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Catalytic Hydrogenation of Cyclic Carbonates using Manganese Complexes

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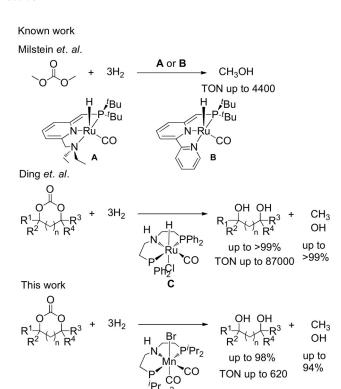
Abstract: Catalytic hydrogenation of cyclic carbonates to diols and methanol was achieved using a molecular catalyst based on earth-abundant manganese. The complex $[Mn(CO)_2(Br)-[HN(C_2H_4P^iPr_2)_2]$ **1** comprising commercially available MACHO ligand is an effective pre-catalyst operating under relatively mild conditions $(T=120\,^{\circ}\text{C},\ p(H_2)=30-60\ \text{bar})$. Upon activation with NaOⁱBu, the formation of coordinatively unsaturated complex $[Mn(CO)_2[N(C_2H_4P^iPr_2)_2)]$ **5** was spectroscopically verified, which confirmed a kinetically competent intermediate. With the pre-activated complex, turnover numbers up to 620 and 400 were achieved for the formation of the diol and methanol, respectively. Stoichiometric reactions under catalytically relevant conditions provide insight into the stepwise reduction form the CO_2 level in carbonates to methanol as final product.

Currently, there is a strong interest in the hydrogenation of CO₂ to methanol for the chemical supply chain and within the context of novel energy carriers.^[1,2] The synthesis of methanol by hydrogenation of CO₂ using molecular catalyst systems has been successfully addressed by various working groups in recent years. The field was pioneered in 2011 by Milstein and co-workers, who demonstrated the possibility to reduce CO₂ indirectly via hydrogenation of isolated derivatives such as cabonates, carbamates, and formates using Ru pincer complex under mild conditions (Scheme 1).[3] Seminal contributions in this field were made by the groups of Sanford, [4] Prakash, and Olah, [5] and Klankermayer and Leitner. [6] The latter work demonstrated that there are also direct pathways that do not require a stable organic intermediate. [6a] While these studies used noble metals as active catalytic centers, few examples employing non-noble metal catalyst systems have also been described. The group of Beller reported a catalytic system based on Cobalt reaching turnover numbers (TONs) of up to

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Scheme 1. Molecular homogeneous catalysts for the hydrogenation of carbonates $(n=0, 1; R^1-R^4=H \text{ or alkyl})$.

 $78.^{[7]}$ Recently, Prakash et al. reported a Manganese catalyzed sequential hydrogenation of CO_2 to methanol via a preformed formamide reaching TONs up to $36.^{[8]}$

Cyclic carbonates are particularly attractive as intermediate CO₂ derivatives in this context, as they can be formed readily from the reaction of CO₂ with the corresponding epoxides or oxetanes. In 2012, Ding et al. reported a highly efficient catalytic system for the hydrogenation of cyclic carbonates using Ru-MACHO pincer catalyst with TONs up to 87000 (Scheme 1).^[9] The diols formed as stoichiometric coproduct are valuable products, making this transformation in particular also as an attractive synthetic approach to these compounds.^[10] In fact, the carbonate group has been suggested as valuable protecting group for diols in organic synthesis.^[11]

The potential of hydrogenation catalysts based on abundant and cheap third-row metal Manganese and its pincer complexes^[12] has been pointed out by the groups of Milstein^[13] and Beller^[14] in 2016. In particular, complexes of this type have been successfully employed in the hydrogenation of CO_2 to formic acid derivatives.^[5,15] Encouraged by these reports, we were able to develop a catalytic procedure for





catalytic hydrogenation of cyclic carbonates to diols and methanol using manganese complex **1** comprising the well-known and commercially available PNP pincer ligand MACHO. While this manuscript was in preparation, we became aware of two independent parallel studies employing newly synthesized PNN-pincer ligands.^[16,17]

Table 1: Manganese catalyzed hydrogenation of $\bf 6a$: Influence of catalyst precursors and reaction conditions. $^{[a,b]}$

Entry	[Mn] No.	[Mn] [mol%]	NaO ^t Bu [mol%]	H ₂ [bar]	t [h]	X [%]	7 a (%) [TON]	8 (%) [TON]
1	1	1	2	30	26	86	86 (86)	62 (62)
2	2	1	2	30	26	23	10 (10)	4 (4)
3	3	1	2	30	26	23	14 (14)	3 (3)
4	4	1	2	30	26	21	11 (11)	5 (5)
5 ^[c]	1	1	2	30	26	74	71 (71)	62 (62)
6	1	2	3	30	26	98	90 (45)	75 (38)
7	1	0.5	1	30	26	70	66 (132)	46 (92)
8 ^[d]	1	0.2	0.5	30	40	56	48 (240)	35 (175)
$9^{[d]}$	1	0.2	0.5	60	40	60	52 (260)	30 (147)
10 ^[d]	5 ^[e]	0.2	_	60	14	38	37 (187)	26 (129)
11 ^[d]	5 ^[e]	0.2	_	60	40	70	67 (336)	44 (220)
12 ^[d]	5 ^[e]	0.1	-	60	40	66	62 (620)	40 (400)

[a] Conditions: **6a** (44 mg, 0.5 mmol), H_2 , Mn complex, NaO^tBu, temp. (120°C), THF (0.7 mL). [b] Yield was calculated using gas chromatography, ethyl heptanoate (25 μ L, 0.15 mmol) was used an internal standard. [c] T=100°C. [d] **6a** (440 mg, 5 mmol), H_2 , Mn complex, NaO^tBu, temp. (120°C), THF (2 mL). [e] Pre-catalyst 1 was treated with NaO^tBu in THF for 30 min at RT; reaction mixture was passed through celite, after removal of all volatiles, the formation of **5** was verified by 31 P{ 1 H} NMR spectroscopy and it was used directly without further work-up.

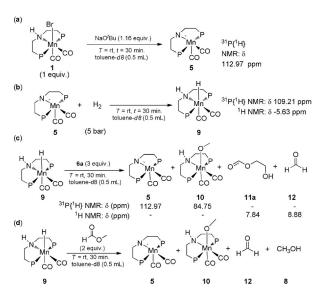
Initial studies were conducted using ethylene carbonate **6a** as a benchmark substrate (Table 1). Reactions were carried out with 1 mol % of catalyst in presence of NaO'Bu as basic co-catalyst (2 equiv) in THF (0.7 mL) at 120 °C under 30 bar of H₂. While complex **2–4** showed only low activity, the Mn-MACHO complex **1** gave 86 % conversion already under screening conditions. Ethylene glycol (**7a**) was detected by standard analytical techniques in quantities corresponding to nearly perfect selectivity, while the yield of methanol was consistently somewhat lower. Formate esters were observed as side products in small amounts to account for the difference at least partly. Complex **1** was still quite active at 100 °C, reaction giving 74 % conversion with 71 % yield to **7a** and 62 % yield into methanol.

Next, we investigated the influence of catalyst and cocatalyst loading on catalyst performance with the most promising pre-catalyst 1 (Table 1, entries 6–9). Increasing the loading of 1 to 2 mol% lead to almost full conversion of 6a and 90% yield of 7a. Reducing the Mn loading to 0.5 mol% lead to 70% conversion and 66% yield of 7a corresponding to a TON of 132. At a loading as low as 0.2 mol% for complex **1** and 0.5 mol% for NaO'Bu and extended reaction time of 40 h, TONs of 240 for **7a** and 175 for methanol were obtained, respectively.

Interestingly, the reaction showed significantly higher TONs to the corresponding products, when complex 1 was pre-activated with NaO'Bu in THF for 30 min at room

temperature. After removal of all volatiles, the nearly quantitative formation of the unsaturated complex 5 was verified by ¹H and ³¹P{¹H} NMR spectroscopy (Scheme 2).^[18] The remaining solid was re-dissolved in THF and used directly without further purification. At a 0.2 mol % of manganese loading, the use of 5 at 60 bar pressure of hydrogen after 14 h gave 38 % conversion with 187 TONs into diol and 129 TONs to MeOH (Table 1, entry 10). Gratifyingly, when the reaction time was increased to 40 h, 70 % conversion was achieved with 336 TONs into diol and 220 TONs into methanol (Table 1, entry 11). The best results were found with 0.1 mol % manganese, leading to 66% conversion corresponding to TONs of 620 for 7a and 400 for methanol, respectively (Table 1, entry 12).

The substrate scope of the reaction was assessed for complex 1 using the standard procedure without pre-activation for the hydrogenation of cyclic 5-membered and 6-membered carbonates. Reaction of 5-membered cyclic carbonates in THF (0.7 mL) at 120 °C under 30 bar of H_2 using 1 (1–2 mol %) and NaO'Bu (1.1 equiv) revealed conversion up to >99 % with yield up to 97 % for diol and 74 % into methanol (Table 2, entries 1–7). The activity of complex 1 for the hydrogenation of six-membered ring carbonates was equally high and even exceeded that observed for the five-membered ring substrates under the same conditions. Hydrogenation of six-membered cyclic carbonates under standard conditions showed conversion up to >99 % with yield up



Scheme 2. Formation of presumed Mn^I intermediates and their reactivity towards organic substrates; $P = P^{i}Pr_{2}$.





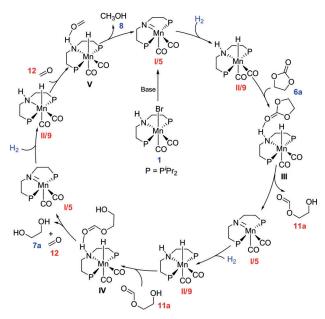
Table 2: Hydrogenation of cyclic carbonates using Mn complex 1 as a pre-catalyst.[a,b]

[a] Conditions: 6 (0.5 mmol), H₂ (30 bar), complex 1, NaO^tBu (1.1 equiv with respect to 1), THF (0.7 mL), temp. (120 °C), 26 h. [b] Yield was calculated using gas chromatography, ethyl heptanoate (25 μL , 0.15 mmol) was used as an internal standard. [c] 1,3-Propanediol (25 μL , 0.34 mmol) was used as an internal standard.

to 98 % for diol and 94 % for methanol (Table 2, entries 8–11).

A series of control reactions were performed to get insight into possible intermediates resulting from pre-catalyst 1 and their reactivity towards the organic substrates. Reaction of complex 1 with NaO'Bu leads to the formation of complex 5 (Scheme 2, entry a), which confirmed a kinetically competent intermediate in the catalytic experiments summarized in Table 1. In presence of hydrogen (5 bar), the Mn-monohydride complex 9 is formed within 30 minutes in [D₈]toluene as confirmed by 1 H NMR and 31 P NMR spectrum (1 H NMR: δ -5.63 ppm (t, J = 51 ppm, Mn-H); ${}^{31}P\{{}^{1}H\}$ NMR: δ 109.21 ppm, Scheme 2, entry b). Adding 3 equiv of ethylene carbonate **6a** to this solution regenerated the unsaturated Mn complex 5 according to ³¹P{¹H} NMR spectra together with the smaller amounts of the methanol coordinated manganese complex **10** (Supporting Information, Figure S2).^[8] The formate ester of ethylene glycol 11a and free formaldehyde 12 were observed as organic products in the ¹H NMR spectrum (11a:12 = 75:25) (Supporting Information, Figure S1; Scheme 2, entry c). Treating complex 9 with methyl formate lead also to formation of manganese complex 5 and 10 together with free formaldehyde and methanol (Supporting Information, Figure S3, S4, and S5; Scheme 2, entry d). These results confirm the high reactivity of the Mn-MACHO framework for the sequential transfer of H₂ formally as H⁻ and H+ to the C=O units of CO2 derivatives along the reduction path to methanol.

The observed species can be related directly to a plausible mechanism for the catalytic cycle in line with previous reports for other metals (Scheme 3). Activation of complex 1 leads to the catalyst species I, which corresponds to the experimen-



Scheme 3. Possible mechanism for catalytic hydrogenation of cyclic carbonates using the Mn-MACHO complex 1 as pre-catalyst; starting compounds and products are shown in blue, experimentally detected complexes and intermediates are highlighted in red.[19]

tally observed complex 5. Heterolytic cleavage of the H₂ molecule across the Mn=N double bond leads to Intermediate II detected as the mono-hydride complex 9. The carbonyl group of the substrate interacts with the protic N-H hydrogen activating the C=O unit for nucleophilic attack by Mn-bound hydride. This leads to an ortho-ester as first organic reduction product. Cyclic *ortho*-esters are typically more stable in the isomeric open form of the formate ester and hydroxyl functionality, in line with the detection of this species in the control reactions. This principle of H-H addition to the C=O unit can be re-iterated until the methanol stage is reached. Coordination of CH₃OH to species I would explain the presence of complex 10.

The catalytic cycle and the observed intermediates are in accord with the DFT calculations reported by the Rüping group for their PNN-ligand system. Their data associated the highest activation barrier with the initial hydride transfer to **6a**. [17] This in line with the observation of organic products at all reduction levels down to methanol upon reaction with the hydride complex 9. However, a concerted H₂ activation and transfer mechanism^[19] as suggested for the ligand framework introduced by Milstein cannot be excluded.[16] The two pathways follow basically the same bond breaking and bond formation trajectory with similar energy spans, differentiated by the existence of structures akin to 9 as intermediates or offloop species. Further studies are required to elucidate these alternatives for manganese catalyzed CO₂ hydrogenation,







which may well depend on the individual ligand framework given their close similarity.

In conclusion, the manganese complex [Mn(CO)₂(Br)- $[HN(C_2H_4P^iPr_2)_2]$ 1 was identified as efficient catalyst for the hydrogenation of cyclic carbonates. The complex is readily accessible from commercially available starting materials comprising the PNP pincer ligand MACHO. High yields for the diols and for methanol were achieved under relatively mild conditions, corresponding to up to 620 TON and 400 TON, respectively. These data match or even surpass the performance of the PNN-ligand based catalysts developed in parallel studies.^[16,17] The formation of unsaturated complex 5 and the hydride complex 9 was validated under relevant reaction conditions, corresponding to two crucial intermediates of a potential catalytic cycle for this reaction. In particular, their reactivity towards H₂ and the organic substrates substantiated the pivotal function of the M=N/ M-N unit as a formal hydride/proton relay in the stepwise reduction of the C=O unit. Further studies are necessary to distinguish between a stepwise or concerted mechanism for this heterolytic H₂ transfer. Overall, these results substantiate the great potential of manganese complexes for hydrogenation of CO₂-derived functional groups, opening the path for catalytic conversion of carbon dioxide into methanol using earth abundant, cheap, and benign manganese as metal component.

Experimental Section

Standard procedure for the catalytic hydrogenation of cyclic carbonates to diols and methanol using Mn catalyst 1: The catalytic reactions were carried out in externally heated 20 mL stainless-steel reactors equipped with a glass inlet and a magnetic stir bar. Mncomplex 1 and NaO'Bu were weighed into the glass inlet inside a glovebox. The glass inlet was closed with a septum and transferred into the bottom part of the steel autoclave, where it was opened under a stream of argon. After sealing, the autoclave was purged with argon three times. The required amounts of carbonates 6 and THF were added by syringe through a needle valve under argon flow at room temperature. The autoclave was sealed and pressurized with hydrogen gas and heated to the reaction temperature. After the given reaction time, the autoclave was cooled to room temperature and carefully vented under continuous stirring. Ethyl heptanoate was added as an internal standard and the resulting solution was analyzed by gas chromatography.

Procedure with pre-activated complex 5: A solution of complex 1 (0.1 mmol) and NaO'Bu (0.12 mmol) in THF (0.5 mL) was stirred for 30 min at RT and the formation of 5 was checked by $^{31}P\{^1H\}$ NMR spectroscopy. After 30 minutes, the reaction mixture was passed through a short pad of celite. After thorough removal of all volatiles under vacuum, the solid was re-dissolved in THF. This solution was used for catalysis following the standard procedure.

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Conflict of interest

The authors declare no conflict of interest.

Keywords: carbon dioxide · carbonates · hydrogenation · manganese · methanol

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