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## Expression of phosphotransacetylase in *Rhodosporidium toruloides* leading to improved cell growth and lipid production<sup>†</sup>

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Microbial lipids (MLs) are potential alternatives to vegetable oils and animal fats for production of biofuels and oleochemicals. It remains critical to improve ML production efficiency and costs for further commercial development. In the present study, we overexpressed a gene encoding phosphotransacetylase (Pta) in the oleaginous yeast *Rhodosporidium toruloides* for enhanced cell growth and lipid production. Compared with the parental strain *R. toruloides* NP11, the engineered strain NP-Pta-15 showed significant improvement in glucose consumption, cell growth and lipid accumulation when cultivated under nitrogen limited conditions in an Erlenmeyer flask as well as a stirred tank bioreactor. The introduction of Pta may establish an additional acetyl-CoA formation route by utilization of acetylphosphate. Our results should inspire more engineering efforts to facilitate the economic viability of ML technology.

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## 1. Introduction

Oleo-chemicals are attractive alternatives to traditional petrochemicals and usually derived from vegetable oils and animal fats, which have limited availability.<sup>1</sup> MLs prepared from oleaginous microorganisms have been demonstrated to have comparable properties to typical plant oils and a number of advantages, such as a shorter production and distribution cycle, and without competing with food supply and land use.<sup>2</sup> However, it remains challenging to produce MLs at a large scale because of high costs.<sup>3</sup>

There are several strategies to improve the economic feasibility of MLs: first of all, exploration of low cost substrates such as lignocellulosic biomass and various organic wastes;<sup>4,5</sup> second, developing more efficient culture strategies and product separation methods to reduce process costs;<sup>6</sup> in another scenario, manufacturing valuable (co-)products such as unsaturated fatty acids and carotenoids through metabolic engineering of oleaginous species.<sup>7,8</sup> However, the theoretical yield of per mole of hexose is limited to two moles acetyl-CoA, since the glycolysis loses a carbon equivalent for each C3 unit upon pyruvate decarboxylation.<sup>9</sup> Ideally, cell growth and lipid production may be further improved by devising more efficient acetyl-CoA generating

<sup>a</sup>Division of Biotechnology, Dalian Institute of Chemical Physics, CAS, Dalian 116023, PR China pathways, but such efforts remain limited in oleaginous yeast. Recently, phosphoketolase (Pk) and phosphotransacetylase (Pta) were successfully expressed in the yeast *Yarrowia lipolytica*, and established an alternative cytosolic acetyl-CoA formation pathway, leading to improved lipid production performance.<sup>10</sup> Pk can convert fructose-6-phosphate (F6P) or xylose-5-phosphate (X5P) into acetylphosphate without ATP consumption, followed by Pta activity to acetyl-CoA (Fig. 1). Thus, acetyl-CoA production was realized independent of the ATP-citrate lyase mediated process being utilized by most oleaginous yeasts for lipid accumulation under nitrogen limited conditions.<sup>9</sup>

The oleaginous yeast *R. toruloides* is a robust lipid producer.<sup>11,12</sup> We have obtained multi-omic information of *R. toruloides* and established reliable genetic manipulation strategies.<sup>13,14</sup> In the present study, the Pta gene originated from *Bacillus subtilis* was sequence-optimized, *de novo* synthesized, and integrated into the genome of *R. toruloides* NP11 through *Agrobacterium* mediated transformation (ATMT). The engineered strain showed significant improvement in glucose consumption, cell mass and lipid production when cultivated in Erlenmeyer flask as well as in stirred tank bioreactor. Our results should inspire more engineering efforts to facilitate the economic viability of MLs.

## 2. Results and discussion

#### 2.1 Expression of Pta in R. toruloides NP11

The codon redressed Pta was introduced into the *R. toruloides* genome by using the ATMT strategy and confirmed by colony PCR analysis.<sup>14</sup> Further genome walking results revealed that 3 of 4 insertion events happened at the same chromosome and that the left-border of two transformants, namely, NP-Pta-4 and

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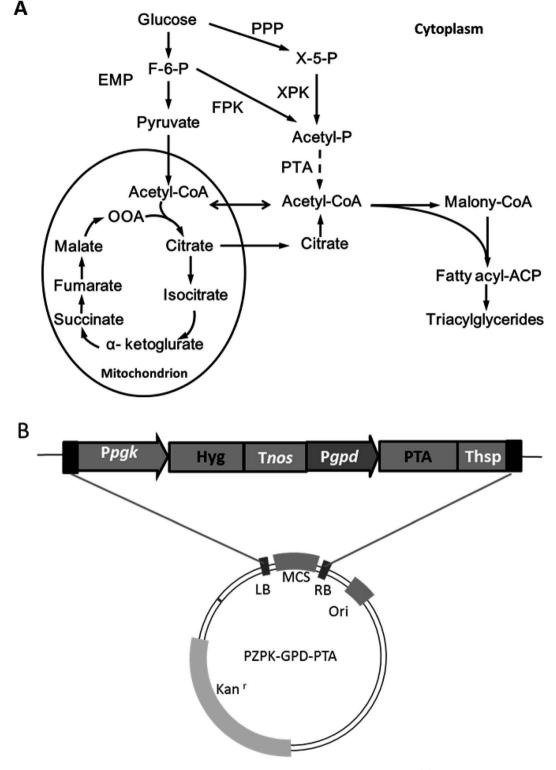


Fig. 1 Fatty acid biosynthetic pathway and the structures of cassette and plasmid for PTA expression. (A) Fatty acid synthesis pathway. Solid line: the native pathway; dashed line: the introduced pathway. EMP: Embden–Meyerhof–Parnas pathway (glycolysis pathway); PPP: pentose phosphate pathway. FPK: fructose6-phosphate phosphoketolase; XPK: xylulose 5-phosphate phosphoketolase. (B) The structures of cassette and plasmid for PTA expression.

NP-Pta-20, was inserted at an identical site (ESI<sup>†</sup>). However, no sequence homology was found among those inserted T-DNA flanking sequences and the insertion positions. The results suggested that T-DNA integrations occurred at random positions in the *R. toruloides* genome *via* a non-homologous recombination process as reported previously.<sup>16,17</sup> RT-PCR results also confirmed successful expression of Pta in those transformants (ESI<sup>†</sup>).

#### 2.2 Lipid production by engineered R. toruloides strains

A number of colonies were first cultured in 50 mL test tubes in 5.0 medium to screen those with improved cell growth profile. This was because colonies obtained by the Agrobacterium-mediated transformation usually had the expression cassette randomly integrated into the genome, and thus could have varied phenotypic profiles.<sup>17</sup> Indeed, many *R. toruloides* transformants were tested to find good fatty alcohol producer in a recent study.7 Our preliminary results showed that 4 out of 24 transformants. namely, NP-Pta-4, NP-Pta-6, NP-Pta-15 and NP-Pta-20, grew much faster than the wild strain NP11. Next, these four strains were grown on N-limited medium with an initial glucose concentration of 50 g  $L^{-1}$  under shake-flask culture conditions. It was found that the wild strain NP11 utilized glucose in 10 d, while NP-Pta-4, NP-Pta-6 and NP-Pta-20 did by 9 d, and NP-Pta-15, by 7 d (Fig. 2), clearly indicating an improved sugar consumption profile by those engineered strains. The cell mass of NP-Pta-4, NP-Pta-6 and NP-Pta-20 were slightly higher than that of NP11. However, NP-Pta-15 produced 12.8 g  $L^{-1}$  cell mass, about 8.5% more than that of NP11. The engineered strains produced 9.6% to 15.1% more lipids than the parental strain NP11 did. More importantly, lipid productivity of the engineered strain NP-Pta-15 reached 1.20 g L<sup>-1</sup> d<sup>-1</sup>, about 64.4% higher than that of the NP11. These data clearly demonstrated the beneficial effects of Pta expression in *R. toruloides* for lipid production.

Therefore, we further compared lipid production performance between NP11 and NP-Pta-15 on 3 L bioreactor (Fig. 3). NP-Pta-15 consumed 200 g L<sup>-1</sup> glucose within 54 h while it took 72 h for NP11, indicating that the engineered strain had 33.3% faster substrate consumption than the parental strain. NP-Pta-15 produced cell mass and lipid of 57.5 g L<sup>-1</sup> and 15.7 g L<sup>-1</sup>, respectively, about 27.1% and 7.6% more than NP11 did. However, cellular lipid content of 28.7% was about 10.3% lower. The fact that NP-Pta-15 cells had a lower lipid content upon consumption of 200 g L<sup>-1</sup> glucose suggested that more cells were produced and thus might be considered as an advantage for high cell density process by feeding more substrates.

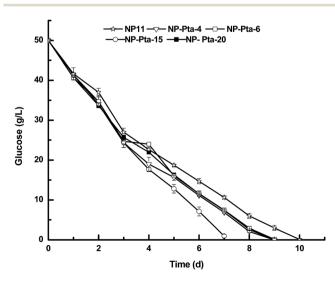
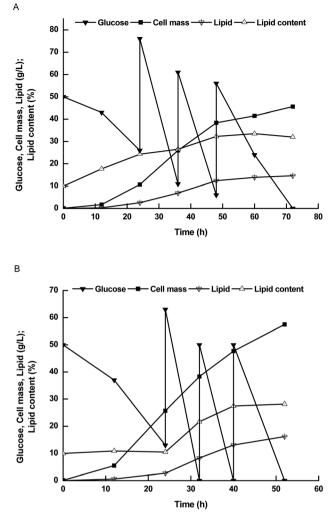


Fig. 2 Glucose depletion curves of various *R. toruloides* strains under shake-flask culture condition.



**Fig. 3** The time courses of lipid production by *R. toruloides* strains in 3 L bioreactor. (A) Results with NP11; (B) results with NP-Pta-15.

The results above indicated that the presence of Pta in *R. toruloides* could facilitate cell growth and lipid production. It should be noted that our genome annotation study had suggested a Pk gene RHTO\_04463 (ESI†) for potential formation of acetylphosphate from F6P or X5P by *R. toruloides* NP11.<sup>13</sup> Therefore, the introduction of Pta may establish an alternative acetyl-CoA supplement by utilization of acetylphosphate from the non-oxidative glycolysis pathway (Fig. 1). Recently, improved higher alcohols and fatty acid derivatives production was achieved in a number of studies, in which a spare acetyl-CoA supplying channel was constructed besides the native acetyl-CoA generating pathway through the combination of Pk and Pta.<sup>10,18</sup> However, more efforts should be conducted to verify the function of RHTO\_04463 in *R. toruloides* NP11.

#### 2.3 Fatty acid compositional profile

Table 2 showed the fatty acid compositional profiles of neutral lipids produced by *R. toruloides* strains. It was found that distributions of major fatty acids were 47.5–55.2% oleic acid (C18:1), 26.1–33.6% palmitic acid (C16:0) and 7.8–11.3% stearic acid (C18:0). Other minor fatty acids included 0.82–1.38%

myristic acid (C14:0), 1.7–2.9% linoleic acid (C18:2) and 1.5– 3.5% linolenic acid (C18:3). Such fatty acid compositional profiles were in line with the previous study with *R. toruloides* and similar to those of vegetable oils.<sup>11</sup> The contents of linoleic acid were below the specified limit of 12% (w/w) for biodiesel production according to the European Standard EN 14214. The fact that no difference was found in terms of fatty acid species among those strains indicated that the Pta enzyme had little direct effects on the enzymes of fatty acid biosynthetic pathway, but might facilitate the fatty acid precursor acetyl-CoA supply. The MLs from engineered strains can be used as alternative feedstock for oleochemicals production (Table 1).

### 3. Experimental

#### 3.1 Strain, media and reagents

*R. toruloides* NP11, a haploid derivative of *R. toruloides* AS 2.1389 from China General Microbiological Culture Collection Center, was maintained at 4 °C on YEPD agar slant containing (g  $L^{-1}$ ): glucose 20, yeast extract 10, peptone 10 and agar powder 20, pH 6. All the strains and plasmids are listed in Table 2.

Lipid production media for flask cultures contained (g L<sup>-1</sup>): glucose 50, yeast extract 0.75, (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> 0.1, Mg<sub>2</sub>SO<sub>4</sub>  $\cdot$ 7H<sub>2</sub>O 1.5 and KH<sub>2</sub>PO<sub>4</sub> 0.4, pH 6.0. The lipid production media for bioreactor experiments contained (g L<sup>-1</sup>): glucose 50, (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> 10.0, yeast extract 10.0, KH<sub>2</sub>PO<sub>4</sub> 1.0, MgSO<sub>4</sub>  $\cdot$ 7H<sub>2</sub>O 1.0 and trace element stock solution (1%, v/v), pH 6.0. For feeding experiments, 1000 g L<sup>-1</sup> glucose solution was used. All media were sterilized by autoclaving at 121 °C for 18 min. Trace element solution was added to all media after sterilization to a final concentration (mg L<sup>-1</sup>): CaCl<sub>2</sub>  $\cdot$ 2H<sub>2</sub>O 40, FeSO<sub>4</sub>  $\cdot$ 7H<sub>2</sub>O 5.5, citric acid  $\cdot$ H<sub>2</sub>O 5.2, ZnSO<sub>4</sub>  $\cdot$ 7H<sub>2</sub>O 1.0 and MnSO<sub>4</sub>  $\cdot$ H<sub>2</sub>O 0.76.

DNA polymerases and restriction enzymes were supplied by TaKaRa (Dalian, China). Acetosyringone, kanamycin, hygromycin and primers were from Dingguo Biotechnology Co. Ltd (Beijing, China). All other chemicals were of analytical grade and bought locally.

#### 3.2 Construction of plasmids

The binary vector was constructed based on the pZPK plasmid with kanamycin resistance coding cassette.<sup>14</sup> A *B. subtilis* 

originated phosphoacetyltransferase gene (*Pta*) was redressed by referring to the *R. toruloides* codon preference (ESI<sup>†</sup>) and synthesized (Synbio Technologies, Suzhou, China). The promoter of glyceraldehyde-3-phosphate dehydrogenase (*Pgpd*) was cloned from *R. toruloides* genome with the primers GPD-Xbal I-F and GPD-EcoR V-R. The PTA gene was then cloned with the primer pair Pta-EcoR V-F/Pta-Spe I-R (ESI<sup>†</sup>). Both the plasmid PZPK-Pgpd-MCS-Thsp and *Pta* gene were cleaved by restriction enzyme *Eco*R I and *Spe* I, and ligated to generate the plasmid PZPK-Pgk-HYG-Tnos-Pgpd-PTA-Thsp for further engineering of *R. toruloides*.

#### 3.3 Genetic transformation and characterization

The Agrobacterium-mediated transformation protocol was based on a published method.<sup>14</sup> *R. toruloides* transformants were picked and grew for five successive generations on YEPD plate containing 50 mg L<sup>-1</sup> hygromycin for stability test. For reversetranscriptional PCR analysis, total RNA and cDNA samples were prepared from *R. toruloides* transformants using the PrimeScript<sup>TM</sup> RT reagent Kit gDNA Eraser (Takara, Dalian, China). The Pta expression was detected with the primer pair Pta-RtPCR-F/Pta-RtPCR-R (ESI†).

For genome walking experiments, total genomic DNA samples were extracted from *R. toruloides* transformants according to a former study.14 The thermal asymmetrical interlaced-polymerase chain reaction (TAIL-PCR) was used to identify the flanking sequence of T-DNA as described.<sup>15</sup> Four arbitrary degenerated primers (LAD-1, LAD-2, LAD-3, LAD-4) and three specific right border (RB) primers (Pta-RB764, Pta-RB826, Pta-RB974) were used (ESI<sup>†</sup>). The four arbitrary degenerate primers and the Pta-RB764 were used in pre-amplification. The secondary TAIL-PCR cooperated with Pta-RB826 and LAD-1. Pta-RB973 and LAD-1 were applied for the last round genome walking. Only the most specific product over 700 bp was purified with San Prep Column DNA Gel Extraction Kit of Sangon Biotech (Shanghai, China), ligated into pMD<sup>™</sup> 18-T Vector and transformed into Escherichia coli DH5a. Transformants were picked out by colony PCR and the sequences between the Tcloning sites were determined by Sangon Biotech. T-DNA location was identified by comparing the sequences with published R. toruloides genome using the BLAST program.<sup>13</sup>

Table 1	Strains and	plasmids used in this study	

Strains or plasmids	Relevant characteristics	Source or resources						
Strains								
R. toruloides NP11 GCMCC A 2.224	MAT A	Zhu <i>et al.</i> , (2012)						
R. toruloides NP-Pta-4	PZPK-Ppgk-HYG-Tnos-Pgpd-PTA-Thsp, HYG <sup>R</sup>	This study						
R. toruloides NP-Pta-6	PZPK-Ppgk-HYG-Tnos-Pgpd-PTA-Thsp, HYG <sup>R</sup>	This study						
<i>R. toruloides</i> NP-Pta-15	PZPK-Ppgk-HYG-Tnos-Pgpd-PTA-Thsp, HYG <sup>R</sup>	This study						
R. toruloides NP-Pta-20	PZPK-Ppgk-HYG-Tnos-Pgpd-PTA-Thsp, HYG <sup>R</sup>	This study						
Agrobacterium tumefaciens AGL1-HYG-Pta	PZPK-Ppgk-HYG-Tnos-Pgpd-PTA-Thsp	This study						
Plasmids								
PZPK-Pgpd-MCS-Thsp	PZPK-Ppgk-HYG-Tnos-Pgpd-MCS-Thsp in PZPK	This study						
PZPK-Pgpd-PTA-Thsp	PZPK-Ppgk-HYG-Tnos-Pgpd-PTA-Thsp in PZPK	This study						

	c !!	Lipid content (%)	Lipid yield (g g <sup>-1</sup> )	Lipid productivity $(g L^{-1} d^{-1})$	Relative fatty acid content (%)					
Strains	Cell mass (g L <sup>-1</sup> )				C14:0	C16:0	C18:0	C18:1	C18:2	C18:3
NP11 <sup>a</sup>	$11.8\pm0.5$	$62.1\pm2.4$	$0.146 \pm 0.002$	$0.73\pm0.01$	$1.38\pm0.22$	$33.6\pm0.4$	$9.6\pm0.8$	$47.5\pm1.5$	$2.7\pm0.3$	$3.3\pm0.6$
NP-Pta-4 <sup>a</sup>	$12.5\pm0.2$	$66.0\pm4.7$	$0.166\pm0.009$	$0.92\pm0.05$	$1.02\pm0.03$	$31.9\pm0.1$	$7.8\pm0.1$	$52.1\pm0.4$	$1.9\pm0.1$	$3.5\pm0.2$
NP-Pta-6 <sup>a</sup>	$12.3\pm0.3$	$65.8 \pm 1.7$	$0.160\pm0.008$	$0.89\pm0.03$	$0.87\pm0.04$	$30.8\pm0.1$	$8.5\pm0.6$	$52.1\pm0.9$	$2.2\pm0.5$	$3.1\pm0.3$
NP-Pta-15 <sup>a</sup>	$12.8\pm0.5$	$65.6 \pm 2.4$	$0.168 \pm 0.008$	$1.20\pm0.06$	$0.82\pm0.02$	$26.1\pm0.2$	$11.3\pm0.8$	$55.2 \pm 1.8$	$1.7\pm0.9$	$3.0\pm1.0$
NP-Pta-20 <sup>a</sup>	$12.2\pm0.2$	$68.0\pm1.0$	$0.166\pm0.002$	$0.92\pm0.01$	$1.14\pm0.24$	$31.7\pm1.2$	$7.8\pm0.7$	$53.1\pm2.1$	$2.9 \pm 1.9$	$1.5\pm0.5$
NP11 <sup>b</sup>	45.6	32.0	0.073	2.43	2.1	30.5	9.5	36.5	13.3	4.8
NP-Pta-15 <sup>b</sup>	57.5	28.2	0.081	3.75	1.5	31.2	12.0	43.0	7.8	2.0

<sup>a</sup> Experiments with shale flasks. <sup>b</sup> Experiments with 3 L stirred-tank bioreactor.

#### 3.4 Lipid production procedures

The inocula were prepared in YEPD liquid medium. A loop of NP11 or the engineered NP11 was inoculated into the YEPD medium and cultivated at 30 °C, 200 rpm for 24 h. Then the seed was transferred into lipid production medium for lipid production. The initial OD<sub>600</sub> was 0.8 and the culture was sampled at intervals of 24 h for cell mass, lipid and glucose consumption analysis. All the experiments in flasks were done with a working volume of 50 mL and performed in triplicate. The experiments on 3 L bioreactor were initiated with a working volume of 1.8 L and an initial OD<sub>600</sub> of 0.8. The air flow rate was 2 L min<sup>-1</sup> and the dissolved oxygen was maintained above 40% by auto-controlled stirring. The cell mass, lipid and glucose consumption analysis were conducted at time intervals of 24 h and the glucose stock solution was added when needed.

#### 3.5 Analytical methods

Glucose was quantified by a glucose analyzer (SBA-50B; Shandong Academy of Sciences, Jinan, China). Cell mass was expressed as dry cell weight (DCW). Cells from 30 mL of culture broth were harvested by centrifugation at  $8000 \times g$  for 5 min, washed twice with distilled water, and dried at 105 °C to a constant weight. Lipids were extracted and the fatty acid composition of lipid samples was profiled by using a 7890F gas chromatography instrument after transesterification.<sup>11</sup> Lipid content was expressed as g lipid per g DCW multiplied by 100%. The cell mass yield was defined as g cell mass per g sugar consumed. The lipid yield was defined as g lipid per g sugar consumed. The lipid productivity was defined as g lipid per litre per day. All values for flask cultures were the average of three independent experiments.

### 4. Conclusions

In summary, this study demonstrated that overexpression of the Pta gene in the yeast *R. toruloides* NP11 can lead to strains with improved performance in terms of glucose consumption, cell growth and lipid production. The presence of Pta may establish an additional acetyl-CoA formation route by utilization of ace-tylphosphate. Our results should inspire more engineering efforts to facilitate the economic viability of large-scale ML production.

## Conflicts of interest

There are no conflicts to declare.

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