



Methane Cracking over Cobalt Molybdenum Carbides

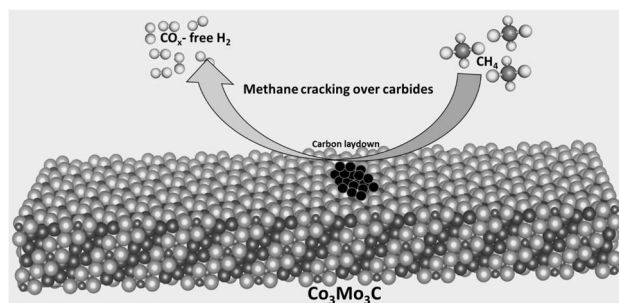
I. Alshibane¹ · S. Laassiri¹ · J. L. Rico² · J. S. J. Hargreaves¹

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Abstract

The catalytic behaviour of $\text{Co}_3\text{Mo}_3\text{C}$, $\text{Co}_6\text{Mo}_6\text{C}$, $\text{Co}_3\text{Mo}_3\text{N}$ and $\text{Co}_6\text{Mo}_6\text{N}$ for methane cracking has been studied to determine the relationship between the methane cracking activity and the chemical composition. The characterisation of post-reaction samples showed a complex phase composition with the presence of $\text{Co}_3\text{Mo}_3\text{C}$, $\alpha\text{-Co}$ and $\beta\text{-Mo}_2\text{C}$ as catalytic phases and the deposition of different forms of carbon during reaction.

Graphical Abstract



Keywords Methane cracking · Catalytic decomposition · Cobalt molybdenum carbide · Cobalt molybdenum nitride

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✉ J. S. J. Hargreaves
Justin.Hargreaves@glasgow.ac.uk
I. Alshibane
I.alshibane.1@research.gla.ac.uk
S. Laassiri
Said.Laassiri@glasgow.ac.uk
J. L. Rico
Jlceri@yahoo.com.mx

¹ WestCHEM, School of Chemistry, University of Glasgow, Joseph Black Building, Glasgow G12 8QQ, UK

² Laboratorio de Catálisis, Facultad de Ingeniería Química, Universidad Michoacana de San Nicolás de Hidalgo, Edif. V1, C.U., 58060 Morelia, Michoacán, Mexico

1 Introduction

The design of novel and efficient materials for catalytic reactions is of major interest. Although, many of the materials studied in heterogeneous catalysis are metal and metal oxide based, attention has been directed towards the development of entirely novel catalyst families that could display modified performance. Examples of the materials investigated include carbides, nitrides and boron alloys [1–3]. Amongst these materials, carbides have arguably received the most attention due to the perceived analogies between their behaviour and that of precious metals, suggesting them to be potential replacements. In this context, the presence of interstitial carbon species has been argued to modify the electronic properties of the parent metal in systems such as those based upon molybdenum or tungsten, making them akin to precious metals such as platinum [4, 5].

Within the literature, metal carbides are known to possess activity for a wide range of applications including

Fischer–Tropsch processes [6–8], hydrogenation [9–11], dehydroaromatisation [12], oxygen and hydrogen evolution [13] and ammonia decomposition [14, 15]. In more recent work, the reactivity of cobalt molybdenum carbide was studied for ammonia synthesis to gain an enhanced understanding of the potential role of lattice composition (i.e. the influence of the presence of interstitial carbon versus interstitial nitrogen) upon catalytic activity [16]. Although $\text{Co}_3\text{Mo}_3\text{C}$ was found to be active for ammonia synthesis, the material was only active at higher temperature (500 °C) compared to its nitride counterpart which is active at 400 °C, and such activity was associated with the presence of some lattice nitrogen residing in 16c Wyckoff sites as determined from in-situ neutron diffraction studies.

In the current manuscript, comparison is made between the performance of $\text{Co}_3\text{Mo}_3\text{C}$ and $\text{Co}_6\text{Mo}_6\text{C}$ for methane cracking to determine the role of stoichiometry and such performance is contrasted with their isostructural nitride counterparts. The methane cracking reaction is of potential interest as an environmentally friendly approach for CO_x -free hydrogen production [17–19].

2 Experimental

2.1 Materials Preparation

The preparation of cobalt molybdenum related materials has been documented in detail in our previous work [16, 20]. In a typical synthesis, CoMoO_4 was prepared by adding 5.59 g of $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ (> 98%, Sigma-Aldrich) and 4.00 g of $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24} \cdot 4\text{H}_2\text{O}$ (99.98%, Sigma-Aldrich) dissolved in 200 mL of deionized water. The solution was then heated to 85 °C and held at this temperature for 5 h. The resulting purple precipitate was filtered and washed with deionized water and ethanol. The precipitate was then calcined in static air at 500 °C for 5 h to obtain dehydrated cobalt molybdate. $\text{Co}_3\text{Mo}_3\text{N}$ was prepared by ammonolysis of CoMoO_4 under NH_3 (BOC, 99.98%) at a flow rate of 100 mL min^{-1} at 785 °C for 5 h. The temperature was increased from ambient to 357 °C at 5.6 °C min^{-1} , then after to 447 °C min^{-1} at 0.2 °C min^{-1} before being finally increased to 785 °C at 2.1 °C min^{-1} . $\text{Co}_3\text{Mo}_3\text{C}$ was prepared by the carburization of $\text{Co}_3\text{Mo}_3\text{N}$ under 20 vol% CH_4 in H_2 (BOC, 99.98%) at a flow rate of 12 mL min^{-1} at 700 °C for 2 h with a ramp rate of 6 °C min^{-1} to reach 350 °C followed by 1 °C min^{-1} to attain 700 °C. $\text{Co}_6\text{Mo}_6\text{C}$ was prepared by reducing $\text{Co}_3\text{Mo}_3\text{C}$ at 900 °C for 5 h under 60 mL min^{-1} of a 75 vol% H_2 in Ar (BOC, 99.98%) gas mixture.

2.2 Materials Characterization

X-ray diffraction patterns were collected on a Panalytical X'Pert PRO instrument, using Cu $\text{K}\alpha$ radiation ($\lambda = 0.154$ nm) over a 2θ range of 5°–85°, a step size of 0.0167°, and a counting time of 1 s per step. Samples were prepared by compaction into a Si sample holder. Phase identification was obtained by comparison with JCPDS database files. The surface areas of the samples were determined by application of the BET method to N_2 physisorption isotherms collected at –196 °C upon samples previously degassed at 110 °C under vacuum for 12 h. Scanning electron microscopy was performed on Philips XLSEM and FEI Quanta 200F Environmental instruments operating at 20 kV for the investigation of morphology. Samples were coated with an Au/Pd alloy prior to imaging. CHN analysis was undertaken by combustion using an Exeter Analytical CE-440 Elemental Analyzer. Thermogravimetric analysis (TGA) was carried out using a TA instruments QA instrument with measurements being undertaken in temperature range from room temperature to 1000 °C (ramp rate 10 degrees per minute) under a flow rate of 50 mL min^{-1} of air. Raman spectra of the samples were recorded at room temperature on a Horiba Jobin Yvon LabRam HR confocal Raman microscope, using a laser excitation of 523 nm.

2.3 Catalytic Activity Tests

Methane cracking reactions were performed using 0.2 g of material which was placed in a quartz tube reactor under a gas feed of 12 mL min^{-1} of a mixture of 75 vol% CH_4 in N_2 (BOC, 99.98%) at 800 °C for 8 h on stream. Hydrogen production was monitored by online gas chromatography (GC) using a TCD with Ar as carrier gas and employing a Molecular Sieve 13 \times column. The gas exhaust was also analysed in a periodic manner for the determination of CO_x by off-line FTIR analyses employing a gas-phase FTIR cell which could be isolated and by-passed for off-line analyses. FTIR spectra were recorded using a FTIR-8400S, Shimadzu apparatus. Each spectrum was collected at a spectral resolution of 2 cm^{-1} , applying a scan range of 500–3500 cm^{-1} .

3 Results

The structural and textural properties of the cobalt molybdenum based materials following the different nitridation and carburisation processes were monitored using a range of techniques. The results of the structural characterisation by XRD have been reported previously [16]. Powder XRD and neutron diffraction studies have confirmed the formation of

high quality pure phases of $\text{Co}_3\text{Mo}_3\text{C}$, $\text{Co}_6\text{Mo}_6\text{C}$, $\text{Co}_3\text{Mo}_3\text{N}$ and $\text{Co}_6\text{Mo}_6\text{N}$. These results can be found in the Supplementary Information (Figs. S1, S2).

Raman spectra of the pre-reaction cobalt molybdenum materials are presented in Fig. 1. The Raman bands at 354, 806, 866, 930 and 941 cm^{-1} are consistent with the presence of a surface cobalt molybdate phase [21] as might

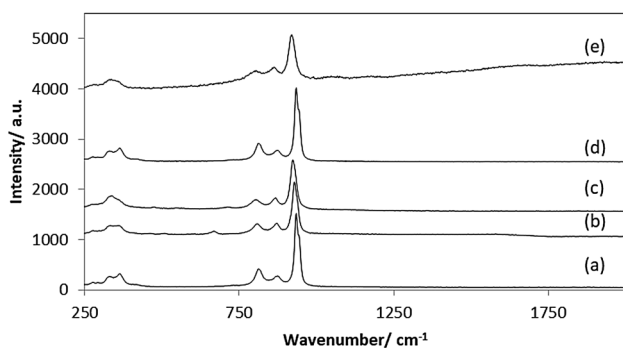
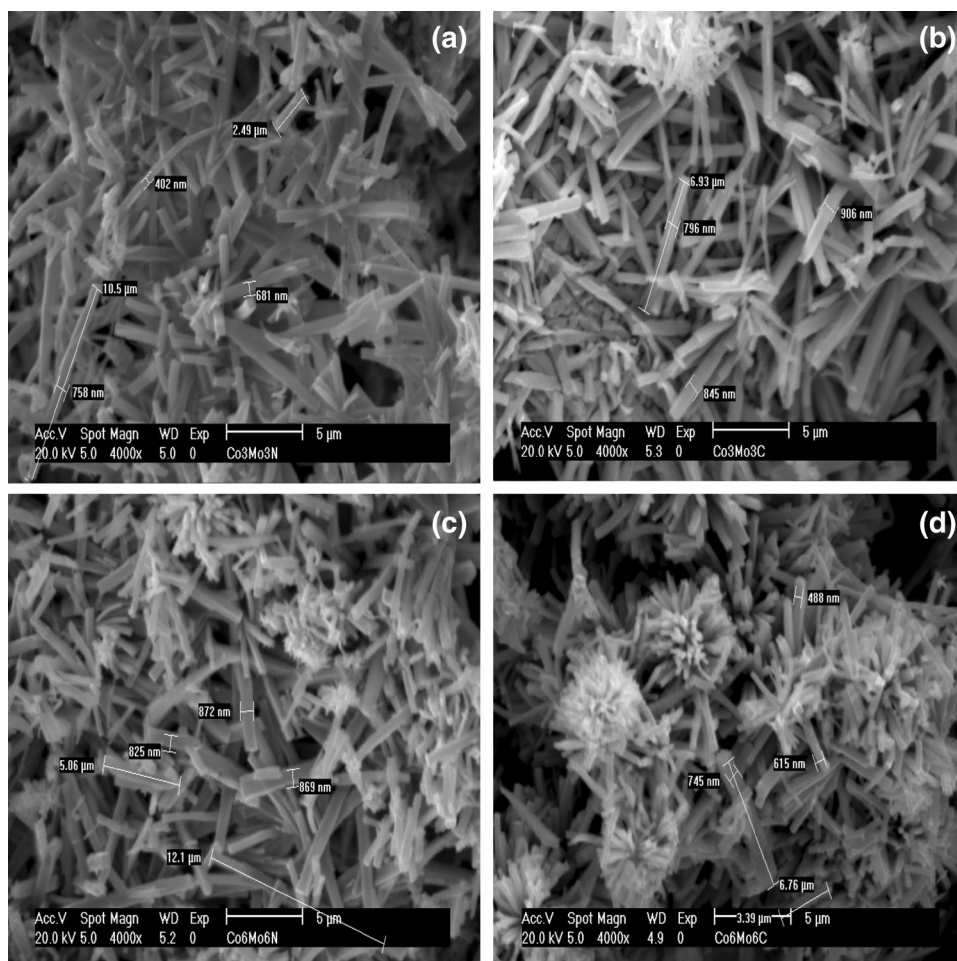


Fig. 1 Raman spectra of as prepared materials (a) CoMoO_4 , (b) $\text{Co}_3\text{Mo}_3\text{N}$, (c) $\text{Co}_3\text{Mo}_3\text{C}$, (d) $\text{Co}_6\text{Mo}_6\text{N}$ and (e) $\text{Co}_6\text{Mo}_6\text{C}$

Fig. 2 SEM images of as prepared materials: **a** $\text{Co}_3\text{Mo}_3\text{N}$, **b** $\text{Co}_3\text{Mo}_3\text{C}$, **c** $\text{Co}_6\text{Mo}_6\text{N}$ and **d** $\text{Co}_6\text{Mo}_6\text{C}$



be expected resulting from the presence of a surface passivation layer [22] for the carbide and nitride materials, which are known to be air-sensitive. Importantly, no Raman bands related to carbon deposition during the synthesis of $\text{Co}_3\text{Mo}_3\text{C}$ and $\text{Co}_6\text{Mo}_6\text{C}$ samples were observed which is consistent with the preparation of non-coked materials.

The SEM images presented in Fig. 2 demonstrate that all the materials prepared are pseudomorphic and exhibit a needle-like morphology as reported elsewhere [16]. The surface areas of the materials were determined to be 7, 18, 4 and 13 $\text{m}^2 \text{g}^{-1}$ for CoMoO_4 , $\text{Co}_3\text{Mo}_3\text{N}$, $\text{Co}_6\text{Mo}_6\text{N}$ and $\text{Co}_3\text{Mo}_3\text{C}$ respectively (Table 1). The lower surface area of the $\text{Co}_6\text{Mo}_6\text{C}$ phase ($\sim 3 \text{m}^2 \text{g}^{-1}$), can be attributed to the higher reaction temperature applied in its preparation.

The role of the nature of the stoichiometry and also the interstitial element present in the catalytic methane cracking activity of cobalt molybdenum materials was investigated by comparing the activity of the $\text{Co}_3\text{Mo}_3\text{C}$ and $\text{Co}_6\text{Mo}_6\text{C}$ to $\text{Co}_3\text{Mo}_3\text{N}$ and $\text{Co}_6\text{Mo}_6\text{N}$ materials. The reaction profiles illustrating the evolution of the mass normalised hydrogen formation rate as a function of time on stream is presented Fig. 3. Although, all materials displayed activity

Table 1 Summary of the textural and structural characterisation of post-reaction catalysts

| | Post-reaction XRD phase | Nitrogen content ^a /wt% | | Carbon content ^a /wt% | | S _{BET} ^b /m ² g ⁻¹ | |
|-----------------------------------|--|------------------------------------|---------------|----------------------------------|---------------|---|---------------|
| | | As-prepared | Post-reaction | As-prepared | Post-reaction | As prepared | Post-reaction |
| CoMoO ₄ | Graphite (003-0401), β-Mo ₂ C (001-1188), α-Co (01-089-7093) | – | N.d. | – | 71 ± 1 | 7 | 31 |
| Co ₃ Mo ₃ N | Co ₃ Mo ₃ C (03-065-7128), graphite (003-0401), β-Mo ₂ C (001-1188), α-Co (01-089-7093) | 3.0 ± 0.1 N | N.d. | – | 85 ± 3 | 18 | 63 |
| Co ₃ Mo ₃ C | Co ₃ Mo ₃ C (03-065-7128), graphite (003-0401), β-Mo ₂ C (001-1188), α-Co (01-089-7093) | – | N.d. | 2.5 ± 0.1 | 84 ± 1 | 13 | 50 |
| Co ₆ Mo ₆ N | Co ₃ Mo ₃ C (03-065-7128), graphite (003-0401), β-Mo ₂ C (001-1188), α-Co (01-089-7093) | 1.6 ± 0.1 N | N.d. | – | 84 ± 1 | 4 | 59 |
| Co ₆ Mo ₆ C | Co ₃ Mo ₃ C (03-065-7128), graphite (003-0401) | – | N.d. | 1.3 ± 0.1 | 69 ± 1 | 3 | 24 |

N.d. not detected

^aNitrogen analysis undertaken using an Exeter Analytical CE-440 Elemental Analyser

^bS_{BET} is the specific surface area evaluated using the BET model

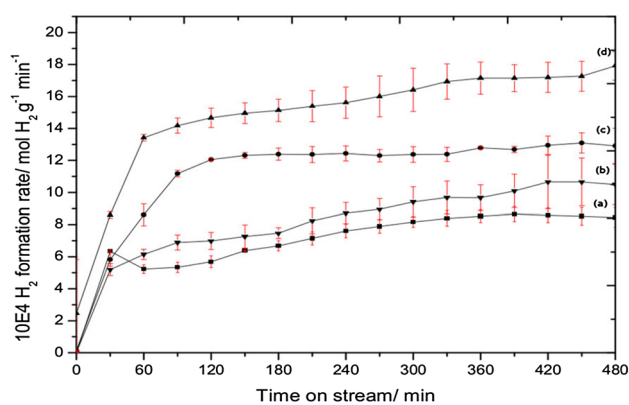


Fig. 3 Hydrogen formation rates as a function of time on stream for methane cracking over (a) CoMoO₄, (b) Co₆Mo₆C, (c) Co₃Mo₃N and (d) Co₆Mo₆N at 800 °C

for hydrogen production, clear differences in the hydrogen formation rates are observed. Hydrogen production tended to reach a plateau after 120 min on stream. However, in the case of the Co₃Mo₃C sample, less reproducible behaviour occurred, which was possibly related to carbon build-up during the reaction resulting in reactor blockage. Similar observations were witnessed upon repeating the experiment and the structural and textural properties of the post-reaction samples were all similar (Fig. S3). Due to the fact that the performance of Co₃Mo₃C is less reproducible, its reaction profile is not presented in Fig. 3 but is instead shown in Fig. S2.

In the presence of N₂ and H₂, as is the case in this study, Co₃Mo₃N and Co₃Mo₃C have been reported to be active catalytic systems for ammonia generation at ambient pressure

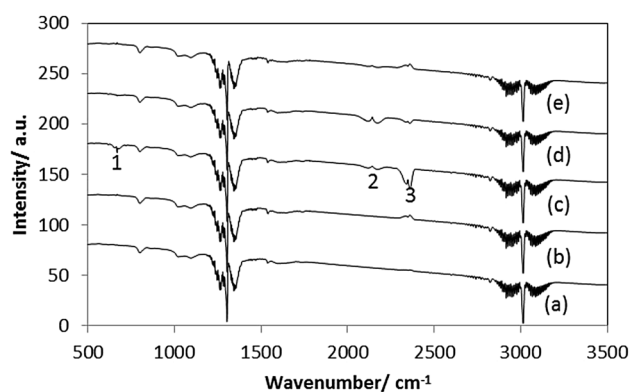


Fig. 4 FTIR analyses of gas-phase products from CoMoO₄ reacted with CH₄/N₂ (a) the feed gas, (b) 800 °C, (c) 800 °C 20 min, (d) 800 °C 50 min, and (e) 800 °C 60 min. Bands 1 and 3 are related to gas-phase CO₂ whereas band 2 is related to gas-phase CO

[16]. However, the reaction is thermodynamically unfavourable at high temperature and ammonia content at equilibrium is ~0.001 mol% at ca. 800 °C. Thus, the consumption of hydrogen to generate ammonia by reaction with the N₂ internal standard within the methane feed under these conditions can be safely ruled out.

In the case of cobalt molybdenum nitride and carbides, off-line FTIR spectra recorded periodically during reaction showed that the production of CO and CO₂ during methane cracking was below the detection limit. However, as might be expected, CO and CO₂ were clearly observed when CoMoO₄ was used as a catalyst (Fig. 4). FTIR analysis of gas products from this sample shows after 20 min of reaction, bands at 660 and 2360 cm⁻¹ which can be related to

CO_2 and at 2177 cm^{-1} which is assigned to CO. However, the production of CO and CO_2 ceased after 50 min of reaction. It is noteworthy that the production of CO, even in small concentrations, can be harmful in the case of some

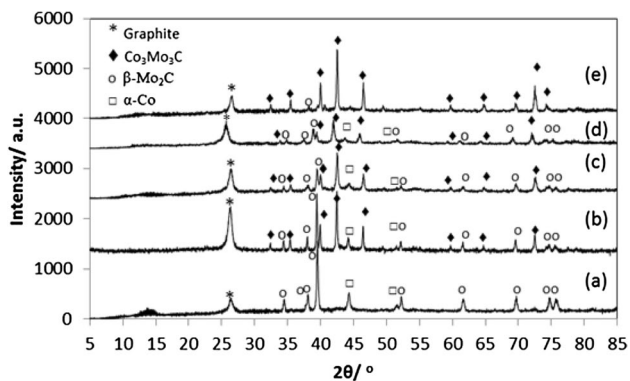
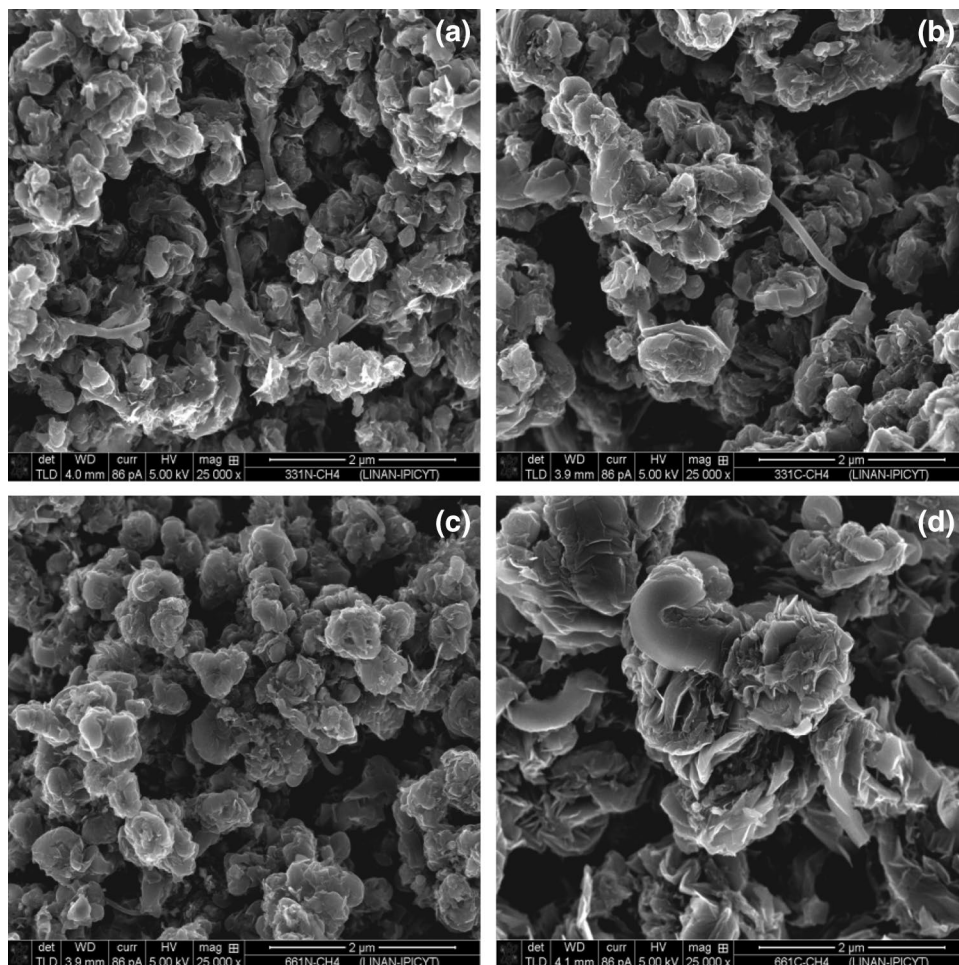


Fig. 5 Powder X-ray diffraction patterns of the post-reaction: (a) CoMoO_4 , (b) $\text{Co}_3\text{Mo}_3\text{N}$, (c) $\text{Co}_3\text{Mo}_3\text{C}$, (d) $\text{Co}_6\text{Mo}_6\text{N}$ and (e) $\text{Co}_6\text{Mo}_6\text{C}$ materials. Diamond: $\text{Co}_3\text{Mo}_3\text{C}$ (03-065-7128), asterisk: graphite (003-0401), open circle: $\beta\text{-Mo}_2\text{C}$ (001-1188), open square: $\alpha\text{-Co}$ (01-089-7093)

Fig. 6 SEM post-reaction images of: **a** $\text{Co}_3\text{Mo}_3\text{N}$, **b** $\text{Co}_3\text{Mo}_3\text{C}$, **c** $\text{Co}_6\text{Mo}_6\text{N}$ and **d** $\text{Co}_6\text{Mo}_6\text{C}$



downstream applications such as the use of H_2 in PEM fuel cells [23, 24]. The results presented herein suggest, beyond the initial loss of the surface passivation layer upon reaction, the use of cobalt molybdenum nitrides or carbides might be suitable for the production of CO_x -free hydrogen from methane cracking for such applications.

The characterisation of the post-reaction materials is presented in Figs. 5, 6, 7, 8 and 9 and in Table 1. Figure 5 presents the post-reaction powder XRD patterns. The XRD results are consistent with the formation of graphite as expected. In addition, a number of significant phase transformations to the original materials have occurred upon reaction (Fig. 5; Table 1). In most cases, $\text{Co}_3\text{Mo}_3\text{C}$ appeared to be the predominant phase, although the formation of some $\beta\text{-Mo}_2\text{C}$ and $\alpha\text{-Co}$ is also apparent. However, interestingly, in the case of CoMoO_4 , only $\beta\text{-Mo}_2\text{C}$, $\alpha\text{-Co}$ and graphite were evident after reaction with the ternary carbide phase being absent.

As shown in Fig. 6, morphological changes also occurred upon reaction. The agglomerated needle-like morphology was transformed to agglomerated block like structures. In contrast, post-reaction $\text{Co}_6\text{Mo}_6\text{C}$ appeared to

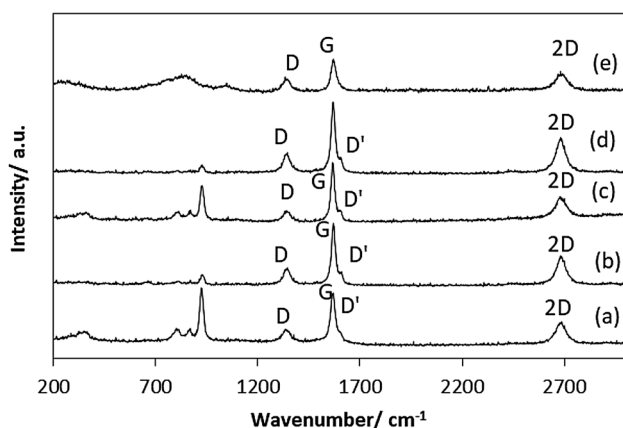


Fig. 7 Raman spectra of the post-reaction materials (a) CoMoO_4 , (b) $\text{Co}_3\text{Mo}_3\text{N}$, (c) $\text{Co}_3\text{Mo}_3\text{C}$, (d) $\text{Co}_6\text{Mo}_6\text{N}$ and (e) $\text{Co}_6\text{Mo}_6\text{C}$

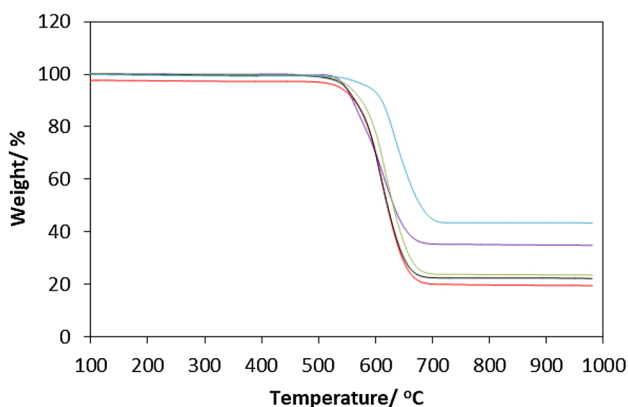


Fig. 8 TGA traces under air for post-reaction materials: (purple) CoMoO_4 , (red) $\text{Co}_3\text{Mo}_3\text{N}$, (green) $\text{Co}_3\text{Mo}_3\text{C}$, (black) $\text{Co}_6\text{Mo}_6\text{N}$ and (blue) $\text{Co}_6\text{Mo}_6\text{C}$

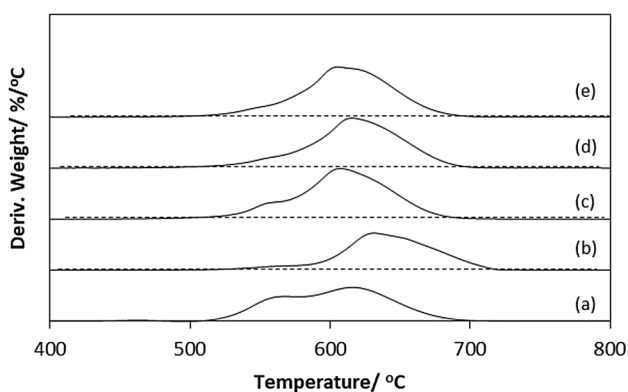


Fig. 9 Derivative weight curves for post-reaction materials under air (a) CoMoO_4 , (b) $\text{Co}_3\text{Mo}_3\text{N}$, (c) $\text{Co}_3\text{Mo}_3\text{C}$, (d) $\text{Co}_6\text{Mo}_6\text{N}$ and (e) $\text{Co}_6\text{Mo}_6\text{C}$

exhibit larger particle sizes compared to its post-reaction $\text{Co}_3\text{Mo}_3\text{N}$, $\text{Co}_3\text{Mo}_3\text{C}$ and $\text{Co}_6\text{Mo}_6\text{N}$ counterparts within the statistical limitations of the observations made. It is also interesting to note that in general, post-reaction catalyst displayed a higher surface area than pre-reaction materials. Both the drastic change in morphology and the enhanced surface area can be, at least partly, attributed to the significant deposition of carbon as a result of reaction. The comparatively lower surface area evident in the case of $\text{Co}_6\text{Mo}_6\text{C}$ is in accordance with the large particle size observed for this sample by SEM.

The CoMoO_4 and $\text{Co}_6\text{Mo}_6\text{C}$ post-reaction samples were found to contain ~ 70 wt% C (Table 1), with a higher post-reaction carbon content (~ 84 wt% C) evident for $\text{Co}_3\text{Mo}_3\text{C}$, $\text{Co}_3\text{Mo}_3\text{N}$ and $\text{Co}_6\text{Mo}_6\text{N}$ as would be anticipated from their higher hydrogen formation rates. The nature of the carbonaceous species deposited was characterized by Raman spectroscopy. Post-reaction Raman spectra, presented in Fig. 7, provide strong evidence of the presence of disordered and graphitic carbon with Raman bands observed at 1350 and 1582 cm^{-1} labelled (D) and (G) respectively [25]. An additional band, of lower intensity, at 1620 cm^{-1} labelled as D' was observed for the $\text{Co}_3\text{Mo}_3\text{N}$, $\text{Co}_3\text{Mo}_3\text{C}$ and $\text{Co}_6\text{Mo}_6\text{N}$ samples. In the literature, several explanations exist and the additional band can be correlated in principle to the presence of a high concentration of defects [26–28]. Additional Raman bands related to cobalt molybdate were detected in the post-reaction CoMoO_4 and post-reaction $\text{Co}_3\text{Mo}_3\text{C}$.

To further characterise the nature of the carbon deposit after reaction, TGA in air was carried out over the temperature range 100–1000 °C (Fig. 8). It was observed that the carbon oxidation started for all materials from 500 °C and was complete by 700 °C. Beyond, this point no further change in the weight of the material was observed. The total weight loss was between 60 and 80 wt% which accords well with the results of post-reaction elemental analysis (Table 1). The first derivative profiles for the different post-reaction materials are presented in Fig. 9. In all materials, two weight loss regions have been observed. The first weight loss peak is observed in the temperature range between 500 and 600 °C while the second weight loss peak is observed at higher temperatures (600–700 °C). The contribution of the first peak was particularly significant in the post-reaction CoMoO_4 material and to some extent in the $\text{Co}_3\text{Mo}_3\text{C}$. However, the oxidation of carbon in $\text{Co}_3\text{Mo}_3\text{N}$, $\text{Co}_6\text{Mo}_6\text{N}$ and $\text{Co}_6\text{Mo}_6\text{C}$ materials occurred mainly at temperature ranging between 600 and 700 °C. The contrast between the two oxidation regions could suggest the presence of two forms of carbon. However, the presence of the oxide phase, as evidenced in their Raman spectra, in the case of post-reaction CoMoO_4 and post-reaction $\text{Co}_3\text{Mo}_3\text{C}$ as observed by Raman spectra (Fig. 7) may have enhanced the oxidation of carbon at low temperature.

4 Discussion

The topotactic transformation pathways and pseudomorphic nature of the cobalt molybdenum carbide and nitride families evident in this study offers, in principle, an elegant route to study the effect of interstitial carbon/nitrogen on the catalytic activity of cobalt molybdenum materials for methane cracking. All the prepared materials possess activity for hydrogen production at 800 °C. Interestingly, the catalytic activity of these materials varied depending upon initial composition with $\text{Co}_6\text{Mo}_6\text{N}$ being the most active (Fig. 3). The activity of the material was found to stabilise around $1.8 \text{ mmol H}_2 \text{ g}_{\text{catalyst}}^{-1} \text{ min}^{-1}$, which is high when compared against the activity of some other nitride systems (e.g. $180 \mu\text{mol H}_2 \text{ g}_{\text{catalyst}}^{-1} \text{ min}$ reported for a silicon-vanadium nitride nanocomposite under directly comparable conditions) [29]. In fact, the activity of the $\text{Co}_6\text{Mo}_6\text{N}$ is directly comparable to the activity of iron oxide (for which a rate of $1 \text{ mmol H}_2 \text{ g}_{\text{catalyst}}^{-1} \text{ min}^{-1}$ was previously reported for iron oxide under the same reaction conditions) [30]. In general, the activity of the carbides and nitrides presented a normalised hydrogen production rate ranging from 1.1 to $1.8 \text{ mmol H}_2 \text{ g}_{\text{catalyst}}^{-1} \text{ min}^{-1}$. A slightly lower activity ($0.8 \text{ mmol H}_2 \text{ g}_{\text{catalyst}}^{-1} \text{ min}^{-1}$) was found for the CoMoO_4 system. In addition to the relatively enhanced activity of the cobalt molybdenum carbide and nitride systems when compared to the oxide counterpart, the absence of significant production of CO_x , beyond that which might be expected from conversion of the surface passivation layer, during the methane cracking reaction is of potential interest in relation to free of $\text{CO}_x\text{-H}_2$ production.

As expected, the production of H_2 was accompanied by carbon deposition. Due to the nature of the reaction, the amount of carbon deposited on carbide and nitride systems can be correlated directly to the activity of methane cracking as expected. Elemental analysis showed significant deposition of carbon $\sim 85 \text{ wt\%}$ on $\text{Co}_3\text{Mo}_3\text{N}$, $\text{Co}_3\text{Mo}_3\text{C}$ and $\text{Co}_6\text{Mo}_6\text{N}$ confirming the high activity of these materials, in spite of the less reproducible hydrogen production behaviour of $\text{Co}_3\text{Mo}_3\text{C}$. Thermogravimetric analyses conducted under air confirmed that the weight loss associated with carbon oxidation to be consistent with the elemental analyses of post-reaction materials. The nature of the carbon present upon reaction has been investigated by Raman spectroscopy (Fig. 7). The Raman features were dominated by the presence of two forms of carbon: disordered and graphitic carbon. The existence of several forms of carbon was also evident from the derivative weight curves for post-reaction samples.

While it is tempting to discuss the activity of the catalysts against their initial composition, post-reaction

analysis revealed changes in the structural properties upon reaction. As might be expected under the reaction conditions applied, post-reaction powder XRD (Fig. 5), showed the carburisation of all the materials studied when reacted. However, the products of carburisation slightly differ depending on the initial composition. In the post-reaction CoMoO_4 , only $\beta\text{-Mo}_2\text{C}$ (001-1188) and $\alpha\text{-Co}$ (01-089-7093) are observed as a result of the carburisation of CoMoO_4 as well as graphite generated from methane cracking. However, a mixture of $\text{Co}_3\text{Mo}_3\text{C}$ (03-065-7128), $\alpha\text{-Co}$ (01-089-7093) and $\beta\text{-Mo}_2\text{C}$ (001-1188) is detected upon reaction of $\text{Co}_3\text{Mo}_3\text{N}$, $\text{Co}_3\text{Mo}_3\text{C}$ and $\text{Co}_6\text{Mo}_6\text{N}$ with methane. In the case of $\text{Co}_6\text{Mo}_6\text{C}$ relocation of the carbon located in the 8a (0 0 0) Wyckoff site to the 16c (1/8 1/8 1/8) site occurs associated with the formation of $\text{Co}_3\text{Mo}_3\text{C}$ without clear evidence of the formation of $\beta\text{-Mo}_2\text{C}$ and $\alpha\text{-Co}$ [01-089-7093 (001-1188)] phases as observed in the previous cases.

In summary, for the three most active catalysts, the phases detected after reaction comprised a mixture of $\text{Co}_3\text{Mo}_3\text{C}$ (03-065-7128), $\alpha\text{-Co}$ (01-089-7093) and $\beta\text{-Mo}_2\text{C}$ (001-1188). While, for the least active material CoMoO_4 , only the $\beta\text{-Mo}_2\text{C}$ and $\alpha\text{-Co}$ (01-089-7093) were detected. Another major aspect, where differences are potentially evident, is the accessible surface area of the active phases. The surface area measured in post-reaction $\text{Co}_3\text{Mo}_3\text{N}$, $\text{Co}_3\text{Mo}_3\text{C}$ and $\text{Co}_6\text{Mo}_6\text{N}$ samples ranged between 50 and $63 \text{ m}^2 \text{ g}^{-1}$ while in the case of CoMoO_4 and $\text{Co}_6\text{Mo}_6\text{C}$ the surface area was limited to $\sim 30 \text{ m}^2 \text{ g}^{-1}$. Despite the fact that no simple link can be established between the catalytic activity to phase composition and accessible surface area, it can be argued that the presence of $\text{Co}_3\text{Mo}_3\text{C}$, $\alpha\text{-Co}$ and $\beta\text{-Mo}_2\text{C}$ and high surface area leads to an enhanced activity for methane cracking. In addition, the initial composition seems to play an important role in the final activity of the catalysts. These differences may indicate differences in the active surface composition resulting from the carburisation process of different cobalt molybdenum precursors. Further characterisation of the carburisation process of cobalt molybdenum materials by in-situ neutron diffraction, in condition of relevance to this study, are currently under investigation and will bring new insight to the process. Elsewhere, cobalt-molybdenum oxy-carbide surface phases have been proposed to be of importance for activity and lifetime [31].

5 Conclusion

A range of cobalt molybdenum containing materials have been prepared and tested as catalysts for the production of hydrogen from methane at 800 °C. After a short induction period, all samples were active and stable for the generation of hydrogen over the period tested, with the exception of

$\text{Co}_3\text{Mo}_3\text{C}$. Amongst the evaluated materials, the $\text{Co}_6\text{Mo}_6\text{N}$ sample showed the highest activity of about $1.8 \text{ mmol H}_2 \text{ g}^{-1} \text{ min}^{-1}$, comparable to those observed for iron oxide systems under similar reaction conditions. The results revealed that a significant phase transformation from metal nitrides to $\text{Co}_3\text{Mo}_3\text{C}$ and $\beta\text{-Mo}_2\text{C}$ occurred throughout the methane cracking reaction. Interestingly, in the case of $\text{Co}_6\text{Mo}_6\text{C}$ relocation of the carbon located in the 0 0 0 (8a) site to $1/8 \ 1/8 \ 1/8$ (16c) sites resulting in the formation of $\text{Co}_3\text{Mo}_3\text{C}$ was observed. Furthermore, results from Raman spectroscopy and powder XRD show that at least two forms of carbon are formed on the catalyst surface during methane decomposition.

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Compliance with Ethical Standards

Conflict of interest The authors declare no conflict of interest.

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