



## Research article

# A comparison between 2D and 3D cobalt–organic framework as catalysts for electrochemical CO<sub>2</sub> reduction

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## ABSTRACT

Electrocatalytic CO<sub>2</sub> reduction, as an effective way to reduce the CO<sub>2</sub> concentration, has gained attention. In this study, we prepared ZIF-67 nanoparticles and nanosheets and investigated them as electrocatalysts for CO<sub>2</sub> reduction. It was found that ZIF-67 nanosheets, because of their two-dimensional morphologies, provide more under-coordinated cobalt nodes and have lower overpotentials for both hydrogen evolution and CO<sub>2</sub> reduction reactions. Also, the rate-determining step for hydrogen evolution changes from Volmer for ZIF-67 nanoparticles to Hyrovsky for ZIF-67 nanosheets. Also, the presence of Mg<sup>2+</sup> ions in solution causes more facile CO<sub>2</sub> reduction, especially for ZIF-67 nanosheets.

## 1. Introduction

It is quite obvious that CO<sub>2</sub> emissions from burning fossil fuels are completely unavoidable, which is at the heart of the problem because it causes serious environmental and human health problems. To overcome these problems, the best approach is to convert CO<sub>2</sub> into hydrocarbon fuels such as methanol and methane as a renewable energy resource because CO<sub>2</sub> is a futuristic source of C1 feedstock for the production of fuels and value-added chemicals [1–3]. Electrochemical CO<sub>2</sub> reduction reaction (CO<sub>2</sub>RR) has received great interest recently, not only for decreasing CO<sub>2</sub> accumulation, as it could be a good process to produce valuable fuels with high energy density [4,5]. Metallic catalysts such as Au, Ag, Pd, and Zn are charming for electrochemical CO<sub>2</sub> reduction due to their excellent catalytic activity and selectivity, but it is practically impossible to use them on a large scale due to their scarcity and high price [6,7]. So far, many attempts have been made to design and synthesize efficient electrocatalysts for CO<sub>2</sub> reduction. However, despite many efforts, the high overpotential, poor product selectivity, and low Faradaic efficiency are still significant hurdles for further development of CO<sub>2</sub>RRs because much energy is required to reduce CO<sub>2</sub> molecules, which have a thermodynamically stable structure [8,9].

Metal–organic frameworks (MOFs) are formed by connecting metal ions and organic linkers through covalent coordination linkages [10,11]. MOFs have attracted much attention due to their attractive properties, such as tunable pore size, high porosity, high specific surface area, regular structure, and open metal sites [12,13]. On the other hand, due to the various types of catalytic sites present in the MOFs, they can provide the inherent advantages of both homogeneous and heterogeneous catalysts [14–17]. In addition, in the field of electrocatalysis, MOFs have been reported as effective electrocatalysts for overall water splitting and CO<sub>2</sub> reduction reactions because these materials contain both organic and inorganic sources [18–20]. Despite all the benefits listed above, some inherent shortcomings in these compounds cannot be ignored, such as conductivity, which leads to a significant reduction in the

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electrochemical applications of these compounds [21–23]. Fortunately, ultrathin two-dimensional (2D) MOF nanosheets (NSs) have attracted much attention in the field of electrocatalysis because of their crystalline structure, microporosity, conductivity, and abundance of exposed active sites [24–28]. Therefore, it is crystal clear that the 2D MOF NSs have the positive points of both MOFs and 2D nanomaterials and eliminate the negative points of MOFs [29]. In this regard, today we witness the widespread electrochemical applications of 2D MOF NSs in a wide variety of fields, especially in electrochemical CO<sub>2</sub>RR [30]. In the previous studies, several 2D MOF catalysts acquired excellent electrocatalytic performance for electrochemical CO<sub>2</sub>RR, such as ultrathin 2D nickel (II) ZIF NSs [31] and ultrathin 2D MOF NSs [TCPP(Co)/Zr–BTB] [32].

On the other hand, it has been shown that the concentration of Mg<sup>2+</sup> ions in the stroma has an important role in CO<sub>2</sub> fixation by chlorophyll [33,34]. Also, the addition of Lewis acid cations such as Mg<sup>2+</sup> ions to the electrolyte improves the catalytic behavior of cobalt phthalocyanine [35] and iron porphyrins [36,37] by the formation of a complex containing Mg<sup>2+</sup> and CO<sub>2</sub>. Due to these observations, researchers have investigated MOFs containing Mg metallic centers, such as Mg-MOF-74 [38] and Mg-centered porphyrin MOF [39]. In this study, for the first time, we have investigated the CO<sub>2</sub> electrochemical reduction in the solution containing Mg<sup>2+</sup> ions on the surface of zeolitic imidazolate framework-67 (ZIF-67), believing the unsaturated metallic nodes in ZIF-67 can make a complex called ZIF-67-CO<sub>2</sub>-Mg<sup>2+</sup> with the similar approach used by Wang et al. for cobalt–phthalocyanine molecules [35].

In this work, we synthesized ZIF-67 as an electrocatalyst for electrochemical CO<sub>2</sub> reduction. ZIF-67 is formed by bridging cobalt cations and 2-methylimidazolate anions with a pore size of about 0.34 nm, although, because of its flexible structure, the pore size may reach 0.4–0.45 nm values [40]. Based on the kinetic diameters of CO<sub>2</sub> gas molecules (0.33 nm), the presence of these pores can affect the exceptional selective capture and storage of CO<sub>2</sub> gas molecules [41]. This is a smart choice for two reasons: 1) Due to its appropriate pore size and selective adsorption abilities of CO<sub>2</sub>, ZIF-67 is an ideal candidate for electrochemical reduction of CO<sub>2</sub> because the CO<sub>2</sub> absorption on the electrode surface is very considerable, since the absorption of CO<sub>2</sub> on the electrode surface can reduce the activation energy of the electrochemical reduction [42]. 2) Cobalt is an earth-abundant metal and less expensive than noble metals, which form compounds with different valence states [43]. Additionally, herein we report an impressive method of morphology regulation to ameliorate the electrocatalytic performance of ZIF-67 without post-treatment. First, we synthesized ultrathin 2D ZIF-67 NSs from a mixed solution of 2-methylimidazole and cobalt using a controllable one-pot hydrothermal preparation strategy. Second, three-dimensional (3D) ZIF-67 nanoparticles (NPs) were successfully synthesized at room temperature (25 °C) in distilled water, which is environmentally friendly. Eventually, we observed that the ultrathin 2D ZIF-67 NSs represent a lower onset potential and superior electrocatalytic activity towards electrochemical CO<sub>2</sub> reduction in alkaline solution and both in the presence and absence of Mg<sup>2+</sup> ions in NaHCO<sub>3</sub> solution because the unsaturated cobalt active centers on the surface of ultrathin 2D ZIF-67 NSs could significantly elevate the electrochemical catalysis performance, which is enhanced in the presence of Mg<sup>2+</sup> ions due to ZIF-67 CO<sub>2</sub>-Mg<sup>2+</sup> complex formation.

## 2. Experimental section

### 2.1. Materials

All solvents and reagents studied were of analytical grade and used without further purification. All chemicals, 2-methylimidazole (C<sub>4</sub>H<sub>6</sub>N<sub>2</sub>, 99%), cobalt (II) nitrate hexahydrate (Co(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O, 98%), N, N-dimethylformamide (C<sub>3</sub>H<sub>7</sub>NO, 99.8%), ethanol (CH<sub>3</sub>CH<sub>2</sub>OH, 99.8%), and methanol (CH<sub>3</sub>OH, 99.8%), were purchased from Sigma–Aldrich. All aqueous solutions were prepared using high-purity deionized water (DI-water, resistance 18 MΩ cm<sup>-1</sup>).

### 2.2. Synthesis of ZIF-67 nanoparticles and nanosheets

For ZIF-67 nanoparticles, a solution of 2-methylimidazole (133.98 mmol, 11.00 g) in 45 mL deionized water was added to a solution of Co(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O (3.10 mmol, 0.90 g) in 10 mL deionized water and vigorously stirred for 7 h at 25 °C. The purple-colored precipitate was separated by centrifugation, washed with water, and dried at 25 °C for 72 h. The schematic of the synthesis procedure is

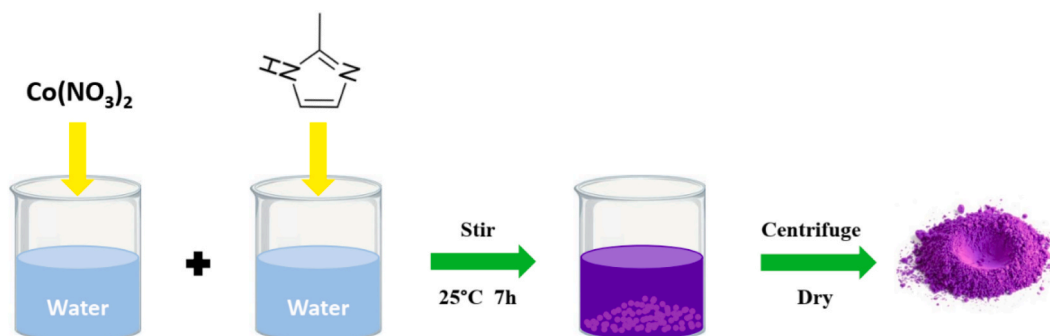


Fig. 1. The schematic of the synthesis procedure for ZIF-67 nanoparticles using the coprecipitation method.

displayed in Fig. 1.

For the synthesis of ZIF-67 nanosheets, 3.44 mmol of  $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  was dissolved in a mixed solution of 30 mL of deionized water, 30 mL of ethanol, and 30 mL of DMF under stirring. Then, 6.10 mmol of 2-methylimidazole was added to the above solution. After the complete dissolution of 2-methylimidazole, the mixture solution was immediately transferred into a Teflon-lined stainless steel autoclave with a 200 mL capacity. Subsequently, the autoclave was kept in an oven at  $160^\circ\text{C}$  for 12 h. Finally, the obtained samples were washed using methanol to remove the impurities and dried at  $100^\circ\text{C}$  in a vacuum for 12 h. Fig. 2 illustrates the schematic of the synthesis of ZIF-67 nanosheets.

### 2.3. Material characterization

Powder X-ray diffraction (XRD) patterns were obtained for synthesized samples using a Rigaku Ultima IV diffractometer equipped with a  $\text{Cu K}\alpha$  source ( $\lambda = 1.5406 \text{ \AA}$ ). Field emission scanning electron microscopy (FE-SEM, Mira3 TESCAN-XMU) was used for examining the morphology of the samples. An atomic force microscope (AFM) instrument (Bruker Dimension Icon) was employed to examine the size and thickness of the ZIF-67 NSs. To investigate the surface area and pore size distribution, Brunauer-Emmett-Teller (BET) and Barrett-Joyner-Halenda (BJH) were tested on Belsorp Mini II.

### 2.4. Electrochemical measurement

The thin film working electrodes were designed precisely the same as the prior electrodes by the electrophoretic deposition method [44–46]. All the electrochemical measurements were performed at  $25^\circ\text{C}$  by a conventional three-electrode cell, with a saturated  $\text{Ag}/\text{AgCl}$  as the reference electrode, an electrophoretically deposited material electrode as the working electrode, and a platinum grid as the counter electrode in an aqueous 1.0 M  $\text{KOH}$  electrolyte solution. The electrolytes for investigation of the effects of the presence of  $\text{Mg}^{2+}$  ions were considered as 0.1 M  $\text{NaHCO}_3 + 0.05 \text{ M NaCl}$  and 0.1 M  $\text{NaHCO}_3 + 0.05 \text{ M MgCl}_2$  solutions, similar to Wang et al.'s report [35], unless here we used chloride salts instead of their chlorate salts. Linear sweep voltammetry was carried out with the Solartron Electrochemical Interface SI 1287.

## 3. Results and discussions

The ZIF-67 NP has been synthesized at room temperature without the presence of any toxic solvent, which can be very beneficial for the production of MOFs on an industrial scale. The ZIF-67 NS is synthesized by a one-pot hydrothermal method; the most important advantage of this method is that it does not use any surfactant molecules.

The crystal structure of the as-prepared samples was examined by XRD. The powder XRD pattern of ZIF-67 NP is collected in Fig. 3 (A). It can be seen that the XRD pattern of the ZIF-67 NP sample is completely consistent with the simulated data from Jeong et al. [47], and no additional peaks are observed, which indicates the purity and the successful synthesis of the sample. As shown in Fig. 3(C), the XRD pattern of the ZIF-67 NS exhibits only first and second reflections from (211) and (422) crystallographic planes, emphasizing crystal growth under our synthetic conditions, which is restricted to these crystalline facets. This is quite obvious because, due to the measures adopted in the synthesis of this sample, it is expected that we will see growth limitations [48]. In Fig. 3(B) and (D), we have presented the crystal structures of ZIF-67 NP and ZIF-67 NS simulated using the CIF file of ZIF-67 [47] and Mercury 4.0 Software, respectively.

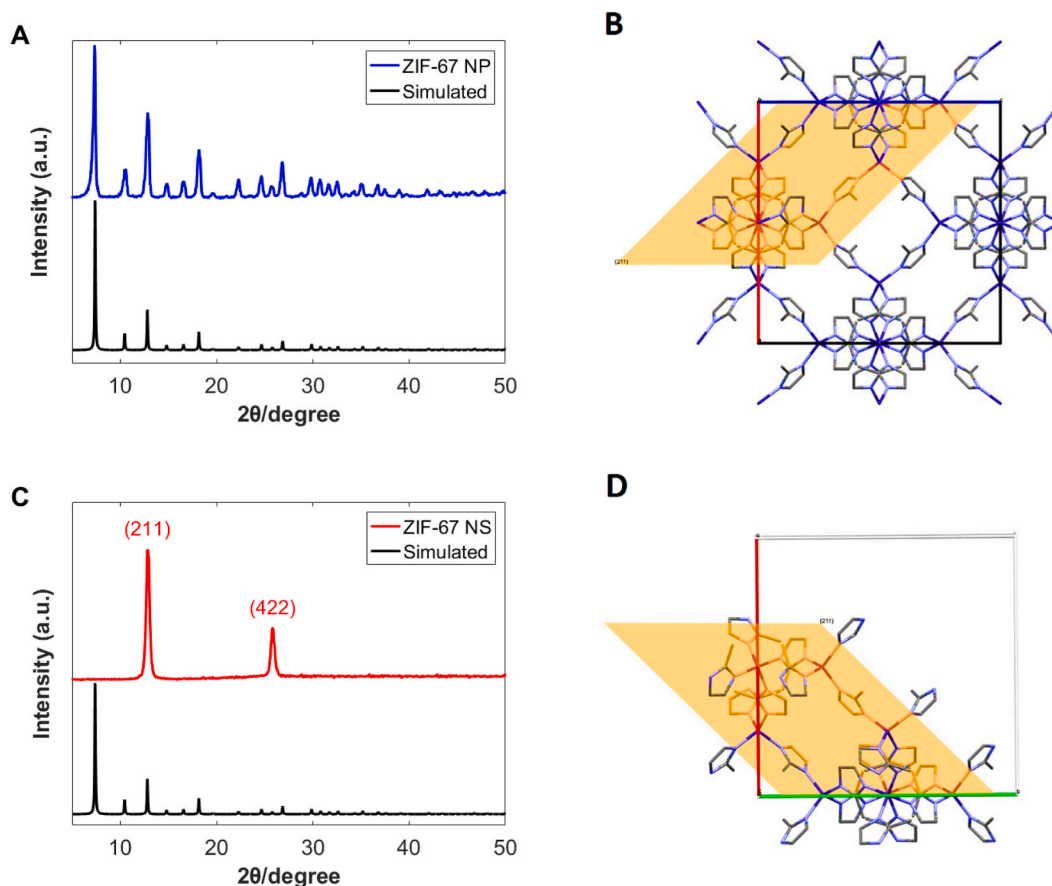
The morphology of both samples was characterized by FE-SEM analysis. Fig. 4 displays the FE-SEM images of the samples. As shown in Fig. 4(A) and (B), the prepared ZIF-67 NP illustrates a smooth surface with a rhombic dodecahedral shape. Fig. 4(C) and (D) demonstrate the FE-SEM images of the ZIF-67 NS, where the stacked nanosheets-like morphology of the sample is clearly visible.

The AFM analysis was used to assess the flake morphology and estimate the thickness of the single nanosheet. Based on the AFM image (Fig. S1), the thickness of ZIF-67 NS is smaller than 2 nm, which confirms the sheet morphology of the prepared ZIF-67 NS.

The  $\text{N}_2$  adsorption-desorption isotherms were employed to evaluate the porosity and surface area of the obtained MOFs. As shown in Fig. 5(A)–a typical type-I isotherm with an  $\text{H}_4$ -type hysteresis loop was observed for the ZIF-67 NP, which is characteristic of



Fig. 2. The schematic of the synthesis procedure for ZIF-67 nanosheets via the hydrothermal method.



**Fig. 3.** (A) Powder XRD patterns of simulated ZIF-67 (JCPDS: 671073) and ZIF-67 NP; (B) the crystal structure of ZIF-67 NP; (C) the XRD patterns of simulated ZIF-67 (JCPDS: 671073) and ZIF-67 NS; and (D) the crystal structure of ZIF-67 NS.

microporous materials [49]. For the ZIF-67 NS sample, we observe the type-III isotherm with an  $H_3$ -type hysteresis loop, which proves the confirmation of the layered structure of the sample, as depicted in Fig. 5(B) [50]. The comparison between these isotherms at low pressures shows that a huge amount of  $N_2$  gas is adsorbed on the surface of ZIF-67 NP compared to ZIF-67 NS because of its minimal porosity, and consequently, it will have a much greater contribution of external surface area in electrocatalysis with a smaller specific surface area compared to ZIF-67 NP [51]. This argument is verified by experimentally specific surface area determination, which shows ZIF-67 NP and ZIF-67 NS have BET surface areas of 953 and 127  $m^2 g^{-1}$ , respectively. The detailed textural parameters of both samples are listed in Table 1.

After the characterization of the prepared samples, they were investigated for electrochemical reduction of  $CO_2$ , a process that happens in negative potentials where cobalt nodes in ZIF-67 have already been reduced in alkaline solution via [52]:



The hydrogen evolution reaction (HER) is a competitor reaction for the  $CO_2$  reduction reaction [53]. Cobalt compounds have illustrated good activity towards HER and introduced a metallic cobalt center as the active site for HER, although the atmosphere around this center has an important role in accelerating water molecule adsorption as well as the desorption of intermediates in HER [43,54–57]. Also, it has been shown that the active site for  $CO_2$  reduction is cobalt atoms in cobalt-based electrocatalysts, which, with a nucleophilic attack, activate  $CO_2$  molecules [58–60]. Therefore, we expect competition between  $H_2O$  and  $CO_2$  molecules to be adsorbed on the surface of cobalt nodes. We used linear sweep voltammetry (LSV) to investigate this competition. We took the LSVs before and after bubbling the 1.0 M KOH solution with  $CO_2$  for both ZIF-67 NP and ZIF-67 NS electrodes.

$CO_2$  bubbling in alkaline solutions causes a decrease in the pH of these solutions because  $CO_2$  in alkaline solutions participates in hydrolysis equilibriums:



So different carbonaceous species ( $HCO_3^-$ ,  $CO_2$ ,  $CO_3^{2-}$ ) exist in the solution. The major species are dependent on the pH of the

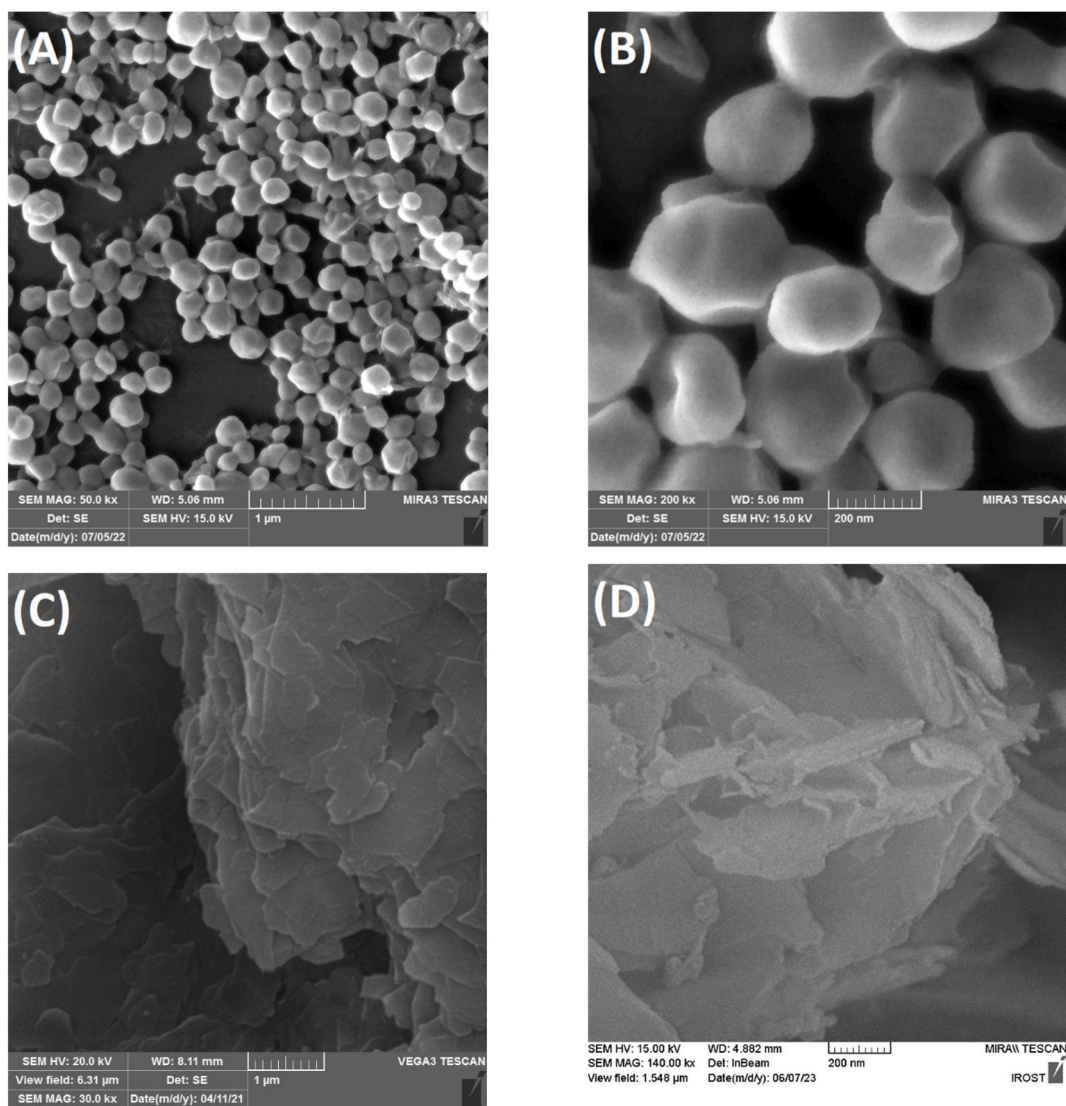


Fig. 4. FE-SEM images of (A) and (B) ZIF-67 NP, and (C) and (D) ZIF-67 NS with two different magnifications.

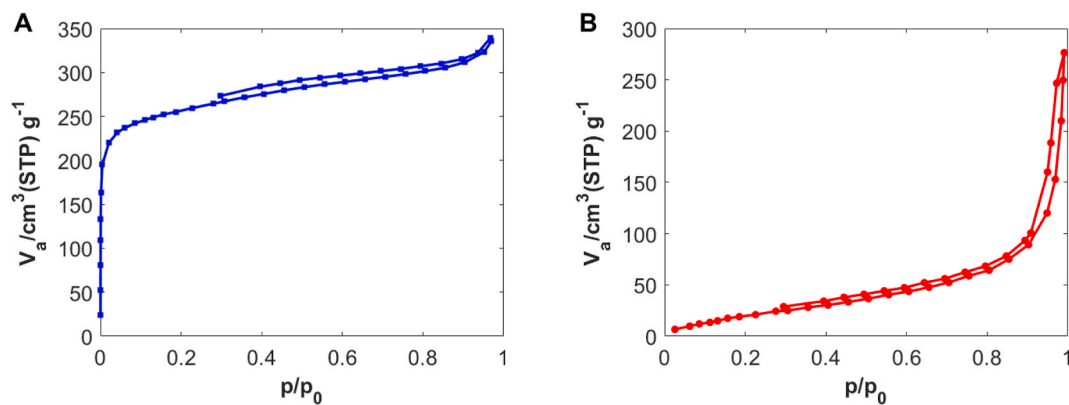


Fig. 5. The  $N_2$  adsorption-desorption isotherms of the prepared (A) ZIF-67 NP and (B) ZIF-67 NS.



**Table 1**

Results of the BET analysis for ZIF-67 NP and ZIF-67 NS.

Samples	BET surface area ( $\text{m}^2 \text{g}^{-1}$ )	Mean pore diameter (nm)	Total pore volume ( $\text{cm}^3 \text{g}^{-1}$ )
ZIF-67 NP	953	1.21	0.36
ZIF-67 NS	127	1.18	0.33

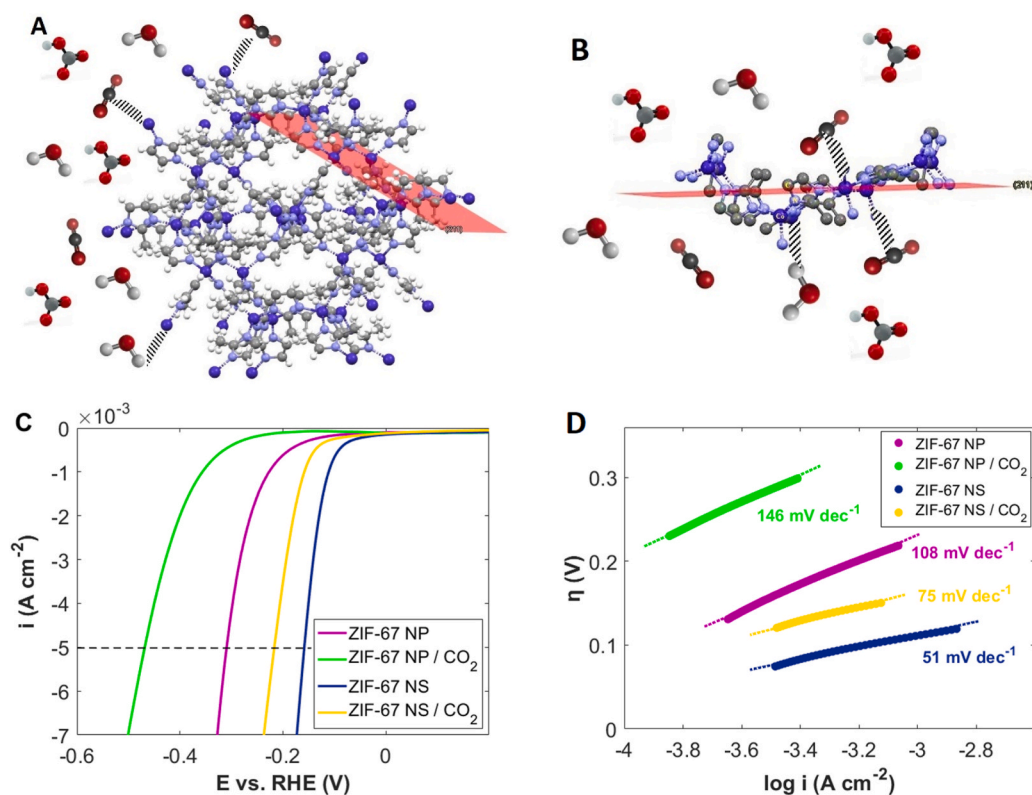
electrolyte. The pH of 1.0 M KOH solution reaches 7.0 with  $\text{CO}_2$  bubbling, where Fujii et al. reported that the dominant anion is  $\text{HCO}_3^-$  [61]. Therefore, the solutions have different pHs before and after  $\text{CO}_2$  bubbling. To remove the effects of pH on the potentials, we have calculated all potentials versus reversible hydrogen electrode (RHE) using:

$$E_{\text{RHE}}(\text{V}) = E_{\text{Ag}/\text{AgCl}} + 0.199 + 0.0592 \times \text{pH} \quad (4)$$

Where  $E_{\text{RHE}}$  and  $E_{\text{Ag}/\text{AgCl}}$  are potentials against reversible hydrogen electrode (RHE) and Ag/AgCl reference electrode, respectively.

Fig. 6(A) and (B) illustrate the existence of  $\text{CO}_2$ ,  $\text{H}_2\text{O}$ , and  $\text{HCO}_3^-$  around the ZIF-67 NP and ZIF-67 NS, respectively, and competition between  $\text{H}_2\text{O}$  and  $\text{CO}_2$  molecules to adsorb on the surface of cobalt atoms. Zheng et al. reported that the existence of  $\text{HCO}_3^-$  ions in the solutions during electroreduction of  $\text{CO}_2$  exhibits a transition from inhibitory to promotional effect by going to higher overvoltage [62], and we used this advantage in all parts of our  $\text{CO}_2$  reduction evaluation. Fig. 6(C) depicts linear sweep voltammetry (LSV) curves of HER in the presence and absence of  $\text{CO}_2$  bubbling for ZIF-67 NS and ZIF-67 NP in 1.0 M KOH solution at a scan rate of  $10 \text{ mV s}^{-1}$ . It is obvious that the presence of  $\text{CO}_2$  in the solution for both ZIF-67 morphologies exhibits a poisoning effect for HER [53]. This implies that either the  $\text{CO}_2$ -reduction intermediates blocked adsorptive sites, here cobalt nodes, for hydrogen adsorption, or chemical species in the solution or adsorbed on the surface led to the weakening of the bonding of hydrogen to the surface [63].

To compare the abilities of ZIF-67 NP and ZIF-67 NS towards  $\text{CO}_2$  reduction, we have obtained the overpotential values at a current density of  $5 \text{ mA cm}^{-2}$  ( $\eta_5$ ) in the presence and absence of  $\text{CO}_2$ , using LSVs presented in Fig. 6(C). The obtained results are tabulated and presented in Table 2. Therefore, we witness that the HER in the presence of  $\text{CO}_2$  is delayed for both samples and is observed at higher potentials because, first, the  $\text{CO}_2$  species are adsorbed on the electrode surface, and after the electrochemical  $\text{CO}_2$  reduction reaction, the produced products on the sites due to the high applied potential leave these sites, and then water molecules are adsorbed on these sites, and HER immediately occurs. In fact, such behavior has been reported for the transition metals, which have weak H-binding energy in HER volcano plot such as Cu and Co [63,64]. In the presence of  $\text{CO}_2$ , onset potential changes from  $-0.05$  to  $-0.15 \text{ V}$  and from



**Fig. 6.** The competition between  $\text{CO}_2$  and  $\text{H}_2\text{O}$  to adsorb on the (A) ZIF-67 NP and (B) ZIF-67 NS in the presence of  $\text{HCO}_3^-$  ions. (C) LSV and (D) Tafel plot for ZIF-67 NP and ZIF-67 NS in  $\text{CO}_2$ -saturated and without  $\text{CO}_2$  addition at 1.0 M KOH.

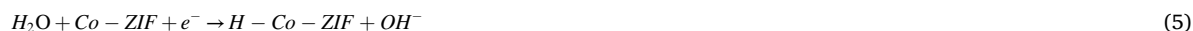
**Table 2**  
Overpotentials and Tafel slopes for ZIF-67 NS and ZIF-67 NP.

Samples	Electrolyte	$\eta_s$ (V)	Tafel slope (mV dec <sup>-1</sup> )
ZIF-67 NP	1.0 M KOH	0.31	108
	1.0 M KOH + CO <sub>2</sub>	0.44	146
ZIF-67 NS	1.0 M KOH	0.16	51
	1.0 M KOH + CO <sub>2</sub>	0.22	75

–0.20 to –0.30 V vs. RHE for ZIF-67 NS and ZIF-67 NP, respectively. This trend remains intact at more negative potentials compared to onset potentials [53]. The numerical values show that ZIF-67 NS exhibits lower overpotentials compared to ZIF-67 NP in both with and without CO<sub>2</sub> bubbling conditions. Yang et al. introduced the energy gap between the counter ion p–band and Co d–band centers as an effective descriptor, which is an optimal balance between H–atom adsorption and hydrogen molecule desorption from the surface [56]. In fact, factors such as size and morphology [54,65], counter ion or organic linker [57,66–69], doping, and defect engineering [57] could affect this descriptor. For our case, both samples have the same metallic nodes and organic linker, but the difference between them returns to the contribution of unsaturated cobalt nodes (under–coordinated), which are more activated than the regular cobalt nodes. As we have already mentioned for the interpretation of BET results, ZIF-67 NS has a smaller internal surface area, lower porosity, and a higher external exposure surface area, and consequently, a major contribution of under–coordinate cobalt nodes because of its 2D morphology compared to ZIF-67 NP. Thus, it is expected that the heat of adsorption of hydrogen atoms on the under–coordinate cobalt node will be greater than that of the regular nodes.

The linear part of the polarization curves (Tafel plot) for the HER in the presence and absence of CO<sub>2</sub> in a 1.0 M aqueous KOH solution has been indicated in Fig. 6(D). The ZIF-67 NS displays the lowest Tafel slopes in the presence and absence of CO<sub>2</sub> bubbling at 75 and 51 mV dec<sup>-1</sup>, respectively. Tafel slopes for ZIF-67 NP were calculated in the presence and absence of CO<sub>2</sub> bubbling at 146 and 108 mV dec<sup>-1</sup>, respectively.

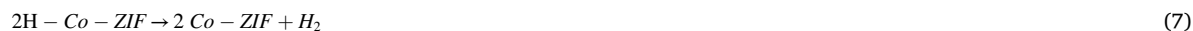
From the mechanistic viewpoint, the first step in HER is cleaving the O–H bond of adsorbed water molecules [52,70], here on the cobalt nodes of ZIF-67 (Co–ZIF), which is called the Volmer step with a Tafel slope of 120 mV dec<sup>-1</sup>:



and after that, HER occurs either via the reaction between another water molecule with an adsorbed hydrogen atom (Hyrovsky step) with a Tafel slope of 40 mV dec<sup>-1</sup>:

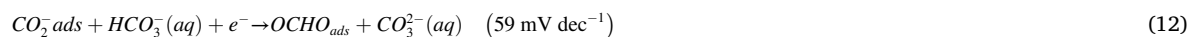
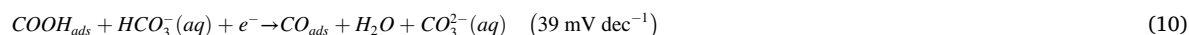
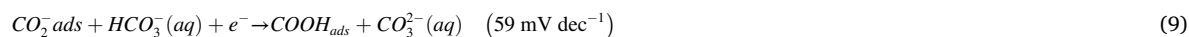


or via the reaction between two adsorbed hydrogen atoms (Tafel step) with a Tafel slope of 30 mV dec<sup>-1</sup>:



As the reported data in Table 2 illustrates, the Tafel slope values for ZIF-67 NS and ZIF-67 NP are close to the Hyrovsky and Volmer steps, respectively. It means the rate–determining step (RDS) for ZIF-67 NP is bond breaking in adsorbed water molecules, whereas for ZIF-67 NS, breaking the O–H bond of free H<sub>2</sub>O, desorption of adsorbed H, and formation of a free H<sub>2</sub> molecule are RDS. As we have already mentioned, in ZIF-67 NS, a greater number of cobalt nodes are under–coordinated and more reactive compared to ZIF-67 NP; consequently, the heat of adsorption assists the reactants to overcome the energy barrier in the Volmer step in the ZIF-67 NS case (see Fig. 6(C) and (D)).

However, because the Tafel slopes are taken around onset potentials in the presence of CO<sub>2</sub>, where a competition between HER and CO<sub>2</sub> reduction exists, the CO<sub>2</sub>–reduction mechanism should be considered when interpreting the Tafel slope values. The Tafels slopes have been calculated and reported for producing both CO and formate ions via different rate–determining steps [71,72]:



The first step is the common step for producing all CO<sub>2</sub> reduction products. Steps 9–11 have been suggested for CO production, while steps 12–14 have been considered for more stable liquid carbonaceous products, i.e., formate or formic acid. Our determined

Tafel slopes in the presence of CO<sub>2</sub> are 146 and 75 mV dec<sup>-1</sup> for ZIF-67 NP and ZIF-67 NS, respectively. It means the rate-determining step in CO<sub>2</sub> depends on the morphology of ZIF-67. Regarding its Tafel slope, the rate-determining step for CO<sub>2</sub>RR on the surface of ZIF-67 NP is reaction 8. Although the obtained values are larger than the calculated ones, the Tafel slopes of 140 mV dec<sup>-1</sup> in 0.1 M NaHCO<sub>3</sub> [73], 145 mV dec<sup>-1</sup> in 0.1 M NaHCO<sub>3</sub> [74], 141 mV dec<sup>-1</sup> in 0.5 M KHCO<sub>3</sub> [75], 148 mV dec<sup>-1</sup> in 0.5 M KHCO<sub>3</sub> [76], and 143–149 in 0.5 M KHCO<sub>3</sub> [77] have been reported for this rate-determining step on the surface of Au, Sn, Au/C, Ag, and Cu, respectively. It is expected that this reaction could be r.d.s. because, with an electroadsorption of CO<sub>2</sub> on the surface, the hybrid of carbon changes from sp to sp<sup>2</sup>, and the bond angle changes from 180° to 120°, and such changes require a lot of energy. However, a different situation exists for r.d.s. with a Tafel slope of 75 mV dec<sup>-1</sup> on the surface of ZIF-67 NS. It has been shown that such a Tafel slope could be related to a chemical reaction with a pre-equilibrium one electron transfer reaction as r.d.s. [78–83], i.e.:



Another point is that the difference between overpotentials in the presence and absence of CO<sub>2</sub> at a current density of 5 mV cm<sup>-2</sup> ( $\Delta\eta_5$ ) for ZIF-67 NS is smaller than that for ZIF-67 NP. Emphasizing the evacuation of occupied reactive sites by CO<sub>2</sub> reduction intermediates for ZIF-67 NS is more facile than ZIF-67 NP. The reason could be the effect of HCO<sub>3</sub><sup>-</sup> ion to promote the electroreduction of CO<sub>2</sub>, which acts as a proton donor and causes a sequential electron transfer–proton transfer mechanism to become dominant [62]. For both morphologies of ZIF-67, HCO<sub>3</sub><sup>-</sup> ion illustrates such behavior in high overpotentials. However, because of the 2D morphology of ZIF-67 NS, diffusion of HCO<sub>3</sub><sup>-</sup> ions between the layers is more facile [84,85] compared to inside the pores of ZIF-67 NP, and HCO<sub>3</sub><sup>-</sup> ions will be more available for CO<sub>2</sub> reduction intermediates.

Finally, we investigate the effects of the existence of Mg<sup>2+</sup> cations inside the electrolyte on CO<sub>2</sub> electroreduction. The reductive LSVs have been taken for both samples in two electrolytes: 0.1 M NaHCO<sub>3</sub> + 0.1 M NaCl and 0.1 M NaHCO<sub>3</sub> + 0.05 M MgCl<sub>2</sub> solutions, and the results have been illustrated in Fig. 7(A) and (B) for ZIF-67 NS and ZIF-67 NP, respectively.

As LSVs show, both ZIF-67 morphologies demonstrate noticeable electrocatalytic activity for CO<sub>2</sub> reduction because they exhibit higher reduction currents in the presence of CO<sub>2</sub> in the absence and the presence of Mg<sup>2+</sup> ions. In comparison with the last part of this work, an interesting point here is that at a current density of 5 mA cm<sup>-2</sup> in the presence of CO<sub>2</sub>, the overpotential is against the previous part of this work. The reason could be the specific adsorption of chloride ions [86]. In fact, it has been reported that halides enhance the CO<sub>2</sub> reduction reaction toward C–C coupling and producing C<sub>2</sub>-products such as ethylene and ethanol because, in the presence of such anions, concentrations of adsorbed CO and maybe other CO<sub>2</sub>-reduction intermediates increase [87,88], which is verified by the high current reduction peak in the presence of CO<sub>2</sub> observed in potential ranges between –0.1 and –0.4 V vs. RHE in LSVs of Fig. 7(A) and (B). Also, as the LSVs depict, the existence of Mg<sup>2+</sup> ions facilitates the reduction of CO<sub>2</sub> in the whole potential range, and a shift in LSVs toward less negative potentials is observed. CO<sub>2</sub> adsorption on the surface of electrocatalysts, in our case, cobalt nodes, is an essential step in the CO<sub>2</sub> reduction mechanism [89,90]. Because of its important role in reducing efficiency, this step is considered a descriptor for CO<sub>2</sub> reduction. By adsorption of CO<sub>2</sub> on the surface and formation of chemisorption bond, the hybrid of central carbon changes from sp to sp<sup>2</sup>. It means the bond angle should be reduced to angles smaller than 180°, which is too hard. It has been reported that Mg<sup>2+</sup> ions can form a complex with adsorbed CO<sub>2</sub>, in which the interaction between Mg<sup>2+</sup> ions and oxygen atoms of CO<sub>2</sub> makes this bond bending more facile [35–37]. We suggest the same mechanism here works for the effects of Mg<sup>2+</sup> ions in the solution for the adsorbed CO<sub>2</sub> molecules on the adsorbed cobalt nodes.

Finally, it should be noted that the effects of Mg<sup>2+</sup> ion complex formation with adsorbed CO<sub>2</sub> molecules to facilitate CO<sub>2</sub> reduction for ZIF-67 NS are more observable than those for ZIF-67 NP, similar to the previous part of this work. Again, it could be related to the greater contribution of under-coordinated cobalt nodes and the facile traveling of CO<sub>2</sub> and Mg<sup>2+</sup> ions into the layered structured ZIF-67 NS compared to ZIF-67 NP.

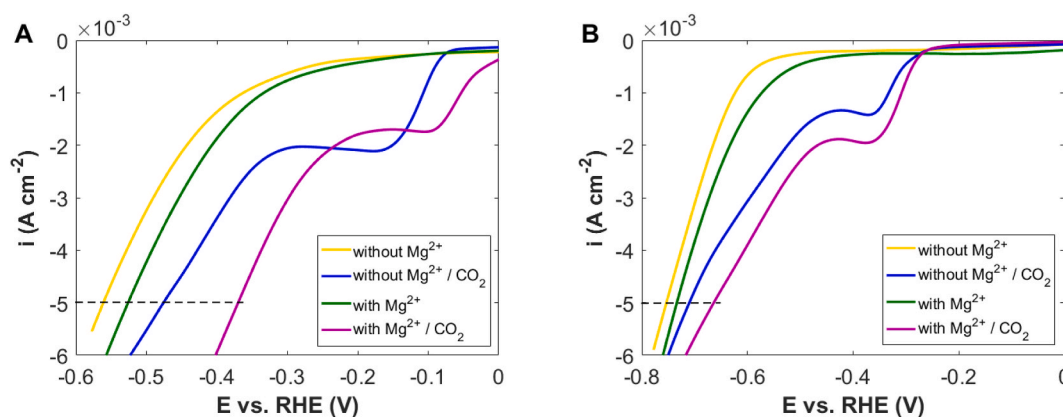
#### 4. Conclusions

In summary, ZIF-67 nanoparticles and ZIF-67 nanosheets were successfully constructed by co-precipitation and one-pot hydrothermal method, respectively. The crystallinities, morphologies, and surface areas of the synthesized samples were confirmed by XRD, FE-SEM, and BET, respectively, and investigated toward CO<sub>2</sub> reduction as electrocatalysts. The ZIF-67 nanosheet exhibits better electrocatalytic activity compared to the ZIF-67 nanoparticle for CO<sub>2</sub> reduction. Such behavior was related to the significant contribution of under-coordinated cobalt nodes in the ZIF-67 nanosheet. Also, the existence of Mg<sup>2+</sup> ions as Lewis acid cations promoted the CO<sub>2</sub> reduction reaction, suggesting the formation of the ZIF-67-CO<sub>2</sub>-Mg<sup>2+</sup> complex.

#### CRedit authorship contribution statement

**Neda Sadat Barekati:** Writing – original draft, Resources, Formal analysis, Data curation. **Hossein Farsi:** Writing – review & editing, Supervision, Conceptualization. **Alireza Farrokhi:** Methodology. **Shokufeh Moghiminia:** Validation, Methodology, Conceptualization.





**Fig. 7.** LSVs for (A) ZIF-67 NS and (B) ZIF-67 NP in the 0.1 M NaHCO<sub>3</sub> + 0.1 M NaCl electrolyte and 0.1 M NaHCO<sub>3</sub> + 0.05 M MgCl<sub>2</sub> electrolyte with and without CO<sub>2</sub> bubbling.

### Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

### Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.heliyon.2024.e26281>.

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