

Article



# The Development and Optimization of Hot-Melt Extruded Amorphous Solid Dispersions Containing Rivaroxaban in Combination with Polymers

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Abstract: Rivaroxaban (RXB), a novel oral anticoagulant that directly inhibits factor Xa, is a poorly soluble drug belonging to Biopharmaceutics Classification System (BCS) class II. In this study, a hot-melt extruded amorphous solid dispersion (HME-ASD) containing RXB is prepared by changing the drug:polymer ratio (Polyvinylpyrrolidione-vinyl acetate 64, 1:1–1:4) and barrel temperature (200-240 °C), fixed at 20% of Cremophor® RH 40 and 15 rpm of the screw speed, using the hot-melt extruding technique. This study evaluates the solubility, dissolution behavior, and bioavailability for application to oral drug delivery and optimizes the formulation of rivaroxaban amorphous solid dispersion (RXB-ASD). Based on a central composite design, optimized RXB-ASD (PVP VA 64 ratio 1:4.1, barrel temperature 216.1 °C, Cremophor® RH 40 20%, screw speed 15 rpm) showed satisfactory results for dependent variables. An in vitro drug dissolution study exhibited relatively high dissolution in four media and achieved around an 80% cumulative drug release in 120 min. Optimized RXB-ASD was stable under the accelerated condition for three months without a change in crystallinity and the dissolution rate. A pharmacokinetic study of RXB-ASD in rats showed that the absorption was markedly increased in terms of rate and amount, i.e., the systemic exposure values, compared to raw RXB powder. These results showed the application of quality by design (QbD) in the formulation development of hot-melt extruded RXB-ASD, which can be used as an oral drug delivery system by increasing the dissolution rate and bioavailability.

**Keywords:** rivaroxaban (RXB); amorphous solid dispersion (ASD); hot-melt extruding technique; quality by design (QbD); bioavailability

# 1. Introduction

Rivaroxaban (RXB), an anticoagulant agent and the active ingredient in Xarelto<sup>®</sup> tablets, is used to treat deep vein thrombosis (DVT) and pulmonary embolism (PE). RXB does not require a cofactor for activity since RXB inhibits free factor Xa (FXa) and prothrombinase activity [1] compared to anticoagulant drugs such as vitamin K and warfarin that are not widely used in the clinic due to their toxic side effects. However, RXB is classified as a Biopharmaceutics Classification System Class II (BCS Class II) drug and it has low solubility (20  $\mu$ g/mL) in aqueous solutions. There have been several attempts in the preparation of polymeric amorphous solid dispersions (ASDs) containing RXB [2,3]. To improve the solubility, various techniques such as liposomes, nanosuspensions, solid



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**Copyright:** © 2021 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license (https:// creativecommons.org/licenses/by/ 4.0/). dispersions, and cyclodextrin inclusions were tested [4–7]. Solvent evaporation, freezedrying, supercritical fluid method, spray drying, and thermal melting are applied in the manufacture of solid dispersion systems [8–15]. Hot-melt extrusion (HME), used for ASDs of poorly water-soluble active pharmaceutical ingredients (APIs), is a complex commercialized technique. In comparison to traditional methods of preparation of ASDs, HME is the most promising solvent-free, continuous, industry feasible, and scalable process for preparation of ASDs [16]. It is possible to improve the stability by preventing hydrolysis and oxidation and reducing residence times at high temperatures and screw rotation. During the preparation of such ASDs, the API is usually mixed/extruded with a molten of thermos-softened polymer.

Recently, many studies have been conducted on methods of preparing physically stable ASDs using polymer mixtures and the QbD approach, which allows for enhancing pharmaceutical development through design efforts from product development conceptualization to its commercialization [17–22]. The design of experiments (DoEs) for the drug development and product process is classified into screening design, factorial design, and response surface methodology (RSM). RSM is used to estimate possible effects, quadratic effects, the shape of the response surface, and interactions, and is positively applied to pharmaceutical development because there can be a variation of only one parameter at a time, keeping other parameters constant, although two or more variables can be studied simultaneously [23,24]. In addition, RSM has the advantage in terms of reduced process variability, higher percentage yields, lower treatment time, and cost-effectiveness. It estimates the relative significance of different variables.

However, a systemic attempt using the QbD to improve the solubility of RXB has not been reported in HME-based ASDs, although there are several approaches of preparation of polymeric ASDs containing RXB [2,3]. Therefore, HME-based ASD on RXB using optimal polymer combination was developed in terms of improvement of the dissolution behavior and oral bioavailability, based on the experimental design method of RSM.

#### 2. Materials and Methods

#### 2.1. Materials

RXB (purity > 98.5%; Hanseo Chemical, Pyeongtaek, Korea) and Xarelto<sup>®</sup> tablets (20 mg, Bayer, Luverkusen, Germany) were purchased.

Polyvinylpyrrolidone-vinyl acetate 64 (PVP VA 64, Kollidone<sup>®</sup> VA 64), Soluplus<sup>®</sup> (Polyvinyl caprolactam-polyvinyl acetate-polyethylene glycol graft co-polymer), Cremophor<sup>®</sup> RH 40 (PEG-40 hydrogenated castor oil), polyvinylpyrrolidone K 90 (PVP 90), Solutol<sup>®</sup> HS 15 (Polyoxyl 15-hydroxystearate), and Kolliphor<sup>®</sup> 188 (Poloxamer 188) were obtained from BASF (Ludwigshafen, Germany). Polyvinylalcohol (PVA, MW 89,000–98,000) was purchased from Sigma (St. Louis, MO, USA), and polyethylene glycol (PEG) was purchased from Daejung (Seoul, Korea). Gelucire<sup>®</sup> 44/14 (Lauroyl polyoxy-32-glycerides) and Gelucire<sup>®</sup> 50/13 (Stearoyl macrogol-32 glycrides) were obtained from Gattefosse (Saint-Priest, France). Carboxymethyl cellulose (CMC) and hydroxypropyl cellulose (HPC) were purchased from J.T. Baker (Seoul, Korea). All the other chemicals and reagents used were of analytical grade.

## 2.2. Before the Study

# 2.2.1. Selection of a Carrier

To study critical material attributes (CMA), first of all, a 1% aqueous solution containing various polymers and surfactants was prepared, and we added various amounts of RXB to determine how much of it dissolved in the solution. The mixtures were stirred continuously for 72 h at  $25 \pm 0.5$  °C and centrifuged at 15,000 rpm for 5 min; then, the supernatants were filtered through membrane filters (0.45 µm, Whatman, PA, USA). The filtrates were diluted in solution (chloroform: methanol = 1:7 (v/v, %), and the concentration of RXB was quantified. Next, by changing the concentration of various polymers and surfactants in aqueous solution from 0.5% to 10% (w/w, i.e., 0.5%, 1%, 2%, 5%, and 10%), the maximum concentration of RXB that could be dissolved was determined.

The concentration of RXB was analyzed by an HPLC (Shimadzu, Japan) system; the system featured an LC10-AD isocratic pump, a SPD-10A VP variable spectrophotometric detector, and a Shimpak GIS ODS column (5  $\mu$ m pore diameter; 4.6  $\times$  150 mm, Shimadzu, Japan). An acetonitrile/water mixture (55/45, v/v, %) served as the mobile phase; the flow rate was 1.2 mL/min, and the detection wavelength was 250 nm. The RXB calibration curve was linear (r = 0.9999) over the concentration range of 0.625–200  $\mu$ g/mL.

## 2.2.2. HME Process Condition

The solubility and dissolution of RXB-ASDs were selected as critical process parameters (CPP) in HME technology. RXB-ASDs were prepared by alternating the barrel temperatures between 140 °C, 180 °C, 200 °C, 220 °C, and 240 °C and the screw speeds between 10, 15, and 20 rpm for a Haake Mini CTW hot-melt extruder (Thermo Scientific Inc., Waltham, MA, USA) fixed at a weight polymer ratio of 1:4 (RXB: Soluplus<sup>®</sup>). The effect of screw speed on solubility was observed by adjusting the screw speed to 10, 15, or 20 rpm with the temperature fixed at 200 °C.

Next, after fixing the temperature and screw speed, the effects on the solubility and dissolution at 6 h in SGF (pH 6.8) of RXB-ASDs, prepared as shown in Figure 1 with various polymer compositions (Table 1), were evaluated.

| RXB and poly     | mer (or surfactant) mixture by ratio  |  |  |  |  |
|------------------|---|--|--|--|--|
|                  | ← Mixed for 30 min<br>←Adding solubilizing agent (solubilizer)<br>← Kneading for 30 min |  |  |  |  |
|                  | Physical mixture  |  |  |  |  |
|                  | ← Barrel temperature: 200 °C<br>← Screw speed: 15 rpm                                   |  |  |  |  |
| Hot melt extr    | uded RXB-ASD (filament or pellet)   |  |  |  |  |
|                  | ← Grinding for 10 min<br>← Sieving (<355 μm)  |  |  |  |  |
| RXB-ASD (powder) |   |  |  |  |  |

Figure 1. Preparation process of hot-melt extruded RXB-ASD.

|             |     |           | τ         | v/w Rati | D                               |                                |                  | nt (%) Dissolution<br>Rate (%) |  |  |  |
|-------------|-----|-----------|-----------|----------|---------------------------------|--------------------------------|------------------|--------------------------------|--|--|--|
| Formulation | RXB | Soluplus® | PVP VA 64 | PVA      | Cremophor <sup>®</sup><br>RH 40 | Gelucire <sup>®</sup><br>50/13 | Content (%)      |                                |  |  |  |
| F1          | 1   | 2         | _         | -        | -                               | -                              | $89.63 \pm 3.31$ | $24.52\pm4.13$                 |  |  |  |
| F2          | 1   | 4         | -         | -        | -                               | -                              | $90.56 \pm 4.36$ | $24.66 \pm 12.94$              |  |  |  |
| F3          | 1   | -         | 2         | -        | -                               | -                              | $94.05\pm3.33$   | $46.57\pm0.57$                 |  |  |  |
| F4          | 1   | -         | 4         | -        | -                               | -                              | $97.01 \pm 1.24$ | $51.89 \pm 0.46$               |  |  |  |
| F5          | 1   | 2         | 2         | -        | -                               | -                              | $91.26\pm6.77$   | $18.83 \pm 4.32$               |  |  |  |
| F6          | 1   | 4         | -         | 1        | -                               | -                              | $76.05\pm2.23$   | $52.72 \pm 2.19$               |  |  |  |
| F7          | 1   | 4         | -         | -        | 1                               | -                              | $92.48 \pm 1.33$ | $35.82\pm6.61$                 |  |  |  |
| F8          | 1   | 4         | -         | -        | -                               | 1                              | $93.70 \pm 1.48$ | $33.44 \pm 0.48$               |  |  |  |
| F9          | 1   | -         | 4         | 1        | -                               | -                              | $73.78 \pm 1.77$ | $80.80 \pm 1.16$               |  |  |  |
| F10         | 1   | -         | 4         | -        | 1                               | -                              | $93.58 \pm 1.26$ | $83.29\pm0.33$                 |  |  |  |
| F11         | 1   | -         | 4         | -        | -                               | 1                              | $95.38 \pm 1.26$ | $73.80\pm3.76$                 |  |  |  |

Table 1. Formulation of hot-melt extruded RXB-ASDs using various polymer mixtures.

#### 2.2.3. Preformulation Study of RXB-ASDs Using a Full Factorial Design (FFD)

Based on the results of failure mode effect analysis (FMEA), with a preformulation experimental design with a hot-melt extruder at a 15 rpm screw speed, the effect of independent variables (PVP VA 64 ratio (X1, 1:1, 1:2, 1:4), total weight of Cremophor<sup>®</sup> RH 40 (X2, 0, 10, 20 w/w%) and barrel temperature (X3, 180, 200, 220 °C) on dependent variables (content (Y1) and the dissolution rate at 6 h in SIF (Y2)) was monitored (Table 2).

**Independent Variables Dependent Variables** X2 Y1 Y2 X1 X3 1 0 180 92.32 48.55 1 0 200 101.52 41.17 1 0 220 94.75 33.90 10 1 180 97.01 44.46 1 10 200 99.49 43.00 1 10 220 96.82 42.30 1 20 180 107.36 40.88 1 20 200 97.98 42.71 20 1 220 88.12 45.27 2 0 180 88.09 48.96 2 0 200 51.30 86.67 2 0 220 91.29 75.32 2 10 180 97.71 44.82 2 10 200 101.77 43.91 2 10 220 77.17 95.68 2 20 180 94.13 44.41 2 20 200 90.45 49.01 2 20 220 101.68 80.51 4 0 180 95.40 60.62 4 0 200 97.76 64.29 4 0 220 105.12 73.36 4 10 94.81 180 53.18 4 10 200 105.81 68.05 4 10 220 97.63 84.40 20 93.35 4 180 50.96 4 20 200 98.53 79.89 4 20 220 96.31 87.40

Table 2. Preformulation experimental design of hot-melt extruded RXB-ASDs.

X1, the PVP VA64 ratio; X2, Cremophor<sup>®</sup> RH40 w/w%; X3, barrel temperature (°C); Y1, the content (%); Y2, the dissolution rate (%) in SIF (6 h).

#### 2.3. Optimization by Central Composite Design (CCD)

Based on preformulation results, the RXB-ASD experimental design and data analysis were conducted using the central composite design module in Minitab version 18 software (Minitab Inc., State College, PA, USA). The RSM central composite design method was used to optimize critical factors at 20% of Cremophor<sup>®</sup> RH 40 and 15 rpm screw speed. The effect of the independent variables such as the polymer ratio (X1, 1:2–1:4) and barrel temperature (X2, 200–220 °C) on the dependent variables such as the content (Y1) and dissolution rate at 2 h (Y2) and 6 h (Y3) in SGF (pH 1.2) and the dissolution rate at 2 h (Y4) and 6 h (Y5) in SIF (pH 6.8) was evaluated.

The linear equation of the model is as follows:

$$Y = A0 + A1 \cdot X1 + A2 \cdot X2 + A3 \cdot X1 \cdot X1 + A4 \cdot X2 \cdot X2 + A5 \cdot X1 \cdot X2$$

where Y is the response of the dependent variables associated with each factor-level combination; A0 is the intercept; A1, A2, A3, A4, and A5 are the regression coefficients; and X1 and X2 are the independent variables.

The data were fitted to a second-order polynomial equation, and regression coefficients were obtained. Analysis of variance (ANOVA) was conducted to evaluate the significance and adequacy of the developed regression model. The adequacy of the response surface models was clarified by the determination coefficient ( $R^2$ ) and the lack of fit.

One-way ANOVA and multiple regression analysis were performed to test the significance of the model and factor coefficients. The polynomial, plots, and two-contour plots also revealed the interactions between each independent variable.

After generating the polynomial equations relating to the dependent and independent variables, optimization of the dependent variables (Y1, Y2, Y3, Y4, and Y5) was performed using a desirability function to obtain the levels of X1 and X2 that maximized the dependent variable.

#### 2.4. Physicochemical Evaluation of RXB-ASD

The calorimetric responses of samples were recorded on a differential scanning calorimetry (DSC) system (N-650, Scinco, Korea) equipped with a refrigerated cooling system, calibrated for temperature and heat flow using a high-purity indium standard. The sample cell was purged with dry nitrogen at a flow rate of 40 mL/min. The 3–5-mg samples were laid on crimped aluminum pans and measured at a heating rate of 20 °C/min up to 250 °C.

Powder X-ray diffraction (PXRD patterns of different samples were recorded at room temperature using a Smartlab X-ray diffractometer (Rigaku Mechatronics Co. Ltd., Tokyo, Japan) equipped with a 2 $\theta$  compensating slit, using Cu K $\alpha$  radiation (1.5406 Å) at 45 kV and 200 mA passing through a nickel filter with an IS slit (0.5°), a soller slit (5°), and receiving slit (20 mm). Samples were mounted on a zero-background sample holder and subjected to a continuous scan over a Bragg angle 2 $\theta$  range of 2–35° at a step size of 0.01° and scan rate of 5°/min. Obtained diffractograms were analyzed with the PDXL processing program.

To monitor the intermolecular interaction between drug and polymers, the crystalline RXB and ASD were monitored with FT-IR by a conventional KBr pellet method using an FTIR-4100 spectrophotometer (JASCO, Tokyo, Japan).

The surface morphology of powder samples was monitored under a scanning electron microscope (SEM) (S-3400, Hitachi, Ltd., Tokyo, Japan) with an excitation voltage of 25 kV. The powder samples were mounted onto a steel stage and sputter-coated with gold using ion sputtering (E-1010, Hitachi, Ltd.) prior to analysis.

#### 2.5. Drug Content, In Vitro Dissolution Test, and Food Effect

For quantification of the drug content, RXB-ASDs containing 2 mg of RXB were dissolved in 2 mL of dimethyl sulfoxide. After stirring for 3 h, the solution was filtered with a membrane and diluted 100-fold (0.1 mL of filtrate in a total volume of 10 mL) in the solution (chloroform: methanol = 12.5:87.5, v/v%). The concentration of RXB in the diluted solution was quantified using HPLC.

Dissolution was tested using a dissolution tester (DRS-14, Labbindia, India) with 900 mL distilled water (DW), SGF (pH 1.2), acetate buffer (pH 4.0), and SIF (pH 6.8), via agitation with a paddle at 75 rpm and  $37 \pm 0.5$  °C.

The optimized RXB-ASD sample, placed within a hard gelatin capsule (size number 2) containing equivalent amounts of RXB (20 mg) in a sinker, was placed in a dissolution medium, and 5-mL aliquot samples were withdrawn at certain time intervals (0.10, 30, 60, 120, 240, and 360 min) and filtered using a membrane filter (0.45  $\mu$ m, Whatman, PA, USA). The filtered samples were diluted with a chloroform and methanol mixture (1:7 v/v%), and the concentration of the drug was determined by HPLC. The release rates were compared with those of a conventional tablet (Xalretol<sup>®</sup>, 20 mg as RXB), with RXB powder as a negative control.

To investigate the effect of food on optimized RXB-ASD, the dissolution rate was monitored for fasted-state simulated gastric fluid (FaSSGF), fed-state simulated gastric fluid (FeSSGF), fasted-state simulated intestinal fluid (FaSSIF), and fed-state simulated intestinal fluid (FeSSIF).

The similarity of release profiles between the test preparation and reference preparation in different dissolution media was evaluated as the similarity factor,  $f_2$ . The relevant equation is as follows [24,25]:

$$f_2 = 50 \times \log \left\{ \left[ 1 + \frac{1}{n} \sum_{i=1}^n |R_j - T_j|^2 \right]^{-0.5} \times 100 \right\}$$

where *n* is the number of sampling time points, and *R* and *T* represent the cumulative dissolution of the drug at the specified time point in the respective reference formulation and the test formulation. The value of  $f_2$  ranged from 0 to 100; when the value exceeded 50, the drug release profiles between the reference formulation and test formulation were considered to be similar.

## 2.6. Stability

To check the stability, hard gelatin capsules (size number 2) filled with RXB-ASD were submitted to accelerated degenerative conditions ( $40 \degree C/75\%$  RH). The appearance, drug content, and in vitro dissolution rates were evaluated for three months.

# 2.7. Application to Pharmacokinetic Study

RXB and RXB-ASD were administered orally at dose of 10 mg/kg to elucidate the absorption in male Sprague–Dawley rats aged seven weeks and weighing 199–225 g (Orient Bio, Seongnam, Korea). In addition, to monitor the bioavailability, RXB-ASD was administered intravenously at dose of 2 mg/kg. For all experiments, the animals were kept in plastic cages with free access to a standard rat diet (PMI Nutrition International, Richmond, IN, USA) and water at a temperature of 20–26 °C, with a 12 h light–dark cycle and a relative humidity of 40–60% under the guidance of the Institutional Animal Care and Use Committee of Chungnam National University (202003A-CNU-055, 23 June and 8 August 2020, Daejeon, Korea).

Prior to dosing, animals were fasted for 14 h and provided with free access to water after a further 4 h. RXB was homogenized in normal saline and administered for oral administration at a volume of 5 mL/kg and solubilized in mixture composed of 10% DMSO, 40% PEG 400, and 50% normal saline for intravenous injection at a volume of 2 mL/kg. Blood samples (300  $\mu$ L) were obtained from the jugular vein at 0.0167, 0.33, 1, 2, 4, 8, 12, and 24 h after oral dosing and at 0.083, 0.25, 0.5, 1, 2, 5, 8, and 24 h after intravenous dosing in four animals per group. The blood samples were immediately centrifuged at 17,600× g for 5 min, and the separated plasma samples were stored at -20 °C until analysis.

With respect to RXB in rat plasma, the bioanalytical method for RXB in rat plasma was adjusted and optimized based on a previously established method [26]. LC used a 1200 series system from Agilent Technologies (Santa Clara, CA, USA) composed of a binary pump, degasser, autosampler, and column oven. A Zorbax phenyl column ( $50 \times 2.1$  mm, 5 µm particle size; Agilent, Santa Clara, CA, USA) was used with the mobile phase consisting of (A) 10 mM ammonium formate containing 0.1% formic acid of total volume in water (pH 4.5) and (B) methanol with gradient elution at a 0.3 mL/min flow rate. Samples (2 µL) were analyzed using the following isocratic mode for 3 min with a composition of 40% A and 60% B. The temperatures of the column oven and autosampler were maintained at 40 °C and 10 °C, respectively.

MS was performed on the API 4000 Qtrap LC-MS/MS system (AB Sciex, Framingham, MA, USA) operated in the negative ion mode. The ion source parameters were set as follows: curtain gas 20 psi, ion spray voltage 5500 V, ion source temperature 600 °C, nebulizing gas (GS1) 60 psi, drying gas (GS2) 50 psi. The MS parameters of declustering potential and collision energy for RXB were optimized at 86 V and 37 V, respectively, and those for the internal standard were optimized at 81 V and 25 V, respectively. The ion

transitions in multiple-reaction monitoring (MRM) were monitored at m/z 436.2 $\rightarrow$ 145.0 for RXB and m/z 338.2 $\rightarrow$ 296.1 for linezolid, an internal standard. The data were acquired using Analyst (version 1.4.2) from AB Sciex.

The pharmacokinetic analysis was performed by a noncompartmental analysis using Phoenix WinNonlin<sup>®</sup> 8.1 (Pharsight Corp., Cary, NC, USA). The peak plasma concentration  $(C_{max})$  and the time to reach the peak concentration  $(T_{max})$  were obtained directly from the profile of the time-plasma concentration. The elimination rate constant  $(K_{el})$  was determined by linear regression in the terminal phase. The half-life  $(T_{1/2})$  in the terminal phase was calculated by dividing ln 2 by the  $K_{el}$ . In addition, we determined the systemic clearance (CL), the volume of distribution  $(V_d)$ , and mean residence time (MRT). The area under the plasma concentration-time curve from time zero to infinity (AUC<sub>inf</sub>) was calculated via the linear trapezoidal rule and the standard area extrapolation method [27].

#### 3. Results and Discussion

3.1. Before the Study

3.1.1. Selection of Carrier

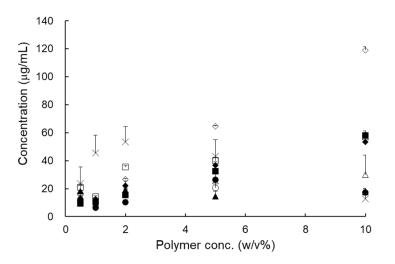
CMA and CPP were selected by FMEA. The CMAs were the type and ratio of the polymer, plasticizer, and polymer combination, and the CPPs were the barrel temperature and screw speed.

The components used should solubilize the drug and ensure continuing solubility in the ultimate dispersion. The solubility of RXB in distilled water is  $0.09 \pm 0.00 \,\mu\text{g/mL}$ , which makes it a very poorly soluble drug. Among the polymers, Cremophor<sup>®</sup> RH 40 showed high-solubilizing capacities for RXB and was  $30.33 \pm 5.24 \,\mu\text{g/mL}$ . However, most polymer solutions, except for HPC and HPMC, had values less than 10  $\mu\text{g/mL}$  (Table 3).

| Polymer         | Solubility (µg/mL) | Polymer                      | Solubility (µg/mL) |
|-----------------|--------------------|------------------------------|--------------------|
| Distilled water | $0.09\pm0.00$      | HPC-L                        | $5.79\pm0.02$      |
| PVP VA 64       | $8.82\pm0.16$      | Poloxamer 188                | $9.67\pm0.09$      |
| PVP K90         | $6.32\pm0.02$      | Solutol <sup>®</sup> HS 15   | $12.45\pm0.12$     |
| PVA             | $29.30\pm8.76$     | Soluplus <sup>®</sup>        | $9.25\pm0.04$      |
| PEG 200         | $12.38 \pm 1.71$   | Gelucire <sup>®</sup> 44/14  | $11.00\pm0.02$     |
| PEG 4000        | $10.76\pm0.21$     | Gelucire <sup>®</sup> 50/13  | $14.23\pm0.06$     |
| PEG 10000       | $8.97\pm0.14$      | Labrasol®                    | $6.02\pm0.60$      |
| PEG 20000       | $9.02\pm0.09$      | Cremophor <sup>®</sup> RH 40 | $30.33 \pm 5.24$   |
| HPMC 4M         | $6.47\pm0.26$      | Cremophor <sup>®</sup> EL    | $10.44 \pm 1.51$   |
| HPMC 15M        | $5.12\pm0.07$      | Tween 80                     | $12.59 \pm 1.07$   |

**Table 3.** Solubility of RXB in 1% aqueous polymer solution (n = 3, means  $\pm$  SD).

The solubility of RXB, according to the polymer concentration, was significantly increased in Soluplus<sup>®</sup> and PVP VA 64 (Figure 2). However, the solubility increased by 2% and then decreased in Gelucire<sup>®</sup> 50/14 and PVA. Finally, based on these results, a combination of PVP VA 64 and Cremophor<sup>®</sup> RH 40 (or Soluplus<sup>®</sup>) was selected for the preparation of RXB-ASDs using HME technology.



**Figure 2.** Solubility of RXB according to the aqueous polymer solution concentration (n = 3, means  $\pm$  SD). (Key:  $\blacksquare$ : Gelucire<sup>®</sup> 44/14,  $\Box$ : Gelucire<sup>®</sup> 50/13,  $\blacklozenge$  Solutol<sup>®</sup> HS 15,  $\blacktriangle$ : PEG 4000,  $\triangle$ : PEG 20,000,  $\bigcirc$ : PVP VA 64,  $\bullet$ : PVP K 90,  $\times$ : PVA,  $\diamond$ : Soluplus<sup>®</sup>.

# 3.1.2. HME Process Conditions

In general, to prepare thermodynamically stable ASD using hot-melt extrusion, high temperatures above the melting point of API are avoided [28]. Therefore, the processing temperatures were selected based on  $T_g$  of the blend of the polymeric system (i.e., 180–240 °C) and a melting point of API (i.e., 228–234 °C) to obtain well-solidified extrudates.

When RXB-ASDs were prepared with various barrel temperatures and screw speeds, the solubility increased as the barrel temperature increased, but was not affected by the screw speed (data not shown).

When RXB-ASDs were prepared at 200 °C barrel temperature and 15 rpm screw speed, the content of RXB was approximately 90–100% except for the PVA formulation (F6 and F9). This is thought to be due to the relatively high viscosity of PVA.

The dissolution rate was higher in formulations with the polymer mixture than in the polymer alone. In the formulations of F9 and F10 with PVP VA 64 and Cremophor<sup>®</sup> RH 40 (or PVA), the dissolution rates were  $80.80 \pm 1.16$  and  $83.29 \pm 0.33\%$ , respectively (Table 1). By comparison, the formulation of F4, which used the polymer alone, had a rate of 51.89% and the value increased by approximately 160%, which indicated that PVP VA 64 and Cremophor<sup>®</sup> RH 40 (or PVA) can be recommended to increase the dissolution rate.

# 3.1.3. Preformulation Study of RXB-ASDs by FFD

Considering the thermodynamic stability of API, the critical process factors were selected as follows: 200-240 °C barrel temperature,  $1:1\sim1:4$  PVP VA 64 ratio, and 0-20% Cremophor<sup>®</sup> RH 40 based on the total weight.

After evaluating the contents and dissolution rate of the RXB-ASDs, prepared according to the FFD, multiple regression analysis was performed (data not shown). That is, the content was approximately 90–105% and was not significantly affected by the independent variables. However, the dissolution rate was significantly affected by the ratio of PVP VA 64 and the barrel temperature (p < 0.05) and increased sharply over 1:2 and 200 °C. In addition, the dissolution rate increased by more than 15% with Cremophor<sup>®</sup> RH 40, but this result was not significant; it had a significant interaction with the PVA VA64 barrel temperature. Therefore, in the present study, to obtain solid and free-flow powder, the content of Cremophor<sup>®</sup> RH 40 was set to 20% (w/w) of the total weight.

## 3.2. Optimization by CCD

Based on the results of the preformulation study in Section 3.1.3, the independent variables were the ratio (X1) of PVA VA 64 and the barrel temperature (X2). The results of

the dependent variable for the central synthesis design and the regression variance analysis for the quadratic term for the model fit (p < 0.05) and the multiple correlation coefficients are shown in Tables 4 and 5. In addition, the response surface method and contour plot are shown in Figures 3 and 4.

| Independe | ent Variable |        | De    | pendent Varia | dent Variable |       |
|-----------|--------------|--------|-------|---------------|---------------|-------|
| X1        | X2           | Y1     | Y2    | ¥3            | Y4            | ¥5    |
| 1.59      | 210          | 91.60  | 44.25 | 49.46         | 49.85         | 54.42 |
| 2         | 220          | 98.44  | 44.16 | 55.30         | 54.66         | 62.36 |
| 2         | 200          | 97.87  | 42.01 | 43.33         | 46.38         | 49.11 |
| 3         | 224.14       | 99.99  | 57.60 | 74.58         | 65.00         | 78.32 |
| 3         | 210          | 101.69 | 67.85 | 71.93         | 71.49         | 75.48 |
| 3         | 210          | 100.15 | 64.45 | 71.70         | 67.83         | 75.39 |
| 3         | 195.86       | 94.80  | 53.94 | 54.37         | 63.62         | 72.17 |
| 3         | 210          | 98.78  | 69.54 | 74.86         | 73.59         | 78.83 |
| 3         | 210          | 99.14  | 63.98 | 73.55         | 67.67         | 78.05 |
| 3         | 210          | 102.54 | 63.29 | 73.33         | 66.77         | 77.37 |
| 4         | 200          | 97.84  | 63.79 | 77.08         | 69.79         | 85.27 |
| 4         | 220          | 101.22 | 70.06 | 80.23         | 76.71         | 85.24 |
| 4.41      | 210          | 96.65  | 67.29 | 78.58         | 75.68         | 84.62 |

Table 4. Experimental design of hot-melt extruded RXB-ASDs by CCD.

X1, the PVP VA64 ratio; X2, the barrel temperature ( $^{\circ}$ C); Y1, the content ( $^{\circ}$ ); Y2, the dissolution rate ( $^{\circ}$ ) in SGF (2 h); Y3, the dissolution rate ( $^{\circ}$ ) in SGF (6 h); Y4, the dissolution rate ( $^{\circ}$ ) in SIF (2 h); Y5, the dissolution rate ( $^{\circ}$ ) in SIF (6 h).

## Table 5. ANOVA results for all responses.

|                                      |                       | Parameter               |              |  |
|--------------------------------------|-----------------------|-------------------------|--------------|--|
| Variable —                           | <i>p</i> -Value       | R <sup>2</sup>          | Lack of Fit  |  |
| Y1: Content (%)                      | 0.092                 |                         |              |  |
| X1: Polymer ratio                    | 0.153                 |                         |              |  |
| X2: Barrel Temp.                     | 0.110                 | 0 ( 0 2 0               | 0.1/5        |  |
| X1·X1                                | 0.023                 | 0.6820                  | 0.165        |  |
| X2·X2                                | 0.388                 |                         |              |  |
| X1·X2                                | 0.540                 |                         |              |  |
|                                      | Regressio             | on equation             |              |  |
| Y1 = -246 + 0                        | .9X1 + 3.13X2 - 2.397 | X1·X1 - 0.000762X2·X2 + | + 0.070X1·X2 |  |
| Y2: Dissolution rate<br>(%)—SGF, 2 h | 0.000                 |                         |              |  |
| X1: Polymer ratio                    | 0.000                 |                         |              |  |
| X2: Barrel Temp.                     | 0.146                 | 0.9507                  | 0.367        |  |
| X1·X1                                | 0.002                 |                         |              |  |
| X2·X2                                | 0.002                 |                         |              |  |
| X1·X2                                | 0.506                 |                         |              |  |
|                                      | Regressic             | n equation              |              |  |
| Y2 = -2283 +                         | 19.7X1 + 2177X2 - 5.5 | 22X1·X1 - 0.0522X2·X2 + | 0.103X1·X2   |  |
| Y3: Dissolution rate<br>(%)—SGF, 6 h | 0.000                 |                         |              |  |
| X1: Polymer ratio                    | 0.000                 |                         |              |  |
| X2: Barrel Temp.                     | 0.002                 | 0.9628                  | 0.018        |  |
| X1·X1                                | 0.006                 |                         |              |  |
| X2·X2                                | 0.008                 |                         |              |  |
| X1·X2                                | 0.199                 |                         |              |  |

| Variable —                           | Parameter              |                        |              |  |
|--------------------------------------|------------------------|------------------------|--------------|--|
| variable —                           | <i>p</i> -Value        | $R^2$                  | Lack of Fit  |  |
|                                      | Regressior             | equation               |              |  |
| Y3 = -2184 +                         | 86.3X1 + 19.54X2 - 4.5 | 59X1·1 - 0.0437X2·X2 - | - 0.221X1·X2 |  |
| Y4: Dissolution rate<br>(%)—SIF, 2 h | 0.001                  |                        |              |  |
| X1: Polymer ratio                    | 0.000                  |                        |              |  |
| X2: Barrel Temp.                     | 0.100                  | 0.9344                 | 0.353        |  |
| X1·X1                                | 0.017                  |                        |              |  |
| X2·X2                                | 0.043                  |                        |              |  |
| X1·X2                                | 0.353                  |                        |              |  |
|                                      | Regressior             | equation               |              |  |
| Y4 = -1382 + 4                       | 0.0X1 + 12.89X2 - 3.7  | 7X1·X1 - 0.0299X2·X2 - | - 0.034X1·X2 |  |
| Y5: Dissolution rate<br>(%)—SIF, 6 h | 0.000                  |                        |              |  |
| X1: Polymer ratio                    | 0.000                  |                        |              |  |
| X2: Barrel Temp.                     | 0.025                  | 0.9668                 | 0.057        |  |
| X1·X1                                | 0.005                  |                        |              |  |
| X2·X2                                | 0.231                  |                        |              |  |
| X1·X2                                | 0.046                  |                        |              |  |
|                                      | Regressior             | equation               |              |  |
| Y5 = -866 + 10                       | 07.8X1 + 6.99X2 - 4.22 | X1·X1 - 0.0136X2·X2 -  | - 0.332X1·X2 |  |



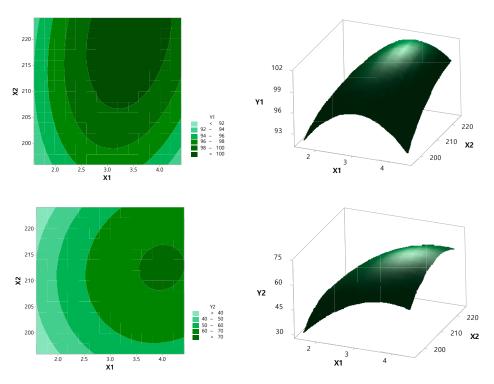
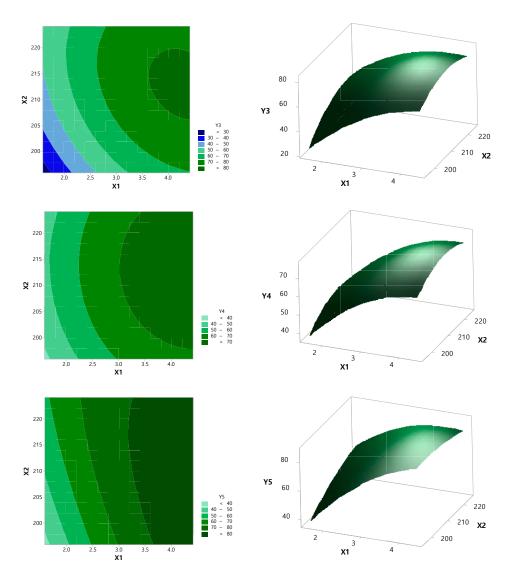


Figure 3. Cont.



**Figure 3.** Contour and 3D response surface plot of dependent variables against independent variables: X1, PVP VA64 ratio; X2, barrel temperature (°C); Y1, content (%); Y2, dissolution rate (%) in SGF (2 h); Y3, dissolution rate (%) in SGF (6 h); Y4, dissolution rate (%) in SIF (2 h); Y5, dissolution rate (%) in SIF (6 h).

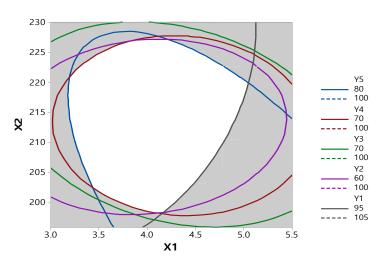
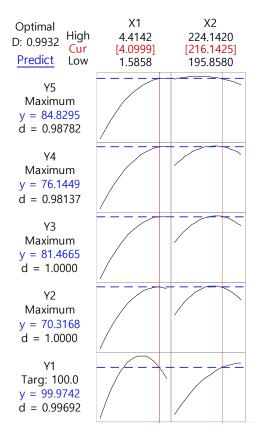


Figure 4. Nesting contour plot of dependent variables versus independent variables for all responses.

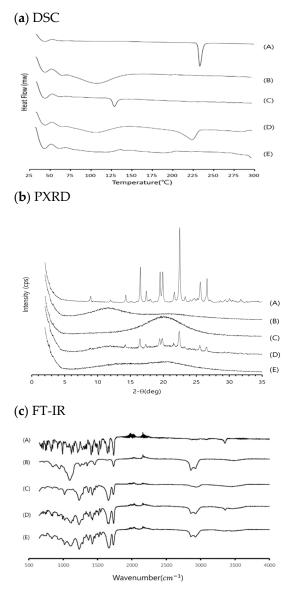
As the ratio of PVP VA 64 increased, the dissolution rate increased normally, then steeply to 1:3, and then became slower. This result is consistent with Pawar's study [29]. The enhancement in the dissolution rate of RXB-ASD may be due to the amorphous state drug that offers a lower thermodynamic barrier to dissolution. The glassy state of RXB-ASD yielded the highest solubility and dissolution rate because the drug is molecularly dispersed in a polymer mixture system resulting in the formation of an amorphous system. Other different factors that might contribute to the increase in the dissolution rate of RXB are increased wettability and hydrophilicity, improved dispersibility, and reduced particle size of the drug. In addition, as the barrel temperature increased to 215 °C, the dissolution rate increased, but it decreased above 220 °C. The contour plot at a content of 95–105% and also 60–70% for 2 h and 70–80% for 6 h of dissolution is shown in Figure 5. The ratio of RXB to PVP VA 64 and the barrel temperature were set to 1:4.099 and 216.1425 °C, respectively, to show the optimum dissolution rate at SGF (pH 1.2) or SIF (pH 6.8), which indicated that the values had a high prediction ability (99.32%).



**Figure 5.** Response optimization profile of dependent variables for independent variables of hot-melt extruded RXB-ASD.

#### 3.3. Physicochemical Evaluation of RXB-ASD

The DSC spectrum of RXB showed a sharp endothermic peak at 232.92 °C, which corresponds to its melting point. The distinct characteristic peak of RXB observed in the thermogram of the physical mixture signifies the existence of crystalline RXB. A shift (224.17 °C) in the characteristic endotherm of RXB was noticed along with a slightly reduced peak intensity which can be attributed to the partial interaction of RXB with PVP VA 64 (Figure 6a). However, the characteristic endotherm of RXB completely disappeared in optimized RXB-ASD, indicating an amorphous or molecular dispersion state. The formation of a disordered molecular structure or a reduction in the particle size of the drug can occur since the binding force between the drug molecules was weakened in the mixture of the drug and the polymer [30].



**Figure 6.** DSC (**a**), PXRD (**b**), and FT-IR (**c**) profiles of samples: (A) RXB, (B) PVP VA64, (C) Cremophor<sup>®</sup> RH 40, (D) physical mixture, and (E) optimized RXB-ASD.

Analysis of powder diffraction patterns of RXB showed a distinct crystalline phase with characteristic sharp peaks, confirming the polymorphic form I of RXB. The diffractogram of physical mixtures showed distinct characteristics peaks for RXB with/without reduced peak intensity, suggesting the existence of crystalline RXB in physical mixtures (Figure 6b). All the polymers showed a small and broad endotherm of moisture in DSC and a halo pattern in PXRD. Optimized RXB-ASD was found to be stable and showed the absence of crystallinity as evidenced by DSC and PXRD.

The FT-IR spectra of samples (RXB, PVP VA 64, Cremophor<sup>®</sup> RH 40, and RXB-ASD) at 500–4000 cm<sup>-1</sup> wavenumber are stacked for visual analysis in Figure 7c. RXB was identified by characteristic peaks at 3353 cm<sup>-1</sup> (N–H stretch), 1735 cm<sup>-1</sup> (C=O stretch), and 1590 cm<sup>-1</sup> (Ar-Cl stretch). On the whole, the spectrum of the RXB-ASD showed no significant differences from excipients, which indicated that no new chemical bonds were created in RXB-ASD and proved there was good compatibility between the drug and excipients.

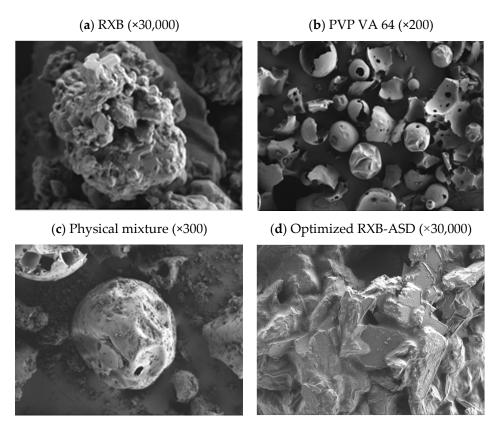
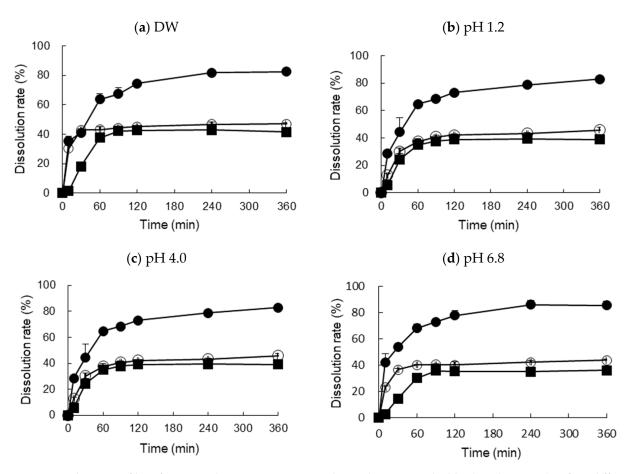


Figure 7. SEM images of samples: (a) RXB; (b) PVP VA64; (c) physical mixture; (d) optimized RXB-ASD.

SEM analysis of ASD is widely used to probe the particle morphology after the formation of amorphous dispersions, conducted to acquire the photomicrographs for RXB, polymers, and optimized RXB-ASD. RXB consists of a mixture of large and small particles deposited with microparticles, which could be due to micronization or any other size reduction processes at the time of manufacturing (Figure 7). The PVP VA 64 has spherical particles with a smooth surface. RXB-ASD showed morphologies consisting of a collapsed and corrugated surface without crystallinity, indicating that the binding force between molecules was reduced and finally increased the solubility and dissolution rate.

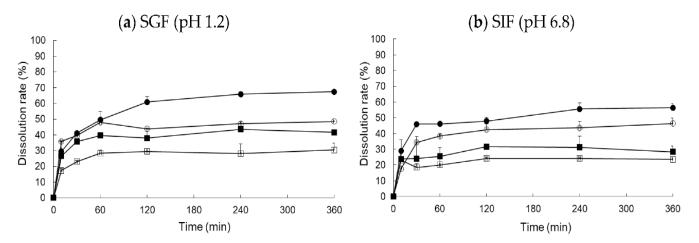
# 3.4. In Vitro Dissolution Test and Food Effect

The commercial Xarelto<sup>®</sup> (20 mg RXB) and RXB powders showed a relatively low dissolution of about 35–45% of the dose that dissolved after 120 min in distilled water (DW), SGF (pH 1.2), acetate buffer (pH 4.0), and SGF (pH 6.8), while the dissolution of the optimized RXB-ASD formulation reached approximately 80% after 120 min, which is more than a 2-fold change compared to the commercial Xarelto<sup>®</sup> (20 mg RXB) and RXB powder (Figure 8). The optimized RXB-ASD formulation successfully improved the solubility of RXB. In addition, the similarity factor f2 in dissolution curves of Xarelto<sup>®</sup> (20 mg RXB), RXB powder, and the optimized RXB-ASD formulation between water and SGF (pH 1.2) was 52.75, 69.15, and 73.74, respectively. The f2 values of those three between water and acetic acid buffer (pH 4.0) were 33.31, 57.15, and 60.92, respectively. The f2 values of those three in terms of the capacity for overall dissolution, it is considered that the dissolution of the optimized RXB-ASD formulation would not be affected by the pH variation in vivo.



**Figure 8.** Dissolution profiles of optimized RXB-ASD, RXB powder, and commercial tablet (Xarelto 20 mg) in four different media (n = 3, means  $\pm$  SD). (Key: •: Optimized RXB-ASD,  $\bigcirc$ : Xarelto<sup>®</sup> 20 mg,  $\blacksquare$ : RXB powder).

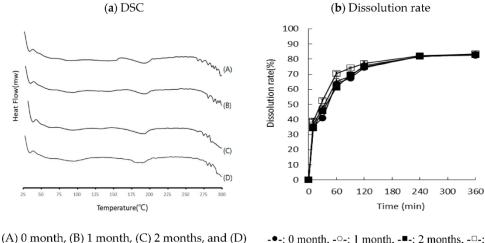
To monitor the food effect, the change in the dissolution of the formulations was monitored in in vitro dissolution tests in FaSSGF, FeSSGF, FaSSIF, and FeSSIF (Figure 9). As in the literature, we saw a 10–20% higher dissolution rate after ingestion, but high bioavailability can be expected because the dissolution rate was approximately 20% higher in the optimized formulation.



**Figure 9.** Food-effect dissolution rate of optimized RXB-ASD and a commercial tablet (Xarelto<sup>®</sup>, 20 mg) in simulated gastric fluid (SGF, pH 1.2) and simulated intestinal fluid (SGF, pH 6.8). (Key: ○: Optimized RXB-ASD in FaSSGF (or FaSSIF), □: Xarelto in FASSGF (or FaSSIF), •: Optimized RXB-ASD in FeSSGF (or FeSSIF), ■: Xarelto in FeSSGF (or FeSSIF).

# 3.5. *Stability*

The optimized RXB-ASD was stored for three months under accelerated conditions to monitor the stability, which was assessed in terms of the crystallinity, physicochemical change, and dissolution rate. It showed the same endothermic behavior for three months without recrystallizing and exhibited excellent stability without a significant change in the dissolution rate (Figure 10).



A) 0 month, (B) 1 month, (C) 2 months, and (D) -•-: 0 month, -•-: 1 month, -**u**-: 2 months, -**u**-: 3 months

Figure 10. DSC and dissolution profile of optimized RXB-ASD for three months.

## 3.6. Application to Pharmacokinetic Studies

The established analytical method was applied to a pharmacokinetic study following oral administration of 10 mg/kg RXB and RXB-ASD and intravenous administration of 2 mg/kg RXB to four male rats per group. The calibration curve exhibited linearity from 0.5 to 3000 ng/mL with a correlation of 0.0995 (Y = 0.014 x + 0.0002).

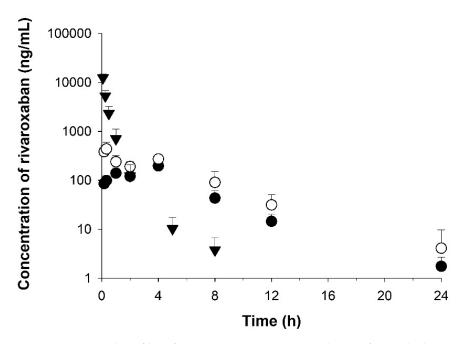
The mean plasma concentration vs. time profiles for RXB are shown in Figure 11. Following an oral gavage dose, in the group treated with the optimized RXB-ASD, the concentration rapidly increased and reached the peak concentration ( $C_{max}$ ) at 0.33 h ( $T_{max}$ ), with a mean value of 206.26 ng/mL (Table 6). Compared to after approximately 4 h in the group treated with the powder, RXB was very rapidly absorbed in the optimized RXB-ASD, indicating that it is possible to increase the systemic exposure of drugs with poor bioavailability. In addition,  $C_{max}$  and  $AUC_{0-24 \text{ h}}$  in the group treated with the optimized RXB-ASD were 2.1-fold and 1.8-fold higher, respectively, than in the group treated with the powder. Around 4 h after oral administration, a double-peak phenomenon was observed, caused by entero–hepatic circulation, delayed gastric emptying, or absorption at various sites in the gastrointestinal tract [31]. In addition, the absorption process comprehensively describes the double-peaks of RXB plasma concentrations and the corresponding changes in the pharmacodynamic effect on prothrombin time in rats [32].

Comparing partial AUC<sub>0-4 h</sub>, the value of the optimized RXB-ASD was 1.8-fold higher than that of the powder formulation (HME, 1000 ng\*h/kg vs. powder formulation, 548 ng\*h/mL); comparing the partial AUC <sub>4-24 h</sub>, the value of the optimized RXB-ASD was 1.7-fold higher than that of the powder formulation (the optimized RXB-ASD, 1190 ng\*h/kg, vs, powder formulation 696 ng\*h/mL). At the 4-h time point, the partial AUC was equally separated with half of the total AUC<sub>last</sub>. This indicated that the absorption within 4 h (a short period) contributed to increasing the amount of the total AUC by 45% for the optimized RXB-ASD (AUC<sub>0-4 h</sub>, 1000 ng\*h/mL; AUC<sub>last</sub>, 2180 ng\*h) formulation, although the remaining 55% of the total AUC increased for 20 h, from 4 to 24 h (AUC<sub>0-4 h</sub>, 1190 ng\*h/mL; AUC<sub>last</sub>, 2180 ng\*h). The half-life (T<sub>1/2</sub>) and elimination rate constant (K<sub>el</sub>) were similar in both groups, at 3.1–3.2 h and 0.223–0.237 h, respectively. Although the

mean residence time (MRT) was approximately 4.7–4.8 h, and a similar value was observed for both groups, the clearance (CL) value in the HME formulation was 0.58-fold that of the powder, and the  $V_d$  in the optimized RXB-ASD was 0.62-fold that of the powder. Considering CL and  $V_d$  values, the RXB of the HME formulation was not eliminated more rapidly than the powder. The bioavailability for RXB-ASD increased 1.8-fold to 8.6% compared with 4.9% for the RXB-powder.

**Table 6.** Pharmacokinetic parameters of optimized RXB-ASD and raw RXB powder in rats after intravenous administration of 2 mg/kg and oral administration of 10 mg/kg. Data are shown as the mean  $\pm$  SD (n = 4).

|                               | Formulation (RXB-ASD) | Reference (RXB Powder) |                   |  |
|-------------------------------|-----------------------|------------------------|-------------------|--|
|                               | P.O.                  | P.O.                   | I.V.              |  |
| T <sub>1/2</sub> (h)          | $3.10\pm0.98$         | $3.18\pm0.98$          | $1.21\pm0.19$     |  |
| AUC <sub>last</sub> (h·ng/mL) | $2180\pm455$          | $1240\pm170$           | $5130 \pm 1530$   |  |
| $AUC_{0-4 h}$ (h·ng/mL)       | $1000\pm257$          | $548 \pm 104$          | -                 |  |
| $AUC_{4-24 h}$ (h·ng/mL)      | $1190\pm295$          | $696\pm101$            | -                 |  |
| AUC <sub>inf</sub> (h·ng/mL)  | $2210\pm459$          | $1250\pm172$           | $5140 \pm 1530$   |  |
| MRT (h)                       | $4.78\pm0.74$         | $4.73\pm0.32$          | $0.381\pm0.093$   |  |
| T <sub>max</sub> (h)          | $3.25\pm1.50$         | $0.33\pm0.00$          | -                 |  |
| $C_{max}$ (ng/mL)             | $436 \pm 168$         | $206\pm26$             | -                 |  |
| $V_d (mL/kg)$                 | $22,700 \pm 6300$     | $36,700 \pm 2400$      | $740\pm267$       |  |
| CL(mL/h/kg)                   | $4690\pm1030$         | $8130 \pm 1100$        | $420\pm140$       |  |
| Kel (1/h)                     | $0.237\pm0.059$       | $0.223\pm0.039$        | $0.583 \pm 0.100$ |  |
| Bioavailability (%)           | 8.6                   | 4.9                    | -                 |  |



**Figure 11.** Temporal profiles of RXB concentrations in rat plasma after oral administration of optimized RXB-ASD ( $\bigcirc$ ) and RXB powder (•) at a dose of 10 mg/kg and after intravenous administration of RXB powder ( $\triangledown$ ). Data are shown as the mean  $\pm$  SD (n = 4).

Based on a pharmacokinetic study in rats, the results show that hot-melt extruded ASD containing RXB with combinations of polymers increased the absorption and bioavailability by improving the solubility in an in vivo animal study.

# 4. Conclusions

In this study, RXB-ASD was successfully prepared by HME technology using optimized compositions of PVA VA 64 and Cremophor<sup>®</sup> RH 40. The in vitro drug dissolution study exhibited relatively high dissolution in four media and achieved about an 80% cumulative drug release in 120 min. The pharmacokinetic study of RXB-ASD in rats showed that the absorption was markedly increased in terms of the rate and amount, i.e., AUC and  $C_{max}$ , compared to the raw RXB powder. This indicated that enhanced oral bioavailability can be obtained by our optimized RXB-ASD formulation.

**Author Contributions:** Conceptualization, G.W.L., Y.H.C. and J.-H.L.; data curation, H.S.J. and D.-K.K.; writing—original draft preparation, J.-H.L. and G.W.L.; writing—review and editing, G.W.L. and J.-H.L.; methodology, J.-H.L.; formal analysis, J.-W.J., H.S.J. and T.-S.K.; project administration, G.W.L. and Y.H.C.; supervision, G.W.L. All authors have read and agreed to the published version of the manuscript.

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Data Availability Statement: Not applicable.

Conflicts of Interest: The authors declare no conflict of interest.

### References

- Kubitza, D.; Becka, M.; Wensing, G.; Voith, B.; Zuehlsdorf, M. Safety, pharmacodynamics, and pharmacokinetics of BAY 59-7939— An oral, direct Factor Xa inhibitor—After multiple dosing in healthy male subjects. *Eur. J. Clin. Pharmacol.* 2005, *61*, 873–880. [CrossRef]
- Kapourani, A.; Vardaka, E.; Katopodis, K.; Kachrimanis, K.; Barmpalexis, P. Rivaroxaban polymeric amorphous solid dispersions: Moisture-induced thermodynamic phase behavior and intermolecular interactions. *Eur. J. Pharm. Biopharm.* 2019, 145, 98–112. [CrossRef]
- 3. Metre, S.; Mukesh, S.; Samal, S.K.; Chand, M.; Sangamwar, A.T. Enhanced biopharmaceutical performance of rivaroxaban through polymeric amorphous solid dispersion. *Mol. Pharm.* **2018**, *15*, 652–668. [CrossRef]
- 4. Torchilin, V.P. Recent advances with liposomes as pharmaceutical carriers. Nat. Rev. Drug Discov. 2005, 4, 145–160. [CrossRef]
- Gao, Y.; Li, Z.; Sun, M.; Li, H.; Guo, C.; Cui, J.; Li, A.; Cao, F.; Xi, Y.; Lou, H.; et al. Preparation, characterization, pharmacokinetics, and tissue distribution of curcumin nanosuspension with TPGS as stabilizer. *Drug Dev. Ind. Pharm.* 2010, 36, 1225–1234. [CrossRef]
- 6. Wan, S.; Sun, Y.; Qi, X.; Tan, F. Improved bioavailability of poorly water-soluble drug curcumin in cellulose acetate solid dispersion. *AAPS PharmSciTech* **2011**, *13*, 159–166. [CrossRef] [PubMed]
- Wang, D.; Chen, G.; Ren, L. Preparation and characterization of the sulfobutylether-β-cyclodextrin inclusion complex of amiodarone hydrochloride with enhanced oral bioavailability in fasted state. *AAPS PharmSciTech* 2017, *18*, 1526–1535. [CrossRef] [PubMed]
- 8. Gurusamy, S.; Umar, V.I.K.; Ishra, D.N.M. Preparation, characterization and in vitro dissolution studies of solid dispersion. *Yakugaku Zasshi* **2006**, *126*, 657–664.
- Papageorgiou, G.Z.; Bikiaris, D.; Karavas, E.; Politis, S.; Docoslis, A.; Park, Y.; Stergiou, A.; Georgarakis, E. Effect of physical state and particle size distribution on dissolution enhancement of nimodipine/PEG solid dispersions prepared by melt mixing and solvent evaporation. *AAPS J.* 2006, *8*, E623–E631. [CrossRef] [PubMed]
- 10. Sethia, S.; Squillante, E. Solid dispersion of carbamazepine in PVP K30 by conventional solvent evaporation and supercritical methods. *Int. J. Pharm.* 2004, 272, 1–10. [CrossRef] [PubMed]
- 11. Shin, S.-C.; Cho, C. Physicochemical characterizations of piroxicam-poloxamer solid dispersion. *Pharm. Dev. Technol.* **1997**, *2*, 403–407. [CrossRef] [PubMed]
- 12. Verreck, G.; Six, K.; Mooter, G.V.D.; Baert, L.; Peeters, J.; Brewster, M.E. Characterization of solid dispersions of itraconazole and hydroxypropylmethylcellulose prepared by melt extrusion—Part I. *Int. J. Pharm.* **2003**, *251*, 165–174. [CrossRef]
- 13. Zajc, N.; Obreza, A.; Bele, M.; Srčič, S. Physical properties and dissolution behaviour of nifedipine/mannitol solid dispersions prepared by hot melt method. *Int. J. Pharm.* 2005, 291, 51–58. [CrossRef]
- 14. Chen, Y.; Zhang, G.; Neilly, J.; Marsh, K.; Mawhinney, D.; Sanzgiri, Y. Enhancing the bioavailability of ABT-963 using solid dispersion containing Pluronic F-68. *Int. J. Pharm.* **2004**, *286*, 69–80. [CrossRef]

- 15. Chokshi, R.J.; Sandhu, H.K.; Iyer, R.M.; Shah, N.H.; Malick, A.; Zia, H. Characterization of physico-mechanical properties of indomethacin and polymers to assess their suitability for hot-melt extrusion process as a means to manufacture solid dispersion/solution. *J. Pharm. Sci.* **2005**, *94*, 2463–2474. [CrossRef]
- Shah, S.; Maddineni, S.; Lu, J.; Repka, M.A. Melt extrusion with poorly soluble drugs. *Int. J. Pharm.* 2013, 453, 233–252. [CrossRef] [PubMed]
- 17. Huang, D.; Xie, Z.; Rao, Q.; Liamas, E.; Pan, P.; Li, Q.; Zhang, Z.J.; Lu, M.; Li, Q. Hot melt extrusion of heat-sensitive and high melting point drug: Inhibit the recrystallization of the prepared amorphous drug during extrusion to improve the bioavailability. *Int. J. Pharm.* **2019**, *565*, 316–324. [CrossRef]
- Vasoya, J.M.; Desai, H.H.; Gumaste, S.G.; Tillotson, J.; Kelemen, D.; Dalrymple, D.M.; Serajuddin, A.T.M. Development of solid dispersion by hot melt extrusion using mixtures of polyoxylglycerides with polymers as carriers for increasing dissolution rate of a poorly soluble drug model. *J. Pharm. Sci.* 2019, 108, 888–896. [CrossRef]
- Alshetaili, A.S.; Almutairy, B.K.; Alshahrani, S.M.; Ashour, E.A.; Tiwari, R.V.; AlShehri, S.M.; Feng, X.; Alsulays, B.B.; Majumdar, S.; Langley, N.; et al. Optimization of hot melt extrusion parameters for sphericity and hardness of polymeric face-cut pellets. *Drug Dev. Ind. Pharm.* 2016, 42, 1833–1841. [CrossRef]
- Alshahrani, S.M.; Lu, W.; Park, J.-B.; Morott, J.T.; Alsulays, B.B.; Majumdar, S.; Langley, N.; Kolter, K.; Gryczke, A.; Repka, M.A. Stability-enhanced hot-melt extruded amorphous solid dispersions via combinations of Soluplus<sup>®</sup> and HPMCAS-HF. *AAPS PharmSciTech* 2015, 16, 824–834. [CrossRef]
- Justine, T.; Pieere, L.; Chole, V.; Martine, A.; Laureanne, N.; Eric, Z.; Philippe, H.; Krier, F.; Evrard, B. Continuous production of itraconazole-based solid dispersions by hot melt extrusion: Preformulation, optimization and design space determination. *Int. J. Pharm.* 2016, 151, 114–124. [CrossRef]
- 22. Fan, W.; Zhang, X.; Zhu, W.; Di, L. The preparation of curcumin sustained-release solid dispersion by hot melt extrusion-II. Optimization of preparation process and evaluation in vitro and in vivo. *J. Pharm. Sci.* **2020**, *109*, 1253–1260. [CrossRef]
- 23. Mogal, V.; Dusane, J.; Borase, P.; Thakare, P.; Kshirsagar, S. A review on quality by design. Pharm. Biol. Eval. 2016, 3, 313–319.
- 24. Sarwar, B.M.; Saquib, H. *Pharmaceutical Quality by Design—Principles and Applications*, 1st ed.; Elsevier: Amsterdam, The Netherlands, 2019.
- 25. Costa, P.; Sousa Lobo, J.M. Modeling and comparison of dissolution profiles. *Eur. J. Pharm. Sci. Off. J. Eur. Fed. Pharm. Sci.* 2001, 13, 123–133. [CrossRef]
- 26. Wang, L.; Gai, S.; Zhang, X.; Xu, X.; Gou, N.; Wang, X.; Zhou, N.; Feng, T. Simultaneous determination of RXB and TAK-438 in rat plasma by LC–MS/MS: Application to pharmacokinetic interaction study. *Bioanalysis* **2020**, *12*, 11–22. [CrossRef] [PubMed]
- 27. Gibaldi, M.; Perrier, D. Pharmacokinetics. In *Revised and Expanded*, 2nd ed.; Marcel Dekker, Inc.: New York, NY, USA, 1982; pp. 409–416.
- Patil, H.; Tiwari, R.V.; Repka, M.A. Hot-melt extrusion: From theory to application in pharmaceutical formulation. *AAPS Pharm.* 2016, 17, 20–42. [CrossRef]
- Pawar, J.; Tayade, A.; Gangurde, A.; Moravkar, K.; Amin, P. Solubility and dissolution enhancement of efavirenz hot melt extruded amorphous solid dispersions using combination of polymeric blends: A QbD approach. *Eur. J. Pharm. Sci.* 2016, *88*, 37–49. [CrossRef] [PubMed]
- 30. Al-Zoubi, N.; Alkhatib, H.S.; Bustanji, Y.K.; Aiedeh, K.; Malamataris, S. Sustained-release of buspirone HCl by co spray-drying with aqueous polymeric dispersions. *Eur. J. Pharm. Biopharm.* **2008**, *69*, 735–742. [CrossRef]
- 31. Godfrey, K.R.; Arundel, P.A.; Dong, Z.; Bryant, R. Modelling the double peak phenomenon in pharmacokinetics. *Comput. Methods Programs Biomed.* **2011**, *104*, 62–69. [CrossRef] [PubMed]
- 32. Kim, M.; Son, H.; Noh, K.; Kim, E.; Shin, B.S.; Kang, W. Effects of verapamil and diltiazem on the pharmacokinetics and pharmacodynamics of rivaroxaban. *Pharmaceutics* **2019**, *11*, 133. [CrossRef] [PubMed]