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Research article

Advanced cell-based products generated via automated and manual manufacturing platforms under the quality by design principle: Are they equivalent or different?

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ABSTRACT

Mesenchymal stem/stromal cells (MSCs) are multipotent stem cells that can be isolated from bone marrow, adipose tissue, the umbilical cord, dental pulp, etc. These cells have unique properties that give them excellent therapeutic potential, including immunoregulation, immunomodulation, and tissue regeneration functions. MSC-based products are considered advanced therapy medicinal products (ATMPs) under European regulations (1394/2007); thus, they must be manufactured under good manufacturing practices and via effective manufacturing methods. The former can be achieved via a proper laboratory design and compliance with manufacturing protocols, whereas the latter requires an approach that ensures that the quality of the products is consistent regardless of the manufacturing procedure. To meet these daunting requirements, this study proposes an exchangeable approach that combines optimized and equivalent manufacturing processes under the Quality by Design (QbD) principle, allowing investigators to convert from small laboratory-scale to large-scale manufacturing of MSC-based products.

1. Introduction

Mesenchymal stem/stromal cells (MSCs) are multipotent stem cells that were first isolated from bone marrow aspirate [1] and later found in other tissues, including adipose tissue [2], the umbilical cord (UC) [3], umbilical cord blood [4], the placenta membrane [5], dental pulp [6], etc. Among these sources, bone marrow, adipose tissue, and the UC are the three most widely used sources of MSCs for therapeutic applications [7]. MSC-based therapy has evolved rapidly both scientifically and clinically in recent decades, with

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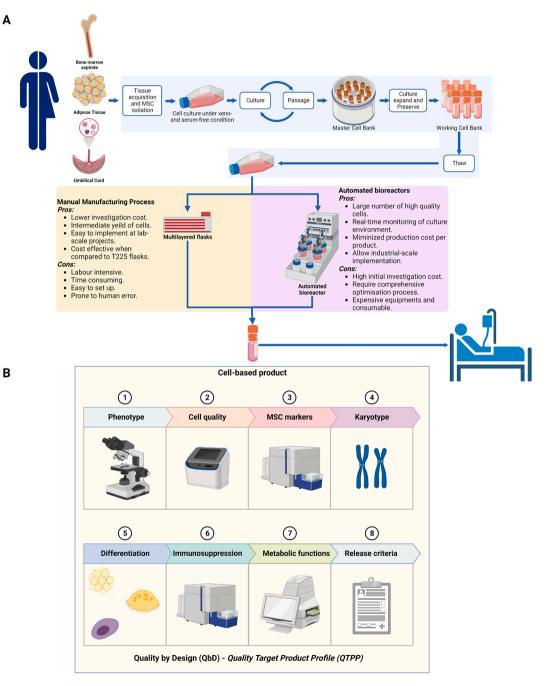
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approximately 1400 clinical trials being conducted worldwide [8]. The popularity of this therapy originates from the unique nature of MSCs themselves, which have low immunogenicity due to a lack of HLA-DR expression, supporting their use as "allogeneic" or "off-the-shelf" products for therapeutic treatments [9]. In addition, MSCs have the ability to participate in immunoregulatory functions [10], immunosuppression and modulation of the host inflammatory response via cell-to-cell contacts and paracrine effects mediated by a wide range of secreted growth factors [11], cytokines and chemokines [12]. As many studies of MSCs have supported their safety and potential therapeutic effects in certain diseases, they have been considered advanced therapeutic medicinal products in Europe since 2006 [13–15]. Although the first administration of stem cells could be traced back to the late 1950s, MSC-based therapies for diverse medical indications have begun to be popular recently due to the rapid development of cultivation methods and standardized xeno-free and serum-free conditions [16]. To meet the high demand for MSCs in the clinical setting, the manufacturing process plays a critical



(caption on next page)

Fig. 1. Manufacturing process of an allogeneic MSC-based product under the Quality by Design principle for clinical applications. (A) Manufacturing process of an allogeneic MSC-based product under manual and automated culture conditions. MSC-based products can be derived from bone marrow, adipose tissue, or umbilical cord tissue, followed by culture under xeno- and serum-free conditions to establish a Token cell bank, master cell bank, and working cell bank for the manufacturing process. Conventional manufacturing processes (manual vs. automated) have both advantages and limitations, but there is a need for an interchangeable system that allows investors to easily switch from one to another depending on the scale of downstream applications of the product. (B) Cell-based product with the Quality by Design (QbD) principle and Quality Target Product Profile (QTPP). In the context of MSC-based products, a QTPP describes the desired characteristics of the product, including MSC morphology, cell viability/purity, MSC markers, karyotype, MSC differentiation, immunosuppression, and metabolic function. The QTPP was predefined to cover the identification of MSCs, the potency, the purity, and the safety requirements. The manufacturing process of an allogeneic MSC-based product under the QbD principle involves identifying critical quality attributes (CQAs), determining the impact of process parameters on the CQAs, and optimizing the process parameters within a design space. The resulting product is evaluated against the pre-defined QTPP to ensure that it meets the desired characteristics for clinical applications. The QbD strategy presented in this study provides a robust framework for the development and manufacture of MSC-based products that adhere to the highest standards of quality and safety, making them suitable for regulatory approval and clinical use.

role in ensuring that high-quality MSCs are generated and provided in time for patients in need. The manufacture of MSCs for clinical applications typically comprises several steps, such as the determination of MSC sources, the acquisition of the raw materials, isolation, expansion, harvest, purification, formulation, fill and finish, cryopreservation, thawing and quality control. Although the principle underlying the MSC manufacturing process is similar to that of other pharmaceutical products, the variability in cell sources, proliferation rates, and nonstandardized culture conditions introduce complexity and challenges to the manufacture of MSC-based products.

To address these challenges of the MSC manufacturing process, we propose a combination of standardized xeno- and serum-free culture conditions, cell line screening and selection, the advantages of the Quality by Design (QbD) approach, and a standardized manufacturing process using either manual planar culture or an automated system [17]. Since their initial discovery, MSCs have been cultured with media containing fetal bovine serum (FBS), which is of animal origin, has undefined components and exhibits batch-to-batch variations [18]. The multitude of components found in serum greatly affect the proliferation and potency of cultured cells, especially MSCs, resulting in variations in their therapeutic potential [19]. Moreover, serum also has the risk of high endotoxin levels, hemoglobin effects, infectious agents, and supply concerns related to the availability of GMP-grade serum for the cell manufacturing process [20]. Thus, the use of xeno-free and serum-free culture conditions has emerged as an alternative approach for MSC expansion for downstream clinical applications. The recent establishment of standardized xeno-free and serum-free culture conditions that allow the use of a single platform to support the expansion of MSCs derived from bone marrow, adipose tissue, and the UC provides a powerful tool to directly compare the similarities and differences of these sources [16]. In addition, xeno- and serum-free culture conditions allow more consistent performance, better reproducibility, and stable large-scale production of cell-based products. As culture conditions could be standardized and stabilized using xeno- and serum-free culture conditions, for a consistent cellular manufacturing process, a stable cell line is needed to provide a good master and working cell bank. Umbilical cord tissue is easy to obtain using a noninvasive method, there is no ethical barrier, and the acquisition procedure does not introduce any potential risk or harm to newborns and mothers. We proved that UC-MSCs cultured under standardized xeno- and serum-free culture conditions had great proliferation ability and could be expanded in a large-scale process [16]. These advantages provide us with a unique opportunity to establish stable cell lines via genetic screening and biological function selection processes. Therefore, it has been suggested that when manufacturing such complex and variable products as cell-based therapeutic agents, it is of the utmost importance to acknowledge that any changes and variations in the expansion process, regardless of how minor, might directly affect the quality of the final products, which is a critical point for a cell-based therapy in relation to the safety and efficacy of the treatment.

An increasing number of stem cell-based therapies are being developed and used, together with an increasing number of regulatory approvals being issued worldwide, resulting in a pressing need for large-scale production procedures and industrial translation [21, 22]. Thus, an efficient, cost-effective manufacturing process and compliance with regulations are important for the success of stem cell-based clinical trials. Currently, cellular manufacturing processes are manual and semiautomated and are mostly performed under laboratory-scale and planar culture conditions [21]. They are time consuming, labor intensive, and often involve open processes, which limit their applications in large-scale expansion at the industrial scale [23]. As a result, they are prone to human error and largely experience-dependent, and they can result in batch-to-batch variability, lack of reproducibility, increased production costs, and an increased risk of culture contamination. To address the current challenges of manual cell culture, the introduction of multilayered cell culture flasks to enhance the scale-up process from single-layered T-flasks provides an alternative approach for the cellular manufacturing industry [24]. Recent advances in culture vessel design allow researchers to not only upscale the process but also reduce medium consumption, make the process less labor intensive and increase cell numbers. In terms of automated platforms, bioreactor systems are the most widely used methods for culturing cells to harvest proteins, as they are scalable, amenable to the integration of environmental control and real-time monitoring of the cell culture, and capable of an automated response to changes in culture conditions to maintain a high protein yield [25]. However, these systems are designed and optimized to obtain the highest yield of the protein of interest but do not prioritize the quality of the cells themselves. Thus, the use of bioreactors needs to be carefully considered to allow cells of the best quality to be produced and harvested. However, there has been no direct comparison of the quality of MSCs produced via either multilayered flasks or automated culture platforms to date.

A direct comparison between a manual manufacturing process and its automated counterpart allows researchers and investigators

Table 1	
Genome sequencing of 20 cell lines.	

4

Cell line	Mutation gene	Position	Variations	Location	Homozygous/ heterozygous	Variant classification	Traits	Disease
UC-1	TGM1	14:24,261,783	c.420A > G p.(Ile140Met)	Missense	Heterozygous	Likely pathogenic	Recessive	Congenital Ichthyosis
	ADSL	22:40,358,950	c.569G > A p.(Arg190Gln)	Missense	Heterozygous	Likely pathogenic	Recessive	Adenylosuccinase deficiency
	MYO15A	17:18,154,745	c.8215delG p.(Ala2739ProfsTer15)	Frameshift	Heterozygous	Not reported on ClinVar (**)	Recessive	Deafness 3
UC-2	SLC22A5	5:132,385,435	c.832C > T p.(Arg278Ter)	Stop-gained	Heterozygous	Pathogenic	Recessive	Systemic primary carnitine deficiency
	POLG	15:89,319,065	c.3139C > T p.(Arg1047Trp)	Missense	Heterozygous	Likely Pathogenic	Recessive	Alpers disease
	CCDC88C	14:91,321,256	c.1391G > A p.(Arg464His)	Missense	Heterozygous	Not reported on ClinVar (**)	Dominant	Spinocerebellar ataxia
UC-3	AGPAT2	9:136,674,750	c.646A > T p.(Lys216Ter)	Stop-gained	Heterozygous	Likely pathogenic	Recessive	Lipodystrophy type 1
	UROC1	3:126,508,419:126,508,418	c.405_408dupGGCT p.(Gln137GlyfsTer57)	Frameshift	Heterozygous	Not reported on ClinVar (*)	Recessive	Urocanase deficiency
UC-4	MMACHC	1:45,508,870: 45,508,882	c.507_519delAGAGGTGCCAGAT p.(Glu170CysfsTer36)	Frameshift	Heterozygous	Pathogenic	Recessive	Methylmalonic Aciduria and homocystinuria, type cblC
	USH2A	1:215,671,222	c.13883delC p.(Pro4628LeufsTer6)	Frameshift	Heterozygous	Not reported on ClinVar (*)	Recessive	Usher syndrome 2A/Retinitis pigmentosa
UC-5	HPS4	22:26,458,578	c.1714-1G > T	Splice acceptor	Heterozygous	Not reported on ClinVar (*)	Recessive	Hermansky-Pudlak syndrome
	РАН	12:102,855,326	c.517G > T p.(Gln172His)	Missense	Heterozygous	Not reported on ClinVar (**)	Recessive	Phenylketonuria
	G6PD	X:154,533,122	c.961G > A p.(Val321Met)	Missense	Heterozygous	Likely pathogenic	Dominant	G6PD deficiency
	ITGA3	17:50,081,328	c.2839C > T p.(Arg947Ter)	Stop_gained	Heterozygous	Not reported on ClinVar (**)	Recessive	Congenital interstitial lung disease, nephrotic syndrome, epidermolysis bullosa
UC-6	ATP7B	13:51,950,132	c.2605G > A p.(Gly869Arg)	Missense	Heterozygous	Pathogenic	Recessive	Wilson disease
	TTR	18:31,592,974	c.148G > A p.(Val50Met)	Missense	Heterozygous	Pathogenic	Dominant	Familial amyloidosis with polyneuropathy type 1
	SLC34A2	4:25,662,843	c.250 + 1G > A	Splice donor	Heterozygous	Not reported on ClinVar (*)	Recessive	Pulmonary alveolar microlithiasis
	TPM3	1:154,159,025	c.688C > T p.Arg230Ter	Missense	Heterozygous	Not reported on ClinVar (*)	Dominant/ Recessive	Myopathy
	ALDH5A1	6:24,502,592:24,502,593	c.424_425delAT p.(Ile142HisfsTer3)	Frameshift	Heterozygous	Not reported on ClinVar (*)	Recessive	Succinic semialdehyde dehydrogenase deficiency
UC-8	GCNT2	6:10,528,925	c.14G > A p.Trp5Ter	Stop-gained	Heterozygous	Not reported on ClinVar (**)	Recessive	Cataract
	DTNA	18:34,838,756	c.1184delG p.(Ser395ThrfsTer2)	Frameshift	Heterozygous	Not reported on ClinVar (**)	Dominant	Left ventricular noncompaction

Heliyon 9 (2023) e15946

Table 1 (continued)

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Cell line	Mutation gene	Position	Variations	Location	Homozygous/ heterozygous	Variant classification	Traits	Disease
UC-9	RYR1	19:38,443,612	c.325C > T p.(Arg109Trp)	Missense	Heterozygous	Likely pathogenic	Recessive	Congenital myopathy
	AMPD1	1:114,677,465	c.1373G > A p.(Arg458His)	Missense	Heterozygous	Likely pathogenic	Recessive	Myopathy due to myoadenylate deaminase deficiency
	USH2A	1:215,648,564	c.14546G > A p.(Trp4849Ter)	Stop_gained	Heterozygous	Not reported on ClinVar (*)	Recessive	Usher syndrome 2A/Retinitis pigmentosa
UC-12	PAH	12:102,855,326	c.517G > T p.(Gln172His)	Missense	Heterozygous	Not reported on ClinVar (*)	Recessive	Phenylketonuria
UC-16	COL12A1	6:75,181,213	c.1892-2A > G	Splice acceptor	Heterozygous	Not reported on ClinVar (*)	Dominant/ Recessive	Bethlem myopathy 2 /Ullrich congenital muscular dystrophy 2
	ANO5	11:22,272,913:22,272,912	c.2159_2160dupTA p.(Ala721Ter)	Frameshift	Heterozygous	Not reported on ClinVar (**)	Dominant/ Recessive	Gnathodiaphyseal dysplasia/ Muscular dystrophy
UC-18	SLCO1B1	12:21,222,355	c.1738C > T p.(Arg580Ter)	Stop gained	Heterozygous	Pathogenic	Multiple recessive gene	Digenic hyperbilirubinemia
	PSEN2	1:226,885,652	c.472delG p.(Val158CysfsTer15)	Frameshift	Heterozygous	Not reported on ClinVar (**)	Dominant	Alzheimer/Dilated Cardiomyopathy
UC-20	CPOX	3:98,585,631	c.982C > T p.(Arg328Cys)	Missense	Heterozygous	Likely pathogenic	Dominant	Coproporphyria
	SLC22A5	5:132,392,565	c.1472C > G p.(Ser491Cys)	Missense	Heterozygous	Pathogenic	Recessive	Systemic primary carnitine deficiency
	MVK	12:109,596,554	c.1168C > T p.(Gln390Ter)	Stop-gained	Heterozygous	Not reported on ClinVar (**)	Dominant/ Recessive	Porokeratosis/Mevalonic aciduria/Hyper-IgD syndrome
	GJB2	13:20,189,473	c.109G > A p.(Val37Ile)	Missense	Heterozygous	Pathogenic	Recessive	Digenic deafness
	G6PD	X:154,533,122	c.961G > A p.(Val321Met)	Missense	Heterozygous	Pathogenic	Dominant	G6PD deficiency
	IGSF3	1:116,600,246	c.1784G > A p.(Trp595Ter)	Stop-gained	Heterozygous	Pathogenic	Recessive	Lacrimal duct defect
	PDE6A	5:149,933,932	c.715C > T p.(Gln239Ter)	Stop-gained	Heterozygous	Not reported on ClinVar (*)	-	Retinitis pigmentosa
UC-21	ABCA4	1:94,008,252	c.5881G > A p.(Gly1961Arg)	Missense	Heterozygous	Pathogenic	Recessive	Stargardt disease
	FANCD2	3:10,081,465	c.3224 + 1G > T	Spice donor	Heterozygous	Not reported on ClinVar (*)	Recessive	Fanconi anemia
UC-22	ATP7B	13:51,949,772	c.2755C > T p.(Arg919Trp)	Missense	Heterozygous	Likely pathogenic	Recessive	Wilson syndrome
	ITGA7	12:55,694,633	c.2259delC p.(Met754Ter)	Frameshift	Heterozygous	Not reported on ClinVar (**)	Recessive	Congenital muscular dystrophy
UC-23	CHAT	10:49,619,786:49,619,785	c.451_466dupCGACACTTGGTGTCTG p.(Glu156AlafsTer6)	Frameshift	Heterozygous	Not reported on ClinVar (**)	Recessive	Congenital myasthenic syndrome

(continued on next page)

Table 1 (continued)

Cell line	Mutation gene	Position	Variations	Location	Homozygous/ heterozygous	Variant classification	Traits	Disease
UC-25	PIGT	20:45,416,673	c.344G > A p.(Trp115Ter)	Stop-gained	Heterozygous	Not reported on ClinVar (**)	Dominant /Recessive	Paroxysmal nocturnal hemoglobinuria/Multiple congenital anomalies- hypotonia-seizures syndrome
	LMF1	16:854,610:854,609	c.1610_1626dupGGAAGAGGATCGGAGCC p.(Tyr543GlyfsTer16)	Frameshift	Heterozygous	Not reported on ClinVar (**)	Recessive	Lipase deficiency
	GJB2	13:20,189,347	c.235delC p.(Leu79CysfsTer3)	Frameshift	Heterozygous	Pathogenic	Recessive	Digenic deafness
UC-27	CLPB	11:72,372,923	c.736+2T > C	Splice donor	Heterozygous	Not reported on ClinVar (*)	Recessive	3-methylglutaconic aciduria type 7, cataracts, neurologic involvement and neutropenia
UC-28	ACE	17:63,494,382	c.3292C > T p.(Gln1098Ter)	Stop-gained	Heterozygous	Not reported on ClinVar (*)	Recessive	Renal tubular dysgenesis
	EIF2B5	3:184,138,239	c.758delC p.(Ser253PhefsTer25)	Frameshift	Heterozygous	Not reported on ClinVar (*)	Recessive	Leukoencephalopathy/ Ovarioleukodystrophy
	TRMT1	17:18,154,745	c.394_395delAG p.(Ser132Ter)	Frameshift	Heterozygous	Not reported on ClinVar (*)	Recessive	Intellectual development disorder
UC-29	EVC2	4:5,622,562	c.2476C > T p.(Arg826Ter)	Stop-gained	Heterozygous	Pathogenic	Recessive	Ellis-van Creveld syndrome
	COG4	16:70,514,334	c.544+1G > T	Splice donor	Heterozygous	Not reported on ClinVar (*)	Dominant/ Recessive	Saul-Wilson syndrome/ Congenital disorders of glycosylation
	OFD1	X:13,751,358	c.1045G > T p.(Glu349Ter)	Stop-gained	Heterozygous	Not reported on ClinVar (*)	X-linked dominant/ recessive	Orofaciodigital syndrome/ Joubert syndrome, Simpson- Golabi-Behmel syndrome, retinitis pigmentosa
	GIGYF2	2:232,844,096:232,844,095	c.3002_3003insGC p.(Gln1002HisfsTer70)	Frameshift	Heterozygous	Not reported on ClinVar (**)	-	Parkinson disease
	ΟΤΟΑ	16:21,736,318	c.2359G > T p.(Glu787Ter)	Stop-gained	Heterozygous	Not reported on ClinVar (**)	Recessive	Deafness
UC-30	WNT10B	12:48,968,025	c.632G > A p.(Arg211Gln)	Missense	Heterozygous	Likely pathogenic	Dominant	Selective tooth agenesis
	GJB2	13:20,189,473	c.3292C > T p.(Gln1098Ter)	Missense	Heterozygous	Pathogenic	Recessive	Digenic deafness

(*): Not reported on ClinVar, pathogenic. (**): Not reported on ClinVar, likely pathogenic.

to transform from laboratory-based manufacturing to the industrial scale without extensive investigations to optimize the process. In our opinion, a successful optimization process that demonstrates that the equivalent quality of cell products generated via the manual manufacturing process and the automated culture platform would become a driving force for the cell-based therapy process (Fig. 1). One might use the manual process to generate enough cells for small-scale applications of targeted cell-based therapy, such as phase I and II clinical trials or the early stage of the commercialization process, where a small number of patients are included and the target doses are used at a lower pace. At a larger scale with a high demand for high-quality cells, one might switch from a manual process to an automated culture process, allowing a higher number of cells to be produced with equivalent quality and characteristics similar to those of the cells produced via the manual process (Fig. 1A). According to the guidelines CPMP/ICH/5721/03 ICH topic Q5E "Comparability of Biotechnological/Biological products" and EMA/CAT/499821/2019 Committee for Advanced Therapies (CAT), the comparability is a key concept in the development, manufacture and evaluation of the biological product, in which, any changes before and after manufacturing process or any other relevant factors should not alter the quality of the product. Thus, achieving a consistent efficacy of cell-based therapy heavily depends on the consistent quality of the cell products, which is achieved via a reliable manufacturing process. In addition, the QbD principle was implemented to ensure that the quality of MSC-based products generated using either manual manufacturing (multilavered flasks) or an automated cell culture platform under xeno-free and serum-free conditions was maintained throughout the procedure [17]. The QbD is defined as a scientific, risk-based approach for cellular manufacturing design that is based on product and process attributes that contribute to product quality. The success of the QbD principle relies on a thorough understanding of the cellular biology and culture process underlying a product and its manufacture. It

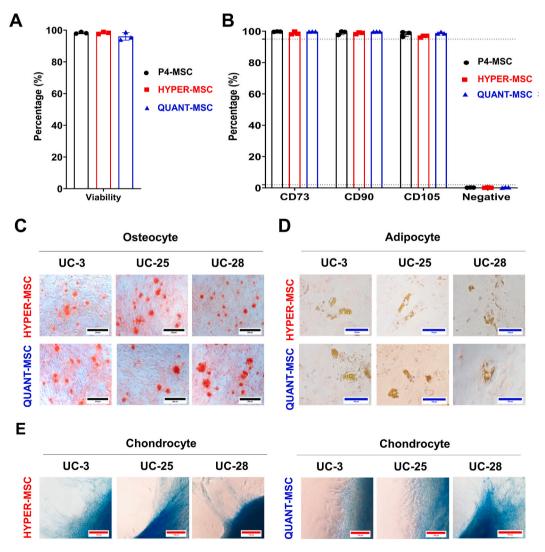
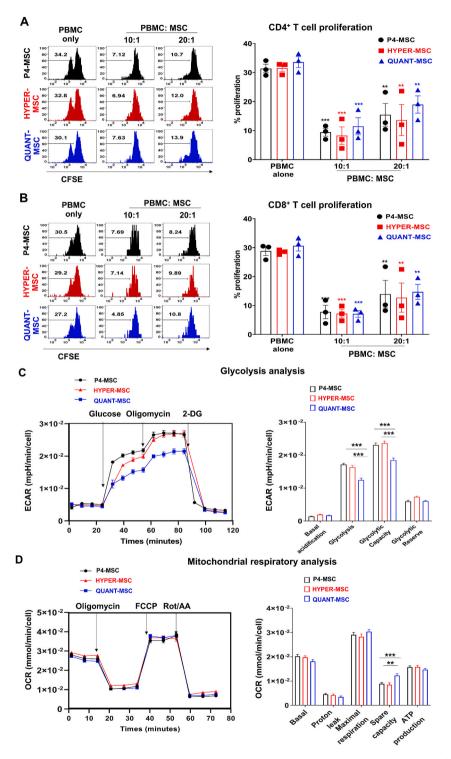


Fig. 2. Characterization of UC-MSCs manufactured with the Quantum Cell Expansion system and HYPERflasks. (A) Cell viability for QUANT-MSCs (96.05 \pm 1.4%) and HYPER-MSCs (98.25 \pm 0.4%) after optimized harvesting. (B) Flow cytometry analysis of MSC surface markers (positive: CD73, CD90, and CD105; negative: CD11, CD19b, CD34, CD45, and HLR-DR) for P4-MSCs, QUANT-MSCs, and HYPER-MSCs showing no significant differences. (C–E) Trilineage differentiation potential of QUANT-MSCs and HYPER-MSCs into (C) osteocytes, (D) adipocytes, and (E) chondrocytes.

usually starts with a detailed description of the quality characteristics of the desired product, in our case, MSCs, followed by a detailed investigation of the attributes that directly influence product quality throughout the manufacturing process and the development of a design space that considers the effects of these attributes on quality to identify potential solutions to minimize their detrimental effects (Fig. 1B). A comprehensive review on the QbD principle can be found in a previous publication [17,26]. Thus, an experimental design



(caption on next page)

Fig. 3. Immunomodulatory effects and metabolic activities of UC-MSCs manufactured with the Quantum Cell Expansion system and HYPERflasks. (A) Proliferation of CD4⁺ T cells in the presence of P4-MSCs, QUANT-MSCs, and HYPER/MSCs. Percentage of CD4⁺ T cell proliferation in the presence of P4-MSCs, HYPER-MSCs, and QUANT-MSCs at PBMC:MSC ratios of 10:1 and 20:1 compared to the control (PBMCs only). (B) Proliferation of CD8⁺ T cells in the presence of P4-MSCs, QUANT-MSCs, and HYPER/MSCs. Percentage of CD8⁺ T cell proliferation under the same conditions as in (A). Results demonstrate that both QUANT-MSCs and HYPER-MSCs significantly suppress the proliferation of CD4⁺ (A) and CD8⁺ (B) T cells. No significant differences were observed in the suppression of T cell proliferation among P4-MSCs, HYPER-MSCs, and QUANT-MSCs, indicating that both HYPERFlask and Quantum manufacturing methods did not alter the immunoregulatory effects of hUC-MSCs. (C) Glycolysis capacity of P4-MSCs, QUANT-MSCs, and HYPER/MSCs. QUANT-MSCs show reduced glycolysis and glycolytic capacity compared to P4-MSCs, and HYPER-MSCs, including basal respiration rate, proton leakage, maximal respiration, and ATP production, are similar among P4-MSCs, QUANT-MSCs, and HYPER-MSCs. QUANT-MSCs exhibit a higher spare respiratory capacity than input cells (P4-MSCs) and HYPER-MSCs.

in accordance with QbD principle plays a critical role in manufacturing process and involves the following steps: (1) define the objective/quality target product profile (QTPP), (2) identify critical process parameters (CPPs), (3) develop a design space, (4) define the control strategy, (5) conduct experiments, (6) analyze the results, (7) develop a final control strategy, and (8) monitor and review. Here, we describe the process of screening and selecting stable MSCs, followed by identification the QTPP of the MSC products according to the QbD principle. Based on the QTPP, the experiment design was conducted to direct comparisons of MSCs produced via a manual manufacturing process and their counterparts produced via an automated platform to identify the CPPs and critical quality attributes (CQAs) of the two processes (Fig. 1). The results of our study provide a standardized platform supporting the manufacturing process of allogeneic MSC-based therapy under manual and automated culture conditions.

2. Results

2.1. Establishment of clinical-grade UC-MSC lines for the cellular manufacturing process

In the primary screening process, 22 out of 30 parents participated in genetic consulting and answered 97 questions related to inherited diseases, infant medical history, parental medical background, and lifestyle and behavior. The results indicated that two families had scores higher than 32, which is our established threshold for cut-off; thus, the two UC-MSC lines derived from these two families were excluded from the secondary screening (Supplementary Fig. 1A). The results of cellular characterization showed that all UC-MSC lines expressed normal MSC markers (Supplementary Figs. 1B–C) and had population doubling times from 18 to 24 h. However, five UC-MSC lines had CFU-F numbers lower than 200 CFU-F/1000 cells (Supplementary Fig. 1D), three UC-MSC lines were unable to differentiate into either osteocytes or chondrocytes (Supplementary Table 3), and one UC-MSC line did not undergo the differentiation assay. These lines and one UC-MSC line derived from the same donor as another line were excluded. The 20 remaining UC-MSC lines were subjected to final screening by genome sequencing of 6700 genes using the TRUESIGHT ONE EXPANDED kit. The genomic sequencing strategy and quality results are shown in Supplementary Table 4. Our data showed that three out of 20 UC-MSC lines had pathogenic and dominant mutations at *G6PD* and *TTR*, which led us to exclude these lines from the pool. Although the remaining 17 UC-MSC lines carry genetic mutations, these mutations are mostly recessive with normal phenotypes (Table 1). Taken together, the combination of the primary, secondary and final screening processes indicated that 17 out of 30 UC-MSC lines met the requirement for production of the master cell bank at passage 2 (P2) and the working cell bank at P4. Three out of 17 lines were then randomly selected for the cellular manufacturing process.

2.2. Optimization of the automated cell culture platform and manual manufacturing process for large-scale expansion of UC-MSCs under xeno-free and serum-free conditions

As our UC-MSC lines cultured under xeno-free and serum-free culture conditions required CellStart coating for long-term expansion using single-layered T flasks, we first investigated whether this coating is required when culturing UC-MSCs using HYPERFlask. Two different concentrations of CellStart were used, 1:300 and 1:500 dilutions, and compared to the uncoated flask. The results showed that there were no significant differences in terms of cell yield, days in culture, cell viability, MSC markers, or karyotype between coated and noncoated flasks (Supplementary Table 5). These results confirm that coating is not required for MSC culture using HYPERflasks. Although there were fluctuations in cell yield between batches, these differences resulted from the HYPERFlask handling skills, which were later optimized to allow an equal distribution of cells across the 10 layers of the flask. At a seeding density of 3500 cells/cm², the maximum yield of UC-MSCs peaked at 110×10^6 cells/flask after 4 days of culture.

Next, we investigated the coating reagents for the Quantum bioreactor using either 2 mL CellStart or vitronectin at different concentrations (2.5, 4.5, or 10 mg). Coating the bioreactor with 2 mL CellStart yielded the lowest number of harvested viable cells (53 × 10⁶ cells) after 9 days in culture. While coating the bioreactor with 2.5 mg vitronectin generated 380×10^6 cells from 17×10^6 input cells after 8 days in culture, the use of 4.5 mg vitronectin with 17×10^6 fresh input cells resulted in 270×10^6 cells and 380×10^6 cells after 3 days and 6 days in culture, respectively. However, we noticed a reduction in CD105 marker expression in the two batches, with values of 90.8% and 85.6%, respectively. Further increasing the concentration of vitronectin to 10 mg enhanced the numbers of harvested viable cells to (773 ± 140) × 10⁶ cells from (26 ± 2) × 10⁶ fresh-thawed cells (n = 3, mean \pm SEM), with normal MSC marker expression (Supplementary Table 6). Taken together, these results suggested that 10 mg vitronectin is the most suitable coating

reagent for a quantum bioreactor that supports the attachment and expansion of UC-MSCs under xeno-free and serum-free conditions.

2.3. Comparative analysis of UC-MSCs produced from Quantum Expansion system and the HYPERFlask platform

2.3.1. Biological analysis

To explore the differences in terms of cell production quality between the Quantum Cell Expansion system and the HYPERFlask platform, the biological characteristics of UC-MSCs generated from these two systems (called QUANT-MSCs and HYPER-MSCs) were first explored using the minimal guidelines of ISCT for MSC identification [27]. As three UC-MSC lines (passage 4) were used as the starting cell sources for both platforms, these cells (called P4-MSCs) were used as controls for a direct comparison between the two systems. Although there was a difference in cell yield between the two systems, the harvesting method was optimized, with equivalent and high cell viability (96.05 \pm 1.4% for QUANT-MSCs and 98.25 \pm 0.4% for HYPER-MSCs) (Fig. 2A). Analysis of MSC surface markers, including positive markers (CD73, CD90, and CD105) and negative markers (CD11, CD19b, CD34, CD45, and HLR-DR), indicated no significant differences between P4-MSCs (99.79 \pm 0.08% CD73, 99.04 \pm 0.71% CD90, 98.27 \pm 0.93% CD105, and 0.19 \pm 0.04% negative markers), QUANT-MSCs (99.86 \pm 0.04% CD73, 99.83 \pm 0.04% CD90, 98.91 \pm 0.34% CD105, and 0.35 \pm

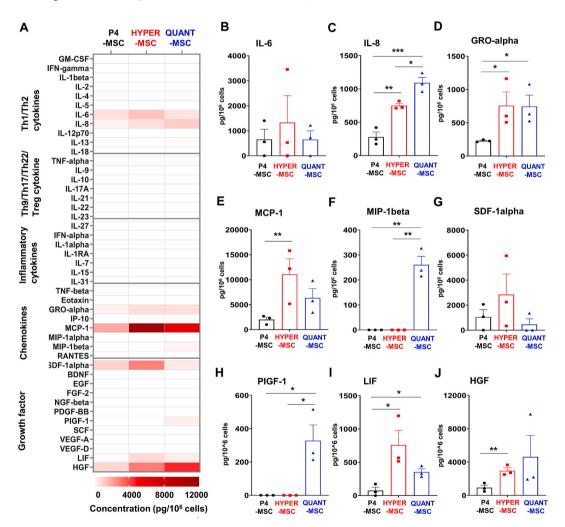


Fig. 4. Supernatant cytokine secretion profiles of UC-MSCs expanded in the Quantum Cell Expansion system and HYPERflasks. Levels of 45 cytokines, chemokines, and growth factors were measured in the cell culture media for QUANT-MSCs, HYPER-MSCs, and P4-MSCs. (A) A heatmap of supernatant cytokines, chemokines, and growth factors released by UC-MSCs expanded in the Quantum Cell Expansion system and HYPERflasks. No induction of cytokines related to Th9, Th17, Th22, or T regulatory cell responses or inflammatory cytokines in any of the cell groups. (B) Higher levels of IL-6 secretion in HYPER-MSCs compared to QUANT-MSCs. (C) Higher levels of IL-8 secretion in QUANT-MSCs compared to HYPER-MSCs. (D) Similar GRO-alpha secretion levels in QUANT-MSCs and HYPER-MSCs, both significantly higher than in P4-MSCs. (E) Higher MCP-1 and (G) SDF-1 α levels in HYPER-MSCs compared to QUANT-MSCs. (J) Higher HGF levels in QUANT-MSCs compared to HYPER-MSCs. (I) Higher LIF levels in HYPER-MSCs produce high levels of cytokines, chemokines, and growth factors with slightly different secretion profiles. QUANT-MSCs tend to release higher levels of growth factors, chemokines, and Th1/Th2 cytokines than HYPER-MSCs.

0.09% negative maker), and HYPER-MSCs (98.78 \pm 0.52% CD73, 98.83 \pm 0.33% CD90, 96.73 \pm 0.38% CD105, and 0.14 \pm 0.07% negative makers) (Fig. 2B). Both QUANT-MSCs and HYPER-MSCs were able to differentiate into osteocytes (Fig. 2C), adipocytes (Fig. 2D), and chondrocytes (Fig. 2E). Taken together, the results showed that QUANT-MSCs and HYPER-MSCs are equivalent in terms of MSC phenotype according to ISCT guidelines.

2.3.2. Immunoregulatory analysis

To reveal the immunoregulatory function of QUANT-MSCs and HYPER-MSCs, we investigated their ability to suppress the proliferation of activated T cells *in vitro*. The results showed that the percentages of proliferation of both CD4⁺ T cells (Fig. 3A) and CD8⁺ T cells (Fig. 3B) in the presence of UC-MSCs at ratios of PBMC:UC-MSC = 10:1 and 20:1 were markedly lower than those of T cells cultured in the presence of PBMCs only. In the absence of UC-MSCs, the percentage of CD4⁺ T cell proliferation was $32.17 \pm 0.85\%$. However, in the presence of MSC at PBMC: MSC = 10: 1 and 20:1, percentages of CD4⁺ T cell proliferation were $9.4 \pm 1.4\%$ and $15.4 \pm 3.9\%$ (P4-MSCs) $8.3 \pm 3\%$ and $13.6 \pm 5.4\%$ (HYPER-MSCs), and $11.5 \pm 2.9\%$ and $18.9 \pm 2.9\%$ (QUANT-MSCs), respectively (Fig. 3A). Similarly, while the percentage of CD8⁺ T cell proliferation without MSCs was $29.3 \pm 0.8\%$, the percentages of the cell proliferation was reduced when co-cultured with MSC at both ratios, PBMC: MSC = 10: 1 and 20:1 ($7.8 \pm 2.3\%$ and $13.9 \pm 4.8\%$ for P4-MSC, $7.2 \pm 1.5\%$ and $12.7 \pm 5.04\%$ for HYPER-MSCs, and $7.1 \pm 1.2\%$ and $14.7 \pm 2.6\%$ for QUANT-MSCs, respectively) (Fig. 3B). These data indicated that both QUANT-MSCs and HYPER-MSCs significantly suppressed the proliferation of both CD4⁺ T cells (Fig. 3A) and CD8⁺ T cells (Fig. 3B). Importantly, there was no significant difference in the percentages of proliferation of both CD4⁺ T cells and CD8⁺ T cells when using UC-MSCs from the two systems and P4-MSCs, suggesting that manufacturing hUC-MSCs using both HYPERFlask and Quantum did not alter the immunoregulatory effects of the cells.

2.3.3. Metabolic activities

In terms of glycolysis, QUANT-MSCs exhibited a significant reduction in glycolysis and glycolytic capacity $(1.2 \pm 0.06 \times 10^{-2} \text{ and } 1.8 \pm 0.07 \times 10^{-2}$, respectively) compared to P4-MSCs $(1.7 \pm 0.04 \times 10^{-2} \text{ and } 2.3 \pm 0.07 \times 10^{-2}$, respectively) and HYPER-MSCs $(1.6 \pm 0.06 \times 10^{-2} \text{ and } 2.4 \pm 0.07 \times 10^{-2}$, respectively) (Fig. 3C and D). No significant differences in the basal glycolytic rate or glycolytic reserve in UC-MSCs were found among P4-MSCs, QUANT-MSCs and HYPER-MSCs. Analysis of mitochondrial activities showed that both QUANT-MSCs and HYPER-MSCs had a basal respiration rate, proton leakage, maximal respiration, and ATP production $(1.8 \pm 0.07 \times 10^{-2}, 0.3 \pm 0.04 \times 10^{-2}, 3.0 \pm 0.08 \times 10^{-2}, \text{ and } 1.5 \pm 0.05 \times 10^{-2}$, respectively, for QUANT-MSCs and $(2.0 \pm 0.06 \times 10^{-2}, 0.4 \pm 0.05 \times 10^{-2}, 0.4 \pm 0.05 \times 10^{-2}, 2.9 \pm 0.10 \times 10^{-2}$, and $1.6 \pm 0.06 \times 10^{-2}$, respectively. However, QUANT-MSCs exhibited a higher spare respiratory capacity $(1.2 \pm 0.08 \times 10^{-2})$ than input cells $(0.9 \pm 0.05 \times 10^{-2})$ and HYPER-MSCs $(0.8 \pm 0.08 \times 10^{-2})$ (Fig. 3C and D).

2.3.4. Growth factor and cytokine secretion profile

To elucidate the growth factor and cytokine secretion profile of OUANT-MSCs and HYPER-MSCs, the levels of the 45 cytokines, chemokines, and growth factors were measured in both cell culture media and the UC-MSC-derived EVs of the three selected cell lines and their input P4-MSCs. In terms of secretion into the culture media, OUANT-MSCs, HYPER-MSCs and P4-MSCs did not induce cytokines related to Th9, Th17, Th22, or T regulatory cell responses, including IL-9, IL-10, IL-17A, IL-21, IL-22, IL-23, and IL-27, or inflammatory cytokines, including TNF-alpha, IL-1 alpha, IL-1RA, IL-7, IL-15, IL-31, and TNF-beta (Fig. 4A). HYPER-MSCs tended to secrete higher levels of IL-6 than QUANT-MSCs (Fig. 4B) (1327.4 \pm 1074.7 pg/10⁶ cells vs 648.4 \pm 354.1 pg/10⁶ cells), while QUANT-MSCs released higher levels of IL-8 than HYPER-MSCs (Fig. 4C) (1091.7 \pm 81.4 pg/10⁶ cells vs 750.3 \pm 34.1 pg/10⁶ cells). Both QUANT-MSCs and HYPER-MSCs released similar level of GRO-alpha (745.95 \pm 169.3 pg/10⁶ cells vs 757.1 \pm 204.6 pg/10⁶ cells, respectively), and significantly higher than that of P4-MSCs (229.1 \pm 9.6 pg/10⁶ cells) (Fig. 4D). The levels of the chemokines MCP-1 (Fig. 4E) and SDF-1 α (Fig. 4G) were higher in HYPER-MSCs than in QUANT-MSCs (MCP-1: 11062.0 \pm 3129.2 pg/10⁶ cells vs 6351.1 \pm 1861.6 pg/10⁶ cells; SDF-1 α : 2844.1 \pm 1647.2 pg/10⁶ cells vs 453.2 \pm 453.2 pg/10⁶ cells). However, MIP-1 β (Fig. 4F) and PLGF-1 (Fig. 4H) were secreted by QUANT-MSCs ($0.4 \pm 33.9 \text{ pg}/10^6$ cells and $328.3 \pm 94.6 \text{ pg}/10^6$ cells, respectively) but not HYPER-MSCs. LIF levels were higher in HYPER-MSCs (Fig. 4I) (759.9 \pm 219.4 pg/10⁶ cells vs 354.1 \pm 48.4 pg/10⁶ cells), but HGF levels were higher in QUANT-MSCs (Fig. 4J) (4623.9 \pm 2560.7 pg/10⁶ cells vs 2959.4 \pm 355.1 pg/10⁶ cells). Collectively, our data revealed that both methods generated UC-MSCs with the ability to produce high levels of cytokines, chemokines and growth factors. The UC-MSCs obtained via each method showed slightly different secretion profiles, and culturing UC-MSCs in the Quantum system tended to result in the release of secretion factors with higher levels of growth factors, chemokines and Th1/Th2 cytokines than those observed for cells cultured in HYPERflasks.

2.3.5. EV characterization

To characterize EVs from QUANT-MSCs (EV/QUANT-MSCs), HYPER-MSCs (EV/HYPER-MSCs) and P4-MSCs (EV/P4-MSCs), EV morphology was observed by TEM, and total protein was measured by a bicinchoninic acid assay (Fig. 5). EVs comprise a heterogeneous population of vesicles, including exosomes and microvesicles with different sizes and shapes (Fig. 5A, red arrow). EV/QUANT-MSCs and EV/HYPER-MSCs were found to be similar in morphology (Fig. 5A). EV/QUANT-MSCs and EV/HYPER-MSCs presented higher levels of total protein than EV/P4-MSCs (Fig. 5B), suggesting that QUANT-MSCs and HYPER-MSCs could release more EVs than P4-MSCs.

Next, EV-derived growth factors, chemokines, and cytokines were examined by a Luminex assay. Similar to EV/P4-MSCs, EV/ QUANT-MSCs and EV/HYPER-MSCs did not produce cytokines related to Th9, Th17, Th22, and T regulatory responses, including IL-9, IL-10, IL-17A, IL-21, IL-22, and IL-27, or inflammatory cytokines, including IFN-alpha, IL-1 alpha, IL-1RA, IL-7, IL-15, IL-31, and TNFbeta (Fig. 5C). The levels of Th1/Th2-related cytokines (IL-8), chemokines (MCP-1) and growth factors (FGF-2 and HGF) were found to be higher in EV/QUANT-MSCs ($2.9 \pm 1.7 \text{ pg}/10^6$ cells IL-8, $15.1 \pm 8.8 \text{ pg}/10^6$ cells MCP-1, $63.48 \pm 19.59 \text{ pg}/10^6$ cells FGF-2, and $37.5 \pm 16.8 \text{ pg}/10^6$ cells HGF) and EV/HYPER-MSCs ($0.31 \pm 0.31 \text{ pg}/10^6$ cells IL-8, $5.5 \pm 2.3 \text{ pg}/10^6$ cells MCP-1, $30.96 \pm 11.17 \text{ pg}/10^6$ cells FGF-2, and $14.4 \pm 1.5 \text{ pg}/10^6$ cells HGF) than in EV/P4-MSCs ($0 \text{ pg}/10^6$ cells IL-8, $3.3 \pm 1.98 \text{ pg}/10^6$ cells MCP-1, $7.3 \pm 3.2 \text{ pg}/10^6$ cells FGF-2, and $2.2 \pm 1.1 \text{ pg}/10^6$ cells HGF) (Fig. 5D, F, H, I). Regarding Th1/Th2 cytokines, while EV/QUANT-MSCs showed significantly higher levels of IL-8 than EV/HYPER-MSCs (Fig. 5D), EV/HYPER-MSCs had higher levels of TNF- α than EV/QUANT-MSCs (TNF- α : $3.8 \pm 2.2 \text{ pg}/10^6$ cells vs $0.99 \pm 1.7 \text{ pg}/10^6$ cells, respectively) (Fig. 5E). EV/QUANT-MSCs showed higher levels of growth factors (FGF-2 and HGF), chemokines (MCP-1) and Th1/Th2 cytokines (IL-8) than those of EV/HYPER-MSCs (Fig. 5D, F, H, I). A higher level of RANTES was found in EV/QUANT-MSCs ($2.8 \pm 2.5 \text{ pg}/10^6$ cells) than in EV/HYPER-MSCs ($0.24 \pm 0.15 \text{ pg}/10^6$ cells), but there was no statistically significant difference between the EVs (Fig. 5G). Taken together, these results confirmed that EV/QUANT-MSCs are able to produce higher levels of growth factors, chemokines and Th1/Th2 cytokines and Th1/Th2 cytokines than EV/HYPER-MSCs.

3. Discussion

The establishment of a high-quality master cell bank plays a crucial role in the cellular manufacturing process for downstream clinical applications. In our study, 30 UC-MSC lines that were obtained in a previous study and cultured under xeno-free and serumfree culture conditions were subjected to a screening process to prepare a Token Cell stock (premaster stock) at P1, Master Cell Bank (P2, P3) and Working Cell Bank (P4). Following the International Stem Cell Bank Initiative (ISCBI) guidelines, our selected UC-MSCs were cultured under standardized xeno- and serum-free conditions, and all results met the minimal criteria for MSC identification established by the ISCT [28]. In most studies, the genetic stability of MSCs has been evaluated using diploid Geimsa-banded karyotype techniques to confirm the normal karyotype, which represents the genetic stability during culture [29,30]. All 30 UC-MSC lines used in this study have previously been proven to have a normal and stable karyotype after 7 passages [16]. However, it was reported that the accumulation of genetic changes can occur, which would not necessarily alter the higher-order characteristics of chromosomes or be detected by the G-banding technique [30]. Thus, to ensure high quality of the MSC bank, UC-MSCs that met our screening criteria were subjected to whole-genome sequencing, which is a high-resolution genetic analysis technique. Our results presented a genome-wide screen of UC-MSCs to identify cell lines that are suitable for downstream clinical application with minimal risks of carrying mutations related to cancer, metabolic disorder, cardiovascular disease, etc. In addition, our results also provided a starting data set for the identification of genetic variations in culture-expanded UC-MSCs, which further enhances the reliability of the cell sources during the manufacturing process. It was reported that the emergence of multiple low-frequency single nucleotide changes (SNCs) in primary MSCs does occur. However, early passages of MSCs in vitro did not show a dramatically increased mutation frequency, as human culture-expanded MSCs maintain a relatively stable genomic composition [31].

To establish a robust, reliable and reproducible manufacturing process, it is important that the principle of QbD be applied [32]. For any cell-based products generated under the QbD principle, the most important step is defining the quality target product profile, which describes in detail the properties of the desired end products, including production capacity, cellular identity, potency, and purity [33]. The definition and establishment of the QTPP are also the starting points of the QbD process. Thus, in our study, once the master and working cell banks were established, we created our QTPP for cell products generated via either manual or automated manufacturing processes. Typically, MSC-based products must meet all minimal criteria established by the ISCT to ensure the identification of MSCs throughout the manufacturing process. In fact, the minimal criteria are necessary but are not sufficient to ensure the high quality of MSC-based products. Thus, potency tests are introduced to provide a solid background on the functions of MSCs for their downstream clinical applications. In our study, potency tests, including investigations of immunosuppressive activity and MSC secretion profiles post-manufacture, were performed. As MSCs are known to deliver their therapeutic effects via effectors such as growth factors, cytokines and extracellular vesicles (EVs), it is important to evaluate the components and concentrations of secreted factors from MSCs post-manufacture to assess their potency prior to clinical applications. Identifying the QTPP and the CQAs are critical steps to ensure UC-MSC safety and efficacy and to provide background data for measurements and quality control to ensure robust manufacturing processes.

One of the major challenges of clinical trials is the conversion for laboratory-scale manufacturing to larger-scale for large trials (Phase III) or commercialization of products, which is also one of the critical process parameters (CPPs) [34]. This issue arises from the fact that the methods that are used at the laboratory scale to support small-scale trials might not be able to provide enough cells for larger trials, where billions of cells with equivalent quality and quantity are needed. Several studies have tried to adapt the manufacturing process from 2D culture to 3D platforms with automated culture systems without assessing the potency of MSC-based products [35]. In addition, several CQAs and CPPs of the QbD change significantly when methods are switched from small-scale to large-scale manufacturing, resulting in alteration of the therapeutic potential of the final product. Thus, the results of this study provide a solution to address these challenges. We proposed a system that allows easy switching from a small scale (i.e., using the HYPERflask system) to an adapted scale-out platform (i.e., Quantum Automated Cell Expansion System) to provide acceptable and equivalent MSC products under xeno-free and serum-free culture conditions without any changes in CQAs or QTPP under the QbD principle.

This study provides the first data set that directly compares the biological properties and potency of UC-MSCs generated via either manual (HYPERflasks) or automated manufacturing platforms (the Quantum Cell Expansion System). In terms of MSC characteristics, both QUANT-MSCs and HYPER-MSCs showed similar morphology, MSC markers, differentiation ability, and normal karyotypes. Our previous study demonstrated that providing a coating substrate allowed MSCs to proliferate and maintain their characteristics during

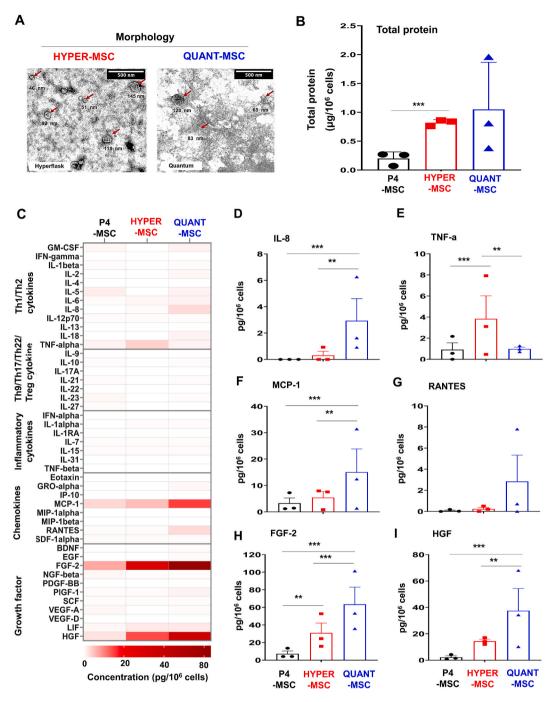


Fig. 5. Characterization of EVs derived from QUANT-MSCs, HYPER-MSCs, and P4-MSCs. (A) TEM observation of EV morphology, showing a heterogeneous population of vesicles, including exosomes and microvesicles with different sizes and shapes (red arrow). EV/QUANT-MSCs and EV/HYPER-MSCs exhibit similar morphology. (B) Higher total protein levels in EV/QUANT-MSCs and EV/HYPER-MSCs compared to EV/P4-MSCs, indicating greater EV release by QUANT-MSCs and HYPER-MSCs. (C) Luminex assay (heat map) results showing no production of Th9, Th17, Th22, T regulatory cell-related cytokines, or inflammatory cytokines in EV/QUANT-MSCs, EV/HYPER-MSCs, or EV/P4-MSCs. (D) Significantly higher IL-8 levels in EV/QUANT-MSCs compared to EV/HYPER-MSCs. (E) Higher TNF-α levels in EV/HYPER-MSCs than in EV/QUANT-MSCs and EV/HYPER-levels of Th1/Th2-related cytokines (IL-8), chemokines (MCP-1), and growth factors (FGF-2 and HGF) in EV/QUANT-MSCs and EV/HYPER-MSCs compared to EV/P4-MSCs. (G) Higher RANTES levels in EV/QUANT-MSCs compared to EV/P4-MSCs. (G) Higher RANTES levels in EV/QUANT-MSCs compared to EV/HYPER-MSCs. (F) Higher levels of DV/P4-MSCs. (G) Higher RANTES levels in EV/QUANT-MSCs compared to EV/HYPER-MSCs. (G) Higher RANTES levels in EV/QUANT-MSCs compared to EV/HYPER-MSCs. (F) Higher levels of growth factors, chemokines, and Th1/Th2 cytokines than EV/HYPER-MSCs. (F) respectively in this figure legend, the reader is referred to the Web version of this article.)

prolonged culture on T-flasks under xeno- and serum-free conditions. However, in this study, our results supported the elimination of the coating substrate for the HYPERflasks, which in turn reduced the manufacturing cost per cell product without changing the cell quality. These results were not surprising, as MSCs were propagated under either serum-free or serum-containing conditions and did not require a coating substrate when they were maintained in the HYPERflasks due to the unique treated culture surface [36]. For HYPERflasks, the maximum number of harvested cells was approximately 1×10^8 cells/flask, equivalent to a yield of approximately 25 T225 flasks, whereas the maximum number of harvested cells obtained from the Quantum system was 9×10^8 cells/run using our optimized protocol. The number of harvested cells was higher than that previously reported [37–39]. As cell quality and potency are tightly regulated by metabolic activities, it is important to understand how these cells behave under the culture conditions of HYPERflasks and the Quantum system. Our metabolic analysis revealed that QUANT-MSCs generated an amount of ATP equivalent to that generated by P4-MSCs and HYPER-MSCs while maintaining a lower glycolysis rate and glycolytic capacity. These data suggest that MSCs cultured on dynamic porous scaffolds (in the Quantum bioreactor with automated real-time feeding) showed higher glycolytic activity than cells cultured under the static 2D culture conditions found in HYPERflasks. As glycolysis is a critical energy production pathway in MSCs, recent studies demonstrated that increases in the glycolytic activity of MSCs improved their therapeutic effects in several disease conditions [40], upregulating their proliferation ability, enhancing their survival after transplantation, and increasing the secretion of growth factors and cytokines involved in tissue regeneration [41,42]. Interestingly, QUANT-MSCs also show higher respiratory spare capacity, supporting the notion that these cells confer better energy production via either glycolysis or mitochondrial respiration. This finding is consistent with the previous suggestion that mitochondrial activities play important roles in signal transmission in MSCs, especially for cell signals related to reactive oxygen species (ROS) [43], calcium homeostasis, and membrane potential. In fact, we speculated that the lower glycolysis rate and glycolytic capacity together with the higher respiratory spare capacity found in QUANT-MSCs illustrate energy compensation between glycolysis and mitochondrial respiration to maintain low levels of ROS, supporting previous findings [44,45].

MSCs usually exhibit therapeutic potential via a wide range of signaling molecules, including cytokines and growth factors. Our study showed that among 19 interleukins (ILs), only IL-6 and IL-8 were highly secreted from manufactured MSCs. The level of IL-6 was similar among all tested cell types, whereas QUANT-MSCs secreted the highest level of IL-8, followed by HYPER-MSCs and P4-MSCs. The secretion of IL-6 and IL-8 together with GRO-α and MCP-1 supports the ability of UC-MSCs from either the Quantum system or HYPERflasks to suppress PBMC proliferation in vitro [46]. Our findings are consistent with previous studies suggesting that MSCs from bone marrow, adipose tissue, and the umbilical cord secrete high levels of IL-6, IL-8, GRO-α, and MCP-1, and these chemokines can be detected in the supernatants of MSC-conditioned medium under xeno- and serum-free culture conditions [47,48]. Interestingly, we detected a high level of MIP-16, a specific chemokine involved in the anti-inflammatory response of MSCs, produced by HYPER-MSCs in their resting state [49]. Manufactured MSCs also showed high levels of growth factors, including PLGF-1, LIF and HGF, reflecting their high quality and potency after manufacture. It is now accepted that MSCs exert their therapeutic potential by communicating with other cells through a wide range of EVs. Our data showed a significant improvement in EV production from both HYPER-MSCs and OUANT-MSCs, with approximately 10 µg EV/1 million cells. The number of EVs produced via our optimized manufacturing platform could potentially meet the needs of clinical trials, such as trials of treatments for bronchopulmonary dysplasia (requiring 200 pmol EV/kg patient body weight, NCT03857841), dry eye (10 µg EV/drop, NCT04213248), or ischemic stroke (200 µg EV/patient, NCT03384433). A detectable number of exosomes was also found in conditioned medium from both the Quantum and Hyperflask culture platforms in our study, with the size of exosomes ranging from 30 to 150 nm. Detailed analysis of EV components, mostly cytokines, chemokines and growth factors, notably IL-8, TNF-α, MCP-1, RANTES, FGF-2, and HGF, showed a diverse range of EVs from both QUANT-MSCs and HYPER-MSCs. These factors are produced at high levels by manufactured MSCs.

In our study, we aimed to directly compare two manufacturing process of MSCs, including an automated cell culture system (Quantum Expansion System, Terumo) and a manual process using multilayer HYPERflask. By optimizing for both manufacturing processes, the results demonstrated the feasibility of generating high-quality MSC products with equivalent QTPPs. Our predefined QTPPs encompassed the CQAs such as MSC morphology, cell viability, MSC marker expression, karyotype, cytokine profile, exosome production and metabolic function. Despite differences in yield, the two manufacturing processes produced MSC products with comparable QTPPs. Our findings not only align with the principles set forth in QbD development, but also highlight the optimization process required in the CPMP/ICH/5721/03 ICH Topic Q5E "Comparability of Biotechnological/Biological Products" and EMA/CAT/ 499821/2019 Committee for Advanced Therapies (CAT) guidelines [50]. The results of our study illustrated the value of implementing a systematic approach for MSC-based product development, ensuring comparability, consistency, and reproducibility of the manufacturing process regardless of the chosen approach – automated culture system or multiplayer flask. By using the data provided from this study, researchers or manufacturers would save time and effort in conducting experimental design for MSC-based product, as our system employs xeno- and serum-free culture conditions with all materials being GMP-graded and commercially available. This optimized processes ensures that manufacturing platforms can be utilized interchangeably without compromising the quality, safety, or efficacy of the MSC-based products.

4. Conclusions

Overall, our study demonstrated that MSCs generated from the automated Quantum Expansion system and the manual HYPERflask approach under xeno- and serum-free conditions exhibited equivalent biological phenotypes, metabolic profiles, immunosuppression abilities, and secretion profiles (supernatant and extracellular vesicles). By adhering to the principles of the CPMP/ICH/5721/03 ICH Topic Q 5 E "Comparability of Biotechnological/Biological Products" and EMA/CAT/499821/2019 Committee for Advanced Therapies (CAT) guidelines, as well as incorporating the QbD strategy, our study contributes to the ongoing efforts to standardize and

improve MSC manufacturing processes in line with regulatory expectations. Furthermore, our research offers a valuable resource for other researchers or manufacturers looking to streamline the development of MSC-based products using either automated culture systems or multilayer flask approaches. Although the regulatory path for MSC-based products as advanced cell therapies has been proposed and accepted, certain challenges remain. One such problem might be the problem of MSC heterogeneity, as it is difficult to obtain a monoclonal MSC population. In addition, as our protocols generate MSCs without priming or stimulating factors, it is difficult to anticipate the potential therapeutic potential of these cells in their downstream applications.

5. Material and methods

5.1. Cell culture

All cell culture was conducted at 37 °C and 5% CO_2 in a humidified atmosphere. All culture reagents were purchased from Thermo Fisher and Miltenyi Biotec unless otherwise stated. All 30 UC-MSC lines were established under xeno- and serum-free culture conditions in a previous study. A single vial of each cell line at passage 0 (P0) was thawed and cultured to establish a master cell bank (at P1 and P2) and working cell bank (at P3).

5.2. Primary and secondary screening of UC-MSCs

Prior to initiating the cellular manufacturing process, we conducted screening of 30 established UC-MSC lines, which were previously fully characterized under xeno-free and serum-free conditions [16]. To start the screening process, all parents who participated in the previous project and donated their child's umbilical cord to establish the UC-MSC lines were invited to Vinmec International Hospital (Hanoi, Vietnam) to undergo genetic counseling using a prepared questionnaire containing 97 questions related to the infant's medical history, general health, family genetic background, clinical history of cancer, cardiovascular disease, diabetes, metabolic disorders, etc., and lifestyle and behavior (Supplementary Table 1). The scoring system was applied to select 20 lines that had a score less than 32 to enter the secondary screening. The secondary screening focused on the biological characterization of the UC-MSC lines following the International Society for Cell and Gene Therapy (ISCT) guidelines. Several criteria were set to evaluate the quality of the UC-MSCs, including population doubling time, karyotyping, number of colony-forming units (CFUs), MSC markers as ISCT guidelines, and differentiation ability (Supplementary Table 2). After two rounds of screening, the selected UC-MSC lines were subjected to whole-genome sequencing to exclude UC-MSC lines that carry genetic mutations related to cardiovascular disease, cancer, metabolic disorders, etc.

5.3. Genome sequencing of UC-MSCs

Once the culture of selected UC-MSCs at P2 reached 80% confluence, they were harvested for further expansion, and two million UC-MSCs were collected for DNA extraction using a QIAamp DNA Mini Kit (Qiagen). The DNA concentration and quality were measured with a Nanodrop and Quibit dsDNA BR Assay kits (Invitrogen, US). The TruSight One Expanded Sequencing Panel, which covers the coding regions of 6794 genes and 16.6 Mb of genomic content, was used for DNA library preparation, and then the size and quality of the DNA library were calculated by Quibit and Tape Station (Agilent, US). The NextSeq 550 High Output Kit (v2.5) was used for DNA sequencing. BWA-MEM and DRAGEN-GATK software were used for alignment and variant calling. Variants were classified according to ACMG and AMP guidelines by TAPE, ANNOVAR, and Variant Interpreter (Illumina, US). Three cell lines that met all screening criteria were randomly selected for the manufacturing process.

5.4. Manual manufacturing process of UC-MSCs using Corning® CellBIND® surface HYPERFlasks®

The selected UC-MSC lines at P4 were thawed in prewarm StemMACSTM MSC expansion medium (Miltenyi Biotec) and centrifuged at $500 \times g$ for 5 min at room temperature. The cells were then resuspended in StemMACS medium and reseeded into a T75 NuncTM EasYFlaskTM Cell Culture Flask at a density of 3200 cells/cm². Once the culture reached 80% confluence, the cells were incubated with TrypLE Select for 4 min at 37 °C and diluted with StemMACS medium, followed by centrifugation at $400 \times g$ for 5 min. The cells were counted and seeded into Corning[®] CellBIND[®] Surface HYPERFlask[®] cell culture vessels at a density of 3400 cells/cm². When the culture reached 80% confluence, the cells were harvested for further analysis and cryopreserved in CryoStor CS10 cell freezing medium (Stemcell Technologies, Canada), followed by storage in liquid nitrogen for further use.

5.5. Automated manufacturing process of UC-MSCs using the Quantum® Cell Expansion System

To expand UC-MSCs under xeno- and serum-free culture conditions using the Quantum® Cell Expansion System (Terumo BCT, USA), the cell expansion set was installed according to the manufacturer's protocol and primed with PBS. The standard operation protocol followed a previous study with modifications of a particular section [51]. The bioreactor was then coated with vitronectin (A14700, Thermo Fisher Scientific, 2.5–10 mg) in PBS overnight. On the following day, the bioreactor was washed with PBS to remove vitronectin residue followed by inoculation of 25×10^6 UC-MSCs at P4. The cells were cultured automatically under continuous flow of StemMACS medium at a low feeding rate with a premixed gas supply (20% O₂, 5% CO₂, and 75% N₂). The feeding rate was changed daily to meet the nutrient requirements of the cultured cells based on measurement of the glucose consumption rate using a glucose

meter (Arkrey, Japan) and lactate production levels using a lactate measurement device (Nova Biomedical, USA). The cells were harvested after 7 days in culture using 200 mL TrypLE Select, followed by neutralization using 400 mL PBS supplemented with human albumin (0.1%, vol/vol). The harvested cells were then subjected to other analyses, cryopreserved in CryoStor CS10 cell freezing medium (Stem Cell Technologies) in cryogenic vials at 20×10^6 cells/vial using a CryoMedTM Controlled-Rate Freezer (Thermo Fisher Scientific) and stored in liquid nitrogen for further use.

5.6. Comparative analysis of UC-MSCs generated via the manual and automated manufacturing platforms

5.6.1. Biological characterization

UC-MSCs harvested from either Corning® CellBIND® Surface HYPERFlask® cell culture vessels or the Quantum® Cell Expansion System were subjected to quality control tests, including tests for cell yield, cell viability (Trypan Blue), MSC markers and differentiation. The identification of MSCs included evaluations of the expression of positive MSC markers (CD73, CD90, and CD105) and negative markers (CD11b, CD19, CD34, CD45 and HLA-DR) using the Human MSC Analysis Kit (Becton Dickinson, USA). The cells were analyzed using a FACSLyric flow cytometer (Becton Dickinson, USA), followed by data analysis using FlowJo software. To assess differentiation ability, the harvested UC-MSCs were tested using a StemPro Osteogenesis, Adipogenesis, and Chondrogenesis Differentiation kit following the manufacturer's instructions. Once differentiation was completed, the cells were fixed with 4% paraformaldehyde and stained with Alizarin Red S, Oil Red O, and Alcian Blue to detect osteogenic, adipogenic, and chondrogenic lineages, respectively.

5.6.2. Metabolic activities

The cellular mitochondrial stress and glycolytic stress assays were performed using an Agilent Seahorse XFe96 Analyzer (Agilent Technologies) as previously described [52]. Briefly, 1×10^4 UC-MSCs in 100 µL of StemMACS medium were seeded into each well of Seahorse XF96 cell culture microplates (Agilent Technologies) coated with CTSTM CellStartTM (1:300 in PBS) and were then incubated overnight at 37 °C in 5% CO₂. The XFe96 Extracellular Flux sensor cartridges (Agilent Technologies) were hydrated with distilled water for 24 h, followed by incubation with Agilent Seahorse XF Calibrant (pH 7.4) (Agilent Technology) for 1 h at 37 °C in a non-CO₂ incubator before the assay. On the day of the experiment, the StemMACS medium from the microplates was removed, and the wells were rinsed with prewarm XF assay medium containing 10 mM glucose (Agilent Technologies, #103577-100), 2 mM glutamine (Agilent Technologies, #103579-100), and 1 mM pyruvate (Agilent Technologies, #103578-100). The wells were then filled with 180 µL of the XF assay medium, and the cell culture plates were incubated for 1 h at 37 °C without CO₂.

To measure the glycolytic function of hUC-MSCs, glucose (10 mM), oligomycin (1 μ M), and 2-deoxy-glucose (2-DG; 50 mM) from the Seahorse XF Cell Glycolysis Stress Test Kit (Agilent Technologies, #103020-100) were sequentially injected to establish parameters including basal acidification, glycolysis rate, glycolytic capacity, and glycolytic reserve. To measure the mitochondrial function of hUC-MSCs, oligomycin (1 μ M), fluoro-carbonyl cyanide phenylhydrazone (FCCP; 2.0 μ M) and rotenone (Rot; 0.5 μ M) together with antimycin A (AA; 0.5 μ M) from the Seahorse XF Cell Mito Stress test kit (Agilent Technologies, #103015-100) were sequentially injected to establish parameters, including basal respiration, proton leakage, maximal respiration, spare respiratory capacity, and ATP production. The cells were fixed with 4% paraformaldehyde (PFA) and stained with DAPI staining solution (1:5000, Abcam, #ab228549) after the assay. The ImageXpress® Micro Confocal High-content Imaging System (Molecular Devices) was used to count the cells in each well via DAPI staining for normalization.

5.6.3. Immunoregulation assay

Peripheral blood mononuclear cells (PBMCs) were isolated by the Ficoll gradient centrifugation method as previously described. The cells were then stored in CryoStor CS10 cell freezing medium at -80 °C until use. One day before coculture with MSCs, the cells were plated in RPMI medium supplemented with 10% FBS and 1% PS overnight. On the day of coculture, PBMCs were harvested and stained with carboxyfluorescein succinimidyl ester (CFSE) according to the manufacturer's instructions. Cryopreserved hUC-MSCs were thawed and plated in StemMACS medium for 3 days at 37 °C and 5% CO₂. The hUC-MSCs were then harvested and seeded in 96-well flat-bottom plates containing StemMACS medium at serial dilutions overnight for cell attachment.

For the T-cell proliferation assay, hUC-MSCs were washed with PBS and cocultured with 5×10^4 PBMCs/well in 200 µl RPMI in the presence of anti-CD2, anti-CD3, and anti-CD28 (α CD3/CD28) T-cell activation beads (Miltenyi Biotec) according to the manufacturer's instructions. After 5 days, all cells were harvested. To measure T-cell proliferation, all cells were stained with anti-CD3-V450, anti-CD4-APC-Vio770, and CD8-PE-Vio777 (Miltenyi Biotec) for 30 min at 4 °C. The cells were then stained with Cytox Red to discriminate a viable cell population and subjected to flow cytometry. All stained cells were acquired on a FACSLyric flow cytometer (BD). Fluorescence compensation was optimized using cells individually labeled with each fluorochrome-conjugated antibody. Data were obtained from the live population based on cell size- and morphology-based gating, which was used to eliminate cell debris and dead cells. The data were analyzed using FlowJo software (Tree Star).

5.6.4. Growth factor and cytokine secretion profile

The concentrations of 45 cytokines, chemokines, and growth factors were measured in the supernatant from MSC cultures and EV lysates using Cytokine/Chemokine/Growth Factor 45-Plex Human ProcartaPlex[™] Panel 1 (EPX450-12171-901) in accordance with the manufacturer's recommendations (MAN0019825) with a Luminex 200 instrument (Luminex Corporation, Austin, Texas, USA) and analyzed using ProcartaPlexAnalyst software; the evaluated cytokines included the following: Th1/Th2 cytokines: granulocyte-macrophage colony-stimulating growth factor (GM-CSF), interferon - gamma (IFN-γ), interleukin-1 beta (IL-1β), IL-2, IL-4, IL-5, IL-

6, IL-8, IL-12p70, IL-13, IL-18, and tumor necrosis factor-alpha (TNF- α); Th9/Th17/Th22/Treg cytokines: IL-9, IL-10, IL-17A (Cytotoxic T-lymphocyte-associated antigen-8 – CTLA-8), IL-21, IL-22, IL-23, and IL-27; inflammatory cytokines: IFN- α , IL-1 α , interleukin-1 receptor antagonist (IL-1RA), IL-7, IL-15, IL-31, and TNF- β ; chemokines: Eotaxin (C–C motif chemokine ligand 11 – CCL11), Growthrelated Oncogene alpha (GRO- α or C-X-C motif ligand 1 – CXCL1), Interferon-gamma inducible protein 10 (IP-10 or CXCL10), Monocyte chemoattractant protein-1 (MCP-1 or CCL2), Macrophage Inflammatory Protein 1 alpha (MIP-1 α or CCL3), MIP-1 β (CCL4), RANTES (CCL5), and Stromal cell-derived factor 1 alpha (SDF-1 α); and growth factors: brain-derived neurotrophic factor (BDNF), epidermal growth factor (EGF), fibroblast growth factor 2 (FGF-2), hepatocyte growth factor (HGF), nerve growth factor-beta (NGF- β), platelet-derived growth factor BB (PDGF-BB), placenta growth factor-1 (PIGF-1), stem cell factor (SCF), vascular endothelial growth factor-D (VEGF-D), vascular endothelial growth factor-A (VEGF-A) and leukemia inhibitory factor (LIF). After measurement, the values were normalized to the total number of harvested cells. Values less than the lowest limit of quantification (LLOQ) were assigned a value of 0.0 pg/mL. All samples were analyzed in duplicate according to the manufacturer's instructions.

5.6.5. Isolation and characterization of extracellular vesicles

After harvesting UC-MSCs via either the manual manufacturing process or the automated culture platform, the cell culture supernatants were collected for extracellular vesicle (EV) collection using the ultracentrifugation method as previously described [53]. Briefly, the supernatants were centrifuged at $300 \times g$ for 10 min at 4 °C to remove the cell pellet. The collected supernatants were then centrifuged at $2000 \times g$ for 20 min at 4 °C to remove dead cells and large EVs and then at $10,000 \times g$ for 30 min at 4 °C to remove cell debris. The supernatants were then centrifuged at $100,000 \times g$ for 70 min at 4 °C to collect pellets containing EVs and contaminating proteins. The pellets were washed with 10 mL PBS and subjected to an additional centrifugation at $100,000 \times g$ for 70 min at 4 °C to remove contaminating protein. The remaining EVs were resuspended in $100 \ \mu$ PBS and stored at $-80 \ ^{\circ}$ C for further use. To visualize and measure the EV size, TEM images of EV samples were obtained using a JEOL 1100 Transmission Electron Microscope (TEM, JEOL Ltd., Tokyo, Japan) at 80 kV. For visualization, EV samples were dropped and dried on a formvar- and carbon-coated copper grid (Ted Pella, Inc.).

5.6.6. Statistical analysis

Data are presented as the means \pm SEM. Significant differences among multiple groups were assessed using one-way ANOVA followed by Bonferroni's correction (ANOVA/Bonferroni). Pvalues < 0.05 were considered to be statistically significant. All analyses were performed using GraphPad PRISM software (GraphPad).

Author contribution statement

Duc M. Hoang: Conceived and designed the experiments; Performed the experiments; Analyzed and interpreted the data; Contributed reagents, materials, analysis tools or data; Wrote the paper.

Quyen T. Nguyen, Trang T.K. Phan, Anh T.L. Ngo, Phuong T. Pham: Performed the experiments; Analyzed and interpreted the data; Contributed reagents, materials, analysis tools or data; Wrote the paper.

Trung Q. Bach: Performed the experiments; Contributed reagents, materials, analysis tools or data; Wrote the paper.

Phuong T.T. Le, Hoa T.P. Bui: Performed the experiments.

Liem Nguyen Thanh: Conceived and designed the experiments; Contributed reagents, materials, analysis tools or data; Wrote the paper.

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Data availability statement

Data will be made available on request.

Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper

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Appendix A. Supplementary data

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