


Special issue article

Multi-modular engineering of *Saccharomyces cerevisiae* for high-titre production of tyrosol and salidroside

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Summary

Tyrosol and its glycosylated product salidroside are important ingredients in pharmaceuticals, nutraceuticals and cosmetics. Despite the ability of *Saccharomyces cerevisiae* to naturally synthesize tyrosol, high yield from *de novo* synthesis remains a challenge. Here, we used metabolic engineering strategies to construct *S. cerevisiae* strains for high-level production of tyrosol and salidroside from glucose. First, tyrosol production was unlocked from feedback inhibition. Then, transketolase and ribose-5-phosphate ketol-isomerase were overexpressed to balance the supply of precursors. Next, chorismate synthase and chorismate mutase were overexpressed to maximize the aromatic amino acid flux towards tyrosol synthesis. Finally, the competing pathway was knocked out to further direct the carbon flux into tyrosol synthesis. Through a combination of these interventions, tyrosol titres reached

$702.30 \pm 0.41 \text{ mg l}^{-1}$ in shake flasks, which were approximately 26-fold greater than that of the WT strain. *RrU8GT33* from *Rhodiola rosea* was also applied to cells and maximized salidroside production from tyrosol in *S. cerevisiae*. Salidroside titres of $1575.45 \pm 19.35 \text{ mg l}^{-1}$ were accomplished in shake flasks. Furthermore, titres of $9.90 \pm 0.06 \text{ g l}^{-1}$ of tyrosol and $26.55 \pm 0.43 \text{ g l}^{-1}$ of salidroside were achieved in 5 l bioreactors, both are the highest titres reported to date. The synergistic engineering strategies presented in this study could be further applied to increase the production of high value-added aromatic compounds derived from the aromatic amino acid biosynthesis pathway in *S. cerevisiae*.

Introduction

Tyrosol and its glycosylated derivative salidroside (8-O- β -D-glucoside of tyrosol) are widely used in food and medicine industries. For example, tyrosol serves as the precursor for several phenylethanoids (Xue and Yang, 2016; Chung *et al.*, 2017) and anticancer drug candidates (Ahn *et al.*, 2008). Salidroside has anticancer potential (Chen *et al.*, 2016b) and can be used to ameliorate insulin resistance (Zheng *et al.*, 2015) in cardiovascular and cerebrovascular diseases (Tang *et al.*, 2014; Chen *et al.*, 2016a; Zhang *et al.*, 2017a, 2018). Salidroside has also been used in cosmetic industries due to its antioxidant and anti-photoaging properties (Mao *et al.*, 2015).

Currently, tyrosol and salidroside are mainly extracted from plants, such as olive and *Rhodiola* roots, or chemically synthesized. Low extraction efficiency (Mao *et al.*, 2007; Miralles *et al.*, 2015) and dwindling plant resources (Galambosi, 2006; Moyo *et al.*, 2015; Chen *et al.*, 2016c) limit the applications of plant-extraction. Furthermore, chemical synthesis and semi-synthesis of tyrosol and salidroside require expensive substrates that are often not environmentally friendly (Woodburn and Stuntz, 1950; Troshchenko and Yuodvirshis, 1969;

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Delépée *et al.*, 2007). Conversely, microbial biosynthesis provides a sustainable and economically feasible platform for producing natural products originally derived from plants (Lee *et al.*, 2012; Borodina and Nielsen, 2014; Paddon and Keasling, 2014). In recent years, *E. coli* was successfully used to produce tyrosol and salidroside (Satoh *et al.*, 2012; Bai *et al.*, 2014; Chung *et al.*, 2017; Fan *et al.*, 2017; Xue *et al.*, 2017; Liu *et al.*, 2018; Yang *et al.*, 2019). Through these studies, titres of tyrosol achieved using sugar (glucose, or xylose and glucose mixture) as the carbon source, have increased from 69.08 mg l⁻¹ (0.5 mM) to 1.47 g l⁻¹ (Satoh *et al.*, 2012; Liu *et al.*, 2018; Yang *et al.*, 2019). The production of salidroside from sugar increased from 56.90 to 670.58 mg l⁻¹ in shake flasks and to 6.03 g l⁻¹ in a 5 l bioreactor, using a codon-optimized UDP-glycosyltransferase synUgt85a1 from *Arabidopsis thaliana* and adopting a co-culture strategy (Liu *et al.*, 2018).

Yeasts offer a suitable chassis for high-value plant molecule production, due to properties such as the availability of versatile genetic engineering tools and their robustness in large-scale fermentations (Zhang *et al.*, 2015, 2017b; Lian *et al.*, 2018; Xu *et al.*, 2020). *Saccharomyces cerevisiae* is a GRAS (generally regarded as safe) yeast organism that is highly suitable for food, potentially pharmaceutical compound and cosmetic production (Borodina and Nielsen, 2014; Sewalt *et al.*, 2016). The aromatic amino acid synthesis pathway of *S. cerevisiae* was successfully engineered to increase the production of aromatic molecules such as reticuline (Trenchard *et al.*, 2015), p-coumaric acid (Rodriguez *et al.*, 2015), mandelic acid and 4-hydroxymandelic acid (Suastegui *et al.*, 2017). Therefore, the construction of a high-titre tyrosol or salidroside-producing *S. cerevisiae* strain is highly desirable.

In *S. cerevisiae*, tyrosol is produced from the shikimate pathway and the L-tyrosine branch. Erythrose-4-phosphate (E4P) and phosphoenolpyruvate (PEP) are derived from the pentose phosphate pathway (PPP) and glycolysis, respectively, and are condensed by DAHP synthase (encoded by *ARO4* and *ARO3*) into 3-deoxy-D-arabinoheptulosonate-7-phosphate (DAHP; Hazelwood *et al.*, 2008; Suastegui and Shao, 2016). Next, pentafunctional enzyme (encoded by *ARO1*) and chorismate synthase (encoded by *ARO2*) catalyse chorismate synthesis from DAHP. The conversion of chorismate to prephenate is catalysed by the enzyme chorismate mutase (encoded by *ARO7*), followed by conversion of prephenate to 4-hydroxyphenylpyruvate (4-HPP) by prephenate dehydrogenase (encoded by *TYR1*). Phenylpyruvate decarboxylase (encoded by *ARO10*) converts 4-HPP into 4-hydroxyphenylacetaldehyde (4-HPAA). 4-HPAA is reduced by endogenous alcohol dehydrogenases (ADHs) to tyrosol (Fig. 1). Salidroside is produced via the glycosylation of

tyrosol at the 8-OH group, which is catalysed by a regio-specific uridine 5'-diphospho-glucosyltransferase (UGT; Fan *et al.*, 2017). Previous studies increased tyrosol titres to 927.68 ± 25.26 mg l⁻¹ in shake flasks and 8.37 g l⁻¹ in a bioreactor in a haploid industrial *S. cerevisiae* strain HLF-Dα (Jiang *et al.*, 2018; Torrens-Spence *et al.*, 2018; Guo *et al.*, 2019; Guo *et al.*, 2020). The highest salidroside titres reported for engineered *S. cerevisiae* are 239.5 mg l⁻¹ in a shake flask and 1.82 g l⁻¹ in a bioreactor (Jiang *et al.*, 2018; Torrens-Spence *et al.*, 2018; Guo *et al.*, 2020).

In this study, a widely used model organism, *S. cerevisiae* strain CEN.PK2-1C was engineered to produce tyrosol and salidroside. In short, four modules in the pathway for tyrosol production were systematically optimized (Fig. 1). Firstly, *ARO4*^{K229L} and *ARO7*^{G141S} mutations were introduced, which encoded feedback-inhibition-insensitive DAHP synthases and chorismate mutase respectively. Then, *RKI1* and *TKL1* were overexpressed to tune the flux of the precursor pathway. To direct the carbon flux into tyrosol, the genes of the shikimate pathway and the L-tyrosine branch from different species were screened, and competing pathways were blocked by deleting *PHA2* and *PDC1*. Finally, another copy of *ARO4*^{K229L}, *ARO3*^{K222L} and *ARO7*^{G141S} was integrated into the 308a locus to enable preferential production of tyrosol. To produce salidroside, three UDP-glycosyltransferases from diverse species were tested; codon-optimized *RrU8GT33*^{opt} was optimal for the glycosylation of tyrosol. Finally, 9.90 ± 0.06 g l⁻¹ tyrosol and 26.55 ± 0.43 g l⁻¹ salidroside were produced in separate 5 l bioreactors, both presenting the highest titres reported to date. Our study paves the way for further industrial production of tyrosol and salidroside.

Results

Unlocking the carbon flux into the aromatic amino acid pathway

Previous studies showed that the mutations of *ARO4*^{K229L} and *ARO7*^{G141S} could efficiently relieve feedback inhibition and increase the production of phenylethanol and their para-hydroxyl analogues in *S. cerevisiae* (Luttik *et al.*, 2008). To develop a fully integrated and plasmid-free *S. cerevisiae* strain for industrial applications, in the present study, the *in situ* *ARO4*^{K229L} and *ARO7*^{G141S} mutations were performed in CEN.PK2-1C using the PCRCT system (Bao *et al.*, 2015), generating strains LYTY1. After 72 h of fermentation with LYTY1 strains, tyrosol production increased ~ 3-fold compared to that of the WT strain, reaching the titre of 105.10 ± 0.66 mg l⁻¹.

Erythrose-4-phosphate (E4P) derived from the pentose phosphate pathway (PPP) and phosphoenolpyruvate (PEP) produced from glycolysis are starting precursors

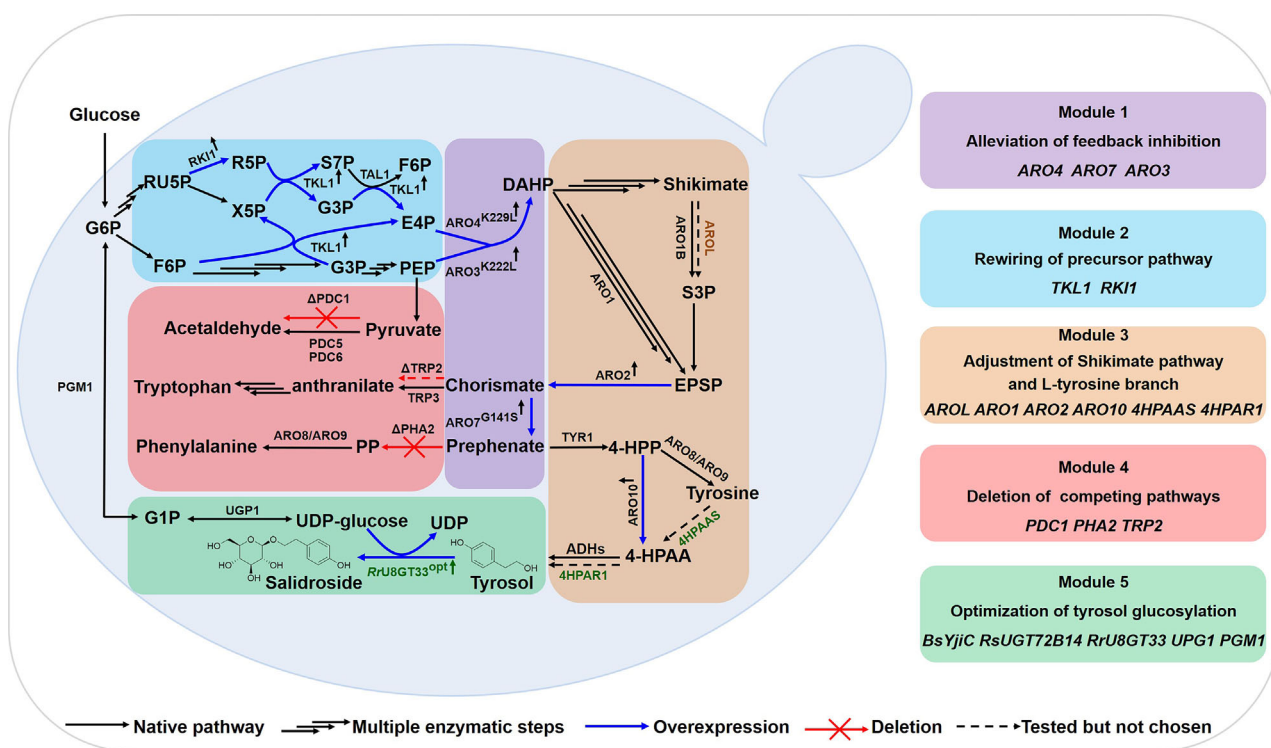


Fig. 1. Schematic representation of the modular engineering strategy for high-level tyrosol and salidoside production in *S. cerevisiae*. The modular engineering strategy consists of alleviation of feedback inhibition (module 1), rewiring of precursor pathway (module 2), adjustment of shikimate pathway and L-tyrosine branch (module 3), deletion of competing pathways (module 4) and optimization of tyrosol glucosylation (module 5). Black arrows represent the native pathways in *S. cerevisiae*; blue bold arrows represent the overexpressed genes in this study; red crosses represent gene deletions; dashed arrows indicate that the reactions were tested but not used in this study and the treble arrows represent multiple enzymatic steps. Native genes of *S. cerevisiae* are shown in black colour; the gene *AROL* from *E. coli* is indicated in orange; the heterologous genes from *Rhodiola rosea* were shown in green. Metabolite abbreviations: G6P: Glucose 6-phosphate; RU5P: D-Ribulose 5-phosphate; X5P: D-Xylulose 5-phosphate; R5P: D-Ribose 5-phosphate; S7P: Sedoheptulose 7-phosphate; G3P: D-Glyceraldehyde 3-phosphate; F6P: beta-D-Fructose 6-phosphate; PEP: phosphoenolpyruvate; E4P: D-Erythrose 4-phosphate; DAHP: 3-deoxy-D-arabino-heptulosonate-7-phosphate; S3P: shikimate-3-phosphate; EPSP: 5-enolpyruvyl-3-shikimate; 4-HPP: p-hydroxyphenylpyruvate; PP: phenylpyruvate; 4-HPAA: 4-hydroxyphenylacetylaldehyde; G1P: Glucose 1-phosphate; UDP: Uridine diphosphate; Gene abbreviations: *RKI1*: ribose-5-phosphate ketol-isomerase1; *TKL1*: transketolase 1; *TAL1*: transaldolase 1; *ARO3^{K222L}/ARO4^{K229L}*: feedback-insensitive DAHP synthases; *ARO1*: pentafunctional aromatic enzyme; *AROL*: shikimate kinase II from *E. coli*; *ARO2*: chorismate synthase; *ARO7^{G141S}*: feedback-insensitive chorismate mutase; *PHA2*: prephenate dehydratase; *TRP2*: anthranilate synthase; *TRP3*: bifunctional anthranilate synthase/indole-3-glycerol-phosphate synthase; *PDC1*: pyruvate decarboxylase 1; *PDC5*: pyruvate decarboxylase 5; *PDC6*: pyruvate decarboxylase 6; *TYR1*: prephenate dehydrogenase; *ARO10*: phenylpyruvate decarboxylase; *ARO8/9*: aromatic amino transferases; *ADHs*: alcohol dehydrogenases; *4HPAAS*: 4-HPAA synthase from *Rhodiola rosea*; *4HPAR1*: 4-HPAA reductase 1 from *Rhodiola rosea*; *RrU8GT33^{opt}*: tyrosol: UDP-glucose 8-O-glucosyltransferase 33 from *Rhodiola rosea*; *PGM1*: Phosphoglycerate mutase 1; *UPG1*: UDP-glucose pyrophosphorylase 1.

for the production of aromatic amino acid-derived compounds in *S. cerevisiae*. Based on the catalytic mechanism of the condensation of PEP and E4P to DAHP (Konig *et al.*, 2004), a 1:1 molar ratio of PEP and E4P seems to promote the biosynthesis of aromatic amino acid derivatives. However, in *S. cerevisiae*, according to the metabolic flux analysis, E4P flux is at least one order of magnitude lower than that of PEP flux (Suastegui *et al.*, 2016). To facilitate the carbon flux afflux in E4P, we first overexpressed *RKI1* under the control of the *TEF1* promoter in strain LYTY1 to generate strain LYTY1R. Strain LYTY1R produced $132.40 \pm 3.52 \text{ mg l}^{-1}$ of tyrosol, increasing 29.78% than that of strain LYTY1. Then, overexpression of *TKL1* in LYTY1R led to about 38.10%

increase in tyrosol production compared to that of strain LYTY1R. (Fig. 2C).

Optimization of the shikimate pathway and the L-tyrosine branch

In *S. cerevisiae*, tyrosol is derived from the shikimate pathway and the subsequent L-tyrosine branch, as shown in Fig. 2B. In the shikimate pathway, a single pentafunctional enzyme (encoded by *ARO1*) catalyses the formation of 5-enolpyruvyl-3-shikimate phosphate (EPSP) from DAHP. Then, the conversion of chorismate from EPSP is catalysed by the *Aro2*. In contrast to *S. cerevisiae*, the formation of EPSP from DAHP is

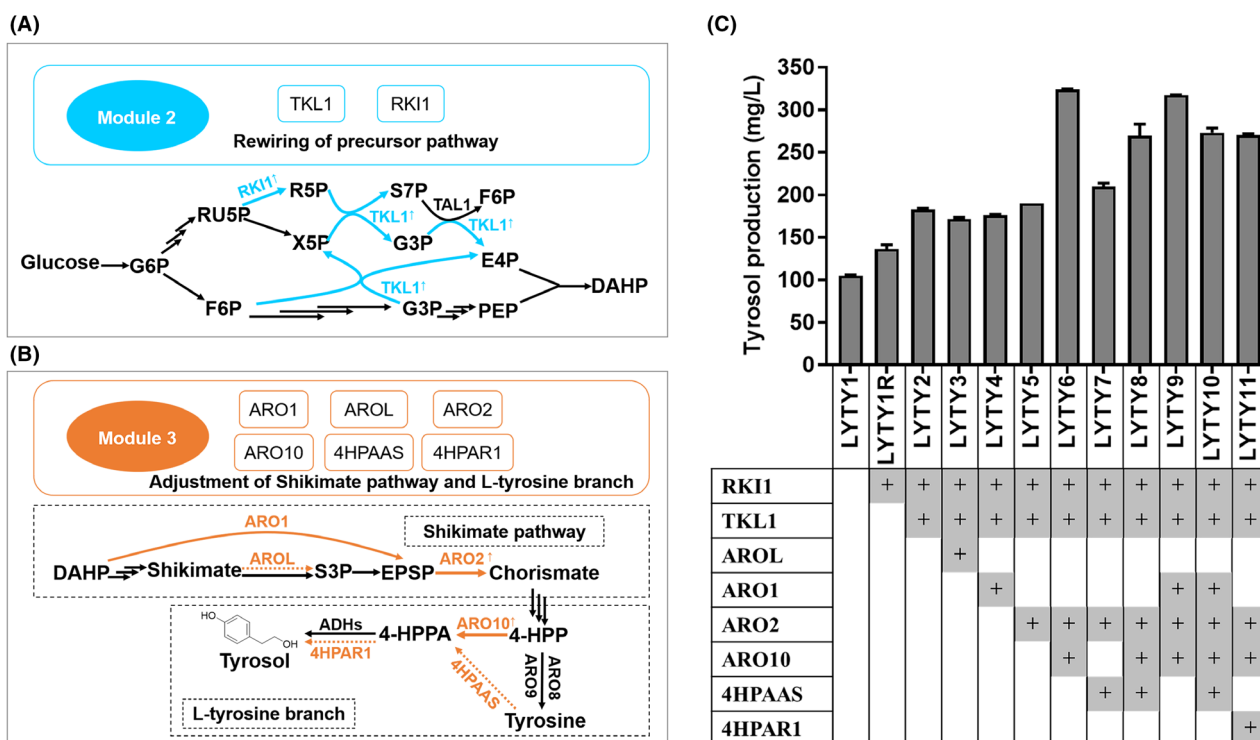


Fig. 2. (A) Schematic illustration of rewiring the metabolic pathway for improving supply of E4P. Cyan arrows represent the overexpressed genes. The abbreviations of metabolites and gene details were shown in Fig. 1. (B) Overview of genetic modifications of Module 3. Module 3 consists of Shikimate pathway and L-tyrosine branch (the dashed boxes). Orange arrows indicate that the actions were tested. See Fig. 1 legend regarding abbreviations of these metabolites. (C) Tyrosol production after engineering of module 2 and module 3. The fermentations were performed at 30 °C in 50 ml YPD medium in shake flasks. Titre of tyrosol was detected after 72 h fermentation. Error bars represent the standard deviation of three biological duplicates.

catalysed by five monofunctional enzymes in *E. coli*. Overexpression of the shikimate kinase II gene *AROL* from *E. coli* or endogenous *ARO1* from *S. cerevisiae* was regarded as a useful strategy to produce high level of shikimate derivatives (Rodriguez *et al.*, 2015). However, by integrating *AROL* or *ARO1* into the 1622b locus (high expression levels were observed when gene cassettes were integrated in this locus; Reider Apel *et al.*, 2017) of strain LYTY2, the titre of tyrosol was marginally decreased (Fig. 2C). These results suggested that methods used to optimize the conversion of DAHP to EPSP did not lead to increased tyrosol production in *S. cerevisiae*. Next, *ARO2* was overexpressed under the control of the *PGK1* promoter (resulting in strain LYTY5), and the titre of tyrosol was slightly greater than that of strain LYTY2.

Tyrosol biosynthesis diverges from the conversion of chorismate in both yeasts and plants. In *S. cerevisiae*, chorismate is first converted into prephenate by Aro7p, then prephenate can be transformed into 4-HPP by Tyr1p. Next, 4-HPP is decarboxylated to 4-HPAA by Aro10p, and alcohol dehydrogenases finally converts 4-HPAA into tyrosol (Fig. 1). In plants, chorismate is

converted into tyrosine over several steps, and then, tyrosine can be directly converted into 4-HPAA by 4-HPAA synthase (encoded by *4HPAAS*). 4-HPAA reductase (encoded by *4HPAR1* and *4HPAR2*) finally converts 4-HPAA into tyrosol (Schenck and Maeda, 2018; Torrens-Spence *et al.*, 2018). To direct flux towards tyrosol, we first overexpressed the endogenous gene *ARO10* and the codon-optimized gene *4HPAAS^{opt}* from *R. rosea* in strain LYTY5, resulting in strains LYTY6 and LYTY7 respectively. The yields of strains LYTY6 and LYTY7 reached 323.90 ± 0.41 and 209.70 ± 2.88 mg l⁻¹, which were approximately 70% and 10% greater compared to that of strain LYTY5. Due to these positive effects, both genes (*ARO10* and *4HPAAS^{opt}*) were overexpressed in strain LYTY5, generating strain LYTY8, which led to the accumulation of 42% more tyrosol than that of the parental LYTY5 but 16% less than that of LYTY6 (Fig. 2C), demonstrating that Aro10p can efficiently convert 4-HPP into 4-HPAA. Furthermore, *ARO1* overexpression in strains LYTY6 and LYTY8 did not lead to increase in tyrosol production (Fig. 2C). Finally, the overexpression of the plant-derived gene *4HPAR1*, which showed high catalytic activity and specificity for

the reduction of 4-HPAA to tyrosol (Torrens-Spence *et al.*, 2018), resulted in decrease in tyrosol production (Fig. 2C). These results indicated that the conversion of DAHP to EPSP and the reduction of 4-HPAA to tyrosol may not be limiting steps in the tyrosol synthetic pathway, whereas the conversion of 4-HPP to 4-HPAA was a rate-limiting step.

Deletion of competing pathways

Pyruvate decarboxylases (encoded by *PDC1*, *PDC5* and *PDC6*) catalyse the decarboxylation of pyruvate to acetaldehyde, which is a competing pathway for the accumulation of PEP and E4P. Disruption of *PDC1* resulted in ~30% lower total pyruvate decarboxylase activity and increased the production of aromatic compound vanillin in *S. cerevisiae* (Brochado *et al.*, 2010). We disrupted *PDC1* in strain LYTY6, generating strain LYTY12, with a yield of $338.72 \pm 0.1 \text{ mg l}^{-1}$. As chorismate serves as a precursor to the biosynthesis of L-tryptophan, L-phenylalanine and L-tyrosine, *TRP2* and *PHA2* were knocked out separately in strain LYTY12 (Fig. 1), yielding strains LYTY13 and LYTY14 respectively. Strain LYTY14 accumulated $522.39 \pm 0.99 \text{ mg l}^{-1}$ tyrosol, which was 54.2% greater than that of strain LYTY12. However, unexpectedly, tyrosol titre was 19.7% less in strain LYTY13 than that of strain LYTY12 (Fig. 3), which could be due to significant growth deficiency caused by the *TRP2* deletion (Fig. S1).

Optimization of tyrosol glycosylation for salidroside production

According to previous studies, salidroside and tyrosol production are positively correlated (Jiang *et al.*, 2018; Liu *et al.*, 2018); therefore, the key aim in this study was to improve the salidroside yield through increasing tyrosol yield. Previous studies have also shown that the addition of a copy of *ARO4*^{K229L}/*ARO7*^{G141S}/*ARO3*^{K222L} under a strong constitutive promoter led to increased aromatic compounds production (Rodriguez *et al.*, 2015; Reifenrath and Boles, 2018). To further increase tyrosol production, a copy of *ARO4*^{K229L}/*ARO7*^{G141S} or *ARO4*^{K229L}/*ARO7*^{G141S}/*ARO3*^{K222L} with strong constitutive promoters (*ARO4*^{K229L} under *TDH3* promoter, *ARO7*^{G141S} under *TEF2* promoter and *ARO3*^{K222L} under *HSP26* promoter) was introduced into LYTY14. However, no viable clones were obtained using this approach. On the other hand, by integrating *ARO4*^{K229L}/*ARO7*^{G141S} or *ARO4*^{K229L}/*ARO7*^{G141S}/*ARO3*^{K222L} with native promoters into 308a locus (Reider Apel *et al.*, 2017) of LYTY14, the tyrosol titres of $653.79 \pm 0.06 \text{ mg l}^{-1}$ (strain LYTY15) or $702.30 \pm 0.41 \text{ mg l}^{-1}$ (strain LYTY16) were obtained, respectively, after 72 h of shake flask cultivation in YPD medium.

Salidroside is produced by the glycosylation of tyrosol at its 8-OH group, which is catalysed by regio-specific uridine 5'-diphospho-glucosyltransferases (UGTs). The *RsUGT72B14* and *RrUGT33* from *Rhodiola*

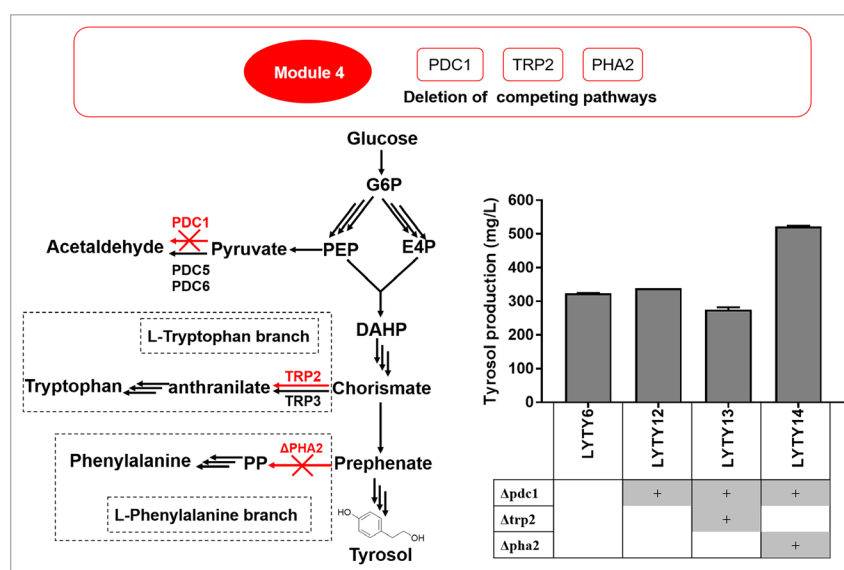


Fig. 3. Effect of *PDC1*, *PHA2* and *TRP2* deletion on tyrosol production. The left schematic represents the competing pathways. The right pane represents the tyrosol production of the modified strains. Titre of tyrosol was produced after 72 h fermentation in 50 ml YPD medium. Error bars represented the standard deviation from three replicates.

sachalinensis and *Rhodiola rosea*, respectively, showed high catalytic efficiencies for salidroside synthesis (Yu *et al.*, 2011; Torrens-Spence *et al.*, 2018). The glycosyltransferase *BsYjC* from *Bacillus subtilis* 168 performs robust glycosylation on a variety of glycosides (Dai *et al.*, 2017). Here, codon-optimized *RsUGT72B14^{opt}*, *RrUGT33^{opt}* and *BsYjC^{opt}* under the control of a strong constitutive *TEF1* promoter were expressed in strain LYTY16, showing more than 20-fold higher transcription levels compared to that of the housekeeping gene *ALG9* (Fig. S2B). Strain SAL3 expressing *RrUGT33^{opt}* produced the highest salidroside titre of $1575.45 \pm 19.35 \text{ mg l}^{-1}$ and presented a conversion rate of approximately 95% (Fig. 4). UDP-glucose is a substrate for tyrosol glycosylation. A previous study showed that overexpression of *PGM1* and *UGP1* together can increase the UDP-glucose accumulation (Zhuang *et al.*, 2017). Thus, *PGM1* and *UGP1* genes were overexpressed in strain SAL3 under *HSP26* and *RAL3* promoters, respectively, yielding strain SAL4. The transcription levels of *PGM1* and *UGP1* genes in strain SAL4 are 1.5-fold higher than those of the WT strain (Fig. S2). However, this strategy led to a salidroside titre of $1560.34 \pm 5.89 \text{ mg l}^{-1}$, which was not significantly different to that of strain SAL3. To our knowledge, this is the highest titre of salidroside reported for shake flask cultures.

Production of Tyrosol and Salidroside in Fed-Batch Fermentation

Until this stage, strain LYTY16 had produced the highest tyrosol titres; therefore, it was used to further promote tyrosol production in a 5-L fed-batch bioreactor. Similarly, strain SAL3 was used for salidroside production by fed-batch fermentation. After the initial glucose was consumed, a carbon restriction strategy was applied to glucose supplementation. The glucose concentration was controlled at $0.5\text{--}5 \text{ g l}^{-1}$ by adjusting the feeding rate. As shown in Fig. 5A, the cell density (OD_{600}) of strain LYTY16 reached approximately 93.4 (the biomass reached about 36.05 g l^{-1}) after 168 h cultivation, and the tyrosol titre consistently increased and finally reached $9.90 \pm 0.06 \text{ g l}^{-1}$. The maximal biomass reached about 42.32 g l^{-1} ($\text{OD}_{600} \approx 109.6$) of strain SAL3 was achieved after 168 h cultivation and the production of salidroside reached up to $26.55 \pm 0.43 \text{ g l}^{-1}$. In addition, $2.12 \pm 0.06 \text{ g l}^{-1}$ tyrosol was produced during the fermentation of strain SAL3 after 168 h (Fig. 5B).

Discussion

Previous studies on tyrosol production in *S. cerevisiae* have mainly focused on the introduction of heterologous pathways, such as plant-derived pathways and bacteria-

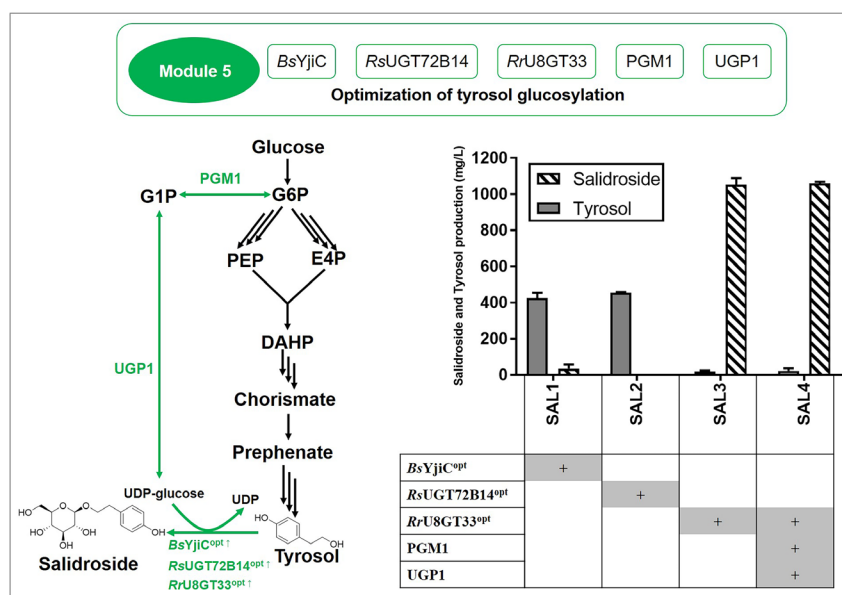


Fig. 4. Production of salidroside (striated bars) and tyrosol (grey bars) after overexpression of different UGTs and native *PGM1* and *UGP1*. The left schematic represents the biosynthesis of salidroside through optimization of tyrosol glycosylation. *BsYjC* from *Bacillus subtilis* 168, *RsUGT72B14* from *Rhodiola sachalinensis* and *RrUGT33* from *Rhodiola rosea* were codon optimized for salidroside synthesis. The right pane represents the salidroside and tyrosol production of the modified strains. The strains were grown in 50 ml YPD medium in shaker flasks at 220 rpm, 30°C. Titres of tyrosol and salidroside were detected after 72 h fermentation. Standard deviations are based on three biological duplicates.

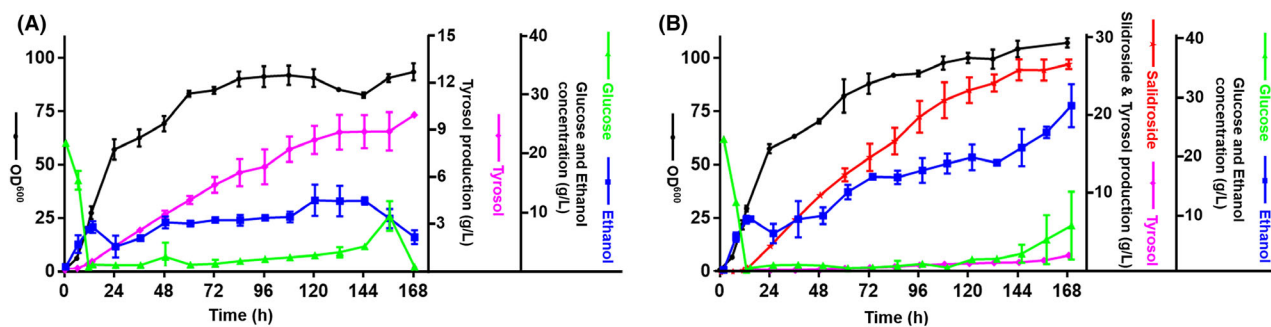


Fig. 5. Fed-batch fermentation for tyrosol and salidroside production. (A) Tyrosol production in 5-l fed-batch bioreactors using engineered strain LYTY16. (B) Salidroside production (red line) of strain SAL3 in 5-l fed-batch bioreactors. The accumulation of low tyrosol titre (purple line) was observed during fed-batch fermentation. Purple lines indicated tyrosol production, red lines indicated salidroside production, black line showed cell densities (OD_{600}), blue lines represented the ethanol production and green lines represented concentration of glucose. The error bars are represented by the standard deviation from two biological replicates.

derived pathways (Jiang *et al.*, 2018; Guo *et al.*, 2019; Guo *et al.*, 2020). Particularly, Guo (Guo *et al.*, 2020) recently increased tyrosol titre ~ 15 -fold compared to that of the WT strain in a haploid industrial strain *S. cerevisiae* strain HLF-D α through introduction of the Xfpk-based pathway, disruption of endogenous genes (*PDC1*, *PHA2* and *TRP3*) and introduction of heterogenous genes (*PcAAS* and *EcTyr^{AM53/A354V}*). In our work, the tyrosol-producing capability of *S. cerevisiae* itself was highly inspired. All modifications in our final tyrosol-producing strain LYTY16 were based on endogenous genes, containing overexpression of endogenous genes *TKL1*, *RK11*, *ARO2*, *ARO10*, *ARO4^{K229L}*, *ARO7^{G141S}* and *ARO3^{K222L}* and disruption of *PDC1* and *PHA2*. As shown in Fig. S2A, the transcription levels of these overexpressed genes are at least 2-fold higher compared to those of the WT strain. Finally, tyrosol titres of $702.30 \pm 0.41 \text{ mg l}^{-1}$ were achieved in an engineered *S. cerevisiae* strain, which were 26-fold higher than those of the WT strain. With bioprocess engineering, the final strain LYTY16 produced $9.90 \pm 0.06 \text{ g l}^{-1}$ tyrosol, which highlights this as a promising platform for further industrial applications.

In our work, *in situ* mutation of *Aro4p^{K229L}* and *Aro7p^{G141S}* in *S. cerevisiae* led to 3-fold increase in tyrosol production. In combination with rewiring the glycolysis pathway and pentose phosphate pathway through overexpression of *Tki1p* and *Rki1p*, the titre of tyrosol was 7-fold compared to that of the WT strain (Fig. 2A). To further increase the tyrosol production and to simplify the fermentation conditions, constitutive promoters were given priority rather than inducible promoters. At first time, we tried several times to overexpress the *ARO4^{K229L}/ARO7^{G141S}* or *ARO4^{K229L}/ARO7^{G141S}/ARO3^{K222L}* under the control of strong constitutive promoters (*ARO4^{K229L}* under *TDH3* promoter, *ARO7^{G141S}* under *TEF2* promoter and *ARO3^{K222L}* under *HSP26* promoter) in the engineered strain LYTY14. Unfortunately, no viable clones were

obtained. A possible explanation for this might be that these manipulations down-regulated some transporter genes. Finally, another copy of feedback-inhibition-insensitive DHP synthase and chorismate mutase (*Aro4p^{K229L}/Aro7p^{G141S}*, or *Aro4p^{K229L}/Aro7p^{G141S}/Aro3p^{K222L}*) was integrated into LYTY14, resulting in about 30% increase in tyrosol production. These results were consistent with previous reports, where overexpression of *Aro4p^{K229L}*, *Aro7p^{G141S}* and *Aro3p^{K222L}* unlocked the production of aromatic amino acid derivatives (Luttik *et al.*, 2008; Bruckner *et al.*, 2018).

It was reported that the overexpression of *ARO1* or *AROL* gene could improve the production of shikimate pathway-derived products in *S. cerevisiae*. For example, *p*-coumaric acid production increased $\sim 50\%$ compared to that of a control strain when *ARO1* or *AROL* were overexpressed (Rodriguez *et al.*, 2015); *para*-hydroxybenzoic acid production also increased $\sim 13\%$ compared to that of the control strain due to *AROL* overexpression (Averesch *et al.*, 2017). However, when the *ARO1* or *AROL* gene was overexpressed in the engineered strain LYTY2 in this study, the transcription level of *ARO1* was more than 20-fold compared to that of the WT strain (Fig. S2A) and the transcription level of *AROL* was 3.5-fold higher than that of the housekeeping gene *ALG9* (Fig. S2B), but the production of tyrosol decreased slightly (Fig. 2C). It seems that the step from DAHP to EPSP may not be a rate-limiting step of the tyrosol biosynthetic pathway in *S. cerevisiae*.

Early engineering of the L-tyrosine branch for tyrosol production in *S. cerevisiae* was performed via a combination with the plant-derived pathway (Jiang *et al.*, 2018; Guo *et al.*, 2019; Guo *et al.*, 2020). In this work, the effect of overexpressing endogenous genes and plant-derived genes on tyrosol production was compared. As a result, the overexpression of endogenous *ARO10* led to higher titres of tyrosol than overexpressing codon-

optimized 4HPAAS^{opt} from *Rhodiola rosea* or co-overexpression of *ARO10* and 4HPAAS^{opt} (Fig. 2). We hypothesized that this result might be attributed to the shortage of L-tyrosine after the combinational overexpression strategy had been conducted. This also indicates that the conversion from 4-HPP to 4-HPAA in *S. cerevisiae* was a rate-limiting step in tyrosol biosynthesis.

The deletion of *PDC1* led to an approximate 5% increase in the tyrosol titre in strains LYTY6, whereas the additional deletion *PHA2* increased above 50% the titre of tyrosol (Fig. 4). Although the deletion of *PHA2* was thought to introduce phenylalanine auxotrophy in *S. cerevisiae* (Urrestarazu *et al.*, 1998), our *pha2* disrupting strains did not result in growth deficiency by culturing in YPD medium. On the contrary, although supplementing enough extra tryptophan (20 mg l⁻¹) to the fermentation medium, deletion of *TRP2* resulted in an obvious growth defect and low tyrosol production (Fig. S1).

Recent studies (Jiang *et al.*, 2018; Guo *et al.*, 2020) showed that glucosyltransferase UGT85a1 from *Arabidopsis thaliana* was used to transform tyrosol to salidroside in *S. cerevisiae*. Nevertheless, in those studies, less than 25% of tyrosol was glycosylated into salidroside through expressing UGT85a1. We screened several reported UGTs, and discovered the best performer, *RrU8GT33* from *Rhodiola rosea*. This strain, achieved 95% and 80% conversion of tyrosol into salidroside in shake flasks and fed-batch fermentation respectively. Finally, in 5-l fed-batch bioreactors, salidroside over-producing strain SAL3 produced 26.55 ± 0.43 g l⁻¹ salidroside, which to our knowledge is the highest level of salidroside production via microbial biosynthesis.

Conclusions

In summary, this study demonstrated that high titres of tyrosol and salidroside can be produced in a widely used model organism *S. cerevisiae* CEN.PK2-1C and the multi-modular engineering strategy increased the tyrosol titre ~ 26-fold over the initial strain CEN.PK2-1C. Two best performing strains LYTY16 and SAL3 produced tyrosol and salidroside at titres of 702.30 ± 0.41 and 1575.45 ± 19.35 mg l⁻¹, respectively, in shake flasks. The strains have the capacity to produce tyrosol and salidroside at titres of 9.90 ± 0.06 and 26.55 ± 0.43 g l⁻¹, respectively, in 5 l fed-batch bioreactors. To our knowledge, these are the highest levels of tyrosol or salidroside production to date in microbial cell factories.

Experimental procedures

Strains and plasmids

Saccharomyces cerevisiae strain CEN.PK2-1C was used for genetic manipulations. All engineered strains used in

Table 1. Strains used in this study.

Strains	Characteristics
BY4741 α	MATa <i>his3Δ1 leu2Δ0 met15Δ0 ura3Δ0</i>
CEN.PK2-1C	MATa <i>ura3-52 his3-Δ1 leu2-3_112 trp1-289, MAL2-8c SUC2</i>
LYTY1	CEN.PK2-1C <i>ARO4^{K229L} ARO7^{G141S}</i>
LYTY1R	LYTY1 <i>ZWF1::P_{TEF1}-RKI1-T_{PGK1} TRP1</i>
LYTY2	LYTY1 <i>ZWF1::P_{HXT7} TKL1-T_{ADH1}-P_{TEF1}-RKI1-T_{PGK1} TRP1</i>
LYTY3	LYTY2 <i>1622b::P_{ENO2}-AROL-T_{TEF1}</i>
LYTY4	LYTY2 <i>URA3::P_{ENO2}-ARO1-T_{TEF1}</i>
LYTY5	LYTY2 <i>URA3::P_{PGK1}-ARO2-T_{GPD}</i>
LYTY6	LYTY2 <i>URA3::P_{PGK1}-ARO2-T_{GPD}-P_{TEF1}-ARO10-T_{PGK1}</i>
LYTY7	LYTY2 <i>URA3::P_{PGK1}-ARO2-T_{GPD}-P_{TEF1}-4HPAAS^{opt}-T_{PGK1}</i>
LYTY8	LYTY2 <i>URA3::P_{PGK1}-ARO2-T_{GPD}-P_{CCW12}-ARO10-T_{ADH1}-P_{TEF1}-4HPAAS^{opt}-T_{PGK1}</i>
LYTY9	LYTY2 <i>URA3::P_{PGK1}-ARO2-T_{GPD}-P_{CCW12}-ARO10-T_{ADH1}-P_{ENO2}-ARO1-T_{TEF1}</i>
LYTY10	LYTY2 <i>URA3::P_{PGK1}-ARO2-T_{GPD}-P_{CCW12}-ARO10-T_{ADH1}-P_{TEF1}-4HPAAS^{opt}-T_{PGK1}-P_{ENO2}-ARO1-T_{TEF1}</i>
LYTY11	LYTY6 <i>1622b::P_{TRP1}-4HPAR1^{opt}-T_{PGK1}</i>
LYTY12	LYTY6 <i>Δpdc1</i>
LYTY13	LYTY6 <i>Δpdc1 Δtrp2</i>
LYTY14	LYTY6 <i>Δpdc1 Δpha2</i>
LYTY15	LYTY6 <i>Δpdc1 Δpha2 308a::P_{ARO4}-ARO4^{K229L}-T_{ARO4}-P_{ARO7}-ARO7^{G141S}-T_{ARO7}</i>
LYTY16	LYTY6 <i>Δpdc1 Δpha2 308a::P_{ARO4}-ARO4^{K229L}-T_{ARO4}-P_{ARO7}-ARO7^{G141S}-T_{ARO7}-P_{ARO3}-ARO3^{K222L}-T_{ARO3}</i>
SAL1	LYTY16 <i>LEU2::P_{TEF1}-YjiC^{opt}-T_{PGK1}</i>
SAL2	LYTY16 <i>LEU2::P_{TEF1}-UGT72B14^{opt}-T_{PGK1}</i>
SAL3	LYTY16 <i>LEU2::P_{TEF1}-RrU8GT33^{opt}-T_{PGK1}</i>
SAL4	LYTY16 <i>LEU2::P_{TEF1}-RrU8GT33^{opt}-T_{PGK1}-P_{HSP26}-PGM1-T_{TDH2}-P_{RAL3}-UPG1-T_{ENO2}</i>

this work are listed in Table 1. *E. coli* strains DH5 α and DH10 β were used for sub-cloning. Plasmids used in this study are listed in Table S1.

All native genes (*TKL1*, *RKI1*, *ARO1*, *ARO2*, *ARO10*, *ARO3*, *ARO4*, *ARO7*, *UPG1*, *PGM1*) were amplified from CEN.PK2-1C genomic DNA. The *AROL* gene was amplified from the genomic DNA of *E. coli* DH5 α . Codon-optimized *RrU8GT33*, *BsYjiC*, *RsUGT72B14*, *4HPAR1* and *4HPAAS* were synthesized by GENEWIZ, China. All promoters and terminators were amplified from *S. cerevisiae* BY4741 genomic DNA except for *ARO4*-promoter, *ARO4*-terminator, *ARO3*-promoter, *ARO3*-terminator, *ARO7*-promoter and *ARO7*-terminator, which were amplified from CEN.PK2-1C genomic DNA. All primers used in this study are listed in Table S2.

DNA manipulations

All native or synthetic genes were first cloned to helper plasmids and then assembled to integrated plasmids (PRS404, PRS405 and PRS406) or PUC19 plasmid to generate integration-cassette plasmids and donor plasmids respectively. First, vector backbone PRS423 was

linearized using restriction enzymes *EcoRI-HF* and *BamHI-HF* (New England Biolabs, US). Adjacent promoters and terminators with the restriction site *PmeI* were cloned into the linearized PRS423 vector, which generated helper plasmids (Table S1). Then, amplified gene fragments were assembled to helper plasmids (digested by *PmeI*), yielding gene-cassette plasmids. Integrated plasmids and donor plasmids were constructed with Gibson assembly by adding corresponding gene-cassette fragments. The pCas plasmid (Ryan *et al.*, 2014) was modified by introducing two *BsaI* sites between HDV ribozyme and sgRNA to generate the pCas-*BsaI* plasmid. All Cas9-gRNA plasmids were constructed using the Golden Gate assembly method (Engler *et al.*, 2009).

Strains construction

All integrated plasmids harbouring gene-overexpression cassette were integrated into chromosomal loci. To integrate plasmid pTYR1 into *ZWF1* loci, pTYR1 was linearized using the restriction enzyme *BamHI-HF*. One microgram of the purified linearized fragment was transformed into yeast using the LiAc/ssDNA/PEG method (Gietz and Schiestl, 2007), and then, yeast were plated on a SC-TRP plate. The integration of other fragments was similar to the integration of linearized pTYR1 except transformants were plated on SC-LEU or SC-URA for selection. Gene-overexpression cassettes of *AROL*, *4HPAR1^{opt}*, *ARO4^{K229L}/ARO7^{G141S}* and *ARO4^{K229L}/ARO7^{G141S}/ARO3^{K222L}* were integrated into specific *S. cerevisiae* chromosomal loci (308a locus or 1622b locus) using a Cas9-based toolkit (Reider Apel *et al.*, 2017). Clones were screened using PCR on yeast colonies with KOD FX PCR mix (Toyobo, Osaka, Japan), which were then verified by DNA sequencing. Deletion of *PHA2*, *PDC1* and *TRP2* was performed using the pCas system (Ryan *et al.*, 2014; Table S2). The specific guide RNA sequences were designed using the CHOPCHOP web tool (<http://crispor.tefor.net>; Labun *et al.*, 2016). All gRNA sequences used in this study are listed in Table S3.

Cultivations and fermentations

Yeast strains were picked from pre-cultured plates and cultured in 2 ml YPD medium (20 g l⁻¹ Peptone, bacteriological (Sangon Biotech#A100636), 10 g l⁻¹ yeast extract and 20 g l⁻¹ dextrose) at 30°C, shaking at 220 rpm for 18 h. Portions of pre-cultured mixture were then transferred into 50 ml YPD medium in 250 ml shake flasks until the OD₆₀₀ value reached approximately 0.2. The strains were cultured at 30°C, shaking at 220 rpm for 72 h. To monitor cell growth, samples fermented for various lengths of time were measured at

600 nm using a spectrophotometer. Samples of 500 µl were collected after 72 h and centrifuged at 5000 rpm for 5 min. The supernatant was stored at -20°C until analysis.

Fed-batch fermentation for tyrosol and salidroside production

Strain LYTY16 was used to produce tyrosol and strain SAL3 was used to produce salidroside. Seed cultures of 250 ml were transferred into 5 l bioreactors (Bailun, China) containing 2.25 l fed-batch medium (20 g l⁻¹ peptone, 20 g l⁻¹ yeast extract and 20 g l⁻¹ glucose) when the OD₆₀₀ of seed cultures reached 5. Fermentation was performed at 30°C; pH was maintained at 5.7 by automated addition of 5 M NaOH. Air flow was set at 2.5 vvm (air volume/working volume min⁻¹) and the dissolved oxygen (dO₂) concentration was controlled above 40% saturation by agitation cascade (400–600 rpm). Glucose solution (600 g l⁻¹) was fed periodically into the fermentation system to maintain the glucose concentration under 5.0 g l⁻¹. To maintain the glucose concentration under 5.0 g l⁻¹, the glucose concentration was monitored every 4 h. After the initial glucose was depleted, the glucose was added to the fermenter at a rate of 3 g l⁻¹ h⁻¹ (initiated at 9.5 h). The supplementary rate of glucose was adjusted to ~0.6 g l⁻¹ h⁻¹ at 32 h and this rate was maintained to the end of the fermentation. Yeast extract (125 ml, 500 g l⁻¹) was added into the bioreactor at 8, 16, 24 and 32 h time points. Cell density, glucose and ethanol concentration were constantly monitored during the fermentation process. One millilitre supernatant of fermentation cultures was stored every four hours at -20°C until analysis.

Analytical methods

Samples were analysed using an Agilent HPLC 1260 series instrument equipped with a Zorbax SB-C18 column (Agilent, 5 µm, 4.6 mm × 250 mm), which was maintained at 30°C. Mobile phase A was 0.05% formic acid in water and solvent D was acetonitrile; the flow rate was 1 ml min⁻¹. The gradient profile was as follows: 10% D (0–20 min), then 5% D from 20 min to 25 min, then a linear gradient from 5% D to 95% D (25–35 min), then hold 95% D for 5 min, finally return to 10% D for 10 min. Tyrosol and salidroside absorbance was detected at 224 nm. Tyrosol (Solarbio, China) and salidroside (Solarbio, China) standards were added to culture medium and used to generate standard curves for metabolite quantification. The R² coefficient for the calibration curve was higher than 0.999. At least three biological replicates were analysed for each strain.

Conflict of interest

The authors have declared the competing financial interests in the form of a pending patent application.

Author contributions

Huayi Liu, Wenhai Xiao and Yunzi Luo designed the experiments. Huayi Liu, Yujuan Tian, Yi Zhou, Yeyi Kan and Tingting Wu performed the experiments. Huayi Liu and Yunzi Luo wrote the manuscript.

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Supporting information

Additional supporting information may be found online in the Supporting Information section at the end of the article.

Fig. S1. (A) Deletion of *TRP2* decreased the cell growth rate of the engineered strain LYTY12. (B). The tyrosol production after adding 20 mg l⁻¹ extra tryptophan to the fermentation medium in strain LYTY13. The strains were cultured in shake flasks at 220 rpm, 30°C with YPD medium, or YPD medium with additional 20 mg l⁻¹ tryptophan. The cell densities were monitored with the spectrophotometer at 600 nm wavelength. Titters of tyrosol were detected after 72 h fermentation. Error bars represented the standard deviation from three replicates.

Fig. S2. (A) The transcription levels of endogenous genes compared to those of the WT strains. (B) The transcription levels of heterogenous genes compared to that of the housekeeping gene *ALG9*. Strains were cultured for 24 h before RNA extraction. The transcription levels of those genes were measured with RT-qPCR, and the housekeeping gene *ALG9* was selected as the reference. The expression level of *ALG9* was set as 1. Error bars represent the standard deviation of three biological replicates.

Table S1. Plasmids used in this study.

Table S2. Primers used in this study.

Table S3. List of the gRNA sequences used for gene deletions, mutations, and insertions via the CRISPR system.