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Non-isothermal crosslinking of ethylene vinyl acetate initiated by crosslinking agents: kinetic modelling†

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The non-isothermal crosslinking process of ethylene vinyl acetate (EVA) initiated by several crosslinking agents was studied by using differential scanning calorimetry (DSC). The crosslinking agent *tert*-butylperoxy 2-ethylhexyl carbonate (TBEC) exhibited much shorter reaction time and lower reaction temperature. The effect of the crosslinking agent TBEC on the EVA crosslinking process was further analyzed by using Avrami, Ozawa, Mo and Flynn-Wall-Ozawa (FWO) methods, respectively. The small fluctuations in the values of Avrami exponent n and Mo parameter a indicate that the EVA crosslinking mechanism is basically unchanged with increasing heating rate and crosslinking agent content. The change of the Ozawa exponent m is presumably due to the increase in viscosity of EVA/TBEC samples during the crosslinking process. The heating/cooling function $F(T)$ values and the activation energy E_a are dependent on the conversion rate α . In addition, E_a shows irregular changes in the early stages of crosslinking, and increases with the increase of conversion rate α in the later stages of crosslinking.

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1. Introduction

The rapid growth of solar photovoltaics (PV) is critical to meet the growing demand for clean energy, and to decarbonize global power systems as well. Currently, wafer-based crystalline silicon (c-Si) PV modules are widely used in solar installations worldwide. A typical PV module consists of front glass, polymer encapsulant, PV cell, and backsheets (Fig. 1).^{1,2} The encapsulant is one of the important layers in the structure of the PV module, as the long-term reliability of the PV module is dependent on the effectiveness of the encapsulation material in preventing corrosion of the solar cells under extreme environmental conditions.^{3,4}

In early 1970s, polydimethylsiloxane (PDMS) was used as an encapsulant because of its excellent intrinsic stability against thermal-induced stress and ultraviolet (UV) light-induced stress.^{5,6} Later, many alternative materials such as ethylene vinyl acetate copolymer (EVA), polyvinyl butyral (PVB), thermoplastic polyolefin (TPO), and thermoplastic polyurethane (TPU) methacrylate polyethylene copolymer acids were developed.^{3,7} Nowadays, EVA is widely used in PV modules as an encapsulation material due to its excellent high transmittance, resistance to UV radiation, good adhesion to glass, and relative good weather resistance properties.^{8–12}

Some additives, such as crosslinking agent, UV absorber, light stabilizer, antioxidant, *etc.*⁸ were added to prevent the degradation reaction of EVA during long-term operation,^{13,14} in order to achieve the feasible and economical goal of 25–30 years of stable operation.^{15,16} The type of crosslinking agent has a significant impact on the kinetics of the lamination process, which further affects the energy consumption and the cost of the production. Considering that the crosslinking agent plays an important role in the lamination process, it is crucial to find a crosslinking agent with high crosslinking rate at relative low processing temperature to meet the industrial needs.^{1,17} The organic peroxide thermochemical crosslinking agent is widely used due to its controllable decomposition rate, low amount of by-products, and economical process.¹⁸ Traditionally, the crosslinking of EVA was mainly initiated by dicumyl peroxide (DCP). In recent years, modified organic peroxides, including *tert*-butylperoxy 2-ethylhexyl carbonate (TBEC), 2,5-dimethyl-2,5-di(*tert*-butylperoxy) hexane (DBPH), benzoyl peroxide (BPO), *etc.*^{19–23} have been used to improve the crosslinking efficiency of EVA. Therefore, understanding the effect of the crosslinking agent on the crosslinking process of EVA samples is of crucial

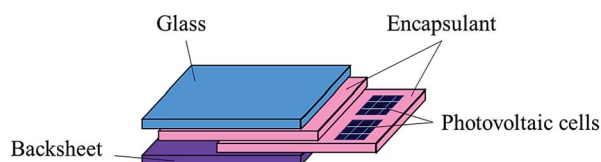


Fig. 1 Components of a PV module.

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importance in selecting a suitable crosslinking agent and optimizing the lamination process.²⁴

The crosslinking process of EVA in the solid or melting state follows a complex mechanism involving several reaction steps, and the apparent activation energy and rate of EVA crosslinking reaction increase with increasing of the vinyl acetate (VA) content.²⁵ Several mathematical models of non-isothermal kinetics, such as Avrami, Ozawa, and Mo methods, have been developed to describe the crystallization kinetics.^{26–29} These models also fit well with experimental data in the study of apparent kinetic parameters of crosslinking reactions of EVA with a VA content of 18 wt%.³⁰ In the above-mentioned work, only EVA with low VA content (<28 wt%) was studied. However, the VA content is usually in a range of 28–33 wt% for PV applications.¹ It is necessary to expand the knowledge of the crosslinking kinetics of EVA in order to further improve its long-term performance for photovoltaic encapsulation.

In this work, the effect of crosslinking agents on the crosslinking process of EVA was systematically investigated. The non-isothermal DSC analysis was first performed to obtain the crosslinking temperature, crosslinking rate, and crosslinking enthalpy of four crosslinking agents, including DCP, TBEC, DBPH, and BPO. Then, the kinetic parameters of EVA/TBEC crosslinking process were investigated by using Avrami, Ozawa, Mo, and Flynn-Wall-Ozawa (FWO) methods, respectively.

2. Materials and methods

2.1 Material

The granulated EVA copolymer (KA-40) with vinyl acetate content of 28 wt%, a melt flow index of 20 g/10 min, a melting point of 65 °C, and density of 0.945 g cm⁻³ was supplied by the Polyolefin Company Pte. Ltd. (Singapore). The weight-average molecular weight (M_w) of EVA is 101 000 g mol⁻¹, and the dispersibility index (M_w/M_n) is 2.09.

The TBEC was purchased from Shanghai Qinshang Chemical Co. Ltd. with a purity of 95%. The DCP was purchased from Shanghai Lingfeng Chemical Reagent Co. Ltd. with a purity of 99.5%. The DBPH was purchased from Shanghai Maclean Biochemical Technology Co. Ltd. with a purity of 93%. The BPO was purchased from Adamas with a purity of 98%.

2.2 EVA/crosslinking agent compounding

The granulated EVA copolymer was mixed with 0.4, 0.8, and 1.6 wt% of crosslinking agent, respectively. Then, the mixture was treated by melt compounding in a twin-screw extruder (Thermo minilab II) with a screw speed of 100 rpm at 90 °C for 5 min. Then, the samples were cooled to room temperature.

2.3 Differential scanning calorimetric (DSC) analysis

The non-isothermal crosslinking experiments of EVA/ (crosslinking agent) were carried out using a TA instrument Discovery DSC. The heat flow *versus* temperature (or time) curves for each sample were collected in scanning mode from 40 to 250 °C under N₂ atmosphere (50 mL min⁻¹) at five

different heating rates of 2.5, 5, 10, 20, 40 °C min⁻¹ using 3–10 mg of the sample, respectively.

The conversion rate α at time t is calculated according to the eqn (1):^{31,32}

$$\alpha = \frac{\Delta H_t}{\Delta H_{\text{total}}} \quad (1)$$

where ΔH_t is the heat of reaction at time t , and ΔH_{total} is the total heat of reaction at a certain heating rate.

Crosslinking time t can be obtained from eqn (2):³³

$$t = \frac{T_0 - T}{\phi} \quad (2)$$

where T_0 is the onset temperature of the crosslinking process, T is the temperature at the crosslinking time t and ϕ is the heating/cooling rate.

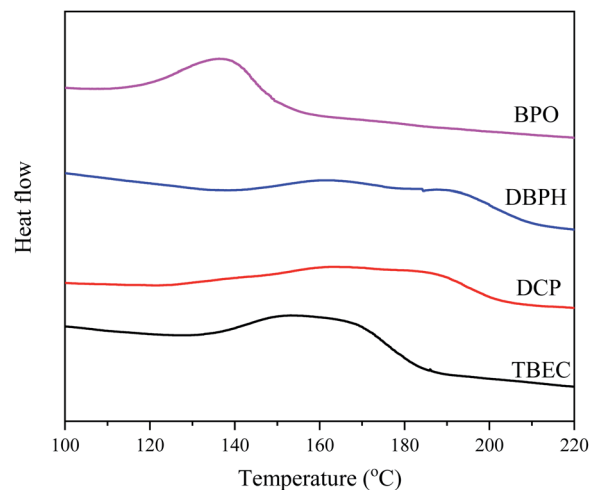


Fig. 2 DSC curves for EVA samples with 0.8 wt% of crosslinking agent at the heating rate of 10 °C min⁻¹.

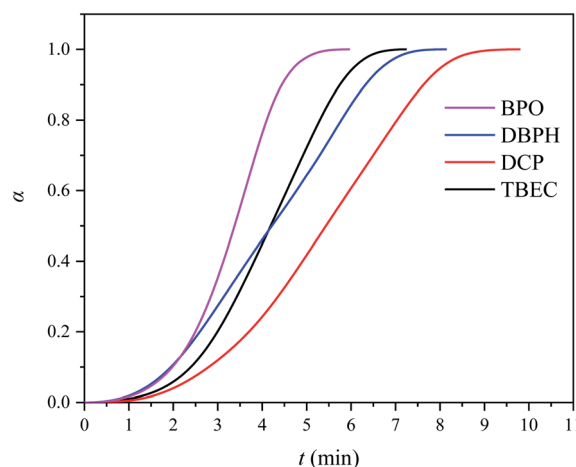


Fig. 3 Conversion rate α vs. time t curves for EVA samples with 0.8 wt% of crosslinking agent at the heating rate of 10 °C min⁻¹.

Table 1 Times, onset temperatures, peak temperatures and enthalpies obtained by DSC analysis

Crosslinking agent	t (min)	T_{onset} ($^{\circ}\text{C}$)	T_{peak} ($^{\circ}\text{C}$)	ΔH (J g^{-1})
BPO	5.97	101	138	7.03
DBPH	8.15	134	190	8.07
DCP	9.81	115	167	10.09
TBEC	7.25	116	162	9.68

3. Results and discussion

3.1 DSC analysis

The characterization of the crosslinking process of the EVA/(crosslinking agent) (0.8 wt%) was carried out by DSC analysis at the heating rate of $10\text{ }^{\circ}\text{C min}^{-1}$. Fig. 2 shows the DSC curves for four different EVA/(crosslinking agent) samples. The calculated conversion rate α versus time t is shown in Fig. 3. The reaction time t , onset temperature T_{onset} , peak temperature

T_{peak} , and enthalpy ΔH measured by DSC of four EVA samples with different crosslinking agents are listed in Table 1.

Among four considered crosslinking agents, the EVA/BPO sample shows the lowest onset temperature (T_{onset}), peak temperature (T_{peak}), and the shortest reaction time t (Table 1). However, the decomposition product from BPO contains aromatic compounds, which is unfavorable for EVA anti-discoloration performance.⁸ The EVA/TBEC sample shows lower onset temperature (T_{onset}), peak temperature (T_{peak}), and shorter reaction time t than the EVA/DCP and EVA/DBPH samples. Both the EVA/TBEC and EVA/DCP samples have large reaction enthalpy ΔH , which is related to the hydrogen abstracting ability of the radicals decomposed by TBEC and DCP during the crosslinking process. The high hydrogen abstracting ability of the radicals from TBEC and DCP can induce the formation of a denser cross-linked network from EVA, resulting in a higher enthalpy change of the reaction.^{19,20,34} Thus, the crosslinking agent TBEC, which exhibits a high reaction rate and low reaction temperature, was selected to investigate the crosslinking kinetics of EVA.

The non-isothermal DSC curves of EVA/TBEC samples are shown in Fig. 4. The peak temperature is constant as the amount of TBEC increased, indicating that the peak temperature is not dependent on the TBEC content (Fig. 4a). The peak temperature increases with the heating rate increased, which indicates that the peak temperature of EVA/TBEC sample is strongly dependent on the heating rate (Fig. 4b). At the same heating rate, the enthalpy ΔH increases with increasing of the TBEC content (Table 2), which suggests that the enthalpy ΔH is dependent on the TBEC content. Generally, at the same TBEC content, ΔH decreases slightly with increasing of the heating rate.

Fig. 5 displays the curves of the crosslinking conversion rate α versus time t for EVA samples with different TBEC contents at different heating rates. The same S-shape appeared in all curves indicates a fast-crosslinking process during the initial stages and a slow crosslinking process in the later stages. As expected,

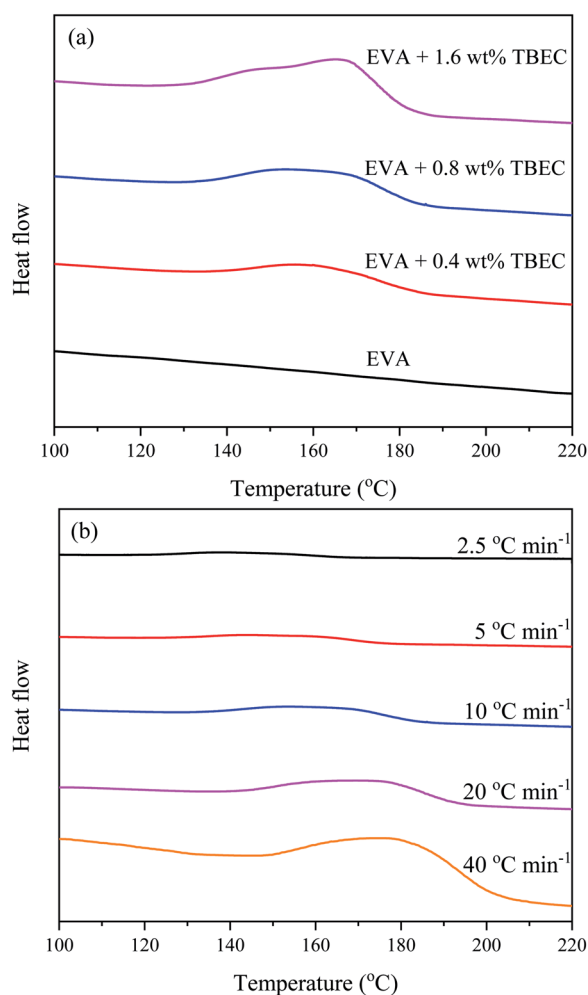


Fig. 4 Non-isothermal DSC curves for (a) different TBEC contents at the same heating rate ($10\text{ }^{\circ}\text{C min}^{-1}$), and (b) the same TBEC content (0.8 wt%) at different heating rates.

Table 2 Crosslinking enthalpies and peak temperatures for different contents at different heating rates

TBEC content	ϕ ($^{\circ}\text{C min}^{-1}$)	ΔH (J g^{-1})	T_{peak} ($^{\circ}\text{C}$)
0.4 wt%	2.5	6.46	141
	5	6.19	149
	10	6.49	160
	20	5.23	170
	40	5.17	178
0.8 wt%	2.5	11.40	140
	5	10.20	157
	10	9.81	162
	20	8.08	175
	40	9.25	179
1.6 wt%	2.5	15.77	150
	5	16.17	158
	10	15.58	166
	20	15.87	174
	40	15.80	182

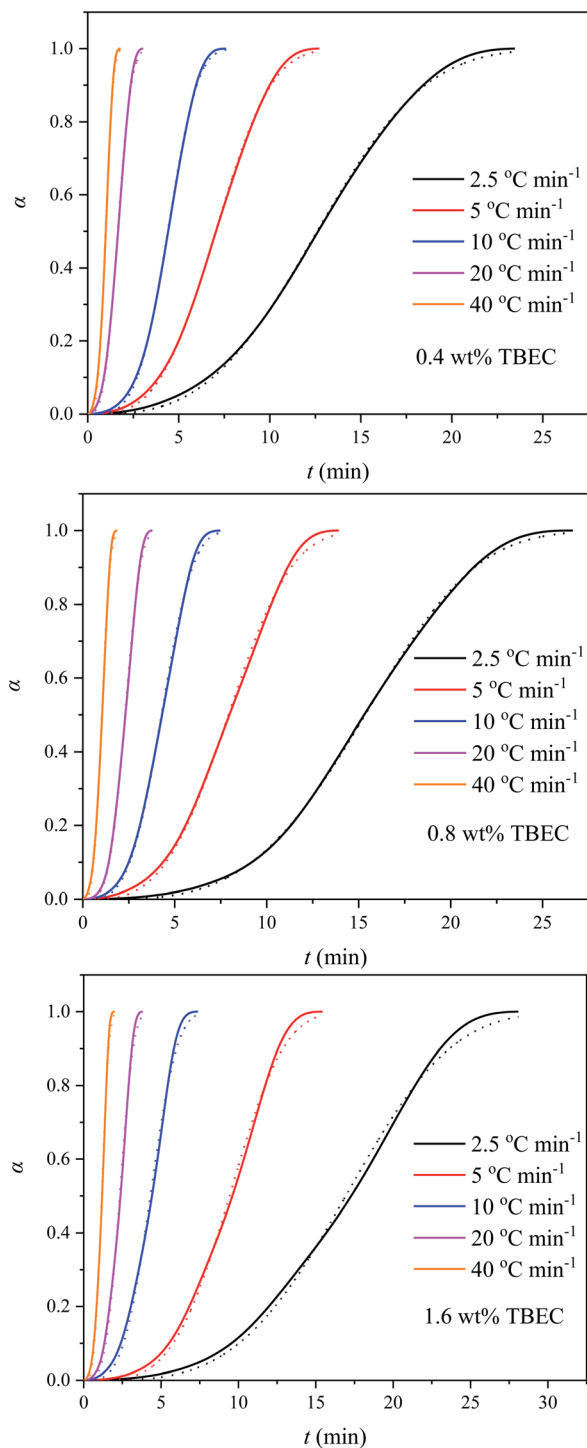


Fig. 5 Conversion rates of EVA samples with different TBEC contents at different heating rates. Dashed lines are fitted values by eqn (3).

the reaction rate of EVA/TBEC samples increase with increasing of the heating rate.

3.2 Non-isothermal kinetics

The crosslinking process of EVA usually includes multiple reaction steps with different activation energies. The apparent kinetic parameters of EVA crosslinking can be obtained by

fitting the experiments to the mathematical models. The kinetic parameters and activation energies of crosslinking process for the EVA/TBEC samples are investigated by using Avrami, Ozawa, Mo, and FWO methods, respectively.

3.2.1 Avrami method. The classical Avrami model was developed to study the kinetics of the isothermal phase change.³⁵ The degree of the phase change is calculated according to eqn (3):

$$\alpha = 1 - \exp(-Z_t t^n) \quad (3)$$

where n is the Avrami exponent, the value of which depends on the type of nucleation and growth process of the crystallization process. t and Z_t are crystallization time and crystallization rate constant, respectively.

The double logarithmic form of eqn (3) is given by

$$\ln[-\ln(1 - \alpha)] = \ln Z_t + n \ln t \quad (4)$$

By analyzing the plot of $\ln[-\ln(1 - \alpha)]$ versus $\ln t$, the Avrami exponent n and the rate constant Z_t can be calculated with the slope and intercept obtained by linear fitting. Considering that the DSC analysis of the crosslinking process is under non-isothermal conditions, the modified rate constant Z_c is introduced by Jeziorny.³⁶ The corrected rate constant Z_c expression is given by eqn (5)

$$\ln Z_c = \frac{\ln Z_t}{\phi} \quad (5)$$

where ϕ is the heating/cooling rate.

With the rate constant Z_c , the reaction half-life time $t_{1/2}$ can be calculated from eqn (6).

$$t_{1/2} = \left(\frac{\ln 2}{Z_c}\right)^{1/n} \quad (6)$$

The curves of the crosslinking conversion α versus time t fitted with eqn (3) are shown in Fig. 5. The Avrami exponent n ,

Table 3 Non-isothermal crosslinking kinetic parameters calculated from curve fitting procedures of Avrami method

TBEC content	ϕ (°C min ⁻¹)	n	Z_c	$t_{1/2}$ (min)	r
0.4 wt%	2.5	3.11	0.04	2.57	0.9998
	5	3.35	0.25	1.35	0.9998
	10	3.89	0.54	1.07	0.9999
	20	3.24	0.91	0.92	0.9997
	40	3.43	0.99	0.90	0.9997
0.8 wt%	2.5	3.66	0.02	2.81	0.9999
	5	3.36	0.23	1.39	0.9995
	10	3.63	0.57	1.06	0.9997
	20	3.97	0.83	0.95	0.9997
	40	3.38	0.99	0.90	0.9995
1.6 wt%	2.5	3.60	0.01	2.92	0.9990
	5	3.85	0.17	1.45	0.9991
	10	3.64	0.57	1.06	0.9989
	20	3.81	0.84	0.95	0.9989
	40	3.69	0.98	0.91	0.9991

rate constant Z_c , half-life time $t_{1/2}$, and correlation coefficient r obtained by curve fitting are listed in Table 3. These parameter values are different from those obtained by linear fitting with eqn (4) (Fig. S1 and Table S1 in the ESI†), which is due to the curve fitting process aims to minimize the level of error

throughout the entire curve.³⁷ In general, the fitted curves are in good agreement with experimental data. The Avrami exponent n is in the range of 3.11–3.97, indicating that the EVA/TBEC crosslinking process is independent of the TBEC content. The obtained n values are higher than those reported by Bianchi *et al.*,³⁰ which is presumably due to the different VA content in the EVA samples. The reaction constant Z_c increases with increasing of the heating rate. However, at the same heating rate, similar reaction constants are obtained with different TBEC contents, which suggests that the reaction constant Z_c is independent of the TBEC content and is a function of the temperature. In addition, the reaction half-life time $t_{1/2}$ decreases with increasing of the heating rate. The correlation coefficient r is in a range of 0.9989–0.9999, indicating that the Avrami model appropriately describes the crosslinking process of EVA/TBEC samples.

3.2.2 Ozawa method. The non-isothermal crystallization process can also be analyzed by using the Ozawa method,³⁸ which is given by

$$1 - \alpha = \exp(-K(T)/\phi^m) \quad (7)$$

where m is the Ozawa exponent, the value of which depends on the crystal growth dimension, and $K(T)$ is the heating/cooling function of the crystallization process. The double logarithmic form of eqn (7) is given by

$$\ln[-\ln(1 - \alpha)] = \ln K(T) - m \ln \phi \quad (8)$$

Fig. 6 shows the plots of $\ln[-\ln(1 - \alpha)]$ versus $\ln \phi$ for different TBEC contents at temperature ranging from 145 to 165 °C. Table 4 lists the Ozawa exponent m , the heating response function $K(T)$, and the correlation coefficient r calculated from the Ozawa curves fitted at different temperatures. The Ozawa model also shows a good correlation to the experimental data.

The Ozawa exponent m decreases with the increase of temperature and TBEC content, which reveals a change in the

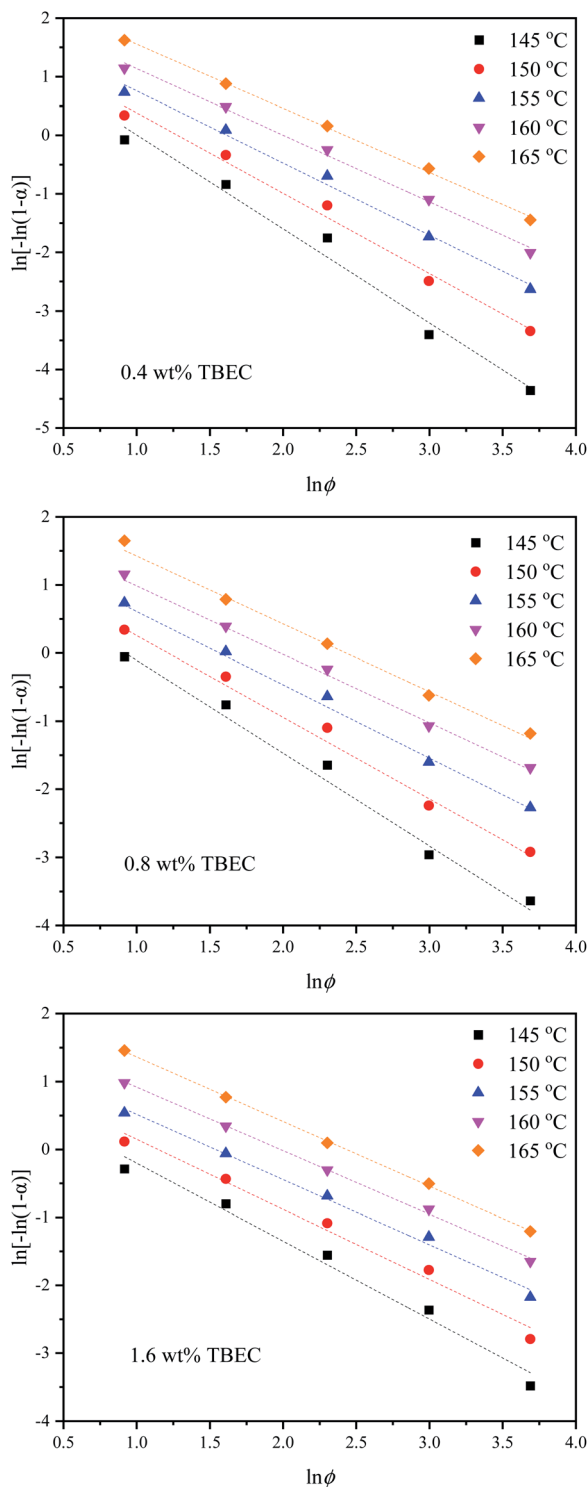


Fig. 6 Ozawa plots for EVA samples with different TBEC contents at various reaction temperatures. Dashed lines are fitted values by eqn (8).

Table 4 Non-isothermal crosslinking kinetic parameters calculated by Ozawa method

TBEC content	Temperature (°C)	m	$K(T)$	r
0.4 wt%	145	1.61	5.01	0.9913
	150	1.37	5.79	0.9945
	155	1.23	7.34	0.9964
	160	1.14	9.75	0.9978
	165	1.10	14.17	0.9992
0.8 wt%	145	1.35	3.68	0.9943
	150	1.21	4.68	0.9959
	155	1.10	5.96	0.9981
	160	1.03	8.05	0.9991
	165	1.02	12.22	0.9977
1.6 wt%	145	1.15	2.57	0.9909
	150	1.03	3.26	0.9927
	155	0.96	4.38	0.9965
	160	0.94	6.39	0.9991
	165	0.95	10.14	0.9998

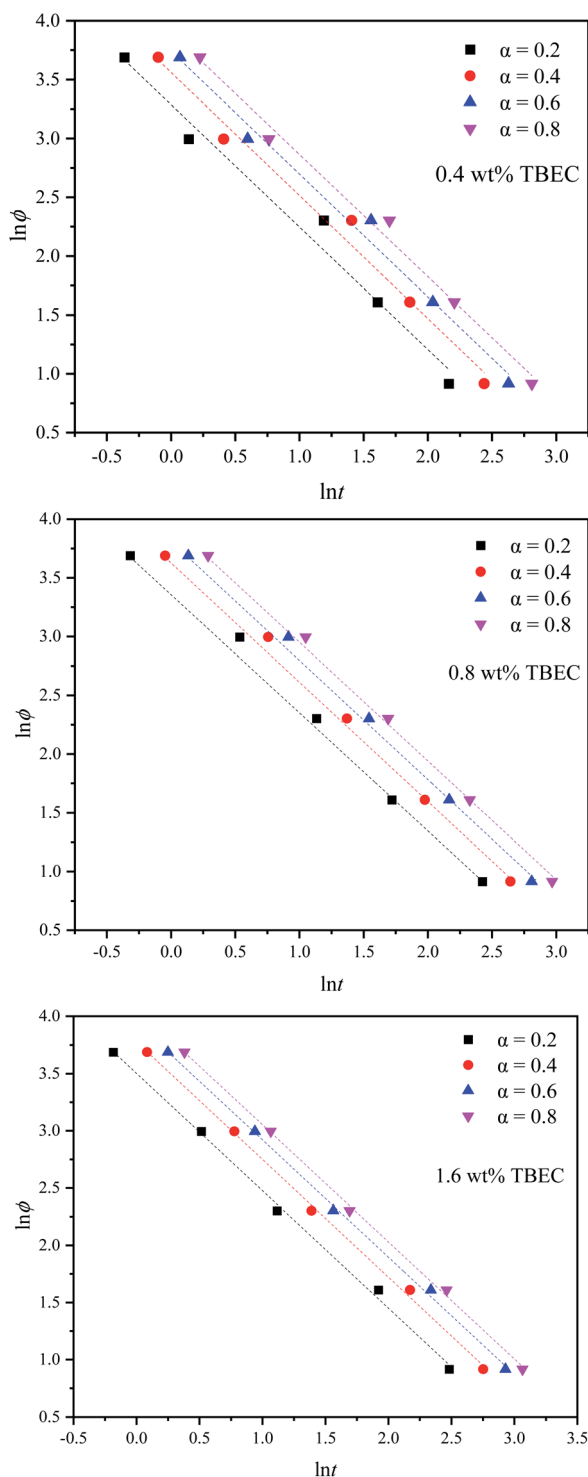


Fig. 7 Mo plots for EVA samples with different TBEC contents at various conversion rates. Dashed lines are fitted values by eqn (9).

crosslinking mechanism, probably due to the change in viscosity of the EVA/TBEC samples. The heating/cooling function $K(T)$ also depends on the reaction temperature. A high $K(T)$ value is expected when the temperature increased from 145 to 165 °C.

3.2.3 Mo method. Mo and co-workers established the relationship between the heating/cooling rate ϕ and time t at a certain degree of crystallinity by combining the Avrami method and the Ozawa method,³⁹ which is expressed as

$$\ln \phi = \ln F(T) - a \ln t \quad (9)$$

where $F(T) = (K(T)/Z_t)^{1/m}$ indicates the heating/cooling rate to reach the specified crystallinity within unit crystallization time, and a is the ratio of Avrami exponent n to Ozawa exponent m .

Fig. 7 shows $\ln \phi$ versus $\ln t$ plots for different TBEC contents at different degrees of conversion. The fitted lines are also in good agreement with the experiments. The non-isothermal crosslinking kinetic parameters calculated by Mo method are summarized in Table 5. The parameter a is independent of the TBEC content and the heating rate, which remains almost unchanged as the conversion rate and the TBEC content increased. $F(T)$ reflects the heating rate required per unit of reaction time.⁴⁰ The value of $F(T)$ increases with the conversion rate α , indicating that the crosslinking of the EVA/TBEC samples is hard to proceed at high conversion rate.

3.2.4 Activation energy analysis. The isoconversion method is a common method to obtain the local activation energy during the phase change, among which the integral isoconversion FWO method is widely used.^{41–46} The approximated FWO method proposed by Doyle⁴⁷ is given as

$$\log \phi = \text{const} - 0.4567 \left(\frac{E_a}{RT} \right) \quad (10)$$

According to eqn (10), the slope is obtained by linear fitting of the plot $\ln \phi$ versus $1/T$ at a certain conversion rate α . Thus, the corresponding activation energy E_a is given by the slope of the fitted line at a certain conversion rate α . The FWO analysis plots at different TBEC contents are depicted in Fig. 8. The FWO fits are also in good agreement with the experiments from r values (Table S2 in the ESI†). The activation energy E_a versus conversion rate α plot is shown in Fig. 9.

The activation energies E_a of EVA/TBEC crosslinking with different TBEC contents at various conversion rates (α) are in a range from 117 to 134 kJ mol⁻¹. The activation energies of

Table 5 Non-isothermal crosslinking kinetic parameters calculated by Mo method

TBEC content	α	a	$F(T)$	r
0.4 wt%	0.2	1.04	26.77	0.9895
	0.4	1.05	35.19	0.9924
	0.6	1.04	42.16	0.9941
	0.8	1.04	49.52	0.9952
0.8 wt%	0.2	1.03	31.13	0.9977
	0.4	1.05	40.69	0.9986
	0.6	1.05	48.82	0.9990
	0.8	1.04	56.72	0.9993
1.6 wt%	0.2	1.03	33.20	0.9988
	0.4	1.03	43.72	0.9992
	0.6	1.02	51.69	0.9994
	0.8	1.02	58.97	0.9994

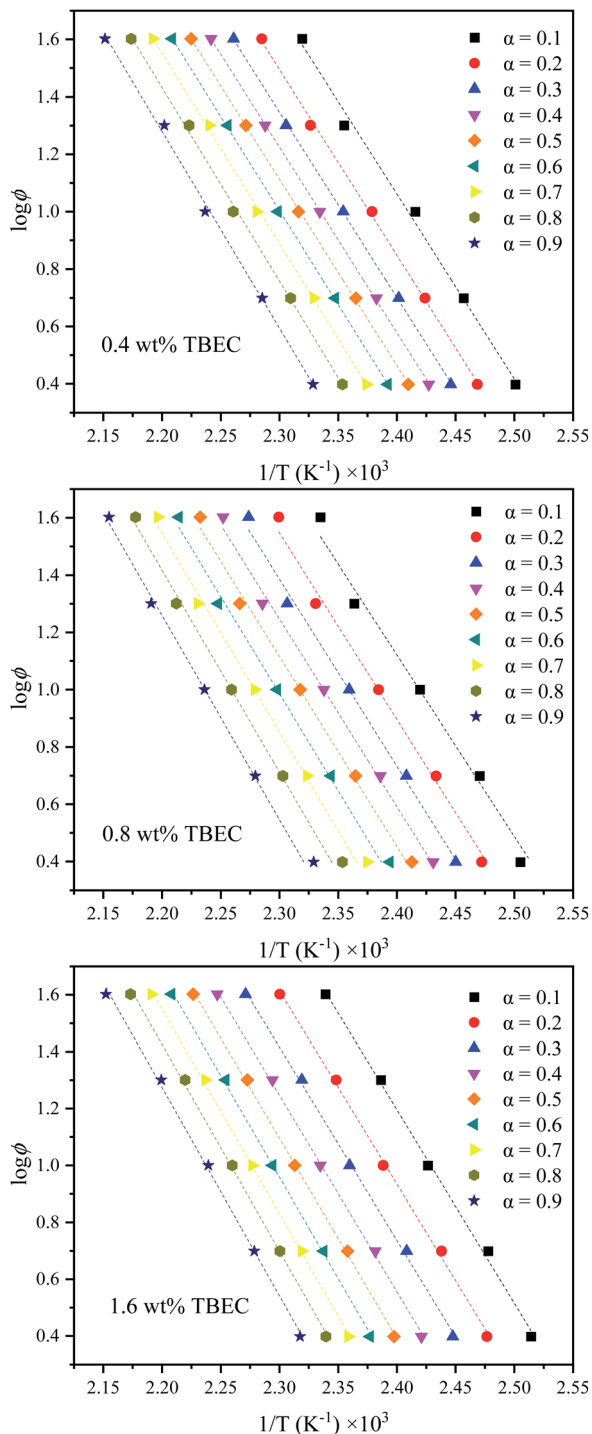


Fig. 8 FWO analysis at specific conversion rates α . Dashed lines are fitted values by eqn (10).

samples with TBEC content of 0.4 wt% and 1.6 wt% change irregularly when α is less than 0.3, while increases significantly with α increasing in the range from 0.3 to 1. For the sample with TBEC content of 0.8 wt%, the regular change of the activation energy occurs only when α is larger than 0.5. The reason for the irregular change is that the molecular chain can move freely in the insufficiently crosslinked EVA.²⁵ However, the viscosity of

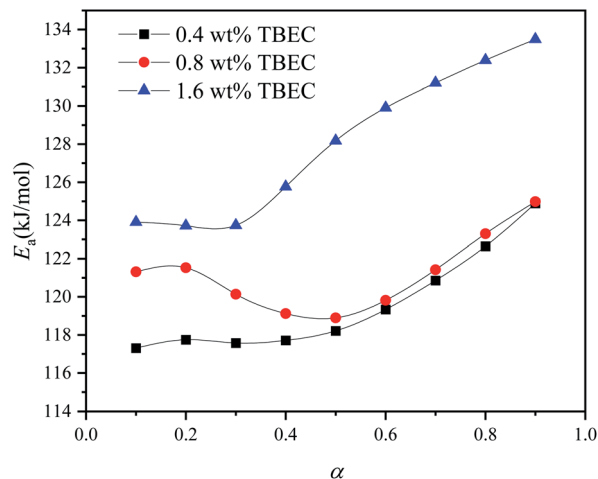


Fig. 9 Activation energies (E_a) calculated by FWO method for EVA samples with different TBEC content at various conversion rates α .

the EVA/TBEC sample increases with the conversion rate α further increasing, which inhibits the macromolecular chain movement of EVA and prohibits further crosslinking. Thus, the energy barrier of crosslinking increases as the reaction proceeds. This also supports the analysis of the reason for the changes in $K(T)$ and $F(T)$ parameters as mentioned above.

4. Conclusions

In this work, the non-isothermal crosslinking process of different crosslinking agents is analyzed by DSC method. The crosslinking agent TBEC, which is more favorable for EVA anti-discoloration performance than BPO, shows a higher crosslinking rate and lower crosslinking temperature in the crosslinking process with comparison to DCP and DBPH. Then, the DSC data of EVA samples with different TBEC contents are analyzed at different heating rates. The peak temperature of EVA/TBEC sample is strongly dependent on the heating rate. The crosslinking rate increased with the heating rate.

The non-isothermal kinetics of the EVA/TBEC samples crosslinking process are investigated by using Avrami, Ozawa, Mo, and FWO methods, respectively. The Avrami exponent n is in a range of 3.11–3.97, indicating that the EVA/TBEC crosslinking process is independent of the TBEC content. The change of the Ozawa exponent m is presumably due to the increase in viscosity of EVA/TBEC samples during the crosslinking process. The heating/cooling function $F(T)$ values and the activation energy E_a are dependent on the conversion rate α . In addition, E_a shows irregular changes in the early stage of crosslinking, while increase with increasing of the conversion rate α in the later stage of crosslinking.

Author contributions

Fanwei Zeng: conceptualization, design of experiment, investigation, writing; Xing Guo and Xuelian He: validation,

characterization; Li Sun and Zhen Liu: review and editing; Zuoxiang Zeng: project administration, funding.

Conflicts of interest

There are no conflicts to declare.

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References

- 1 M. C. C. d. Oliveira, A. S. A. Diniz Cardoso, M. M. Viana and V. d. F. C. Lins, *Renew. Sust. Energ. Rev.*, 2018, **81**, 2299–2317.
- 2 A. Sinha, O. S. Sastry and R. Gupta, *Sol. Energy Mater. Sol. Cells*, 2016, **155**, 234–242.
- 3 B. Adothu, P. Bhatt, S. Chattopadhyay, S. Zele, J. Oderkerk, H. P. Sagar, F. R. Costa and S. Mallick, *Sol. Energy*, 2019, **194**, 581–588.
- 4 A. Dadaniya and N. V. Datla, *Sol. Energy Mater. Sol. Cells*, 2019, **201**, 110063.
- 5 M. A. Green, *Prog. Photovolt: Res. Appl.*, 2005, **13**, 447–455.
- 6 M. D. Kempe, *2008 33rd IEEE Photovoltaic Specialists Conference*, 2008, pp. 1–6, DOI: [10.1109/PVSC.2008.4922771](https://doi.org/10.1109/PVSC.2008.4922771).
- 7 M. D. Kempe, *2011 37th IEEE Photovoltaic Specialists Conference*, 2011, pp. 000085–000090, DOI: [10.1109/PVSC.2011.6185851](https://doi.org/10.1109/PVSC.2011.6185851).
- 8 A. W. Czanderna and F. J. Pern, *Sol. Energy Mater. Sol. Cells*, 1996, **43**, 101–181.
- 9 J. Schlothauer, S. Jungwirth, M. Koehl and B. Roeder, *Sol. Energy Mater. Sol. Cells*, 2012, **102**, 75–85.
- 10 M. Gagliardi, P. Lenarda and M. Paggi, *Sol. Energy Mater. Sol. Cells*, 2017, **164**, 93–106.
- 11 C. Abderafi, L. Remi and B. David, *J. Photonics Energy*, 2013, **3**, 1–11.
- 12 A. El Amrani, A. Mahrane, F. Y. Moussa and Y. Boukennous, *Int. J. Photoenergy*, 2007, **2007**, 1–5.
- 13 S. S. Ghadikolaei, A. Omrani and M. Ehsani, *Thermochim. Acta*, 2017, **655**, 87–93.
- 14 J. Jin, S. Chen and J. Zhang, *Polym. Degrad. Stab.*, 2010, **95**, 725–732.
- 15 B. Ottersböck, G. Oreski and G. Pinter, *Polym. Degrad. Stab.*, 2017, **138**, 182–191.
- 16 G. Perrakis, A. C. Tasolamprou, G. Kenanakis, E. N. Economou, S. Tzortzakis and M. Kafesaki, *OSA Continuum*, 2020, **3**, 1436–1444.
- 17 S. Jiang, K. Wang, H. Zhang, Y. Ding and Q. Yu, *Macromol. React. Eng.*, 2015, **9**, 522–529.
- 18 O. Bianchi, R. Fiorio, J. N. Martins, A. J. Zattera, C. H. Scuracchio and L. B. Canto, *J. Elastomers Plast.*, 2009, **41**, 175–189.
- 19 A. Thitithammawong, C. Nakason, K. Sahakaro and J. Noordermeer, *Polym. Test.*, 2007, **26**, 537–546.
- 20 I. Hudec, R. Sýkora and J. Kruželák, *Rubber Chem. Technol.*, 2017, **90**, 60–88.
- 21 H. Y. Xue, W. H. Ruan, M. Q. Zhang and M. Z. Rong, *Express Polym. Lett.*, 2014, **8**, 116–122.
- 22 J. Kruželák, A. Kvasničáková and I. Hudec, *Ind. Eng. Chem. Res.*, 2020, **3**, 120–128.
- 23 Y. T. Sung, C. K. Kum, H. S. Lee, J. S. Kim, H. G. Yoon and W. N. Kim, *Polymer*, 2005, **46**, 11844–11848.
- 24 K. Thaworn, P. Buahom and S. Areerat, *Polym. Chem.*, 2012, **02**, 77–85.
- 25 C. P. Liu, W. F. Song, Q. X. Lu and M. F. Chen, *Ind. Eng. Chem. Res.*, 2014, **53**, 10080–10089.
- 26 R. Zhang and X. He, *RSC Adv.*, 2015, **5**, 130–135.
- 27 X. Jin, X. Chen, Q. Cheng, N. Zhang, S. Cai and J. Ren, *RSC Adv.*, 2017, **7**, 46014–46021.
- 28 A. Dołęga and P. M. Zieliński, *J Non Cryst Solids*, 2022, **575**, 121198.
- 29 X. Zhao, T. Wang, S. Hong, D. Sun, N. Wang, G. Chae and Y. Qi, *RSC Adv.*, 2019, **9**, 35280–35288.
- 30 O. Bianchi, R. V. B. Oliveira, R. Fiorio, J. D. N. Martins, A. J. Zattera and L. B. Canto, *Polym. Test.*, 2008, **27**, 722–729.
- 31 M. Á. Vargas-Hernández, B. Sulbarán-Rangel and H. Vázquez-Torres, *Thermochim. Acta*, 2020, **684**, 178485.
- 32 S. Kumar, S. K. Samal, S. Mohanty and S. K. Nayak, *J. Therm. Anal. Calorim.*, 2019, **137**, 1567–1578.
- 33 L. Wang, F. Zhang, Y. Bai and L. Ding, *Thermochim. Acta*, 2016, **645**, 43–49.
- 34 A. J. Zattera, O. Bianchi, R. V. B. Oliveira, L. B. Canto, C. A. Ferreira and M. Zeni, *Prog. Rubber Plast. Recycl. Technol.*, 2006, **22**, 69–87.
- 35 M. Avrami, *J. Chem. Phys.*, 1940, **8**, 212–224.
- 36 A. Jeziorny, *Polymer*, 1978, **19**, 1142–1144.
- 37 C. A. Kelly and M. J. Jenkins, *Polym J*, 2022, **54**, 249–257.
- 38 T. Ozawa, *Polymer*, 1971, **12**, 150–158.
- 39 T. Liu, Z. Mo, S. Wang and H. Zhang, *Polym. Eng. Sci.*, 1997, **37**, 568–575.
- 40 C. Jiao, Z. Wang, X. Liang and Y. Hu, *Polym. Test.*, 2005, **24**, 71–80.
- 41 M. Wang and L. Chen, *J. Cryst. Growth*, 2021, **565**, 126159.
- 42 J. C. Domínguez, J. C. Grivel and B. Madsen, *Thermochim. Acta*, 2012, **529**, 29–35.
- 43 W. Bessa, D. Trache, M. Derradji and A. F. Tarchoun, *ChemistrySelect*, 2020, **5**, 5374–5386.
- 44 J. Li, J. Huang and R. Yin, *RSC Adv.*, 2019, **9**, 27305–27317.
- 45 X. Xiong, X. Guo, R. Ren, L. Zhou and P. Chen, *Polym. Test.*, 2019, **77**, 105917.
- 46 W. Wu, C. Wan, S. Wang and Y. Zhang, *RSC Adv.*, 2013, **3**, 26166–26176.
- 47 C. D. Doyle, *J. Appl. Polym. Sci.*, 1962, **6**, 639–642.