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# Bimetallic Cu-Bi catalysts for efficient electroreduction of $\mathrm{CO}_{2}$ to formate 

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#### Abstract

Electrochemical $\mathrm{CO}_{2}$ reduction offers an effective means to store renewable electricity in value-added chemical feedstocks. Much effort has been made to develop catalysts that achieve high Faradaic efficiency toward Formate production, but the catalysts still need high operating potentials to drive the $\mathrm{CO}_{2}$-to-formate reduction. Here we report physical vapor deposition to fabricate homogeneously alloyed, compositionally controlled $\mathrm{Cu}_{1-x} \mathrm{Bi}_{x}$ bimetallic catalysts over a large area with excellent electrical conductivity. Operating electrochemical studies in Ar -saturated and $\mathrm{CO}_{2}$-saturated electrolytes identified that $\mathrm{Cu}-\mathrm{Bi}$ catalysts notably suppress the competing $\mathrm{H}_{2}$ evolution reaction and enhance $\mathrm{CO}_{2}$-to-formate selectivity. We reported a formate Faradaic efficiency of $>95 \%$ at an improved cathodic potential of $\sim-0.72 \mathrm{~V}$ vs. RHE and a high formate cathodic energy efficiency of $\sim 70 \%$. The electrochemical reaction is stable over 24 h at a current density of $200 \mathrm{~mA} \mathrm{~cm}{ }^{-2}$. The work shows the advantages of bimetallic catalysts over single metal catalysts for increased reaction activity and selectivity.


## KEYWORDS

electrocatalysis, $\mathrm{Cu}-\mathrm{Bi}$, bimetal, $\mathrm{CO}_{2} \mathrm{R}$, formate

## Introduction

With the rapid development of modern society, the excessive burning of fossil fuels has led to huge amounts of $\mathrm{CO}_{2}$ emissions, breaking the ecological carbon cycle and causing the growing greenhouse effect (Singh et al., 2016; Xiao et al., 2017; Garza et al., 2018; Birdja et al., 2019; Li et al., 2020). Renewably powered $\mathrm{CO}_{2}$ conversion to valueadded fuels or chemical raw materials, such as $\mathrm{CO}, \mathrm{HCOO}^{-}, \mathrm{C}_{2} \mathrm{H}_{4}, \mathrm{C}_{2} \mathrm{H}_{5} \mathrm{OH}$, etc., is becoming an important way to maintain energy and environmental sustainability (Kortlever et al., 2015; Wang et al., 2021a; Wang et al., 2021b; Wang et al., 2022). For example, the electroreduction of $\mathrm{CO}_{2}$ using renewable electricity has attracted great research attention (Wang et al., 2021c). Among the commonly reported $\mathrm{CO}_{2} \mathrm{R}$ products, formic acid or formate stands out as a promising liquid chemical due to its high energy value in the techno-economic analysis and high volumetric mass density ( $53.4 \mathrm{~g} \mathrm{~L}^{-1}$ ) for easy storage and transport (Yoo et al., 2016; Chi et al., 2021).

Conventionally, p block metals such as $\mathrm{Bi}, \mathrm{Pb}$, and In have appropriate ${ }^{*} \mathrm{OCHO}$ binding energy, favoring the $\mathrm{CO}_{2}$-to-formate conversion. However, the electrical
conductivity of these metals is not satisfactory, causing a large potential loss at high current densities. Cu is naturally abundant and has good electrical conductivity, possible for practical use (Huang et al., 2018). Cu-based materials are widely investigated as electrocatalysts for $\mathrm{CO}_{2} \mathrm{R}$ to multi-carbon $\left(\mathrm{C}_{2+}\right)$ production (Mistry et al., 2016a; Mistry et al., 2016b; Gao et al., 2019; Zaza et al., 2022). However, due to the modest binding to $\mathrm{H}, \mathrm{C}$, and O (Qin et al., 2019; Zheng et al., 2021; Zhang et al., 2022), Cu shows poor selectivity to one specific product which leads to an increased product separation cost.

Bimetallic catalysts have been reported to increase the activity and selectivity of electrocatalytic $\mathrm{CO}_{2} \mathrm{R}$ by taking the advantage of both metals. Zeng et al. improved the formate production by fabricating single atom Pb anchored Cu catalysts (Zheng et al., 2021); Thomas J. Meyer et al. enhanced selectivity for methane production by forming Cu-Pd bimetal alloys (Zhang et al., 2015); Douglas R. MacFarlane et al. improved the electrocatalytic reduction of $\mathrm{CO}_{2}$ to CO by loading Au on Cu (Chen et al., 2017); Wang et al. (2010) prepared novel silvercoated nanoporous copper composite electrocatalysts for $\mathrm{CO}_{2} \mathrm{R}$ to produce dimethyl carbonate. As for formate production, Bi is extensively studied as a promising $\mathrm{CO}_{2} \mathrm{R}$-to-formate catalyst due to its abundance on Earth, low cost, and environmental-benign properties. Jiang and collaborators reported that a Bi nanostructured catalyst electrochemically reduced by BiOCl nanosheets obtained $92 \% \mathrm{FE}_{\mathrm{HCOOH}}$ at -1.5 V vs. SCE at room temperature (Zhang et al., 2014); Zhong et al. achieved over 95\% formate selectivity with ultra-long stability of more than 100 days (Li et al., 2021); Li et al. (2019) achieved nearly $100 \%$ formate selectivity using $\mathrm{Bi} / \mathrm{Bi}_{2} \mathrm{O}_{3}$ with abundant grain boundaries as catalysts. Yet the Bi-based catalysts still require a high potential to conduct electrocatalytic reduction of $\mathrm{CO}_{2}$ (Tian et al., 2021).

Herein, we present the large-area fabrication of $\mathrm{Cu}_{1-x} \mathrm{Bi}_{x}$ $(x=0.1,0.2,0.25)$ catalysts using controllable thermal evaporation. We evaluated the $\mathrm{CO}_{2} \mathrm{R}$ and also the competing hydrogen evolution reaction (HER) performance in flow cells in $\mathrm{CO}_{2}$-saturated and Ar-saturated electrolytes. We obtained a formate selectivity of $95 \%$ and a cathode energy efficiency of $70 \%$ at -0.72 V vs. RHE with $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$. The $\mathrm{CO}_{2} \mathrm{R}$ can proceed stably and efficiently at a current density of $200 \mathrm{~mA} \mathrm{~cm}^{-2}$ over 24 h . We conclude that the bimetallic $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ improves formate selectivity and enhances the $\mathrm{CO}_{2} \mathrm{R}$ activity and cathodic energy efficiency, which may offer new perspectives for future design and synthesis of bimetallic $\mathrm{CO}_{2} \mathrm{R}$ catalysts.

## Experimental section

## Synthesis of $\mathrm{Cu}_{1-x} \mathrm{Bi}_{x}(x=0.1,0.2,0.25), \mathrm{Cu}$ and Bi catalyst

$\mathrm{Cu}_{1-x} \mathrm{Bi}_{x}(x=0.1,0.2,0.25), \mathrm{Cu}$, and Bi catalysts were synthesized by using the thermal evaporation (SKY-RH400)
method. To prepare the $\mathrm{Cu}_{1-x} \mathrm{Bi}_{x}(x=0.1,0.2,0.25)$ catalyst, the precursors Cu and Bi particles are evaporated onto the PTFE gas diffusion electrodes by thermal evaporation. In brief, 2 g of Bi metal particles and 2 g of Cu metal particles were put into the tungsten boats in the deposition chamber. The metal powder was slowly melted in a vacuum environment below $5^{*} 10^{-4} \mathrm{~Pa}$. The evaporation rate of Bi was set to $0.03,0.04$, and $0.05 \mathrm{~nm} \mathrm{~s}^{-1}$ and Cu was set to $0.07,0.06$, and $0.05 \mathrm{~nm} \mathrm{~s}^{-1}$ to obtain $\mathrm{Cu}_{1-x} \mathrm{Bi}_{x}(x=0.1,0.2,0.25)$ samples. The thickness of the as-deposited $\mathrm{Cu}_{1-x} \mathrm{Bi}_{x}(x=0.1,0.2$, 0.25 ) films was about 500 nm as measured by a thickness meter placed inside the evaporation chamber. Uniform bimetallic films were obtained. To prepare the pure Bi and Cu films with the same thickness as control samples, we evaporated both Bi and Cu at $0.1 \mathrm{~nm} \mathrm{~s}^{-1}$ under the same conditions.

## Characterization

Field Emission Scanning Electron Microscope (FESEM) images were taken on a SU8100 Scanning Electron Microscope. SEM-EDX test voltage is 20 kV . Powder X-ray diffraction (XRD) was performed using a Bruker D8 Advance X-ray diffractometer using Cu Ka radiation ( $\lambda=0.15418 \mathrm{~nm}$ ) in the $2 \theta$ range of $20^{\circ}-80^{\circ}$ at a scan rate of $7 \%$ min. X-ray photoelectron spectroscopy (XPS) studies were performed using PHI5000 VersaProbe. The binding energy data were calibrated relative to the C 1 s signal at 284.6 eV .

## Electrochemical measurements

The electrochemical $\mathrm{CO}_{2} \mathrm{R}$ experiments were carried out in a flow cell setup of a three-electrode system. The $\mathrm{CO}_{2} \mathrm{R}$ catalysts, $\mathrm{Ag} / \mathrm{AgCl}$ electrodes, and foamed nickel films were used as working electrodes, reference electrodes, and counter electrodes, respectively. 1 M KOH electrolytes were used as both catholyte and anolyte. An anion exchange membrane (Fumasep FAB-PK-130) was used to separate the catholyte and anolyte. All measurements were performed by using an electrochemical workstation (AOTU-Lab). All experiments were performed under the standard conditions with a $\mathrm{CO}_{2}$ gas flow rate of 25 standard cubic centimeter per minute (sccm) at the flow cell outlet. The potential range of linear sweep voltammetry (LSV) is 0 to $-1.2 \mathrm{~V}_{\mathrm{RHE}}$, with a sweep speed of $50 \mathrm{mV} \mathrm{s}^{-1}$. The electrode potentials were converted to the RHE potentials using $\mathrm{V}_{\mathrm{RHE}}=\mathrm{V}_{\mathrm{Ag} / \mathrm{AgCl}}+0.197+0.059 \times$ pH . Electrochemical impedance spectroscopy (EIS) was measured at open circuit potential with amplitudes of 10 mV over the frequency range of 1 MHz to 1 Hz . The liquid products of $\mathrm{CO}_{2}$ reduction were quantitatively analyzed by ion chromatography (Shenghan ICS-1000). Gaseous products were analyzed by gas chromatography


FIGURE 1
(A) A schematic illustration of the synthetic process of $\mathrm{Cu}-\mathrm{Bi}$ catalyst on polytetrafluoroethylene (PTFE). (B) The insert optical image shows a $5 \mathrm{~cm}^{2} \times 5 \mathrm{~cm}^{2}$ sample of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ on the PTFE substrate.
(PE GC9790). ${ }^{1} \mathrm{H}$ nuclear magnetic resonance (NMR) spectroscopy was used to identify other liquid products other than formate. All measurements were made at room temperature and ambient pressure.

The Faradaic Efficiency (FE) of formate is calculated as follows:

$$
\mathrm{FE}_{\text {formate }}=\frac{n * F * V * c}{1000 * M * Q}
$$

where $n$ is the number of electrons transferred $(n=2) . F$ is Faraday's constant $\left(96,485 \mathrm{C} \mathrm{mol}^{-1}\right) . c$ is the mass concentration of formate produced by the reaction $\left(\mathrm{mg} \mathrm{L}^{-1}\right)$. $V$ is the volume of catholyte (L). $M$ is the molar mass of formate ( $46.03 \mathrm{~g} \mathrm{~mol}^{-1}$ ). Q is the total amount of charge consumed by the entire reaction monitored by the electrochemical workstation (C).

The FE of the gas product is calculated according to the following equation:

$$
\mathrm{FE}_{\text {gas }}=\frac{n * F * V}{1000 * 22.4 * \mathrm{Q}}
$$

where $n$ is the number of electrons transferred $(n=2) . F$ is Faraday's constant $\left(96,485 \mathrm{C} \mathrm{mol}^{-1}\right) . V$ is the volume of catholyte (L). $Q$ is the total amount of charge consumed by the entire reaction monitored by the electrochemical workstation (C).

Cathode Energy Efficiency (CEE) Calculation Formula:

$$
\mathrm{CEE}_{\text {formate }}=\frac{\left(1.23-E_{\text {formate }}\right) * F E_{\text {formate }}}{1.23-E_{\text {cathode }}}
$$

where $E_{\text {formate }}$ of -0.199 V vs. RHE is the standard potential of the formate formation. $F E_{\text {formate }}$ is the measured formate Faradaic efficiency. $E_{\text {cathode }}$ is the applied potential vs. RHE.

## Results and discussion

We prepared a series of $\mathrm{Cu}_{1-x} \mathrm{Bi}_{x}(x=0.1,0.2,0.25)$ bimetallic materials, pure Cu , and pure Bi samples on a large area by thermal evaporation. As shown in Figures $1 \mathrm{~A}, \mathrm{~B}$ and Supplementary Figure S1, the as-prepared $\mathrm{Cu}_{1-x} \mathrm{Bi}_{x}(x=0.1$, $0.2,0.25)$ catalysts were all tightly wrapped on the PTFE fibers and formed uniformly distributed Cu and Bi nanoparticles with a size of $100-200 \mathrm{~nm}$. It can be seen from Figure 2 A and Supplementary Figure S1 that with the increase of Bi content, the particles gradually form nanocrystals, and the particle size of $\mathrm{Cu}_{1-x} \mathrm{Bi}_{x}(x=0.1,0.2,0.25)$ is about $100-200 \mathrm{~nm}$, and the $\mathrm{Cu}-\mathrm{Bi}$ bimetallic distribution is uniform. The particle sizes of Bi and Cu are 200 nm and $50-100 \mathrm{~nm}$, respectively. Then we measured the element distribution using SEM-EDX. As shown in the mapping spectrum, Cu and Bi elements were uniformly distributed on the catalyst surfaces (Figures 2B,C; Supplementary Figure S2). Through SEM-EDX and XPS analysis, the element ratio of our prepared Cu -Bi was 0.8:0.2 (Supplementary Figure S3).

The chemical states of the synthesized $\mathrm{Cu}, \mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$, and Bi catalysts were studied by the high-resolution XPS spectra of Bi 4f and Cu 2 p , respectively (Figures $3 \mathrm{~A}, \mathrm{~B}$ ). We observed that the strong peaks at 158.7 and 164.0 eV corresponded to $\mathrm{Bi}^{3+} 4 \mathrm{f}_{7 / 2}$ and $\mathrm{Bi}^{3+} 4 \mathrm{f}_{5 / 2}$, and the peaks at $157.0 \mathrm{eV}, 162.3 \mathrm{eV}$ corresponded to $\mathrm{Bi}^{0}$ $4 \mathrm{f}_{7 / 2}$ and $\mathrm{Bi}^{0} 4 \mathrm{f}_{5 / 2}$. From the high-resolution XPS spectrum of Cu 2 p, the peaks at 932.0 and 951.8 eV corresponded to $\mathrm{Cu}^{0,1+}$, while the peaks at 933.9 and 953.6 eV were consistent with $\mathrm{Cu}^{2+}$. It should be explained that both Cu and Bi are easily oxidized in air, the positively charged $\mathrm{Bi}^{3+}$ and $\mathrm{Cu}^{2+}$ are detected, probably because the oxidation occurred during the storage of the sample in air. Compared with Cu , the d-band center of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ moved more positively after the introduction of Bi


FIGURE 2
(A) SEM images of the synthesized $C u_{0.8} B i_{0.2}$ by thermal evaporation. (B) EDX spectrum of the $C u_{0.8} B i_{0.2}$. (C) EDX Mapping results of the $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$.


FIGURE 3
(A) Cu 2 p XPS spectra of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2 \text {. }}$ (B) Bi 4 f XPS spectra of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2 \text {. }}$. (C) Surface valence band photoemission spectra of Cu and $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$. The white bar in (C) highlights the $d$-band center of various materials
species (Figure 3C). As reported, the positively shifted d-band center likely increases the electron donation from the catalysts to the adsorbed ${ }^{*} \mathrm{OCHO}$ intermediate, strengthening the ${ }^{*} \mathrm{OCHO}$
surface binding (Xin et al., 2014; Zhang et al., 2018). This is consistent with our electrochemical $\mathrm{CO}_{2} \mathrm{R}$ test that $\mathrm{Cu}-\mathrm{Bi}$ catalysts show improved performance.


FIGURE 4
Schematic of Cu -Bi electrocatalyst on PTFE for electroreduction of $\mathrm{CO}_{2}$ in a flow cell.


FIGURE 5
(A) The LSV curves under $\mathrm{CO}_{2}$ or $\mathrm{N}_{2}$ conditions of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}, \mathrm{Cu}$, and Bi . (B) The particular current density of formate of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}, \mathrm{Cu}$, and Bi . (C,E) The faradaic efficiency of formate and $\mathrm{H}_{2}$ of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}, \mathrm{Cu}$, and Bi at current densities of 100,200 , and $300 \mathrm{~mA} \mathrm{~cm}{ }^{-2}$. (D) The cathode energy efficiency of formate at current densities of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}, \mathrm{Cu}$, and Bi of 100,200 , and $300 \mathrm{~mA} \mathrm{~cm}^{-2}$. (F) The EIS curve of $\mathrm{Cu}, \mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$, and Bi .


FIGURE 6
The stability test of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ in 1 M KOH at $200 \mathrm{~mA} \mathrm{~cm}^{-2}$.

The $\mathrm{CO}_{2} \mathrm{R}$ electrochemical performance of the $\mathrm{Cu}_{1-x} \mathrm{Bi}_{x}$ ( $x=0.1,0.2,0.25$ ), pure Cu , and pure Bi catalysts were tested in a flow cell with a three-electrode system (Figure 4). The anode was Ni , the reference electrode was an $\mathrm{Ag} / \mathrm{AgCl}$ electrode, and the electrolyte was 1 M KOH solution ( $\mathrm{pH}=$ 14). From the linear sweep voltammetry (LSV), we can intuitively see that the reaction overpotential of $\mathrm{Cu}-\mathrm{Bi}$ bimetal was reduced significantly (Figure 5A; Supplementary Figure S4). As shown in Figure 3B, the overpotential $(520 \mathrm{mV})$ of the $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ catalyst is significantly smaller than that of the Bi catalyst ( 660 mV ) at the same current density $\left(100 \mathrm{~mA} \mathrm{~cm}^{-2}\right)$. The overpotential for Cu is the best $(400 \mathrm{mV})$, but the product selectivity is poor (Figure 5B). The cathodic current density on $\mathrm{Cu}, \mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$, and Bi electrodes was largely reduced when $\mathrm{N}_{2}$ was passing through (Figure 5A). In the presence of $\mathrm{N}_{2}$, the current density started to increase slowly at -0.70 V vs. RHE, which was mainly caused by the hydrogen evolution reaction (HER). It is also clear that HER on the Cu electrode is worse than $\mathrm{CO}_{2} \mathrm{R}$ on the Bi electrode, indicating that the introduction of Bi into Cu can suppress HER In the presence of $\mathrm{CO}_{2}$, which is more beneficial to $\mathrm{CO}_{2} \mathrm{R}$.

To investigate the product selectivity of $\mathrm{CO}_{2} \mathrm{R}$ with $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}, \mathrm{Cu}$, and Bi catalysts, chronopotentiometry tests were performed at current densities of 100,200 , and $300 \mathrm{~mA} \mathrm{~cm}^{-2}$, respectively (Supplementary Figure S5). The products were quantitatively analyzed by gas chromatography (GC), ion chromatography (IC), and nuclear magnetic resonance (NMR). As shown in Figures $5 \mathrm{C}-\mathrm{E}$, and Supplementary Figure S 6 , the $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ catalyst achieved over $90 \%$ selectivity to formate at all current densities, in particular, the selectivity for formate reached $95 \%$ at a current density of $100 \mathrm{~mA} \mathrm{~cm}^{-2}$, with a cathode energy efficiency reaching about $70 \%$. Although the singlemetal Bi catalyst has a formate selectivity close to that of
$\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$, its cathode energy efficiency is much lower than that of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ at all current densities due to its high reaction potential. In the case of the Cu catalyst, the formate selectivity is very low. Considering both the selective and energy efficiency, $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ outperforms Bi and Cu in the electroreduction of $\mathrm{CO}_{2}$ to formate.

As shown in Figure 5E, we found that the introduction of Bi into Cu can significantly reduce HER, which is consistent with the LSV results under $\mathrm{N}_{2}$ environment. To explain the reason for the excellent performance of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ catalysts, we performed EIS tests on the three samples. As is shown in Figure $5 \mathrm{~F}, \mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ shows a smaller semicircle diameter than Bi in the impedance spectrum, suggesting that the charge transfer resistance of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ is lower than that of Bi , ensuring a faster electron transfer during the reaction. The conductivity of Cu is $58.13953 \mathrm{~S} / \mathrm{m}$, and that of Bi is $0.95238 \mathrm{~S} /$ m . The conductivity of Cu is significantly better than that of Bi. Therefore, we analyze that the loading of Cu metal increases the conductivity of the material and reduces the charge transfer resistance, also the HER is greatly suppressed in the presence of $\mathrm{CO}_{2}$, as a result, $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ can reduce the reaction overpotential and maintain high $\mathrm{CO}_{2} \mathrm{R}$ catalytic activity and selectivity.

To verify the stability of the $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ catalyst, we performed the stability test at a current density of $200 \mathrm{~mA} \mathrm{~cm}^{-2}$, and SEM characterization of the reacted sample was performed. It can be seen from Figure 6 that during the reaction process of the $24 \mathrm{~h} \mathrm{CO}_{2}$ reduction, the reaction potential did not change significantly, and the selectivity of $\mathrm{HCOO}^{-}$was maintained above $90 \%$. We also carried out SEM, SEM-EDX, and XRD analyses of the sample after 24 h of reaction. From Supplementary Figure S7, we can observe that the morphology and structure of the $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ bimetallic catalyst did not change after the reaction. The XRD characterizations also showed that the catalyst did not
change significantly after the reaction, indicating that good stability with $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ for $\mathrm{CO}_{2} \mathrm{R}$.

## Conclusion

In conclusion, we developed a simple, controllable, and large-area preparation method for the synthesis of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ catalysts. $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ exhibited excellent formate selectivity and cathode energy efficiency under all current densities. Specifically, it exhibited a formate selectivity of $95 \%$ and a cathode energy efficiency of $70 \%$ at a potential of -0.72 V vs. reversible hydrogen electrode and maintained the $\mathrm{CO}_{2} \mathrm{R}$ durability for over 24 h at a current density of $200 \mathrm{~mA} \mathrm{~cm}{ }^{-2}$. The excellent catalytic performance of $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ is attributed to the following factors: 1) CuBi alloy likely has a favorable work function to improve $\mathrm{CO}_{2}$ adsorption for formate production; 2) CuBi alloy improves electron transport. We expect that the bimetal $\mathrm{Cu}_{0.8} \mathrm{Bi}_{0.2}$ electrocatalyst may offer a material foundation for the improved catalytic $\mathrm{CO}_{2} \mathrm{R}$ to formate conversion.

## Data availability statement

The original contributions presented in the study are included in the article/Supplementary Material, further inquiries can be directed to the corresponding author.

## Author contributions

MZ supervised the project. MZ conceived the idea and designed the experiments. LL and XJ conducted the synthesis, characterizations, and flow-cell tests. LL, XJ, XY, and MZ discussed the experiment results. MZ, XY, and LL wrote the manuscript. All authors discussed the results and assisted during manuscript preparation.

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## Conflict of interest

The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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## Supplementary material

The Supplementary Material for this article can be found online at: https://www.frontiersin.org/articles/10.3389/fchem. 2022.983778/full\#supplementary-material

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