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Research Article

Steering the Methane Dry Reforming Reactivity of Ni/La₂O₃ Catalysts by Controlled In Situ Decomposition of Doped La₂NiO₄ Precursor Structures

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ABSTRACT: The influence of A- and/or B-site doping of Ruddlesden–Popper perovskite materials on the crystal structure, stability, and dry reforming of methane (DRM) reactivity of specific A_2BO_4 phases (A = La, Ba; B = Cu, Ni) has been evaluated by a combination of catalytic experiments, in situ X-ray diffraction, X-ray absorption spectroscopy (XAS), X-ray photoelectron spectroscopy (XPS), and aberration-corrected electron microscopy. At room temperature, B-site doping of La_2NiO_4 with Cu stabilizes the orthorhombic structure (*Fmmm*) of the perovskite, while A-site doping with Ba yields a tetragonal space group (*I*4/*mmm*). We observed the orthorhombic-to-tetragonal transformation above 170 °C for $La_2Ni_{0.9}Cu_{0.1}O_4$ and $La_2Ni_{0.8}Cu_{0.2}O_4$, slightly higher than for undoped La_2NiO_4 . Loss of oxygen in interstitial sites of the tetragonal structure causes further structure transformations for all samples before decomposition in the temperature range of 400 °C-600 °C. Controlled in situ decomposition of the parent or A/B-site doped perovskite structures in a DRM mixture (CH₄:CO₂ = 1:1) in all cases yields an active phase consisting of exsolved nanocrystalline metallic Ni particles in



contact with hexagonal La_2O_3 and a mixture of (oxy)carbonate phases (hexagonal and monoclinic $La_2O_2CO_3$, BaCO_3). Differences in the catalytic activity evolve because of (i) the in situ formation of Ni–Cu alloy phases (in a composition of >7:1 = Ni:Cu) for $La_2Ni_{0.9}Cu_{0.1}O_4$, $La_2Ni_{0.8}Cu_{0.2}O_4$, and $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$, (ii) the resulting Ni particle size and amount of exsolved Ni, and (iii) the inherently different reactivity of the present (oxy)carbonate species. Based on the onset temperature of catalytic DRM activity, the latter decreases in the order of $La_2Ni_{0.9}Cu_{0.1}O_4 \sim La_2Ni_{0.8}Cu_{0.2}O_4 \ge La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4 > La_2NiO_4 > La_{1.8}Ba_{0.2}NiO_4$. Simple A-site doped $La_{1.8}Ba_{0.2}NiO_4$ is essentially DRM inactive. The Ni particle size can be efficiently influenced by introducing Ba into the A site of the respective Ruddlesden–Popper structures, allowing us to control the Ni particle size between 10 nm and 30 nm both for simple B-site and A-site doped structures. Hence, it is possible to steer both the extent of the metal-oxide-(oxy)carbonate interface and its chemical composition and reactivity. Counteracting the limitation of the larger Ni particle size, the activity can, however, be improved by additional Cu-doping on the B-site, enhancing the carbon reactivity. Exemplified for the La_2NiO_4 based systems, we show how the delicate antagonistic balance of doping with Cu (rendering the La_2NiO_4 structure less stable and suppressing coking by efficiently removing surface carbon) and Ba (rendering the La_2NiO_4 structure more stable and forming unreactive surface or interfacial carbonates) can be used to tailor prospective DRM-active catalysts.

KEYWORDS: in situ decomposition, perovskite, Ruddlesden-Popper phase, in situ X-ray diffraction, copper, phase transformation

1. INTRODUCTION

The anthropogenically induced climate change and the greenhouse effect the most important challenges mankind faces nowadays, releasing billions of tons of carbon dioxide and methane annually.¹ To potentially reduce such emissions, dry reforming of methane (DRM), that is, the simultaneous utilization of both CO_2 and CH_4 , is a particularly rewarding pathway to convert two harmful climate gases at the same time to H_2 and $CO.^{2-20}$ This so-called "syngas" mixture can subsequently be used for the synthesis of other useful fuels or chemicals, for example, via the Fischer–Tropsch reaction or for methanol production.²¹ Typically used catalysts involve

noble metals, Ni or Ni alloys.^{1,6,7,9–12,16,22–25} Recently, activated carbon has also been investigated.²⁶ Apart from the inherent economical issues concerning the use of noble metals, one particular challenge is connected to the deactivation and long-term stability of especially Ni-containing catalysts by coke

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Figure 1. Panels A and B: Ex situ collected PXRD patterns of the initial doped La_2NiO_4 Ruddlesden–Popper materials. The lower panel indicates the phase assignment to the respective reference structures. Panels B focus on a narrower 2 θ window for closer analysis. Panels C and D: Similar analysis of the five spent doped La_2NiO_4 Ruddlesden–Popper materials after a catalytic DRM (CO₂:CH₄:He = 1:1:3) runs in a total gas flow of 100 mL min⁻¹ up to 800 °C for a total time of 2 h.

formation.²⁷ In the search for alternative catalyst materials, a new class of prospective compounds based on perovskite and perovskite-related structures has evolved.^{18,19,22,23,28,29} Perovskites, with the general formula ABO₃ (A usually being a lanthanide, alkaline, or earth alkaline metal ion with a valency of 2 or 3; B being a transition metal ion with a valency of 3 or 4), are often used as catalyst precursor materials that are converted into the active phase by a reductive treatment in hydrogen, triggering the partial or complete decomposition of the parent perovskite structure and the formation, of a metal-oxide-system, or in-case of in situ DRM activation, of an oxide-(oxy)carbonate system, consisting of small nm-sized metal particles attached to the oxide- or (oxy)carbonate matrix.^{18,19,22,28} One particularly rewarding perovskite entity is the archetypical system LaNiO₃, which has already shown very promising coking properties.

Specifically, the active phase resulting from LaNiO₃ has been reported to be formed via reductive decomposition and the creation of highly dispersed Ni particles in contact with and hexagonal La₂O₃ and/or distinct oxycarbonate phases^{18,22} In a nutshell, the current understanding of catalytic DRM operation is a bifunctional synergistic action of both metal (mostly Ni, ^{18,22,30,31} but e.g., also Pd^{32}) for methane activation and oxide (e.g., La_2O_3 in case of perovskite precursors) for CO_2 activation. It is currently controversially discussed whether spillover effects or special interfacial sites represent the active phase. The common structural denominator of all prospective catalyst materials, encompassing not only perovskite-related structures but also (oxy)carbides or alloy/intermetallic compounds is the presence of a selected precursor structure, which via in situ decomposition in the DRM mixture yields the active metal/oxide material. The latter can be present as Ni/ $La_2O_3/La_2O_2CO_3$ (in the case of $LaNiO_3$ -based perovskites^{18,22,30,31}), Ni/Mo_2C(WC) (in case of carbide materials³³) or Pd/ZrO₂ (in case of Pd–Zr alloys/intermetallic compound precursors³²).

Readdressing the particular importance of perovskites, intermediate perovskite-related structures found during this activation process, such as the Ruddlesden–Popper phase La_2NiO_4 , also exhibit similar beneficial properties.^{19,25} The common reactivity-steering denominator of all systems is the possibility to influence the structural breakdown of the perovskites by deliberate A- and B-site doping. In general, it is assumed that B-site doping has a greater effect, as it allows

sample	parameters	Fmmm	I4/mmm
La ₂ NiO ₄	a (Å)	5.4579(2)	3.86119(4)
	b (Å)	5.4631(2)	3.86119(4)
	c (Å)	12.6874(2)	12.6876(2)
	V (Å ³)	378.30(2)	189.16(1)
	orthorhombicity $\delta \times 10^{-4}$	4.8	0
	$R_{ m wp}$	3.9	4.8
	$R_{\rm p}$	2.9	3.5
	$R_{ m B}$	3.1	3.9
$La_2Ni_{0.9}Cu_{0.1}O_4$	a (Å)	5.4555(3)	3.85987(5)
	b (Å)	5.4619(3)	3.85987(5)
	c (Å)	12.7339(3)	12.7339(3)
	$V(Å^3)$	379.44(3)	189.72(1)
	orthorhombicity $\delta \times 10^{-4}$	5.9	0
	$R_{\rm wp}$	2.4	2.8
	R _p	2.0	2.2
	$R_{\rm B}$	1.7	2.1
$La_2Ni_{0.8}Cu_{0.2}O_4$	a (Å)	5.4463(2)	3.8535(1)
	b (Å)	5.4531(2)	3.8535(1)
	c (Å)	12.7768(4)	12.7768(3)
	$V(Å^3)$	379.45(3)	189.73(1)
	orthorhombicity $\delta \times 10^{-4}$	6.2	0
	R _{wp}	2.7	3.1
	R _p	2.1	2.3
	R _B	2.1	2.3
La _{1.8} Ba _{0.2} NiO ₄	a (Å)	5.4495(7)	3.8540(2)
	b (Å)	5.4509(7)	3.8540(2)
	c (Å)	12.7977(5)	12.7976(6)
	V (Å ³)	380.15(7)	190.09(2)
	orthorhombicity $\delta \times 10^{-4}$	1.3	0
	R _{wp}	3.9	3.4
	R _p	2.4	2.3
	R _B	3.2	3.0
$La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$	a (Å)	5.4423(5)	3.84885(8)
	b (Å)	5.4438(5)	3.84885(8)
	c (Å)	12.8398(3)	12.8397(2)
	$V(Å^3)$	380.40(5)	190.203(7)
	orthorhombicity $\delta \times 10^{-4}$	1.4	0
	, R _{wp}	4.2	3.8
	R_n	2.9	2.7
	$R_{\rm B}$	3.2	2.9
	D	-	

Table 1. Summary of Structural Parameters Extracted from Powder XRD Patterns by Rietveld Refinement for All Initial Samples Using the Orthorhombic *Fmmm* and tetragonal *I4/mmm* Space Groups

the reduction of the B-site cation to usually highly dispersed exsolved B metal particles.³⁰ This has been especially also highlighted for LaNiO₃ and La₂NiO₄.^{18,19,23-25}

One inherent problem in the characterization of the active phase of these perovskite materials in DRM catalysis refers to the usual two-step mechanism in its formation: a prereduction step in hydrogen is usually carried out before the DRM run is performed over the reduced (i.e., metal-oxide) system.^{18,22} This problem is overcome by recent recognition that decomposition/activation can also be achieved operando by annealing directly in the DRM mixture–leading to different size distributions of the exsolved metal particles and, thus, different extents of interfaces and reactivity patterns.^{19,31} Nevertheless, despite the benefits of direct decomposition, in situ and operando characterization of the active state is clearly underrepresented in the literature. For La-based perovskites, this is a particular pity, as during DRM, the CO₂-activated species apparently is La₂O₂CO₃, reversibly formed as a function of the gas atmosphere and partial pressure by the reaction of La_2O_3 with CO_2 and decomposed by the reaction of $La_2O_2CO_3$ with deposited carbon to La_2O_3 and CO, respectively.³⁴

To reveal the influence of doping on the reactivity of selected Ruddlesden–Popper perovskite systems and to assess general principles in reactivity steering, we deliberately synthesized A- and B-site doped La_2NiO_4 structures by an autoignition method and subjected them to catalytic reactivity measurements in the DRM reaction. As an A-side dopant, Ba was selected to potentially control the surface basicity of the perovskite entity and to eventually steer the reactivity of the interfacial (oxy)carbonate species, which are presumed to be most crucial for self-regeneration.³⁵ To potentially enhance the coking resistance, Cu (in various compositions) was added as B-side dopant. As the most complex entity, simultaneous A-and B-side doped La_2NiO_4 was prepared. Hence, four doped La_2NiO_4 samples (apart from pure La_2NiO_4) were analyzed:

La_{1.8}Ba_{0.2}NiO₄, La₂Ni_{0.9}Cu_{0.1}O₄, La₂Ni_{0.8}Cu_{0.2}O₄, and $La_{18}Ba_{02}Ni_{09}Cu_{01}O_4$. We opted to study the corresponding Ruddlesden-Popper phases in favor of LaNiO₃ because the latter, especially in doped samples, is structurally unstable toward La₂NiO₄ upon synthesis and subsequent annealing.^{25,36,37} To directly establish reactivity-structure relationships, we carried out the decomposition of the respective perovskites in the DRM reaction mixture and also analyzed the corresponding structural changes by synchrotron-based in situ X-ray diffraction. Besides the determination of structural changes of the catalysts, the in situ synchrotron XRD experiments allow us also to follow the chemical expansion^{38,39} of each catalyst, being crucial for its respective catalytic behavior. Bulk and surface structural and elemental changes occurring during decomposition were also monitored by X-ray absorption spectroscopy (XAS), X-ray photoelectron spectroscopy (XPS), aberration-corrected electron microscopy, and energy-dispersive X-ray spectroscopy imaging of selected catalyst states during DRM.

2. EXPERIMENTAL SECTION

2.1. Synthesis of the Materials. All samples were synthesized following a dedicated autoignition method.⁴⁰ As a first step, an aqueous solution using stoichiometric amounts of La(NO₃)₃·6H₂O, Ni(NO₃)₂·6H₂O, Ba(NO₃)₂, and Cu- $(NO_3)_2 \cdot 3H_2O$. Subsequently, glycine was added to the solution in a molar ratio of 1 with respect to NO₃⁻:NH₂⁻ to form glycine-metal complexes and to induce a homogeneous distribution of all ions. All solutions containing Cu²⁺ exhibited a blue color due to the presence of glycinate-copper complexes, whereas all other exhibited a greenish color. Excess water was removed upon heating the solution at 80 °C for 2 h. The resulting viscous liquid was heated to 250 °C, causing selfignition at 1200 °C and the formation of stoichiometric amounts of metal oxides and residual carbon from glycine. Annealing at 900 °C for 12 h forms the Ruddlesden-Popper La_{2-x}Ba_xNi_{1-v}Cu_vO₄ perovskite structures, as evidenced by ex situ XRD (Figure 1 and Table 1).

2.2. Catalytic Measurements in DRM. The performance of the catalysts with respect to DRM activity was tested in a home-built fixed-bed flow tubular quartz reactor (inner diameter = 7 mm, outer diameter = 9 mm, catalyst bed length: 2.5 cm). Catalyst powder (50 mg) was used for each reaction and uniformly distributed over the catalyst bed length using thoroughly degassed quartz wool. Each gas required for DRM ($CH_4:CO_2:He = 1:1:3$ ratio) was injected through a corresponding mass flow controller (MKS). Helium acts both as a carrier gas and as a heat conductor. Heating was performed by using a Linn High Term furnace up to 800 °C at a fixed rate of 10 °C min⁻¹. The heating process was controlled by a S-type Pt/PtRh thermocouple placed in close vicinity to the sample. The output gas was continuously extracted through a capillary and analyzed by a quadrupole mass spectrometer mounted in cross-beam geometry (Balzers QMA 125). We especially emphasize here that because of the bifunctional operating mechanism of DRM catalysts, normalization of the catalytic activity solely to the surface area of the exsolved Ni particles would grossly overestimate the role of Ni and is therefore not considered (i.e., calculating metal surface-based turnover frequencies is not meaningful during in situ activation). Hence, a qualitative picture of the effect of the structure and composition of doped La₂NiO₄ catalyst precursors on the methane dry reforming reactivity is derived

from temperature-programmed DRM experiments, focusing on onset temperatures of catalytic activity, conversion (%), and H_2/CO product ratios. With respect to activity, the relative catalytic behavior is compared on the basis of conversion vs *T* plots.

2.3. Structural, Morphological, and Elemental Characterization. The specific surface area of all samples prior to catalysis was assessed by BET surface quantification via nitrogen adsorption in a QuadraSorb Station 4 apparatus (Quantachrome, U.S.A.). BET surface area was obtained from 5 point measurements recorded at 77 K after degassing the samples in vacuo for 10 h at 200 °C. As shown in Table S1, BET areas of the samples are varied between 2.2 and 4.5 m² g⁻¹.

Ex situ powder X-ray diffraction (PXRD) was carried out using a STOE stadi P powder diffractometer in transmission geometry and Mo K α 1 radiation ($\lambda = 0.7093$ Å). A focusing Ge(111) primary beam monochromator, as well as a linear position sensitive detector system was employed. Corresponding in situ synchtrotron-based PXRD experiments have been conducted in DRM mixtures at beamline 12.2.2, Advanced Light Source (ALS) at Berkeley National Laboratory. The diffraction patterns were measured in angle-dispersive transmission mode with a focused 25 keV monochromatic beam (λ = 0.4984 Å/30 μ m spot size). The powders were heated in a 0.7 mm outer diameter quartz capillary under quasi flowing conditions (CH₄:CO₂:He = 1:1:3). The gases were injected through a 0.5 mm outer diameter tungsten tube. Heating was performed using a SiC furnace with an infrared light source up to 800 °C at a rate of 10 °C min⁻¹. The patterns were recorded by a PerkinElmer flat panel detector (XRD 1621, dark image, and strain correction).^{41,42} Rietveld refinement was performed using the FULLPROF program.⁴³ The profile function 7 (Thompson-Cox-Hastings pseudo-Voigt convoluted with axial divergence asymmetry function)⁴⁴ was used in all refinements. The resolution function of the diffractometers was obtained from the structure refinement of a LaB₆ standard. The weight fraction W_i of the *i*th phase in *n* mixture of crystalline phases is calculated by Rietveld refinement according to⁴

$$W_i = \frac{S_i Z_i M_i V_i / t_i}{\sum_{i}^{n} S_j Z_j M_j V_j / t_j}$$

where S_i is the refined scale factor of the phase, Z_i is the number of formula units per unit cell, M_i is the molecular mass of the formula unit, V_i is the refined unit cell volume, and t_i is the Brindley particle absorption contrast factor.⁴⁶ The sum of the weight fractions is constrained to 100% by assuming that the samples contain negligible amounts of amorphous phases.

Structural and morphological characterization has been further performed by transmission electron microscopy (TEM) using two setups: TEM measurements were done using a FEI Tecnai F20 S-TWIN analytical high-resolution microscope operated at 200 kV and located at the USTEM, Vienna. For EDX experiments, a windowless Apollo XLTW silicon drift detector was employed with the elemental analysis based on the automated Cliff-Lorimer method.⁴⁷ Aberrationcorrected electron microscopy has been performed at the Ernst-Ruska Center for Microscopy and Spectroscopy with Electrons at FZ Jülich. Sample morphology, geometry, and electron diffraction patterns were additionally studied using a Tecnai G2 F20 microscope at 200 kV. Diffraction patterns were obtained with a camera length of 175 mm for all samples. A Gatan UltraScan 1000P (2k × 2k) charge-coupled digital (CCD) camera is used as a detector for TEM bright-field imaging. Additionally, a Gatan Tridiem 863P postcolumn image filter (GIF) is installed for electron energy loss spectroscopy (EELS). All aberration-corrected high-resolution transmission electron microscopy experiments were conducted using FEI Titan 80–300 TEM and STEM microscopes operated at 300 kV. Information limits (TEM) of below 90 pm at 300 kV⁴⁸ and <200 pm (at 300 kV; STEM)⁴⁹ are obtained.

X-ray absorption measurements were carried out with a novel self-developed wavelength-dispersive spectrometer in von Hámos geometry.^{50,51} The spectrometer is equipped with a microfocus X-ray tube, a curved Highly Annealed Pyrolytic Graphite mosaic crystal and a hybrid photon counting CMOS detector with 512 \times 1030 pixel and a pixel size of 75 μ m \times 75 μ m. The tube was operated with a high voltage of 16 kV and a current of 300 μ A. As the Ni reference, a 2 μ m Ni foil was used. All other references and samples were in powder form and prepared as wax-pellets (mixed with Hoechst Wax C), due to its lower concentration of Ni. The blending of the sample and reference sample with Hoechst Wax was necessary to achieve pellets with an adequate thickness for stability. After wax and sample material were stirred in a mortar to get a homogeneous mixture, a pellet with a 13 mm diameter was pressed by using a hydraulic pellet press with force up to 6 tons for not longer than 60 s. Since the samples were measured in transmission mode, the absorption spectrum is acquired by measuring once with and once without the sample. The measurement time for each sample varied from 8 h to 10 h depending on the thickness of the prepared sample. All references and samples were constantly moved during the measurements to minimize the effects of local thickness inhomogeneity. The beam size on the samples is around 3 mm × 3 mm. The gathered spectral range is covering the Ni K absorption edge at 8332 eV. Normalization of the spectra, as well as linear combination fitting (LCF), was done by using the XAS analyzing and processing software ATHENA which is part of the Demeter software package.⁵

Surface characterization was performed using X-ray photoelectron spectroscopy (XPS) on a Thermo Scientific MultiLab 2000 spectrometer, equipped with a monochromatic Al K α Xray source (E = 1486 eV) and an Alpha 110 hemispherical analyzer. The base pressure lies in 10^{-10} mbar range, and charging of the sample upon measurement is compensated by a flood gun supplying electrons with a kinetic energy of 6 eV. The used pass energy was 20 eV. High-resolution spectra in the relevant La 3d, Ni 2p, and Ni 3p regions have been collected and used for qualitative and quantitative analysis. The latter, with respect to Ni, has been exclusively performed using Ni 3p due to the strong overlap of the La 3d and Ni 2p peaks. After background subtraction using a Shirley-type function, deconvolution of the Ni 3p peak into Ni³⁺, Ni²⁺, and metallic Ni components was done, obeying the spin-orbit coupling of the individual Ni $3p_{1/2}$ and Ni $3p_{3/2}$ peaks for each relevant component.

3. RESULTS AND DISCUSSION

3.1. Stability and Decomposition of Doped Perovskites in the DRM Mixture: Benchmark States before and after DRM. A short note on the naming of the catalysts is appropriate at this point: The formulas (e.g., La_{1.8}Ba_{0.2}NiO₄),

in essence, refer to the initial catalyst precursor materials. Although the active phases, formed by the controlled decomposition of the Ruddlesden-Popper structures, are only inadequately described by the above formulas, we will keep the respective naming for the sake of simplicity also for the decomposed materials. Figure 1A,B summarizes the joint ex situ PXRD structural characterization for all A- and B-side doped perovskites before the catalytic DRM run up to 800 °C. The perovskite La2NiO4 structure is clearly present for all Ruddlesden-Popper phases in the initial states. La₂NiO₄ can, in principle, crystallize either in tetragonal (space groups: I4/ *mmm* and $P4_2/ncm$) or orthorhombic (space groups: *Bmab* and *Fmmm*) structures.⁵³⁻⁵⁵ Space groups discrimination is possible by the appreciation of an orthorhombic distortion leading to peak splitting or appearance of superstructure reflections exclusively allowed in the orthorhombic symmetry. If the orthorhombic distortion is very small (i.e., the difference between the *a* and *b* parameters is very small), anisotropic broadening can be observed in some XRD peaks instead of their splitting. Figure 1A,B reveals that all peaks in the XRD patterns can be indexed in the tetragonal structure (PDF card #00-076-0055), with small shifts of the (004) and (200) reflections to lower and higher 2θ angles, respectively, in the case of Cu and Ba doping. These shifts suggest an increase in the lattice parameter c_i , but a decrease in the a and bparameters of the tetragonal lattice. A close inspection of the XRD patterns reveals anisotropic broadening of reflections in some samples, which may be due to the orthorhombic symmetry of these materials. Therefore, we performed structural refinement of the five samples using the two reported structures (i.e., tetragonal I4/mmm and orthorhombic *Fmmm*). Comparing the convergence factors R_{wv} , R_v and R_B (Table 1), obtained from structure refinement of the diffraction data, revealed that undoped La2NiO4 and exclusively Cu-doped La_2NiO_4 (e.g., $La_2Ni_{0.9}Cu_{0.1}O_4$ and La2Ni08Cu02O4) prefer to adapt an orthorhombic structure (Fmmm), while Ba-doped La2NiO4 (e.g., La18Ba02NiO4 and La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O₄) exhibit a tetragonal structure (I4/ mmm). The results are corroborated by the very low orthorhombicity factor δ [i.e., $\delta = (a - b)/(a + b)$, with a and *b* representing in-plane orthorhombic lattice parameters] of Ba-doped La₂NiO₄ samples ($\delta \leq 1.4 \times 10^{-4}$), suggesting a higher symmetry, for example, of a tetragonal lattice type. These results are consistent with previous works reporting that undoped La₂NiO₄ and La₂Ni_{1-x}Cu_xO₄ (x < 0.2) perovskites exhibit an orthorhombic lattice (*Fmmm*), while $La_{2-x}Ba_xNiO_4$ $(x \le 1.0)$ crystallize in the tetragonal *I*4/*mmm* structure.^{54–7} Very small amounts (less than 1 wt.%) of hexagonal La₂O₃ and La(OH)₃ phases were detected in all initial samples. In situ PXRD experiments showed that the La(OH)₃ phase transforms first to LaOOH (PDF card #00-077-2349) and subsequently to La2O3 before the decomposition of the perovskite starts. La2O3 remains stable during the DRM run and before the final breakdown of the perovskite structure. As confirmed in Table 1, slight deviations in the lattice parameters of the doped samples from the parent La2NiO4 structure suggest the successful introduction of Ni and Ba ions in the perovskite lattice. Tang et al.⁵⁷ showed that substitution of larger Ba²⁺ for smaller La³⁺ $[r (Ba^{2+}) = 1.47 \text{ Å}, r (La^{3+}) = 1.216 \text{ Å}; all cations are 9-fold coordinated]⁵⁷ into the perovskite$ lattice leads to an increase in the *c* parameter. On the contrary, a decrease in the *a* parameter could be observed because of the partial oxidation of larger Ni²⁺ to smaller Ni³⁺ ions $[r (Ni^{2+}) =$



Figure 2. Weight fractions (Panel A), crystallite size and lattice parameters of the exsolved metallic Ni particles (Panel B) extracted from Rietveld refinement of the ex situ PXRD patterns of the five spent doped La_2NiO_4 Ruddlesden–Popper materials after one DRM cycle (CO₂:CH₄:He = 1:1:3) in a total gas flow of 100 mL min⁻¹ up to 800 °C for a total time of 2 h.

0.69 Å, r (Ni³⁺) = 0.6 Å and 0.56 Å for high and low spin, respectively. All cations are 6-fold coordinated]⁵⁸ to compensate the charge difference resulting from Ba²⁺ substitution. The presence of Ni³⁺ in the doped samples is confirmed by XANES and XPS characterizations, as discussed in section 3.3. The substitution of Ni²⁺ by Cu²⁺ increases the length of the apical bonds of the [(Ni/Cu)O₆] octahedra along the *c*-axis to exceed the equatorial ones along the *ab* direction due to the Jahn–Teller effect of Cu²⁺ with an electronic configuration of d^{9.56} Therefore, the *c* parameter increases with Cu substitution, while the *a* and *b* parameters decrease.

After the respective catalytic DRM ($CO_2:CH_4:He = 1:1:3$) runs in a total gas flow of 100 mL min⁻¹ for 2 h (Figure 1C,D), clear signs of total decomposition of the Ruddlesden-Popper phase are visible. Phase mixtures of Ni metal (PDF card #00-004-0850), hexagonal La₂O₃ (PDF card #00-005-0602), monoclinic La₂O₂CO₃ (PDF card #00-048-1113), La(OH)₃ (PDF card #00-036-1481), and BaCO₃ (PDF card #00-78-2057) (for the A-site doped samples) are a common structural leading theme for all studied samples. A more detailed analysis of the phase composition results in the lattice parameter and Ni crystallite size obtained from Rietveld refinement of the diffraction data (Figure 2). Whereas the phase composition, as judged by the weight fraction of the participating structures, appears more or less unaltered (with the exception of $La(OH)_3$ formation for the B-site doped perovskites and the presence of BaCO₃ for the A-site doped ones), pronounced differences appear in the lattice parameter upon introduction of Cu into the B site and the resulting Ni crystallite size difference between the A-site doped and the corresponding undoped or B-site doped samples. As expected, the lattice parameter of Ni increases slightly upon the introduction of Cu due to the formation of Ni-Cu alloy. The compositions of the formed Ni-Cu alloy, which are determined from the lattice parameter according to Vegard's law,⁵⁹ are Ni_{0.89}Cu_{0.11}, Ni_{0.80}Cu_{0.20}, and $Ni_{0.88}Cu_{0.12}$ for $La_2Ni_{0.9}Cu_{0.1}O_4$, $La_2Ni_{0.8}Cu_{0.2}O_4$, and La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O₄, respectively. These are in good agreement with the Ni/Cu ratios used in the synthesis of the perovskites. Whereas the introduction of Cu has no apparent effect on the Ni metal crystallite size, adding Ba to the A site

increases the Ni crystallite size by a factor of at least 3, from around 10 nm to more than 30 nm. Qualitatively, the patterns before subjecting the samples to DRM and the Ni crystallite sizes of pure and B-site substituted La₂NiO₄ after the DRM run resemble those reported in literature.^{19,25} The comparison after the catalytic DRM run is less straightforward because literature usually reports structures after a prereduction step and subsequent DRM treatment at temperatures $T \ge 700$ °C. After prereduction, usually a mixture of metallic Ni and La₂O₃ results, which then transforms to metallic Ni and hexagonal/ monoclinic La₂O₂CO₃ after prolonged DRM treatments at reaction times t > 5 h. Temperatures below T = 750 °C cause only partial decomposition of La₂NiO₄.¹⁸ This might explain the difference to the data shown in Figure 1, which correspond to treatments after 2 h.

As for the structural trends apart from Ni crystallite size and the lattice parameter, we note that with increasing the amount of Cu, the final oxy-carbonate amount decreases, and the amount of $La(OH)_3$ increases. We might anticipate interfacial stabilization of the (oxy)carbonate species by Ni and, vice versa, stabilization of $La(OH)_3$ through Cu at the (inter)metallic surface. This is at least in part backed up by the in situ XRD experiments, which show a very low amount of (oxy)carbonate species after catalysis for $La_2Ni_{0.8}Cu_{0.2}O_4$.

In Figure 3 and Figures S1-S5, the complementary ex situ TEM analysis of three representative samples is shown (Figure 3 - La $_2Ni_{0.9}Cu_{0.1}O_4$, Figure S1 - La $_{1.8}Ba_{0.2}NiO_4$ and Figure S2 -La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O₄, Figure S3 - overview images, Figure S4 -SAED patterns, Figure S5 - Fast Fourier Transform (FFT)filtered HRTEM image of La2Ni09Cu01O4 and La18Ba02Ni09- $Cu_{0,1}O_4$ in the initial state). The common feature of all catalysts is the more or less uniform elemental distribution of all constituting elements without agglomeration of species and the corroboration of the successful synthesis of the structures in the initial state (some inhomogeneity is present for Ba, cf. Figures S1 and S2). Taking La₂Ni_{0.9}Cu_{0.1}O₄ as one representative example (Figure 3), the oxide grain size is found between 500 nm and 2 μ m (as derived from Figure S3). In the spent catalyst after one DRM cycle at 800 $^\circ C$ for 2 h (Figure 3, lower panel), oxygen and lanthanum are still



Figure 3. Electron microscopy analysis of $La_2Ni_{0.9}Cu_{0.1}O_4$ in the initial and spent state after one DRM cycle ($CO_2:CH_4:He = 1:1:3$) in a total gas flow of 100 mL min⁻¹ up to 800 °C for a total time of 2 h. Panels A and C: HAADF images, Panels B and D: EDX analysis of the O–K, La-L, Cu–K, and Ni–K intensities. Some exsolved Ni particles are marked by arrows in Panel C.

uniformly distributed, in contrast to Ni and Cu. The latter directly confirms the decomposition of the Ruddlesden– Popper structure and the exsolution of Ni and the formation of small Ni (or Ni/Cu in the case of B-site doped phases) particles after one catalytic DRM cycle. Most of the Ni particles are found at typical diameters between 10 nm and 30 nm, and due to the match of the Ni–K and Cu–K intensities, the formation of a Ni–Cu alloy phase is likely. Some agglomerated Ni(Cu) particles are also shown. The Ni particle sizes of B-site substituted La₂NiO₄ after the DRM run agrees with those reported in literature.²⁵

In parallel to the decomposition, the formation of hexagonal La_2O_3 , as well as hexagonal $La_2O_2CO_3$ and monoclinic $La_2O_2CO_3$, is also prevalent. HRTEM analysis corroborates the PXRD results on a local scale and confirms a mixture of Ni/NiCu alloy phases, hexagonal La_2O_3 , and monoclinic (and locally also hexagonal) $La_2O_2CO_3$. To discriminate between different phases, representative lattice fringes have been Fourier-filtered and accordingly color-coded in Figure 4A,B

A particularly important question, especially for prospective DRM catalysts is connected to the coking resistance. The latter has been reported to be especially improved for Cu-doped Nicontaining perovskite materials.⁶⁰ As discussed above, we suspect alloy formation between Cu and Ni based on ex situ XRD measurements and their stoichiometry has been determined from the lattice parameter using Vegard's law, also confirmed by HRTEM and EDX analysis. Figure 5, for La2Ni0.9Cu0.1O4 and La1.8Ba0.2Ni0.9Cu0.1O4, reveal that B-site doping with Cu (irrespective of eventual A-site doping with Ba) always causes the formation of Ni-Cu particles with an approximate nominal composition between Ni7Cu (La2Ni0.9Cu0.1O4, Figure 5B) and Ni9Cu (La1.8Ba0.2Ni0.9Cu0.1-O₄, right and left particle in Figure 5D,F) as evidenced by locally resolved EDX mapping. Hence, very Ni-rich alloys are encountered almost in the same nominal overall bulk composition as after synthesis. In the remaining parent Ruddlesden-Popper phase (right area in Figure 5B), the nominal composition between Cu and Ni is almost 1:1, corroborating the drastic local loss of Ni by exsolution. Although the according data is not provided in the literature, estimations from XRD shifts for similar compositions indicate alloys with a nominal Ni:Cu composition of <1:1. 25 Table 2 summarizes the full quantitative analysis by EDX of



Figure 4. Aberration-corrected high-resolution electron microscopy images of $L_{2}Ni_{0.9}Cu_{0.1}O_{4}$ (Panel A and C) and $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_{4}$ (Panel B and D) in the spent state after one DRM cycle (CO₂:CH₄:He = 1:1:3) in a total gas flow of 100 mL min⁻¹ at 800 °C for 2 h. Representative lattice fringes of relevant individual structures and phases have been color-coded. Color codes: Panel A – red: NiCu (200), green: hexagonal $La_2O_2CO_3$ (002); Panel B – red: NiCu (111), green: hexagonal $La_2O_2CO_3$ (202), blue: hexagonal La_2O_3 (011). The respective FFT patterns used for color-coding are shown as insets. The lattice fringes in Panels C and D correspond to hexagonal $La_2O_2CO_3$ (102), NiCu (111), and monoclinic $La_2O_2CO_3$ (023).



Figure 5. Panel A and B: HAADF image and EDX analysis of spent $La_2Ni_{0.9}Cu_{0.1}O_4$ (Ni–K (red), Cu–K (yellow), and La-L (green) after one DRM cycle (CO₂:CH₄:He = 1:1:3) in a total gas flow of 100 mL min⁻¹ up to 800 °C for a total time of 2 h. Panels C/D and E/F show HAADF images and EDX maps of different spots on spent $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$. (Ni–K (red), Cu–K (yellow), La–L (green), and Ba–L (magenta)). The areas that have been used for quantitative analysis are encircled.

representative samples. In essence, the composition of all catalysts before and after the catalytic DRM runs remains constant.

3.2. Dynamic Structural Response during DRM Monitored by In Situ Powder X-ray Diffraction. In this section, the structural and phase changes occurring during a

Table 2. Full Quantitative EDX Analysis of La_2NiO_4 , $La_2Ni_{0.9}Cu_{0.1}O_4$, and $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$ in the Initial and Spent Catalyst State^{*a*}

DRM	sample	La-L at%	Ni-K at%	O−K at%	Cu–K at%	Ba-L at%	total at%
before	LaNiO ₃	17.87 ± 1.61	15.61 ± 2.82	66.51 ± 3.21	-	-	100
after	LaNiO ₃	23.31 ± 3.41	18.42 ± 3.83	58.26 ± 6.33	-	-	100
before	La_2NiO_4	30.09 ± 4.73	15.16 ± 2.76	54.74 ± 7.29	-	-	100
after	La_2NiO_4	21.64 ± 3.18	11.59 ± 2.23	66.75 ± 5.27	-	-	100
before	$La_2Ni_{0.9}Cu_{0.1}O_4$	27.36 ± 2.07	14.42 ± 4.49	56.63 ± 5.13	1.57 ± 1.26	-	100
after	$La_2Ni_{0.9}Cu_{0.1}O_4$	21.84 ± 2.19	10.7 ± 1.42	65.26 ± 3.56	2.19 ± 0.43	-	100
before	$La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$	24.66 ± 3.25	12.07 ± 2.53	60.6 ± 4.29	2.66 ± 0.66	0 ^b	100
after	$La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$	23.34 ± 4.02	12.47 ± 2.48	62.36 ± 6.67	1.80 ± 0.30	0 ^b	100

^{*a*}For the sake of comparability, the EDX data of the archetypical $LaNiO_3$ system is also shown. ^{*b*}Ba could not be quantified directly using this method due to the strong overlap of the Ba-L edge with that of La-L. This means that La-L is slightly overestimated, but still within the error margin of the method.

Table 3. Summary of Weight Fractions Extracted from PXRD Patterns by Rietveld Refinement for All Initial Samples, as well as for the Recovered Ones after the In Situ PXRD Experiments and after the DRM Treatment

sample/weight fraction (%)		LaNi ₂ O ₄	La_2O_3	La(OH) ₃	La ₂ O ₂ CO ₃ hex.	La ₂ O ₂ CO ₃ mono.	Ni metal	BaCO ₃
$La_2Ni_{0.9}Cu_{0.1}O_4$	initial	98.9(0.9)	0.2(0.1)	0.9(0.3)	-	-	-	-
	recovered from in situ experiment	99.2(0.8)	0.2(0.2)	-	-	0.6(0.2)	-	-
	recovered from DRM experiment	-	63.2(1.6)	10.8(0.8)	-	10.7(1.0)	15.3(1.2)	-
$La_2Ni_{0.8}Cu_{0.2}O_4$	initial	98.6(0.8)	0.5(0.2)	0.9(0.2)	-	-	-	-
	recovered from in situ experiment	-	73.3(0.8)	-	1.3(0.3)	5.8(0.7)	19.6(0.7)	-
	recovered from DRM experiment	-	56.7(0.9)	24.4(0.7)	-	1.8(0.3)	17.1(0.3)	-
La _{1.8} Ba _{0.2} NiO ₄	initial	97.3(1.3)	1.8(0.2)	0.9(0.2)	-	-	-	-
	recovered from in situ experiment	97.7(1.4)	0.9(0.2)	-	0.7(0.2)	0.5(0.2)	0.2(0.1)	-
	recovered from DRM experiment	-	65.6(0.9)	-	-	11.9(0.6)	16.4(0.6)	6.1(0.4)
$La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$	initial	98.6(0.6)	0.8(0.1)	0.6(0.1)	-	-	-	-
	recovered from in situ experiment	-	28.6(0.5)	-	13.6(0.4)	40.0(0.7)	17.8(0.5)	-
	recovered from DRM experiment	-	65.4(0.9)	-	-	12.0(0.6)	17.4(0.6)	5.2(0.4)

catalytic DRM run are jointly discussed for all four relevant Ruddlesden-Popper precatalysts to correlate the changes to the catalytic patterns discussed in section 3.3 but also to the ex situ-determined states after the factual DRM run. As the benchmark states before and after the DRM run have been already highlighted in section 3.1, the goal in this section is to characterize the dynamic structural response of the materials to the DRM mixture in the temperature range between 25 °C and 800 °C and also upon an isothermal treatment to mimick the catalytic experiments as closely as possible. The discussion and analysis will be split in a qualitative and quantitative part for each sample. For the summarized sample composition in the initial and the spent catalyst state, we generally refer to Table 3. As representative examples, we show the full analysis for La2Ni08Cu02O4 and the simultaneously A- and B-site substituted La1.8Ba0.2Ni0.9Cu0.1O4 phase in the main manuscript. For all other samples, including the undoped La2NiO4 material, the qualitative and quantitative analysis is highlighted in the Supporting Information Figures S6-S10.

One particular issue entangled with the effect of the structure and composition of doped La_2NiO_4 catalyst precursors on the methane dry reforming reactivity is the already well-known orthorhombic-tetragonal phase transformation for La_2NiO_4 occurring at around 150 °C and the loss of the interstitial oxygen from the tetragonal structure above 450 °C upon annealing.^{38,39,53} As the onset temperature of these two phase transformations has been suspected to be a function of the gas atmosphere,⁶¹ a dependence on the doping level is therefore likely, potentially also affecting the catalytic performance.

As shown in Figure 6, we observe several consecutive phase changes during heating La2Ni0.8Cu0.2O4 catalyst under DRM conditions. The minor $La(OH)_3$ phase existing in the initial sample transforms first to the intermediate LaOOH phase at 320 °C and then both phases irreversibly transform into La_2O_3 before the decomposition of the perovskite starts. The monoclinic La2O2CO3 phase forms first at 625 °C due to the reaction between CO_2 and La_2O_3 that is already present as a minor phase in the catalyst. The amount of monoclinic $La_2O_2CO_3$ increases up to 750 °C to a maximum amount of \sim 10 wt.%, above which intertransformation into hexagonal $La_2O_2CO_3$ takes place (Figure 6C,D). In parallel, the parent $La_2Ni_{0.8}Cu_{0.2}O_4$ perovskite remains largely stable up to 750 °C before partial decomposition into La2O3, Ni, and a Ni-Cu alloy phase starts. After isothermal heating at 800 °C for 20 min, full decomposition of $La_2Ni_{0.8}Cu_{0.2}O_4$ into metallic Ni, a NiCu alloy phase, hexagonal La2O3, and minimal amounts of hexagonal and monoclinic La₂O₂CO₃ takes place within a very short period of time. The recovered sample after in situ XRD is characterized by 73.7 wt.% hexagonal La₂O₃, but very little monoclinic (5.8 wt.%) and hexagonal (1.3 wt.%) La₂O₂CO₃, as well as 19.6 wt.% metallic Ni. Compared with the ex situ structural state after the catalytic DRM experiment (ex situ final state composition in Figure 2, left panel), the amount of La_2O_3 is higher, and $La(OH)_3$ is practically absent. The partial transformation of La_2O_3 to $La(OH)_3$ in the ex situ sample might be at least partially caused by contact to ambient moisture,⁶² which was not the case for the in situ sample (analyzed directly after cooling under dry conditions). Otherwise, the phase composition is comparable. In summary,



Figure 6. Panel A: In situ collected XRD patterns of $La_2Ni_{0.8}Cu_{0.2}O_4$ during heating up to 800 °C under DRM conditions. Panel C: In situ collected XRD patterns of $La_2Ni_{0.8}Cu_{0.2}O_4$ during holding at 800 °C for 30 min under DRM conditions. Panels B and D focus on a narrower 2 θ windows for closer analysis. The lower panels indicate the phase assignment to the respective reference structures. Panel E and F: Weight fractions of different crystalline phases formed during DRM as a function of temperature (E) and time at 800 °C (F) obtained by Rietveld refinement of the in situ collected XRD patterns of $La_2Ni_{0.8}Cu_{0.2}O_4$.

the carbonation in this Cu-doped sample is present, but yet not very pronounced.

A similar course of phase decomposition has been observed on $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$, although it exhibits a different starting structure (i.e., tetragonal). Obviously, the introduction of Ba stabilizes the tetragonal structure also at elevated temperatures. As shown in Figure 7, the overall course of decomposition, including the appearance of specific phases, is qualitatively comparable to $La_2Ni_{0.8}Cu_{0.2}O_4$, although the decomposition temperature of $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$ is shifted to 800 °C. A higher decomposition temperature is likely to influence the nucleation- and growth kinetics of the exsolved Ni^0 species toward larger and fewer nuclei, which can explain the observed larger Ni particle size. Another particular difference is the very efficient carbonation process, as judged by the phase composition of 10 wt.% monoclinic $La_2O_2CO_3$ and 20 wt.% hexagonal $La_2O_2CO_3$ in the recovered sample, the remainder being Ni metal (10 wt.%) and $BaCO_3$ (10 wt.%). Thus, the carbonation process is very efficient in this case. Note that LaOOH and $La(OH)_3$ again appear as intermediate phases upon heating, but decompose to hexagonal La_2O_3 well before catalytic DRM activity is observed. Thus, they appear of minor importance in determining the effects of structure and composition of doped La_2NiO_4 precursors on the DRM reactivity.

The La_{1.8}Ba_{0.2}NiO₄ material highlighted in Figure S6 is structurally stable over the entire temperature range. Minimal Ni exsolution starts at temperatures slightly below 800 °C and continues on a low level upon holding the temperature for 60 min at 800 °C (corresponding to ~0.1 wt.%). In parallel, the



Figure 7. Panel A: In situ collected XRD patterns of $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$ during heating up to 800 °C under DRM conditions. Panel C: In situ collected XRD patterns of $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$ during holding at 800 °C for 30 min under DRM conditions. Panels B and D focus on a narrower 2 Θ windows for closer analysis. The lower panels indicate the phase assignment to the respective reference structures. Panel E and F: Weight fractions of different crystalline phases formed during DRM as a function of temperature (E) and time at 800 °C (F) obtained by Rietveld refinement of the in situ collected XRD patterns of $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$.

formation of hexagonal La₂O₃ and both hexagonal and monoclinic La₂O₂CO₃ is observed. Monoclinic La₂O₂CO₃ starts to be formed around 500 °C, proceeding at a constant slow rate up to 800 °C, finally reaching about 0.8(0.2) wt.%. In the isothermal period at 800 °C, intertransformation of the two polymorphic forms of La₂O₂CO₃ occurs, forming hexagonal La₂O₂CO₃ directly from the associated monoclinic modification. The data suggest that this oxycarbonate formation directly arises from La₂O₃ present as a minor stray structure at the surface or at interfaces of the initial sample and that the La_{1.8}Ba_{0.2}NiO₄ bulk structure is in essence stable. Compared with undoped La₂NiO₄, apparently, the introduction of Ba²⁺ effectively stabilizes the parent perovskite structure. In total, the amount of exsolved metallic Ni corresponds to ~0.2 wt.% in the spent sample, suggesting an exsolution process limited to surface-near regions.

These observations are of more general interest for all catalysts, where decomposition into nanoparticles in contact with a specific oxide support is performed to generate the active phase. This particularly also refers to perovskite and perovskite-related materials that are specifically selected because of their structural metastability toward decomposition into the active phase. The outlined results indicate that apart from the inherent thermodynamical metastability, also the control of the exsolution kinetics plays a crucial role. As it is suspected that in particular Ni particles in contact with La₂O₂CO₃ (as the regenerative active CO₂-captivating species) are active species during DRM, we might infer that the especially the delicate antagonistic balance of doping with Ba²⁺

on the A-site (enhancing the basicity and eventually stabilizing the perovskite lattice toward decomposition) and doping with Cu^{2+} on the B-site (enhancing the reducibility of the structure and triggering the early exsolution of Ni, as well as the full decomposition of the parent La_2NiO_4 structure) appears as a key parameter in the controlled decomposition of $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$.

To evaluate the extent of the Ni-oxide-(oxy)carbonate interface, Figure 8 details the evolution of the metallic Ni or



Figure 8. Crystallite size of Ni/NiCu metal formed during DRM at 800 °C as a function of time obtained by Rietveld refinement of the in situ collected XRD patterns of $La_2Ni_{0.8}Cu_{0.2}O_4$ and $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$ samples.

NiCu crystallite size for two representative doped perovskite samples during the respective isothermal period. Being immediately obvious, B-site doping with Cu without Ba at the A-site results in much smaller Ni/NiCu crystallite sizes (around 5 nm at the end of the isothermal period), compared with those observed after treating $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$ under similar experimental conditions. In that case, the Ni crystallite sizes appear almost doubled at around 10 nm. The differences to the Ni crystallite sizes obtained after DRM by ex situ analysis appear basically due to the different extent of the isothermal period (120 min vs 30 min for the in situ XRD experiments), although the qualitative trend is exactly the

same. As a potential explanation for the catalytic results of the exclusively Ba-doped sample discussed below, we note that we have proven by in situ XRD that the Ba-containing sample exhibits around 0.2 wt.% Ni after exsolution compared with the Ba-free sample exhibiting around 20 wt.%. The Ni crystallite size of the Ba-free sample is also smaller but exhibits more metallic Ni. This is a two-factor improvement compared with the Ba-containing sample: more metallic Ni and a smaller Ni crystallite size (increasing the surface area) both contribute to an increased DRM activity. This finding is also confirmed by measuring the BET surface area of the catalysts before and after DRM. As shown in Table S1, the BET surface area of all catalysts are slightly increased after DRM (i.e., after the formation of metallic Ni), except for La₁₈Ba_{0.2}NiO₄ catalyst showing a decrease in the BET surface area after decomposition.

The tetragonal *I4/mmm* structure of our catalysts can be distinguished from the low-temperature orthorhombic *Fmmm* structure by the change in the broadening of some XRD peaks. In consequence, this change in peak broadening will cause a remarkable change in the cell parameters *a* and *b* at the transition temperature. Similarly, the loss of oxygen from interstitial sites or chemical expansion of the catalyst at high temperatures is evident from the evolution of the lattice parameters and the unit cell volume. Therefore, for a more detailed analysis, Figure 9 (and Figure S10) highlights a comparative assessment of the evolution of the cell parameters *a*, *b*, and *c* with temperature for the four catalyst samples as well as undoped La₂NiO₄. *a*_o, *b*_o, as well as *a*_t and *b*_t refer to the lattice parameter of the orthorhombic and tetragonal structures, respectively, where $a_t = b_t$ but $a_o \neq b_o$.

As discussed above, undoped La₂NiO₄ and Cu-doped La₂NiO₄ (e.g., La₂Ni_{0,9}Cu_{0,1}O₄ and La₂Ni_{0,8}Cu_{0,2}O₄) exhibit an orthorhombic *Fmmm* structure, while Ba-doped La₂NiO₄ (e.g., La_{1.8}Ba_{0.2}NiO₄ and La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O₄) adopt the tetragonal *I*4/*mmm* structure at room temperature. Upon heating, the cell parameters *a* and *b* of the orthorhombic La₂NiO₄, La₂Ni_{0.9}Cu_{0.1}O₄, and La₂Ni_{0.8}Cu_{0.2}O₄ materials (converted through a $\sqrt{2a}$ arelationship to tetragonal cell) converge at 125 °C, 170 °C, and 175 °C, respectively, indicating the orthorhombic-to-tetragonal transformation. This result agrees with previous in situ neutron diffraction studies



Figure 9. Evolution of the lattice parameters a and c of all doped La₂NiO₄ samples as a function of reaction temperature. a_0 , b_0 , as well as a_t and b_t refer to the lattice parameter of the orthorhombic and tetragonal structures, respectively, where $a_t = b_0$, but $a_0 \neq b_0$.



Figure 10. Methane dry reforming profiles (1st (magenta) and 2nd (green) cycle) on $La_{1.8}Ba_{0.2}NiO_4$, $La_2Ni_{0.9}Cu_{0.1}O_4$ and La_2NiO_4 , $Cu_{0.2}O_4$, $La_{1.8}Ba_{0.2}NiO_4$, La_2NiO_4 , La_2N

reported the irreversible orthorhombic-to-tetragonal transformation of undoped La₂NiO₄ at about 150 °C.^{53,55} Our experiments showed that introducing Cu in the B site to reach a nominal composition of La2Ni0.8Cu0.2O4 reveals that the orthorhombic-tetragonal transformation is inhibited up to 175 °C, inferring a hindering influence of a higher Cu amount on the onset of phase transformation. This might be explained by the increase in reducibility upon the introduction of larger amounts of Cu, thus supporting the formation of a tetragonal oxygen-depleted phases at higher temperatures. A similar situation prevails for a lower Cu content of La₂Ni_{0.9}Cu_{0.1}O₄. With a further increase in the temperature, there is a clear chemical expansion observed for pure and exclusive Cu-doped La₂NiO₄ in the temperature range of 450 °C-650 °C. This expansion is accompanied by a decrease in the *c* parameter and an increase in the *a* parameter, which can be explained by the loss of excess oxygen occupying the interstitial sites located in the La-O plane in the *ab* direction of the tetragonal lattice. The loss of these interstitial oxygen leads to a compression along the c direction and an expansion in the ab direction.^{54,55} In contrast, Ba doping reduces the chemical expansion due to the increase in the oxidation state of Ni from +2 to +3, as well as due to the reduction of the amount of interstitial oxygen in the initial tetragonal structure at room temperature. Although it appears as some sort of chemical expansion, we might link the observed expansion to the loss of interstitial oxygen from the tetragonal lattice, as the expansion is clearly absent for the Ba-doped samples that do not show the transformation. It is now confirmed, as it was earlier suspected for pure La_2NiO_4 that the decomposition of the doped La₂NiO₄ samples, in fact, is preceded by the orthorhombic-to-tetragonal transformation followed by another structural transformation because of the loss of interstitial oxygen from the tetragonal lattice, and the breakdown rather starts from the progressively oxygendepleted tetragonal structure.

3.3. Influence of Doping on the Catalytic Behavior in DRM: Key Factors Steering the Reactivity. The catalytic profiles of all relevant samples, including undoped La₂NiO₄,

are jointly summarized in Figure 10. For all samples, we have conducted two sequential DRM cycles up to 800 °C, including a cooling down phase to 25 °C before the second cycle. The two consecutive cycles have been conducted to follow the development of the catalytic activity during the decomposition of the Ruddlesden-Popper structure, as well as to assess the activity of the resulting metal-oxide system, which is formed after the completion of the first DRM cycle. All samples show at least some DRM activity, with A-site substituted La_{1.8}Ba_{0.2}NiO₄ clearly exhibiting the worst behavior. For this particular sample, hardly any activity is observed even at the highest reaction temperatures, which is explained by the generally lower amount of exsolved Ni and the comparatively larger Ni crystallite size, alongside the particular stabilization by Ba. DRM activity of the undoped La₂NiO₄ material in the first cycle is observed at around 700 °C, and this onset temperature is shifted to somewhat higher temperatures for both the B-site doped $La_2Ni_{0.9}Cu_{0.1}O_4$ (720 °C) and La2Ni08Cu02O4 (740 °C) as well as the A-site and B-site doped La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4 sample (740 $^\circ C).$ Conducting a second DRM cycle exclusively results in a significant lowering of the catalytic light-off temperatures by at least 100 °C, depending on the individual catalyst. Doping on the B site (even if Ba is simultaneously present at the A site) is thereby clearly beneficial as judged by the light-off temperatures of undoped La2NiO4. Qualitively, the catalytic profiles of the second cycles are comparable between La2Ni09Cu01O4, La2Ni0.8Cu0.2O4, and La1.8Ba0.2Ni0.9Cu0.1O4, although the exclusively B-site doped structures exhibit somewhat smaller light-off temperatures (450 °C vs 500 °C for $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4).$

For La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O₄, we also conducted prolonged isothermal reactions at 800 °C (3 h) and subsequently, after lowering the temperature, also for 3 h at 700 °C. During the isothermal treatment at 800 °C, the catalyst is still selfactivating. At 700 °C, the activity remains stable over the entire isothermal period (Figure 10B). The stable conversion of CO₂ and CH₄ over these isothermal periods points to the lack of



Figure 11. Normalized Ni K-edge X-ray absorption near-edge structure (XANES) of $La_2Ni_{0.8}Cu_{0.2}O_4$ (A), $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$ (B), $La_2Ni_{0.9}Cu_{0.1}O_4$ (C), and $La_{1.8}Ba_{0.2}NiO_4$ (D) Ruddlesden–Popper materials before and after one catalytic DRM cycle in a total gas flow of 100 mL min⁻¹ at different conditions. The spectra are compared with those of the reference materials (Ni and La_2NiO_4).

formation of deactivating surface carbon and to the absence of substantial metal particle sintering. Surface carbon formation does not necessarily deactivate the catalyst and, for some systems, is a necessary intermediate of reaction.^{27,63} Previously shown in situ XRD data (cf. Figures 6, 7, and S6-S8) and microscopy data (Figures 3-5 and S1-S4) also support the claim of the absence of graphitic carbon formation under DRM conditions. Figure 8 shows a minor increase of the Ni crystallite size with time on stream for the La2Ni08Cu02O4 and $La_{18}Ba_{02}Ni_{09}Cu_{01}O_4$ samples. The H₂/CO ratios, monitored during the isothermal periods (Figure 10B, blue color, right axis) are close to unity at all reaction temperatures and reaction times. Two points are noteworthy: the comparatively discussed catalytic profiles of the respective first cycles indicate already that the pathway of decomposition of the differently doped materials is clearly different, corroborating the XRD results. The resulting active phase, in all cases, a Ni/La₂O₃/ $La_2O_2CO_3$ composite material with a more or less extended metal-oxide-(oxy)carbonate interface is, thus, formed differently. Second, once the active interface is established during the first runs, the second DRM cycles are comparable, with minor differences due to different doping on the A and/or B site-resulting from different Ni crystallite sizes and extents of the Ni/La₂O₃/La₂O₂CO₃ interfaces (cf. Figure 8).

To gain more insights into the influence of structural chemistry and surface area of the catalysts on their catalytic behaviors, the four catalysts were characterized by XRD, XPS, BET, and XANES techniques before and after DRM experiments. Figure S11 shows ex situ collected PXRD patterns of the four Ruddlesden–Popper materials before and after a catalytic DRM (CO₂:CH₄:He = 1:1:3) runs in a total gas flow of 100 mL min⁻¹ at different conditions. XRD results reveal that a slight decomposition of La₂Ni_{0.8}Cu_{0.2}O₄ and La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O₄ into La₂O₃, metallic Ni, and monoclinic La₂O₂CO₃ phases is observed upon heating the catalysts at 770 °C under DRM conditions. The full decomposition of the catalysts takes place after heating at 800 °C for 30 min, except for the La_{1.8}Ba_{0.2}NiO₄ that is partially stable even after 90 min, which agrees with the results of in situ XRD experiments. Hexagonal La₂O₂CO₃ is formed in all catalysts after prolonged DRM treatments at reaction times t > 1 h. These results confirm those of in situ XRD experiments that reveal the formation of active Ni/La₂O₃/La₂O₂CO₃ materials at 800 °C under catalytic DRM conditions.

The chemical and oxidation state of Ni in the catalysts were further investigated by X-ray absorption characterizations. Figure S12 shows the normalized Ni K-edge X-ray absorption near-edge structure (XANES) of pure and doped La2NiO4 Ruddlesden-Popper materials as well as reference materials (NiO and LaNiO₃). The characteristic features observed in the XANES spectra of all the materials are consistent with previous works.⁶⁴ The relative shift in the position of the main adsorption edge, which is attributed to $1s \rightarrow 3p$ transitions, gives information about the average oxidation state of transition elements because of the high sensitivity of outer porbitals to chemical changes.^{65,66} The K-edge position for pure and doped La₂NiO₄ samples locates between those of NiO and LaNiO₃ standards, indicating the presence of both Ni²⁺ and Ni³⁺ cations in all La₂NiO₄ samples. These results can be explained by the accommodation of excess oxygen in the



Figure 12. Evolution of the individual Ni surface species as a function of DRM treatment. Panel A: $La_{1.8}Ba_{0.2}NiO_4$, Panel B: $La_2Ni_{0.8}Cu_{0.2}O_4$, Panel C: $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$. Analysis is based on the deconvolution profiles of Figure S14 and the values highlighted in Table 4.

Table 4. Full XPS Quantification in at.% of All Studied Catalysts after Selected DRM Treatments Based on the Deconvolution Profiles of Figure S14

	$\mathrm{La}_{1.8}\mathrm{Ba}_{0.2}\mathrm{NiO}_4$			$La_2Ni_{0.8}Cu_{0.2}O_4$			$La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4\\$		
XPS fitting data (atom %) of Ni 3p region for catalysts	3p 3/2 (Ni ³⁺)	${3p_{3/2} \atop (Ni^{2+})}$	3p _{3/2} (Ni ⁰)	3p 3/2 (Ni ³⁺)	${3p_{3/2} \over (Ni^{2+})}$	3p _{3/2} (Ni ⁰)	3p _{3/2} (Ni ³⁺)	$_{\rm (Ni^{2+})}^{\rm 3p}$	3p _{3/2} (Ni ⁰)
before DRM	19.99	80.01	0	0	100	0	18.03	81.97	0
cooled down at 770 $^\circ\mathrm{C}$	-	-	-	0	75.12	24.88	13.92	63.28	22.8
after keeping at 800 $^\circ \mathrm{C}$ for 30 min	10.55	42.18	47.27	0	60	40	0	60.45	39.55
after keeping at 800 $^\circ\mathrm{C}$ for 90 min	7.29	36.46	56.25	0	49.11	50.89	0	51.44	48.56

interstitial sites of La2NiO4 lattice and/or the charge compensation due to the Ba and Cu doping. As shown in Figure 11, the Ni K-edge shifts to lower energies upon heating the La₂Ni_{0.8}Cu_{0.2}O₄ and La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O₄ catalysts at 770 °C under catalytic DRM conditions, suggesting the partial reduction of Ni³⁺/Ni²⁺ cations and formation of metallic Ni. As displayed in Figure S13, the linear combination fitting (LCF) of normalized Ni K-edge XANES spectra of La2Ni0.8Cu0.2O4 and La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O₄ with those of reference materials confirm the exsolution of metallic Ni at 770 °C. The weight ratio Ni/La2NiO4 in La2Ni0.8Cu0.2O4 and La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O₄ samples heated at 770 °C is found to be 0.25 and 0.15, respectively, indicating the suppression of perovskite decomposition by Ba doping. Moreover, the XANES spectra of La₂Ni_{0.8}Cu_{0.2}O₄, La₂Ni_{0.9}Cu_{0.1}O₄, and $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$ samples heated at 800 °C for $t \ge 30$ min can be fitted with that of metallic Ni reference, pointing out that the decomposition of the Ruddlesden-Popper materials is complete after 30 min under catalytic DRM conditions. In contrast, the decomposition of La_{1.8}Ba_{0.2}NiO₄ materials is not complete by heating at 800 °C for 90 min as their XANES spectra can be fitted by combining the spectra of both Ni and La2NiO4 references. These are in good agreement with XRD results (Figure S11).

Figure 12 and Table 4 highlight the complementary surface chemical characterization by XPS. We have performed the XPS analysis for three representative catalysts, $La_2Ni_{0.8}Cu_{0.2}O_4$, $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$ and $La_{1.8}Ba_{0.2}NiO_4$ at selected spots on the DRM reaction axis to follow the individual chemical states of the constituting elements: before DRM, quenched at 770 °C during the onset of catalytic activity (cf. Figure 10), after 30 min at 800 °C and after 90 min at 800 °C. The XRD

diffraction patterns of all states are shown in Figure S11, alongside the deconvoluted Ni 3p peaks in Figure S14. The quantification (in at.%) of different Ni species in the samples is shown in Table 4. Figure 12 highlights the evolution of the individual Ni species for La₁₈Ba_{0.2}Ni_{0.9}Cu_{0.1}O₄, La₂Ni_{0.8}Cu_{0.2}-O₄, and La_{1.8}Ba_{0.2}NiO₄. For the former, both Ni³⁺ component (as expected from the Ba doping, corroborating the XANES analysis) and Ni²⁺ before the DRM reaction are clearly visible. A Ni⁰ component arises already after quenching at 770 °C, as expected from the onset of catalytic activity. Correspondingly, the oxidized Ni species decrease as a function of treatment. The presence of the Ni²⁺ species even after full decomposition of the parent Ruddlesden-Popper phase is due to the postoxidation of the exsolved Ni particles upon the transfer to the XPS spectrometer. As already indicated by both XANES and XRD analysis, A-site substituted La_{1.8}Ba_{0.2}NiO₄ appears much more stable compared to the A/B-substituted and the exclusively B-site substituted structure, and accordingly, the amount of Ni³⁺ during the DRM treatment remains higher.

The exsolution of metallic Ni nanoparticles from doped La_2NiO_4 Ruddlesden–Popper materials can also be confirmed by BET surface area. As listed in Table S1, the BET surface area of $La_2Ni_{0.8}Cu_{0.2}O_4$, $La_2Ni_{0.9}Cu_{0.1}O_4$, and $La_{1.8}Ba_{0.2}Ni_{0.9}Cu_{0.1}O_4$ samples increases after heating at 800 °C under catalytic DRM conditions for $t \ge 1$ h due to the formation Ni nanoparticles on the surface of the catalyst. In contrast, BET surface area of $La_{1.8}Ba_{0.2}NiO_4$ catalyst is slightly decreased because of the particle sintering and incomplete decomposition of the perovskite.

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4. CONCLUSIONS

Exemplified for the La2NiO4 system, we have shown the complex interplay of different key parameters that govern the structural integrity and associated DRM activity of different Aand B-site doped Ruddlesden-Popper perovskite materials. Doping directly affects the phase transformation from orthorhombic-to-tetragonal La2NiO4: introduction of Ba to the A site effectively stabilizes the tetragonal structure from room temperature up to 800 °C. Undoped and Cu-doped samples show different extents of transformation to the tetragonal phase in the temperature region from 25 °C to 200 °C and markedly lowered decomposition temperatures toward Ni⁰. As a direct correlation to the observed Ni⁰ particle size after decomposition of the perovskite, A site doping with Ba also leads to much larger particles. We suggest that the nucleation- and growth kinetics of Ni⁰ are shifted toward these larger particles because of the elevated decomposition temperatures due to bulk structure stabilization by Ba. Naturally, this also directly affects the extent of the so-formed, supposedly DRM-active Ni-La2O2-(oxy)carbonate interface. The detailed sequence of transformation and decomposition steps as a function of temperature is a strong function of the catalyst precursor and, therefore, is directly linked to the surface, interface and bulk properties of the final catalyst.

Apart from the apparently different Ni particle size, the bulk structure composition of all in situ decomposed samples is similar, although with different weights in the composition mixture. In due course, the differences in catalytic activity between the undoped and differently doped La2NiO4 materials are also a strong function of doping. Exclusive A-site doping with Ba essentially suppresses catalytic activity due to two factors: a large Ni particle size (hence, a decreased extent of metal-oxide-(oxy)carbonate interface) and a generally lower amount of exsolved Ni. Potentially, also the formation of very stable Ba-related carbonate species is detrimental for a high activity. As can be derived from the TEM results, additional highly thermally stable BaCO₃-Ni⁰ interfaces are generated, with most likely rather poor CO2-activation properties. Cudoping, however, enhances the catalytic DRM activity at lower temperatures in comparison to undoped La2NiO4 by partial alloying with Ni while at the same time keeping the Ni(Cu) particle size small. The introduction of Cu apparently also allows overcoming the limitations of simple A-site doping with Ba by steering the carbonation tendency and distribution of reactive oxycarbonate species. Moreover, we suggest that the exsolved Cu-modified Ni⁰ particles feature a combination of reduced carbon solubility and modulation of the bond strength of reactive C-species. The resulting improved coking properties-due to suppressed graphene/graphite nucleation and growth—may be combined with enhanced reactivity of carbon atoms at the phase boundary, contributing to the observed superior catalytic properties.

ASSOCIATED CONTENT

Supporting Information

The Supporting Information is available free of charge at https://pubs.acs.org/doi/10.1021/acscatal.0c04290.

Additional electron microscopy (TEM overview images, selected area electron diffraction patterns, aberration-corrected high-resolution images) and in situ X-ray diffraction measurements and data evaluation, BET and XPS analysis (PDF)

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Notes

The authors declare no competing financial interest.

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REFERENCES

(1) Global Carbon Project of Future Earth. Surge in Methane Emissions Threatens Efforts To Slow Climate Change. See the following:https://phys.org/news/.

(2) Muraza, O.; Galadima, A. A Review On Coke Management During Dry Reforming Of Methane. *Int. J. Energy Res.* 2015, 39, 1196–1216.

(3) Usman, M.; Wan Daud, W. M. A.; Abbas, H. F. Dry Reforming Of Methane: Influence Of Process Parameters - A Review. *Renewable Sustainable Energy Rev.* **2015**, *45*, 710–744.

(4) Mondal, K.; Sasmal, S.; Badgandi, S.; Chowdhury, D. R.; Nair, V. Dry Reforming Of Methane To Syngas: A Potential Alternative Process For Value Added Chemicals - A Techno-Economic Perspective. *Environ. Sci. Pollut. Res.* **2016**, *23*, 22267–22273.

(5) Er-Rbib, H.; Bouallou, C.; Werkoff, F. Dry Reforming Of Methane-Review Of Feasibility Studies. *Chem. Engin. Trans.* **2012**, *29*, 163–168.

(6) Edwards, J. H.; Maitra, A. M. The Chemistry Of Methane Reforming With Carbon Dioxide And Its Current And Potential Applications. *Fuel Process. Technol.* **1995**, *42*, 269–289.

(7) Dębek, R.; Zubek, K.; Motak, M.; Da Costa, P.; Grzybek, T. Effect Of Nickel Incorporation Into Hydrotalcite-Based Catalyst Systems For Dry Reforming Of Methane. *Res. Chem. Intermed.* **2015**, *41*, 9485–9495.

(8) Al-Fatesh, A. Suppression Of Carbon Formation In $CH_4 - CO_2$ Reforming By Addition Of Sr Into Bimetallic Ni $-Co/\gamma$ -Al₂O₃ Catalyst. J. King Saud Univ. Eng. Sci. **2015**, 27, 101–107.

(9) Ruckenstein, E.; Hu, Y. H. Carbon Dioxide Reforming of Methane Over Nickel/Alkaline Earth Metal Oxide Catalysts. *Appl. Catal., A* **1995**, *133*, 149–161.

(10) Hao, Z.; Zhu, Q.; Jiang, Z.; Hou, B.; Li, H. Characterization Of Aerogel Ni/Al₂O₃ Catalysts And Investigation On Their Stability For CH₄-CO₂ Reforming In A Fluidized Bed. *Fuel Process. Technol.* **2009**, *90*, 113–121.

(11) Lucredio, A. F.; Assaf, J. M.; Assaf, E. M. Methane Conversion Reactions On Ni Catalysts Promoted With Rh: Influence of Support. *Appl. Catal., A* **2011**, *400*, 156–165.

(12) Gould, T. D.; Montemore, M. M.; Lubers, A. M.; Ellis, L. D.; Weimer, A. W.; Falconer, J. L.; Medlin, J. W. Enhanced Dry Reforming Of Methane On Ni And Ni-Pt Catalysts Synthesized By Atomic Layer Deposition. *Appl. Catal., A* **2015**, *492*, 107–116.

(13) Kang, K. M.; Kim, H. W.; Shim, Il.W.; Kwak, H. Y. Catalytic Test Of Supported Ni Catalysts With Core/Shell Structure For Dry Reforming Of Methane. *Fuel Process. Technol.* **2011**, *92*, 1236–1243.

(14) Crnivec, I. G.; Djinovic, P.; Erjavec, B.; Pintar, A. Effect Of Synthesis Parameter On Morphology And Activity Of Bimetallic Catalysts For CH_4 - CO_2 Reforming. *Chem. Eng. J.* **2012**, 207–208, 299–307.

(15) Zhang, X.; Lee, C. S. M.; Michel, D.; Mingos, P.; Hayward, D. O. Carbon Dioxide Reforming Of Methane With Pt Catalyst Using Microwave Electric Heating. *Catal. Lett.* **2003**, *88*, 129–139.

(16) Nagaoka, K.; Okamura, M.; Aika, K. I. Titania Supported Ruthenium As A Coking Resistant Catalyst For High Pressure Dry Reforming Of Methane. *Catal. Commun.* **2001**, *2*, 255–260.

(17) Juan, J. J.; Roman-Martinez, M. C.; Illan-Gomez, M. J. Nickel Catalyst Activation In The Carbon Dioxide Reforming Of Methane: Effect Of Pretreatments. *Appl. Catal., A* **2009**, *355*, 27–32.

(18) Batiot-Dupeyrat, C.; Valderrama, G.; Meneses, A.; Martinez, F.; Barrault, J.; Tatibouët, J. Pulse Study Of CO₂ Reforming of Methane Over LaNiO₃. *Appl. Catal., A* **2003**, *248*, 143–151.

(19) Sierra Gallego, G.; Mondragón, F.; Tatibouët, J.-M.; Barrault, J.; Batiot-Dupeyrat, C. Carbon Dioxide Reforming Of Methane Over La_2NiO_4 As Catalyst Precursor - Characterization Of Carbon Deposition. *Catal. Today* **2008**, 133–135, 200–209.

(20) Wender, I. Reactions Of Synthesis Gas. Fuel Process. Technol. 1996, 48, 189–297.

(21) Jager, B. Developments In Fischer-Tropsch Technology. Stud. Surf. Sci. Catal. 1997, 107, 219-224.

(22) Kühl, S.; Düdder, H.; Girgsdies, F.; Kähler, K.; Muhler, M.; Behrens, M. Perovskites As Precursors For Ni/La₂O₃ Catalysts In The Dry Reforming Of Methane: Synthesis By Constant pH Co-Precipitation, Reduction Mechanism And Effect Of Ru-Doping. Z. Anorg. Allg. Chem. **2017**, 643, 1088–1095.

(23) Moradi, G. R.; Khosravian, F.; Rahmanzadeh, M. Effects Of Partial Substitution Of Ni By Cu In LaNiO₃ Perovskite Catalyst For Dry Methane Reforming. *Chin. J. Catal.* **2012**, *33*, 797–801.

(24) Touahra, F.; Rabahi, A.; Chebout, R.; Boudjemaa, A.; Lerari, D.; Sehailia, M.; Halliche, D.; Bachari, K. Enhanced Catalytic Behaviour Of Surface Dispersed Nickel On LaCuO₃ Perovskite In The Production Of Syngas: An Expedient Approach To Carbon Resistance During CO_2 Reforming Of Methane. *Int. J. Hydrogen Energy* **2016**, *41*, 2477–2486.

(25) Wang, M.; Zhao, T.; Li, M.; Wang, H. Perovskite La₂(NiCu)O₄
Catalyst Precursors For Dry Reforming of Methane: Effects of Cu-Substitution On Carbon Resistance. RSC Adv. 2017, 7, 41847–41854.
(26) Fidalgo, B.; Menendez, A. Carbon Materials as Catalysts for Decomposition and CO₂ Reforming of Methane: A Review. Chin. J.

Catal. 2011, 32, 207–216. (27) Gili, A.; et al. Surface Carbon As A Reactive Intermediate In

Dry Reforming Of Methane To Syngas On A 5% Ni/MnO Catalyst. ACS Catal. 2018, 8, 8739-8750.

(28) Fierro, J. Surface Properties Of LaNiO₃: Kinetic Studies Of Reduction And Of Oxygen Adsorption. J. Catal. **1985**, *93*, 83–91.

(29) Sagar, T. V.; Padmakar, D.; Lingaiah, N.; Rama Rao, K. S.; Reddy, I. A. K.; Sai Prasad, P. S. Syngas Production By CO_2 Reforming of Methane On LaNi_xAl_{1-x}O₃ Perovskite Catalysts: Influence Of Method Of Preparation. *J. Chem. Sci.* **2017**, *129*, 1787–1794.

(30) Royer, S.; Duprez, D.; Can, F.; Courtois, X.; Batiot-Dupeyrat, C.; Laassiri, S.; Alamdari, H. Perovskites As Substitutes of Noble Metals for Heterogeneous Catalysis: Dream or Reality. *Chem. Rev.* **2014**, *114*, 10292–10368.

(31) Bonmassar, N.; Bekheet, M.; Schlicker, L.; Gili, A.; Gurlo, A.; Doran, A.; Gao, Y.; Heggen, M.; Bernardi, J.; Klötzer, B.; Penner, S. In Situ - Determined Catalytically Active State of LaNiO₃ in Methane Dry Reforming. *ACS Catal.* **2020**, *10*, 1102–1112.

(32) Köpfle, N.; Götsch, T.; Grünbacher, M.; Carbonio, E.; Hävecker, M.; Knop-Gericke, A.; Schlicker, L.; Doran, A.; Kober, D.; Gurlo, A.; Penner, S.; Klötzer, B. Zirconium-Assisted Activation of Palladium To Boost Syngas Production by Methane Dry Reforming. *Angew. Chem., Int. Ed.* **2018**, *57*, 14613–14618.

(33) Yao, Z.; Jiang, J.; Zhao, Y.; Luan, F.; Zhu, J.; Shi, Y.; Gao, H.; Wang, H. Insights Into The Deactivation Mechanism Of Metal Carbide Catalysts For Dry Reforming Of Methane Via Comparison Of Nickel-Modified Molybdenum And Tungsten Carbides. *RSC Adv.* **2016**, *6*, 19944–19951. (34) Bakiz, B.; Guinneton, F.; Arab, M.; Benlhachemi, A.; Villain, S.; Satre, P.; Gavarri, J.-R. Carbonatation And Decarbonatation Kinetics In The La₂O₃ - La₂O₂CO₃ System Under CO₂ Gas Flows. *Adv. Mater. Sci. Eng.* **2010**, *2*, 1–6.

(35) Dama, S.; Ghodke, S. R.; Bobade, R.; Gurav, H. R.; Chilukuri, S. Active And Durable Alkaline Earth Metal Substituted Perovskite Catalysts For Dry Reforming Of Methane. *Appl. Catal., B* **2018**, *224*, 146–158.

(36) Moradi, G. R.; Rahmanzadeh, R. The Influence Of Partial Substitution Of Alkaline Earth With La In The LaNiO₃ Perovskite Catalyst. *Catal. Commun.* **2012**, *26*, 169–172.

(37) Alvarez, J.; Valderrama, G.; Pietri, E.; Pérez-Zurita, M. J.; de Navarro, C.; Sousa-Aguiar, E. F.; Goldwasser, M. R. Ni–Nb-Based Mixed Oxides Precursors For The Dry Reforming Of Methane. *Top. Catal.* **2011**, *54*, 170–178.

(38) Bekheet, M. F.; Grünbacher, M.; Schlicker, L.; Gili, A.; Doran, A.; Epping, J. D.; Gurlo, A.; Klötzer, B.; Penner, S. On The Structural Stability Of Crystalline Ceria Phases In Undoped And Acceptor-Doped Ceria Materials Under In Situ Reduction Conditions. *CrystEngComm* **2019**, *21*, 145–154.

(39) Götsch, T.; Schlicker, L.; Bekheet, M. F.; Doran, A.; Grunbacher, M.; Praty, C.; Tada, M.; Matsui, H.; Ishiguro, N.; Gurlo, A.; Klotzer, B.; Penner, S. Structural Investigations Of $La_{0.6}Sr_{0.4}FeO_{3.\delta}$ Under Reducing Conditions: Kinetic And Thermodynamic Limitations For Phase Transformations And Iron Exsolution Phenomena. *RSC Adv.* **2018**, *8*, 3120–3131.

(40) Pechini, M.P. Method of preparing lead and alkaline earth titanates and niobates and coating method using the same to form a capacitor. US Patent No. 3,330,697, July 11, 1967.

(41) Doran, A.; Schlicker, L.; Beavers, C. M.; Bhat, S.; Bekheet, M. F.; Gurlo, A. Compact Low Power Infrared Tube Furnace For In Situ X-ray Powder Diffraction. *Rev. Sci. Instrum.* **2017**, *88*, 013903.

(42) Schlicker, L.; Doran, A.; Schneppmüller, P.; Gili, A.; Czasny, M.; Penner, S.; Gurlo, A. Transmission In Situ And Operando High Temperature X-ray Powder Diffraction In Variable Gaseous Environments. *Rev. Sci. Instrum.* **2018**, *89*, 033904.

(43) Rodriguez-Carvajal, J. Recent Developments Of The Program FULLPROF. *Newsletter of the Commission for Powder Diffraction of the IUCr* **2001**, *26*, 12–19.

(44) Finger, L. W.; Cox, D. E.; Jephcoat, A. P. A Correction for Powder Diffraction Peak Asymmetry Due to Axial Divergence. *J. Appl. Crystallogr.* **1994**, *27*, 892–900.

(45) Hill, R. J.; Howard, C. J. Quantitative Phase Analysis from Neutron Powder Diffraction Data Using the Rietveld Method. *J. Appl. Crystallogr.* **1987**, *20*, 467–476.

(46) Brindley, G. W. The Effect Of Grain Or Particle Size On X-Ray Reflections From Mixed Powders And Alloys, Considered In Relation To The Quantitative Determination Of Crystalline Substances By X-Ray Methods. *Philos. Mag.* **1945**, *36*, 347–369.

(47) Cliff, G.; Lorimer, G. W. The Quantitative Analysis Of Thin Specimens. J. Microsc. 1975, 103, 203–207.

(48) Thust, A.; Barthel, J.; Tillmann, K. FEI Titan 80–300 TEM. *Journal of Large-Scale Facilities* **2016**, *2*, A41.

(49) Heggen, M.; Luysberg, M.; Tillmann, K. FEI Titan 80–300 STEM. Journal of Large-Scale Facilities **2016**, *2*, A42.

(50) Schlesiger, C.; Anklamm, L.; Stiel, H.; Malzer, W.; Kanngießer, B. XAFS Spectroscopy By An X-Ray Tube Based Spectrometer Using A Novel Type Of HOPG Mosaic Crystal And Optimized Image Processing. J. Anal. At. Spectrom. **2015**, 30, 1080–1085.

(51) Schlesiger, C.; Praetz, S.; Gnewkow, R.; Malzer, W.; Kanngießer, B. Recent Progress In The Performance Of HAPG Based Laboratory EXAFS And XANES Spectrometers. J. Anal. At. Spectrom. 2020, 35, 2298.

(52) Ravel, B.; Newville, M. ATHENA, ARTEMIS, HEPHAESTUS: Data Analysis For X-Ray Absorption Spectroscopy Using IFEFFIT. J. Synchrotron Radiat. 2005, 12, 537–541.

(53) Tamura, H.; Hayashi, A.; Ueda, Y. Phase Diagram Of La₂NiO_{4+ δ} ($0 \le \delta \le 0.18$). *Phys. C* **1993**, 216, 83–88.

(54) Skinner, S. J. Characterisation Of La₂NiO_{4+ δ} Using In-Situ High Temperature Neutron Powder Diffraction. *Solid State Sci.* **2003**, 5 (3), 419–426.

(55) Aguadero, A.; Alonso, J. A.; Martinez-Lope, M. J.; Fernandez-Diaz, M. T.; Escudero, M. J.; Daza, L. In Situ High Temperature Neutron Powder Diffraction Study Of Oxygen-Rich La₂NiO_{4+ δ} In Air: Correlation With The Electrical Behaviour. *J. Mater. Chem.* **2006**, *16*, 3402–3408.

(56) Aguadero, A.; Alonso, J. A.; Escudero, M. J.; Daza, L. Evaluation Of The $La_2Ni_{1-x}Cu_xO_{4+\delta}$ System As SOFC Cathode Material With 8YSZ. And LSGM As Electrolytes. *Solid State Ionics* **2008**, *179*, 393–400.

(57) Tang, J. P.; Dass, R. I.; Manthiram, A. Comparison Of The Crystal Chemistry And Electrical Properties Of $La_{(2-x)}A_{(x)}NiO_{(4)}$ (A = Ca, Sr, and Ba). *Mater. Res. Bull.* **2000**, 35, 411–424.

(58) Shannon, R. D. Revised Effective Ionic-Radii and Systematic Studies of Interatomic Distances in Halides and Chalcogenides. Acta Crystallogr., Sect. A: Cryst. Phys., Diffr., Theor. Gen. Crystallogr. 1976, 32, 751–767.

(59) Vegard, L. Die Konstitution Der Mischkristalle Und Die Raumfüllung Der Atome. *Eur. Phys. J. A* **1921**, *5*, 17–26.

(60) Rameshan, R.; Mayr, L.; Klötzer, B.; Eder, D.; Knop-Gericke, A.; Hävecker, M.; Blume, R.; Schlögl, R.; Zemlyanov, D. Y.; Penner, S. Near-Ambient-Pressure X-ray Photoelectron Spectroscopy Study of Methane-Induced Carbon Deposition on Clean and Copper-Modified Polycrystalline Nickel Materials. *J. Phys. Chem. C* **2015**, *119*, 26948–26958.

(61) Fernandez-Diaz, M. T.; Martinez, J. L.; Rodriguez-Carvajal, J. High-Temperature Phase Transformation of Oxidized $R_2NiO_{4+\delta}$ (R = La, Pr, Nd) Under Vacuum. *Solid State Ionics* **1993**, 63–65, 902–906.

(62) Fleming, P.; Farrell, R. A.; Holmes, J. D.; Morris, M. A. The Rapid Formation Of $La(OH)_3$ From La_2O_3 Powders On Exposure To Water Vapor. J. Am. Ceram. Soc. **2010**, 93, 1187–1194.

(63) Wei, J.; Iglesia, E. Isotopic And Kinetic Assessment Of The Mechanism Of Reactions of CH_4 With CO_2 Or H_2O To Form Synthesis Gas And Carbon On Nickel Catalysts. J. Catal. 2004, 224, 370–383.

(64) Woolley, R. J.; Illy, B. N.; Ryan, M. P.; Skinner, S. J. In Situ Determination Of The Nickel Oxidation State In $La_2NiO_{4+\Delta}$ And $La_4Ni_3O_{10-\Delta}$ Using X-Ray Absorption Near-Edge Structure. *J. Mater. Chem.* **2011**, *21*, 18592–18596.

(65) Bekheet, M. F.; Dubrovinsky, L.; Gurlo, A. Compressibility And Structural Stability Of Spinel-Type Mnin₂o₄. *J. Solid State Chem.* **2015**, 230, 301–308.

(66) Bekheet, M. F.; Schlicker, L.; Doran, A.; Siemensmeyer, K.; Gurlo, A. Ferrimagnetism In Manganese-Rich Gallium And Aluminium Spinels Due To Mixed Valence Mn²⁺- Mn³⁺ States. *Dalton Trans.* **2018**, 47, 2727-2738.