Supporting Information

The Role of Oxygen-Vacancy in Bifunctional Indium Oxyhydroxide Catalysts for Electrochemical Coupling of Biomass Valorization with CO₂ Conversion

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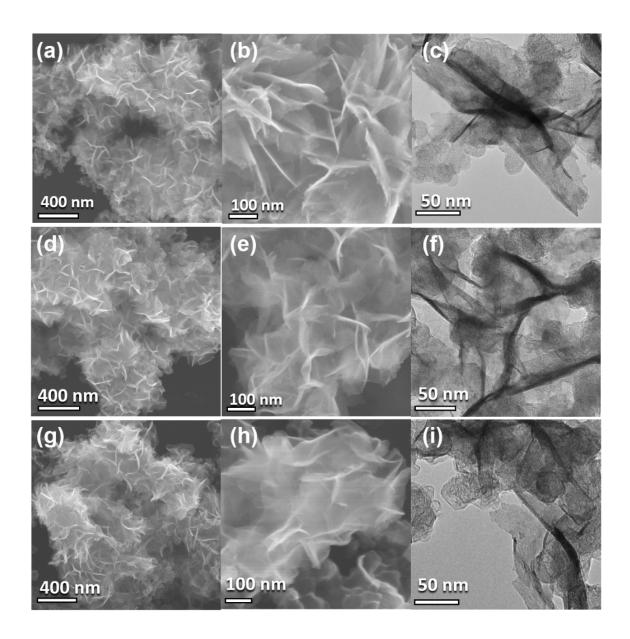
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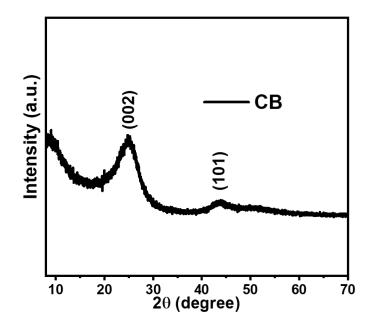
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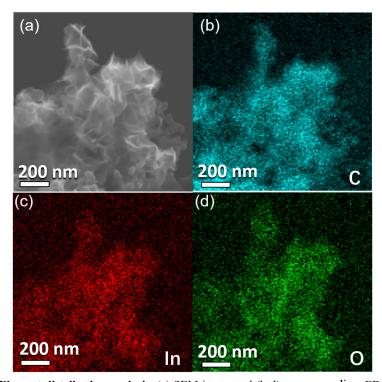
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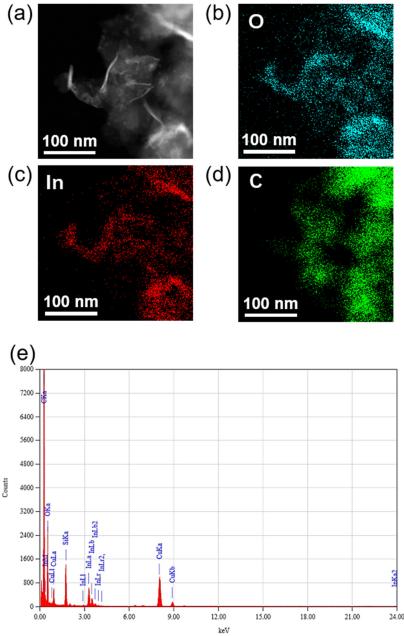
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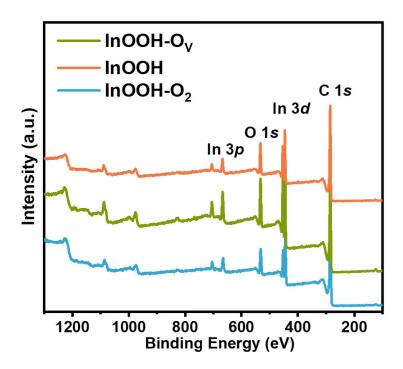
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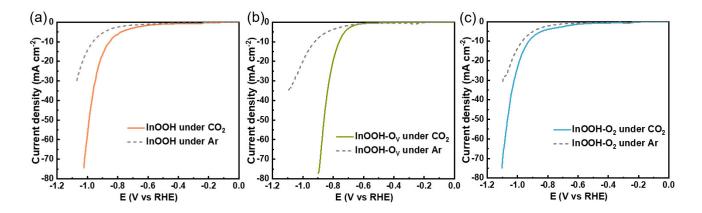
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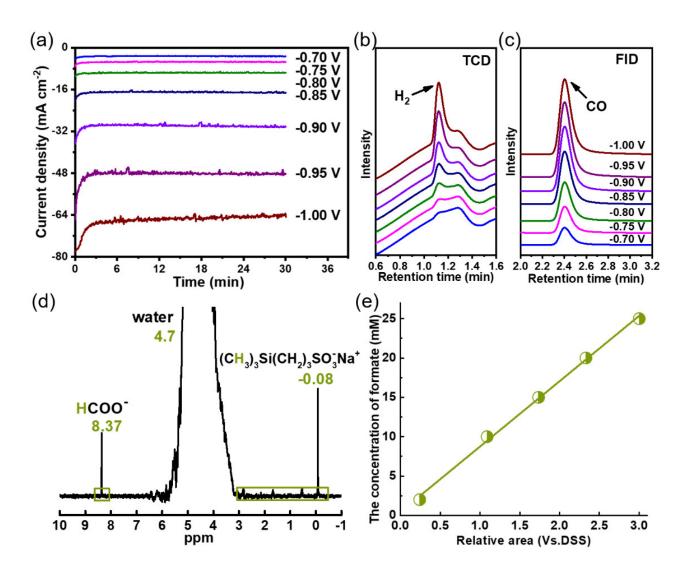
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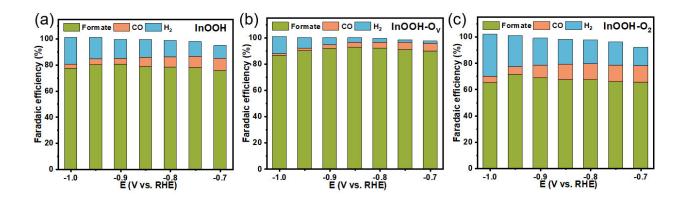


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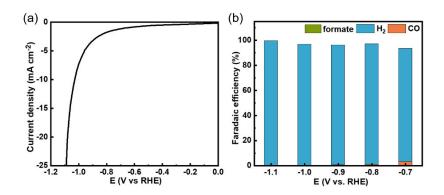


Supplementary Figure 7. The product analysis for CO₂RR. (a) The typical potentiostatic *i-t* curves over InOOH-Ov for CO₂RR. (b-c) The profiles of online GC tests showing H₂ and CO signals. (d) ¹H-NMR spectra for formate determination; (e) Linear relationship between the formate concentration and relative area *vs.* DSS.

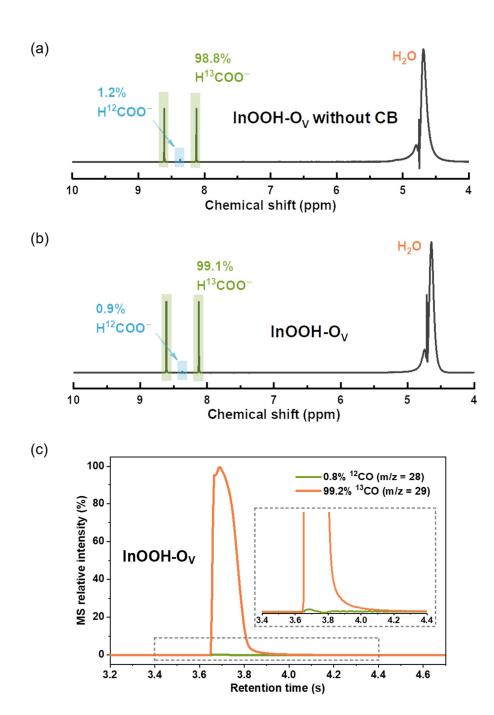
To prepare the liquid sample for ¹H-NMR test, 0.5 mL electrolyte after electrolysis was extracted out to add in a solution containing 0.1 mL D₂O and 0.1 mL 6 mM DSS (1-Propanesulfonic acid 3-(trimethylsilyl) sodium salt). The calibration curve was achieved by testing sodium formate (HCOONa·2H₂O) solution in different concentration from 2 mM to 25 mM. Then the formate concentration over relative area ratio of the formate peak to the DSS peak was plotted.



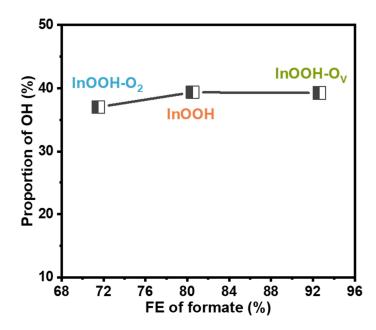
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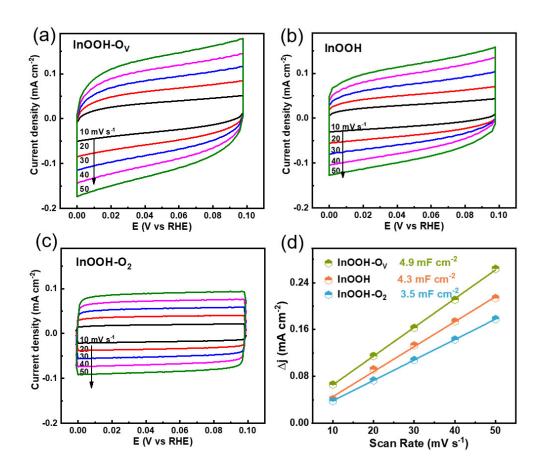
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Supplementary Figure 10. The ¹³CO₂ isotope labling experiments. ¹H-NMR spectrum of produced H¹³COO⁻ and H¹²COO⁻ on InOOH-Ov electrodes (a) without CB and (b) with CB as support at -0.85 V using ¹³CO₂ as the feeding gas. The overwhelming superiority in proportion of doublet of H¹³COO⁻ over the single peak of H¹²COO⁻ confirms the source of the obtained formate is ¹³CO₂ gas, ¹ and the similar results for InOOH-O_V electrodes with/without CB further exclude the probability of potential carbon contamination from CB. Note that the proportion of ¹³CO₂ we used for the isotope labeling experiment is primarily 99%, this is the reason why the tiny part of ¹²C can be still detected in the products. (c) MS spectra of the CO product generated by InOOH-O_V electrode with CB at -0.85 V using ¹³CO₂ as the feeding gas, showing the majority proportion of ¹³CO (99.2%) and a negligible amount of ¹²CO (0.8%), confirming the CO product is derived from the CO₂ reduction.

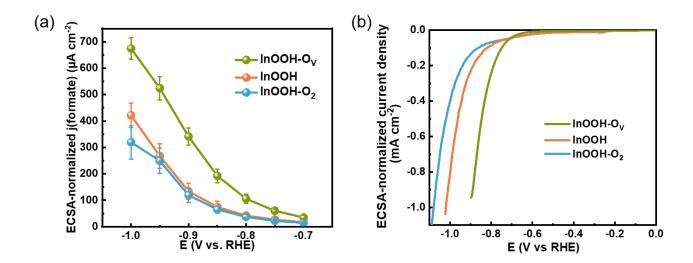


Supplementary Figure 11. The relationship of FE of formate and the propotion of OH species. No correlationship can be observed between the two factors.



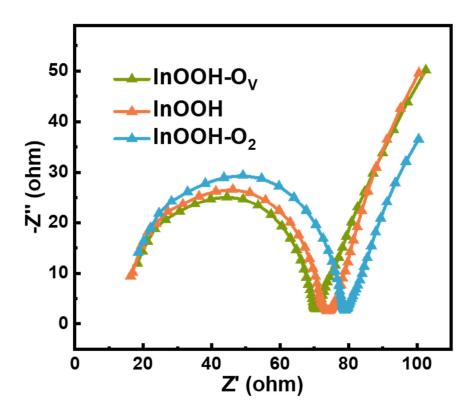
Supplementary Figure 12. ECSA measurements. (a-c) Cyclic voltammetry (CV) curves in the Non-faradaic regions for three samples of InOOH, InOOH-O₂, (d) The linear relation of Δj and scan rates for ECSA tests.

Electrochemical specific surface area (ECSA) was determined by CV method within the non-faradaic potential region between 0 and 0.1 V, as shown in Supplementary Figure 11. Specifically, ECSA was calculate from the formula of ECSA = $R_fS = (C_{dl}/60)S$, where R_f denotes the roughness factor of the working electrode, S represents the geometric surface area of the gas diffusion electrode, and C_{dl} is the double-layer capacitance. For the samples in this work, the values of C_{dl} were obtained by plotting the differences of current density between the anode and cathode (Δj) at 0.05 V against the scan rates, equaling to the half of the linear slopes.

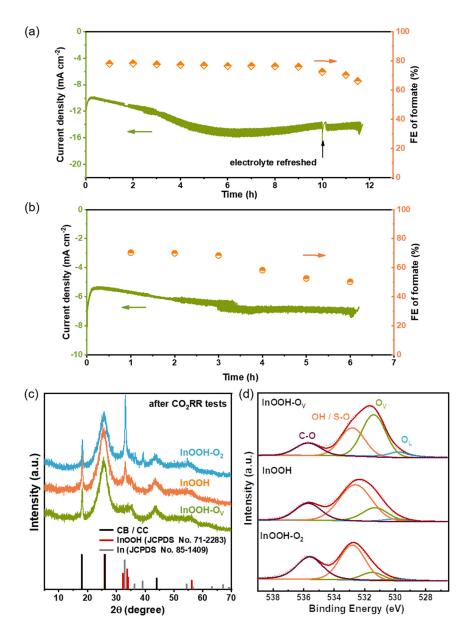


Supplementary Figure 13. Analysis of the effect of ECSA on CO₂RR performance. The ECSA normalized (a) j_{formate} and (b) LSV curves. The error bars represent the standard deviations for three independent tests under the same conditions.

The total electrolysis current densities (i.e., LSV curves) and $j_{formate}$ of the three samples were normalized based on the ECSA from Supplementary Figure 12.

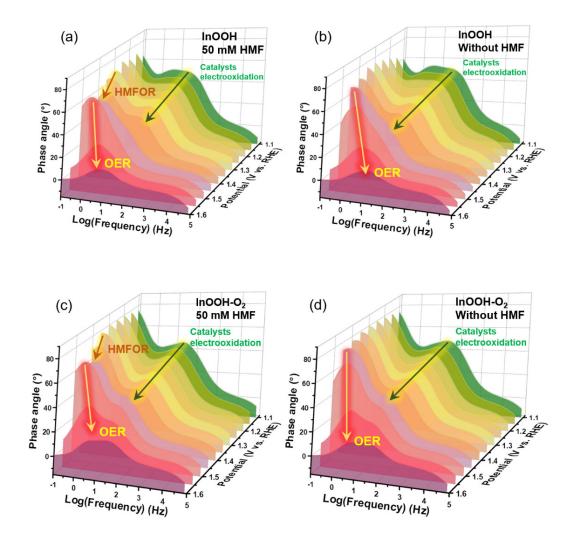


Supplementary Figure 14. EIS tests. The charge transfer impedance decreased from InOOH-O2 through InOOH to InOOH-Ov.

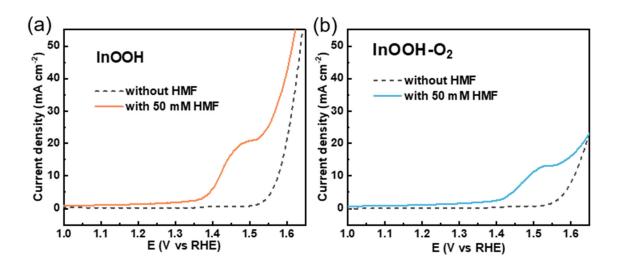


Supplementary Figure 15. The stability tests and physical charactrization of the samples before and after test for CO₂RR. The stability tests of (a) InOOH and (b) InOOH-O₂ for CO₂RR at -0.85 V. (c) XRD patterns and (d) O 1s XPS spectra of three electrodes after CO₂RR tests.

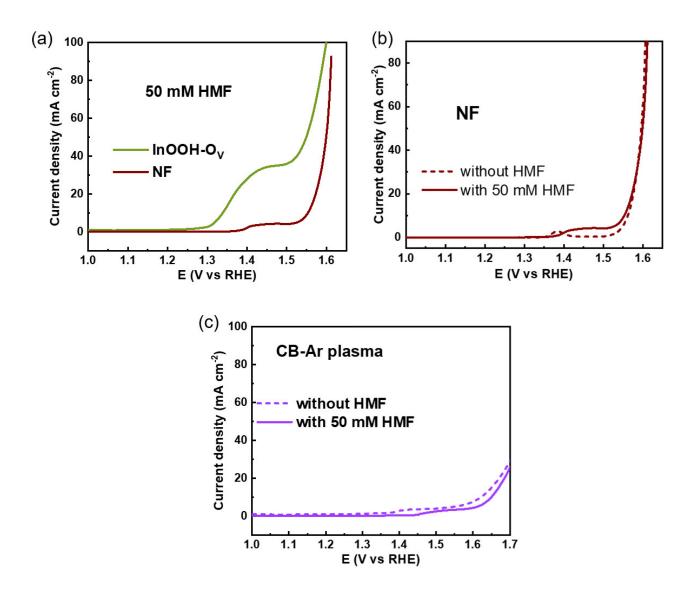
Note: The XRD patterns of electrodes after test show the signal of carbon cloth (CC). The deconvoled O 1s peak at binding energy of 532.8 eV represents an overlap of -OH and the sulfonic acid groups (labeled as S-O) in Nafion ionomer, and peak at binding energy of 535.7 eV is attributable to ether oxygen in Nafion ionomer (labeled as C-O).³



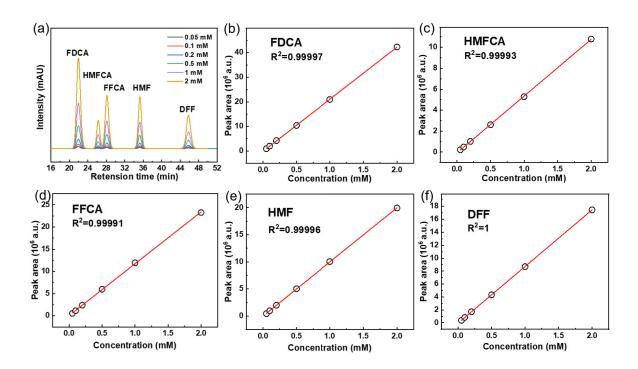
Supplementary Figure 16. The in situ EIS tests. Bode phase plots for EIS tests of (a-b) InOOH and (c-d) InOOH-O₂. The disappeared peaks for HMFOR were both observed for InOOH and InOOH-O₂ without adding 10 mM HMF. However, their HMFOR peaks were not as distinct as those of InOOH-O_V in Figure 4b of manuscript, depicting the weakened HMFOR activities due to the low content of O_V.



Supplementary Figure 17. The comparison of LSV curves with and without HMF. (a) InOOH, (b) InOOH-O₂ catalysts.

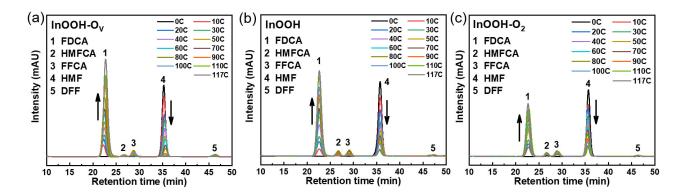


Supplementary Figure 18. The confirmation of HMFOR perofrmance for InOOH-Ov. (a) The comparison of LSV curves for HFMOR between InOOH-O_V and NF. LSV curves for (b) bare NF and (c) Ar-plasma treated CB on NF substrate with and without the addition of HMF.

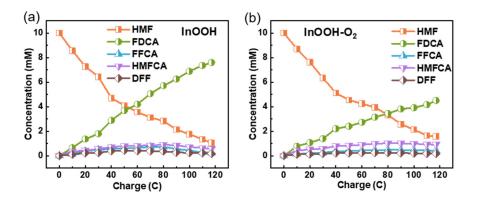


Supplementary Figure 19. The calibration curves of HMFOR products for HPLC tests. (a) The retention time curves. The linear fitting curves for (b) FDCA, (c) HMFCA, (d) FFCA, (e) HMF and (f) DFF.

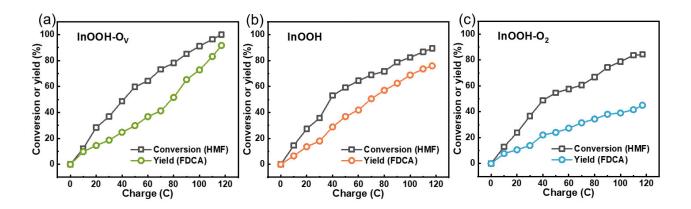
Supplementary Figure 20. Reaction pathways illustration for HMFOR processes. The two reaction pathways involves asynchronous oxidation steps of hydroxyl and aldehyde groups oxidation.



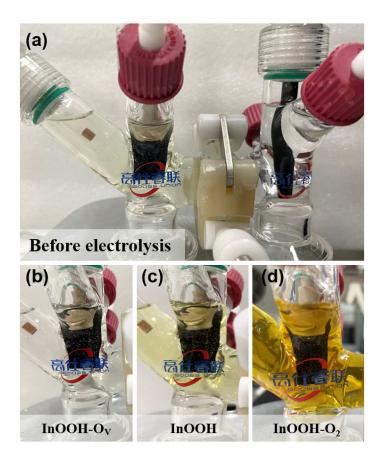
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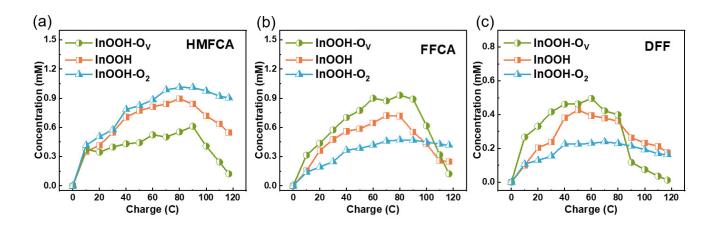
 $\textbf{Supplementary Figure 22. The concentration variation of HMFOR products.} \ (a) \ In OOH \ and \ (b) \ In OOH-O_2 \ catalysts.$



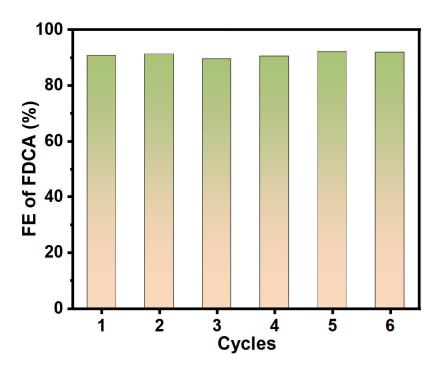
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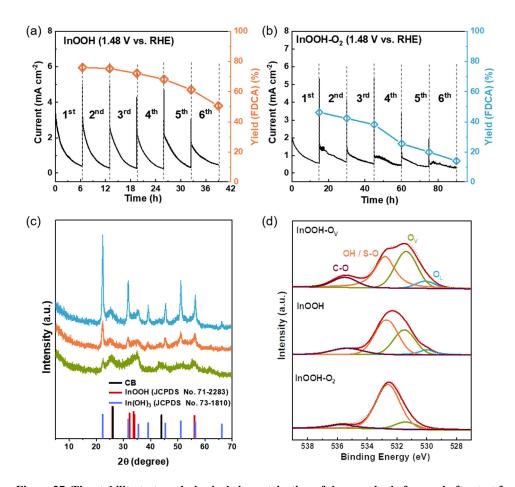
Supplementary Figure 24. The changing colors of anodic electrolyte before and after HMFOR tests for different samples of InOOH, InOOH-O_V, and InOOH-O₂. (a) The freshly prepared HMF solution (10 mM) appears the color of light-yellow. (b) HMF was oxidized efficiently and timely over InOOH-O_V, resulting in colorless electrolyte after electrolysis. (c,d) The sequentially weakened catalytic activities of HMFOR over InOOH and InOOH-O₂ lead to deeper and deeper electrolyte colors with electrolysis, as the strongly basic environment can cause HMF degradation through furan ring opening up and cross-polymerization to form brown, undesirable humins when HMF can not be consumed in time.⁴



Supplementary Figure 25. Comparision of the concentration variations among samples of InOOH, InOOH-O₂, and InOOH-O₂. (a) HMFCA, (b) FFCA, and (c) DFF.

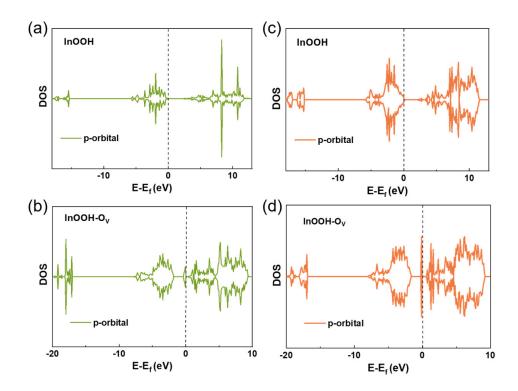


Supplementary Figure 26. Stability test. The FE of FDCA for six sequential electrolysis batches of HMFOR on InOOH-O_V at 1.48 V.

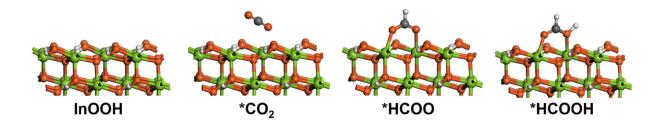


Supplementary Figure 27. The stability tests and physical charactrization of the samples before and after test for HMFOR. The stability tests of (a) InOOH and (b) InOOH-O₂ for HMFOR at 1.48 V. (c) The XRD patterns and (d) O 1s XPS spectra of three electrodes after HMFOR tests.

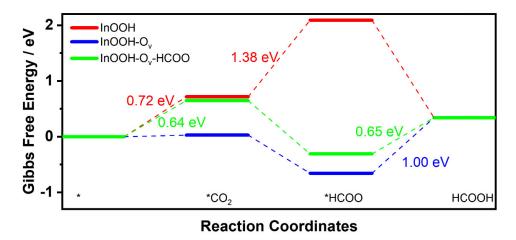
Note: The samples were removed from NF substrate by ultrasonic treatment and re-collected for characterization. The deconvoled O 1s peak at binding energy of 532.8 eV represents an overlap of -OH and the sulfonic acid groups (labeled as S-O) in Nafion ionomer, and peak at binding energy of 535.7 eV attributes to ether oxygen in Nafion ionomer (labeled as C-O).³



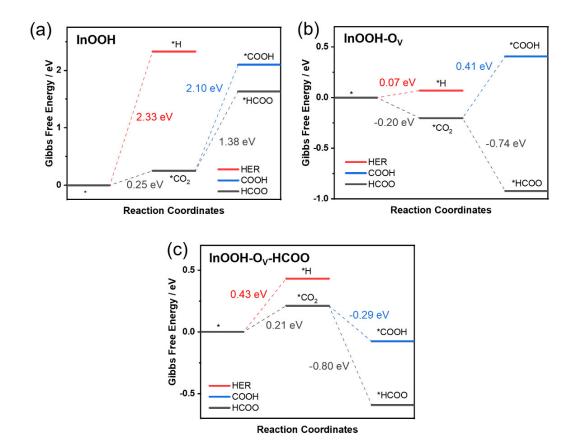
Supplementary Figure 28. The PDOS of the p-orbital on In atoms. The PBE-determined partial DOS of the p-orbital for In atom (a) on intact InOOH (110) plane and (b) adjcent to O_V site on InOOH-O_V. The HSE06-determined partial DOS of the p-orbital for In atom (c) on intact InOOH (110) plane and (d) adjcent to O_V site on InOOH-O_V.



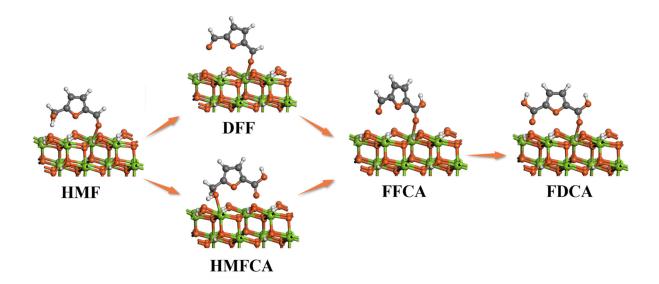
Supplementary Figure 29. Configurations of intermediates. The simulated results on models of InOOH (110) during CO₂RR.



Supplementary Figure 30. Free energy diagrams for CO₂RR. RPBE was used to explore the functional sensitivity.



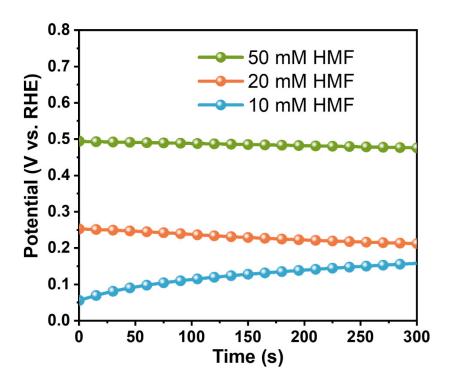
Supplementary Figure 31. Free energy diagrams for HER and CO₂RR. (a) InOOH, (b) InOOH-O_V, and (c) InOOH-O_V-HCOO.



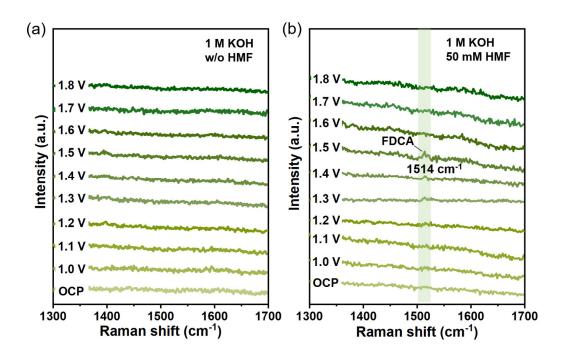
Supplementary Figure 32. Configurations of intermediates. The simulated results on models of InOOH (110) during HMFOR.



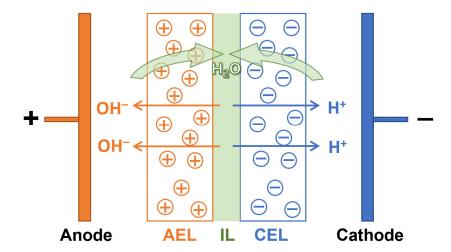
Supplementary Figure 33. Operando Raman spectra acquisition. The H-shape electrolysis cell with an optical quartz window was used.



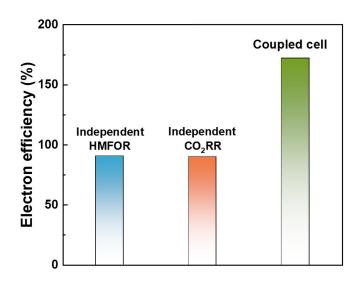
Supplementary Figure 34. The OCP measurements for InOOH-Ov. Different HMF concentrations of 10, 20, and 50 mM in 1 M KOH were used under in situ Raman spectroscopy acquisition condition. The bigger OCP for the higher HMF concentration indicated the more occupied Ov sites by HMF molecules.



Supplementary Figure 35. The in situ Raman spectroscopies. The potential-dependent in situ Raman spectroscopies obtained in the range of 1300 and 1700 cm^{-1} over InOOH-O_V in (a) 1 M KOH without adding HMF and (b) with 50 mM HMF.



Supplementary Figure 36. The illustration of BPM structure. A typical BPM consists of laminated films of anion-exchange layer (AEL) and cation-exchange layer (CEL) with a bipolar interfacial layer (IL) formed between that allows selective diffusion of protons and hydroxide anions towards the negative and positive electrode, respectively.⁵



Supplementary Figure 37. The electron efficiency comparison of independent HMFOR, CO₂RR, and coupled cell. "Combined electron efficiency" represents the overall utilization efficiency of electrons that are transferred between cathode and anode to produce target value-added chemicals (formate and FDCA) in terms of the whole electrolysis system. The higher the "combined electron efficiency", the higher the utilization of electricity.

Table S1. The atomic contents of different elements in the three samples

Sample	C (at. %)	O (at. %)	In (at. %)	Mass fraction of InOOH
InOOH	84.8	12.0	3.3	32.1 %
InOOH-Ov	86.1	10.7	3.3	31.9 %
InOOH-O2	82.7	13.7	3.6	34.8 %

Table S2. The area fraction of deconvolved O 1s peaks of InOOH, InOOH-O $_{\rm V}$, and InOOH-O $_{\rm 2}$

Sample	O_L	Ov	ОН	
InOOH	28.0%	32.6%	39.4%	
$In OOH\text{-}O_{V}$	19.9%	40.9%	39.3%	
InOOH-O2	34.0%	29.0%	37.0%	

Table S3. Recent works using metal oxides as catalysts for CO₂RR to formate testing in H-shape cell at ambient condition

Catalysts	Electrolyte	Potential	FE _{max} (%)	j(formate) (mA cm ⁻²)	Ref.
CoO _x	0.1 M Na ₂ SO ₄	-0.25 V vs.RHE	90	9	6
SW-Cu ₂ O/Cu	0.5 M KHCO ₃	-0.84 V vs RHE	27.1	-	7
PVP@Cu2O	0.1 M K ₂ SO ₄	-0.65 V vs RHE	77.6	-	8
In ₂ O ₃ -rGO	0.1 M KHCO ₃	-1.20 V vs.RHE	84.6	22	9
SnO ₂ /Graphene	0.1 M NaHCO ₃	-1.8 V vs.SCE	93.6	10.2	10
SnO ₂ QWs	0.1 M KHCO ₃	-1.16 V vs.RHE	87.3	13.7	11
SnO ₂ nanosheets	0.5 M NaHCO ₃	-1.6 V vs.SCE	87	45	12
V _o -SnO ₂	0.5 M NaHCO ₃	-0.7 V vs.RHE	92.4	~2.5	13
Co ₃ O ₄ layers	0.1 M KHCO ₃	-0.87 V vs.SCE	87.6	2.7	2
InO _x nanoribbons	0.5 M NaHCO ₃	-0.7 V vs.RHE	91.7	5	14
SnO ₂ nanowires	0.1 M KHCO ₃	-0.8 V vs.RHE	80.1	4.8	15
Vo-rich N-SnO ₂	0.1 M KHCO ₃	-0.9 V vs.RHE	83	6.7	16
InOOH-Ov	0.1 M KHCO ₃	-0.85 V vs.RHE	92.6	16.0	This work
InOOH-Ov	0.1 M KHCO ₃	-0.95 V vs.RHE	90.0	43.7	This work
InOOH-Ov	0.1 M KHCO ₃	-1.00 V vs.RHE	86.4	56.2	This work

Table S4. Recent works on catalysts for HMFOR to FDCA

Catalysts	Onset potential (V vs. RHE)	HMF conversion (%)		
InOOH-Ov	1.30	98.5	91.6	This work
Ni ₂ P NPA/NF	1.35	100	98	17
Ni ₃ S ₂ /NF	1.35	100	98	18
hp-Ni	1.35	100	98	19
NiFe LDH	1.25	98	98	20
Ni _x B/NF	1.38	100	98.5	21
NiCo ₂ O ₄ /NF	1.35	100	90	22
CuNi(OH) ₂ /C	1.38	98.8	93.3	23
NiOOH/FTO	NA	99.8	96	24
CoOOH/FTO	NA	95.5	35.1	24
FeOOH/FTO	NA	16	1.59	24
VN/NiF	1.36	98	96	25
NiSe@NiOx	1.35	100	99	26
MoO ₂ -FeP@C	~1.35	99.4	98	27
Ni ₃ N@C	1.35	100	98	28
NiCoFe-LDHs	~1.50	~84.9	~90	29
CoO-CoSe ₂	1.30	100	99	30
Vo-Co3O4	~1.30	NA	91.9	31
P-HEOs	~1.30	99	97.4	32

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