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Supporting Information

Grape Stalks Valorization towards Circular Economy: A Cascade Biorefinery Strategy

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Supporting information

Table S1: MTC-5 medium composition.

Solution	Volume (mL)	Composition
A	45	Carbon source (Cellobiose, Avicel® or S2), Sodium MOPS salt C ₇ H ₁₄ NNaO ₄ S in MilliQ water
B	2	Potassium citrate monohydrate (C ₆ H ₅ O ₇ K ₃ ·H ₂ O), monohydrate citric acid (C ₆ H ₈ O ₇ ·H ₂ O), sodium sulphate (Na ₂ SO ₄), potassium dihydrogen phosphate (KH ₂ PO ₄), sodium bicarbonate (NaHCO ₃) in MilliQ water
C	1	Urea (CH ₄ N ₂ O), ammonium chloride (NH ₄ Cl) in MilliQ water
D	1	magnesium chloride (MgCl ₂ ·6H ₂ O), calcium chloride (CaCl ₂ ·H ₂ O), iron (II) chloride (FeCl ₂ ·4H ₂ O), L-Cysteine hydrochloride monohydrate (C ₃ H ₇ NO ₂ S·HCl·H ₂ O), trace mineral (see F solution), MilliQ water
E	1	Pyridoxamine hydrochloride (C ₈ H ₁₂ N ₂ O ₂ ·2HCl), p-aminobenzoic acid (C ₇ H ₇ NO ₂), d-biotin (C ₁₀ H ₁₆ N ₂ O ₃ S), vitamin B12 (C ₆₃ H ₈₈ CoN ₁₄ O ₁₄ P), MilliQ water
F	2.5 (in 50 mL of D)	manganese chloride (MnCl ₂ ·4H ₂ O), oxalyl chloride (COCl ₂ ·6H ₂ O), zinc chloride (ZnCl ₂), copper chloride (CuCl ₂ ·2H ₂ O), boric acid (H ₃ BO ₃), sodium molybdate (Na ₂ MoO ₄ ·2H ₂ O), nickel chloride (NiCl ₂ ·6H ₂ O) in MilliQ water

Fig. S1: Scheme of the cascade process with mass balance.

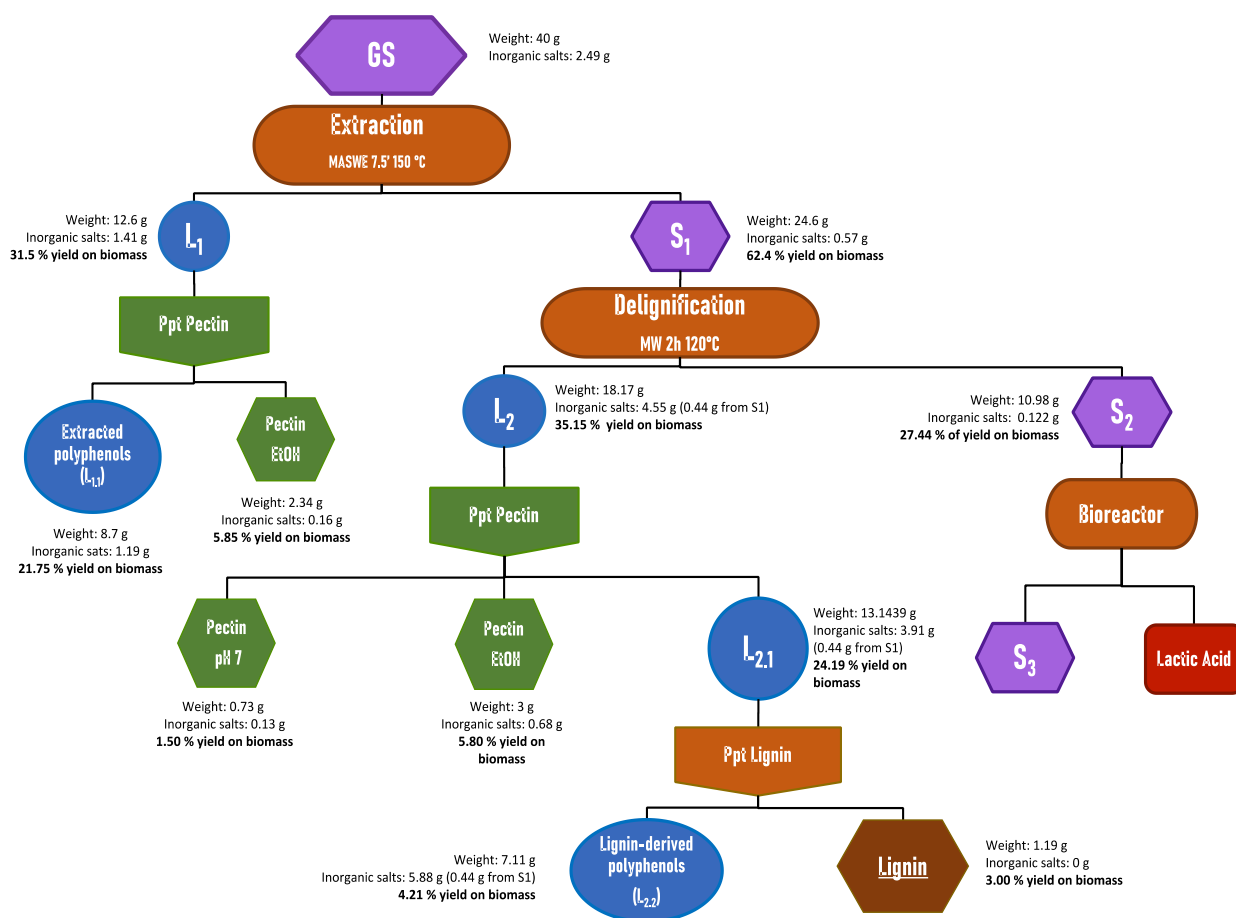


Table S2: Moscato must *characterization*.

°Bx	20
Volatile acidity (g/L)	0.07
pH	3.185
Organic nitrogen (mg/L)	84
Inorganic nitrogen (mg/L)	47

Table S3: Moscato wine *characterization*.

Volatile acidity (g/L)	0.52
Alcohol (% v/v)	11.53
Acetaldehyde (mg/L)	< 18
SO ₂ (mg/L)	< 15 mg/L

Table S4: Analyses of the four different treatments after 3 months of conservation.

	No additives	S.D.	200 mg/mL SO ₂	S.D.	100 mg/mL SO ₂ + 5 mg /mL extracts	S.D.	5 mg/L extracts	S.D.
Volatile acidity (g/L)	1.085	0.035	0.935	0.021	1.005	0.007	> 1.2	-
Acetaldehyde (mg/L)	< 18	-	< 18	-	< 18	-	< 18	-
SO₂ (mg/L)	< 15	-	112.000	1.414	31.500	0.707	< 15	-
Free SO₂ (mg/L)	< 1	-	56.000	1.414	12.000	0.000	< 1	-
IPT (GAE mg/L)	146.500	2.828	159.000	1.414	377.000	24.042	308.500	20.506
Tannins (g/L)	< 0.3	-	< 0.3	-	< 0.3	-	< 0.3	-
Catechins (mg/L)	2.250	0.354	2.800	0.566	> 30	-	> 30	-
Polyphenols (mg/L)	< 150	-	< 150	-	913.500	130.815	737.500	27.577
Abs 420	0.128	0.010	0.094	0.000	0.697	0.262	0.637	0.003
Abs 520	0.055	0.009	0.031	0.005	0.311	0.150	0.256	0.000
Abs 620	0.036	0.004	0.021	0.001	0.122	0.106	0.056	0.005
Intensity	0.219	0.023	0.141	0.012	1.130	0.518	0.949	0.001
Tonality	2.388	0.235	3.122	0.508	2.302	0.262	2.489	0.008

Table S5: ANOVA and Post Hoc Tukey test results conducted on volatile acidity (A), IPT (B), catechins (C), polyphenols (D), Abs 420 nm (E), with the aim of comparison of the four different treatments.

A	Mean - Volatile acidity (g/L)	Groups		
5 mg/L L1.1	1.3	A		
No Additives	1.085		B	
100 mg/mL SO₂ + 5 mg /mL L1.1	1.005		B	C
200 mg/mL SO₂	0.935			C

B	Mean - IPT (GAE mg/L)	Groups		
100 mg/mL SO₂ + 5 mg /mL L1.1	377	A		
5 mg/L L1.1	308.5		B	
200 mg/mL SO₂	159			C
No Additives	146			C

C	Mean - Catechins (mg/L)	Groups	
5 mg/L L1.1	30	A	
100 mg/mL SO ₂ + 5 mg /mL L1.1	30	A	
200 mg/mL SO ₂	2.8		B
No Additives	2.25		B

D	Mean - Polyphenols (mg/L)	Groups	
100 mg/mL SO ₂ + 5 mg /mL L1.1	913.5	A	
5 mg/L L1.1	737.5	A	
No Additives	140		B
200 mg/mL SO ₂	140		B

E	Mean - Abs 420	Groups		
100 mg/mL SO ₂ + 5 mg /mL L1.1	0.697	A		
5 mg/L L1.1	0.637	A	B	
No Additives	0.128		B	C
200 mg/mL SO ₂	0.094			C

Pectin_L1_EtOH



Pectin_L2_EtOH



Fig. S2: Pectin precipitated with ethanol from L1 and L2.

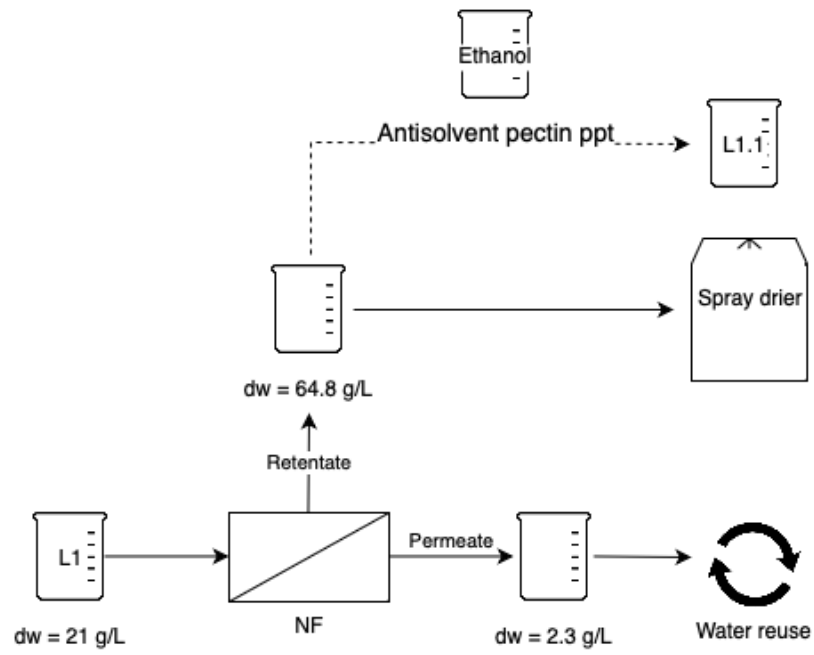


Fig. S3: Workflow of L1 membrane treatment process

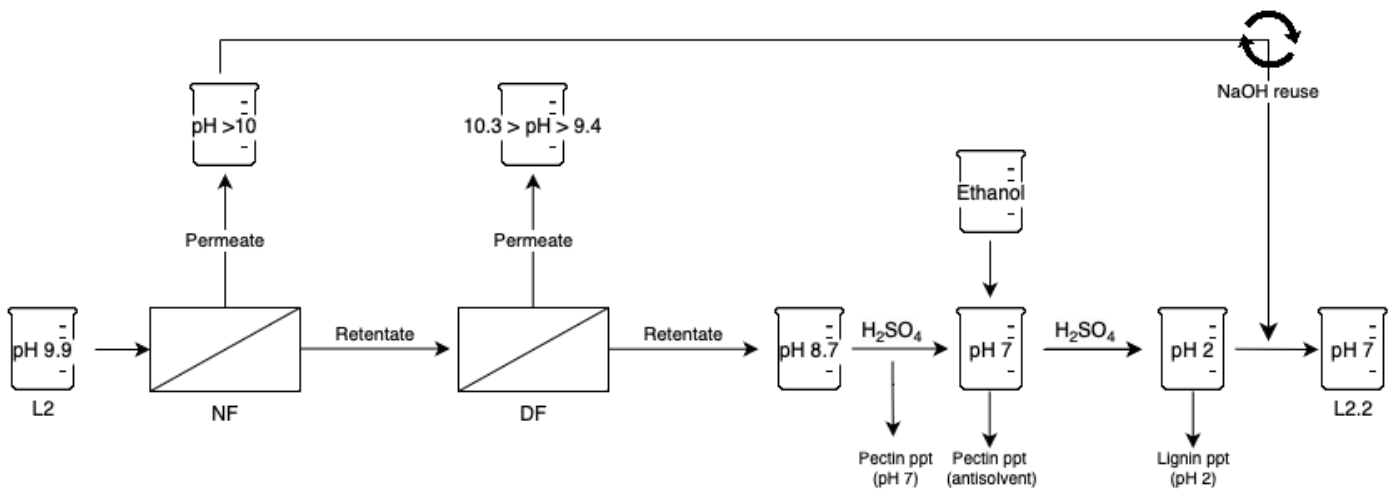


Fig. S4: Workflow of L2 membrane treatment process

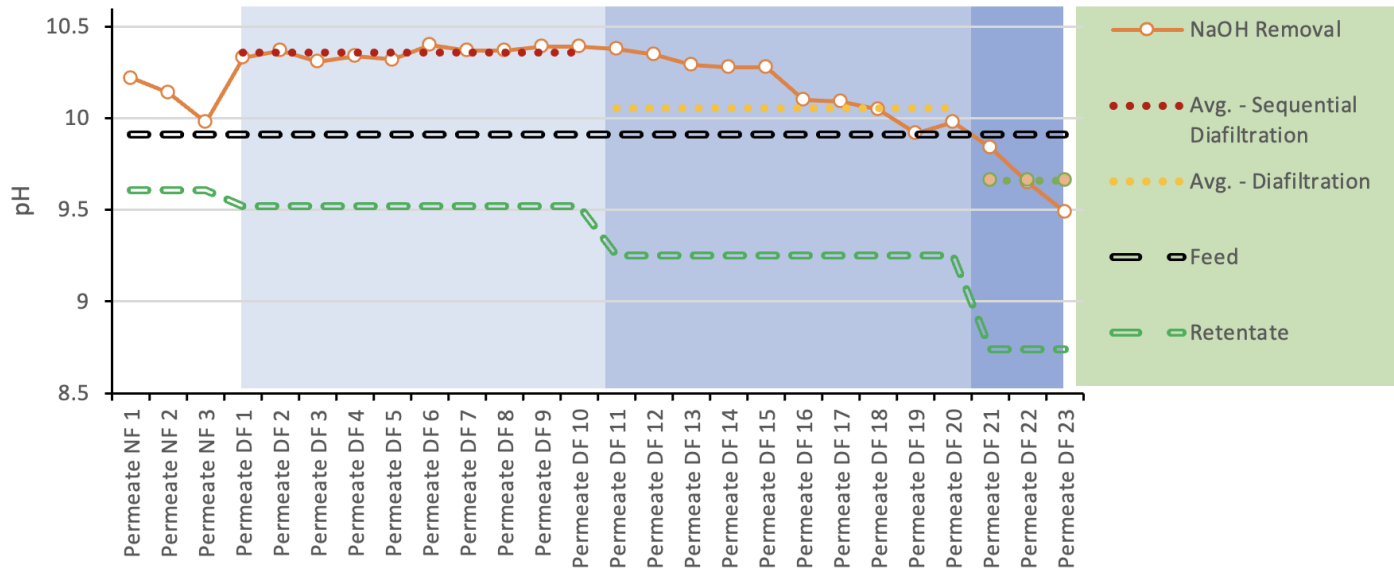


Fig. S5: Continuous NaOH diafiltration from L2

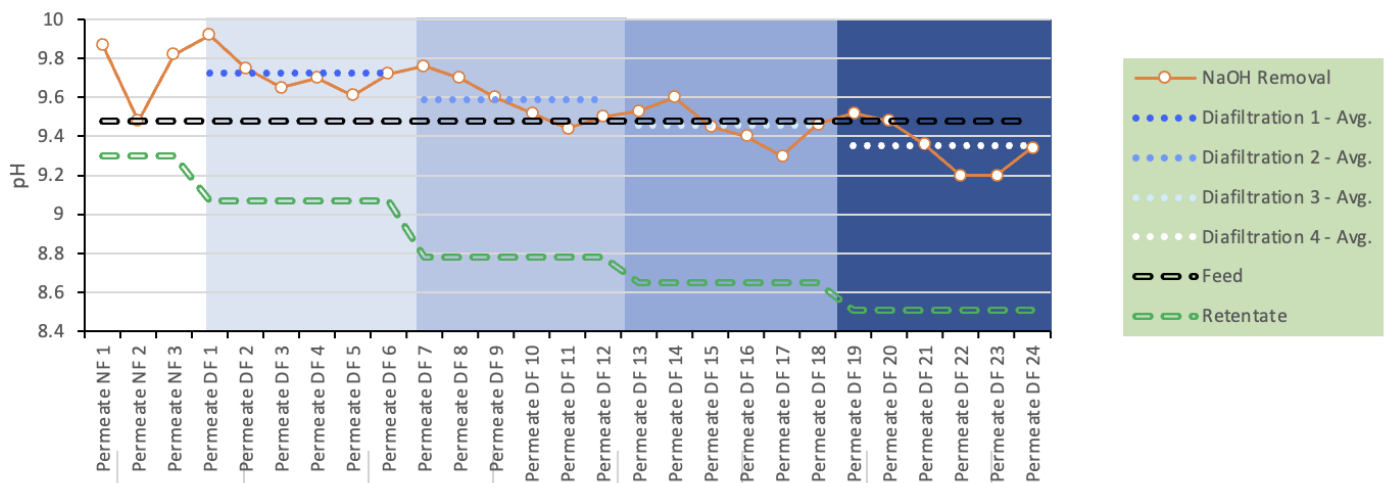


Fig. S6: Discontinuous NaOH diafiltration from L2

Table S6: A) Materials flow during the reuse and recycling of solvents and additives B) Reduction rates obtained in L2 downstream treatment

A			
L1 nanofiltration			
Process	Solvents and Additives	NF process	Conventional
Extraction	Extraction Water (L)	1.80	1.80
NF	Recovered Water (L)	1.30	-
	Volume of Retentate (L)	0.50	1.80
Pectin precipitation	EtOH for pectin precipitation (L)	0.50	1.80
L2 membrane treatment			
Process	Solvents and Additives	NF process	Conventional
Delignification	Water (L)		1.498
	NaOH (g)		7.488
	pH of L2		9.910
	Residual NaOH in L2 (g)		4.84E-03
NF+DF	NaOH recovery in Permeate (g)	4.80E-03	-
	NaOH recovery in Permeate (%)	99.060	-
	Volume of Retentate (L)	0.21	-
	pH of Retentate	8.740	-
	NaOH remaining in Retentate (g)	4.55E-05	-
Pectin precipitation	H ₂ SO ₄ addition to neutrality (g)	5.61E-05	0.006
	EtOH for pectin precipitation (L)	0.208	1.498
Lignin precipitation	Addition of alkaline permeate from ND+DF (L)	0.160	-
	NaOH addition to neutrality (g)	-	0.596
	Final Volume (L)	0.368	1.498

B	Ratio	Reduction %
H ₂ SO ₄ pH 7	106.50	99.06
EtOH	7.2	86.11
NaOH	-	100
Water	4.07	75.43

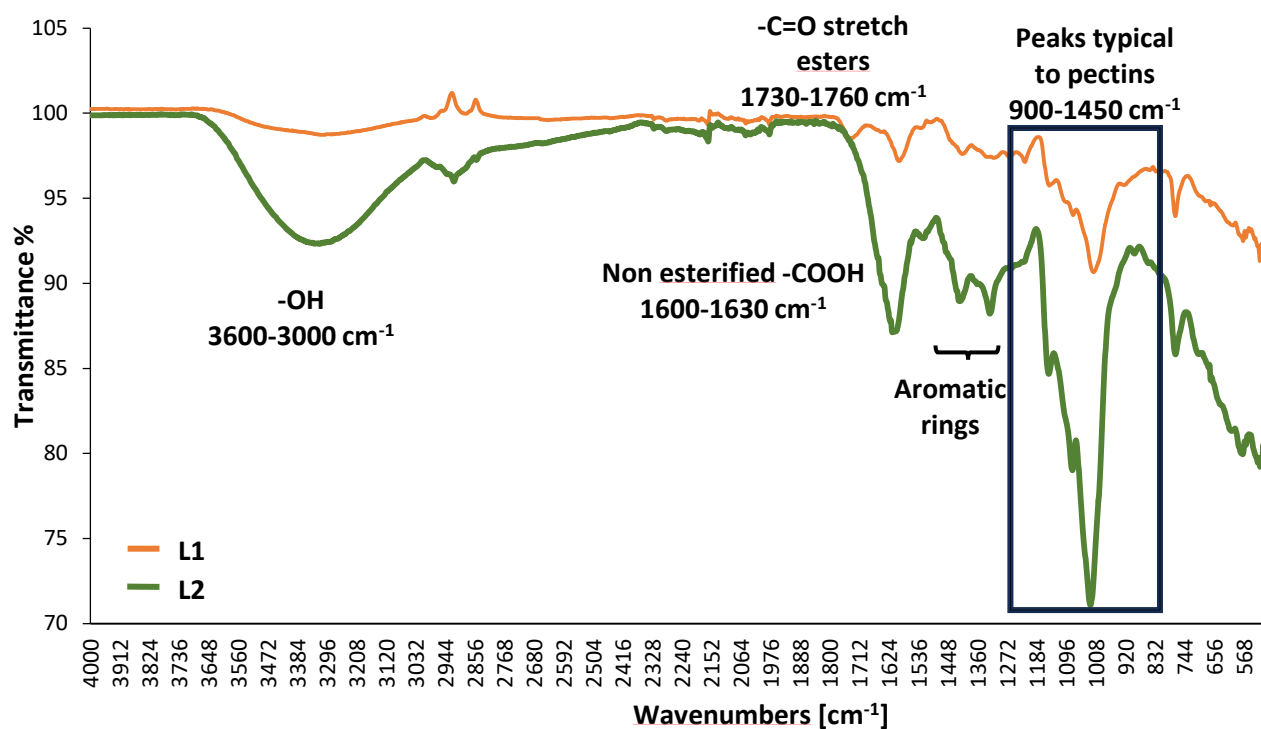


Fig. S7: ATR-FTIR of pectin precipitated from L1 and L2 with ethanol.

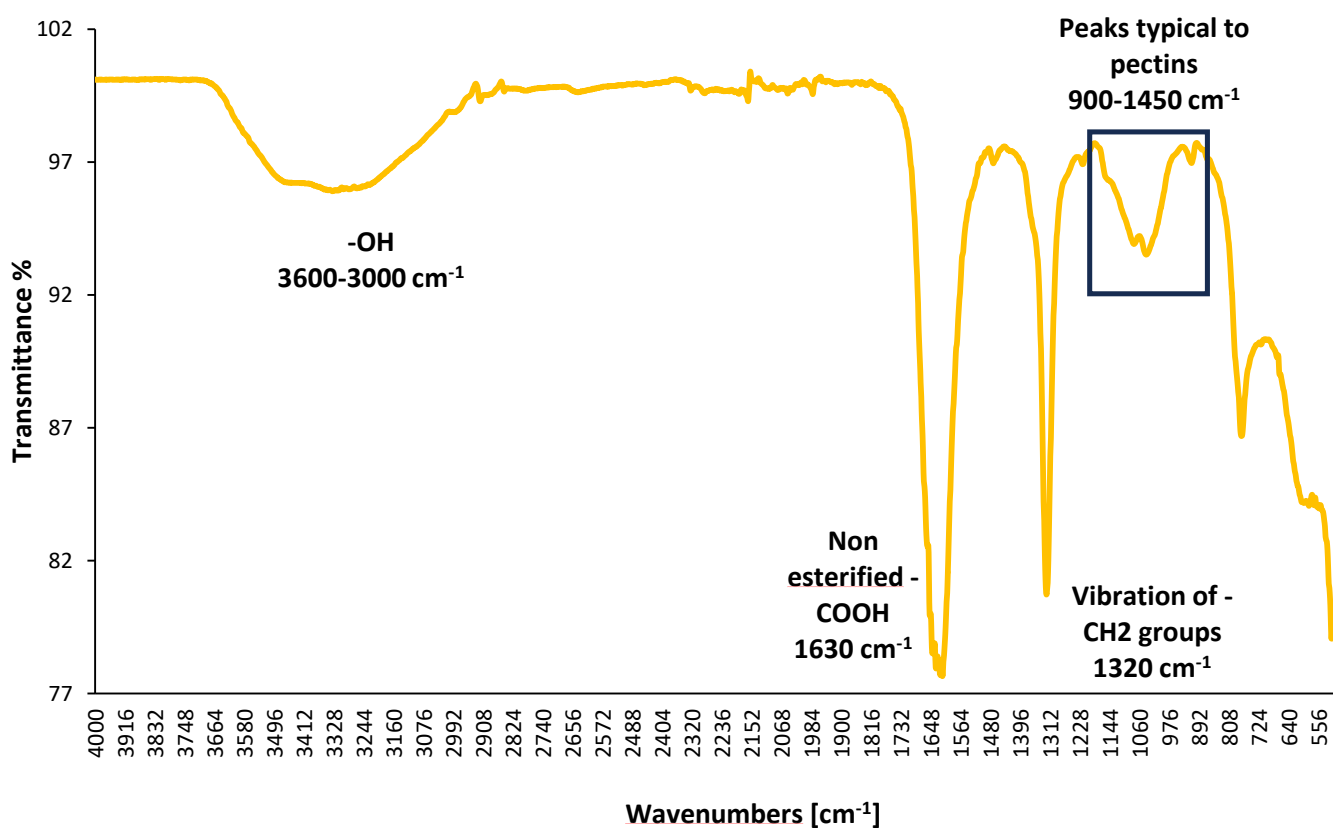


Fig. S8: ATR-FTIR of pectin precipitated at pH 7 from L2.

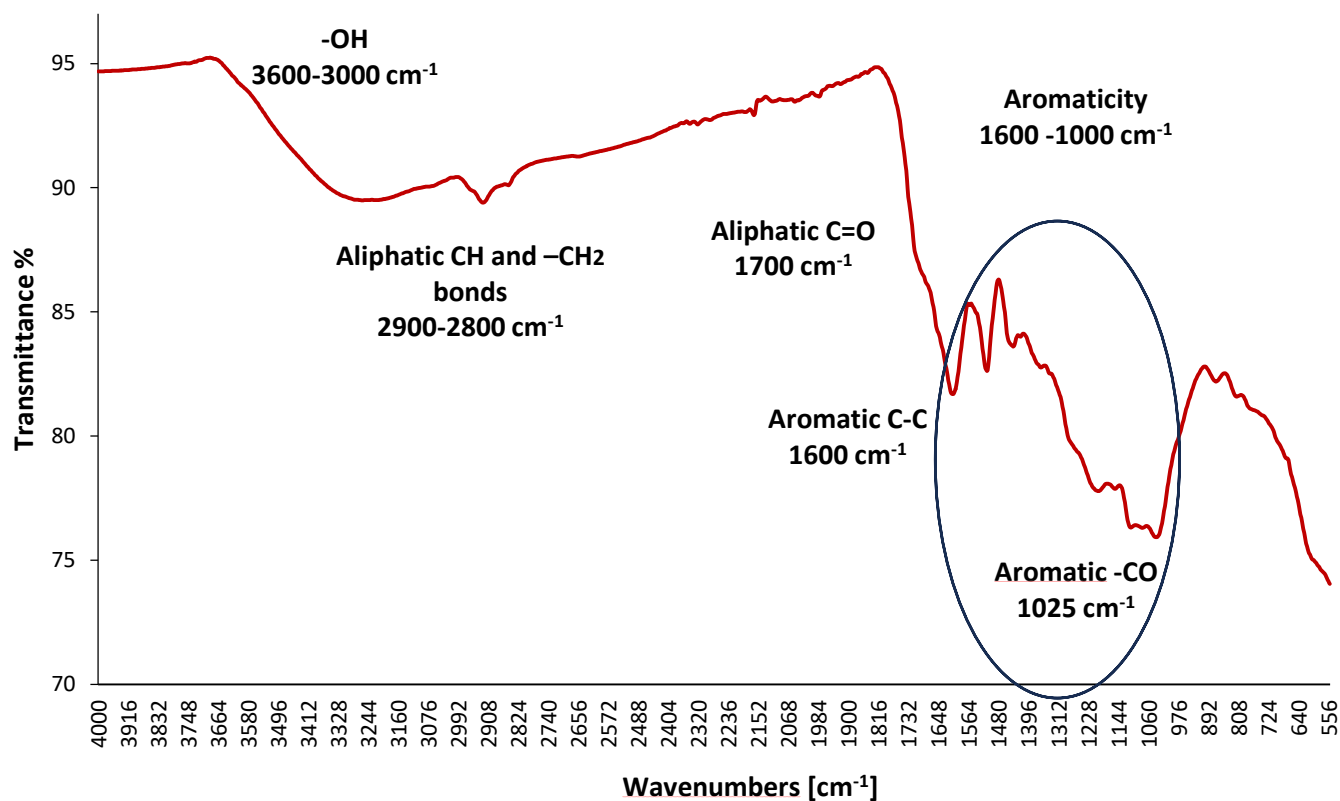


Fig. S9: ATR-FTIR of lignin fraction.

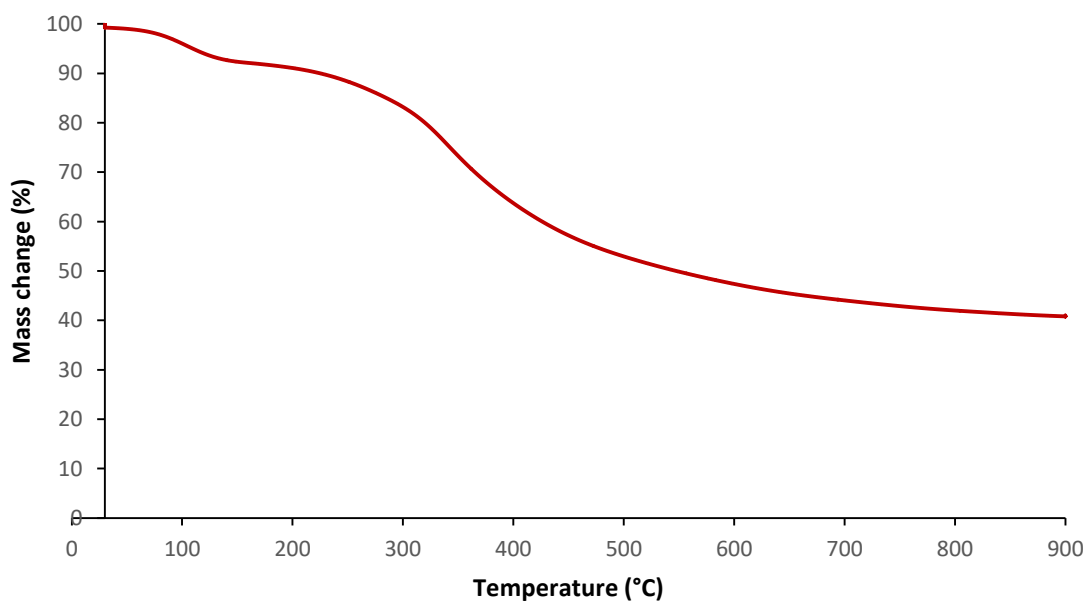


Fig. S10: TG analysis of lignin.

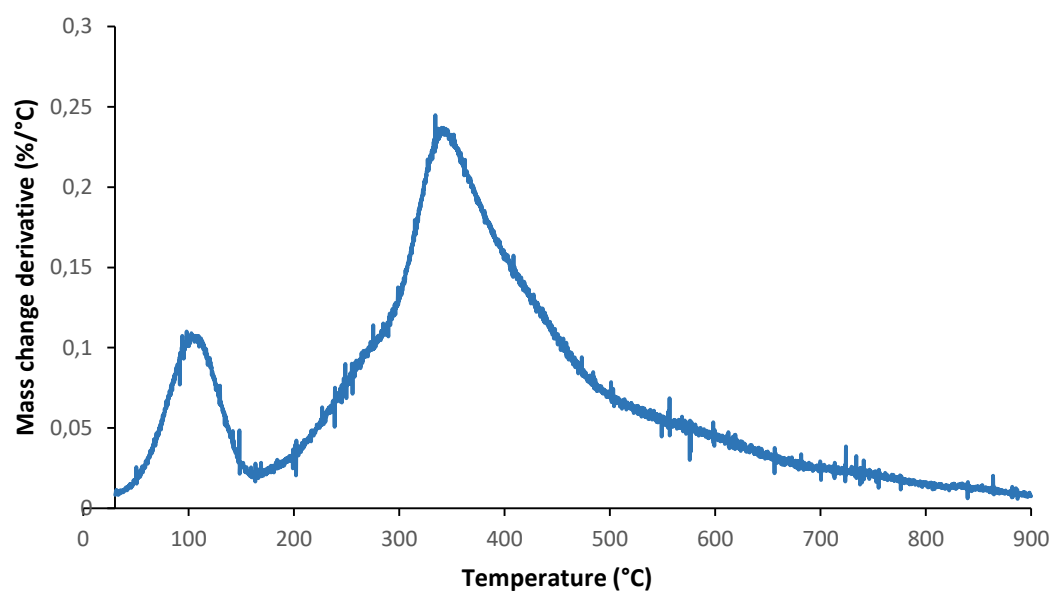


Fig. S11: DTG analysis of lignin.



Fig. S12: Biomass fragmentation of GS during cascade process.

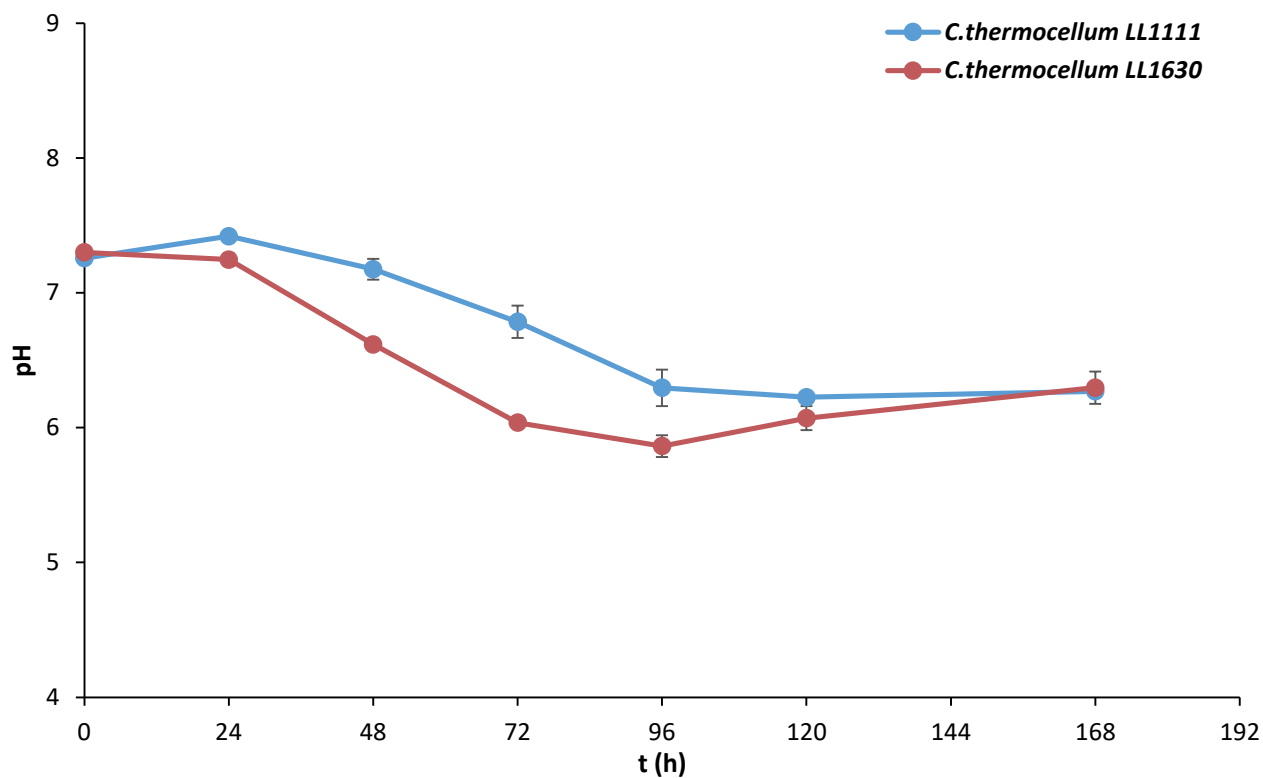


Fig. S13: pH evolution during flask fermentation of Avicel®.

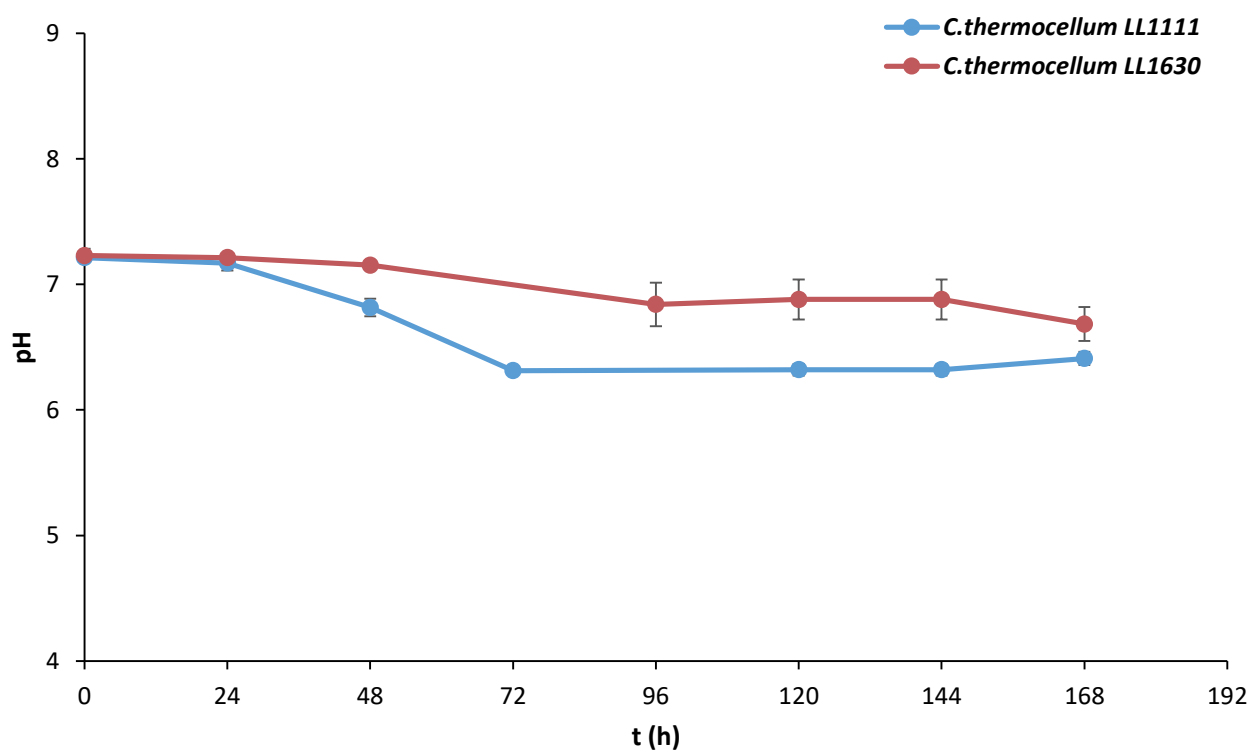


Fig. S14: pH evolution during flask fermentation of S2.

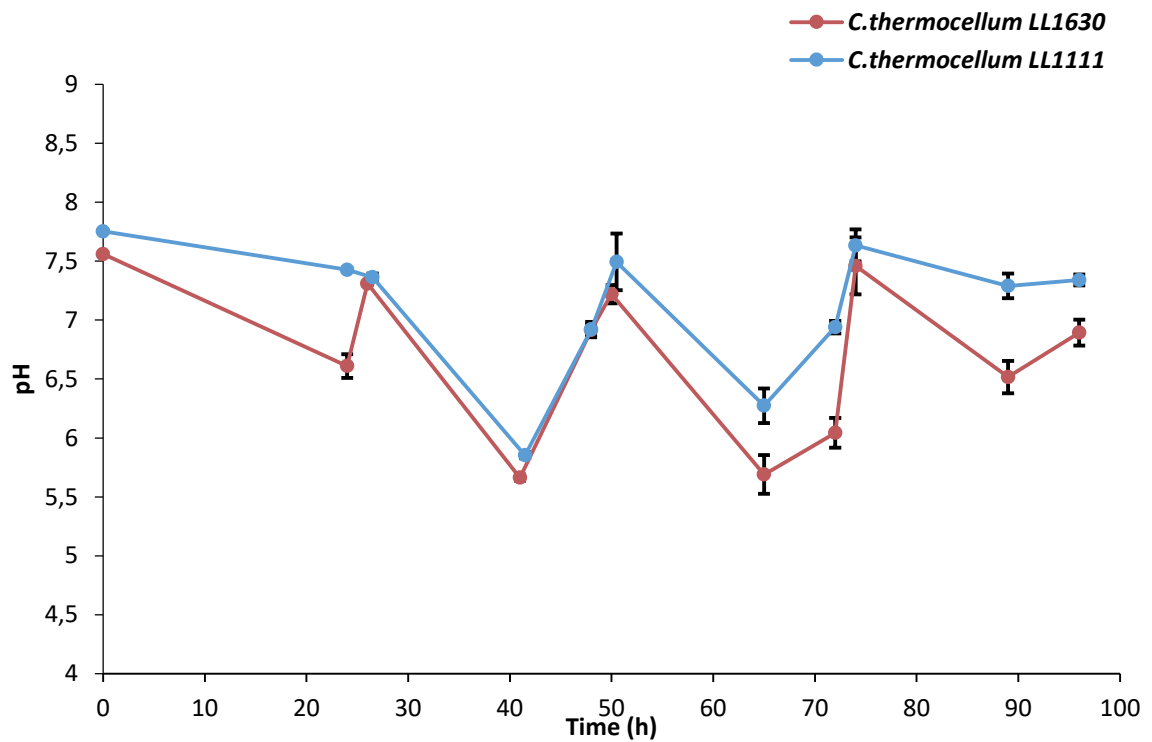


Fig. S15: pH evolution during bottle fermentation of Avicel® with manual pH regulation.

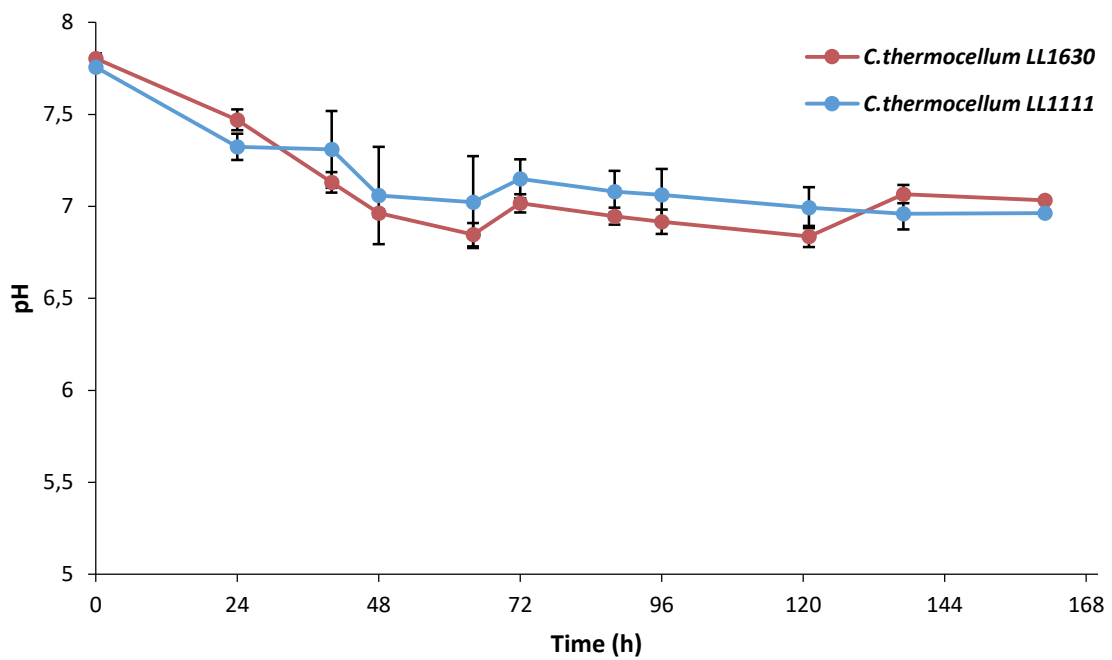


Fig. S16: pH evolution during bottle fermentation of S2 with manual pH regulation.