nanoseconds. In short, the capture of CO₂ at oscillation temperatures benefits from both the diffusion of CO₂ in the higher temperature stage and the rebuilding of CO_2 hydrate in the lower temperature stage. In addition, it should be noted from the blue circle in Figure 8e,f that when the temperature returns to the higher level, the amount of captured CO₂ molecules decreases for a period of time due to the decomposition of CO₂ hydrate. Subsequently, the diffusion process of CO_2 molecules and the rebuilding



Figure 10. Changes in the amount of hydrated H_2O molecules over time for (a) oscillation case 1, (b) oscillation case 2, (c) oscillation case 3, (d) oscillation case 4, (e) oscillation case 5, and (f) oscillation case 6.



Figure 11. (a) Average amounts of escaped CH₄ molecules from 19,500 to 20,000 ps of different cases; (b) average amounts of captured CO₂ molecules from 19,500 to 20,000 ps of different cases; (c) average amounts of hydrated H₂O molecules from 19,500 to 20,000 ps of different cases; (d) average CO₂/CH₄ ratio in region II from 19,500 to 20,000 ps of different cases; (e) different degrees of damaged hydrate structures in the system.

process of CO_2 hydrate are repeated, resulting in a zigzag upward trend of captured CO_2 molecules. However, a noteworthy anomaly exhibited in the red circle in Figure 8f is that the CO_2 capture does not rise between 2500 and 5000 ps and does not fall between 5000 and 7500 ps, which is inconsistent with the patterns found above. It is due to the fact that at the beginning of the replacement, not enough incomplete hydrate structures are produced. At this time, CO_2 capture depends mainly on the CO_2 diffusion rather than the rebuilding of CO_2 hydrate. Therefore, in this stage, a temperature decrease is unfavorable to the CO_2 diffusion and CO_2 capture, but a temperature returning is advantageous.

In terms of the maintenance of the hydrate cage structure, Figure 10 shows that the amounts of hydrated H_2O molecules decrease rapidly when the temperature is 300 K but increase when the temperature drops to a lower temperature. It indicates that hydrate structures are repaired in the lower temperature stage. The repairment is the inevitable result of CH_4 hydrates stopping to decompose and CO_2 hydrates rebuilding. Therefore, the rebuilding process caused by temperature oscillations can also be conducive to the maintenance of hydrate stability. In addition, it is worth noting that the hydrate structures are repaired to different extents under different kinds of temperature oscillations.

In order to quantitatively evaluate the replacement processes under different oscillating temperatures and constant temperatures, Figure 11a-c displays the average amounts of escaped CH₄ molecules, captured CO₂ molecules, and hydrated H₂O molecules from 19,500 to 20,000, respectively. Furthermore, the average CO₂/CH₄ ratios in region II range from 19,500 to 20,000 ps and are exhibited in Figure 11d. The ratio can be regarded as a comprehensive indicator that describes the extent of conversion of CH4 hydrate to CO2 hydrate during the replacement process. Overall, all oscillating temperatures can improve the CH_4 – CO_2 replacement process in certain aspects. Especially, the CH_4 - CO_2 replacement process is comprehensively improved in oscillation cases 3, 4, and 5. Also, it is worth noting that the average temperatures of these oscillating temperatures are lower than 290 K. Therefore, it might mean that these oscillating temperatures can help obtain more CH_{4y} capture more CO₂, and maintain the hydrate stability better but need no additional thermal energy input, which may reduce the cost effectively.

3.4. Effects of the Lower Temperature Duration. From Figure 11, it can be seen that temperature oscillations are effective, but the aspects and strengths of their effects are different, which are supposed to be determined by the different oscillation waveforms. In order to explore the patterns, different temperature oscillation cases are compared and discussed.

Oscillation case 1 and oscillation case 2 have different lower temperature durations. It can be obviously observed from Figure 11a,c that extending the lower temperature duration can decrease the amount of escaped CH4 molecules and increase the amount of hydrated H₂O molecules. By comparing Figure 7a,b, it can be attributed to that the longer lower temperature duration means the shorter higher temperature duration, leading to a shorter time for CH₄ molecules to escape. Thus, the amount of escaped CH₄ molecules decreases. Meanwhile, as shown in Figure 10a,b, the shorter higher temperature stage can break up fewer hydrate cage structures and the longer lower temperature stage can repair more hydrate cage structures. Therefore, the amount of hydrated H₂O molecules rises. In addition, from Figure 11b, it is noteworthy that the amount of captured CO_2 molecules does not change much and even slightly increases after extending the lower temperature duration in oscillation case 2. This is because the capture of CO_2 requires both the higher temperature to break the mass transfer barrier and the lower temperature to rebuild the CO₂ hydrate. Extending the lower temperature duration limits the diffusion of CO_2 molecules but enhances the reconstruction of CO₂ hydrate. For the same reason, it is not thought that the amount of captured CO₂ molecules always keeps unchanged with the extending of the lower temperature duration. Considering a limiting case where the low temperature persists for one full period, that is, the case at a constant temperature of 280 K, the amount of captured CO2 is much lower than that of the oscillation case 1. Overall, it is thought that the lower temperature duration should be moderate but not extreme to use the complementary effects of high temperature and low

temperature and to avoid the serious drawbacks of them. Besides, because CH_4 production and hydrate stability may be production indicators of varying importance and the effects of lower temperature duration on them are completely opposite, the lower temperature duration needs to be further determined for a given situation and specific goals.

3.5. Effects of the Lower Temperature Value. Oscillation case 1, oscillation case 3, and oscillation case 4 have different lower temperature values. As shown in Figure 11a, it is indicated that reducing the lower temperature value can marginally decrease the amount of escaped CH₄ molecules. The results may be due to the fact that the lower temperatures make it easier for a few escaped CH₄ molecules to return to hydrate cages like CO₂ molecules. Moreover, reducing the lower temperature value can rise the amount of captured CO_2 molecules and hydrated H₂O molecules, as displayed in Figure 11b,c. The underlying reason might be that the lower temperatures can make fuller use of the memory effects of hydrates.⁷⁴ In detail, the intact hydrate cages are broken and produce incomplete hydrate cage structures at high temperatures. Since the destruction of the hydrate structure is gradual, there are different degrees of damaged hydrate structures in the system, as exhibited in Figure 11e. It is supposed that the lower temperatures have a more powerful ability to allow the more severely damaged hydrate structures to be reconstructed with CO_2 molecules into intact CO_2 hydrates. As a result, decreasing the lower temperature value can help the capture of CO₂ molecules and maintain the hydrate cage structures.

3.6. Effects of the Oscillation Frequency. The oscillation frequencies of oscillation case 1, oscillation case 5, and oscillation case 6 are 0.05, 0.1, and 0.2 GHz, respectively. With the oscillation frequency rising, the amount of escaped CH₄ molecules slightly reduces, as shown in Figure 11a. It can be attributed to the fact that a start-up time is required for the decomposition of hydrates and the escape of CH₄ molecules. During the start-up time, no CH₄ molecules escaped. The higher the frequency, the more starts and the longer the start-up time consumed. As a result, the amount of escaped CH₄ molecules decreases slightly. With regard to the capture of CO₂ molecules and the maintenance of hydrate cage structures, as shown in Figure 11b,c, the frequency of 0.1 GHz produces the best performance among the three frequencies. The reason is that it best balances the diffusion of CO₂ molecules and the rebuilding of CO₂ hydrate and thus benefits the most. For the lower frequency (0.05 GHz), the continuous time of higher temperature is longer, and the hydrate cage structures are more seriously damaged, as exhibited in Figure 11e. Therefore, the memory effects of hydrate⁷⁴ are weakened, and the rebuilding of CO₂ hydrate becomes more difficult. For the higher frequency (0.2 GHz), the continuous time of higher or lower temperature is too short, leading to that the CO₂ molecules have no enough time to finish the diffusion to the deeper of the hydrate phase, and the CO_2 hydrate has no enough time to finish the rebuilding process. In other words, both of the two kinds of behaviors that can enhance CO_2 capture are inhibited by the higher frequency. Therefore, the oscillation frequency should be moderate (0.05– 0.2 GHz) to produce the best optimization effects, and it is close to 0.1 GHz. This is an ideal intrinsic frequency determined by the fundamental properties of gas hydrate. For real production, it is worth noting that the oscillation frequency is difficult to reach as high as that optimal frequency. Therefore, on a macroscopic level, it is possible that the higher the oscillation frequency, the better the replacement effect, which can be supported by

previous work.⁷⁷ The previous work⁷⁷ reported that increasing the decompression frequency could effectively improve CH_4 recovery and CO_2 storage.

Summarizing all temperature oscillation cases, it can be found that the key to improving CH_4-CO_2 replacement is fully enhancing the cooperation between the diffusion of CO_2 molecules and the rebuilding of CO_2 hydrate. Furthermore, it is worth noting that though temperature oscillation within several nanoseconds may be hard to achieve, the physical-chemical mechanisms and the regularity found in our paper are not limited to the smaller time scale reported by our work but can also provide a benchmark and important guidance for larger-scale real exploitation.

4. CONCLUSIONS

In this work, the MD method is used to investigate the CH_4 – CO_2 replacement at different constant temperatures and pressures. Temperature oscillations are introduced in the replacement process as an optimization strategy. The main conclusions of this work are as follows:

- Increasing the temperature can improve the amounts of CH₄ escape and CO₂ capture but is unfavorable to long-term CO₂ storage and hydrate stability. In comparison, the effects of pressure are not as significant and definite as those of temperature.
- Under temperature oscillations, the CH₄-CO₂ replacement benefits from both the deep diffusion of CO₂ in the higher temperature stage and the rapid rebuilding of CO₂ hydrate within just nanoseconds caused by the memory effects in the lower temperature stage.
- Compared with the constant temperature, temperature oscillations can achieve various improvements, including obtaining more CH₄, storing more CO₂, maintaining the hydrate stability better, and saving cost.
- For temperature oscillations, the lower temperature duration and the oscillation frequency should be moderate to produce the optimization effects. Decreasing the lower temperature value can distinctly improve the CO₂ capture and the maintenance of hydrate stability.

AUTHOR INFORMATION

Corresponding Author

Gongming Xin – School of Energy and Power Engineering, Shandong University, Jinan, Shandong 250061, China;
orcid.org/0000-0003-3974-0391; Phone: +86 531 88399919; Email: xingm@sdu.edu.cn

Authors

Yinglong Zhang – School of Energy and Power Engineering, Shandong University, Jinan, Shandong 250061, China

Mao Cui – School of Energy and Power Engineering, Shandong University, Jinan, Shandong 250061, China

Dexiang Li – School of Energy and Power Engineering, Shandong University, Jinan, Shandong 250061, China; orcid.org/0000-0002-6937-572X

Complete contact information is available at: https://pubs.acs.org/10.1021/acsomega.2c06502

Notes

The authors declare no competing financial interest.

ACKNOWLEDGMENTS

The authors would like to appreciate the support from the Shandong Natural Science Foundation (ZR2019BA004) and Shandong Provincial Key Research and Development Program (grant no. 2019JZZY010454).

REFERENCES

(1) Mann, J.; Sephton, P. A (negative) replication of 'The relationship between energy consumption, energy prices, and economic growth: Time series evidence from Asian developing countries'. *Energy Economics* **2019**, *82*, 78–84.

(2) Zheng, W.; Walsh, P. P. Economic growth, urbanization and energy consumption - A provincial level analysis of China. *Energy Economics* **2019**, *80*, 153–162.

(3) Lei, R.; Feng, S.; Lauvaux, T. Country-scale trends in air pollution and fossil fuel CO2 emissions during 2001–2018: confronting the roles of national policies and economic growth. *Environ. Res. Lett.* **2021**, *16*, 014006.

(4) Vohra, K.; Vodonos, A.; Schwartz, J.; Marais, E. A.; Sulprizio, M. P.; Mickley, L. J. Global mortality from outdoor fine particle pollution generated by fossil fuel combustion: Results from GEOS-Chem. *Environ. Res.* **2021**, *195*, 110754.

(5) Horvath, A.; Rachlew, E. Nuclear power in the 21st century: Challenges and possibilities. *Ambio* **2016**, *45*, S38–S49.

(6) Martin, P. G.; Tomkinson, N. G.; Scott, T. B. The future of nuclear security: Commitments and actions - Power generation and steward-ship in the 21st century. *Energy Policy* **2017**, *110*, 325–330.

(7) Zhao, Z.-Y.; Chang, R.-D.; Chen, Y.-L. What hinder the further development of wind power in China?-A socio-technical barrier study. *Energy Policy* **2016**, *88*, 465–476.

(8) Faramawy, S.; Zaki, T.; Sakr, A. A. E. Natural gas origin, composition, and processing: A review. J. Nat. Gas Sci. Eng. 2016, 34, 34–54.

(9) Li, X.-S.; Xu, C.-G.; Zhang, Y.; Ruan, X.-K.; Li, G.; Wang, Y. Investigation into gas production from natural gas hydrate: A review. *Appl. Energy* **2016**, *172*, 286–322.

(10) Chong, Z. R.; Yang, S. H. B.; Babu, P.; Linga, P.; Li, X.-S. Review of natural gas hydrates as an energy resource: Prospects and challenges. *Appl. Energy* **2016**, *162*, 1633–1652.

(11) Koh, C. A.; Sum, A. K.; Sloan, E. D. State of the art: Natural gas hydrates as a natural resource. *J. Nat. Gas Sci. Eng.* **2012**, *8*, 132–138.

(12) Milkov, A. V. Global estimates of hydrate-bound gas in marine sediments: how much is really out there? *Earth-Sci. Rev.* **2004**, *66*, 183–197.

(13) Liu, L.; Sun, Z.; Zhang, L.; Wu, N.; Yichao, Q.; Jiang, Z.; Geng, W.; Cao, H.; Zhang, X.; Zhai, B.; Xu, C.; Shen, Z.; Jia, Y. Progress in Global Gas Hydrate Development and Production as a New Energy Resource. *Acta Geol. Sin. (Engl. Ed.)* **2019**, *93*, 731–755.

(14) Yu, Y.-S.; Zhang, X.; Liu, J.-W.; Lee, Y.; Li, X.-S. Natural gas hydrate resources and hydrate technologies: a review and analysis of the associated energy and global warming challenges. *Energy Environ. Sci.* **2021**, *14*, 5611–5668.

(15) Chen, X.; Yang, J.; Gao, D.; Hong, Y.; Zou, Y.; Du, X. Unlocking the deepwater natural gas hydrate's commercial potential with extended reach wells from shallow water: Review and an innovative method. *Renewable Sustainable Energy Rev.* **2020**, *134*, 110388.

(16) Madhusudhan, B. N.; Clayton, C. R. I.; Priest, J. A. The Effects of Hydrate on the Strength and Stiffness of Some Sands. *J. Geophys. Res.: Solid Earth* **2019**, *124*, 65–75.

(17) Song, Y.; Luo, T.; Madhusudhan, B. N.; Sun, X.; Liu, Y.; Kong, X.; Li, Y. Strength behaviors of CH4 hydrate-bearing silty sediments during thermal decomposition. *J. Nat. Gas Sci. Eng.* **2019**, *72*, 103031.

(18) Feng, Q.; Zhang, Y.; Peng, Z.; Zheng, Y.; Chen, X. Preparation and investigation of microencapsulated thermal control material used for the cementing of gas hydrate formations. *Colloids Surf., A* **2022**, *648*, 129182.

(19) Wan, Y.; Wu, N.; Hu, G.; Xin, X.; Jin, G.; Liu, C.; Chen, Q. Reservoir stability in the process of natural gas hydrate production by

Article

depressurization in the shenhu area of the south China sea. *Nat. Gas Ind.* **2018**, *5*, 631–643.

(20) Luo, T.; Han, T.; Zhao, X.; Zou, D.; Song, Y. Strength and Deformation Behaviors of Methane Hydrate-Bearing Marine Sediments in the South China Sea during Depressurization. *Energy Fuels* **2021**, *35*, 14569–14579.

(21) Wang, F.; Zhao, B.; Li, G. Prevention of Potential Hazards Associated with Marine Gas Hydrate Exploitation: A Review. *Energies* **2018**, *11*, 2384.

(22) Wu, N.; Li, Y.; Chen, Q.; Liu, C.; Jin, Y.; Tan, M.; Dong, L.; Hu, G. Sand Production Management during Marine Natural Gas Hydrate Exploitation: Review and an Innovative Solution. *Energy Fuels* **2021**, *35*, 4617–4632.

(23) Zhao, J.; Xu, K.; Song, Y.; Liu, W.; Lam, W.; Liu, Y.; Xue, K.; Zhu, Y.; Yu, X.; Li, Q. A Review on Research on Replacement of CH4 in Natural Gas Hydrates by Use of CO2. *Energies* **2012**, *5*, 399–419.

(24) Koh, D.-Y.; Kang, H.; Lee, J.-W.; Park, Y.; Kim, S.-J.; Lee, J.; Lee, J. Y.; Lee, H. Energy-efficient natural gas hydrate production using gas exchange. *Appl. Energy* **2016**, *162*, 114–130.

(25) Hamza, A.; Hussein, I. A.; Al-Marri, M. J.; Mahmoud, M.; Shawabkeh, R.; Aparicio, S. CO2 enhanced gas recovery and sequestration in depleted gas reservoirs: A review. *J. Pet. Sci. Eng.* **2021**, *196*, 107685.

(26) Zhou, X.; Liang, D.; Liang, S.; Yi, L.; Lin, F. Recovering CH4 from Natural Gas Hydrates with the Injection of CO2–N2 Gas Mixtures. *Energy Fuels* **2015**, *29*, 1099–1106.

(27) Chaturvedi, K. R.; Sinha, A. S. K.; Nair, V. C.; Sharma, T. Enhanced carbon dioxide sequestration by direct injection of flue gas doped with hydrogen into hydrate reservoir: Possibility of natural gas production. *Energy* **2021**, *227*, 120521.

(28) Ren, L.-L.; Jiang, M.; Wang, L.-B.; Zhu, Y.-J.; Li, Z.; Sun, C.-Y.; Chen, G.-J. Gas hydrate exploitation and carbon dioxide sequestration under maintaining the stiffness of hydrate-bearing sediments. *Energy* **2020**, *194*, 116869.

(29) Luo, T.; Han, T.; Zhang, T.; Li, Y.; Zhao, X.; Zhang, C.; Sun, X.; Song, Y. Deformation behaviors of hydrate-bearing silty sediments during CH4–CO2 replacement. *J. Pet. Sci. Eng.* **2022**, *211*, 110225.

(30) Chen, L.; Sasaki, H.; Watanabe, T.; Okajima, J.; Komiya, A.; Maruyama, S. Production strategy for oceanic methane hydrate extraction and power generation with Carbon Capture and Storage (CCS). *Energy* **2017**, *126*, 256–272.

(31) Anderson, J.; Rode, D.; Zhai, H.; Fischbeck, P. Reducing carbon dioxide emissions beyond 2030: Time to shift U.S. power-sector focus. *Energy Policy* **2021**, *148*, 111778.

(32) Bianco, V.; Cascetta, F.; Marino, A.; Nardini, S. Understanding energy consumption and carbon emissions in Europe: A focus on inequality issues. *Energy* **2019**, *170*, 120–130.

(33) Gao, P.; Yue, S.; Chen, H. Carbon emission efficiency of China's industry sectors: From the perspective of embodied carbon emissions. *J. Cleaner Prod.* **2021**, 283, 124655.

(34) Melnikov, V. P.; Nesterov, A. N.; Reshetnikov, A. M.; Istomin, V. A.; Kwon, V. G. Stability and growth of gas hydrates below the icehydrate-gas equilibrium line on the P-T phase diagram. *Chem. Eng. Sci.* **2010**, *65*, 906–914.

(35) Liu, J.; Yan, Y.; Liu, H.; Xu, J.; Zhang, J.; Chen, G. Understanding effect of structure and stability on transformation of CH4 hydrate to CO2 hydrate. *Chem. Phys. Lett.* **2016**, *648*, 75–80.

(36) Dornan, P.; Alavi, S.; Woo, T. K. Free energies of carbon dioxide sequestration and methane recovery in clathrate hydrates. *J. Chem. Phys.* **2007**, *127*, 124510.

(37) Xu, C.-G.; Cai, J.; Yu, Y.-S.; Chen, Z.-Y.; Li, X.-S. Research on micro-mechanism and efficiency of CH4 exploitation via CH4-CO2 replacement from natural gas hydrates. *Fuel* **2018**, *216*, 255–265.

(38) Lee, S.; Lee, Y.; Lee, J.; Lee, H.; Seo, Y. Experimental verification of methane-carbon dioxide replacement in natural gas hydrates using a differential scanning calorimeter. *Environ. Sci. Technol.* **2013**, *47*, 13184–13190.

(39) Nguyen, A. H.; Molinero, V. Identification of Clathrate Hydrates, Hexagonal Ice, Cubic Ice, and Liquid Water in Simulations: the CHILL + Algorithm. *J. Phys. Chem. B* **2015**, *119*, 9369–9376.

(40) Ota, M.; Abe, Y.; Watanabe, M.; Smith, R. L.; Inomata, H. Methane recovery from methane hydrate using pressurized CO2. *Fluid Phase Equilib.* **2005**, 228–229, 553–559.

(41) Ryou, J. E.; Al-Raoush, R. I.; Alshibli, K.; Lee, J. Y.; Jung, J. Effects of soaking process on CH4–CO2 replacement efficiency for hydratebearing sediments. *J. Pet. Sci. Eng.* **2021**, *196*, 107772.

(42) Li, B.; Xu, T.; Zhang, G.; Guo, W.; Liu, H.; Wang, Q.; Qu, L.; Sun, Y. An experimental study on gas production from fracture-filled hydrate by CO2 and CO2/N2 replacement. *Energy Convers. Manage.* **2018**, *165*, 738–747.

(43) Yuan, Q.; Sun, C.-Y.; Liu, B.; Wang, X.; Ma, Z.-W.; Ma, Q.-L.; Yang, L.-Y.; Chen, G.-J.; Li, Q.-P.; Li, S.; Zhang, K. Methane recovery from natural gas hydrate in porous sediment using pressurized liquid CO2. *Energy Convers. Manage.* **2013**, *67*, 257–264.

(44) Yuan, Q.; Wang, X.-H.; Dandekar, A.; Sun, C.-Y.; Li, Q.-P.; Ma, Z.-W.; Liu, B.; Chen, G.-J. Replacement of Methane from Hydrates in Porous Sediments with CO2-in-Water Emulsions. *Ind. Eng. Chem. Res.* **2014**, 53, 12476–12484.

(45) Heydari, A.; Peyvandi, K. Study of biosurfactant effects on methane recovery from gas hydrate by CO2 replacement and depressurization. *Fuel* **2020**, *272*, 117681.

(46) Pandey, J. S.; Karantonidis, C.; Karcz, A. P.; von Solms, N. Enhanced CH4-CO2 Hydrate Swapping in the Presence of Low Dosage Methanol. *Energies* **2020**, *13*, 5238.

(47) Zhang, X.; Li, Y.; Yao, Z.; Li, J.; Wu, Q.; Wang, Y. Experimental Study on the Effect of Pressure on the Replacement Process of CO2-CH4 Hydrate below the Freezing Point. *Energy Fuels* **2017**, *32*, 646–650.

(48) Xu, C.-G.; Cai, J.; Yu, Y.-S.; Yan, K.-F.; Li, X.-S. Effect of pressure on methane recovery from natural gas hydrates by methane-carbon dioxide replacement. *Appl. Energy* **2018**, *217*, 527–536.

(49) Gambelli, A. M.; Rossi, F. Natural gas hydrates: Comparison between two different applications of thermal stimulation for performing CO2 replacement. *Energy* **2019**, *172*, 423–434.

(50) Zhang, L.; Yang, L.; Wang, J.; Zhao, J.; Dong, H.; Yang, M.; Liu, Y.; Song, Y. Enhanced CH 4 recovery and CO 2 storage via thermal stimulation in the CH 4 /CO 2 replacement of methane hydrate. *Chem. Eng. J.* **2017**, 308, 40–49.

(51) Li, S.; Zhang, G.; Dai, Z.; Jiang, S.; Sun, Y. Concurrent decomposition and replacement of marine gas hydrate with the injection of CO2-N2. *Chem. Eng. J.* **2021**, *420*, 129936.

(52) Mok, J.; Choi, W.; Lee, J.; Seo, Y. Effects of pressure and temperature conditions on thermodynamic and kinetic guest exchange behaviors of CH4 - CO2 + N2 replacement for energy recovery and greenhouse gas storage. *Energy* **2022**, 239, 122153.

(53) Chen, Y.; Gao, Y.; Chen, L.; Wang, X.; Liu, K.; Sun, B. Experimental investigation of the behavior of methane gas hydrates during depressurization-assisted CO2 replacement. *J. Nat. Gas Sci. Eng.* **2019**, *61*, 284–292.

(54) Wei, W.-N.; Li, B.; Gan, Q.; Li, Y.-L. Research progress of natural gas hydrate exploitation with CO2 replacement: A review. *Fuel* **2022**, *312*, 122873.

(55) Kondori, J.; Zendehboudi, S.; Hossain, M. E. A review on simulation of methane production from gas hydrate reservoirs: Molecular dynamics prospective. *J. Pet. Sci. Eng.* **2017**, *159*, 754–772.

(56) English, N. J.; MacElroy, J. M. D. Perspectives on molecular simulation of clathrate hydrates: Progress, prospects and challenges. *Chem. Eng. Sci.* **2015**, *121*, 133–156.

(57) Zhao, J.; Jin, J.; Lv, K.; Sun, J.; Wang, R.; Wang, J.; Guo, X.; Hou, Q.; Liu, J.; Bai, Y.; Huang, X.; Liu, J. Effects of PVP and NaCl on the decomposition of methane hydrate by MD simulation. *Colloids Surf.*, A **2022**, 633, 127817.

(58) Liu, J.; Yan, Y.; Chen, G.; Zhang, J.; Liu, S. Kinetic hydrate inhibitor performance and adsorption characteristics of poly(N-alkyl-N-vinyl acetamide)s: A first-principles study. *Colloids Surf.*, A **2022**, 635, 128097. (59) He, Z.; Linga, P.; Jiang, J. What are the key factors governing the nucleation of CO2 hydrate? *Phys. Chem. Chem. Phys.* **2017**, *19*, 15657–15661.

(60) He, Z.; Gupta, K. M.; Linga, P.; Jiang, J. Molecular Insights into the Nucleation and Growth of CH4 and CO2 Mixed Hydrates from Microsecond Simulations. J. Phys. Chem. C 2016, 120, 25225–25236.

(61) He, Z.; Mi, F.; Ning, F. Molecular insights into CO2 hydrate formation in the presence of hydrophilic and hydrophobic solid surfaces. *Energy* **2021**, *234*, 121260.

(62) Kirchner, M. T.; Boese, R.; Billups, W. E.; Norman, L. R. Gas Hydrate Single-Crystal Structure Analyses. J. Am. Chem. Soc. **2004**, 126, 9407–9412.

(63) Abascal, J. L.; Sanz, E.; García Fernández, R.; Vega, C. A potential model for the study of ices and amorphous water: TIP4P/Ice. *J. Chem. Phys.* **2005**, *122*, 234511.

(64) Gajanayake, S.; Gamage, R. P.; Wanniarachchige, P.; Zhang, D. Quantification of CO2 Replacement in Methane Gas Hydrates: A Molecular Dynamics Perspective. J. Nat. Gas Sci. Eng. **2022**, *98*, 104396.

(65) Jorgensen, W. L.; Maxwell, D. S.; Tirado-Rives, J. Development and Testing of the OPLS All-Atom Force Field on Conformational Energetics and Properties of Organic Liquids. *J. Am. Chem. Soc.* **1996**, *118*, 11225–11236.

(66) Conde, M. M.; Vega, C. Determining the three-phase coexistence line in methane hydrates using computer simulations. *J. Chem. Phys.* **2010**, *133*, 064507.

(67) Harris, J. G.; Yung, K. H. Carbon Dioxide's Liquid-Vapor Coexistence Curve And Critical Properties as Predicted by a Simple Molecular Model. *J. Phys. Chem.* **1995**, *99*, 12021–12024.

(68) Tung, Y.-T.; Chen, L.-J.; Chen, Y.-P.; Lin, S.-T. Growth of Structure I Carbon Dioxide Hydrate from Molecular Dynamics Simulations. J. Phys. Chem. C 2011, 115, 7504–7515.

(69) Matsui, H.; Jia, J.; Tsuji, T.; Liang, Y.; Masuda, Y. Microsecond simulation study on the replacement of methane in methane hydrate by carbon dioxide, nitrogen, and carbon dioxide–nitrogen mixtures. *Fuel* **2020**, *263*, 116640.

(70) Ryckaert, J.; Ciccotti, G.; Berendsen, H. J. C. Numerical integration of the cartesian equations of motion of a system with constraints: molecular dynamics of n-alkanes. *J. Comput. Phys.* **1977**, *23*, 327–341.

(71) Goel, N. In situ methane hydrate dissociation with carbon dioxide sequestration: Current knowledge and issues. *J. Pet. Sci. Eng.* **2006**, *51*, 169–184.

(72) Thompson, A. P.; Aktulga, H. M.; Berger, R.; Bolintineanu, D. S.; Brown, W. M.; Crozier, P. S.; in 't Veld, P. J.; Kohlmeyer, A.; Moore, S. G.; Nguyen, T. D.; Shan, R.; Stevens, M. J.; Tranchida, J.; Trott, C.; Plimpton, S. J. LAMMPS - a flexible simulation tool for particle-based materials modeling at the atomic, meso, and continuum scales. *Comput. Phys. Commun.* **2022**, *271*, 108171.

(73) Zhao, J.; Zhang, L.; Chen, X.; Fu, Z.; Liu, Y.; Song, Y. Experimental Study of Conditions for Methane Hydrate Productivity by the CO2 Swap Method. *Energy Fuels* **2015**, *29*, 6887–6895.

(74) Bai, D.; Zhang, X.; Chen, G.; Wang, W. Replacement mechanism of methane hydrate with carbon dioxide from microsecond molecular dynamics simulations. *Energy Environ. Sci.* **2012**, *5*, 7033.

(75) Li, Y.; Liu, W.; Zhu, Y.; Chen, Y.; Song, Y.; Li, Q. Mechanical behaviors of permafrost-associated methane hydrate-bearing sediments under different mining methods. *Appl. Energy* **2016**, *162*, 1627–1632.

(76) Chen, Y.; Gao, Y.; Zhao, Y.; Chen, L.; Dong, C.; Sun, B. Experimental investigation of different factors influencing the replacement efficiency of CO2 for methane hydrate. *Appl. Energy* **2018**, 228, 309–316.

(77) Sun, L.; Wang, T.; Dong, B.; Li, M.; Yang, L.; Dong, H.; Zhang, L.; Zhao, J.; Song, Y. Pressure oscillation controlled CH4/CO2 replacement in methane hydrates: CH4 recovery, CO2 storage, and their characteristics. *Chem. Eng. J.* **2021**, *425*, 129709.