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Method Article

Functionalization of kaolinite for removal of phosphate from urban sewage



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ABSTRACT

The PO₄³⁻ widespread in urban sewages promotes eutrophication of water sources, with harmful effects to natural life and endanger human health. The removal of PO₄³⁻ from urban sewage requires treatment at tertiary level, with high costs and low efficiency in most cases. Thus, a functionalization method for surface modification of kaolinite was proposed to improve the removal of PO₄³⁻ from urban sewage. The kaolinite commercial did not remove PO₄³⁻ from aqueous solution. However, the functionalized kaolinite (FK) was efficient, with a maximum removal capacity of 8.4 ± 0.1 mg PO₄³⁻/L, within less than 1 min of reaction. The removal of PO₄³⁻ is associated with precipitation of pyromorphite, a mineral with low solubility ($K_{sp} < 10^{-79.6}$). Finally, real urban sewage samples (raw and treated) were also tested for removal of PO₄³⁻ using FK, confirming its effectiveness. The central aspects of this development are:

- Functionalized kaolinite (FK), with Pb(II), for removal of PO₄³⁻ from urban sewage was studied.
- The FK was efficient for removal of up to 8.4 mg PO₄³⁻/L from aqueous solution, within a short reaction time.
 The precipitation of pyromorphite was the mechanism responsible for removal of PO₄³⁻ and FK efficiency have been confirmed for real urban sewage samples.

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Specifications table

Method details

Background

The PO_4^{3-} present in urban sewage promotes eutrophication in the water bodies [1]. This anion is difficult to remove during the treatment of urban sewage, requiring treatment at the tertiary level [2]. The most used method for the removal of PO_4^{3-} from urban sewage is the chemical precipitation, involving the addition of bivalent or trivalent metal salts [3–5]. Recently, studies have shown the precipitation of pyromorphite ($5Pb^{2+} + 3PO_4^{3-} + H_2O \rightarrow Pb_5(PO_4)_3(OH)_{(pyromorphite)} + H^+$) in natural surface waters due to presence of PO_4^{3-} and Pb(II), reducing the concentration of dissolved Pb(II) [6,7]. The pyromorphite has a low solubility constant ($K_{sp} < 10^{-79.6}$), preventing that the Pb(II) returns to the environment as a dissolved cation [8–10].

Kaolinite $[Al_2Si_2O_5(OH)_4]$ has its negatively-charged surface, becoming this mineral an important adsorbent for cationic ions [11]. The functionalization of kaolinite with acid treatment [12] and bivalent trace elements can promote the removal of anionic molecules, such as PO_4^{3-} , present in the urban sewage [13–15]. Based on the functionalization of commercial kaolinite (CK) with bivalent trace elements, the functionalized kaolinite (FK) with Pb(II) was produced. The efficiency for removal of PO_4^{3-} from aqueous solution using FK was studied and compared with CK. Furthermore, the reaction time and maximum removal capacity of PO_4^{3-} was determined using FK. Finally, the FK was applied in real urban sewage samples, attesting its effectiveness.

Functionalization of commercial kaolinite

The CK (Sigma-Aldrich®, CAS Number 1318-74-7) was used in this study. The following procedures have been applied for the functionalization:

- 1 About 1.0 g of CK was placed in a beaker;
- 2 10 mL of aqueous solution with Pb(II) initial concentration of 40 mg/L was added;
- 3 The beaker was agitated (digital shaker Biothec model BT 645) for 24 h at 145 rpm;
- 4 The solution was centrifuged (centrifuge Excelsa II® model 206-BL) for 25 min at 3000 rpm;
- 5 The FK was separated and washed three times, using ultrapure water (Milli-Q® system model IQ 7000) with electrical conductivity lower than 0.02 µS/cm;
- 6 Finally, the FK was dried for 12 h at 40 °C.

Method validation

For validation purposes, 1.0 g of each sample (CK and FK) was mixed with 10 mL of aqueous solution containing PO_4^{3-} in the initial concentration (C_0) of 1 mg/L at pH 6 [9]. The suspension was shaken for 24 h at 145 rpm, and then centrifuged at 3000 rpm for 25 min. The supernatant was separated and the PO_4^{3-} concentration remaining in solution (C_e) was measured using a Hach DR-2800 spectrophotometer, with a detection limit of 0.1 mg/L. The removal efficiency of PO_4^{3-} (%A – in percentage) was determined according to the Eq. 1. The experimental procedures were carried out in triplicate.

$$^{\text{$\%$}A = [(C_0 - -C_e)/C_e].100}$$
(1)

Table 1

(1112) (112) (112) (112) (112) (112) (112) (112) (112) (112) (112) (112) $(11$	Removal efficiency	(%A) of PO4 ³⁻ ((mg/L) using FK and CK in aqueous solution.
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СК		FK			
C ₀	C _e	%A	$\overline{C_0}$	C _e	%A
1.0	1.0 ± 0.1	0	1.0	< 0.1	100

Table 2

Reaction time (min) and removal efficiency (%A) of PO43- (mg/L) using FK in aqueous solution.

Time	C ₀	Ce	%A
0	1.0	1.0 ± 0.1	0
1	1.0	< 0.1	100
5	1.0	< 0.1	100
15	1.0	< 0.1	100
30	1.0	< 0.1	100
60	1.0	< 0.1	100

Table 3

Maximum removal capacity of PO4³⁻ using FK and concentration of residual Pb(II) in aqueous solution.

PO ₄ ³⁻ (mg/L)			Pb(II) (mg/L)
Co	Ce	%A	
1	< 0.1	100	692 ± 20
2	< 0.1	100	91 ± 4
3	< 0.1	100	63 ± 3
4	< 0.1	100	< 0.006
7	< 0.1	100	< 0.006
9	0.6 ± 0.1	93.3	< 0.006

The results are presented in Table 1. The removal efficiencies of PO_4^{3-} were 0 and 100% using CK and FK, respectively. These results evidenced the functionalization plays a crucial role on the removal of PO_4^{3-} . The precipitation of pyromorphite was the main mechanism associated with PO_4^{3-} removal using FK with Pb(II), as shown in Fig. 1.

Reaction time and maximum removal capacity of PO₄³⁻ using functionalized kaolinite

The reaction time for removal of PO_4^{3-} using KF has been investigated, according the following procedures carried out in triplicate. The FK (1.0 g) was mixed in 10 mL of an aqueous solution with C_0 of 1 mg PO_4^{3-}/L at pH 6 [9]. The suspension was shaken at 145 rpm, with samples taken after 1, 5, 15, 30 and 60 min. The solution was centrifuged at 3000 rpm for 25 min, with the supernatant separated and the C_e determined. The experiments have shown no residuals of PO_4^{3-} after 1 min of reaction time (Table 2), showing a fast reaction time for removal of PO_4^{3-} associated to the mineral pyromorphite precipitation.

The maximum removal capacity of PO_4^{3-} using FK was also determined (in triplicate). The samples with 1.0 g: 10 mL of an aqueous solution with C_0 of 1 mg/L were stirred at 145 rpm for 5 min at pH 6 [9], with C_0 of 1, 2, 3, 4, 7 and 9 mg/L. The solutions were centrifuged for 25 min at 3000 rpm and the C_e determined in the supernatants. The maximum removal capacity of PO_4^{3-} using FK was 8.4 \pm 0.1 mg/L (Table 3) or 8.4 mg/g, indicating an efficiency of 93.3% for removal of PO_4^{3-} from aqueous solutions with C_0 of 9 mg/L. The value of 8.4 mg/g is higher than the removal capacities obtained for natural or functionalized kaolinite, i.e., CK used in this study (< 0.1 mg/g), kaolinite from Linthipe (ca. 0.15 mg/g) [12], modified kaolinite with FeCl₃ (1.31 mg/g) [13] and modified kaolinite with seawater in different temperatures (4.07 mg/g at 600 °C) [15].

Trace levels of residual Pb(II) in the treated effluent can pose a serious environmental risk for aquatic systems due to its toxicity. Thus, the concentration of Pb(II) were also determined in the



Fig. 1. SEM-EDS images of functionalized kaolinite after the removal of PO₄³⁻, showing the precipitation of small grains (lower than 5 µm) of pyromorphite (spots 1, 2 and 3).

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Table 4 C_0 and C_e averages of PO₄³⁻ and Pb(II) (in mg/L) measured in the urban sewage collected in a WWTP located in Rio Claro.

Sample	C_0 of PO_4^{3-}	C_e of PO ₄ ³⁻	C_0 of Pb(II)	C_e of Pb(II)
Raw	$\begin{array}{l} 6.1 \pm 0.1 \\ 3.8 \pm 0.1 \end{array}$	< 0.1	< 0.006	< 0.006
Treated		< 0.1	< 0.006	< 0.006

supernatants by inductively coupled plasma optical emission spectrometry (ICP OES), iCAP 6000 SERIES machine Thermo Scientific, with detection limit of 0.006 mg/L. The presence of residual Pb(II) in aqueous solutions was measured in aqueous solutions with C_0 of 1, 2 e 3 mg/L of PO₄³⁻. Residual Pb(II) was not detected for C_0 of PO₄³⁻ \geq 4 mg/L, indicating the use of FK for removal of PO₄³⁻ only in urban sewage with $C_0 \geq$ 4 mg/L. Further studies for lower C_0 concentrations in urban sewage are encouraged before application.

Removal of PO₄³⁻ using functionalized kaolinite in real urban sewage samples

Three samples of raw and treated urban sewage were collected in a wastewater treatment plant (WWTP) located in Rio Claro, São Paulo State, Brazil. These samples were stored in labeled amber container at 4°C and transported immediately to the laboratory, where they were filtered, using 0.45 μ m MF-Millipore® membrane filter, and the C_0 of PO₄^{3–} and Pb(II) measured (Table 4). In order to verify the real removal efficiency of PO₄^{3–} from urban sewage (raw and treated), 10 mL of each filtered sample were mixed with 1.0 g of FK. The solutions were shaken at 145 rpm for 5 min at pH 6 [9], centrifuged at 3000 rpm for 25 min, and then the C_e of PO₄^{3–} and Pb(II) were determined in the supernatants (Table 4).

The C_0 averages of PO₄³⁻ were 6.1 ± 0.1 e 3.8 ± 0.1 mg/L, respectively, for raw and treated urban sewage. After the use of FK, C_e averages of PO₄³⁻ were lower than 0.1 mg/L. In addition, the C_0 and C_e averages of Pb(II) were always lower than the detection limit of 0.006 mg/L. These results show the efficiency during the use of FK for removal of PO₄³⁻ from urban sewage in real samples collected in a WWTP.

Conclusions

A method for functionalization of kaolinite for removal of PO_4^{3-} from urban sewage was studied. The functionalized kaolinite (FK) with Pb(II) have shown a promising alternative for removal of PO_4^{3-} in aqueous solution, with maximum removal capacity of 8.4 mg/L, within a reaction time lower than 1 min. The precipitation of PO_4^{3-} is associated with pyromorphite, a mineral with low solubility ($K_{sp} < 10^{-79.6}$). Finally, real urban sewage samples (raw and treated) were also tested for removal of PO_4^{3-} using KF, confirming its effectiveness for removal of PO_4^{3-} from urban sewage with $C_0 \ge 4$ mg/L.

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Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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