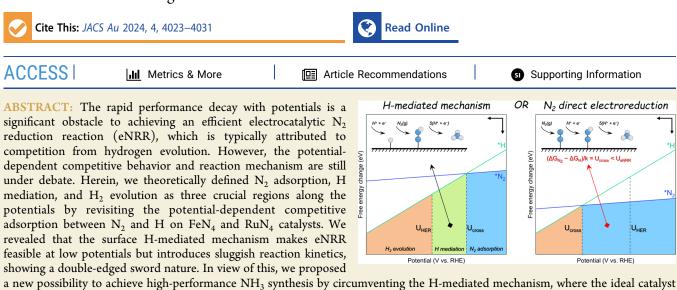


Article

# Toward High-Performance Electrochemical Ammonia Synthesis by Circumventing the Surface H-Mediated N<sub>2</sub> Reduction

Zhe Chen and Tao Wang\*



a new possibility to achieve high-performance  $NH_3$  synthesis by circumventing the H-mediated mechanism, where the ideal catalyst should have a wide potential interval with N<sub>2</sub>-dominated adsorption to trigger direct eNRR. Using this mechanistic insight as a new criterion, we proposed a theoretical protocol for eNRR catalyst screening, but almost none of the theoretically reported electrocatalysts passed the assessment. This work not only illustrates the intrinsic mechanism behind the low-performance dilemma of eNRR but also points out a possible direction toward designing promising catalysts with high selectivity and high current density.

# KEYWORDS: electrochemical nitrogen reduction, H-mediated mechanism, DFT, constant potential, catalyst design

# **1. INTRODUCTION**

Nitrogen  $(N_2)$  fixation to ammonia  $(NH_3)$  is significant to human beings due to its essential role in the fertilizer industry.  $^{1-3}$   ${\rm Meanwhile,\ NH_3}$  is a crucial feedstock for synthesizing nitrogen-containing fine chemicals. In addition, it is also regarded as an ideal carbon-free fuel and hydrogen carrier in a sustainable-energy system. In 2020, the global production of NH<sub>3</sub> reached 147 million tons and was mainly from the Haber–Bosch process, which worked at 300–500 °C and 150-200 atm on the iron-based heterogeneous catalysts. However, this century-old technology is less sustainable due to the high energy consumption and use of gray hydrogen, which indirectly consumes 2% of global fossil energy and results in annual CO<sub>2</sub> emissions of 300 million tons. Therefore, planning a sustainable N<sub>2</sub> fixation alternative scheme to the traditional Haber-Bosch method is significant to the world's long-term development.

The sustainable-energy-driven electrochemical N<sub>2</sub> reduction reaction (eNRR) has been widely proposed as a promising, green, and economical route for NH<sub>3</sub> synthesis due to the mild reaction conditions and carbon neutrality.<sup>1–3</sup> Noteworthy, the rigorous protocol proposed by Chorkendorff and colleagues has dramatically standardized this field and was viewed as a benchmark to qualify eNRR results.<sup>4</sup> Later on, the eNRR reproducibility checklist was established in 2022.<sup>5</sup> Despite the

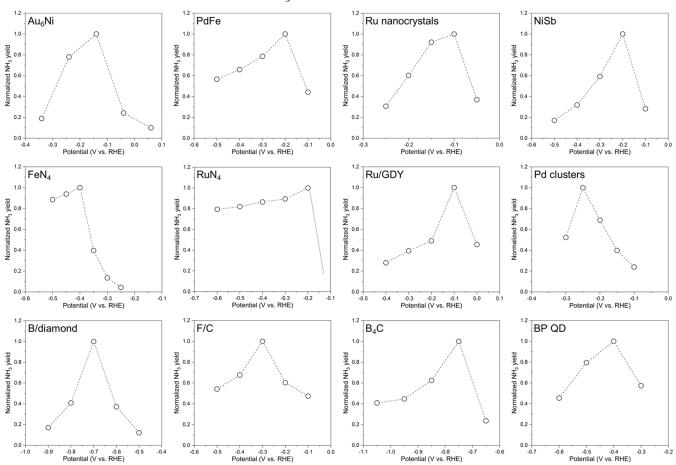
fruitful experimental and theoretical achievements, the industrial-scale application is still severely impeded by the low NH<sub>3</sub> yield and current density, as well as poor selectivity, which is typically attributed to the chemical inertness of the N<sub>2</sub> molecule and the competitive hydrogen evolution reaction (HER).<sup>6,7</sup> Recently, our group reviewed the experimental and theoretical progress in the catalyst design for eNRR during the past decade,<sup>3</sup> where we identified the following three in-debate scientific questions. (1) Why does the  $NH_3$  yield decay rapidly with potentials, typically showing a volcanic relationship as summarized in Scheme 1? (2) How is extremely inert  $N_2$ reduced at low potentials? (3) Why do most catalysts show very low NH<sub>3</sub> current densities during eNRR experimentally, even at high potentials? To the best of our knowledge, it still lacks a model system to adequately answer the above three key issues with proper computational methods.

In this work, the  $FeN_4$  and  $RuN_4$  catalysts were chosen as model systems to clarify the above in-debate questions during

Received:August 14, 2024Revised:September 11, 2024Accepted:September 16, 2024Published:September 25, 2024







Scheme 1. Universal Volcanic Relation between NH<sub>3</sub> Yield and Potential<sup>4</sup>

<sup>*a*</sup>Experimentally observed rapid decay of eNRR performance on various catalysts and the volcanic-shaped relationship between the normalized  $NH_3$  yield and potential. (The normalized  $NH_3$  yield is defined as dividing their absolute value by its maximum. See Table S1 for more details and references).

eNRR, and the double-reference method combined with a hybrid solvent model was used to obtain the constant potential framework. Our newly defined N2 adsorption, H mediation, and hydrogen evolution regions along the potential explain the volcanic shape between the NH<sub>3</sub> yield and potential. Then, the identified H-mediated N<sub>2</sub> hydrogenation mechanism with a higher energy barrier answers why and how inert N<sub>2</sub> was reduced in a narrow and low potential range. Thus, achieving direct eNRR by circumventing H mediation is proposed to be a promising strategy to dramatically increase  $\mathrm{NH}_3$  current density, where the ideal catalyst needs to directly drive eNRR over a wide potential range of N2-dominated adsorption. Finally, based on this new mechanistic insight, we established a new theoretical protocol to evaluate the eNRR performances of widely reported catalytic systems, including single-atom catalysts (SACs), metal-borides, and transition metals. Unfortunately, none of them passed the assessment of our established protocol, again indicating the grand challenge of discovering truly high-performance eNRR catalysts.

## 2. RESULTS AND DISCUSSION

#### 2.1. Potential-Dependent N<sub>2</sub> and H Adsorption

We first revisited the trend of competitive  $N_2$  and H adsorption with potentials over the FeN<sub>4</sub> and RuN<sub>4</sub> model systems, which have been reported as good eNRR catalysts

experimentally.<sup>8–10</sup> The schematic structures of the catalyst, as well as the N<sub>2</sub> adsorption and H adsorption at zero-excess charges, are presented in Figures S1A and S2, where eight explicit water molecules combined with implicit solvation model were used to fully simulate the electrochemical reaction environment. The potential-dependent energies of corresponding systems are presented in Figure S1B,C, showing a fairly good quadratic relation. The detailed fitted parameters are summarized in Table S2. Note that the surface area normalized capacitances of the FeN<sub>4</sub> and RuN<sub>4</sub> systems are calculated to be 18.11 and 19.51  $\mu$ F cm<sup>-2</sup>, respectively, which are close to that of the reported SACs,<sup>11–13</sup> validating the rationality of our systems.

On this basis, the free energy change of  $N_2$  ( $\Delta G_{N2}$ ) and H ( $\Delta G_H$ , which comes from the proton-electron pair) binding at different potentials can be obtained on the FeN<sub>4</sub> and RuN<sub>4</sub> catalysts (Figure 1A,B as well as Table S3). At 0 V vs reversible hydrogen electrode (RHE),  $\Delta G_{N2}$  is slightly more negative than  $\Delta G_H$ , indicating the preferential binding of N<sub>2</sub> to the active site of the FeN<sub>4</sub> and RuN<sub>4</sub> catalysts, and the corresponding electronic properties before and after adsorption are shown in Figure S3. Noteworthy, the binding strength of H is more sensitive to the applied potentials than N<sub>2</sub>, which is manifested by the much sharper decrease of  $\Delta G_H$  with potentials than  $\Delta G_{N2}$ . Therefore, the adsorption of N<sub>2</sub> and H will become equally competitive at a certain potential (-0.25

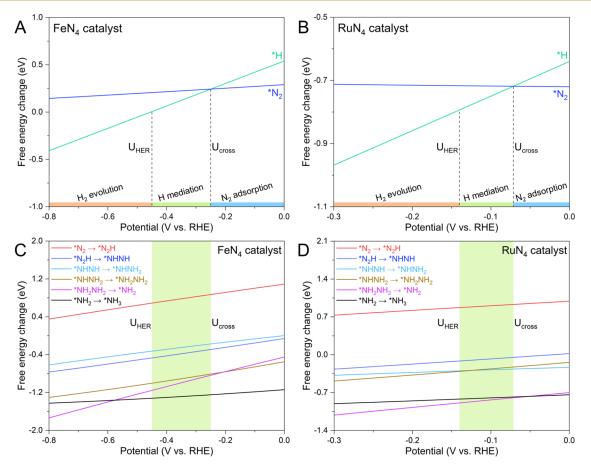


Figure 1. Competitive adsorption and reaction pathway. Calculated potential-dependent free energy changes of  $N_2$  and H adsorption over (A) FeN<sub>4</sub> catalyst and (B) RuN<sub>4</sub> catalyst. Calculated free energy changes of elementary steps of eNRR over (C) FeN<sub>4</sub> catalyst and (D) RuN<sub>4</sub> catalyst as functions of potential.

 $V_{\rm RHE}$  for FeN<sub>4</sub> and  $-0.08 V_{\rm RHE}$  for RuN<sub>4</sub>), which is defined as  $U_{\rm cross}$  (crossover potential). Indeed, this result is consistent with the work of Choi et al.,<sup>14</sup> where they used this information to explain the rapid decay of eNRR performance before reaching the mass transfer limit.

Then, dominant H adsorption will remain on the catalytic sites until the potential reaches the threshold to trigger hydrogen evolution  $(U_{\text{HER}})$ . After the potential exceeds  $U_{\text{HER}}$  $(-0.45 V_{\text{RHE}} \text{ for FeN}_4 \text{ and } -0.14 V_{\text{RHE}} \text{ for RuN}_4)$ , rapid H<sub>2</sub> formation will be achieved dominantly on the catalysts. Note that the definition of  $U_{\text{HER}}$  is based on the different H–H bond formation mechanisms,<sup>15</sup> including the Volmer step (\* +  $H^+$  +  $e^- \rightarrow *H$ ), Heyrovskey step (\*H + H<sup>+</sup> +  $e^- \rightarrow H_2$ ), and Tafel step (\*H + \*H  $\rightarrow$  H<sub>2</sub>). For the FeN<sub>4</sub> catalyst with weak H binding strength,  $U_{\text{HER}}$  is the potential at which the free energy of \*H adsorption approaches zero (i.e., Volmer-Heyrovskey mechanism). For the RuN<sub>4</sub> catalyst with a strong H binding (Figure S4), the potential at which  $\Delta G_{\rm H}$  of the second H approaches zero is  $U_{\text{HER}}$  (i.e., Volmer–Tafel mechanism). Besides, the low energy barriers for the H-H bond formation at a wide potential range indicate the kinetic feasibility of H mediation at  $U_{\rm cross}$  and H<sub>2</sub> formation at  $U_{\rm HER}$  (Figures S5 and S6).

Therefore, by combining the above two potential fences, three regions can be divided, i.e.,  $N_2$  adsorption region before  $U_{cross}$ . H mediation region between  $U_{cross}$  and  $U_{HER}$ , and hydrogen evolution region after  $U_{HER}$ . Notably, experimental observations universally reported a volcanic relationship of the

eNRR performance with potentials on different catalysts, as shown in Scheme 1 and Figure S7. In detail, the eNRR exhibits no experimental performance at the initial stage of the potential (corresponding to the  $N_2$  adsorption region). However, as the potential increases, the experimental performance increases significantly (corresponding to the H mediation region) and then drops rapidly (corresponding to the hydrogen evolution region). Therefore, in combination with our theoretically identified regions, the eNRR is likely to be triggered in the H mediation region. In this regard, we further computationally investigated the detailed reaction process of eNRR at different potentials on the FeN<sub>4</sub> and RuN<sub>4</sub> catalysts.

#### 2.2. Potential-Dependent N<sub>2</sub> Reduction

Typically, there are three reaction mechanisms for eNRR, including distal, alternating, and enzymatic pathways (Figure S8). Previous theoretical studies<sup>14,16</sup> have revealed that eNRR energetically favors the alternating mechanism over the FeN<sub>4</sub> and RuN<sub>4</sub> catalysts, involving \*N<sub>2</sub>H, \*NHNH, \*NHNH<sub>2</sub>, \*NH<sub>2</sub>NH<sub>2</sub>, \*NH<sub>2</sub>, and \*NH<sub>3</sub> intermediates. Therefore, we summarized the elementary steps of eNRR at different potentials via the alternating pathway in Figures 1C,D and S9, where the protonation of N<sub>2</sub> to the \*N<sub>2</sub>H intermediate (\*N<sub>2</sub> + H<sup>+</sup> + e<sup>-</sup>  $\rightarrow$  \*N<sub>2</sub>H) with the most positive free energy change represents the biggest challenge to NH<sub>3</sub> electrosynthesis. Although this process has an obvious slope with potentials (0.85 for FeN<sub>4</sub> and 0.83 for RuN<sub>4</sub>), it still has a significant positive free energy requirement (+0.71 eV for FeN<sub>4</sub>

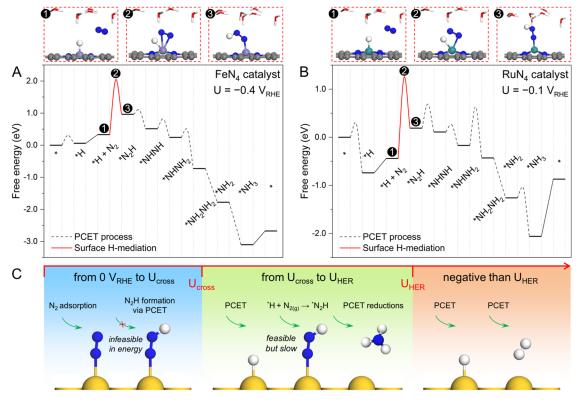


Figure 2. Surface H-mediated mechanism. Free energy diagram of the eNRR process through the surface H-mediated mechanism at the specific potentials on (A)  $FeN_4$  catalyst and (B)  $RuN_4$  catalyst. (C) Schematic diagram of reaction processes during eNRR within different potential regions.

and +0.87 eV for RuN<sub>4</sub>) when the potential reaches  $U_{\text{HER}}$ . Clearly, the formation of a  $*N_2\text{H}$  intermediate via protoncoupled electron transfer (PCET) reaction is forbidden at low potentials thermodynamically, which can be attributed to the high inertness of the N<sub>2</sub> molecule. However, once this bottleneck is overcome, the subsequent five PCET processes ( $*N_2\text{H} \rightarrow *\text{NHNH} \rightarrow *\text{NHNH}_2 \rightarrow *\text{NH}_2\text{NH}_2 \rightarrow *\text{NH}_2 +$ NH<sub>3</sub>(g)  $\rightarrow *\text{NH}_3$ ) will become energetically feasible (all below zero). The result clearly reveals that the eNRR is unlikely to be triggered within the N<sub>2</sub>-dominated adsorption region (from 0  $V_{\text{RHE}}$  to  $U_{\text{cross}}$ ) on the FeN<sub>4</sub> and RuN<sub>4</sub> catalysts. Therefore, new mechanistic analysis is needed to better understand the experimentally observed eNRR performance at low potentials.

#### 2.3. Surface H-Mediated Mechanism for N<sub>2</sub>H Formation

As shown above, the binding of H becomes stronger than  $N_2$  from  $U_{cross}$  to  $U_{HER}$ , which results in the accumulation of \*H at the active site. Therefore, the role of surface \*H species in driving eNRR to NH<sub>3</sub> is worth exploring. Here, we considered the direct reaction of the N<sub>2</sub> molecule with surface \*H to produce the \*N<sub>2</sub>H intermediate rather than the PCET process, which was defined as the surface H-mediated mechanism (\*H + N<sub>2</sub>  $\rightarrow$  \*N<sub>2</sub>H).

To start, we examined the thermodynamic and kinetic feasibility of this process within the potential range of  $U_{\rm cross}$  to  $U_{\rm HER}$ , where we chose  $-0.4 V_{\rm RHE}$  for FeN<sub>4</sub> and  $-0.1 V_{\rm RHE}$  for RuN<sub>4</sub> for a detailed analysis. As shown in Figure S10A,B, the calculated energy barrier of N<sub>2</sub>H formation at low potentials was 1.71 and 1.69 eV on the FeN<sub>4</sub> and RuN<sub>4</sub> catalysts, respectively, which was similar to the reported values of 1.10–1.98 eV on metallic Au and Pd catalysts by Ling et al.<sup>17</sup> Despite this pioneering work elegantly proposing the surface hydrogenation as the main mechanism driving N<sub>2</sub> reduction reaction

on catalysts with weak  $N_2$ -binding strength at low potentials, its calculations did not discuss the potential-dependent electrochemical competition between  $N_2$  and H adsorption.

In this respect, we examined the complete reaction pathways of eNRR via the surface H-mediated mechanism at low potentials, where the free energy diagrams, including both thermodynamic and kinetic information, are shown in Figures 2A,B and S11. It reveals that the free energy changes of all PCET steps after  $*N_2H$  formation are downhill on the FeN<sub>4</sub> catalyst at  $-0.4 V_{\text{RHE}}$  and the RuN<sub>4</sub> catalyst at  $-0.1 V_{\text{RHE}}$ . Meanwhile, our calculated energy barriers also indicate that these subsequent PCET processes (black dashed lines) will not be an obstacle toward NH<sub>3</sub> synthesis once the formation of the \*N<sub>2</sub>H intermediate with a high energy barrier is achieved via the surface H-mediated mechanism (red lines). In addition, the possibility of coadsorption of H and different  $N_x H_y$ intermediates on the FeN4 and RuN4 catalysts has been fully considered. Our results in Figure S12 show that \*H cannot coexist with  $N_r H_v$  intermediates on planar metal- $N_4$  sites.

As a summary in Figures 2C and S13, we proposed that  $*N_2H$  formation via PCET is unlikely at a potential range from 0  $V_{\text{RHE}}$  to  $U_{\text{cross}}$  due to the thermodynamic prohibition on the FeN<sub>4</sub> and RuN<sub>4</sub> catalysts. Instead, the surface H-mediated formation of  $*N_2H$  at the potential range from  $U_{\text{cross}}$  to  $U_{\text{HER}}$  is more plausible despite the sluggish kinetics, which is responsible for the measurable but low activity and current density of electrochemical NH<sub>3</sub> synthesis at low potentials. As the potential exceeds  $U_{\text{HER}}$ , the eNRR performance starts to degrade rapidly and the HER will become dominant. Therefore, our systematic mechanism analysis clearly indicates a volcanic relationship between the eNRR performance and potentials with the appearance of the plateau at  $U_{\text{HER}}$ , which is

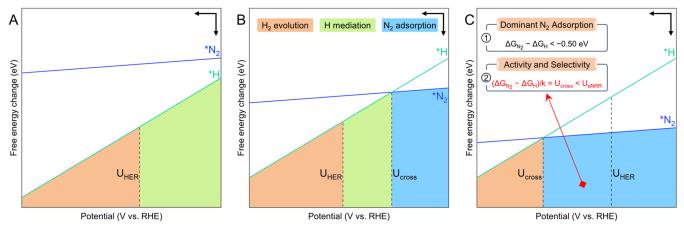


Figure 3. Cases of eNRR with different reaction mechanisms. Three possible competitive adsorptions of  $N_2$  and H at different potential intervals, where at 0  $V_{RHE}$  (A) H binding strength is stronger than  $N_{2}$ , (B)  $N_2$  is slightly stronger than H, and (C)  $N_2$  is significantly stronger than H. The newly established framework for screening direct eNRR catalysts is inserted in (C).

consistent with the experimental observations. Notably, our above computational insight into the H mediation mechanism in eNRR is also supported by the experimental evidence from in situ electron paramagnetic resonance measurements by Zhang and co-workers,<sup>18</sup> where the surface hydrogen was proven to participate in the eNRR process on the designed Ru single-atom catalyst at low potentials.

# 2.4. Diverse Scenarios of Competitive $\mathrm{N}_{\mathrm{2}}$ and H Adsorption

Despite the H mediation mechanism from  $U_{cross}$  to  $U_{HER}$  being a rational explanation of the experimentally detected eNRR performance at low potentials, its high energy barrier results in sluggish kinetics and a low NH<sub>3</sub> partial current density. Therefore, the surface H-mediated mechanism has a doubleedged sword nature in eNRR. In principle, a high eNRR performance is achievable if a catalyst can avoid the Hmediated mechanism to drive N<sub>2</sub> direct electroreduction.

Based on the binding strength difference between N<sub>2</sub> and H on the active sites, as well as the fact that  $\Delta G_{\rm H}$  is more sensitive to potential, three scenarios are possible. As shown in Figure 3A, if the binding strength of H on the catalyst is stronger than  $\mathrm{N}_2$  at 0  $V_{\mathrm{RHE}}$  there are only two intervals, i.e., H mediation before  $U_{\rm HER}$  and hydrogen evolution after  $U_{\rm HER}$ . As shown in Figure 3B, if there is a small gap between  $\Delta G_{
m N2}$  and  $\Delta G_{\rm H}$ ,  $U_{\rm cross}$  will appear at low potentials. Then, three regions will appear, i.e., the  $N_2$  adsorption region before  $U_{cross}$ , the H mediation region between  $U_{\rm cross}$  and  $U_{\rm HER}$ , and the significant hydrogen evolution region above  $U_{\text{HER}}$ . Although the potential range with N2-dominated adsorption can be observed, eNRR is difficult to achieve in such a narrow potential range due to the high inertness of the N2 molecule. Thus, in both cases, the Hmediated mechanism would be responsible for the limited eNRR performance. Figure 3C represents the ideal scenario to achieve high-performance eNRR, where N<sub>2</sub> binding strength is much stronger than H, and no free sites are available for the HER. As a result,  $U_{\rm cross}$  will appear at high potentials even beyond  $U_{\rm HER}$ , where the potential region from 0  $V_{\rm RHE}$  to  $U_{\rm cross}$ is dominant by N2 adsorption, and the HER can only be triggered above  $U_{\rm cross}$ . Such a wide potential region of dominant N<sub>2</sub> adsorption will enable NH<sub>3</sub> production in an efficient way on a catalyst with high selectivity and high current density. In this case, enlarging the adsorption gap between  $N_2$ 

and H will be a promising direction, i.e., enhancing  $\rm N_2$  adsorption or weakening H adsorption.

#### 2.5. New Protocol for Screening eNRR Catalysts

Indeed, the scenario shown in Figure 3C inspires us to revisit the prevailing theoretical framework for screening promising eNRR catalysts (typically including the assessments of the stable  $N_2$  adsorption, catalytic activity, and multiple reaction selectivity shown in Figure S14), where the essence of the competitive adsorption between  $N_2$  and H was underestimated. This will inevitably result in too many candidates being theoretically reported as promising for eNRR, which fails to provide effective guidance for experimental NH<sub>3</sub> electrosynthesis with improved performance.

To incorporate our above mechanistic understanding into the catalyst design for achieving direct eNRR by circumventing the H-mediated mechanism, we theoretically established a new protocol. As shown in Figure 3C, this protocol requires a sufficiently negative  $\Delta G_{N_2} - \Delta G_H (\Delta \Delta G)$  as the first priority to guarantee a wide potential range for N2-dominated adsorption, which was set to be -0.50 eV in this work. Then, the activity of the eNRR catalyst will be determined by the theoretical limiting potential  $(U_{eNRR})$ , where a more positive  $U_{eNRR}$  indicates a higher activity. Remarkably, the value of  $U_{\rm cross}$  should be more negative than  $U_{\rm eNRR}$  ( $U_{\rm cross}$  <  $U_{eNRR}$ ) to avoid triggering the H-mediated eNRR and HER. This key criterion ensures both the activity and selectivity of catalyst candidates. Besides, if coadsorption of N<sub>2</sub> and H on the active site is possible, an additional criterion of  $U_{\rm HER}$  –  $U_{eNRR}$  < 0 is required to guarantee proton priority for eNRR.

In short, an ideal eNRR catalyst should simultaneously have a very negative  $\Delta\Delta G$  and a very positive  $U_{eNRR}$ . Note that the potential-dependent slope (k) of  $\Delta\Delta G$  equals 1 within the constant-charge computational hydrogen electrode (CHE) model. Therefore, the aforementioned key criterion can be simplified as  $\Delta\Delta G < e \times U_{eNRR}$  within the CHE framework, enabling a rapid screening.

# 2.6. Grand Challenges in Identifying a Catalyst to Trigger Direct eNRR

Our newly established protocol was further used to evaluate the feasibility of computationally typical electrocatalysts for direct eNRR, including 16 single-atom catalysts (SACs) with transition metals embedded in 4N-graphene (TMN<sub>4</sub>) and 2H-

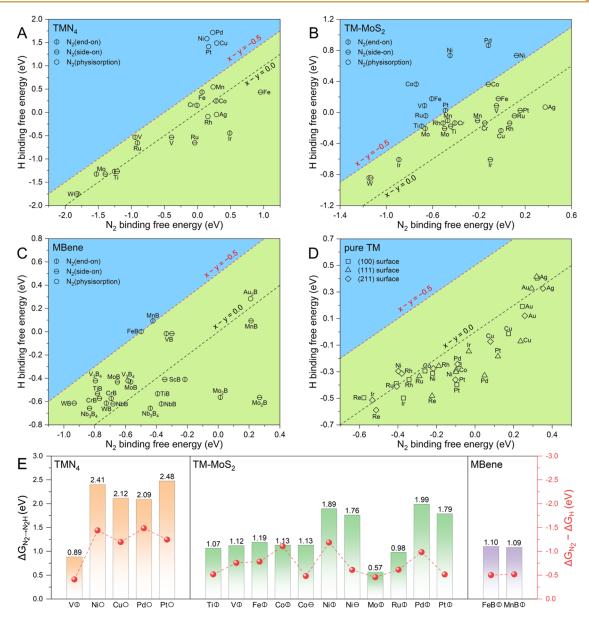


Figure 4. Screening for direct eNRR catalysts. Calculated adsorption free energies of  $N_2$  and H at the constant charge over (A) TMN<sub>4</sub>, (B) TM-MoS<sub>2</sub>, (C) MBene, and (D) pure transition-metal (TM). (E) Calculated free energy of  $N_2$  protonation with respect to the difference in the binding free energy between  $N_2$  and H.

molybdenum disulfide (TM-MoS<sub>2</sub>), as well as 13 metal-borides (MBenes) and 11 transition metals with face-centered cubic crystals. The schematic atomic structures of models are shown in Figure S15, and three N<sub>2</sub> adsorption configurations are shown in Figure S16. Note that the following results were calculated by the CHE model at a constant charge to save computational resources. It can qualitatively show the effectiveness of the designed catalyst in driving eNRR (Figure S17 and Table S4).

As shown in Figure 4A–D, we plotted the binding free energies of N<sub>2</sub> and H on different catalysts to illustrate their differences. Note that the amount of surface  $*N_2$  is closely related to the binding strength of N<sub>2</sub> on the catalyst, i.e., a catalyst with strong N<sub>2</sub> binding tends to have a larger amount of adsorbed N<sub>2</sub> than that with a weak N<sub>2</sub> binding, which will influence the reaction rate of eNRR. Clearly, three regions are possible based on the value of  $\Delta\Delta G$  (dashed lines), which also correspond to those shown in Figure 3A–C. For example, the electrocatalysts below the black dashed line (y = x) will show dominant H adsorption at low potential, corresponding to the scenario in Figure 3A. Then, the electrocatalysts located between the black and red (x - y = -0.5) dashed lines will present a narrow N<sub>2</sub>-dominated adsorption region, which will be gradually covered by H with increasing potentials, corresponding to the scenario in Figure 3B. Obviously, most of these electrocatalysts fall into these two regions, thus showing the universality of the H-mediated mechanism in eNRR.

Close inspections show that only a few electrocatalysts fall into the region near or above the red (x - y = -0.5) dashed line, which shows the dominant ability to adsorb N<sub>2</sub> molecule, greatly suppressing the competitive adsorption of H, including 5 TMN<sub>4</sub> candidates (V, Ni, Cu, Pd and Pt), 9 TM-MoS<sub>2</sub> candidates (Ti, V, Fe, Co, Ni, Mo, Ru, Pd and Pt), and 2 MBenes (FeB and MnB). Thus, we further investigated the N<sub>2</sub> reduction process on these candidates to determine whether they could trigger NH<sub>3</sub> synthesis before the applied potential reaches  $U_{\rm cross}$ . As shown in Figure 4E, the protonation process of \*N<sub>2</sub> to \*N<sub>2</sub>H (typical potential-determining step during eNRR) has very positive free energy change ( $\Delta G_{\rm N_2 \rightarrow N_2H}$ ), indicating a very negative value of  $U_{\rm eNRR}$  as well as  $\Delta\Delta G > e \times U_{\rm eNRR}$ , which clearly violates the requirement of  $\Delta\Delta G < e \times U_{\rm eNRR}$  as shown in Figure 3C. Therefore, these candidates cannot electrochemically reduce N<sub>2</sub> to NH<sub>3</sub> before reaching  $U_{\rm cross}$  despite their capabilities of forming dominant N<sub>2</sub> adsorption at a wide range of potential.

The above results clearly reveal the grand challenge of achieving high-performance electrochemical nitrogen fixation for  $NH_3$  synthesis due to the lack of electrocatalysts to simultaneously achieve overwhelming adsorption and sufficient activation for the  $N_2$  molecule. Therefore, innovative strategies and concepts for catalyst design need to be sought in the future to enable it to pass our newly established screening framework. In this regard, the spatially confined dual-site with the ability to enhance  $N_2$  adsorption proposed in our previous work may be a feasible approach (Figure S18).<sup>19</sup>

#### 3. CONCLUSIONS

In summary, we revisited the electrochemical competition between eNRR and HER based on the potential-dependent N<sub>2</sub> and H adsorption over FeN4 and RuN4 catalysts by using constant potential density functional theory (DFT) calculations with a hybrid solvent model. For the first time, we defined three regions along potential changes due to the high sensitivity of H electrochemical adsorption to potentials, which include the N2 adsorption region, H mediation region, and hydrogen evolution region. Our mechanism simulations indicate that eNRR is difficult to be triggered in the N<sub>2</sub> adsorption region (from 0  $V_{\rm RHE}$  to  $U_{\rm cross}$ ) due to the huge uphill in energy, but could achieve NH3 synthesis with slow reaction kinetics and unsatisfactory performance in the Hmediated region (from  $U_{\rm cross}$  to  $U_{\rm HER}$ ). Further increase of the electrode potential will lead to rapid degradation of eNRR performance due to entering the HER-dominated potential region. The results clearly explain the experimentally observed volcanic relationship of the eNRR performance with potentials, where we believe the eNRR performance starts at  $U_{\rm cross}$  and approaches its peak at  $U_{\text{HER}}$ . Based on this insight, obtaining direct eNRR by circumventing H mediation is a promising direction to achieve NH<sub>3</sub> synthesis with an industrial-scale current density. In this regard, a new theoretical framework for screening direct eNRR catalysts was proposed, and a series of typical catalysts were tested, among which, unfortunately, no candidates passed our assessment. This work pointed out the high necessity of proposing new strategies and concepts to design promising catalysts for triggering direct eNRR.

# 4. COMPUTATIONAL METHODS

All spin-polarized density functional theory calculations were performed by the Vienna Ab Initio Simulation Package (VASP) code with the projector augmented wave pseudopotential.<sup>20,21</sup> The revised Perdew–Burke–Ernzerhof (RPBE) functional was employed to describe the exchange-correlation interactions within the generalized gradient approximation.<sup>22,23</sup> The kinetic energy cutoff of the plane wave was set to be 400 eV, and the convergence criterion for the residual forces and total energies was set to be 0.03 eV Å<sup>-1</sup> and  $10^{-5}$  eV, respectively. The empirical correction in Grimme's method (DFT + D3) was used to describe the van der Waals interaction.<sup>24</sup> frequency was based on the climbing image nudged elastic band (CI-NEB) method.<sup>25</sup> The single transition-metal (TM) site catalyst (a = 8.52 Å and b = 9.84 Å) was built based on two-dimensional (2D) graphene containing 26 C, 4 N, and 1 TM atoms, as well as 8 explicit H<sub>2</sub>O molecules. A vacuum layer of 15 Å was set in the *c* direction to minimize the interaction between periodic images, and a 4 × 3 × 1 Monkhorst–Pack *k*-point mesh was used to sample the Brillouin zone.<sup>26</sup>

The implicit solvent environment was simulated by the VASPsol code,<sup>27,28</sup> which treats the electrode–electrolyte interface as a polarizable continuum and places ionic counter-charges at the interface. The relative permittivity of 78.4 was used to represent the aqueous solution, and the surface tension parameter was set to 0 to ignore the cavitation energy contribution. We assigned the Debye length of 3.0 Å to use the linearized Poisson–Boltzmann model, corresponding to a 1 M concentration of electrolyte. The constant electrode potential framework was achieved by the double-reference method,<sup>29,30</sup> and the different electrode potentials were obtained by changing the excess charge of the unit cell ( $\Delta n$ ) from –2.0e to +2.0e in steps of 0.5e.

The potential-dependent energy of the system  $(E_{a})$  is defined as

$$E_{\rm a} = E_{\rm DFT} - \Delta n (V_{\rm sol} + \Phi_{\rm a})$$

where  $E_{\rm DFT}$  is the energy obtained from DFT calculation,  $V_{\rm sol}$  is the electrostatic potential of the bulk electrolyte, and  $-\Phi_{\rm q}$  is the work function of the system and is equal to the Fermi level compared to the electrostatic potential at the bulk electrolyte.

The electrode potential  $(U_q)$  referenced to the standard hydrogen electrode (SHE) scale is given by

$$U_{\rm q}(V/\rm{SHE}) = -4.6 \,\mathrm{V} - \Phi_{\rm q}/e$$

where 4.6 V is the absolute potential of the SHE used in this work.  $^{11,12}$ 

We further added a QV correction to the system energy that is missing in the current VASPsol release. The Q and V are the net charge and negative value of the electrostatic potential in the bulk electrolyte, respectively.

The  $E_{a}-U_{a}$  points present a quadratic function as follows:

$$E(U_{\rm q}) = -0.5C(U_{\rm q} - U_{\rm 0})^2 + E_{\rm 0}$$

where C,  $U_{0}$ , and  $E_0$  are the fitted values of capacitance, the potential of zero charge (PZC), and the energy at the PZC of the system, respectively.

The equation of eNRR can be expressed as N<sub>2</sub> + 6H<sup>+</sup> + 6e<sup>-</sup> → 2NH<sub>3</sub>, and the theoretical reaction framework during eNRR was constructed by the computational hydrogen electrode (CHE) method to handle the chemical potential of the proton-electron pair (H<sup>+</sup> + e<sup>-</sup>) in the aqueous solution.<sup>31</sup> The electrode potential (U<sub>q</sub> versus SHE) obtained by the CEP method can be converted to the reversible hydrogen electrode (RHE) scale according to the relation: U<sub>q</sub>(V vs. RHE) = U<sub>q</sub>(V vs. SHE) + k<sub>B</sub>T × ln 10 × pH. In this work, the electrode potential is represented as SHE (pH = 0) or the RHE scale. More computational details can be found in the Supporting Information.

#### ASSOCIATED CONTENT

#### **1** Supporting Information

The Supporting Information is available free of charge at https://pubs.acs.org/doi/10.1021/jacsau.4c00741.

Computational details, structure models, kinetic information, and additional supplementary data mentioned in the main text (PDF)

# AUTHOR INFORMATION

#### **Corresponding Author**

Tao Wang – Center of Artificial Photosynthesis for Solar Fuels and Department of Chemistry, School of Science and Research Center for Industries of the Future, Westlake University, Hangzhou 310030 Zhejiang, China; Institute of Natural Sciences, Westlake Institute for Advanced Study, Hangzhou 310024 Zhejiang, China; Division of Solar Energy Conversion and Catalysis at Westlake University, Zhejiang Baima Lake Laboratory Co., Ltd., Hangzhou 310000 Zhejiang, China; Orcid.org/0000-0003-4451-2721; Email: twang@westlake.edu.cn

#### Author

**Zhe Chen** – Center of Artificial Photosynthesis for Solar Fuels and Department of Chemistry, School of Science and Research Center for Industries of the Future, Westlake University, Hangzhou 310030 Zhejiang, China; Department of Chemistry, Zhejiang University, Hangzhou 310027 Zhejiang, China; orcid.org/0000-0003-0172-7546

Complete contact information is available at: https://pubs.acs.org/10.1021/jacsau.4c00741

#### Notes

The authors declare no competing financial interest.

## ACKNOWLEDGMENTS

This work was supported by the National Natural Science Foundation of China (22273076) and the National Key Research and Development Program of China (2022YFA0911900); T.W. thanks for the start-up packages from Westlake University and the Research Center for Industries of the Future (RCIF) at Westlake University for supporting this work. We thank Westlake University HPC Center for computation support.

## REFERENCES

(1) MacFarlane, D. R.; Cherepanov, P. V.; Choi, J.; Suryanto, B. H.; Hodgetts, R. Y.; Bakker, J. M.; Vallana, F. M. F.; Simonov, A. N. A roadmap to the ammonia economy. *Joule* **2020**, *4* (6), 1186–1205.

(2) Guo, W.; Zhang, K.; Liang, Z.; Zou, R.; Xu, Q. Electrochemical nitrogen fixation and utilization: theories, advanced catalyst materials and system design. *Chem. Soc. Rev.* **2019**, *48* (24), 5658–5716.

(3) Chen, Z.; Liu, C.; Sun, L.; Wang, T. Progress of Experimental and Computational Catalyst Design for Electrochemical Nitrogen Fixation. *ACS Catal.* **2022**, *12* (15), 8936–8975.

(4) Andersen, S. Z.; Čolić, V.; Yang, S.; Schwalbe, J. A.; Nielander, A. C.; McEnaney, J. M.; Enemark-Rasmussen, K.; Baker, J. G.; Singh, A. R.; Rohr, B. A.; et al. A Rigorous Electrochemical Ammonia Synthesis Protocol with Quantitative Isotope Measurements. *Nature* **2019**, 570 (7762), 504–508.

(5) A checklist for reproducibility in electrochemical nitrogen fixation. *Nat. Commun.* **2022**, *13*, 4642. DOI: 10.1038/s41467-022-32146-x.

(6) Suryanto, B. H. R.; Du, H.-L.; Wang, D.; Chen, J.; Simonov, A. N.; MacFarlane, D. R. Challenges and prospects in the catalysis of electroreduction of nitrogen to ammonia. *Nat. Catal.* **2019**, *2* (4), 290–296.

(7) Ren, Y.; Yu, C.; Tan, X.; Huang, H.; Wei, Q.; Qiu, J. Strategies to suppress hydrogen evolution for highly selective electrocatalytic nitrogen reduction: challenges and perspectives. *Energy Environ. Sci.* **2021**, *14* (3), 1176–1193.

(8) Lü, F.; Zhao, S.; Guo, R.; He, J.; Peng, X.; Bao, H.; Fu, J.; Han, L.; Qi, G.; Luo, J.; et al. Nitrogen-coordinated single Fe sites for

efficient electrocatalytic  $N_2$  fixation in neutral media. Nano Energy **2019**, 61, 420–427.

(9) Geng, Z.; Liu, Y.; Kong, X.; Li, P.; Li, K.; Liu, Z.; Du, J.; Shu, M.; Si, R.; Zeng, J. Achieving a record-high yield rate of 120.9  $\mu$ g<sub>NH3</sub> mg<sub>cat.</sub><sup>-1</sup> h<sup>-1</sup> for N<sub>2</sub> electrochemical reduction over Ru single-atom catalysts. *Adv. Mater.* **2018**, *30* (40), No. 1803498.

(10) Wang, M.; Liu, S.; Qian, T.; Liu, J.; Zhou, J.; Ji, H.; Xiong, J.; Zhong, J.; Yan, C. Over 56.55% Faradaic efficiency of ambient ammonia synthesis enabled by positively shifting the reaction potential. *Nat. Commun.* **2019**, *10* (1), No. 341.

(11) Hu, X.; Chen, S.; Chen, L.; Tian, Y.; Yao, S.; Lu, Z.; Zhang, X.; Zhou, Z. What is the Real Origin of the Activity of Fe-N-C Electrocatalysts in the  $O_2$  Reduction Reaction? Critical Roles of Coordinating Pyrrolic N and Axially Adsorbing Species. J. Am. Chem. Soc. **2022**, 144 (39), 18144–18152.

(12) Duan, Z.; Henkelman, G. Surface charge and electrostatic spin crossover effects in  $CoN_4$  electrocatalysts. ACS Catal. 2020, 10 (20), 12148–12155.

(13) Hossain, M. D.; Huang, Y.; Yu, T. H.; Goddard, W. A., III; Luo, Z. Reaction mechanism and kinetics for  $CO_2$  reduction on nickel single atom catalysts from quantum mechanics. *Nat. Commun.* **2020**, *11* (1), No. 2256.

(14) Choi, C.; Gu, G. H.; Noh, J.; Park, H. S.; Jung, Y. Understanding potential-dependent competition between electrocatalytic dinitrogen and proton reduction reactions. *Nat. Commun.* **2021**, *12* (1), No. 4353.

(15) Di Liberto, G.; Cipriano, L. A.; Pacchioni, G. Role of dihydride and dihydrogen complexes in hydrogen evolution reaction on singleatom catalysts. J. Am. Chem. Soc. **2021**, 143 (48), 20431–20441.

(16) Wu, T.; Melander, M. M.; Honkala, K. Coadsorption of NRR and HER intermediates determines the performance of Ru-N<sub>4</sub> toward electrocatalytic N<sub>2</sub> reduction. ACS Catal. **2022**, 12 (4), 2505–2512.

(17) Ling, C.; Zhang, Y.; Li, Q.; Bai, X.; Shi, L.; Wang, J. New mechanism for  $N_2$  reduction: the essential role of surface hydrogenation. *J. Am. Chem. Soc.* **2019**, *141* (45), 18264–18270.

(18) Feng, X.; Liu, J.; Chen, L.; Kong, Y.; Zhang, Z.; Zhang, Z.; Wang, D.; Liu, W.; Li, S.; Tong, L.; Zhang, J. Hydrogen Radical-Induced Electrocatalytic  $N_2$  Reduction at a Low Potential. *J. Am. Chem. Soc.* **2023**, 145 (18), 10259–10267.

(19) Chen, Z.; Liu, Y.; Wang, T. Steering competitive  $N_2$  and CO adsorption toward efficient urea production with a confined dual site. *Chem. Sci.* **2023**, *14* (44), 12707–12714.

(20) Kresse, G.; Furthmüller, J. Efficient iterative schemes for ab initio total-energy calculations using a plane-wave basis set. *Phys. Rev.* B **1996**, *54* (16), 11169.

(21) Blöchl, P. E. Projector augmented-wave method. *Phys. Rev. B* **1994**, 50 (24), 17953.

(22) Hammer, B.; Hansen, L. B.; Nørskov, J. K. Improved adsorption energetics within density-functional theory using revised Perdew-Burke-Ernzerhof functionals. *Phys. Rev. B* 1999, 59 (11), 7413.

(23) Perdew, J. P.; Burke, K.; Ernzerhof, M. Generalized gradient approximation made simple. *Phys. Rev. Lett.* **1996**, 77 (18), 3865.

(24) Goerigk, L.; Grimme, S. A thorough benchmark of density functional methods for general main group thermochemistry, kinetics, and noncovalent interactions. *Phys. Chem. Chem. Phys.* **2011**, *13* (14), 6670–6688.

(25) Henkelman, G.; Uberuaga, B. P.; Jónsson, H. A climbing image nudged elastic band method for finding saddle points and minimum energy paths. *J. Chem. Phys.* **2000**, *113* (22), 9901–9904.

(26) Monkhorst, H. J.; Pack, J. D. Special points for Brillouin-zone integrations. *Phys. Rev. B* **1976**, *13* (12), 5188.

(27) Mathew, K.; Kolluru, V. C.; Mula, S.; Steinmann, S. N.; Hennig, R. G. Implicit self-consistent electrolyte model in plane-wave density-functional theory. *J. Chem. Phys.* **2019**, *151* (23), No. 234101.

(28) Mathew, K.; Sundararaman, R.; Letchworth-Weaver, K.; Arias, T.; Hennig, R. G. Implicit solvation model for density-functional study of nanocrystal surfaces and reaction pathways. *J. Chem. Phys.* **2014**, *140* (8), No. 084106.

(29) Filhol, J. S.; Neurock, M. Elucidation of the electrochemical activation of water over Pd by first principles. *Angew. Chem., Int. Ed.* **2006**, 45 (3), 402–406.

(30) Taylor, C. D.; Wasileski, S. A.; Filhol, J.-S.; Neurock, M. First principles reaction modeling of the electrochemical interface: Consideration and calculation of a tunable surface potential from atomic and electronic structure. *Phys. Rev. B* **2006**, 73 (16), No. 165402.

(31) Nørskov, J. K.; Rossmeisl, J.; Logadottir, A.; Lindqvist, L.; Kitchin, J. R.; Bligaard, T.; Jonsson, H. Origin of the overpotential for oxygen reduction at a fuel-cell cathode. *J. Phys. Chem. B* **2004**, *108* (46), 17886–17892.