



## Research article

# Efficient removal of oxytetracycline antibiotic from aqueous media using UV/g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> photocatalytic process

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## ABSTRACT

Residual pharmaceuticals in the environment are a class of emerging pollutants that endanger human health. Tetracycline's family, including oxytetracycline (OTC), are known as one of the most produced and consumed antibiotics worldwide. The g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> nanocomposite with high level of catalytic efficiency features suitable performance in water/wastewater treatment. Therefore, in the present study, this nanocomposite was applied to remove the oxytetracycline from the aqueous environment. In this research study, g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> nanocomposite (serving as catalyst) was initially synthesized by a simple hydrothermal method. The effect of key operating parameters such as initial solution pH, dose of catalyst, contact time and initial concentration of OTC in aqueous solutions was investigated under UV irradiation. In addition, COD and TOC tests, the kinetics and the effect of radical scavengers on the applied photocatalytic process were all evaluated. The maximum removal efficiency of OTC (99.8 %) was achieved under the following conditions: neutral solution pH 7; catalyst dose, 0.7 g/L; and an initial OTC concentration of 5 mg/L. The data showed that the kinetics of the reaction followed the first-order model with R<sup>2</sup> of 0.9755. The respective COD and TOC efficiency values for the applied photocatalytic process were determined to be 87 and 59 %, respectively. In addition, the lowest removal efficiency of OTC was observed in the presence of tert-butanol radical scavengers, and OH radicals played a main role. The UV/g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> photocatalytic process proved to be highly efficient for the removal of OTC antibiotic and could be potentially applied for the removal of other pollutants from aqueous solutions.

## 1. Introduction

With no doubt, water remains the greatest asset for humans and other creatures to survive and continue life on the planet. Unfortunately, with increasing industrialization, rapid population growth, urbanization, and widespread agricultural activities, a sharp decline in quality of water resources is inevitable [1]. Water pollution poses a serious threat to human health, biodiversity and ecosystem stability, so that the quality of water resources has become a major concern for human beings [2].

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Antibiotics have revolutionized medicine in many ways and their discovery is regarded as a corner stone in history. Nevertheless, the excessive use of these drugs has been associated with the rapid emergence of resistant strains [3]. The presence of antibiotics and their transformation products in the environment result in the creation of antibiotic-resistant bacteria and antibiotic-resistant genes [4]. The World Health Organization (WHO) has acknowledged antibiotic resistance as one of the three most important threats to public health in the 21st century [5].

Amongst the antibiotic pollutants contaminating water sources, tetracycline's family are known as the second most produced and consumed antibiotics worldwide [6]. Of this family, oxytetracycline (OTC) is widely used as a prescribed treatment and growth stimulant in veterinary medicine, poultry farming and aquaculture due to its medicinal properties [7]. This antibiotic features a complex four-ring structure bearing a number of ionizable functional groups (see Fig. 1) [8].

OTC enters the surface and underground water through household and hospital sewage, livestock and aquaculture centers. It also enters the human body through drinking, eating fruits and vegetables. Even at very low concentration, its appearance at a high frequency can cause bacteria-resistance and promote the production of antibiotic-resistant genes [8,9].

Dissemination of antibiotics in natural waters is mainly performed in the effluents of municipal sewage treatment plants (STPs) and pharmaceutical factories. Current wastewater treatment technologies are not sufficiently capable of removing antibiotics, so updated, efficient and low-cost technologies are high on demand [10]. Various methods have been applied to remove antibiotics from water and wastewater sources. In a study by Trovó AG et al., they applied photo-Fenton process to degrade Chloramphenicol [11] and also Arefi-Oskoui S et al. implemented the membrane process for the removal of Rifampicin [12]. In addition, Renyong Geng et al. utilized adsorption process for the removal of several antibiotics namely, chlorhexidine acetate, minocycline, and erythrocin [13]. In a similar reported work, Hassan Mohamed NA applied the photocatalytic process for the degradation of some antibiotics namely, Ciprofloxacin, Ampicillin and Erythromycin [14]. Nevertheless, the main drawbacks associated with these above-mentioned methods are high level of energy consumption, high cost and low efficiency of mineralization [15]. Advanced oxidation processes (AOPs) featuring fast reaction rate and strong oxidation ability have received more attention than other methods used for the removal of antibiotics [16]. The photocatalytic process is categorized as one of the main advanced oxidation processes, in which a total mineralization of organic pollutants and their transformation into harmless and environmentally friendly products takes place. This process is on the basis of the reaction between organic pollutants and strong oxidation/reduction agents, which are generated by ultraviolet ray (UV) or visible light (Vis) on the surface of the catalysts [17].

In a heterogeneous photocatalytic process, a semiconductor material is employed with featuring a valence band ( $V_B$ ) of low energy and a conduction band ( $C_B$ ) of high energy. The distance between  $V_B$  and the  $C_B$  is recognized as the band gap of the semiconductor. It is clear cut that once the energy of radiation light is higher than the band gap of the semiconductor, the electrons in the  $V_B$  of the semiconductor are excited and transferred to the  $C_B$  and as a result the holes are created in the  $V_B$ . The generated electrons and holes ( $e^-/h^+$ , pairs) have strong oxidizing properties and are able to oxidize the potential pollutants adsorbed on the surface of semiconductor [18–21]. Recently, the graphite carbon nitride ( $g-C_3N_4$ )-based nanocomposites have been widely used for the photocatalytic degradation of various pollutants in water media.  $g-C_3N_4$  is an organic polymer semiconductor featuring the wonderful properties such as compatibility with the environment, high chemical stability and low cost. Nevertheless, it is associated with several drawbacks including the possibility of rapid recombination of electron/hole pairs and difficult separation throughout the reaction in aqueous media. To remedy, a new method based on the doping of a semiconductor with metallic and non-metallic elements have been introduced. For instance, the coupling of  $Fe_3O_4$  nanoparticles with  $g-C_3N_4$  sheets seems to a viable choice of interest. The results of various research studies have demonstrated that the photocatalytic process using the combined  $g-C_3N_4/Fe_3O_4$  nanocomposite is highly efficient for the degradation and removal of pollutants [22].

Therefore, in this study,  $g-C_3N_4/Fe_3O_4$  nanocomposite was synthesized and characterized to remove the well-known antibiotic of OTC from aqueous solutions, and the efficiency of the photocatalytic process was evaluated through the optimization of influential factors involved.  $g-C_3N_4/Fe_3O_4$  nanocomposite with high level of catalytic efficiency features suitable performance in water/

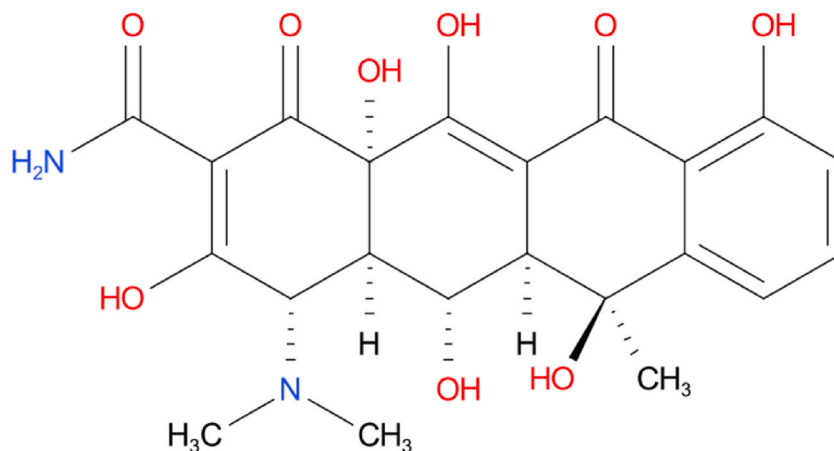


Fig. 1. Chemical structure of OTC.

wastewater treatment. Therefore, in the present study, this nanocomposite was applied as an efficient catalyst to remove OTC from the aqueous environment.

## 2. Methods and materials

### 2.1. Chemicals

The chemicals used in this study include OTC, melamine, ferric chloride hexahydrate, ferrous chloride tetrahydrate, ammonia, hydrochloric acid, sodium hydroxide, sulfuric acid, ethanol, and methanol, which were all purchased from Merck Company. In addition, distilled water was used throughout to prepare all aqueous solutions.

### 2.2. Preparation of nanocomposite

#### 2.2.1. Synthesis of g-C<sub>3</sub>N<sub>4</sub> powder

g-C<sub>3</sub>N<sub>4</sub> was produced by direct calcination of melamine at 550 °C in a furnace. For this purpose, 5 g of melamine powder was poured in a ceramic crucible and placed in an oven at 550 °C for 4 h, after that the prepared g-C<sub>3</sub>N<sub>4</sub> was cooled to room temperature.

#### 2.2.2. Preparation of Fe<sub>3</sub>O<sub>4</sub> nanoparticles

A modified co-precipitation method was implemented for the preparation of Fe<sub>3</sub>O<sub>4</sub> nanoparticles [23]. Briefly, 4.72 g FeCl<sub>3</sub>·6H<sub>2</sub>O and 1.72 g FeCl<sub>2</sub>·4H<sub>2</sub>O were thoroughly mingled and dissolved in distilled water (100 ml) followed by the basification with NH<sub>4</sub>OH (10 ml) The resulting mix was then vigorously mixed at 80 °C for 1 h. Finally, an external magnet was used to recover Fe<sub>3</sub>O<sub>4</sub> nanoparticles which further were washed with pure water and ethanol, and eventually dried at 60 °C.

#### 2.2.3. Preparation of g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> nanocomposite

Initially, 0.07 g of g-C<sub>3</sub>N<sub>4</sub> powder was weighed and added to 250 ml of 1:2 ethanol/water solution and the resulting suspension was placed in an ultrasound bath for 6 h. To the above suspension, 0.92 g of FeCl<sub>3</sub>·6H<sub>2</sub>O and 0.45 g of FeCl<sub>2</sub>·4H<sub>2</sub>O previously dissolved in 10 ml distilled water was added. The resulting mixture was stirred in at 80 °C for 30 min. Then, 10 ml of ammonia was added to the mixture while agitating for 30 min. The solution was then allowed to cool at ambient temperature. The obtained g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> nanocomposite was separated from the solution by a magnet and washed several times with ethanol and water. Finally, the nanocomposite was dried at 60 °C for further studies [24].

#### 2.2.4. Characteristics of g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> nanocomposite

Following the synthesis of g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> nanocomposite, its physiochemical properties were determined by a number of analytical instruments as follows: X-ray diffraction (XRD) analysis was applied to mainly determine the phases of the nanoparticles involved within 2θ of 10–80°. Field emission scanning electron microscopy (FE-SEM) was used to study the surface properties and morphology of the nanoparticles. Energy dispersive X-ray analysis (EDAX) was employed to identify the contribution of the elements within the structure of synthesized nanocomposite. In addition, Fourier transform infrared spectroscopy (FTIR) was used to identify the presence of main organic functional groups. UV–vis diffuse reflectance spectroscopy (DRS) spectra were obtained by a spectrophotometer. Finally, Vibrating-sample magnetometry (VSM) was used to verify the magnetic properties of the nanocomposite.

### 2.3. Photocatalytic degradation of OTC

The experiments with regard to photocatalytic degradation of OTC were carried out in a 2-L Pyrex reactor continuously agitated at ambient temperature. A UV-A lamp (15 W) was served as the radiation source. A mechanical stirrer was used to agitate the content of the reactor. A dilute solution of HCl/NaOH (0.1 M) was also used to adjust the pH of the aqueous sample solutions. It is noted that each experiment was repeated three times and the Excel software was used for the data analysis.

The variables studied in this research were optimized univariety. During each experiment, the sampling of the solutions was done at specific time intervals (5–120 min) and the nanocomposite catalyst was separated off the solution using a magnet and the remaining concentration of OTC was determined by a HPLC (Cecil 4100, England), with a C18 column (250 nm × 4.6 mm × 5 μm) at 354 nm. The following equation was used to calculate the removal efficiency of OTC (Eq. (1)).

$$\text{Removal (\%)} = \frac{(C_0 - C_t)}{C_0} \times 100 \quad (1)$$

Where respective C<sub>0</sub> and C<sub>t</sub> represent the initial and final concentration of OTC (mg/L).

The TOC values were measured by a total organic carbon analyzer (Multi N/C, TOC 3100 analyzer, Germany). The removal efficiency was calculated by the following equation (Eq. (2)):

$$\text{TOC Removal (\%)} = \frac{\text{TOC}_0 - \text{TOC}_t}{\text{TOC}_0} \times 100 \quad (2)$$

Where respective TOC<sub>0</sub> and TOC<sub>t</sub> represent the initial and final TOC values.

### 3. Results and discussion

#### 3.1. Characteristics of nanocomposite

In Fig. 2a, the XRD patterns of  $\text{Fe}_3\text{O}_4$ ,  $\text{g-C}_3\text{N}_4$  and  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  nanoparticles are presented.  $\text{g-C}_3\text{N}_4$  has two peaks at  $13.5$  and  $27.4^\circ$  corresponding to the tri-S-triazine unit with the file (JCPDS file number 87-15-26). The characteristic peaks within  $\text{Fe}_3\text{O}_4$  structure are observed at  $2\theta = 30.2^\circ, 35.6^\circ, 43.3^\circ, 53.7^\circ, 57.3^\circ,$  and  $62.8^\circ$ . These peaks are in line with the crystal planes of  $\text{Fe}_3\text{O}_4$  corresponding to the JCPDS data: 19-0629 [25,26]. As shown, the XRD pattern of  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  nanocomposite is composed of all the diffraction peaks belonging to  $\text{g-C}_3\text{N}_4$  and  $\text{Fe}_3\text{O}_4$ , implying that  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  was well synthesized.

In Fig. 2b, the FT-IR spectra of  $\text{Fe}_3\text{O}_4$ ,  $\text{g-C}_3\text{N}_4$  and  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  nanoparticles are demonstrated. In the  $\text{g-C}_3\text{N}_4$  structure, a sharp band at  $808\text{ cm}^{-1}$  is related to the vibrational bending of triazine rings. The absorption band located within the region of  $1200\text{--}1600\text{ cm}^{-1}$  is ascribed to the stretching mode of  $\text{C-N/C=N}$  belonging to the heterocyclic part of  $\text{g-C}_3\text{N}_4$ . The peaks at  $1241, 1318, 1425,$  and  $1635\text{ cm}^{-1}$  are assigned to the stretching mode of  $\text{C-N}$  aromatic rings. The respective broad adsorbed band at  $3100\text{--}3400\text{ cm}^{-1}$  could be related to the vibration mode of  $\text{N-H}$  and  $\text{O-H}$  bonds belonging to the free amino groups and adsorbed water molecules. In addition, the sharp band at  $600\text{--}900\text{ cm}^{-1}$  is highly likely attributed to  $\text{Fe-O}$  tensile vibration.

FE-SEM images of  $\text{g-C}_3\text{N}_4$  and  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  nanoparticles are depicted in Fig. 3. Within the Figure is vividly seen that  $\text{g-C}_3\text{N}_4$  is in sheet forms (Fig. 3(a and b)), while  $\text{Fe}_3\text{O}_4$  particles are coated on  $\text{g-C}_3\text{N}_4$  sheets (Fig. 3(c and d)).

EDAX patterns of  $\text{g-C}_3\text{N}_4$ ,  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  nanocomposite and the elemental mapping of  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  are also shown in Fig. 1s (a, b and c). Accordingly, the presence of carbon and nitrogen elements in  $\text{g-C}_3\text{N}_4$  structure and carbon, nitrogen, oxygen and iron elements within  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  nanocomposite are visibly seen. The elemental mappings of  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  nanocomposite (Fig. 1s(c)) reaffirmed the uniform arrangement of all elements involved, including C, N, O and Fe.

The DRS experimental test was employed to determine the properties with respect to the optics of the nanocomposite. Fig. 2S(a) shows the UV-vis DRS spectra of  $\text{g-C}_3\text{N}_4$ ,  $\text{Fe}_3\text{O}_4$  and  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  nanocomposites. Accordingly, the utmost absorption band was obtained within the UV region ( $300\text{--}350\text{ nm}$ ), which corresponds to the excitation band gap of the applied catalyst.

Meanwhile, the Kubelka-Munk function was used to estimate the band gap energy of the nanocomposites (Fig. 2S(b)) [27]. The respective band gap energies for  $\text{g-C}_3\text{N}_4$ ,  $\text{Fe}_3\text{O}_4$  and  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  nanocomposites were measured to be  $2.7, 2.23$  and  $1.7\text{ eV}$ . It can be deduced that the band gap of  $\text{g-C}_3\text{N}_4$  declined once it was integrated with  $\text{Fe}_3\text{O}_4$  nanoparticles. This leads to the promotion of the photocatalytic efficiency with regard to the  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  nanocomposite.

VSM analysis was performed to determine the magnetic properties of  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  nanocomposite. As it is clear in Fig. 4, due to the presence of magnetic particles of  $\text{Fe}_3\text{O}_4$  within the nanocomposite structure, a favorable magnetic property is associated with the catalyst.

In a further related identification analysis, the pHzpc of the nanocomposite was determined to be  $7.8$  (see Fig. 3s). It is clear cut that at this pH, the surface charge of the catalyst is zero and the catalyst remains neutral.

#### 3.2. Optimization of influential parameters

##### 3.2.1. Effect of pH

The effect of variations in the initial pH of the solution within the range of  $3\text{--}11$  containing the antibiotic OTC on the efficiency of the photocatalytic process is illustrated (see Fig. 5). As can be seen, the maximum removal rate of OTC was observed at  $\text{pH} = 7$  ( $89.3\%$ ). Therefore, neutral pH (i.e.,  $7$ ) was chosen as the optimal pH for further experiments.

Meanwhile,  $\text{pH}_{\text{zpc}}$  of the catalyst as an important factor for finding out the OTC removal mechanism involved was determined to be

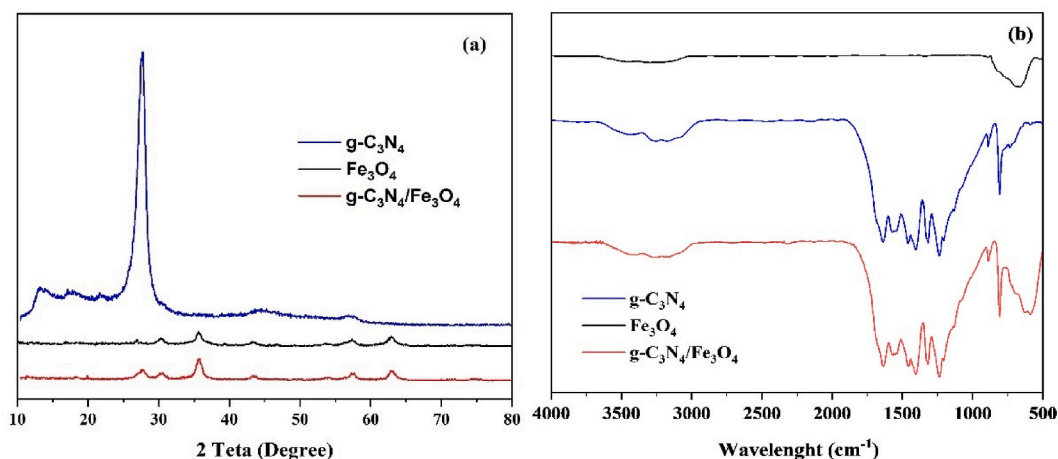


Fig. 2. XRD patterns of  $\text{Fe}_3\text{O}_4$ ,  $\text{g-C}_3\text{N}_4$  and  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  (a), FT-IR images of  $\text{Fe}_3\text{O}_4$ ,  $\text{g-C}_3\text{N}_4$  and  $\text{g-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  (b).

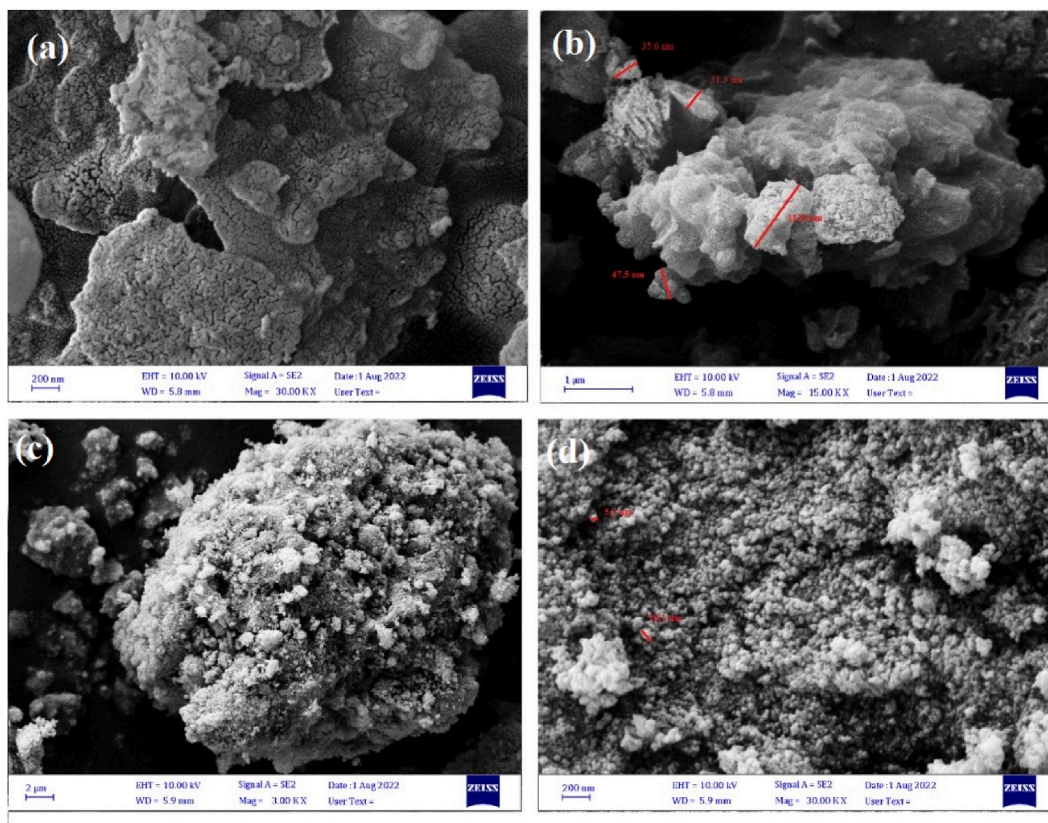


Fig. 3. FE-SEM images of g-C<sub>3</sub>N<sub>4</sub> (a and b) and g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> (c and d).

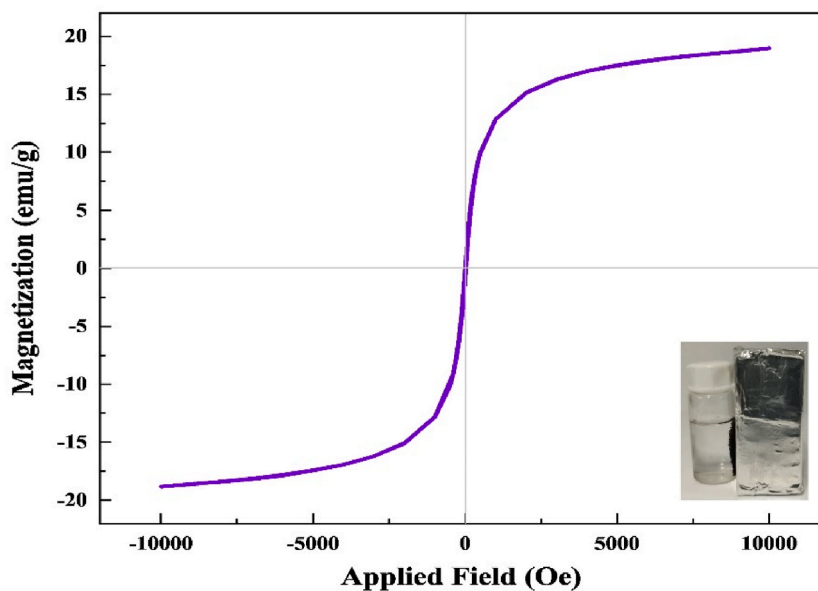


Fig. 4. VSM analysis of g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> nanocomposite.

7.8. At  $\text{pH} \leq \text{pH}_{\text{zpc}}$  values, the catalyst surface is positively charged; whilst at  $\text{pH} \geq \text{pH}_{\text{zpc}}$ , it is negatively charged. Therefore, it is expected that the efficiency of the photocatalytic process alters under different pH values. In addition, varying the pH of the reaction medium definitely results in the changes of the surface charge of the catalyst [28,29]. OTC antibiotic has been reported to have two

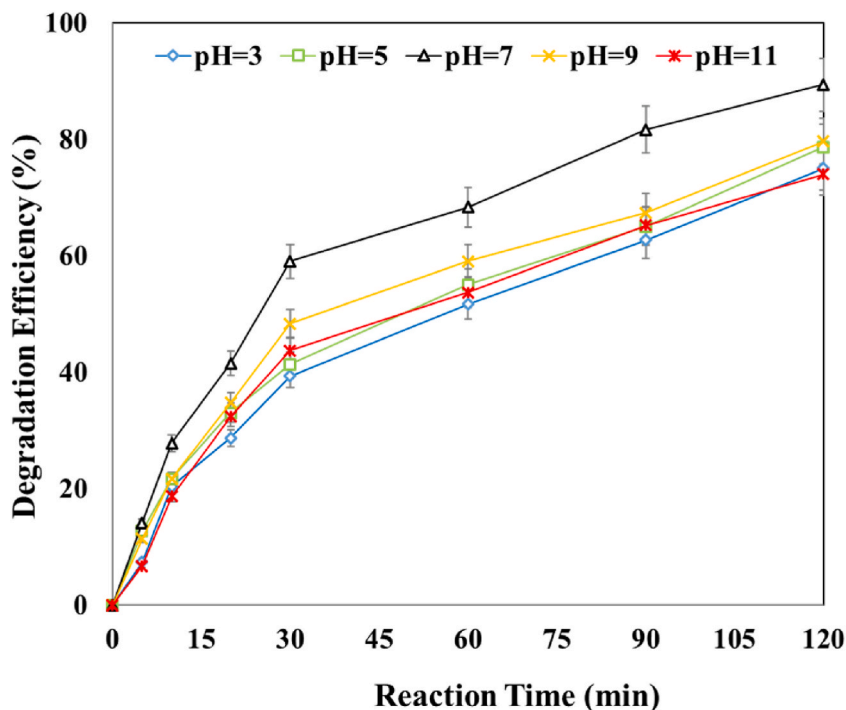


Fig. 5. Effect of variation of pH of solution on the efficiency of the photocatalytic process (catalyst dose = 0.5 g/L, initial OTC concentration = 30 mg/L).

$pK_{a1}$  ( $pK_{a1} = 3.18$  and  $pK_{a2} = 8.29$ ) [30]. Thus, once  $pH < 3.18$ , the cationic form of OTC is dominant ( $OTC^+$ ), whilst at  $pH > 8.29$  the anionic form ( $OTC^-$ ) is a major species in the aqueous solution [31]. Given the  $pH_{zpc}$  of the catalyst used (i.e., 7.8) and the optimal solution pH earlier obtained (i.e., 7), it is thought that the molecular form of OTC is adsorbed on the surface of the catalyst. This adsorption is likely related to the strong electrostatic interactions between the catalyst surface and the functional groups of OTC [32, 33]. In a study by Xu et al. they demonstrated that the efficiency of the photocatalytic process was enhanced in the presence of the

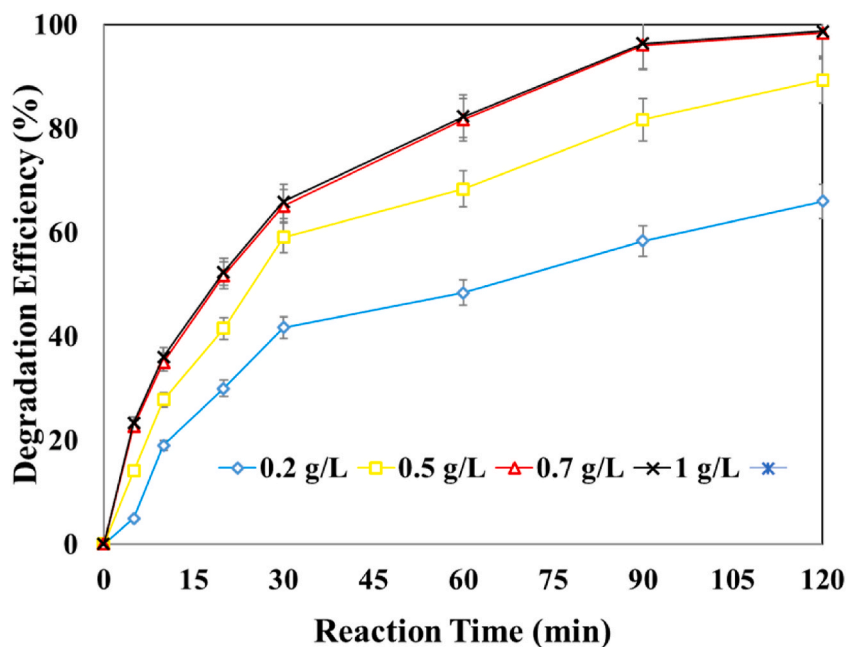


Fig. 6. Effect of catalyst dose on the efficiency of the photocatalytic process ( $pH = 7$ , and initial antibiotic concentration = 30 mg/L).

magnetic nanocomposite  $g\text{-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  for the removal of catechol. In this study, the efficiency of the process was reported to be highest at pH 7 than other pH values [34]. In another related study by Chi et al. they also reported the maximum photocatalytic removal of arsenate was obtained at about neutral pH in the presence of the  $g\text{-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  catalyst [35].

### 3.2.2. Effect of catalyst dosage

In Fig. 6, the effect of the catalyst dosage ranging from 0.2 to 1.0 g/L on the efficiency of the photocatalytic process is shown. As illustrated, the efficiency of the process enhanced (98 %) by increasing the dose of the catalyst (up to 0.7 g/L) and thereafter levelled out. Therefore, the value of 0.7 g/L for the optimal catalyst dose was chosen.

An improvement in the efficiency of the process which followed the rise in the dose of the catalyst could be attributed to an increase in the number of active sites on the catalyst surface. The tiny drop in the efficiency of the process (observed between the corresponding values of 0.7 and 1.0 g/L) could be related to the fact that high amounts of catalyst in the solution prevents the effective penetration of UV into the reactor. In addition, high amounts of catalyst can lead to an increase in the production of hydroxyl radicals resulting in a decrease in the efficiency [36]. In a study conducted by Zhang et al. the optimal dose of  $g\text{-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  catalyst was determined as 0.4 g/L [37]. Also, in a further related study by Ghodsi et al. the optimal amount of catalyst in diazinon removal was determined to be 0.5 g/L [38].

### 3.2.3. Effect of initial concentration of OTC antibiotic

The effect of changes in the initial concentration of the antibiotic OTC (within the range 5–50 mg/L) on the efficiency of the photocatalytic process is depicted in Fig. 7. According to the results obtained, the efficiency of the photocatalytic process dropped as the initial concentration of OTC increased. This finding is explained by the fact that by increasing OTC concentration and consequent further UV absorption, a decline in the rate of production of radical species, which are responsible for the degradation of OTC, takes place leading to a reduction in the removal efficiency of the photocatalytic process [39]. Tang et al. investigated the efficiency of the photocatalytic process in the removal of methylene blue and rhodamine B dyes and found out that with an increase in the concentration of the both dyes, the efficiency of the process decreased [40]. In an almost similarly related report by Berkani et al. the efficiency of the photocatalytic process in the removal of penicillin G decreased as the concentration of the pollutant increased and the best removal efficiency was obtained at the concentration of 5 mg/L [41].

### 3.3. Radical scavenger studies

In this experiment, the respective three well-known radical scavengers namely, tert-butanol (TBA), benzoquinone (BQ) and potassium iodide (KI) were used to investigate the influence of hydroxyl ( $\text{OH}^\bullet$ ), superoxide ( $\text{O}_2^{\bullet-}$ ) and hole ( $\text{h}^+$ ) on the efficiency of the photocatalytic process under the optimal conditions established earlier. As shown in Fig. 8, the presence of all three radical scavengers led to the reduction of OTC removal efficiency through the consumption of hydroxyl radical ( $\text{OH}^\bullet$ ), superoxide radical ( $\text{O}_2^{\bullet-}$ ) and hole ( $\text{h}^+$ ). It is reported that the radical scavenging agents have led to a decline in the efficiency of oxidation/reduction reactions in the

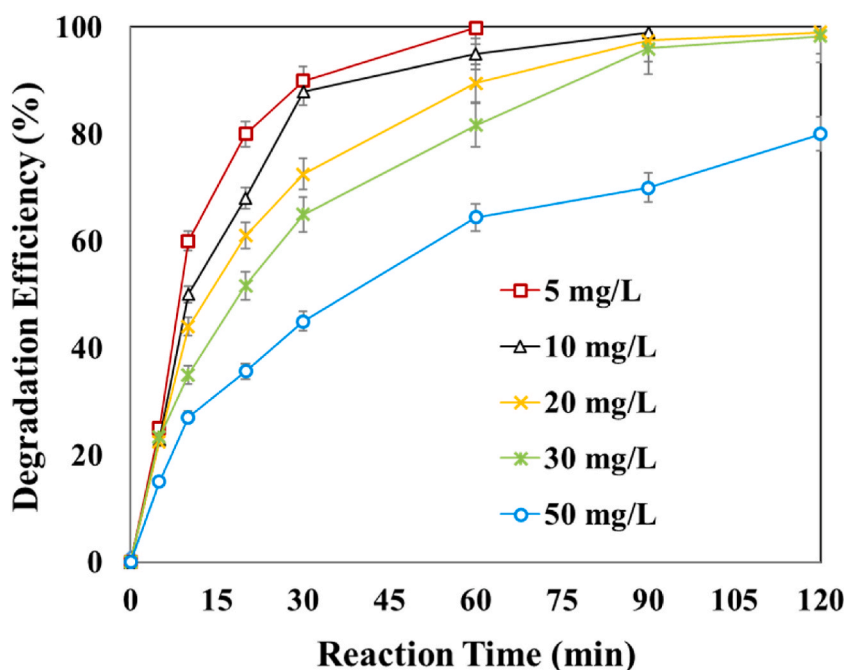
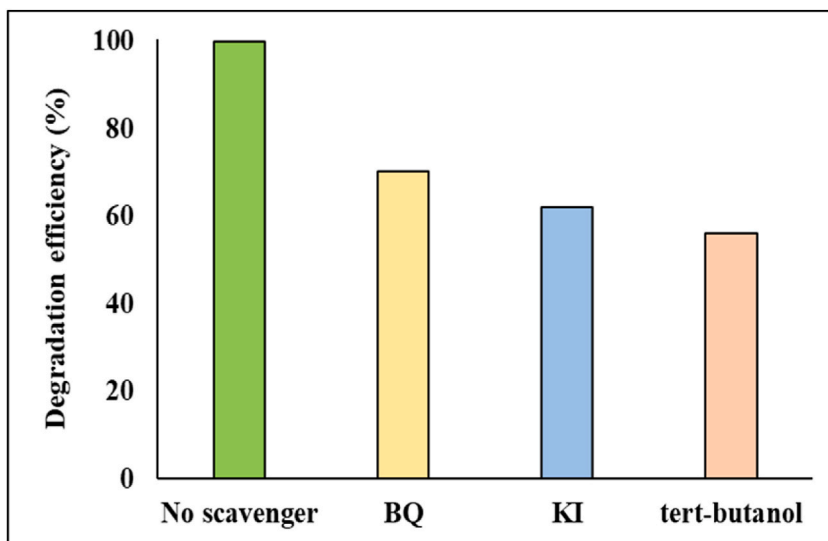


Fig. 7. Effect of initial concentration of OTC on the efficiency of the photocatalytic process (pH = 7, catalyst dose = 0.7 g/L).



**Fig. 8.** Effect of radical scavengers on the efficiency of the photocatalytic process (pH = 7, catalyst dose = 0.7 g/L, OTC concentration = 5 mg/L, scavenger concentration = 0.5 mmol/L and time = 60 min).

photocatalytic process [42]. Hao et al. investigated the presence of scavengers in the removal of RhB in the photocatalytic process and revealed that hydroxyl radical, superoxide radical and  $h^+$  were the main active species in the decomposition of RhB [43].

#### 3.4. Reusability and stability of $g\text{-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$

In a different experiment, the stability and reusability of  $g\text{-C}_3\text{N}_4/\text{Fe}_3\text{O}_4$  catalyst was tested. Under the optimal conditions, following four consecutive cycles of use, the efficiency of the photocatalytic process did not almost alter and just a tiny drop (<5 %) was observed (see Fig. 4s). This implies that the applied catalyst in this study features great stability and reusability and can be reused at least for four times with almost no drop in its efficiency. In a study conducted by Sarkar et al. the applied catalyst was used over four consecutive cycles and the removal efficiency of the process remained almost unchanged [44]. In a similarly related report by Gupta et al. the same results were obtained as well [45].

#### 3.5. Kinetics of photocatalytic process

The mathematical relationships and the corresponding reaction rate coefficients ( $R^2$ ) based on the zero-order, first-order, pseudo-first-order, and second-order kinetic models are tabulated in Table 1.

The results obtained revealed that the kinetics of the process follows the first-order model. In a first-order kinetic model, the rate of reaction is proportional to the concentration of reactant (pollutant). The highest coefficient calculated ( $R^2 = 0.9755$ ) implies that the active species are sufficiently produced during the removal process [39]. In a study by Wang et al. they investigated the efficiency of the photocatalytic process in the degradation of fluoroquinolones' antibiotics using  $g\text{-C}_3\text{N}_4$  nanoparticles and found out that the kinetics followed the first-order model [46]. Furthermore, in a study by Liu et al. they also reported that the kinetics involved in the photocatalytic process using  $g\text{-C}_3\text{N}_4$  and ZnO, best fitted to the first-order model [47].

#### 3.6. Determination of COD and TOC values

The efficiency of the applied photocatalytic process with regard to the reduction of COD and TOC values under the optimal conditions is illustrated in Fig. 5s. Based on the results, the applied photocatalytic process can reduce COD and TOC values to a great extent.

As shown, under the optimal conditions, the COD and TOC efficiency values for the photocatalytic process with regard to the

**Table 1**

Kinetic data of the photocatalytic process (pH = 7, catalyst dose = 0.7 g/L, and OTC concentration = 5 mg/L).

Kinetic model							
Zero-order		First-order		Pseudo-First-order		Second-order	
k	$R^2$	k	$R^2$	k	$R^2$	k	$R^2$
0.0748	0.7031	0.0372	0.9755	0.039	0.5027	0.0047	0.9393



removal of OTC antibiotic were reduced and determined to be 87 and 59 %, respectively. In a study by Ata et al. the respective efficiency values of COD and TOC were reported to be within the range of 62–79 % and 62–86 % using the NFC-doped catalyst [48]. Furthermore, in a study by Kordestani et al. they reported that only 59.8 % of the initial COD and 48.7 % of the initial TOC were reduced in ceftriaxone removal case [49].

### 3.7. Contribution of involving components to OTC degradation

A number of control tests were performed to find out the contribution of each individual component engaged in the photo-degradation process. In this regard, the degree of contribution concerning each individual component involved in the OTC degradation was determined. For this aim, five involving components, namely UV, UV/g-C<sub>3</sub>N<sub>4</sub>, UV/Fe<sub>3</sub>O<sub>4</sub>, UV/g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> and g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> were applied separately under the established optimum conditions and 60 min of contact time. As depicted in Fig. 9, the respective values of the degradation efficiency of OTC for each component were as follows: g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> (11.8 %) and UV (20.1 %), UV/g-C<sub>3</sub>N<sub>4</sub> (38.2 %), UV/Fe<sub>3</sub>O<sub>4</sub> (29.5 %) and UV/g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> (99.8 %). These results are indicative of a synergetic effect, which stems from the integration of UV light irradiation and the nanocomposite. It is concluded that the combined system (UV/g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub>) definitely facilitates the degradation process [37].

### 3.8. Real environmental samples

The efficiency and applicability of the applied photocatalytic process in two real environmental samples (tap water and treated wastewater) were also assessed under the optimal conditions earlier established. The results showed that the tiny drop in the efficiency of the photocatalytic process was observed once the tap water was tested. This can be due to the presence of various cations and anions in the tap water, which may serve as radical or interfering scavengers. In the case of the wastewater the corresponding drop in the efficiency of the photocatalytic process was more appreciable (see Fig. 10). According to the reports published, the presence of some anions and cations in water sources competing with the target pollutant(s) lead to the consumption of active radicals and thereby reduces the efficiency of the process [50]. In a study by Yazdanbakhsh et al. the efficiency of the photocatalytic process in the removal of the antibiotic sulfamethoxazole in wastewater samples was reduced from 100 to 92 % [39]. It should be also noted that the presence of organic compounds such as humic acid may reduce the efficiency of the photocatalytic process. In further related studies by Xie et al. [51], almost similar report on the reduction of the efficiency of the photocatalytic process in wastewater samples were released.

### 3.9. Photocatalytic mechanism

The possible mechanism with regard to OTC photo degradation process using the catalyst (g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub>) under UV-irradiation is depicted in Scheme 1. The values (band gap energy levels) of the valence band (VB) and conduction band (CB) of g-C<sub>3</sub>N<sub>4</sub> and Fe<sub>3</sub>O<sub>4</sub> nanoparticles were calculated using the following empirical formula (Eq. (3) and (4)).

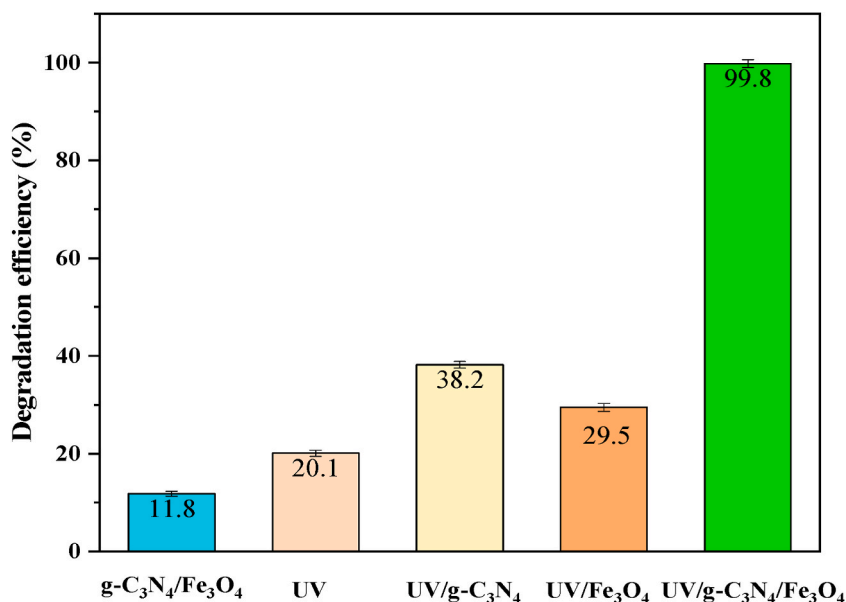
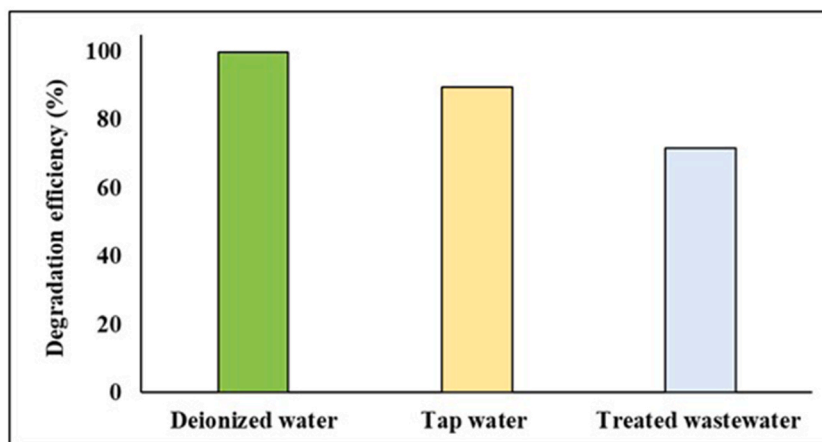
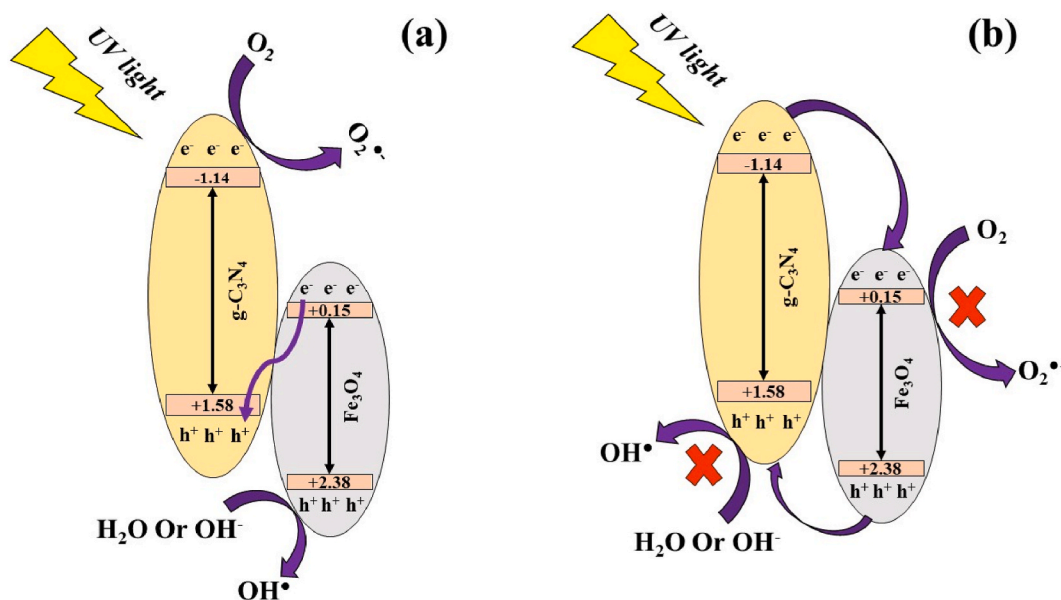


Fig. 9. Contribution of each component engaged in the degradation of efficiency of OTC under the optimum conditions (pH = 7, catalyst dose = 0.7 g/L, OTC concentration = 5 mg/L and time = 60 min).



**Fig. 10.** Efficiency of the photocatalytic process in OTC removal in real environmental samples (pH = 7, catalyst dose = 0.7 g/L, OTC concentration = 5 mg/L and time = 60 min).



**Scheme 1.** Illustration of the photocatalytic mechanism using  $\text{Fe}_3\text{O}_4/\text{g-C}_3\text{N}_4$  catalyst for simultaneous OTC degradation: S-scheme heterojunction (a) and type-II heterojunction (b).

$$E_{\text{VB}} = \chi - E_{\text{e}} + 1/2E_{\text{g}} \quad (3)$$

$$E_{\text{CB}} = E_{\text{VB}} - E_{\text{g}} \quad (4)$$

$E_{\text{g}}$  represents the band gap values;  $\chi$  denotes the Mulliken's absolute electronegativity ( $\chi\text{-g-C}_3\text{N}_4 = 4.72$  eV and  $\chi\text{-Fe}_3\text{O}_4 = 5.73$  eV);  $E_{\text{e}}$  outlines the energy of free electrons (4.5 eV). The CB and VB values for  $\text{g-C}_3\text{N}_4$  were determined to be  $-1.14$  eV and  $+1.58$  eV and the corresponding values for  $\text{Fe}_3\text{O}_4$  were  $+0.15$  eV and  $+2.38$  eV, respectively.

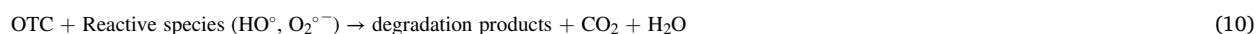
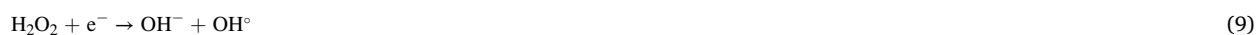
**Scheme 1** (a) illustrates the S-scheme heterojunction-based mechanism through the charge transfer within  $\text{Fe}_3\text{O}_4/\text{g-C}_3\text{N}_4$  catalyst under UV-light irradiation. As the applied catalyst is exposed to UV-light irradiation, the electrons are excited resulting in the production of electron-hole pairs (Eq. (5)).

The electrons in the CB of  $\text{Fe}_3\text{O}_4$  could be transferred to the VB of  $\text{g-C}_3\text{N}_4$ , where the reintegration with the remaining holes takes place. Since the CB value of  $\text{g-C}_3\text{N}_4$  is more negative than the corresponding potential value of  $\text{O}_2/\text{O}_2^{\bullet-}$  ( $-0.33$  eV vs. NHE), its CB electrons could be transferred to the  $\text{O}_2$  molecules and produce  $\text{O}_2^{\bullet-}$  particles (Eq. (6)). In addition, the holes in the VB of  $\text{Fe}_3\text{O}_4$  could oxidize  $\text{H}_2\text{O}/\text{OH}^-$  and generate  $\text{HO}^\bullet$  Eqs. (7)–(9), due to be of more positive energy level than standard potentials of  $\text{HO}^\bullet/\text{OH}^-$  (1.99 eV vs. NHE) and  $\text{HO}^\bullet/\text{H}_2\text{O}$  (2.34 eV vs. NHE), In turn, the  $\text{O}_2^{\bullet-}$  and  $\text{HO}^\bullet$  species could degrade OTC under UV light irradiation (Eq.

(10)) [52–55].

Provided that the charge transfer involving the electron-hole pairs generated by UV light follows the pattern observed in conventional heterojunction systems (Scheme 1(b)), the electrons are pushed away from the CB of g-C<sub>3</sub>N<sub>4</sub> to the CB of Fe<sub>3</sub>O<sub>4</sub>, while the holes located onto the VB of Fe<sub>3</sub>O<sub>4</sub> are transferred to the VB of g-C<sub>3</sub>N<sub>4</sub>. Due to the lower potential VB of g-C<sub>3</sub>N<sub>4</sub> than that of HO<sup>•</sup>/OH<sup>-</sup> (1.99 eV vs. NHE) and HO<sup>•</sup>/H<sub>2</sub>O (2.34 eV vs. NHE), the oxidation of OH<sup>-</sup>/H<sub>2</sub>O for the generation of HO<sup>•</sup> seems unlikely. Therefore, the electrons in the CB of Fe<sub>3</sub>O<sub>4</sub> cannot react with O<sub>2</sub> to produce O<sub>2</sub><sup>•-</sup> radicals, because the CB potential value of Fe<sub>3</sub>O<sub>4</sub> is not more negative than potential of the O<sub>2</sub>/O<sub>2</sub><sup>•-</sup> (-0.33 eV vs. NHE) [55–57].

Considering all mentioned points and Scheme 1 (a and b), the proposed S-scheme heterojunction-based mechanism seems to be suitable to explain and elucidate the degradation of OTC using g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> catalyst under UV irradiation.



### 3.10. A comparative-based study

Herein, a number of previously reported studies on the photocatalytic degradation of OTC published elsewhere were summarized in Table 2 [30,58–62]. As can be seen, the efficiency and merits of this research study concerning the decomposition and removal of OTC are fairly comparable with the other reports.

## 4. Conclusion

Herein, g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> nanocomposite was initially prepared by a simple hydrothermal method and applied as the efficient catalyst for the efficient removal of a well-known antibiotic namely, OTC from the aqueous environmental samples under UV irradiation. Following that, the effect of major operating parameters affecting the photocatalytic process was individually optimized and then the optimal conditions for the removal of OTC in aqueous media were established. Moreover, the effect of radical scavengers on the applied photocatalytic process was evaluated in detail. The maximum removal efficiency of 99.8 % was achieved for OTC under the optimal conditions set. The utmost degradation efficiency of 99.8 % was achieved for OTC under neutral pH 7; catalyst dose, 0.7 g/L; and an initial OTC concentration of 5 mg/L. In addition, the kinetic results well fitted to the first-order model with R<sup>2</sup> of 0.9755. The respective COD and TOC efficiency values for the applied photocatalytic process were obtained to be 87 and 59 %, respectively. Additionally, the lowest degradation efficiency for OTC was observed in the presence of tert-butanol radical scavengers, and the OH radicals played a key role in that regard. Finally, the combined UV/g-C<sub>3</sub>N<sub>4</sub>/Fe<sub>3</sub>O<sub>4</sub> photocatalytic process proved to be highly efficient for the removal of OTC antibiotic in several real water sources and could be potentially applied for the removal of other pollutants from aqueous solutions.

### Data availability

The datasets generated and analyzed during the current study were available from the corresponding author on reasonable request.

**Table 2**  
Comparative study on the photocatalytic degradation of OTC.

Photocatalyst	Light Source	C (mg/L)	Time (min)	R (%)	References
CoFe@NSC	visible light	50	150	90	[58]
TiO <sub>2</sub> /5A zeolite	UV	50	150	100	[30]
g-C <sub>3</sub> N <sub>4</sub> /LaFeO <sub>3</sub> (2 %)	visible light	40	120	90	[59]
B <sub>4</sub> NbO <sub>8</sub> Cl/g-C <sub>3</sub> N <sub>4</sub>	visible light	20	60	87	[60]
ZnO/ZrO <sub>2</sub>	UV	10	120	69	[61]
Br (15 %)/g-C <sub>3</sub> N <sub>4</sub>	visible light	10	120	75	[62]
g-C <sub>3</sub> N <sub>4</sub> /Fe <sub>3</sub> O <sub>4</sub>	UV	5	60	99.8	This work

## CRediT authorship contribution statement

**Kourosh Mahmoudi:** Methodology, Investigation. **Mahdi Farzadkia:** Methodology, Investigation. **Roshanak Rezaei Kalantary:** Validation, Methodology. **Hamid Reza Sobhi:** Conceptualization. **Mojtaba Yeganeh:** Methodology. **Ali Esrafilii:** Validation, Supervision.

## Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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## Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.heliyon.2024.e30604>.

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