



Electrospun nanofibrous membrane for filtration of coconut *neera*

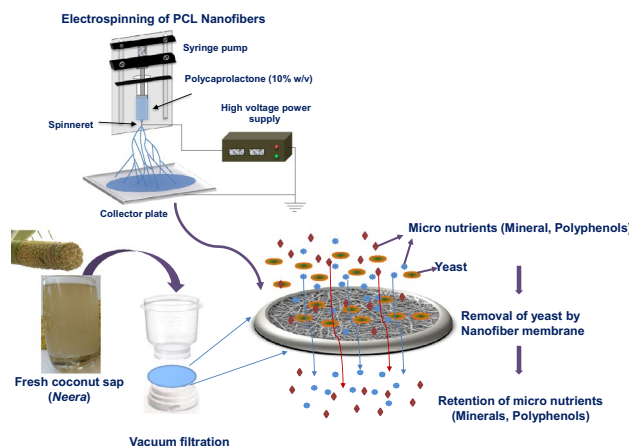
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Abstract

Coconut *neera* is a nutritious natural drink that is rich in amino acids, polyphenols, vitamins, and minerals. Nevertheless, the inherent presence of yeast activates natural fermentation. To prevent the fermentation process, it is necessary to reduce the yeast load in fresh *neera*, at the earliest possible. In this research, an electrospun polycaprolactone nanofibrous membrane was used for the removal of yeast from coconut *neera*. Randomly oriented non-woven nanofibers were fabricated using the electrospinning process. The process conditions were optimized at 15 kV applied voltage, 8 cm distance between the spinneret needle and the collector plate, and 1.6 ml/h feed flow rate for the best nanofiber characteristics and high filtration efficiency. The optimized nanofibrous membrane for *neera* filtration had an average fiber diameter of 942 nm, average porosity of 73.26%, and a mean thickness of 150 μm . Results confirmed that the porosity of the membrane had a significant effect on the flow rate of permeate. The biochemical characteristics of *neera* filtrate were investigated. In comparison with fresh *neera*, the filtered counterpart had significant changes in titratable acidity, pH, and color. While no significant changes were observed in total soluble solids content, slight reductions were noted in the total polyphenolic content and minerals. Importantly, the *neera* filtrate obtained through the optimized nanofibrous membrane showed a 2 log-reduction in yeast load. The effective reusability of the membrane and stability of the nanofiber morphology at repeated usage was confirmed. This approach shows prospects for *neera* filtration while retaining nutrient content and can be extended to other natural extract applications.

Graphic abstract



Keywords Coconut *neera* · Yeasts · Filtration · Electrospinning · Nanofiber membrane

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Introduction

Coconut sap (*neera*) from the coconut tree (*Cocos nucifera* L.) is a healthy and refreshing drink. Fresh *neera* is sweet, contains sugars with less percentage of fructose,

oyster-white, and translucent in appearance [1]. It is rich in amino acids, minerals, and vitamins. It has a neutral pH, low calorific value, and low glycemic index (around 35) [2, 3]. *Neera* provides various health benefits; for example, it is known to improve digestion, provides instant energy, prevents damage of cells, lowers blood pressure, reduces cholesterol level, contributes to skin health. It also aids in postoperative care due to the presence of high electrolyte contents [4]. This explains the growing demand for this product and necessitates the requirement for appropriate post-harvest processing and preservation techniques. This is of significant interest as coconut as a crop is specific to certain regions of the world, and value addition/preservation of *neera* has significant health, technological, and economic benefits [5].

Neera is highly susceptible to natural fermentation by the inherent yeasts (particularly *Saccharomyces cerevisiae*) [6, 7]. Sugar is a major constituent in *neera* (14–18% w/v) [4] and gets rapidly transformed into alcohol by the fermentation process [8, 9]. Fermented *neera* is known as ‘toddy’, an alcoholic beverage [9, 10]. Alternatively, an acetic fermentation process can yield ‘coconut vinegar’ [11, 12]. Post-harvest processing and preservation techniques hold an indispensable role in the shelf-life of coconut *neera*. Especially, the removal of yeast from coconut *neera* is a major concern associated with quality. Numerous research works have attempted to do so, using a range of thermal and non-thermal processing methods. However, the problem remains, particularly as the need is to retain the ‘fresh-like’ attributes of *neera* [13–15].

Electrospinning is an electrohydrodynamic process that involves the fabrication of nanofibrous membranes by the random orientation of non-woven nanofibers under high electrostatic fields at a voltage of around 1–30 kV [16, 17]. Electrospun nanofibers have versatile applications in biomedical (scaffolds, drug delivery, regenerative medicine, medical textile, protective masks), textile (smart fabrics, protective clothing, waterproof textiles), environmental protection, food packaging, sensing, immobilization, catalyst, filtration, membranes, and cosmetic sectors [18–22]. Interestingly, nanofibrous membranes have a high surface-area-to-volume ratio which allows permeate flow at a higher rate, and the porosity of the nanofibrous membrane is responsible for filtration efficiency [23]. The applications of the electrospun nanofibrous membrane in food science, beverage, and water filtration/ treatment are well documented [24–27]. Nanofibrous membranes have been explored for different beverage filtration applications ranging from clarification to removal to selective adsorption of unwanted polyphenols [28]. Interestingly, in certain cases, they can offer a ‘one-step’ clarification process without the need for filter aids and enzymatic treatments in beverage processing.

This work reports the first-of-its-kind study on the filtration of *neera* using an electrospun nanofibrous membrane. It demonstrates the use of electrospun polycaprolactone (PCL) nanofibrous membrane for coconut *neera* filtration. The interconnected porosity of nanofibrous membranes does not allow macromolecules (in this case, yeast with an average size of 4–10 μm) to penetrate through the membrane. However, it can allow micromolecules, micronutrients, and antioxidants, to flow through the membrane. PCL is a low-cost biodegradable synthetic polymer and exhibits good mechanical and antimicrobial properties. It is a biocompatible material approved by the U.S. Food and Drug Administration (FDA) [29, 30]. Also, it is authorized as a direct food contact material by the European Food Safety Authority (EFSA) and FDA [31, 32]. Hence, PCL was chosen as the polymeric material for nanofibrous membrane fabrication. The findings of this study will explicit the ability of electrospun nanofibrous membrane in the removal of yeasts from coconut *neera*.

Materials and methods

Chemicals and materials

PCL (average Mn 80,000), chloroform (anhydrous $\geq 99\%$), ethanol (absolute) were obtained from Sigma Aldrich Chemicals Pvt. Ltd., Bengaluru, India. Methanol, Folin–Ciocalteu’s phenol reagent, phenolphthalein indicator (0.1% w/v), sodium hydroxide anhydrous, and chloramphenicol yeast glucose agar were obtained from HiMedia Laboratories Pvt. Ltd., Mumbai, India. Fresh coconut *neera* was tapped and harvested from the coconut palm trees at Thanjavur, Tamil Nadu, India.

Nanofibrous membrane formation

The PCL solution (10% w/v) was prepared in a mixture of chloroform and methanol in the ratio of 7:3. It was stirred using a magnetic stirrer until the polymer dissolved properly. PCL nanofibrous membranes were produced using the electrospinning unit reported by Maria Leena et al. [33] (Model VP30C, Royal Enterprises, Chennai, India) equipped with a digitally controlled syringe pump and high voltage power supply (up to 30 kV). The polymer feed solution was filled in a 5 ml syringe with a stainless steel spinneret needle and was placed perpendicularly over the collector plate with the ground electrode connection. The spinneret needle was connected with the power supply at a high voltage, and a potential difference was created between the spinneret needle and the collector plate. The flow rate of feed solution and the work distance between the spinneret needle and the collector plate were varied at fixed a voltage

of 15 kV (optimized to form Taylor cone, based on preliminary trials). These nanofibrous membranes were coded as NF01, NF02, and NF03 based on the different experimental conditions (Table 1).

Characterization of nanofibrous membranes

Morphology analyses

The nanofibrous membranes were sputter-coated with gold at 10 mA applied current for 60 s using a mini magnetron sputtering unit (Model SC7620, Quorum Technologies Ltd., Lewes, UK), and the morphology characteristics of nanofibers were examined using a scanning electron microscopy (SEM) (Model VEGA3, Tescan, Czech Republic, EU). Fiber diameter distribution in different nanofibrous membranes and average diameter of nanofibers was estimated by measuring the diameter of randomly selected 25 fibers from the original SEM micrograph using the IMAGE J software (National Institute of Health, Bethesda, Maryland, USA). The thickness of nanofibrous membranes was measured using a digital micrometer (with ± 0.001 mm accuracy) (3109-25S, Insize India LLP, Gujarat, India).

Porosity

The porosity of PCL nanofibrous membranes (NF01, NF02, and NF03) was estimated using a pycnometer (Borosil®) [23]. Based on Archimedes' displacement principle the membrane porosity was calculated using Eq. (1).

$$\text{Porosity (\%)} = \frac{W_2 - W_3 - W_m}{\rho_e} / \frac{W_1 - W_3}{\rho_e} \times 100 \quad (1)$$

where W_1 is the weight of ethanol filled pycnometer (in g), W_2 is the weight of pycnometer filled with absolute ethanol and nanofibrous membrane (in g), W_3 is the weight of the pycnometer with retained ethanol after removal of

the ethanol-soaked nanofibrous membrane from W_2 (in g), W_m is the dry weight of the nanofibrous membrane (in g), and ρ_e is the density of ethanol (in g/cm^3).

Neera filtration

Harvested *neera* was quickly stored under refrigeration temperature after any visual impurity was removed. The filtration process was immediately commenced. The filtration process was performed using a borosilicate glass filtration assembly (Borosil®-5350029) with an oil-free vacuum pump. The filtration assembly consisted of a filtrate flask (1000 ml), funnel (300 ml), anodized aluminum spring clamp, and fritted glass support base (47 mm diameter) with an integral vacuum connection. The filtration base had an effective filtration area of 9.6 cm^2 . Fabricated PCL nanofibrous membranes (NF01, NF02, and NF03) were cut into a circular shape (diameter = 47 mm) and fit in the support base of the filtration unit. *Neera* was filtered through the nanofibrous membrane under vacuum, and the time taken was recorded. Permeate flow rate across the nanofibrous membrane during filtration was estimated as the time taken for a specified volume of the sample to get filtered. The filtration was performed in a sterile environment, and all glasswares used were previously sterilized in an autoclave at 121°C for 15 min to prevent any contamination.

To access the reusability of the nanofiber membrane after filtration, the membrane was washed with water and 70% ethanol and dried. Before the next use, it was UV sterilized for 20 min and reused for filtration of *neera* using the filtration setup. The repeatability of the membrane was tested multiple times considering changes in flux.

Biochemical characteristics of neera filtrate

Total soluble solids and titratable acidity

Total soluble solids (TSS) content of *neera* samples was determined using a portable handheld digital refractometer (range 0–32%) (RHB-32ATC, ERMA, Tokyo). In the refractometer, the sample drop was placed on the angled prism and sealed with the clear plate. The readings of total soluble solids were recorded in terms of °Brix [34]. Titratable acidity (TA) of *neera* samples was determined according to the AOAC method. A 25 ml of *neera* sample was added with two drops of phenolphthalein indicator and titrated with sodium hydroxide (NaOH) solution (0.1 N) until reaching the endpoint (appearance of permanent pink color). Acidity was measured in terms of the percentage of citric acid using Eq. (2) [34, 35].

Table 1 Experimental conditions during the electrospinning process for nanofibrous membrane formation

Sample	Electrospinning conditions				Mean thickness of the nanofibrous membrane (μm)
	Distance between spinneret and collector plate (cm)	Size of spinneret needle (G)	Feed flow rate (ml/h)	Applied voltage (kV)	
NF01	10	24	2.4	15	Fixed as ~150
NF02	8	24	1.6	15	
NF03	8	24	0.8	15	

$$\text{Titrateable Acidity (\%)} = \frac{V_{\text{NaOH}} \times N_{\text{NaOH}} \times F_{\text{Meq}}}{V_{\text{Sample}}} \times 100 \quad (2)$$

where V_{NaOH} is the volume of NaOH solution used for titration (in ml), N_{NaOH} is the normality of NaOH solution (in mol/m³), F_{Meq} is the milliequivalent factor of citric acid (0.0064), and V_{Sample} is the volume of the *neera* sample used for titration (in ml).

Color and pH

CIE color values of the *neera* samples were determined using a colorimeter (Color Flex® EZ, Hunter Associates Laboratory, Inc., USA). L^* , a^* , and b^* values were recorded, and the color change (ΔE^*) was calculated using Eq. (3).

$$\Delta E^* = \sqrt{(L_0^* - L^*)^2 + (a_0^* - a^*)^2 + (b_0^* - b^*)^2} \quad (3)$$

where L_0^* , a_0^* , and b_0^* are color space values of the fresh *neera*; L^* , a^* , and b^* are color space values of the *neera* filtrate.

The pH of the *neera* samples was determined using a pH meter (PC 700, Eutech Instruments Pte. Ltd.; accuracy ± 0.01 pH).

Total polyphenol content

Total polyphenol content (TPC) in the *neera* filtrate was estimated by the Folin-Ciocalteu method [36] and compared with fresh *neera* (control). The optical density (OD) of samples was observed at 765 nm using a multi-mode microplate reader (SpectraMax® iD3, Molecular Devices LLC, USA). TPC of the samples was calculated from a gallic acid standard curve and results were mentioned in terms of gallic acid equivalents (GAE $\mu\text{g/ml}$).

Estimation of minerals

Mineral contents present in *neera* filtrate were determined according to the AOAC method by using inductively coupled plasma optical emission spectrometry (ICP-OES) (Optima™ 2000 DV, PerkinElmer Inc, Shelton, CT, USA) equipped with WinLab32™ software (ver.7.0) [37].

Enumeration of yeasts

Yeast cell load was determined by the standard spread plate method. A ten-fold serial dilutions of each sample (control, NF01, NF02, and NF03) were made with sterile double distilled water and 50 μl of the sample was spread plated on chloramphenicol yeast glucose agar; the plates were incubated at 25 °C for 48 h. Enumeration of yeasts was done by following the standard protocol according to IS 5403 method

[38]. Yeast cell count was estimated as colony forming units (CFU) per ml.

Statistical analysis

All the experiments were carried out in triplicates, and the results were statistically analyzed by one-way ANOVA and interpreted with Duncan's post hoc test ($P < 0.05$) using SPSS (ver. 21.0; IBM, Armonk, NY, USA).

Results and discussion

Characterization of nanofibrous membranes

Morphology analysis

The surface morphology of PCL nanofibrous membranes is shown in Fig. 1. The average diameter of nanofibers was observed to be 1.66 μm , 942 nm, and 857 nm for NF01, NF02, and NF03, respectively. The random orientation of fibers having diameters in nanoscale was formed with a decrease in flow rate to 0.8 ml/hr at 15 kV voltage and 8 cm distance. The fiber diameter distribution in different nanofibrous membranes confirms that with a decrease in flow rate the fiber diameter decreases and formed uniform fiber size distribution. Lala et al. [39] reported cellulose acetate, polyacrylonitrile (PAN), and poly(N-vinyl chloride) electrospun nanofiber membranes with a nanofiber diameter of 415 nm, 153 nm, and 599 nm, respectively, for usage as filters to protect from bacterial contaminants.

Porosity

The influence of the electrospinning process parameters on the porosity of nanofiber membranes was investigated. The porosity of the nanofibrous membrane was determined as a fraction of the void in a total volume of the nanofibrous membrane using a pycnometer. The percentage of porosity of nanofibrous membranes was observed to be 76.16 ± 0.84 , 73.26 ± 1.62 , and 69.55 ± 0.86 for NF01, NF02, and NF03, respectively. Figure 2a shows the porosity of different nanofibrous membranes. The results expressed that there were significant differences in the porosity among NF01, NF02, and NF03 membranes. In a study by Najafi et al. [40], the polysulfone and polysulfone/Triton X-100 nanofiber membranes with a mean diameter of 1069 ± 82.84 nm and 919.2 ± 66.89 nm, respectively, and porosity of $77.5 \pm 4.5\%$ and $80.5 \pm 4\%$, respectively, were tested for the concentration of pomegranate juice. The fiber diameter and porosity values are similar to the result observed in this study. It was observed that with high internal porosity the permeate flux increased in the nanofibrous membrane.

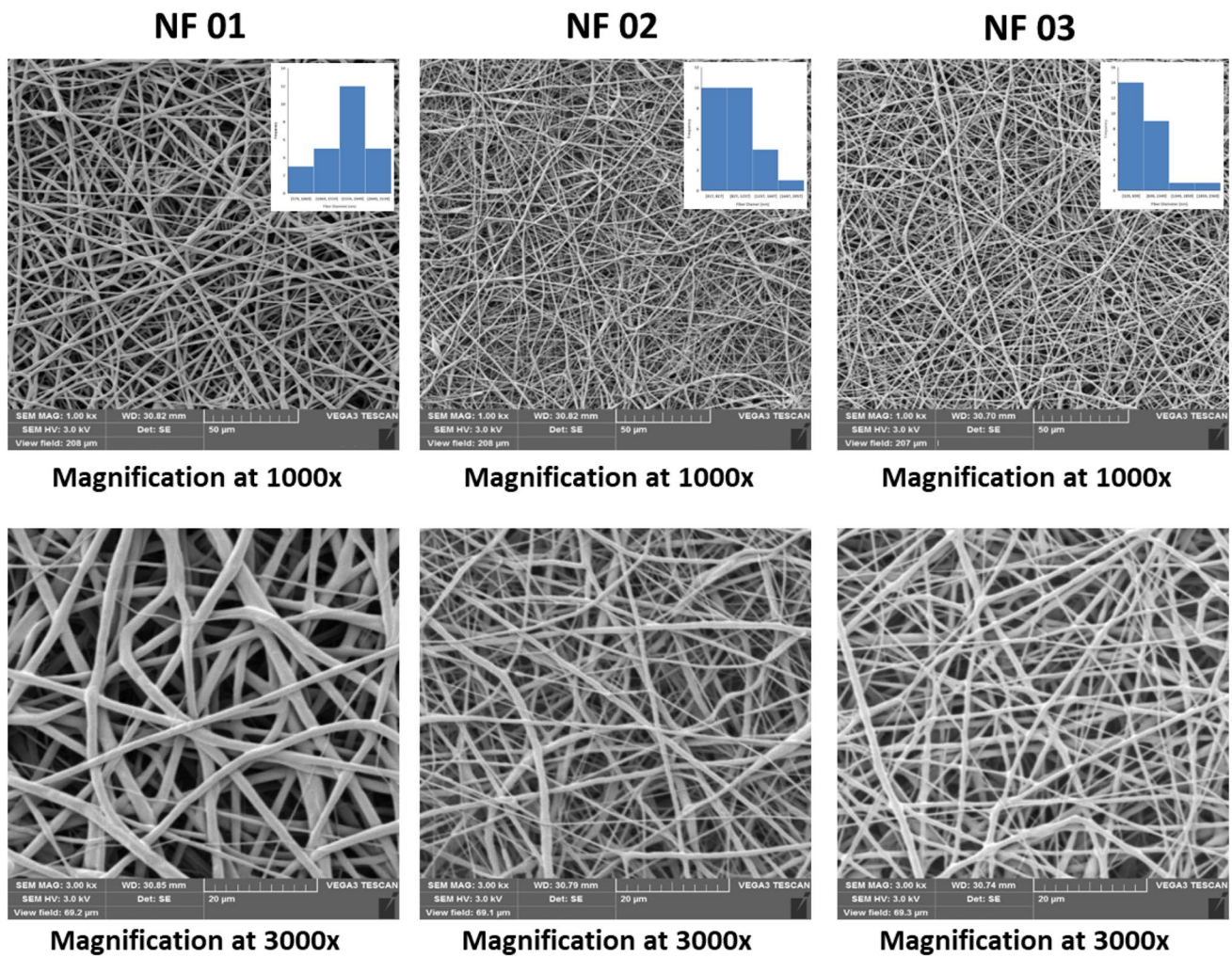
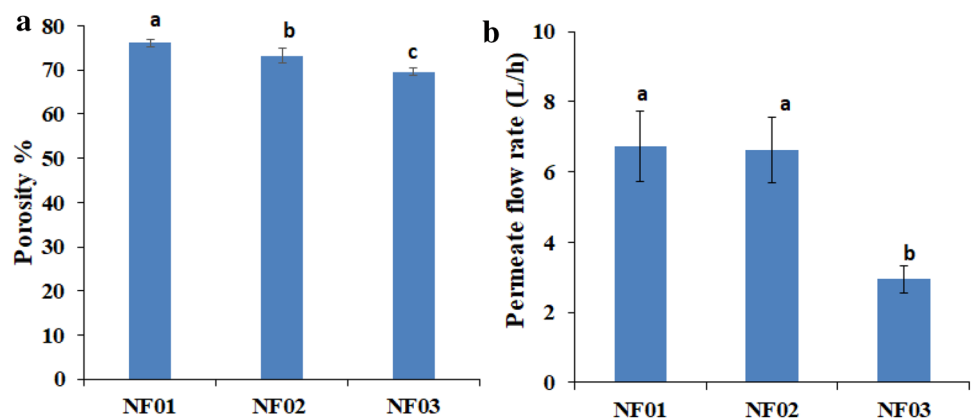


Fig. 1 SEM micrographs of the fabricated nanofibrous membranes

Fig. 2 a Porosity of different nanofibrous membranes and b Permeate flow rate of *neera* across the nanofibrous membranes



Permeate flow rate during *neera* filtration

The permeate flow rate of *neera* passed through the pores of the nanofibrous membrane was estimated by calculating the time required for the filtration process. The permeate flow

rate was found to be 6.73 ± 0.99 L/h, 6.61 ± 0.94 L/h, and 2.94 ± 0.39 L/h for NF01, NF02, and NF03, respectively. Figure 2b shows the permeate flow rate of *neera* across the nanofibrous membranes. The results expressed that there was no significant difference in porosity between NF01 and

NF02 membranes. But both these membranes showed significant differences from the NF03 membrane. Thus, the results demonstrate that the porosity of the nanofibrous membrane has a great impact on the flow rate of permeate. It was observed that the permeate flow rate was increased with an increase in porosity of the membrane. Thus, the permeability of filtrate depends on the porosity of the nanofibrous membranes. Fuenmayor et al., [41] reported that the high porosity (94%) of the electrospun nylon-6 nanofibrous membrane was solely responsible for the increase in permeate flux (1.30 kg/m² h) across the membrane. Adsorption of particles or impurities reduces the porosity of the membrane and leads to a decrease in permeate flux across the membrane. The vacuum can be applied on the downstream side of the membrane to increase the permeate flow rate, thereby enhancing the permeate flux of the membrane. Furthermore, this nanofiber membrane showed better retention of antioxidant activity of apple juice, while selectively removing the bitter phenolic compounds. The nanofiber membrane showed superior performance in removal of color and turbidity compared to the microporous membrane and supported extended stability and shelf-life of beverage products. Bortolassi et al. [42] fabricated a PAN-based composite nanofiber filtration membrane using an electrospinning method and reported mean nanofiber diameters of 292 ± 6 nm, 242 ± 5 nm, and 289 ± 5 nm for Ag/PAN, TiO₂/PAN, and ZnO/PAN nanofibrous membranes, respectively, which formed mean pore sizes of 1.12 ± 0.10 μm, 1.45 ± 0.10 μm, and 2.03 ± 0.10 μm, respectively. Also, they observed that Ag/PAN electrospun nanofibrous membranes show the highest permeability than other counterparts (TiO₂/PAN, ZnO/PAN) due to reduced pressure drop (68.13 Pa) across the filter.

Biochemical characteristics of *neera* filtrate

Biochemical parameters of the *neera* filtrate using different nanofibrous membranes and control are listed in Table 2.

Total soluble solids and titratable acidity

TSS indicates the sugar content of the *neera* sample and is considered a major quality parameter for *neera*. It was determined by the index of refraction using a refractometer, and the values were compared with the control. TSS of the samples was measured in terms of °Brix, and it was observed to be 16.70 ± 0.17, 16.47 ± 0.47, 15.60 ± 0.72, and 15.07 ± 1.80 for control, NF01, NF02, and NF03, respectively. The results showed that the *neera* filtrate had slightly lower TSS as compared to the *neera* control. However, there were no significant differences in TSS content among the *neera* filtrates filtered across the different nanofibrous membranes as well as with the control. Casano et al. [43] developed poly(ether ether ketone) and polysulfone membranes by the dry-wet spinning method for pomegranate juice clarification reported that the TSS content (°Brix) of juice was reduced to 15.4 ± 0.25 and 15.4 ± 0.09 from 16.0 ± 0.10 and 16.0 ± 0.28 while filtration through the poly(ether ether ketone) and polysulfone membranes, respectively. In a different study, Lemma et al. [44] reported the TSS content of beer (5.33 ± 0.05°Brix) remained constant even after filtration with the electrospun nylon nanofibrous membrane. Najafi et al. [40] used a nanofiber membrane to concentrate the pomegranate juice and reported that the TSS content of 35.7°Brix was arrived after concentrated with polysulfone/Triton X-100 nanofiber membrane. Battirola et al. [45] observed a significant reduction in TSS contents in fruit juices and whey after filtration with the cellulose acetate/cellulose nanofiber membranes. They reported that the TSS content (°Brix) of strawberry and raspberry juices were reduced to 1.95 ± 0.49 and 2.55 ± 0.07 from 2.95 ± 0.07 and 2.90 ± 0.00, respectively. Similarly, the TSS content (°Brix) of whey was reduced to 6.88 ± 0.85 and 6.10 ± 0.00 from 7.40 ± 0.14 and 6.35 ± 0.07 while filtration through the cellulose acetate/cellulose nanofiber membrane in the dead-end cell and tangential modules, respectively.

Table 2 Biochemical and physical parameters of the *neera* filtrate and the fresh *neera* (control)

Sample	TSS (°Brix)	TA (% of citric acid)	pH	CIE color values			Color difference (ΔE^*)	TPC (GAE μg/ml)	Yeast load (CFU/ml)
				L^*	a^*	b^*			
Control	16.70 ± 0.17 ^a	2.77 ± 0.20 ^a	6.13 ± 0.21 ^a	9.73 ± 0.12 ^a	-0.57 ± 0.08 ^a	-2.02 ± 0.02 ^a	-	128.42 ± 1.65 ^a	1.55 × 10 ⁶
NF01	16.47 ± 0.47 ^a	1.98 ± 0.29 ^b	6.67 ± 0.01 ^b	3.56 ± 0.06 ^b	-0.32 ± 0.05 ^b	-1.19 ± 0.04 ^b	6.22 ± 0.07 ^a	128.05 ± 2.35 ^a	1.07 × 10 ⁵
NF02	15.60 ± 0.72 ^a	1.88 ± 0.15 ^b	6.74 ± 0.08 ^b	3.34 ± 0.06 ^c	-0.29 ± 0.05 ^b	-1.20 ± 0.13 ^b	6.45 ± 0.15 ^b	123.51 ± 2.24 ^b	2.57 × 10 ⁴
NF03	15.07 ± 1.80 ^a	1.77 ± 0.04 ^b	6.78 ± 0.10 ^b	3.28 ± 0.01 ^c	-0.27 ± 0.06 ^b	-1.21 ± 0.03 ^b	6.51 ± 0.11 ^b	123.42 ± 0.59 ^b	2.38 × 10 ⁴

Results were expressed as mean ± SD (n = 3); different superscripts of lowercase letters along the samples in each parameter represent significant differences at $P < 0.05$ level

TA indicates the acidity of the *neera* samples. The acidity of the *neera* filtrate and fresh *neera* (control) was measured in terms of the percentage of citric acid. The percentage of TA was found to be 2.77 ± 0.20 , 1.98 ± 0.29 , 1.88 ± 0.15 , and 1.77 ± 0.04 for control, NF01, NF02, and NF03, respectively. The results showed that the nanofiber filtration process efficiently decreased the TA of *neera*. There was no significant difference in TA among the *neera* filtrates, but the filtrates showed a significant difference against the control.

Color and pH

Color and pH are crucial quality indicators, particularly for liquid foods/beverages. In this case, the color values reveal the clarity of *neera* filtrate. L^* values were found to be 9.73 ± 0.12 , 3.56 ± 0.06 , 3.34 ± 0.06 , and 3.28 ± 0.01 for control, NF01, NF02, and NF03, respectively. The results showed that the L^* values were significantly lower in the *neera* filtrates as compared with the fresh *neera* control. This also explains the turbidity reduction in the *neera* filtrates. NF03 showed a lower L^* value followed by NF02 and NF01. There was no significant difference in lightness between NF02 and NF03 *neera* filtrates, both these samples showed significant differences in lightness with NF01 *neera* filtrate. *Neera* filtrates exhibited higher a^* and b^* values. ΔE^* values were found to be 6.22 ± 0.07 , 6.45 ± 0.15 , and 6.51 ± 0.11 for NF01, NF02, and NF03, respectively. Higher ΔE^* of the *neera* filtrates from NF02 and NF03 indicates the high clarity of the *neera* filtrate. There was no significant color difference between NF02 and NF03 *neera* filtrates, both these samples showed significant color differences with NF01 *neera* filtrate.

The pH of the *neera* filtrates was slightly higher than the pH of the fresh *neera* control, indicating that the *neera* filtrate had low acidity as compared with the fresh *neera* (Table 2). NF03 showed lower acidity followed by NF02 and NF01. But there were no significant differences

among the *neera* filtrates. Fuenmayor et al. [41] reported that the pH of the apple juice (3.4 ± 0.1) remained constant after filtration with an electrospun nylon-6 nanofibrous membrane. Similarly, Lemma et al. [44] reported that the pH of beer (4.3 ± 0.1) remained constant after filtration with the electrospun nylon nanofibrous membrane. Battirola et al. [45] reported that no significant differences in the pH of strawberry juice (3.53), raspberry juice (3.33), and whey (4.47) after filtration with a cellulose acetate/cellulose nanofiber membrane.

Total polyphenol content

The fresh *neera* exhibited a higher TPC, whereas *neera* filtrates showed slight reductions. TPC was measured in terms of GAE ($\mu\text{g/ml}$) and was found to be 128.42 ± 1.65 , 128.05 ± 2.35 , 123.51 ± 2.24 , and 123.42 ± 0.59 for control, NF01, NF02, and NF03, respectively. The NF01 *neera* filtrate showed no significant difference with the fresh *neera* (control). Similarly, there was no significant difference between NF02 and NF03 *neera* filtrates. But NF02 and NF03 *neera* filtrates showed significant differences with NF01 *neera* filtrate and the fresh *neera* control. Casano et al. [43] reported that the TPC of pomegranate juice (hesperidin equivalent g/L) was reduced to 1.062 ± 0.02 and 1.177 ± 0.02 from 1.576 ± 0.03 and 1.571 ± 0.03 when filtered through poly(ether ether ketone) and polysulfone membranes, respectively. Fuenmayor et al. [41] observed a significant reduction in the TPC of apple juice after filtration with a nylon-6 nanofibrous membrane and reported a reduction of TPC from 327 ± 3 to 83 ± 3 (ppm gallic acid).

Estimation of minerals

The presence of key minerals highlights the nutritional value of coconut *neera*. Mineral contents such as calcium, magnesium, zinc, sodium, phosphorous, potassium, copper, and manganese were quantified using ICP-OES (Table 3). A

Table 3 List of minerals identified by ICP-OES in the *neera* filtrate (NF02) and the fresh *neera* (control)

Minerals	<i>Neera</i> control ($\mu\text{g/ml}$)	<i>Neera</i> filtrate ($\mu\text{g/ml}$)	Difference between control and filtrate ($\mu\text{g/ml}$)	% Reduction
Cu	0.013 ± 0.000^a	0.010 ± 0.001^b	0.003 ± 0.001	23.08
Mn	0.005 ± 0.001^a	0.003 ± 0.001^b	0.002 ± 0.000	44.44
Mg	0.825 ± 0.031^a	0.732 ± 0.030^b	0.093 ± 0.001	11.27
Zn	0.179 ± 0.007^a	0.176 ± 0.002^a	0.003 ± 0.009	1.68
Na	5.301 ± 0.651^a	3.690 ± 0.112^b	1.611 ± 0.763	30.39
Ca	4.344 ± 0.052^a	4.066 ± 0.062^b	0.279 ± 0.010	6.41
K	20.65 ± 0.660^a	18.675 ± 0.045^b	1.975 ± 0.705	9.56
P	1.158 ± 0.034^a	1.022 ± 0.013^b	0.136 ± 0.021	11.71

Results were expressed as mean \pm SD ($n = 3$); different superscripts of lowercase letters along the mineral content (before and after filtration) represent significant differences at $P < 0.05$ level

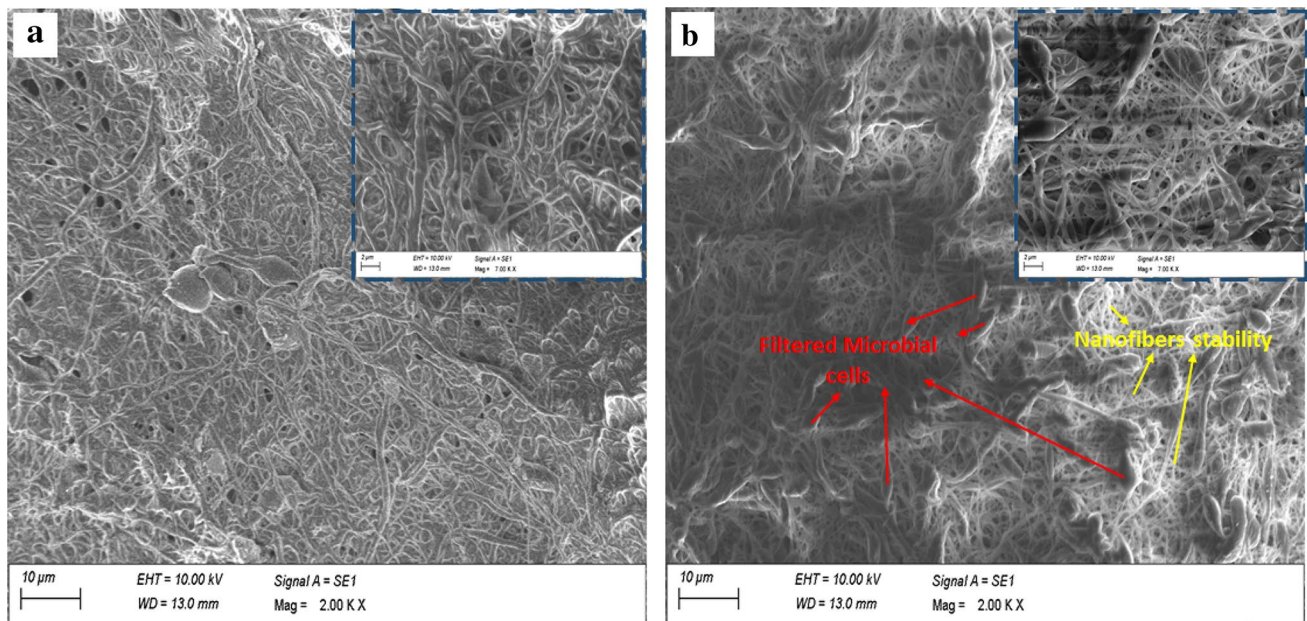


Fig. 3 Nanofiber membrane after the 5th usage **a** just after the filtration and **b** after wash with 70% ethanol (figure inserts at higher (7000 \times) magnification)

minimal reduction in mineral contents was observed after nanofiber filtration. The retention of mineral content is an advantage of the nanomembrane filtration process.

Enumeration of yeasts

Yeast cell load in the *neera* filtrate and the fresh *neera* (control) was estimated to be 1.55×10^6 CFU/ml, 1.07×10^5 CFU/ml, 2.57×10^4 CFU/ml, and 2.38×10^4 CFU/ml for control, NF01, NF02, and NF03, respectively. NF03 nanofibrous membrane showed very low yeast load followed by NF02 and NF01. The yeast cell viability showed significant differences between control and *neera* filtrates. Moreover, NF01 showed significant differences between NF02 and NF03 counterparts. But there was no significant difference between NF02 and NF03. A similar study was reported by Lemma et al. [44], who developed electrospun nylon nanofibrous membranes with a fiber diameter of 197 ± 31 nm and porosity of $\sim 90\%$ and investigated their potential for the removal of bacterial and yeast strains in water and beer. They fortified beer suspensions at different microbial concentrations such as 5.1×10^8 CFU/mL of *Flavobacterium johnsoniae*, 1.0×10^4 CFU/mL of *Iodobacter fluviatilis*, 8.0×10^8 CFU/mL of the mixed cultures (*F. johnsoniae* and *I. fluviatilis*), and 2.9×10^8 CFU/mL of *S. cerevisiae*, and studied the filtration efficiency in removal of these microbial strains. They reported that nylon nanofibrous membranes completely removed yeast (*S. cerevisiae*) and mixed bacterial cultures (*F. johnsoniae* and *I. fluviatilis*); whereas, 3 and 5

log reductions could be achieved in the beer suspensions fortified with *I. fluviatilis* and *F. johnsoniae*, respectively. Bortolassi et al. [42] observed the efficient removal of bacterial cells using the composite-based Ag/PAN nanofiber filtration membrane and reported the reduction of the bacterial load from 10^8 CFU/mL to 10^3 CFU/mL while filtration through the Ag/PAN nanofibrous membrane. In another study, Ma et al. [46] developed functionalized PAN electrospun membranes by a surface modification process for the removal of bacteria and viruses. They reported that surface-modified PAN electrospun membrane showed efficient removal of *Escherichia coli* and MS2 phage at 99.9999% and 99.99%, respectively.

The reusability of the selected nanofiber membrane (NF02) was tested multiple times. At the 5th use, the permeate flow rate was reduced by around 50%. Hence, the yeast count was tested after the 5th usage, and it found that control levels were the same as at the first usage of the membrane. The morphology of the nanofiber membrane just after the 5th usage of filtration (Fig. 3a) shows the deposition of *neera* on the membrane. However, after the washing step, fouling on the membrane was removed, and only yeast cells were retained on the membrane (Fig. 3b). It was evident that the nanofiber membrane was stable even after repeated usage, washing, and sterilization processes. This proves the reusability of the prepared membrane and the stability of nanofibers. Comparing the different sterilization techniques for PCL nanofiber membranes, Horakova et al., (2020) proved that soaking in aqueous

ethanol (70%) for 30 min and UV irradiation for 30 min does not cause any morphological change [48]. This supports the suitability of the selected sterilization technique for the filtration process and reusability of the membrane.

Moreover, with recent advances in the electrospinning technique, large-scale production of nanofibrous membranes is possible [49]. For example, techniques like needleless electrospinning have been proven to be suitable for the mass production of macroscopically homogeneous nanofibrous membranes [48]. Outstanding production capacities of up to 13.7 g/h have been achieved with high curvature using needleless electrospinning [50]. Such advancements in manufacturing techniques allow cost-effective usage of such nanomembranes for filtration applications.

Conclusion

Electrospun nanofibrous membranes were developed using the electrospinning process and used for the filtration of coconut *neera*. The filtration efficiency of nanofibrous membranes (NF01, NF02, and NF03) fabricated under different process conditions was investigated. The NF03 nanofibrous membrane had very fine pores because of the less nanofiber diameter (857 nm) and showed low counts of yeast (2.38×10^4 CFU/ml). But in terms of filtration efficiency, it showed a low permeate flow rate (2.94 ± 0.39 L/h) due to less porosity (69.55%). The NF02 nanofibrous membrane was optimized because of increased porosity (73.26%) and permeate flow rate (6.61 ± 0.94 L/h) while supporting yeast load reduction (2.57×10^4 CFU/ml). Also, it could retain the TPC and showed TSS, TA, pH, and color equivalent to NF03. Hence, the process parameters involved in the fabrication of NF02 membrane are considered as optimized electrospinning parameters. Further, the NF02 nanofibrous membrane showed better retention of minerals and the efficient removal of yeast cells (2 log reduction). Moreover, effective reusability of the nanofibrous membrane was observed for up to 5 usages. Thus, the study confirms the potential of the electrospun nanofibrous membrane for *neera* filtration, quality retention, and shelf-life extension applications.

Authors' contributions M. Maria leena, K.S. Yoha data curation, data analysis, writing—original draft; J.A. Moses supervision, writing—review and editing; C. Anandharamakrishnan conceptualization, supervision, project administration, writing—review and editing.

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Declarations

Conflict of interest The authors declare no conflicts of interest.

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