

Article

# Solubility Data of the Bioactive Compound Piperine in (Transcutol + Water) Mixtures: Computational Modeling, Hansen Solubility Parameters and Mixing Thermodynamic Parameters

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**Abstract:** The solubility values and thermodynamic parameters of a natural phytomedicine/nutrient piperine (PPN) in Transcutol-HP (THP) + water combinations were determined. The mole fraction solubilities ( $x_e$ ) of PPN in THP + water combinations were recorded at T = 298.2-318.2 K and p = 0.1 MPa by the shake flask method. Hansen solubility parameters (HSPs) of PPN, pure THP, pure water and THP + water mixtures free of PPN were also computed. The  $x_e$  values of PPN were correlated well with "Apelblat, Van't Hoff, Yalkowsky–Roseman, Jouyban–Acree and Jouyban–Acree–Van't Hoff" models with root mean square deviations of < 2.0%. The maximum and minimum  $x_e$  value of PPN was found in pure THP ( $9.10 \times 10^{-2}$  at T = 318.2 K) and pure water ( $1.03 \times 10^{-5}$  at T = 298.2 K), respectively. In addition, HSP of PPN was observed more closed with that of pure THP. The thermodynamic parameters of PPN were obtained using the activity coefficient model. The results showed an endothermic dissolution of PPN at m = 0.6–1.0 in comparison to other THP + water combinations studied. In addition, PPN dissolution was recorded as entropy-driven at m = 0.8–1.0 compared with other THP + water mixtures evaluated.

**Keywords:** activity coefficient model; bioactive compound; piperine; solubility; solution thermodynamics; Transcutol

# 1. Introduction

Piperine (PPN; Figure 1) is a bioactive alkaloidal phytomedicine/nutrient that is present in the fruits and roots of *Piper nigrum* and *Piper longum* [1,2]. The pungency and bitter taste of pepper are due to the presence of PPN [2]. PPN is a potent bioactive compound, which has been reported to have several therapeutic activities including "anti-metastatic [3], enzyme activity stimulator [4], antimicrobial [5], antifertility [6], hepatoprotective [7], antiulcer [8], antiamoebic [9], antidiarrheal [10], anti-fibrotic [11], antifungal [12], acaricidal [13], anti-inflammatory [14,15], antioxidant [2,16,17] and anticancer activity [2,18]". In addition, PPN has also been reported as a permeation and bioavailability enhancer for several weakly soluble drugs as well as nutrients [1,2,19–21]. The solubilization of phytomedicines/nutrients in co-solvent–water mixtures had significant role in their "isolation, extraction, purification, recrystallization, drug discovery and dosage form design" [22–24]. Therefore, the solubilization of PPN in co-solvent–water mixtures should be studied in order to obtain its application in pharmaceutical and food industries. Transcutol-HP (THP) is a potential co-solvent that is miscible with all proportions of water [24,25]. Its potential in increasing the solubilization of several poorly soluble bioactive compounds including vanillin, reserpine, sinapic acid and apigenin has been very well reported in the literature [24–27]. Some formulation technologies including solid



dosage forms [28,29], emulsion/self-emulsifying formulations [30–32], nanomedicine-based drug delivery systems [33–36] and solid dispersion technology [37] have been studied in order to enhance solubility and bioactivity/bioavailability of PPN. The solubility of PPN in pure solvents including pure water, pure propylene glycol (PG), pure polyethylene glycol-400 (PEG-400) and pure THP at ambient temperature was reported elsewhere [1,30,31]. The solubility and mixing thermodynamic parameters of PPN in twelve different pure solvents including "water, methanol, ethanol, isopropanol, 1-butanol, 2-butanol, ethylene glycol, PG, PEG-400, ethyl acetate, dimethyl sulfoxide and THP" at "T = 298.2-318.2 K" and "p = 0.1 MPa" have also been reported [38]. The solubility data of PPN in water-ethanol and water-surfactant mixtures was also found elsewhere [39-41]. The solubility values of PPN in super critical carbon dioxide ( $CO_2$ ) and near critical  $CO_2$  at different temperatures has also been reported elsewhere [42]. So far, there is no report on PPN solubilization in "THP + water" mixtures at "T = 298.2-318.2 K" and "p = 0.1 MPa". Therefore, in this research, the solubility profile of PPN in various "THP + water" mixtures, including pure water and pure THP at "T = 298.2–318.2 K" and "p = 0.1 MPa" is studied and reported. Mixing thermodynamic parameters of PPN are also computed and reported using an activity coefficient model. The solubility values of PPN reported in this research could be beneficial in "isolation, extraction, purification, recrystallization, drug discovery, pre-formulation studies and dosage form design" of PPN.



Figure 1. Chemical structure of piperine (PPN).

# 2. Results and Discussion

## 2.1. Experimental Solubility Values of PPN and Literature Comparison

The "mole fraction solubility ( $x_e$ )" values of PPN in various "THP + water" combinations including pure water and pure THP at "T = 298.2-318.2 K' and "p = 0.1 MPa" are summarized in Table 1. The solubility values of PPN in pure water and pure THP have been reported [38]. However, its solubility values in "THP + water" mixtures have not been reported elsewhere so far.

The solubility of PPN in pure water at "T = 298.2 K" was recorded as 0.164 mg g<sup>-1</sup> (equivalent to  $x_e = 1.04 \times 10^{-5}$ ) and 10 µg g<sup>-1</sup> (equivalent to  $x_e = 6.31 \times 10^{-7}$ ) by Shao et al. and Veerareddy et al., respectively [30,31]. In addition, the solubility of PPN in water at "T = 291.2 K" was obtained as 40 µg g<sup>-1</sup> (equivalent to  $x_e = 2.53 \times 10^{-6}$ ) by another report [1]. The  $x_e$  value of PPN in pure water at "T = 298.2 K" was calculated as  $1.03 \times 10^{-5}$  in the current research (Table 1). The solubility of PPN in pure THP at "*T* = 298.2 K" was obtained as 185.29 mg g<sup>-1</sup> (equivalent to  $x_e = 8.01 \times 10^{-2}$ ) [31]. The  $x_e$ value of PPN in pure THP at "T = 298.2 K" was calculated as  $7.88 \times 10^{-2}$  in the current research (Table 1). The  $x_e$  values of PPN in pure water and pure THP obtained in the current research were found to be very close to those reported by Shao et al. [31]. However, the  $x_e$  value of PPN in pure water obtained in the current research was found to have deviated much from those reported by Veerareddy et al. and Vasavirama and Upender [1,30]. This deviation could be due to the variation in shaking speed, equilibrium time and analysis method of PPN [1,30,38]. The solubility values of PPN in pure water and pure THP at five different temperatures, i.e., "T = 298.2-318.2 K" have also been reported [38]. The graphical comparison between  $x_e$  and literature solubility values of PPN in pure water and pure THP at "T = 298.2-318.2 K" are summarized in Figure 2A,B, respectively. The data summarized in Figure 2A,B suggested an excellent correlation of  $x_e$  values of PPN with the literature solubility data

of PPN in pure water and pure THP at "T = 298.2-318.2 K". Overall, the experimental solubility values of PPN obtained in the current research were found in good agreement with those reported in the literature. The reliability of the proposed method of solubility measurement was verified by obtaining the  $x_e$  values of another phytomedicine/nutraceutical apigenin in pure THP at T = 298.2 K and T = 318.2 K. The  $x_e$  value of apigenin in pure THP at T = 298.2 K and T = 318.2 K. The  $x_e$  value of apigenin in pure THP at T = 298.2 K and T = 318.2 K was found as  $3.36 \times 10^{-1}$  and  $3.82 \times 10^{-1}$ , respectively, in the literature [27]. The  $x_e$  value of apigenin in pure THP at T = 298.2 K and T = 318.2 K was determined as  $3.33 \times 10^{-1}$  and  $3.84 \times 10^{-1}$ , respectively, in the current research. These results suggested that the  $x_e$  value of apigenin in pure THP obtained using the current technique was very close to those reported in the literature [27]. Therefore, the present technique of solubility measurement was reliable for the solubility determination of PPN.

т	<i>T</i> = 298.2 K	<i>T</i> = 303.2 K	$x_{\rm e}$ T = 308.2 K	<i>T</i> = 313.2 K	<i>T</i> = 318.2 K
0.0	$1.03 \times 10^{-5}$	$1.17 \times 10^{-5}$	$1.31 \times 10^{-5}$	$1.47 \times 10^{-5}$	$1.59 \times 10^{-5}$
0.1	$2.57 \times 10^{-5}$	$2.85 \times 10^{-5}$	$3.19 \times 10^{-5}$	$3.55 \times 10^{-5}$	$3.80 \times 10^{-5}$
0.2	$6.20  imes 10^{-5}$	$6.88 \times 10^{-5}$	$7.61 \times 10^{-5}$	$8.40  imes 10^{-5}$	$9.01 \times 10^{-5}$
0.3	$1.59 \times 10^{-4}$	$1.71 \times 10^{-4}$	$1.86  imes 10^{-4}$	$1.99 \times 10^{-4}$	$2.15 \times 10^{-4}$
0.4	$3.71 \times 10^{-4}$	$4.07 \times 10^{-4}$	$4.42 \times 10^{-4}$	$4.79  imes 10^{-4}$	$5.09 \times 10^{-4}$
0.5	$9.06  imes 10^{-4}$	$9.80  imes 10^{-4}$	$1.08 \times 10^{-3}$	$1.16 \times 10^{-3}$	$1.25 \times 10^{-3}$
0.6	$2.23 \times 10^{-3}$	$2.39 \times 10^{-3}$	$2.56 \times 10^{-3}$	$2.74 \times 10^{-3}$	$2.88 \times 10^{-3}$
0.7	$5.40 \times 10^{-3}$	$5.74 \times 10^{-3}$	$6.10 \times 10^{-3}$	$6.51 \times 10^{-3}$	$6.80 \times 10^{-3}$
0.8	$1.35 \times 10^{-2}$	$1.40 \times 10^{-2}$	$1.47 \times 10^{-2}$	$1.55 \times 10^{-2}$	$1.63 \times 10^{-2}$
0.9	$3.26 \times 10^{-2}$	$3.37 \times 10^{-2}$	$3.53 \times 10^{-2}$	$3.70 \times 10^{-2}$	$3.87 \times 10^{-2}$
1.0	$7.88 \times 10^{-2}$	$8.12 \times 10^{-2}$	$8.44 \times 10^{-2}$	$8.79 \times 10^{-2}$	$9.10 \times 10^{-2}$
x <sup>idl</sup>	$5.13  imes 10^{-2}$	$6.02 \times 10^{-2}$	$7.06\times10^{-2}$	$8.26\times10^{-2}$	$9.63  imes 10^{-2}$

**Table 1.** Experimental solubilities ( $x_e$ ) of piperine (PPN) in mole fraction in different "Transcutol-HP (THP) + water" mixtures (*m*) at "*T* = 298.2–318.2 K" and "*p* = 0.1 MPa" <sup>a</sup>.

<sup>a</sup> The relative uncertainties  $u_r$  are  $u_r(T) = 0.010$ ,  $u_r(m) = 0.001\%$ , u(p) = 0.003 and  $u_r(x_e) = 0.11$ .



**Figure 2.** Comparison of mole fraction solubility of PPN in (**A**) pure water and (**B**) pure Transcutol-HP (THP) with reported solubilities at "T = 298.2 K to 318.2 K"; the symbol shows the experimental mole fraction solubility of PPN in (**A**) pure water and (**B**) pure THP, and the symbol shows the reported solubilities of PPN in (**A**) pure water and (**B**) pure THP taken from reference [38].

As per the results summarized in Table 1, the  $x_e$  values of PPN were found to increase with increases in both THP mass fraction (*m*) in various "THP + water" combinations and temperature, and therefore the minimum  $x_e$  value of PPN was obtained in pure water ( $x_e = 1.03 \times 10^{-5}$ ) at "T = 298.2 K", and the maximum  $x_e$  value of PPN was observed in pure THP ( $x_e = 9.10 \times 10^{-2}$ ) at "T = 318.2 K". The maximum  $x_e$  value of PPN in pure THP could be due to the lower polarity and low Hansen solubility parameter (HSP) of THP in comparison to high polarity and higher HSP of water [25,26]. The impact of *m* value of THP on PPN solubility at "T = 298.15-318.15 K" is summarized in Figure 3.



**Figure 3.** Effect of mass fraction of THP (*m*) on solubility of PPN at "T = 298.2-318.2 K".

As per these results, the PPN solubility was found to increase linearly with increases in m values of THP at all five temperatures studied. It was also observed that the  $x_e$  values of PPN were significantly enhanced from pure water to pure THP, and therefore THP could be utilized as an excellent co-solvent in PPN solubility enhancement.

## 2.2. Hansen Solubility Parameters (HSPs)

The results of HSPs of different "THP + water" systems free of PPN are tabulated in Supplementary Materials Table S1. The HSP ( $\delta$ ) value of PPN was computed as 22.30 MPa<sup>1/2</sup>. The HSP value for pure THP ( $\delta_1$ ) and pure water ( $\delta_2$ ) were computed as 21.40 and 47.80 MPa<sup>1/2</sup>, respectively. The HSP values for various "THP + water" mixtures free of PPN ( $\delta_{mix}$ ) were computed as 24.04–45.16 MPa<sup>1/2</sup>. As per the data recorded, the HSP value of pure THP ( $\delta_2 = 21.40 \text{ MPa}^{1/2}$ ) and "THP + water" mixtures (at m = 0.9;  $\delta_{mix} = 24.04 \text{ MPa}^{1/2}$ ) were found to close to that of PPN ( $\delta = 22.30 \text{ MPa}^{1/2}$ ). The  $x_e$  values of PPN were also obtained at the maximum in pure THP and at m = 0.9 of THP in "THP + water" mixtures. Hence, the obtained solubility data of PPN in various "THP + water" mixtures was in good agreement with their HSPs

## 2.3. Mixing Thermodynamic Parameters of PPN Solution

The computed values of various mixing thermodynamic parameters such as "mixing Gibbs energy  $(\Delta_{mix}G)$ , mixing enthalpy  $(\Delta_{mix}H)$  and mixing entropy  $(\Delta_{mix}S)$ " along with activity coefficients  $(\gamma_i)$  for PPN in different "THP + water" combinations including pure water and pure THP are given in Supplementary Materials Table S2. The  $\Delta_{mix}G$  values for PPN at m = 0.6-1.0 were found as negative values, which decreased with the increase in temperature. Hence, PPN dissolution was proposed as endothermic at m = 0.6-1.0. The  $\Delta_{mix}S$  values for PPN at m = 0.8-1.0 were found as positive values,

which also decreased with increases in temperature. Therefore, PPN dissolution was proposed as entropy-driven at m = 0.8-1.0. The  $\Delta_{mix}H$  values for PPN were found as negative values in most of the "THP + water" combinations studied.

#### 2.4. Solute–Solvent Molecular Interactions

The data of  $\gamma_i$  for PPN in different "THP + water" combinations including pure water and pure THP at "T = 298.2-318.2 K" is summarized in Table 2. The  $\gamma_i$  value obtained for PPN was highest in pure water at all five temperatures studied. However, the  $\gamma_i$  value obtained for PPN was lowest in pure THP at all five temperatures. The highest  $\gamma_i$  value for PPN in pure water could be possible due to the lowest  $x_e$  value of PPN in pure water. As per these results, the  $\gamma_i$  value for PPN was found to increase with increases in temperature in all "THP + water" mixtures studied. Based on these results, the maximum solute–solvent interactions were considered in PPN–THP compared with PPN–water.

111	γì								
m	T = 298.2  K	T = 303.2  K	T = 308.2  K	T = 313.2  K	T = 318.2  K				
0.0	4980.00	5150.00	5380.00	5620.00	6050.00				
0.1	1995.20	2108.92	2215.74	2339.59	2533.27				
0.2	827.00	875.00	927.00	984.00	1070.00				
0.3	322.00	353.00	380.00	416.00	448.00				
0.4	138.00	148.00	160.00	173.00	189.00				
0.5	56.60	61.40	65.50	71.40	77.30				
0.6	23.00	25.20	27.60	30.20	33.40				
0.7	5.40	5.74	6.10	6.51	6.80				
0.8	3.81	4.31	4.82	5.33	5.92				
0.9	1.57	1.79	2.00	2.23	2.49				
1.0	0.65	0.74	0.83	0.94	1.06				

**Table 2.** Activity coefficients ( $\gamma_i$ ) of PPN in different "THP + water" mixtures (*m*) at "T = 298.2–318.2 K".

## 2.5. Modeling of PPN Solubility

The solubility data obtained for PPN was correlated using "Van't Hoff, Apelblat, Yalkowsky–Roseman, Jouyban–Acree and Jouyban–Acree–Van't Hoff" models [26,43–48]. Results of the "Van't Hoff model" for PPN in different "THP + water" mixtures including pure water and pure THP are summarized in Table 3.

**Table 3.** Results of "Van't Hoff model" for PPN in "THP + water" combinations  $(m)^{b}$ .

т	а	b	$R^2$	<i>RMSD</i> (%)	Overall RMSD (%)
0.0	-4.45	-2093.60	0.9960	1.11	
0.1	-4.20	-1897.30	0.9963	0.91	
0.2	-3.65	-1799.00	0.9973	0.70	
0.3	-3.98	-1421.50	0.9982	0.33	
0.4	-2.83	-1509.30	0.9968	0.62	
0.5	-1.90	-1520.50	0.9981	0.77	0.65
0.6	-1.95	-1238.70	0.9985	0.42	
0.7	-1.49	-1112.00	0.9973	0.42	
0.8	-1.24	-916.75	0.9935	0.56	
0.9	-0.64	-829.34	0.9932	1.01	
1.0	-0.21	-696.21	0.9960	0.31	

<sup>b</sup> The average relative uncertainties are u(a) = 0.30 and u(b) = 0.07.

The graphical correlation between  $x_e$  and "Van't Hoff model solubility ( $x^{Van't}$ )" of PPN is presented in Supplementary Materials Figure S1, which shows good graphical correlation. The root mean square deviations (*RMSDs*) for PPN in various "THP + water" combinations including pure water and pure THP were recorded as 0.31-1.11% with an average *RMSD* of 0.65%. In addition, the determination coefficients ( $R^2$ ) were obtained as 0.9935-0.9985.

The results of the "Apelblat model" for PPN in different "THP + water" mixtures including pure water and pure THP are summarized in Table 4.

т	Α	В	С	<i>R</i> <sup>2</sup>	RMSD (%)	Overall <i>RMSD</i> (%)
0.0	331.19	-17,505.00	-49.84	0.9995	0.78	
0.1	224.66	-12,407.50	-33.98	0.9982	0.73	
0.2	217.93	-11,974.50	-32.90	0.9993	0.58	
0.3	-105.09	3214.87	15.01	0.9988	0.57	
0.4	228.14	-12,114.70	-34.29	0.9999	0.60	
0.5	45.42	-3697.43	-7.02	0.9981	0.45	0.54
0.6	87.58	-5351.77	-13.29	0.9991	0.34	
0.7	84.34	-5054.78	-12.74	0.9981	0.44	
0.8	-157.86	6268.79	23.26	0.9978	0.61	
0.9	-157.97	6388.73	23.36	0.9985	0.45	
1.0	-84.70	3179.61	12.54	0.9982	0.47	

**Table 4.** Results of "Apelblat model" for PPN in "THP + water" combinations  $(m)^{c}$ .

<sup>c</sup> The average relative uncertainties are u(A) = 0.92, u(B) = 1.54 and u(C) = 0.90.

The graphical correlation between  $x_e$  and "Alelblat model solubility  $(x^{Apl})$ " values of PPN are presented in Figure 4, which expressed good graphical correlation.



**Figure 4.** Correlation of experimental solubility values of PPN with "Apelblat model" in different "THP + water" mixtures at "T = 298.2–318.2 K"; Apelblat model solubility values of PPN are represented by solid lines, and experimental solubility values of PPN are represented by the symbols.

The *RMSD*s for PPN in various "THP + water" combinations including pure water and pure THP were estimated as 0.34-0.78% with an average *RMSD* of 0.54%. In addition, the  $R^2$  values were estimated as 0.9978-0.9999.

Results of the "Yalkowsky–Roseman model" for PPN in different "THP + water" combinations are listed in Table 5. The *RMSD* values for PPN in different "THP + water" combinations were computed as 0.46–2.81% with an average *RMSD* of 1.24%.

m -			Overall				
	<i>T</i> = 298.2 K	<i>T</i> = 303.2 K	<i>T</i> = 308.2 K	<i>T</i> = 313.2 K	<i>T</i> = 318.2 K	* KMSD (%)	RMSD (%)
0.1	-4.59	-4.54	-4.50	-4.45	-4.42	1.21	
0.2	-4.21	-4.16	-4.12	-4.07	-4.04	0.46	
0.3	-3.82	-3.77	-3.74	-3.69	-3.67	2.81	
0.4	-3.43	-3.39	-3.35	-3.32	-2.29	0.91	
0.5	-3.04	-3.01	-2.97	-2.94	-2.91	2.27	1.24
0.6	-2.65	-2.62	-2.59	-2.56	-2.54	1.11	
0.7	-2.26	-2.24	-2.21	-2.18	-2.16	0.38	
0.8	-1.88	-1.85	-1.83	-1.81	-1.79	1.31	
0.9	-1.49	-1.47	-1.45	-1.43	-1.41	0.78	

**Table 5.** Results of "Yalkowsky–Roseman model" for PPN in different "THP + water" mixtures (m) at "T = 298.2-318.2 K".

Results of the "Jouyban–Acree model" for PPN in "THP + water" mixtures are listed in Table 6. The average *RMSD* for PPN was estimated as 0.42%.

**Table 6.** Results of "Jouyban–Acree" and "Jouyban–Acree–Van't Hoff" models for PPN in "THP + water" combinations.

System	Jouyban-Acree	Jouyban–Acree–Van't Hoff
		A <sub>1</sub> -0.21
PEG-400 + water	$J_i - 14.43$	$B_1$ -696.21
		$A_2 - 4.45$
		<i>B</i> <sub>2</sub> –2093.60
		$J_{i}$ -16.42
<i>RMSD</i> (%)	0.42	
		0.54

Results of the "Jouyban–Acree–Van't Hoff model" for PPN in "THP + water" mixtures are tabulated in Table 6. The average *RMSD* for PPN was estimated as 0.54%.

As per the results recorded for solubility modeling, it was observed that all investigated models showed low *RMSDs* (average *RMSD* < 2.0%), which indicated good correlation of obtained solubility data of PPN with all investigated models. However, it should be noted that the error values of every model could not be compared with each other as each model was related with different parameters and model coefficients [49]. In general, the performance of all investigated models was good, but the "Jouyban–Acree model" could be considered as the most suitable model because it utilized the least number of model coefficients in addition to having a low *RMSD* value.

## 3. Experimental

#### 3.1. Materials

PPN and THP were procured from "Beijing Mesochem Technology Co. Pvt. Ltd. (Beijing, China)" and "Gattefosse (Lyon, France)", respectively. Water was collected from a Milli-Q water purification unit. The properties of materials are listed in Table 7.

Material	Molecular Formula	Molar Mass (g mol <sup>-1</sup> )	CAS Registry No	Purification Method	Mass Fraction Purity	Analysis Method	Analysis Method	Source
PPN	C <sub>17</sub> H <sub>19</sub> NO <sub>3</sub>	285.34	94-62-2	None	>0.99	HPLC	HPLC	Sigma Aldrich
THP Water	$\begin{array}{c} C_6H_{14}O_3\\ H_2O \end{array}$	134.17 18.07	111-90-0 7732-18-5	None None	>0.99 -	GC -	GC -	Gattefosse Milli-Q

**Table 7.** List of materials used.

Purity and method of analysis were provided by supplier of each material.

#### 3.2. PPN Solubility Measurement

A well-known saturation shake flask method was applied to measure the solubility of PPN in various "THP + water" combinations (m = 0.1–0.9) including pure water (m = 0.0) and pure THP (m = 1.0) [50]. This study was performed at "T = 298.2–318.2 K" and "p = 0.1 MPa", and each study was repeated at least for three times. Excess PPN powder was taken into glass vials having 1.0 g of each "THP + water" mixtures including pure solvents. All the prepared samples were transferred to a "OLS 200 Grant Scientific Biological Shaker (Grant Scientific, Cambridge, UK)" after temperature and shaker speed settings. After equilibrium, the samples were removed from the shaker, centrifuged and diluted using methanol (mobile phase) and utilized for the determination of PPN content using the reported high-performance liquid chromatography method at 254 nm [38]. The amount of PPN in each sample was determined using a calibration curve of PPN. The  $x_e$  values of PPN were calculated using Equations (1) and (2) [26,27]:

$$x_{\rm e} = \frac{m_1/M_1}{m_1/M_1 + m_2/M_2} \tag{1}$$

$$x_{\rm e} = \frac{m_1/M_1}{m_1/M_1 + m_2/M_2 + m_3/M_3} \tag{2}$$

Here,  $m_1$  = PPN mass;  $m_2$  = THP mass;  $m_3$  = water mass;  $M_1$  = PPN molar mass;  $M_2$  = THP molar mass and  $M_3$  = water molar mass. PPN solubility in pure water and pure THP was computed by applying Equation (1). PPN solubility in "THP + water" mixtures was calculated using Equation (2).

#### 3.3. Computation of HSPs

If the solubility parameter of the solute is close to that of pure solvents or cosolvent mixtures, the solubility of solute will be higher in that particular pure solvent or cosolvent mixtures [51]. Therefore, HSPs for PPN, pure THP, pure water and various "THP + water" mixtures free of PPN were computed in this research. The  $\delta$  value for PPN, pure THP and pure water was computed by applying Equation (3) [49,51,52] as follows:

$$\delta^2 = \delta_d^2 + \delta_p^2 + \delta_h^2 \tag{3}$$

in which " $\delta$  = total HSP;  $\delta_d$  = dispersion HSP;  $\delta_p$  = polar HSP and  $\delta_h$  = hydrogen-bonded HSP". The HSPs for PPN, pure THP and pure water were estimated using "HSPiP software (version 4.1.07, Louisville, KY, USA)" [51]. The HSPs of various "THP + water" mixtures free of PPN ( $\delta_{mix}$ ) were calculated using Equation (4) [26,53] as follows:

$$\delta_{\min} = \alpha \,\delta_1 + (1 - \alpha)\delta_2 \tag{4}$$

Here,  $\alpha$  = volume fraction of THP in "THP + water" mixtures;  $\delta_1$  = HSP of pure THP and  $\delta_2$  = HSP of pure water.

## 3.4. Mixing Thermodynamics Parameters of PPN Solution

Different mixing thermodynamic parameters of PPN solution were computed using the "Lewis–Randall rule". For an ideal solution, different mixing thermodynamic parameters such as "mixing Gibbs energy ( $\Delta_{mix}G^{id}$ ), mixing entropy ( $\Delta_{mix}S^{id}$ ) and mixing enthalpy ( $\Delta_{mix}H^{id}$ )" in different "THP + water" mixtures including pure water and pure THP can be calculated using Equations (5)–(7) [54,55] as follows:

$$\Delta_{\min} G^{id} = RT \left( x_1 \ln x_1 + x_2 \ln x_2 + x_3 \ln x_3 \right)$$
(5)

$$\Delta_{\min} S^{id} = -R \left( x_1 \ln x_1 + x_2 \ln x_2 + x_3 \ln x_3 \right)$$
(6)

$$\Delta_{\rm mix} H^{\rm id} = 0 \tag{7}$$

Here, R = universal gas constant (R = 8.314 J/mol/K);  $x_1$  = PPN mole fraction;  $x_2$  = THP mole fraction and  $x_3$  = water mole fraction.

For a non-ideal solution, various mixing thermodynamic parameters such as  $\Delta_{mix}G$ ,  $\Delta_{mix}H$  and  $\Delta_{mix}S$  in different "THP + water" mixtures including pure water and pure THP can be calculated using Equations (8)–(10) [54–56] as follows:

$$\Delta_{\rm mix}G = \Delta_{\rm mix}G^{\rm id} + G^{\rm E} \tag{8}$$

$$\Delta_{\rm mix}H = \Delta_{\rm mix}H^{\rm id} + H^{\rm E} \tag{9}$$

$$\Delta_{\rm mix}H = \Delta_{\rm mix}H^{\rm id} + H^{\rm E} \tag{10}$$

Here,  $G^{E}$  = excess Gibbs energy and  $H^{E}$  = excess enthalpy. The  $G^{E}$  and  $H^{E}$  values were computed using the activity coefficient-based Wilson model by applying Equations (11) and (12) [56,57] as follows:

$$G^{E} = RT \left( x_{1} \ln \gamma_{i} + x_{2} \ln \gamma_{i} + x_{3} \ln \gamma_{i} \right)$$
(11)

$$H^{\rm E} = -T^2 \left[ \partial \left( \frac{G^{\rm E}/T}{\partial T} \right) \right] \tag{12}$$

The  $\gamma_i$  value for PPN in different THP + water combinations including pure water and pure THP was calculated by applying Equation (13) [58–60] as follows:

$$\gamma_{\rm i} = \frac{x^{\rm idl}}{x_{\rm e}} \tag{13}$$

Here,  $x^{idl}$  = ideal solubility of PPN which was computed using Equation (14) [58] as follows:

$$\ln x^{\rm idl} = \frac{-\Delta H_{\rm fus}(T_{\rm fus} - T)}{RT_{\rm fus}T} + \left(\frac{\Delta C_{\rm p}}{R}\right) \left[\frac{T_{\rm fus} - T}{T} + \ln\left(\frac{T}{T_{\rm fus}}\right)\right] \tag{14}$$

Here,  $\Delta C_p$  = difference between the molar heat capacity of solid state and liquid state;  $T_{\text{fus}}$  = fusion temperature of PPN and  $\Delta H_{\text{fus}}$  = fusion enthalpy of PPN [59,61]. The values of  $T_{\text{fus}}$ ,  $\Delta H_{\text{fus}}$  and  $\Delta C_p$  for PPN were taken as 404.88 K, 32.69 kJ mol<sup>-1</sup> and 80.74 J mol<sup>-1</sup> K<sup>-1</sup>, respectively, from reference [38].

### 3.5. Solute–Solvent Molecular Interactions

The molecular interactions between PPN and various "THP + water" mixtures including pure water and pure THP can be explained using activity coefficients values. The  $\gamma_i$  values for PPN in different "THP + water" mixtures and pure solvents at "*T* = 298.2–318.2 K" were calculated by applying Equation (13) listed above.

#### 3.6. Thermodynamics-Based Computational Models

The solubility value obtained in the current research for PPN in various "THP + water" combinations including pure solvents was correlated using "Van't Hoff, Apelblat, Yalkowsky–Roseman, Jouyban–Acree and Jouyban–Acree–Van't Hoff" models [26,43–48]. The  $x^{Van't}$  value of PPN in different "THP + water" mixtures including pure water and pure THP was calculated by applying Equation (15) [26] as follows:

$$\ln x^{\operatorname{Van't}} = a + \frac{b}{T} \tag{15}$$

in which *a* and *b* = model coefficients of Equation (15), which were determined by the graphs constructed between  $\ln x_e$  of PPN and 1/T. The correlation between  $x_e$  and  $x^{Van't}$  values of PPN was carried out using *RMSD* and  $R^2$ . The *RMSD*s of for PPN were calculated using its formula reported previously in the literature [27]. The  $x^{Apl}$  value of PPN in various "THP + water" combinations including pure water and pure THP was calculated using Equation (16) [43,44].

$$\ln x^{\rm Apl} = A + \frac{B}{T} + C\ln(T) \tag{16}$$

Here, *A*, *B* and *C* = the model coefficients of Equation (16), which were obtained using "nonlinear multivariate regression analysis" of  $x_e$  values of PPN summarized in Table 1 [26]. The correlation between  $x_e$  and  $x^{Apl}$  values of PPN was again performed using *RMSD* and  $R^2$ . The logarithmic solubility of "Yalkowsky–Roseman model (log  $x^{Yal}$ )" for PPN in various "THP + water" mixtures was calculated by applying Equation (17) [45] as follows:

$$\log x^{\rm Yal} = m_1 \log x_1 + m_2 \log x_2 \tag{17}$$

Here,  $x_1$  = mole fraction solubility of PPN in THP;  $x_2$  = mole fraction solubility of PPN in water;  $m_1$  = THP mass fraction and  $m_2$  = water mass fraction.

The "Jouyban–Acree model solubility  $(x_{m,T})$ " of PPN in different "THP + water" combinations was calculated by applying Equation (18) [62–64] as follows:

$$\ln x_{m,T} = m_1 \ln x_1 + m_2 \ln x_2 + \left[\frac{m_1 m_2}{T} \sum_{i=0}^2 J_i(m_1 - m_2)\right]$$
(18)

Here,  $J_i$  = model coefficient of Equation (18) which was obtained using "no-intercept regression analysis" [65,66]. Based on the current data set, the trained version of Equation (18) can be expressed using Equation (19).

$$\ln x_{m,T} = m_1 \ln x_1 + m_2 \ln x_2 + \frac{-14.43m_1 m_2}{T}$$
(19)

The correlation between  $x_e$  and  $x_{m,T}$  of PPN was conducted using *RMSD*. The "Jouyban–Acree–Van't Hoff model solubility of PPN ( $x_{m,T}$ )" in different "THP + water" combinations was calculated by applying Equation (20) [26,66] as follows:

$$\ln x_{m,T} = m_1 \left( A_1 + \frac{B_1}{T} \right) + m_2 \left( A_2 + \frac{B_2}{T} \right) + \left[ \frac{m_1 m_2}{T} \sum_{i=0}^2 J_i (m_1 - m_2) \right]$$
(20)

Here,  $A_1$ ,  $B_1$ ,  $A_2$ ,  $B_2$  and  $J_i$  = the model coefficient of Equation (20). Based on the current data set, the trained version of Equation (20) can be expressed using Equation (21).

$$\ln x_{m,T} = m_1 \left( -0.21 - \frac{-696.21}{T} \right) + m_2 \left( -4.45 - \frac{-2093.60}{T} \right) + \frac{-16.42m_1m_2}{T}$$
(21)

# 4. Conclusions

This study was aimed to determine the solubility of a bioactive compound PPN in various "THP + water" combinations including pure water and pure THP at "T = 298.2-318.2 K" and "p = 0.1 MPa". The solubility of PPN was recorded as increasing with arise in both m value of THP and temperature in all "THP + water" mixtures including pure water and pure THP. Obtained solubility data of PPN was correlated well by "Apelblat, Van't Hoff, Yalkowsky–Roseman, Jouyban–Acree and Jouyban–Acree–Van't Hoff" models with an average *RMSD* of <2.0%. Overall, the "Jouyban–Acree model" was found as the most suitable for this modeling. The maximum solute–solvent interactions were observed in the PPN–THP combination in comparison to PPN–water. The results of mixing thermodynamics showed an endothermic dissolution of PPN at m = 0.6–1.0. In addition, the dissolution of PPN was found as entropy-driven at m = 0.8–1.0.

**Supplementary Materials:** The following are available online, Figure S1: Correlation of experimental solubility values of PPN with "Van't Hoff model" in different "THP + water" mixtures at "*T* = 298.2–318.2 K"; Van't Hoff model solubility values of PPN are represented by solid lines, and experimental solubility values of PPN are represented by solid lines, and experimental solubility values of PPN are represented by the symbols, Table S1: Hansen solubility parameters ( $\delta_{mix}/MPa^{1/2}$ ) for various THP + water mixtures free of PPN at "*T* = 298.2 K", Table S2: The values of mixing enthalpy ( $\Delta_{mix}H/J$  mol<sup>-1</sup>), mixing entropy ( $\Delta_{mix}S/J$  mol<sup>-1</sup> K<sup>-1</sup>), mixing Gibbs energy ( $\Delta_{mix}G/J$  mol<sup>-1</sup>) and activity coefficient ( $\gamma_i$ ) for PPN dissolution in different "THP + water" mixtures.

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Sample Availability: Samples of the compound PPN are available from the authors.



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