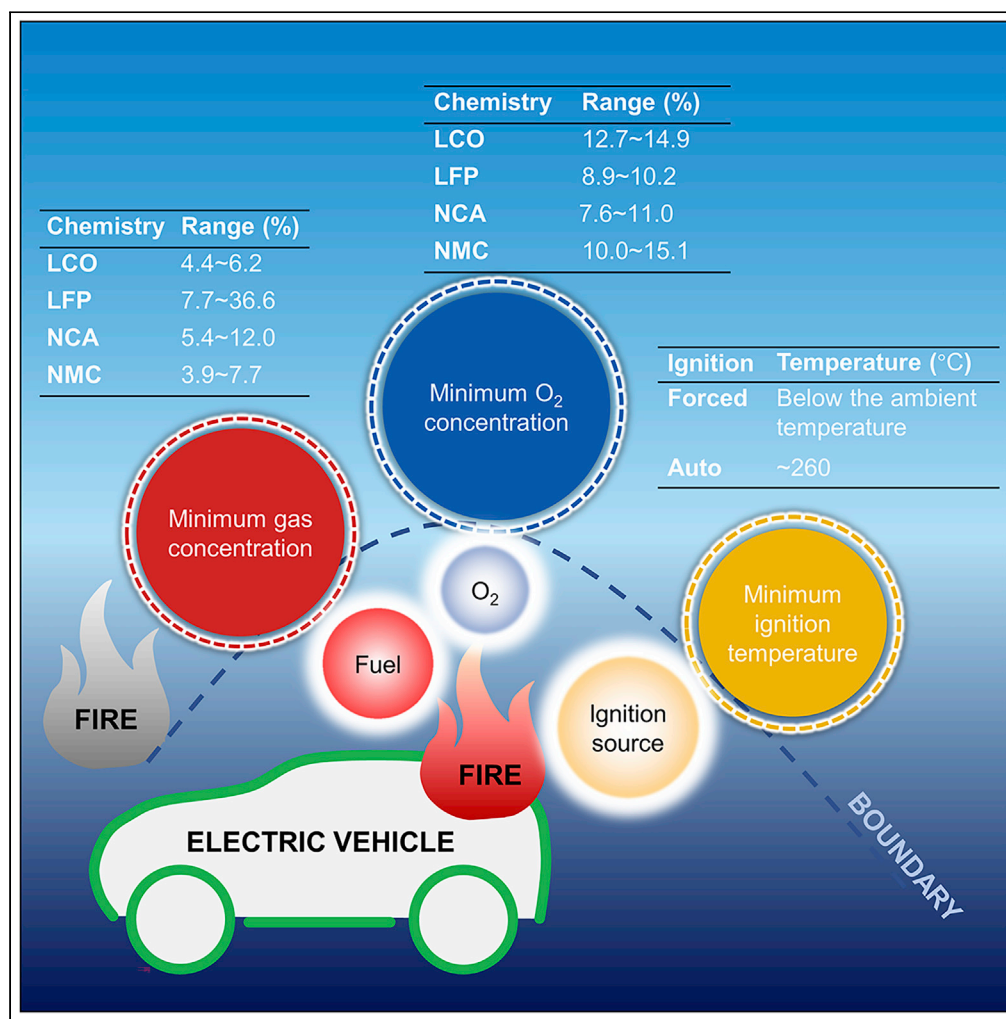


## Article

## Fire boundaries of lithium-ion cell eruption gases caused by thermal runaway



Weifeng Li, Shun Rao, Yang Xiao, Zhenhai Gao, Yupeng Chen, Hewu Wang, Minggao Ouyang

gaozh@jlu.edu.cn (Z.G.)  
ypchen0727@buaa.edu.cn (Y.C.)  
ouymg@tsinghua.edu.cn (M.O.)

**Highlights**

We clarified the three fire boundaries of LIBs corresponding to the fire triangle

Batteries are prone to ignition with forced ignition sources

Batteries are hard to autoignite when temperatures are low enough

LIB ignition modes can be controlled by changing temperatures and ignition sources

## Article

## Fire boundaries of lithium-ion cell eruption gases caused by thermal runaway

Weifeng Li,<sup>1</sup> Shun Rao,<sup>1</sup> Yang Xiao,<sup>1</sup> Zhenhai Gao,<sup>1,4,\*</sup> Yupeng Chen,<sup>2,\*</sup> Hewu Wang,<sup>3</sup> and Minggao Ouyang<sup>3,\*</sup>

## SUMMARY

Lithium-ion batteries are applied in electric vehicles to mitigate climate change. However, their practical applications are impeded by poor safety performance owing mainly to the cell eruption gas (CEG) fire triangle. Here, we report quantitatively the three fire boundaries corresponding to the CEG fire triangle of four types of mainstream cells with the state of charge (SOC) values ranging from 0% to 143% based on 29 thermal runaway tests conducted in an inert atmosphere in open literature. Controlling the SOC and/or selecting a reasonable cell type can alter the minimum CEG and oxygen concentrations required for ignition, thereby changing the probability of a battery fire. The ignition temperature varies greatly according to the type of ignition source type. Temperature and ignition source type play a leading role in the ignition mode. Breaking any fire boundary will stop the ignition of CEG, thus significantly improving the battery safety performance.

## INTRODUCTION

Electric vehicles are paid much attention to mitigate climate change (Stephan et al., 2021; Han et al., 2019; Gourley et al., 2020). After many years of development, lithium-ion batteries (LIBs) have become increasingly acceptable as the main power source of electric vehicles, given their higher energy density and longer life cycle (EIA, 2020; Liu et al., 2018). However, the safety aspects concerning electric vehicles have received increasing attention due to the hazards of possible fires, usually caused by the failure of on-board large capacity power batteries (Sun et al., 2020).

As one of the main energetic failures, thermal runaway refers to the rapid self-heating of a cell, resulting from the exothermic chemical reaction between the highly oxidizing positive electrode and highly reducing negative electrode of the cell. This can occur in batteries with almost any chemistry (Mikolajczak et al., 2011). With the occurrence of LIB thermal runaway, more and more gases are generated inside the cells. Then, when the pressure inside a cell reaches a certain value, the cell's safety valve is released, or the area at the aluminum-plastic film with the lower allowable pressure for the pouch cell develops a crack. Then, the cell erupts and releases gaseous emissions, i.e., cell eruption gases (CEGs) (Finegan et al., 2015; Wang et al., 2019a; Li et al., 2019b; Zhang et al., 2019). These gases are among the main combustion materials that lead to fires (Xu and Hui, 2017; Bi et al., 2015).

Because CEGs are generally released from the inside of a cell to the battery pack and the external environment, the main combustion-supporting material is oxygen ( $O_2$ ) in air. The parameters corresponding to the first two boundaries are the lower flammability limit (LFL) and upper flammability limit (UFL) of the CEGs, which are expressed by the CEG concentration in the CEG-air mixture. When the CEG concentration is lower than the LFL, the CEGs are too thin for ignition. Therefore, the LFL is the  $C_{CEG, ignition}$ . When the CEG concentration is greater than the UFL, because it is too rich, meaning that the surrounding  $O_2$  is too thin, ignition cannot occur. The  $O_2$  concentration in the CEG-air mixture corresponding to the UFL is the minimum  $O_2$  concentration ( $C_{O_2, ignition}$ ) required for ignition. When the CEG concentration is between the LFL and UFL, there is neither a lack of fuel nor  $O_2$  and ignition can occur.

It should be noted that the  $C_{O_2, ignition}$  mentioned here refers to the  $O_2$  concentration in the CEG-air mixture at the LFL (Liu et al., 2004). It is due to the too rich fuel and too lean  $O_2$  for ignition

<sup>1</sup>State Key Laboratory of Automotive Simulation and Control, Jilin University, Changchun 130025, China

<sup>2</sup>Key Laboratory of Bio-inspired Smart Interfacial Science and Technology of Ministry of Education, School of Chemistry, Beihang University, Beijing 100191, P.R. China

<sup>3</sup>State Key Laboratory of Automotive Safety and Energy, Tsinghua University, Beijing 100084, P.R. China

<sup>4</sup>Lead contact

\*Correspondence: gaozh@jlu.edu.cn (Z.G.), ypchen0727@buaa.edu.cn (Y.C.), ouymg@tsinghua.edu.cn (M.O.)

<https://doi.org/10.1016/j.isci.2021.102401>



to take place. Another similar concept is the critical  $O_2$  concentration (Fairweather et al., 1999), which refers to the  $O_2$  concentration in the fuel-air dilution mixture when the LFL coincides with the UFL using inert gas to dilute the fuel-air mixture. In fact, the critical  $O_2$  concentration is a special case of  $c_{O_2, \text{ignition}}$ .

To obtain the flammability limit of the CEG, three research methods are generally used. In the first method, thermal runaway is triggered in an inert atmosphere until eruption, and the CEG components are then detected. Afterward, calculations are performed on the basis of the detected components. Based on the existing results (Somandepalli et al., 2014), Guo et al. (Guo and Zhang, 2016) calculated the flammability limits of CEGs and found that the flammability range increases with an increase in the state of charge (SOC). In our open study (Li et al., 2019b), the flammability limits of the CEGs released by commercial 18,650 LIBs with lithium nickel cobalt aluminum oxide (NCA) and lithium iron phosphate (LFP) cathodes at 0%–143% SOC were calculated using available data in open literature (Golubkov et al., 2015). We found that the UFL and LFL curves of CEGs form a peninsula shape for both cell types with a decrease in the SOC, where the flammability range did not essentially change at first and then dramatically decreased. For the LFP cell, the LFL of the CEGs was higher, and the flammability range was lower than that of the NCA cell at the same SOC.

In the second method, a thermal runaway test is performed in a vacuum environment, and the released cell gases are collected. Then, the flammability limit of the gases is directly tested through an experimental method using a combustion chamber. By using this method, Somandepalli et al. (Somandepalli et al., 2014) found that the LFL of CEGs is about 6.3% and the UFL is between 30 and 40% for cases of 100% and 150% SOC.

The third method is similar to the second but is conducted in an air environment. In this case, the detected gas is the product of the reaction between CEGs and the air in the test container rather than the CEGs alone. However, the results are of important reference value for evaluating whether CEGs are flammable in the atmosphere after being released from battery packs. Long et al. (Long et al., 2014) subjected a 100 Ah 3.3 V cell to thermal runaway by overcharging it and then collected the CEGs. They opened the valve of the gas collection bag, ignited the gas using an igniter in a laboratory, and found that the CEGs continued to burn. Chen et al. (Chen et al., 2020) used a cell in a closed container filled with air to conduct a thermal runaway test and then tested the LFL of the CEG. They found that the LEL of the CEG increased at the initial stage and then decreased with an increase in the SOC. Moreover, they reported that batteries should be stored at 60% SOC in non-extremely dry environments to reduce the risk of explosion and that keeping the SOC at 100%, which has the lowest LEL, poses a high risk of danger caused by thermal runaway.

### However, some problems remain regarding cell eruptions and fires

First, there are few comparisons of the  $c_{\text{CEG, ignition}}$  for different types of cells, which makes it difficult to provide better guidance for cell selection and battery pack design. Baird et al. (Baird et al., 2020) evaluated the LFL of CEGs to quantify the cell chemistry effect and SOC using three modeling methods. They found that the LFL was 7.6–9.0, 8.6–10.0, 6.1–8.8, and 6.7–11.8 for lithium nickel cobalt manganese oxide (NMC), LFP, lithium cobalt oxide (LCO), and NCA cells, respectively. The results showed that the CEG of LFP generally had higher LFL values at 100% SOC, allowing for more gases to accumulate before reaching deflagration or a fire hazard compared with that of NCA or LCO cells. However, these calculation results were based on gases detected in air, vacuum, and inert atmospheres. It is difficult to distinguish which results were based on the CEG and which results were based on the reaction products of the CEG and air. CEGs are generally ejected from the inside of a cell to the battery pack and subsequently react with the air in the pack before being released to the atmosphere. Therefore, it is still difficult to directly provide guidance for the design of battery packs based on these results.

Second, insufficient data are available (Garche and Brandt, 2018) on the minimum  $O_2$ /air concentration (without the introduction of other inert gases) required for CEG ignition for different types of cells. This makes it difficult to provide better guidance for battery pack design. If the amount of air inside a battery pack can be changed to make the  $O_2$  content below the  $c_{O_2, \text{ignition}}$ , ignition can be avoided, thus slowing the spread of heat and the resultant damage to the pack components, cells, circuits, and other parts.

**Table 1. Equipment used to detect the cell eruption gases in the summarized works**

Literature	Equipment	Model	Gas detected
Somandepalli et al. (2014)	GC-MS	–	CO, CO <sub>2</sub> , H <sub>2</sub> , and hydrocarbons
Golubkov et al. (2014)	GC	Agilent 3000 Micro GC, two columns, Mol Sieve and PLOTU	H <sub>2</sub> , O <sub>2</sub> , N <sub>2</sub> , CO, CO <sub>2</sub> , CH <sub>4</sub> , C <sub>2</sub> H <sub>2</sub> , C <sub>2</sub> H <sub>4</sub> , and C <sub>2</sub> H <sub>6</sub>
	TCD	–	Permanent gases
Golubkov, et al., 2015	GC	Agilent 3000 Micro GC, two columns, Mol Sieve and PLOTU	H <sub>2</sub> , O <sub>2</sub> , N <sub>2</sub> , CO, CO <sub>2</sub> , CH <sub>4</sub> , C <sub>2</sub> H <sub>2</sub> , C <sub>2</sub> H <sub>4</sub> , and C <sub>2</sub> H <sub>6</sub>
	TCG	–	Permanent gases
Lammer et al., 2017	GC	Agilent Micro-GC 3000A	H <sub>2</sub> , CO, CO <sub>2</sub> , CH <sub>4</sub> , C <sub>2</sub> H <sub>2</sub> , C <sub>2</sub> H <sub>4</sub> , and C <sub>2</sub> H <sub>6</sub>
Zhang et al., 2019	GC	Agilent 7890A	H <sub>2</sub> , CO, CO <sub>2</sub> , and hydrocarbons
	GC-MS	Agilent 7890B-5977A	DEC, EMC
	IC	Metrohm 930 Compact	HCl
Essl et al., 2020	FTIR	Bruker MATRIX-MG01	CO, CO <sub>2</sub> , CH <sub>4</sub> , C <sub>2</sub> H <sub>6</sub> , C <sub>2</sub> H <sub>4</sub> , C <sub>2</sub> H <sub>2</sub> , DEC, DMC, EC, EMC, H <sub>2</sub> O, C <sub>6</sub> H <sub>14</sub> , HF, C <sub>4</sub> H <sub>10</sub> , and C <sub>3</sub> H <sub>8</sub>
	GC	3000 Micro GC (G2802A) with three columns and TCD detectors	H <sub>2</sub> , O <sub>2</sub> , N <sub>2</sub> , CH <sub>4</sub> , CO, CO <sub>2</sub> , C <sub>2</sub> H <sub>6</sub> , C <sub>2</sub> H <sub>4</sub> , C <sub>2</sub> H <sub>2</sub>

For more information, refer to Zhang et al. (2019); Somandepalli et al. (2014); Golubkov et al. (2015); Golubkov et al. (2014); Lammer et al. (2017); and Essl et al. (2020).

Third, few analysis results (Garche and Brandt, 2018) have been presented for  $T_{\text{ignition}}$ . If this boundary is known, the CEG temperature can be reduced to a value below the boundary through thermal management, thus avoiding the possibility of CEG ignition after their release.

Therefore, based on our previous research on the generation reasons (Li et al., 2019a), eruption characteristics (Wang et al., 2019a; Zhang et al., 2020), component identification (Zhang et al., 2019), ignition sources (Zhang et al., 2019), and flammability analyses (Li et al., 2019b) of CEGs, we summarize the CEG component identification results of 29 thermal runaway tests conducted in an inert atmosphere, as presented in the literature (Zhang et al., 2019; Somandepalli et al., 2014; Golubkov et al., 2014, 2015; Lammer et al., 2017; Essl et al., 2020). According to the results, a time sequence diagram of CEG generation is drawn, and the three fire boundaries of CEGs, including  $C_{\text{CEG}}$ ,  $T_{\text{ignition}}$ , and  $T_{\text{CO}_2}$ , are analyzed on the basis of thermal ignition theory. Overall, this research can provide theoretical guidance for cell selection, pack design, and fire safety design.

### Review of the cell eruption gas components

This study focuses on summarizing the performed works (Zhang et al., 2019; Somandepalli et al., 2014; Golubkov et al., 2014, 2015; Lammer et al., 2017; Essl et al., 2020) in the last 10 years regarding the identification of CEG in an inert atmosphere because triggered thermal runaway in an inert atmosphere avoids chemical changes as much as possible after the CEG is ejected from the cell.

Table 1 shows equipment used in the summarized works (Zhang et al., 2019; Somandepalli et al., 2014; Golubkov et al., 2014, 2015; Lammer et al., 2017; Essl et al., 2020) and the types of gases detected. The used instruments mainly included gas chromatography-mass spectrometers (GC-MSs), gas chromatographers (GCs), thermal conductivity detectors (TCGs), ion chromatographs (ICs), and Fourier transform infrared spectrometers (FTIRs). The types of detected gases mainly included hydrogen (H<sub>2</sub>), oxygen (O<sub>2</sub>), nitrogen (N<sub>2</sub>), carbon monoxide (CO), carbon dioxide (CO<sub>2</sub>), methane (CH<sub>4</sub>), ethyne (C<sub>2</sub>H<sub>2</sub>), ethylene (C<sub>2</sub>H<sub>4</sub>), ethane (C<sub>2</sub>H<sub>6</sub>), and other hydrocarbons. In addition, diethyl carbonate (DEC), methyl ethyl carbonate (EMC),

**Table 2. Details of the cells used in the thermal runaway tests in inert atmosphere in the summarized works**

Test no.	Literature	Legend	Chemistry	Format	Nominal capacity (Ah)	SOC (%)
1	<a href="#">Somandepalli et al. (2014)</a>	LCO_2.1 Ah	LiCoO <sub>2</sub>	–	2.1	50
2						100
3						150
4	<a href="#">Golubkov et al. (2014)</a>	LFP_1.1 Ah (2014)	LiFePO <sub>4</sub>	18650	1.1	100
5	<a href="#">Golubkov, et al., 2015</a>	LFP_1.1 Ah (2015)	Li <sub>0.882</sub> FePO <sub>4</sub>	18650	1.1	0
6						25
7						50
8						75
9						100
10						115
11						130
12	<a href="#">Lammer et al. (2017)</a>	NCA_3.2 Ah	LiNi <sub>0.8</sub> Co <sub>0.15</sub> Al <sub>0.05</sub> O <sub>2</sub>	18650	3.2	100
13	<a href="#">Golubkov et al. (2015)</a>	NCA_3.35 Ah	Li <sub>0.925</sub> (Ni <sub>0.80</sub> Co <sub>0.15</sub> Al <sub>0.05</sub> )O <sub>2</sub>	18650	3.35	0
14						25
15						50
16						75
17						100
18						112
19						120
20						127
21						132
22						143
23	<a href="#">Lammer et al. (2017)</a>	NCA_3.5 Ah (47.68 g)	LiNi <sub>0.8</sub> Co <sub>0.15</sub> Al <sub>0.05</sub> O <sub>2</sub>	18650	3.5	100
24		NCA_3.5 Ah (46.35 g)				100
25	<a href="#">Golubkov et al. (2014)</a>	NMC_1.5 Ah	Li(Ni <sub>0.45</sub> Mn <sub>0.45</sub> Co <sub>0.10</sub> )O <sub>2</sub>	18650	1.5	100
26	<a href="#">Zhang et al. (2019)</a>	NMC_50 Ah	Li(Ni <sub>0.6</sub> Mn <sub>0.2</sub> Co <sub>0.2</sub> )O <sub>2</sub>	Prismatic	50	100
27	<a href="#">Golubkov et al. (2014)</a>	NMC/LCO_2.6 Ah	LiCoO <sub>2</sub> /	18650	2.6	100
			Li(Ni <sub>0.50</sub> Mn <sub>0.25</sub> Co <sub>0.25</sub> )O <sub>2</sub>			
28	<a href="#">Essl et al. (2020)</a>	NMC/LMO_41Ah	LiNiMnCoO <sub>2</sub> /LiMn <sub>2</sub> O <sub>4</sub>	Pouch	41	100
29						30

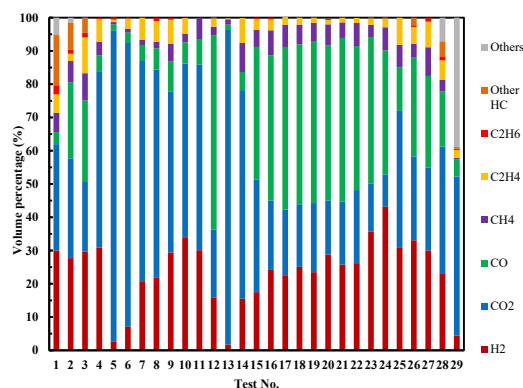
For more information, refer to [Zhang et al. \(2019\)](#); [Somandepalli et al. \(2014\)](#); [Golubkov et al. \(2015\)](#); [Golubkov et al. \(2014\)](#); [Lammer et al. \(2017\)](#); and [Essl et al. \(2020\)](#).

dimethyl carbonate (DMC), hydrogen chloride (HCl), ethylene carbonate (EC), hydrogen fluoride (HF), etc., were also detected.

Table 2 shows the details of the cells used in the summarized works ([Zhang et al., 2019](#); [Somandepalli et al., 2014](#); [Golubkov et al., 2014, 2015](#); [Lammer et al., 2017](#); [Essl et al., 2020](#)). The cell chemistries include common types, such as LCO, LFP, NCA, and NMC. The cell capacity ranged from 1.1 Ah to 50 Ah, and the cell formats included square, 18650, and pouch. The SOC values varied from 0% to 143%.

Figure 1 shows the main CEG components detected in the summarized works ([Zhang et al., 2019](#); [Somandepalli et al., 2014](#); [Golubkov et al., 2014, 2015](#); [Lammer et al., 2017](#); [Essl et al., 2020](#)), which were H<sub>2</sub>, CO<sub>2</sub>, CO, CH<sub>4</sub>, C<sub>2</sub>H<sub>4</sub>, and C<sub>2</sub>H<sub>6</sub>. In addition, the components included electrolyte vapor, HF, and other gases. The formation reactions of the main CEG components are summarized in detail in the study by ([Wang et al., 2019b](#)).

Figure 2 shows the time sequence of the CEG generation. In addition to the electrolyte vaporization (90°C–248°C) caused by physical changes, the CEG also contains new gases generated by chemical reactions, which



**Figure 1. Variations of the volume percentage of the CEG components in the summarized works vs. test number**

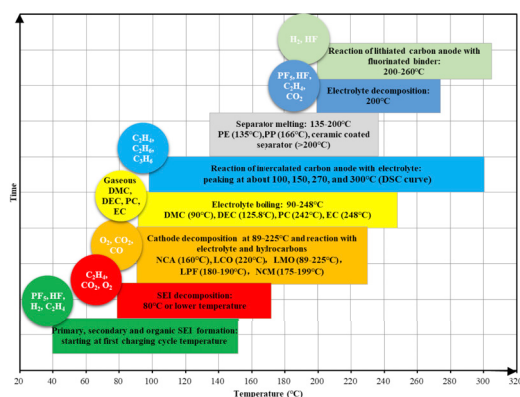
CEG identification result is based on 29 thermal runaway tests conducted in an inert atmosphere in open literature.

can be explained by the thermal decomposition and reactions of the electrolyte, binder, and electrode materials (Golubkov et al., 2014; Wang et al., 2012; Roth and Orendorff, 2012; Fleischhammer and Döring, 2013; Pfrang et al., 2017), as mentioned in the summarized works (Golubkov et al., 2014, 2015; Kocha et al., 2018).

The solid electrolyte interphase (SEI) is a reaction layer that is formed by electrolyte reduction during the first charging cycle on the surfaces of carbon-based anodes (Garche and Brandt, 2018). During the formation of the primary SEI, gases including phosphorus pentafluoride ( $\text{PF}_5$ ), HF,  $\text{H}_2$ ,  $\text{C}_2\text{H}_4$ , etc., are produced (Agubra and Fergus, 2014; Aurbach et al., 1999; Watanabe and Yamaki, 2006). In general, the SEI consists of inorganic and organic compounds. The organic compounds are metastable at around  $80^\circ\text{C}$ , and they start to react and form the so-called secondary SEIs (Wang et al., 2006; Yang et al., 2005; Richard and Dahn, 1999; Andersson and Edström, 2001). The secondary SEI mainly consists of lithium carbonate ( $\text{Li}_2\text{CO}_3$ ) and lithium fluoride (LiF) (Yang et al., 2005). It has been suggested that besides the formation of secondary SEIs, new organic SEIs are formed by solvent reduction. These complex processes of SEI formation and change occur up to a temperature of  $\sim 200^\circ\text{C}$  (Wang et al., 2006; Zhou et al., 2012). During the formation of secondary SEIs, gases including HF,  $\text{C}_2\text{H}_4$ ,  $\text{CO}_2$ ,  $\text{O}_2$ ,  $\text{C}_2\text{H}_6$ , etc., are produced (Agubra and Fergus, 2014; Aurbach et al., 1999; Zhou et al., 2012). The initial decomposition of SEI occurs at  $80^\circ\text{C}$ – $120^\circ\text{C}$  (Spotnitz and Franklin, 2003) with a peak at  $\sim 100^\circ\text{C}$  (Richard and Dahn, 1999). An SEI layer may decompose at relatively lower temperatures, such as  $69^\circ\text{C}$  (Wang et al., 2006) or  $57^\circ\text{C}$  (Wang et al., 2005).  $\text{C}_2\text{H}_4$ ,  $\text{CO}_2$ ,  $\text{O}_2$ , and other gases are produced during the thermal decomposition of SEI (Yang et al., 2005).

The differential scanning calorimetry traces of the lithiated carbon anodes and electrolytes become very complex at the following peaks:  $\sim 100^\circ\text{C}$ ,  $\sim 150^\circ\text{C}$ ,  $\sim 270^\circ\text{C}$ , and  $\sim 300^\circ\text{C}$  (Spotnitz and Franklin, 2003).

Organic solvents (EC, PC, DMC, etc.) can also react with intercalated lithium to release flammable hydrocarbons, such as  $\text{C}_2\text{H}_4$ ,  $\text{C}_3\text{H}_6$ , and  $\text{C}_2\text{H}_6$  (Spotnitz and Franklin, 2003; Aurbach et al., 1997; Gachot et al., 2010, 2012; Yoshida et al., 1997; Onuki et al., 2008; Shin et al., 2002).



**Figure 2. Time sequence of CEG generation**

Temperature without special explanations refers to the onset temperature of reaction, decomposing, boiling, or melting.

The PE and PP separators melt at 135°C and 166°C, respectively, while some ceramic-coated separators may maintain their structural integrity even above 200°C (Mao et al., 2018; Orendorff, 2012). It has not been previously reported in open literature that gas can be produced during this process.

The initial decomposition of cathodes occurs at 89°C–225°C (Biensan et al., 1999; Wang et al., 2007a, 2007b; Huang et al., 2016; Zhang et al., 1998; Martha et al., 2011; Joachin et al., 2009), and then, O<sub>2</sub> is released (Dahn et al., 1994; Li et al., 2006). The release of O<sub>2</sub> can lead to a further reduction of the generated hydrocarbons down to CO<sub>2</sub>. Since this O<sub>2</sub> generation from the cathodes inside the cells and the other O<sub>2</sub> sources are both limited, some hydrocarbons only get reduced to CO (Golubkov et al., 2014; Roth and Orendorff, 2012).

LiPF<sub>6</sub> salt decomposes at 200°C to LiF and PF<sub>5</sub> (Ravdel et al., 2003). The decomposition of the electrolyte is a multistage reaction and mainly takes place in the ranges of 200°C–220°C, 220°C–250°C, and 250°C–300°C, generating gases such as PF<sub>5</sub>, HF, CO<sub>2</sub>, and C<sub>2</sub>H<sub>4</sub> (Ribiere et al., 2012; Wang et al., 2019b; Campion et al., 2004; Gnanaraj et al., 2003; Kawamura et al., 2006).

When a carbon anode is intercalated with lithium-ions, it can react with PVDF, generating HF and H<sub>2</sub> (Pasquier et al., 1998). The temperatures at which the reaction begins were reported to be 200°C (Maleki et al., 1999), 240°C (Biensan et al., 1999), and 260°C (Pasquier et al., 1998).

## RESULTS AND DISCUSSION

Gas can be divided into two types: non-flammable and flammable. In the former case, no gas ignition will occur regardless of the conditions. As determined in tests 5 and 13 shown in Table 2 and Figure 1, CEGs are non-flammable when the SOC is 0% owing to the high CO<sub>2</sub> content (Li et al., 2019b). However, the CEGs were flammable in the other 27 tests. It should be noted that flammable does not guarantee ignition. To achieve fire, combustibles need an oxidizer, an ignition source, ignition energy, ignition critical diameter, etc (Xu and Hui, 2017; Bi et al., 2015; Turns and Haworth, 2021). The main conditions for ignition are collectively known as the fire triangle, i.e., a combustible, an oxidizer, and an ignition source. The three fire boundaries corresponding to the fire triangle are  $c_{CEG, ignition}$ ,  $CO_{2, ignition}$  and  $T_{ignition}$ . According to the thermal ignition theory, these three boundaries are necessary for fire but not sufficient (Xu and Hui, 2017; Bi et al., 2015; Turns and Haworth, 2021). When one of the fire boundaries is met, a fire may occur or not. But when any one of the fire boundaries is not met, a fire cannot occur. This means that if any one of fire boundaries is broken, no fire will occur. This is of great significance for battery fire suppression. This section analyzes the three fire boundaries of flammable CEGs in a cell fire based on the thermal ignition theory. When analyzing the impact of a certain boundary, it is assumed that the other fire boundaries are available. Considering the limited amount of data in open literature (Zhang et al., 2019; Somandepalli et al., 2014; Golubkov et al., 2014, 2015; Lammer et al., 2017; Essl et al., 2020), when discussing the changes in  $c_{CEG, ignition}$  and  $CO_{2, ignition}$  with SOC, only the trends of LFP\_1.1 Ah (2015), NCA\_3.35 Ah (2015), and LCO\_2.1 Ah were discussed. In addition, to compare the differences between cell types, cells using NMC, NMC/LCO, and NMC/LMO as positive electrodes were collectively classified as NMC cells.

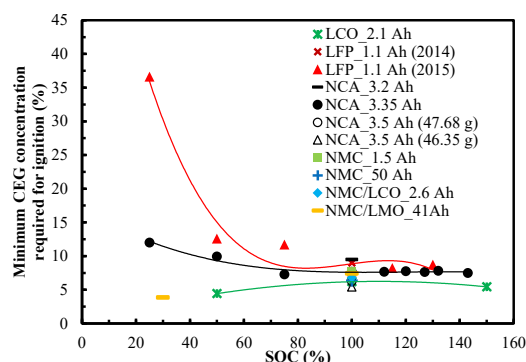
### Minimum CEG concentration required for ignition

Figure 3 shows the variation in  $c_{CEG, ignition}$  with the SOC for different types of cells. The calculation method of  $c_{CEG, ignition}$  is shown in the supplemental information section. It decreases with an increase in the SOC for the LFP\_1.1 Ah (2015) cell at the discharged state, especially when the SOC is below 50%. This shows that the probability of fire increases with the SOC value. Also,  $c_{CEG, ignition}$  remains almost unchanged at the full and overcharged stages. However, from the discharged (25% SOC) to the fully charged (100% SOC) to the overcharged (130% SOC) stages, it successively decreases by 79.0% and increases by 13.0%.

Compared with  $c_{CEG, ignition}$  for the LFP\_1.1 Ah (2015) cell,  $c_{CEG, ignition}$  for the NCA\_3.35 Ah (2015) cell has a similar variety trend with an increase in the SOC. From the discharged (25% SOC) to the fully charged (100% SOC) to the overcharged (143% SOC) stages, it successively decreases by 35.8% and increases by 2.6%.

For the LCO\_2.1 Ah cell,  $c_{CEG, ignition}$  first increases and then slightly decreases with an increase in the SOC. From the discharged (25% SOC) to the fully charged (100% SOC) to the overcharged (143% SOC) stages, it successively increases by 40.9% and decreases by 12.9%.





**Figure 3.** Variations in the minimum CEG concentration required for ignition vs. SOC

Thus, for these three types of cells, at the same SOC, the LFP\_1.1 Ah (2015) cell requires the highest  $c_{\text{CEG, ignition}}$ , followed by the NCA\_3.35 Ah (2015) cell and then the LCO\_2.1 Ah cell. It successively decreases by 21.4% and 55.6% at the discharged state (50% SOC). Then, it successively decreases by 0.8% and 19.5% at the fully charged state (100% SOC). This shows that when the other fire conditions are the same, the LFP\_1.1 Ah (2015) cell has the lowest fire possibility, followed by the NCA\_3.35 Ah (2015) cell and then the LCO\_2.1 Ah cell.

Table 3 shows the range of  $c_{\text{CEG, ignition}}$  under different charging states. The respective  $c_{\text{CEG, ignition}}$  for the LCO, LFP, NCA, and NMC cells is 4.4%, 11.7%–36.3%, 7.3%–12.0%, and 3.9% when not fully charged and 6.2%, 7.7%, 5.4%–9.5%, and 6.4%–7.7% for the case of being fully charged, respectively. When LCO, LFP and NCA are overcharged, the values are 5.4%, 8.2%–8.7%, and 7.5%–7.9%, respectively. Overall, the  $c_{\text{CEG, ignition}}$  for the LCO, LFP, NCA, and NMC cells is 4.4%–6.2%, 7.7%–36.6%, 5.4%–12.0%, and 3.9%–3.9%, respectively. The  $c_{\text{CEG, ignition}}$  for the LFP cell is highest, followed by the NCA and LCO cells and then the NMC cell, as shown in Figure 4. This shows that the fire probability for these types of cells successively increases and that the difficulty of their fire suppression by controlling the CEG concentration also successively increases.

The above analysis results show that by controlling the SOC and/or selecting a reasonable cell type, the  $c_{\text{CEG, ignition}}$  of a cell can be changed, thereby changing the probability of battery fire.

### Minimum $\text{O}_2$ concentration required for ignition

Figure 5 shows the variation in  $c_{\text{O}_2, \text{ ignition}}$  with the SOC for different types of cells. The calculation method of  $c_{\text{O}_2, \text{ ignition}}$  is shown in the supplemental information section. For the LFP\_1.1 Ah (2015) cell, as the SOC value increases, it does not significantly change. From the discharged (25% SOC) to the fully charged (100% SOC) to the overcharged (130% SOC) stages, it successively increases by 8.5% and decreases by 5.9%.

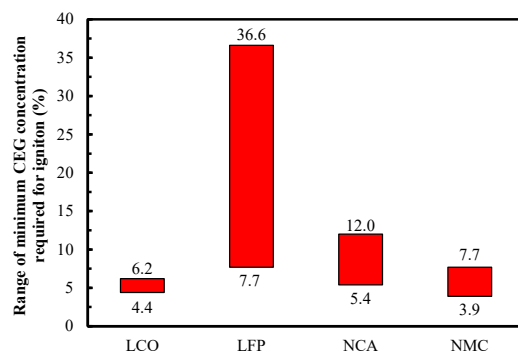
For the NCA\_3.35 Ah (2015) cell, as the SOC value increases,  $c_{\text{O}_2, \text{ ignition}}$  decreases at the discharged state but remains almost unchanged at the fully charged and overcharged stages. From the discharged (25% SOC) to the fully charged (100% SOC) to the overcharged (143% SOC) stages, it successively decreases by 16.4% and increases by 1.1%.

The LCO\_2.1 Ah cell has a similar trend to that of the NCA\_3.35 Ah (2015) cell. From the discharged (50% SOC) to the fully charged (100% SOC) to the overcharged (150% SOC) stages,  $c_{\text{O}_2, \text{ ignition}}$  successively decreases by 13.4% and increases by 1.6%.

**Table 3.** Minimum CEG concentration required for ignition for different cell types.

Chemistry	Not fully charged	Fully charged	Overcharged	Range
LCO	4.4	6.2	5.4	4.4–6.2
LFP	11.7–36.6	7.7	8.2–8.7	7.7–36.6
NA	7.3–12.0	5.4–9.5	7.5–7.9	5.4–12.0
NMC	3.9	6.4–7.7	–	3.9–7.7





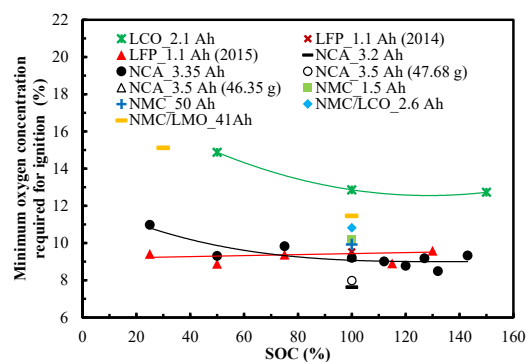
**Figure 4. Variations in the range of the minimum CEG concentration required for ignition vs. cell type**

For these three types of cells, at the same SOC, the LCO\_2.1 Ah cell requires higher  $c_{O_2, \text{ignition}}$  than that of the other two cell types. For the same SOC value, the NCA\_3.35 Ah (2015) cell requires higher  $c_{O_2, \text{ignition}}$  than that of the LFP\_1.1 Ah (2015) cell at the discharged state. However, there is no obvious difference in  $c_{O_2, \text{ignition}}$  at the fully and overcharged states for these two cells. From the LCO\_2.1 Ah cell to the NCA\_3.35 Ah (2015) cell to the LFP\_1.1 Ah (2015) cell,  $c_{O_2, \text{ignition}}$  successively decreases by 37.6% and 4.3% at the discharged state (50% SOC) and successively decreases by 30.2% and increases by 10.9% at the fully charged state (100% SOC), respectively. This shows that when the other fire conditions are the same, the LCO\_2.1 Ah cell has the lowest fire possibility among these three types of cells.

Table 4 shows the range of  $c_{O_2, \text{ignition}}$  under different charging states. For the LCO, LFP, NCA, and NMC cells, the respective values are 14.9%, 8.9%–9.4%, 9.3%–11.0%, and 15.1% for the case of being not fully charged and 12.9%, 10.2%, 7.6%–9.3%, and 10.0%–11.5% when fully charged, respectively. For the overcharged LCO, LFP, NCA cells, the values are 12.7%, 8.9%–9.6%, and 8.5%–9.3%, respectively. In general,  $c_{O_2, \text{ignition}}$  for the LCO, LFP, NCA, and NMC cells is 12.7%–14.9%, 8.9%–10.2%, 7.6%–11.0%, and 10.0%–15.1%, respectively. Thus, the LCO cell requires the highest  $c_{O_2, \text{ignition}}$  to ignite, followed by the NMC and LFP cells and then NCA cell, as shown in Figure 6. This shows that the fire hazard of these types of cells increases in turn and that the difficulty of their fire suppression by controlling the  $O_2$  concentration also successively increases.

The above analysis results show that by controlling the SOC and/or selecting a reasonable cell type, the  $c_{O_2, \text{ignition}}$  of the cell can be changed, thereby changing the probability of battery fire.

It should be noted that the results of evaluating the cell safety based on  $c_{CEG, \text{ignition}}$  and  $c_{O_2, \text{ignition}}$  are different. Based on the former, the order of safety from high to low is LFP > NCA > LCO > NMC. Based on the latter, the order of safety from high to low is LCO > NMC > LFP > NCA. This shows that a cell should be selected based on its application; for different types of cells, different fire prevention and control strategies should be selected.



**Figure 5. Variations in the minimum oxygen concentration required for ignition vs. SOC**

**Table 4. Minimum oxygen concentration required for ignition for different types of cells.**

Chemistry	Not fully charged	Fully charged	Overcharged	Range
LCO	14.9	12.9	12.7	12.7–14.9
LFP	8.9–9.4	10.2	8.9–9.6	8.9–10.2
NA	9.3–11.0	7.6–9.3	8.5–9.3	7.6–11.0
NMC	15.1	10.0–11.5	–	10.0–15.1

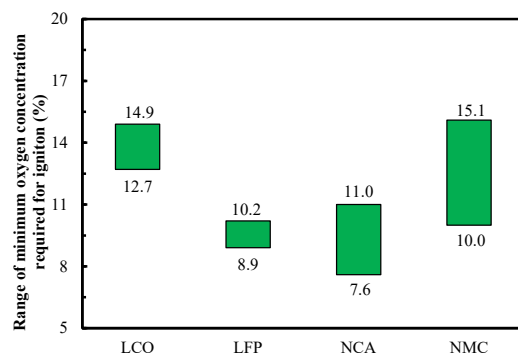
The higher the  $c_{\text{CEG, ignition}}$ , the easier it is to suppress battery fire by controlling the CEG concentration. The same case applies for  $c_{\text{O}_2, \text{ ignition}}$ . For example,  $c_{\text{CEG, ignition}}$  for NMC cells is relatively low, while  $c_{\text{O}_2, \text{ ignition}}$  is relatively high. This shows that to suppress NMC battery ignition, it is easier to control the  $\text{O}_2$  concentration than to control the CEG concentration. From the perspectives of  $c_{\text{CEG, ignition}}$  and  $c_{\text{O}_2, \text{ ignition}}$  for four different types of cells, to achieve fire suppression, it is recommended to control the CEG concentration for the LFP and NCA cells and the  $\text{O}_2$  concentration for the LCO and NMC cells.

However, actual scenarios should also be considered to select appropriate control methods. For example, for the inside of a closed battery box, the CEG and  $\text{O}_2$  concentrations can be reduced by filling incombustible gas or the  $\text{O}_2$  concentration can be reduced by reducing the internal pack space (after a cell erupts). It is difficult to control the  $\text{O}_2$  concentration in the atmosphere, so it should be mixed with incombustible gas before CEGs are released and reduced to a value below  $c_{\text{CEG, ignition}}$  to avoid fires.

Notably, because  $c_{\text{O}_2, \text{ ignition}}$  refers to the concentration of  $\text{O}_2$  in the CEG-air mixture, it is lower than the  $\text{O}_2$  content in the air (21%). In an open environment, sufficient air will continuously dilute the flammable CEG and can easily meet the  $\text{O}_2$  concentration boundary (Xu and Hui, 2017; Bi et al., 2015; Turns and Haworth, 2021). Therefore, if all other fire conditions are met, a fire will occur in an open environment. However, this does not mean that all CEGs will ignite in air because some CEGs are nonflammable (test 5 and 13 shown in Table 2 and Figure 1). In a closed environment, such as inside a battery box or a closed battery transport space, it is easier to control the  $\text{O}_2$  content. The  $\text{O}_2$  concentration boundary can be broken by reducing the amount of air by lowering the pressure, reducing the volume, and filling with inert gas to avoid the occurrence of fire (Li et al., 2019b; Turns and Haworth, 2021; Chen et al., 2017; Xie et al., 2020; Dong et al., 2019).

### Minimum ignition temperature required for ignition

Table 5 shows the main components of CEGs in open literature (Zhang et al., 2019; Somandepalli et al., 2014; Golubkov et al., 2014, 2015; Golubkov et al., 2014; Essl et al., 2020). In addition to  $\text{CO}_2$ ,  $\text{H}_2\text{O}$ , and  $\text{O}_2$ , 33 flammable substances have been found so far, such as  $\text{CO}$ ,  $\text{H}_2$ , alkane, alkene, alkyne, aromatic HC, electrolyte, etc. Based on the substances marked with \*, the ignition mode and  $T_{\text{ignition}}$  of cells were analyzed in this section.


**Figure 6. Variations of the range of the minimum  $\text{O}_2$  concentration required for ignition vs. cell type**

**Table 5. Main components of CEGs found in open literature**

Category	No.	Name	Formular	Essl et al. (2020)	Zhang et al. (2019)	Lammer et al. (2017)	Golubkov et al. (2015)	Golubkov et al. (2014)	Somandepalli et al. (2014)
Non-HC	1	Carbon dioxide	CO <sub>2</sub>	✓	✓	✓	✓	✓	✓
	2	Carbon monoxide	CO	✓	✓*	✓	✓	✓	✓
	3	Hydrogen	H <sub>2</sub>	✓	✓*	✓	✓	✓	✓
Alkane	4	Methane	CH <sub>4</sub>	✓	✓*	✓	✓	✓	✓
	5	Ethane	C <sub>2</sub> H <sub>6</sub>	✓	✓*	✓	✓	✓	✓
	6	Propane	C <sub>3</sub> H <sub>8</sub>	✓	✓*				✓
	7	n-Butane	C <sub>4</sub> H <sub>10</sub>	✓	✓*				✓
	8	Isobutane	C <sub>4</sub> H <sub>10</sub>						✓
	9	n-Pentane	C <sub>5</sub> H <sub>12</sub>		✓*				✓
	10	Isopentane	C <sub>5</sub> H <sub>12</sub>						✓
Alkene	11	Ethylene	C <sub>2</sub> H <sub>4</sub>	✓	✓*	✓	✓	✓	✓
	12	Propylene	C <sub>3</sub> H <sub>6</sub>		✓*				
	13	1-Butylene	C <sub>4</sub> H <sub>8</sub>		✓*				✓#
	14	2-Methyl propene	C <sub>4</sub> H <sub>8</sub>		✓				✓#
	15	trans-2-Butene	C <sub>4</sub> H <sub>8</sub>		✓				✓#
	16	cis-2-Butene	C <sub>4</sub> H <sub>8</sub>		✓				✓#
	17	1-Pentene	C <sub>5</sub> H <sub>10</sub>		✓*				
	18	cis-2-Pentene	C <sub>5</sub> H <sub>10</sub>		✓				
	19	trans-2-Pentene	C <sub>5</sub> H <sub>10</sub>		✓				
	20	2-Methyl-1-butene	C <sub>5</sub> H <sub>10</sub>		✓				
	21	2-Methyl-2-butene	C <sub>5</sub> H <sub>10</sub>		✓				
	22	3-Methyl-1-butene	C <sub>5</sub> H <sub>10</sub>		✓				
	23	2-Methyl-1-pentene	C <sub>6</sub> H <sub>12</sub>		✓*				
Alkyne	24	Ethyne	C <sub>2</sub> H <sub>2</sub>	✓	✓*	✓			
	25	Propyne	C <sub>3</sub> H <sub>4</sub>		✓*				✓
	26	1,3-Butadiene	C <sub>4</sub> H <sub>6</sub>		✓*				
Aromatic HC	27	Benzene	C <sub>6</sub> H <sub>6</sub>		✓*				✓
	28	Methylbenzene	C <sub>7</sub> H <sub>8</sub>						✓*
	29	Ethylbenzene	C <sub>8</sub> H <sub>10</sub>						✓*
	30	m & p-xylene	C <sub>8</sub> H <sub>10</sub>						✓
Electrolyte	31	DMC	C <sub>3</sub> H <sub>6</sub> O <sub>3</sub>		✓*				
	32	EMC	C <sub>4</sub> H <sub>8</sub> O <sub>3</sub>		✓*				
	33	DEC	C <sub>5</sub> H <sub>10</sub> O <sub>3</sub>	✓	✓*				

(Continued on next page)

Table 5. Continued

Category	No.	Name	Formular	Essl et al. (2020)	Zhang et al. (2019)	Lammer et al. (2017)	Golubkov et al. (2015)	Golubkov et al. (2014)	Somandepalli et al. (2014)
Others	34	2,4-Dimethyl-1-heptene	C <sub>9</sub> H <sub>18</sub>		√*				
	35	Oxidane	H <sub>2</sub> O	√	√				
	36	Hydrogen chloride	HCl		√				
	37	Oxygen	O <sub>2</sub>	√					

\* Substance was used to analyze the temperature boundary and ignition mode.

# The type of isomer cannot be determined.

For more information, refer to Essl et al. (2020); Zhang et al. (2019); Golubkov et al. (2014, 2015); and Somandepalli et al. (2014).

According to thermal ignition theory, the ignition of CEG is divided into forced ignition and autoignition, as shown in Table 6. Forced ignition signifies that the CEG is heated locally by forced ignition sources, and the local CEG ignites first. Then, the produced flame spreads from the ignition zone to the others. A forced ignition source often has high temperature. Common forced ignition sources include sparks, hot spots, and flames, as shown in Table 6. The electrification of automobiles creates conditions for the generation of electric sparks, and the maximum temperature of electric sparks can be close to 10,000°C. The minimum temperature required for a substance to be forced to ignite is defined as the forced ignition point ( $T_{\text{forced-ignition}}$ ).

Autoignition signifies that all CEGs are heated by autoignition sources and then ignite. An autoignition source does not require a high temperature but needs to have enough energy to heat the CEG. According to the energy source, autoignition sources are divided into self-heating and nonself-heating sources, as shown in Table 6. The main difference between a nonself-heating source and a forced ignition source is whether the ignition source is in direct contact with combustibles, and whether it can increase the temperature of the overall combustibles. The lowest temperature required for a substance to spontaneously ignite without forced ignition sources is defined as the autoignition point ( $T_{\text{autoignition}}$ ).

Forced ignition and autoignition are essentially the same. After heat accumulates to a certain extent, the chemical reaction rate is automatically and continuously accelerated until a higher chemical reaction rate is reached. The main difference is that the former is local heating, and the latter is overall heating. To facilitate the analysis, the following assumptions were made:

- $T_{\text{forced-ignition}}$  is usually 5°C–20°C higher than the flash point ( $T_{\text{flash}}$ , the minimum temperature required for a substance to flash), but the  $T_{\text{forced-ignition}}$  data are incomplete and are related mainly to testing methods and boundaries. Therefore,  $T_{\text{flash}}$  is used to measure the  $T_{\text{forced-ignition}}$  of CEG components.
- The influences of the pressure and temperature inside a cell on the physical and chemical properties of the CEG components were not considered.
- The cell jet area temperature was used to represent the CEG temperature during eruption.
- For the convenience of analysis, it was considered that the CEG temperature, i.e.,  $T_{\text{eruption}}$ , is about 350°C (Zhang et al., 2019) and that the ambient temperature ( $T_{\text{ambient}}$ ) is ~25°C.

When there is a forced ignition source, the temperature boundary is  $T_{\text{flash}}$ . That is, when the CEG temperature exceeds  $T_{\text{flash}}$ , the CEG may be forced ignited. Figure 7 shows the  $T_{\text{flash}}$  of the CEG main components. As the number of carbon atoms increases,  $T_{\text{flash}}$  increases for alkanes (carbon atoms fewer than 6), alkenes (carbon atoms less than 7), and aromatic hydrocarbons (carbon atoms fewer than 9), but it decreases for alkynes (carbon atoms fewer than 5). The  $T_{\text{flash}}$  values of the three electrolytes are not significantly different. Among the detected substances, the substance with the lowest  $T_{\text{flash}}$  is CH<sub>4</sub>, which is

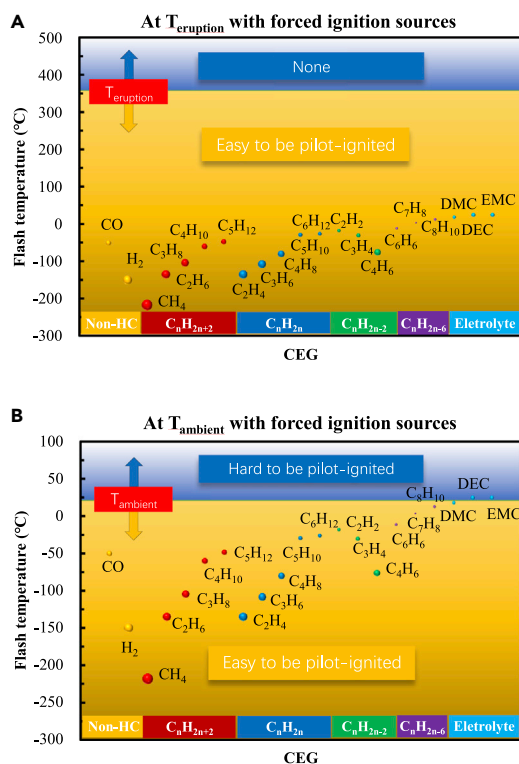
**Table 6. Ignition source and its temperature**

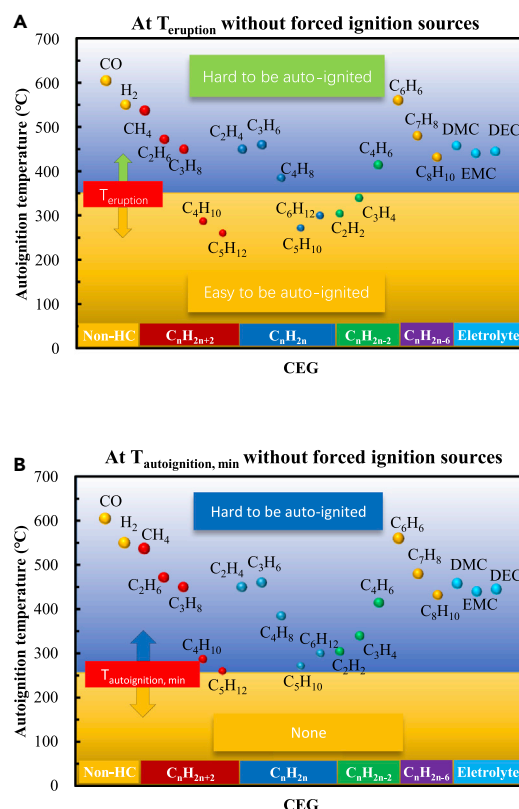
Definition		Ignition source		$T_{\text{Ignition source}}$ °C
Forced ignition	The CEG is heated locally by forced ignitions, and the local CEG ignites first, and then, the flame spreads to the others. Forced ignition sources often have high temperatures.	Spark	(1) Electric spark caused by too small electric clearance between conductive parts	3000–6000
			(2) Electric arc caused by lots of sparks	8700–9700
			(3) Static electric spark caused by invalid equipotential bonding	–
			(4) Mechanical spark caused by friction between the eruption flow and the wall	~1200
			(5) Spark from the ICE pipe	600–800
		Hot spot	(6) High temperature surface of the cell	~1000
			(7) High temperature cable with short circuit or overcurrent	–
		Flame	(8) Cigarette butts	250–800
			(9) Gas flame	1600–2100
			(10) Gasoline flame	~1200
			(11) Match flame	500–650
Autoignition	The CEG is heated whole by autoignition sources and then ignites. The autoignition source does not need to have a high temperature but needs to have enough energy to heat the CEG.	Self-heating	(1) Heats from the chemical reactions during the generating process of CEGs	200–1000
			(2) Heats from slow chemical reactions of CEGs caused by lighting, catalytic reactions by cathode materials, etc.	–
		Non-self-heating	(3) Heats from high temperature autoignition sources often with indirect contact with the CEG, such as the high temperature surface of a cell with thermal runaway, the high temperature surface of the ICE of another vehicle, a heater, etc. They can make the temperature of all the CEG be increased.	–
			(4) An energy source that converts other forms of energy into heat, such as friction, compression, etc.	–

around  $-200^{\circ}\text{C}$ , and the substance with the highest  $T_{\text{flash}}$  is the electrolyte, which is higher than  $0^{\circ}\text{C}$ . When there is a forced ignition source, there are two typical situations:

- When a cell erupts, the CEG is easily ignited if other ignition boundaries are available, as shown in [Figure 7A](#), because the  $T_{\text{flash}}$  values of all of the substances are lower than  $T_{\text{eruption}}$  (about  $350^{\circ}\text{C}$  ([Zhang et al., 2019](#))).
- If the CEG is cooled to  $T_{\text{ambient}}$ , substances with  $T_{\text{flash}}$  lower than  $T_{\text{ambient}}$  can easily ignite. Among the CEG components, CO, hydrogen, small molecular alkanes, small molecular olefins, and other substances generally have a flash point lower than the  $T_{\text{ambient}}$  (about  $25^{\circ}\text{C}$ ), so they are easily ignited first. The electrolyte, macromolecular alkanes, macromolecular alkenes, small molecular alkynes, benzene, and other substances may have a higher flash point than  $T_{\text{ambient}}$  (e.g., cold winter), so these substances may be ignited by the other substances that were already ignited first, as shown in [Figure 7B](#).

When there is no forced ignition source, the temperature boundary is  $T_{\text{autoignition}}$ . That is, when the fuel temperature exceeds  $T_{\text{auto-ignition}}$ , CEGs may be autoignited. [Figure 8](#) shows the  $T_{\text{autoignition}}$  of the main





**Figure 8. Autoignition temperatures of the main CEG components**

When there is no forced ignition source, the temperature boundary is  $T_{autoignition}$ . That is, when the fuel temperature exceeds  $T_{autoignition}$ , CEG may be autoignited.

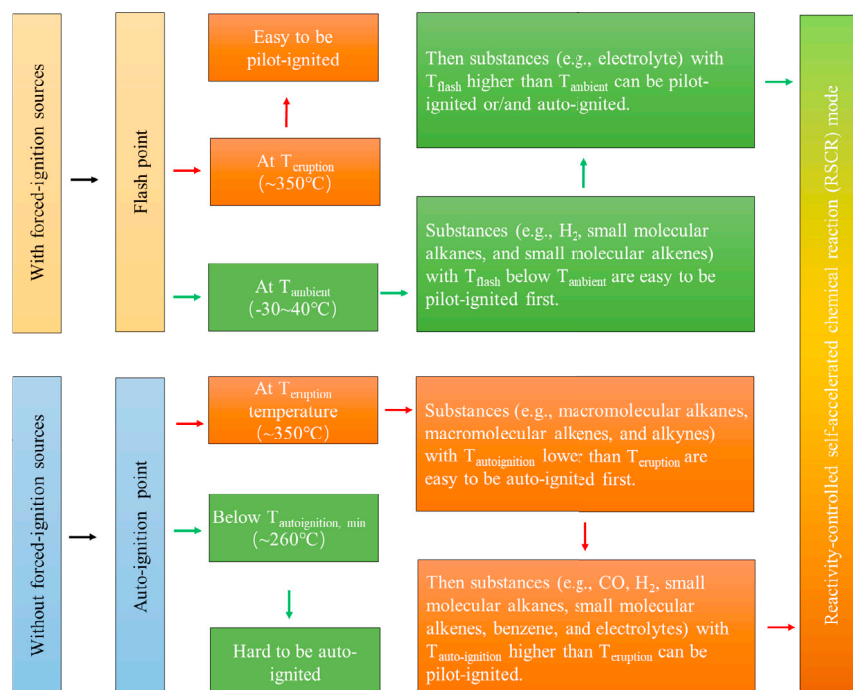
(A) When a cell erupts, the substances with  $T_{autoignition}$  lower than  $T_{eruption}$  are easy to autoignite first, and then, they ignite the substances with  $T_{autoignition}$  higher than  $T_{eruption}$ .

(B) If the CEGs are cooled below  $T_{autoignition, min}$  of  $\sim 260^{\circ}\text{C}$ , autoignition will not occur.

as  $\text{C}_5\text{H}_{12}$ , and  $\text{C}_5\text{H}_{10}$ , have low concentrations. However, according to the thermal ignition theory, even a relatively small amount of a substance can play a leading role in the ignition process. For example, the ignition of a premixed main charge containing gaseous fuel (more than 98% of the total fuel energy) occurs through direct injection of a small amount of diesel fuel (usually 0.5 to 2% of the total fuel energy) in a micro-pilot dual-fuel engine (Park et al., 2021). Diesel is a complex mixture of hydrocarbons containing 10–22 carbon atoms, and its  $T_{autoignition}$  is  $254^{\circ}\text{C}$ – $285^{\circ}\text{C}$ . Gases having a high  $T_{autoignition}$  include NG, which contains mainly  $\text{CH}_4$ ,  $\text{C}_2\text{H}_6$ ,  $\text{C}_3\text{H}_8$ ,  $\text{C}_4\text{H}_{10}$ ,  $\text{N}_2$ , and  $\text{CO}_2$ ; biogas, which contains mainly  $\text{CO}$ ,  $\text{CO}_2$ ,  $\text{CH}_4$ , and  $\text{H}_2$ ;  $\text{H}_2$ ; and others. This ignition process is strongly similar to that of the CET. Therefore, the analysis of autoignition in this study has certain reference value for evaluating the temperature boundary of the CEG. In particular, to leave a safe interval in the design target temperature to avoid fire, it is meaningful to use the lowest  $T_{ignition}$  among the CEG components to evaluate the  $T_{ignition}$  of the CEG.

In short, when there is a forced ignition source, CEGs are prone to ignite regardless of the temperature, and the substances with a low  $T_{flash}$  (e.g.,  $\text{CO}$ , hydrogen, small molecular alkanes, and small molecular olefins) play a leading role in the ignition process. When there are no forced ignition sources, CEGs are prone to autoignition at the  $T_{eruption}$ , and the substances with a low  $T_{autoignition}$  (e.g., macromolecular alkanes, macromolecular alkenes, and small molecular alkynes) play a leading role in the ignition process. If the CEG temperature is cooled below the  $T_{autoignition, min}$ , autoignition will not occur. Therefore, the ignition process of a cell belongs to the self-accelerating reaction mode, which is controlled by the reaction activity, as shown in Figure 9. The CEG ignition mode can be controlled by changing the CEG temperature and ignition sources, i.e., reactivity-controlled self-accelerated chemical reaction mode (Li et al., 2019a).





**Figure 9. CEG ignition mode**

The ignition process of a cell belongs to the self-accelerating reaction mode, which is controlled by the reaction activity.

### Significance of this research

The research results of this paper can provide guidance for cell selection, battery pack design, and safety design.

- According to  $c_{\text{CEG, ignition}}$  and/or  $\text{CO}_2$ , ignition, the following questions can be answered. Which cell type is safer? What is the right SOC value for cell storage? What is the CEG/ $\text{O}_2$  concentration value above which there is a possibility of fire? How much inert gases should be filled in a battery pack to ensure it does not ignite after eruption? How many cells experiencing thermal runaway can make the  $\text{O}_2$  concentration below  $\text{CO}_2$ , ignition by consuming the  $\text{O}_2$  inside a battery pack?
- The research results related to  $T_{\text{ignition}}$  point out the importance of controlling the sources of forced ignition. They also show that when there are no ignition sources, the CEG temperature can be lowered to the  $T_{\text{auto-ignition}}$  (~260°C) to avoid fires, providing a reference for thermal management design. In addition, the relevant results of this part also indicate the ignition mode of CEGs, laying a foundation for further research on related mechanisms.

The above results are only the most important ones. In short, through the analysis of the three fire boundaries, the occurrence of fire can be avoided when any one of the boundaries is avoided. According to the research results of this paper, a variety of solutions can be designed to avoid the occurrence of fire.

### Conclusions

In this study, the three fire boundaries, which are  $c_{\text{CEG, ignition}}$ ,  $\text{CO}_2$ , ignition, and  $T_{\text{ignition}}$ , were theoretically analyzed based on the CEG identification results of 29 thermal runaway tests in inert atmosphere. The main conclusions were summarized as follows:

- $c_{\text{CEG, ignition}}$  decreases and then remains almost unchanged with the increase in SOC for the LFP\_1.1 Ah (2015) and the NCA\_3.35 Ah (2015) cells. For the LCO\_2.1 Ah cell, with the increase in the SOC,  $c_{\text{CEG, ignition}}$  first increases and then decreases. The respective values of  $c_{\text{CEG, ignition}}$  for the LCO, LFP, NCA, and NMC cells are 4.4%–6.2%, 7.7%–36.6%, 5.4%–12.0%, and 3.9%–3.9%, respectively, which indicates that the order of  $c_{\text{CEG, ignition}}$  from high to low is LFP > NCA > LCO > NMC.

- (2)  $c_{O_2, \text{ignition}}$  does not significantly change for the LFP\_1.1 Ah (2015) cell with the increase in the SOC. It decreases at the discharged stage but remains almost unchanged at the fully and overcharged stages for both NCA\_3.35 Ah (2015) and LCO\_2.1 Ah cells. The respective values of  $c_{O_2, \text{ignition}}$  for the LCO, LFP, NCA, and NMC cells are 12.7%–14.9%, 8.9%–10.2%, 7.6%–11.0%, and 10.0%–15.1%, respectively, which indicates that the order of  $c_{O_2, \text{ignition}}$  from high to low is LCO > NMC > LFP > NCA.
- (3) When there is a forced ignition source, CEGs are prone to ignite regardless of the CEG temperature, and the substances with low  $T_{\text{flash}}$  play a leading role in the ignition process. When there are no forced ignition sources, CEGs are prone to autoignite at  $T_{\text{eruption}}$ , and the substances with low  $T_{\text{autoignition}}$  play a leading role in the ignition process. When the CEG temperature is cooled below  $T_{\text{auto-ignition}}$  ( $\sim 260^\circ\text{C}$ ) of the CEG components, autoignition does not occur. The CEG ignition mode can be controlled by changing the CEG temperature and ignition sources.

### Limitations of the study

The release process of cell gas is a dynamic process, which is not considered in this study. In further research, the dynamic process of the cell fire boundary can be analyzed by computational fluid dynamics.

### Resource availability

#### Lead contact

Further information and requests should be directed to and will be fulfilled by the lead contact, Zhenhai Gao (gaozh@jlu.edu.cn).

#### Materials availability

This study did not generate any new materials.

### Data and code availability

Any data utilized in this study can be found in the main manuscript and supplemental information.

## METHODS

All methods can be found in the accompanying [transparent methods supplemental file](#).

## SUPPLEMENTAL INFORMATION

Supplemental information can be found online at <https://doi.org/10.1016/j.isci.2021.102401>.

## ACKNOWLEDGMENTS

This research was supported by the Ministry of Science and Technology of the People's Republic of China under the grant no. 2019YFE0100200, the Major Science and Technology Projects in Jilin Province under the grant no. 20200501012GX, the National Natural Science Foundation of China (52003012), and the China Postdoctoral Science Foundation (2019M660401).

## AUTHOR CONTRIBUTIONS

Conceptualization, Z.G., Y.C., M.O., and W.L.; writing – original draft, W.L., S.R., and Y.X.; writing – review & editing, W.L., S.R., Y.X., Z.G., Y.C., H.W., and M.O.; supervision, Z.G., Y.C., and M.O.; All authors discussed the results and contributed to the manuscript.

## DECLARATION OF INTERESTS

The authors declare no competing interests.

Received: February 10, 2021

Revised: March 17, 2021

Accepted: April 5, 2021

Published: May 21, 2021

## REFERENCES

- Agubra, V.A., and Fergus, J.W. (2014). The formation and stability of the solid electrolyte interface on the graphite anode. *J. Power Sources* 268, 153–162, <https://doi.org/10.1016/j.jpowsour.2014.06.024>.
- Andersson, A.M., and Edström, K. (2001). Chemical composition and morphology of the elevated temperature SEI on graphite. *J. Electrochem. Soc.* 148, A1100–A1109, <https://doi.org/10.1149/1.1397771>.
- Aurbach, D., Markovsky, B., Weissman, I., Levi, E., and Ein-Eli, Y. (1999). On the correlation between surface chemistry and performance of graphite negative electrodes for Li ion batteries. *Electrochim. Acta* 45, 67–86, [https://doi.org/10.1016/S0013-4686\(99\)00194-2](https://doi.org/10.1016/S0013-4686(99)00194-2).
- Aurbach, D., Zaban, A., Ein-Eli, Y., Weissman, I., Chusid, O., Markovsky, B., Levi, M., Levi, E., Schechter, A., and Granot, E. (1997). Recent studies on the correlation between surface chemistry, morphology, three-dimensional structures and performance of Li and Li-C intercalation anodes in several important electrolyte systems. *J. Power Sources* 68, 91–98, [https://doi.org/10.1016/S0378-7753\(97\)02575-5](https://doi.org/10.1016/S0378-7753(97)02575-5).
- Baird, A.R., Archibald, E.J., Marr, K.C., and Ezekoye, O.A. (2020). Explosion hazards from lithium-ion battery eruption gas. *J. Power Sources* 446, 227257, <https://doi.org/10.1016/j.jpowsour.2019.227257>.
- Bi, M., Ren, J., and Gao, W. (2015). *Fire Safety Engineering* (Chemical Industry Press).
- Biensan, P., Simon, B., Peres, J., Guibert, A.D., Broussely, M., Bodet, J., and Pertion, F. (1999). On safety of lithium-ion cells. *J. Power Sources* 81, 906–912, [https://doi.org/10.1016/S0378-7753\(99\)00135-4](https://doi.org/10.1016/S0378-7753(99)00135-4).
- Campion, C.L., Li, W., Euler, W.B., Lucht, B.L., Ravdel, B., DiCarlo, J.F., Gitzendanner, R., and Abraham, K.M. (2004). Suppression of toxic compounds produced in the decomposition of lithium-ion battery electrolytes. *Electrochem. Solid State Lett.* 7, A194–A197, <https://doi.org/10.1149/1.1738551>.
- Chen, M., Liu, J., He, Y., Yuen, R., and Wang, J. (2017). Study of the fire hazards of lithium-ion batteries at different pressures. *Appl. Therm. Eng.* 125, 1061–1074, <https://doi.org/10.1016/j.applthermaleng.2017.06.131>.
- Chen, S., Wang, Z., Wang, J., Tong, X., and Yan, W. (2020). Lower explosion limit of the vented gases from Li-ion batteries thermal runaway in high temperature condition. *J. Loss Prevent. Proc.* 63, 103992, <https://doi.org/10.1016/j.jlp.2019.103992>.
- Dahn, J.R., Fuller, E.W., Obrovac, M., and Sacken, U. (1994). Thermal stability of  $\text{Li}_x\text{CoO}_2$ ,  $\text{Li}_x\text{NiO}_2$  and  $\lambda\text{-MnO}_2$  and consequences for the safety of Li-ion cells. *Solid State Ion* 69, 265–270, [https://doi.org/10.1016/0167-2738\(94\)90415-4](https://doi.org/10.1016/0167-2738(94)90415-4).
- Dong, H., Zhang, S., Li, Y., Xian, X., Yi, C., Liu, L., Yu, D., Han, G., and Sheng, Y. (2019). Thermal runaway fire characteristics of lithium-ion batteries with high specific energy NCM811. *Energy Storage Sci. Technol.* 8, 65–70, <https://doi.org/10.19799/j.cnki.2095-4239.2019.0052>.
- EIA (2020). Global EV Outlook 2020. <https://www.iea.org/reports/global-ev-outlook-2020>.
- Essl, C., Golubkov, A.W., Gasser, E., Nachtnebel, M., Zankel, A., Ewert, E., and Fuchs, A. (2020). Comprehensive hazard analysis of failing automotive lithium-ion batteries in overtemperature experiments. *Batteries* 6, 30, <https://doi.org/10.3390/batteries6020030>.
- Fairweather, M., Hargrave, G.K., Ibrahim, S.S., and Walker, D.G. (1999). Studies of premixed flame propagation in explosion tubes. *Combust. Flame* 116, 504–518, [https://doi.org/10.1016/S0010-2180\(98\)00055-8](https://doi.org/10.1016/S0010-2180(98)00055-8).
- Finegan, D.P., Scheel, M., Robinson, J.B., Tjaden, B., Hunt, I., Mason, T.J., Millichamp, J., Michiel, M.D., Offer, G.J., Hinds, G., et al. (2015). In-operando high-speed tomography of lithium-ion batteries during thermal runaway. *Nat. Commun.* 6, 6924, <https://doi.org/10.1038/ncomms7924>.
- Fleischhammer, M., and Döring, H. (2013). Chemische sicherheit. In *Handbuch Lithium-Ionen-Batterien*, R. Korthauer, ed. (Springer Vieweg), pp. 285–298, [https://doi.org/10.1007/978-3-642-30653-2\\_23](https://doi.org/10.1007/978-3-642-30653-2_23).
- Gachot, G., Grugeon, S., Eshetu, G.G., Mathiron, D., Ribièrè, P., Armand, M., and Laruelle, S. (2012). Thermal behaviour of the lithiated-graphite/electrolyte interface through GC/MS analysis. *Electrochim. Acta* 83, 402–409, <https://doi.org/10.1016/j.electacta.2012.08.016>.
- Gachot, G., Ribièrè, P., Mathiron, D., Grugeon, S., Armand, M., Leriche, J.B., Pilard, S., and Laruelle, S. (2010). Gas chromatography/mass spectrometry as a suitable tool for the Li-ion battery electrolyte degradation mechanisms study. *Anal. Chem.* 83, 478–485, <https://doi.org/10.1021/ac101948u>.
- Garche, J., and Brandt, K. (2018). Electrochemical power sources: fundamentals, systems, and applications. Elsevier. <https://doi.org/10.1016/C2015-0-00574-3>.
- Gnanaraj, J.S., Zinigrad, E., Asraf, L., Gottlieb, H.E., Sprecher, M., Schmidt, M., Geissler, W., and Aurbach, D. (2003). A detailed investigation of the thermal reactions of  $\text{LiPF}_6$  solution in organic carbonates using ARC and DSC. *J. Electrochem. Soc.* 150, A1533–A1537, <https://doi.org/10.1149/1.1617301>.
- Golubkov, A.W., Fuchs, D., Wagner, J., Wilsche, H., Stangl, C., Fauler, G., Voitic, G., Thaler, A., and Hackere, V. (2014). Thermal-runaway experiments on consumer Li-ion batteries with metal-oxide and olivin-type Cathodes. *RSC Adv.* 4, 3633–3642, <https://doi.org/10.1039/C3RA45748F>.
- Golubkov, A.W., Scheikl, S., Planteu, R., Voitic, G., Wilsche, H., Stangl, C., Fauler, G., Thaler, A., and Hacker, V. (2015). Thermal runaway of commercial 18650 Li-ion batteries with LFP and NCA cathodes - impact of state of charge and overcharge. *RSC Adv.* 5, 57171–57186, <https://doi.org/10.1039/c5ra05897j>.
- Gourley, S.W., Or, T., and Chen, Z. (2020). Breaking free from cobalt reliance in lithium-ion batteries. *iScience* 23, 101505, <https://doi.org/10.1016/j.isci.2020.101505>.
- Guo, C., and Zhang, Q. (2016). Determination on explosion limit of venting gas released by lithium-ion battery and its risk analysis. *J. Saf. Sci. Technol.* 12, 46–49, <https://doi.org/10.11731/j.issn.1673-193x.2016.09.008>.
- Han, X., Lu, L., Zheng, Y., Feng, X., Li, Z., and Li, J. (2019). Ouyang, M. A review on the key issues of the LIB degradation around the whole life cycle. *eTransportation* 1, 100005, <https://doi.org/10.1016/j.etran.2019.100005>.
- Huang, Y., Lin, Y.C., Jenkins, D.M., Chernova, N.A., Chung, Y., Radhakrishnan, B., Chu, L., Fang, J., Wang, Q., Omenya, F., et al. (2016). Thermal stability and reactivity of cathode materials for Li-ion batteries. *ACS Appl. Mater. Interfaces* 8, 7013–7021, <https://doi.org/10.1021/acsami.5b12081>.
- Joachim, H., Kaun, T.D., Zaghib, K., and Prakash, J. (2009). Electrochemical and thermal studies of carbon-coated  $\text{LiFePO}_4$  cathode. *J. Electrochem. Soc.* 156, A401–A406, <https://doi.org/10.1149/1.3106121>.
- Kawamura, T., Okada, S., and Yamaki, J.I. (2006). Decomposition reaction of  $\text{LiPF}_6$ -based electrolytes for lithium-ion cells. *J. Power Sources* 156, 547–554, <https://doi.org/10.1016/j.jpowsour.2005.05.084>.
- Kocha, S., Fill, A., and Birke, K.P. (2018). Comprehensive gas analysis on large scale automotive lithium-ion cells in thermal runaway. *J. Power Sources* 398, 106–112, <https://doi.org/10.1016/j.jpowsour.2018.07.051>.
- Lammer, M., Königseder, A., and Hacker, V. (2017). Holistic methodology for characterization of the thermally induced failure of commercially available 18650 lithium-ion cells. *RSC Adv.* 7, 24425–24429, <https://doi.org/10.1039/C7RA02635H>.
- Li, J., Zhang, Z., Guo, X., and Yang, Y. (2006). The studies on structural and thermal properties of delithiated  $\text{Li}_x\text{Ni}_{1/3}\text{Co}_{1/3}\text{Mn}_{1/3}\text{O}_2$  ( $0 < x \leq 1$ ) as a cathode material on lithium-ion batteries. *Solid State Ion* 177, 1509–1516, <https://doi.org/10.1016/j.ssi.2006.03.055>.
- Li, W., Wang, H., Ouyang, M., Xu, C., Lu, L., and Feng, X. (2019a). Theoretical and experimental analysis of the lithium-ion battery thermal runaway process based on the internal combustion engine combustion theory. *Energ. Convers. Manage.* 185, 211–222, <https://doi.org/10.1016/j.enconman.2019.02.008>.
- Li, W., Wang, H., Zhang, Y., and Ouyang, M. (2019b). Flammability characteristics of the battery vent gas: a case of NCA and LFP lithium-ion batteries during external heating abuse. *J. Energy Storage* 24, 100775, <https://doi.org/10.1016/j.est.2019.100775>.
- Liu, B., Tan, Y., and Fu, Z. (2004). The determination of minimum oxygen density of combustible gases (Vapors). *J. Shijiazhuang Inst. Railway Eng.* 3, 35–38.
- Liu, K., Kong, B., Liu, W., Sun, Y., Song, M., Chen, J., Liu, Y., Lin, D., Pei, A., and Cui, Y. (2018). Stretchable lithium metal anode with improved mechanical and electrochemical cycling stability.

- Joule 2, 1857–1865, <https://doi.org/10.1016/j.joule.2018.06.003>.
- Long, B., Xu, R., and Liu, Y. (2014). Gas-flammability testing for Li-ion cells during abusing. *Battery* 44, 121–123.
- Maleki, H., Deng, G., Anani, A., and Howard, J. (1999). Thermal stability studies of Li-ion cells and components. *J. Electrochem. Soc.* 146 (9), 3224–3229, <https://doi.org/10.1149/1.1392458>.
- Mao, B., Chen, H., Cui, Z., Wu, T., and Wang, Q. (2018). Failure mechanism of the lithium-ion battery during nail penetration. *Int. J. Heat Mass Transf.* 122, 1103–1115, <https://doi.org/10.1016/j.ijheatmasstransfer.2018.02.036>.
- Martha, S.K., Haik, O., Zinigrad, E., Enxar, I., Drezen, T., Miners, J.H., and Aurbach, D. (2011). On the thermal stability of olivine cathode materials for lithium-ion batteries. *J. Electrochem. Soc.* 158, A1115–A1122, <https://doi.org/10.1149/1.3622849>.
- Mikolajczak, C., Kahn, M., White, K., and Long, R.T. (2011). *Lithium-ion Batteries Hazard and Use Assessment* (Springer).
- Onuki, M., Kinoshita, S., Sakata, Y., Yanagidate, M., Otake, Y., Ue, M., and Deguchi, M. (2008). Identification of the source of evolved gas in li-ion batteries using <sup>13</sup>C-labeled solvents. *J. Electrochem. Soc.* 155, A794–A797, <https://doi.org/10.1149/1.2969947>.
- Orendorff, C.J. (2012). The role of separators in lithium-ion cell safety. *Electrochem. Soc. Interfaces* 21, 61–65, <https://doi.org/10.1149/2.f07122if>.
- Park, H., Wright, Y., Seddik, O., Srna, A., Kyrtatos, P., and Boulouchos, K. (2021). Phenomenological micro-pilot ignition model for medium-speed dual-fuel engines. *Fuel* 285, 118955, <https://doi.org/10.1016/j.fuel.2020.118955>.
- Pasquier, A.D., Disma, F., Bowmer, T., Gozdz, A., Amatucci, G., and Tarascon, J.M. (1998). Differential scanning calorimetry study of the reactivity of carbon anodes in plastic li-ion batteries. *J. Electrochem. Soc.* 145, 472–477, <https://doi.org/10.1149/1.1838287>.
- Pfrang, A., Kriston, A., Rulz, V., Lebedeva, N., and Perslo, F. (2017). Safety of rechargeable energy storage systems with a focus on Li-ion technology. In *Emerging Nanotechnologies in Rechargeable Energy Storage Systems*, L.M. Rodriguez-Martinez, ed. (Elsevier), pp. 253–290, <https://doi.org/10.1016/B978-0-323-42977-1.00008-X>.
- Ravdel, B., Abraham, K.M., Gitzendanner, R., DiCarlo, J., Lucht, B., and Campion, C. (2003). Thermal stability of lithium-ion battery electrolytes. *J. Power Sources* 119–121, 805–810, [https://doi.org/10.1016/S0378-7753\(03\)00257-X](https://doi.org/10.1016/S0378-7753(03)00257-X).
- Ribiere, P., Grugeon, S., Morcrette, M., Boyanov, S., Laruelle, S., and Marlair, G. (2012). Investigation on the fire-induced hazards of Li-ion battery cells by fire calorimetry. *Energy Environ. Sci.* 5, 5271–5280, <https://doi.org/10.1039/C1EE02218K>.
- Richard, M.N., and Dahn, J.R. (1999). Accelerating rate calorimetry study on the thermal stability of lithium intercalated graphite in electrolyte I. experimental. *J. Electrochem. Soc.* 146, 2068–2077, [https://doi.org/10.1016/S0140-6701\(00\)96499-3](https://doi.org/10.1016/S0140-6701(00)96499-3).
- Rosha, P., Dhir, A., and Mohapatra, S. (2018). Influence of gaseous fuel induction on the various engine characteristics of a dual fuel compression ignition engine: a review. *Renew. Sust. Energ. Rev.* 82, 3333–3349, <https://doi.org/10.1016/j.rser.2017.10.055>.
- Roth, E., and Orendorff, C. (2012). How electrolytes influence battery safety. *Electrochem. Soc. Interfaces* 21 (2), 45–49, <https://doi.org/10.1149/2.F04122if>.
- Shin, J.S., Han, C.H., Jung, U.H., Lee, S.I., Kim, H.J., and Kim, K. (2002). Effect of Li<sub>2</sub>CO<sub>3</sub> additive on gas generation in lithium-ion batteries. *J. Power Sources* 109, 47–52, [https://doi.org/10.1016/S0378-7753\(02\)00039-3](https://doi.org/10.1016/S0378-7753(02)00039-3).
- Somandepalli, V., Marr, K., and Horn, Q. (2014). Quantification of combustion hazards of thermal runaway failures in lithium-ion batteries. *SAE Int. J. Alt. Power* 3, 98–104, <https://doi.org/10.4271/2014-01-1857>.
- Spotnitz, R., and Franklin, J. (2003). Abuse behavior of high-power lithium-ion cells. *J. Power Sources* 113 (1), 81–100, [https://doi.org/10.1016/S0378-7753\(02\)00488-3](https://doi.org/10.1016/S0378-7753(02)00488-3).
- Stephan, A., Anadon, L.D., and Hoffmann, V.H. (2021). How has external knowledge contributed to lithium-ion batteries for the energy transition? *iScience* 24, 101995, <https://doi.org/10.1016/j.isci.2020.101995>.
- Sun, P., Huang, X., Bisschop, R., and Niu, H. (2020). A review of battery fires in electric vehicles. *Fire Technol.* 56, 1361–1410, <https://doi.org/10.1007/s10694-020-00958-2>.
- Turns, S., and Haworth, D.C. (2021). *An Introduction to Combustion: Concepts and Applications* (Mc Graw Hill).
- Wang, H., Zhang, Y., Li, C., Li, W., and Ouyang, M. (2019a). Venting process of lithium-ion power battery during thermal runaway under medium state of charge. *Energ. Stor. Sci. Technol.* 8 (6), 1043–1048, <https://doi.org/10.10288/j.issn.2095-4239.2019.0057>.
- Wang, Q., Mao, B., Stoliarov, S.I., and Sun, J. (2019b). A review of lithium-ion battery failure mechanisms and fire prevention strategies. *Prog. Energ. Combust.* 73, 95–131, <https://doi.org/10.1016/j.pecs.2019.03.002>.
- Wang, Q., Ping, P., Zhao, X., Chu, G., Sun, J., and Chen, C. (2012). Thermal runaway caused fire and explosion of lithium-ion battery. *J. Power Sources* 208, 210–222, <https://doi.org/10.1016/j.jpowsour.2012.02.038>.
- Wang, Q., Sun, J., and Chen, C. (2007a). Thermal stability of delithiated LiMn<sub>2</sub>O<sub>4</sub> with electrolyte for lithium-ion batteries. *J. Electrochem. Soc.* 154, A263–A267, <https://doi.org/10.1149/1.2433698>.
- Wang, Y., Jiang, J., and Dahn, J. (2007b). The reactivity of delithiated Li (Ni<sub>1/3</sub>Co<sub>1/3</sub>Mn<sub>1/3</sub>)O<sub>2</sub>, Li (Ni<sub>0.8</sub>Co<sub>0.15</sub>Al<sub>0.05</sub>)O<sub>2</sub> or LiCoO<sub>2</sub> with non-aqueous electrolyte. *Electrochem. Commun.* 9, 2534–2540, <https://doi.org/10.1016/j.elecom.2007.07.033>.
- Wang, Q., Sun, J., Yao, X., and Chen, C. (2005). Thermal stability of LiPF<sub>6</sub>/EC+DEC electrolyte with charged electrodes for lithium-ion batteries. *Thermochim. Acta* 437, 12–16, <https://doi.org/10.1016/j.tca.2005.06.010>.
- Wang, Q., Sun, J., Yao, X., and Chen, C. (2006). Thermal behavior of lithiated graphite with electrolyte in lithium-ion batteries. *J. Electrochem. Soc.* 153, A329–A333, <https://doi.org/10.1149/1.2139955>.
- Watanabe, I., and Yamaki, J. (2006). Thermal gravimetry-mass spectrometry studies on the thermal stability of graphite anodes with electrolyte in lithium-ion battery. *J. Power Sources* 153, 402–404, <https://doi.org/10.1016/j.jpowsour.2005.05.027>.
- Xie, S., Sun, J., Chen, X., and He, Y. (2020). Thermal runaway behavior of lithium-ion batteries in different charging states under low pressure. *Int. J. Energy Res.* 1–11, <https://doi.org/10.1002/er.6200>.
- Xu, T., and Hui, S. (2017). *Combustion Science* (China machine press).
- Yang, H., Bang, H., Amine, K., and Prakash, J. (2005). Investigations of the exothermic reactions of natural graphite anode for li-ion batteries during thermal runaway. *J. Electrochem. Soc.* 152, A73–A79, <https://doi.org/10.1149/1.1836126>.
- Yoshida, H., Fukunaga, T., Hazama, T., Terasaki, M., Mizutani, M., and Yamachi, M. (1997). Degradation mechanism of alkyl carbonate solvents used in lithium-ion cells during initial charging. *J. Power Sources* 68, 311–315, [https://doi.org/10.1016/S0378-7753\(97\)02635-9](https://doi.org/10.1016/S0378-7753(97)02635-9).
- Zhang, Y., Wang, H., Li, W., and Li, C. (2019). Quantitative identification of emissions from abused prismatic Ni-rich lithium-ion batteries. *eTransportation* 2, 100031, <https://doi.org/10.1016/j.etrans.2019.100031>.
- Zhang, Y., Wang, H., Li, W., Li, C., and Ouyang, M. (2019). Size distribution and elemental component of vent particles from abused prismatic Ni-rich automotive lithium-ion batteries. *J. Energy Storage* 26, 100991, <https://doi.org/10.1016/j.est.2019.100991>.
- Zhang, Y., Wang, H., Li, W., Li, C., and Ouyang, M. (2020). Quantitative analysis of eruption process of abused prismatic Ni-rich automotive batteries based on in-chamber pressure. *J. Energy Storage* 31, 101617, <https://doi.org/10.1016/j.est.2020.101617>.
- Zhang, Z., Fouchard, D., and Rea, J. (1998). Differential scanning calorimetry material studies: implications for the safety of lithium-ion cells. *J. Power Sources* 70, 16–20, [https://doi.org/10.1016/S0140-6701\(98\)93827-9](https://doi.org/10.1016/S0140-6701(98)93827-9).
- Zhou, M., Zhao, L., Okada, S., and Yamaki, J. (2012). Quantitative studies on the influence of LiPF<sub>6</sub> on the thermal stability of graphite with electrolyte. *J. Electrochem. Soc.* 159, 44, <https://doi.org/10.1149/2.066201jes>.

## **Supplemental information**

### **Fire boundaries of lithium-ion cell eruption gases caused by thermal runaway**

**Weifeng Li, Shun Rao, Yang Xiao, Zhenhai Gao, Yupeng Chen, Hewu Wang, and Minggao Ouyang**

## Transparent Methods

### Calculation model of minimum CEG concentration required for ignition

The minimum CEG concentration required for ignition refers to the LFL of CEGs. When the CEG concentration is lower than a certain value, it is too lean to ignite. The calculation of  $c_{\text{CEG,ignition}}$ , i.e., LFL, is based on Le Chatelier's mixing rule (Chatelier, 1891; Mashuga et al, 2000), as shown in Equation 1.

$$c_{\text{CEG,ignition}} = \text{LFL} = \frac{1}{\sum_{i=1}^n \frac{x_i}{\text{LFL}_i}} \times 100\% \quad (\text{Equation 1})$$

where  $\text{LFL}_i$  refers to the LFL of component  $i$  in CEG, and  $x_i$  refers to the volume percentage of component  $i$  in CEG.

During the calculation, the inert gas in CEG is considered to get a more accurate value of the flammability limit (Li, 1998; Tian et al., 2006; Wu et al., 1994)

### Calculation model of minimum oxygen concentration required for ignition

The minimum  $\text{O}_2$  concentration required for ignition refers to the oxygen concentration in the CEG-air mixture at the UFL (i.e., the CEG concentration in the mixture), as shown in Equation 2. When the oxygen concentration is lower than this value, the oxygen is too lean to support ignition. UFL has a similar calculation method to that of LFL, as shown in Equation 2.

$$c_{\text{O}_2, \text{ignition}} = (1 - \text{UFL}) * c_{\text{O}_2 \text{ in air}} = \left(1 - \frac{1}{\sum_{i=1}^n \frac{x_i}{\text{UFL}_i}} \times 100\%\right) * c_{\text{O}_2 \text{ in air}} \quad (\text{Equation 2})$$

where  $c_{\text{O}_2 \text{ in air}}$  refers to the  $\text{O}_2$  volume percentage in air,  $\text{UFL}_i$  refers to the UFL of component  $i$  in CEG, and  $x_i$  refers to the volume percentage of component  $i$  in CEG.

### Supplemental References

Chatelier, L. (1891). Estimation of Firedamp by Flammability Limits (Annals of mines).

Li, D. (1988). Calculation of explosive concentration limit of flammable gas. Chem. Des. Commun. 14, 63-65.

Mashuga, C.V., and Crowl, D.A. (2000). Derivation of Le Chatelier's mixing rule for flammable limits. Process Saf. Prog. 19, 112–117.

Tian, G., Yu, C., and Li, X. Study on calculation on method of gas explosion limits, Gas Heat 26 (2006) 29-33.

Wu, J., Kong, Q., and Wang, B. (1994). Theoretical calculation method for the explosion limit of mixed gas. Oil Gas Storage Trans.13, 10-12.