

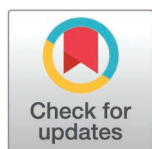
RESEARCH ARTICLE

Preparation of Ni-Mn ferrites magnetic nanoparticles through the ethanol solution combustion-calcination process for the adsorption of methyl blue

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Abstract

Ni-Mn ferrites magnetic nanoparticles (MNPs) were successfully prepared through the ethanol solution combustion-calcination process, and characterized by SEM, TEM, XRD, VSM, BET, and FTIR techniques. For smaller particle size and suitable magnetic property, the optimum element ratio of the material was $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$, and the optimal preparation conditions were appropriate ethanol dosage to attain Fe^{3+} concentrations of approximately 0.85 M, calcination temperature of 400 °C, and calcination time of 2 h, their specific surface area was 136.5 m²/g, and their average particle size and saturation magnetization were 35 nm and 21.66 emu/g, respectively. The adsorption process of methyl blue (MB) onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs conformed to the pseudo-second-order adsorption kinetic model in the initial concentrations of 100–250 mg/L. In comparison with Langmuir and Freundlich adsorption isotherm models, the Temkin model ($R^2 = 0.9865$) was observed to better demonstrate the state of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs, revealing that the adsorption mechanism of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs was the multi-molecular chemical process. The adsorption capacity of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs for MB still maintained about 90% of the initial adsorbance after 6 times cyclic utilization of the nanoparticles by recalcination method, suggesting that $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs had excellent regeneration performance. In general, these results coupled with its environmental friendliness attributed the potential candidates for effluent remediation.

1. Introduction

The issue of pollution is increasingly becoming more severe, and has aroused human's great attention, including water and atmospheric pollution, soil degradation, noise disturbance, and other forms of pollution [1–4]. Among these concerns, water

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pollution has gained increasing prominence due to the extreme scarcity of freshwater resources [5,6]. Especially, dye-containing effluent attaches great importance as it has posed a grave threat on water environment and human health, even human life, owing to its high toxicity, chemical stability, and slow degradation rate [7,8]. However, according to statistics, about 80% of the dye effluent is discharged into the environment without treatment [9].

The treatment of these effluents has been listed as the focus of environmental protection. An effective measure is badly necessitated. A variety of techniques have been developed to eliminate dye-based pollutants from water solutions, including physical method [10], chemical process [11–13], biological process [14,15], and so on. Among them, as the physical method, adsorption has garnered significant attention due to its cost-effectiveness and superior efficiency [16,17]. Additionally, the chemical decomposition or transformation of pollutants is not presented in the adsorption process, thus avoiding the generation of new contaminants. What's more, the adsorption process occurs the surface of adsorbents, including outside surface and internal surface, thus the adsorbents play a significant pivotal role [18].

At present, the commonly used adsorbents include activated carbon, polymer resin and mineral adsorbents, etc., but they all have certain limitations, such as difficulty in regeneration, operational complexity and, most importantly, the limitation in adsorption capacity [19,20]. Compared with conventional adsorbents, nanoparticles have attracted much more attention owing to their large specific surface area and large adsorption capacity [21]. However, practical applications can be inconvenienced by the difficulty of collecting nanoparticles from their dispersing media. In this context, magnetic nanoparticles, which can be easily recycled with an external magnetic field [22], thus facilitating the application and cost management of magnetic nanoparticles while minimizing the number of material syntheses [23–25], are one of the desirable candidate adsorbents for effluent treatment. Particularly, spinel ferrites (MFe_2O_4) nanoparticles, providing excellent magnetic susceptibility, functionalization potential, low cost as well as unique advantages in regenerating and recycling, are among the most promising of these compounds [26].

There are many preparation methods for magnetic ferrite-based nanoparticles, such as precipitation, sol-gel, hydrothermal, high-energy ball milling [27,28], etc. As a new preparation method, the ethanol solution combustion-calcination process has the advantages of simple work-up procedure, shorter reaction time and preparation cycle, low cost, environmental friendliness, low requirements on the equipment, easy realization of industrialized production, and so on.

For the purpose of developing a nanomaterial with high adsorption capacity and satisfactory recycling performance, $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs prepared through the ethanol solution combustion-calcination process were selected and employed to remove dyes in this work, and with methyl blue (MB) as adsorbate model, the adsorption performance of the azo dyes on $Ni_xMn_{(1-x)}Fe_2O_4$ MNPs from water solution was explored [29,30].

2. Experiments

2.1. Preparation and characterization of Ni-Mn ferrites MNPs

$\text{Ni}_x\text{Mn}_{(1-x)}\text{Fe}_2\text{O}_4$ MNPs were prepared through the ethanol solution combustion-calcination process using absolute ethanol as solvent and fuel. $\text{Fe}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$, $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$, and $\text{Mn}(\text{NO}_3)_2 \cdot 4\text{H}_2\text{O}$ were precisely weighed according to the stoichiometric ratio, and dissolved in a beaker with anhydrous ethanol as a solvent to achieve Fe^{3+} concentrations of about 0.85 M, 0.57 M, 0.43 M, 0.34 M, and 0.17 M, respectively. When all the nitrates were completely dissolved to form homogeneous solutions, the solutions were transferred into crucibles and ignited. After the flames were extinguished, the crucibles together with intermediates were calcined at various temperatures (400 °C, 500 °C, 600 °C, and 700 °C) for 2 h. Finally, the calcined products were placed in a mortar and ground to form powders.

The phase identification of Ni-Mn ferrites MNPs was measured by XRD and FTIR, the morphology was investigated with SEM and TEM, the chemical composition was detected by EDS, the magnetic measurement was examined by VSM, and the specific surface area was measured by BET method.

2.2. Adsorption of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs

$\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs were selected to remove MB. At ambient temperature, adsorption kinetics experiments were performed by keeping 5 mg of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs in a series of centrifuge tubes containing 2 mL MB solution with initial concentrations (100, 150, 200, and 250 mg/L). The adsorbents were subsequently separated at regular intervals (10–180 min), and the adsorption capacities of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs were determined based on the change of MB concentration.

The adsorption isotherm of MB onto the nanoparticles was investigated by the similar method, 10 different initial concentrations of MB solution ranging from 400 mg/mL to 4000 mg/mL were adsorbed for 24 h. Subsequently, the supernatants of different initial concentrations were measured.

Additionally, to explore the influence of pH on adsorbance of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs, the pH values of 1, 3, 5, 7, 9, 11, and 13 were adjusted by 1 M dilute HCl or dilute NaOH solutions of, and the adsorption capacities under various pH values were obtained. As to the cycle capacity of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs [31], 75 mg $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs were dispersed into 30 mL MB of 500 mg/L in Erlenmeyer flask for 3 h. Upon completion of the adsorption, $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs were centrifuged and recalcined at 400 °C for 2 h to regenerate the nanoparticles. The experiment described above was replicated after grinding and the adsorption process of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs was verified by infrared spectroscopy.

The absorbances of MB solutions were detected using a UV-Vis spectrophotometer at 600 nm, and the corresponding concentrations were obtained according to the relationship of the absorbance and MB concentration; while, the adsorbance of MB loaded onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs was calculated Using Eq. (1) [32].

$$q_e = \frac{V(C_0 - C_e)}{m} \quad (1)$$

Wherein, q_e represented the equilibrium adsorbance of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs; m was the mass of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs; V indicated the volume of MB solution; C_0 and C_e were the initial and equilibrium concentrations [18].

3. Results and discussion

3.1. Characteristics of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs

Fig 1 showed the characteristics of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs calcined at 400 °C with 20 mL ethanol to achieve a Fe^{3+} concentration of 0.85 M. The SEM morphology (Fig 1A/S1 Fig) displayed that their average particle size was about 35 nm, and the distribution of the particle sizes was uniform. The TEM image (Fig 1B/S2 Fig) suggested that the average particle size of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs was also approximately 35 nm, which was consistent with the result from SEM morphology. The EDS

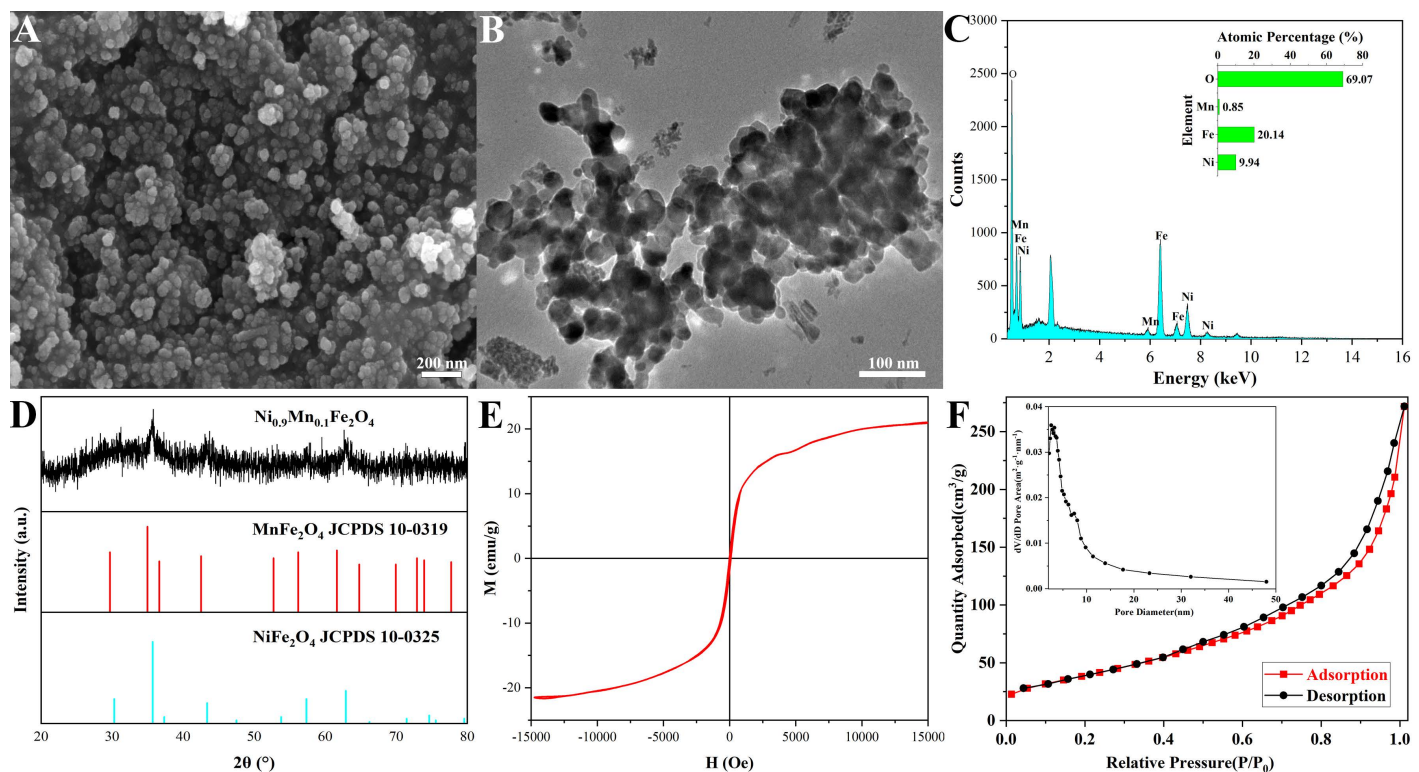


Fig 1. SEM morphology (A), TEM image (B), EDS spectrum (C), XRD pattern (D), the hysteresis loops (E), and N_2 sorption isotherm (F) of $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs calcined at 400 °C with 20 mL ethanol and Fe^{3+} concentrations of 0.85 M.

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spectrum was displayed in Fig 1C, the atomic percentages of Ni, Mn, Fe and O in $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs were basically consistent with the designed composition, which revealed the successful preparation of magnetic $Ni_{0.9}Mn_{0.1}Fe_2O_4$ nanoparticles. The crystal structures of the $Ni_{0.9}Mn_{0.1}Fe_2O_4$ nanoparticles were investigated by XRD. Fig 1D illustrated that the based diffraction peaks of $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs could be indexed to the standard $NiFe_2O_4$ PDF card (JCPDS No. 10–0325) and $MnFe_2O_4$ PDF card (JCPDS No. 10–0319). Fig 1E displayed the hysteresis loops of $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs with typical soft magnetic characteristic, their saturation magnetization (M_s) was about 21.66 emu/g, which demonstrated the superparamagnetism of the material [25,33]. All these results indicated that $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs were successfully prepared. Fig 1F showed the N_2 sorption isotherm of $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs, the adsorption-desorption isotherm curve belonged to the type of IV, and an obvious hysteresis ring appeared, the specific surface area of $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs was 136.5 m^2/g , and their average pore size distributed from 2 nm to 10 nm, the numerous inner bores contributed to large specific surface area, and the large specific surface area was the important factor for the large adsorption capacity of $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs.

3.2. Optimization of preparation process for $NixMn(1-x)Fe_2O_4$ MNPs

3.2.1. Influence of element proportion. It could be seen from Fig 2A that when $x = 0.1–0.5$, there were no obvious characteristic peaks in the spectra, which might ascribe to the fact that the nanoparticles failed to form stable crystallization at this time, and was disregarded. When $x = 0.6–0.9$, there were obvious characteristic peaks. When $x = 0.9$, the characteristic peak was the widest, suggesting that the crystallinity was the lowest, and their average particle size of $Ni_xMn_{(1-x)}Fe_2O_4$ MNPs was the smallest. Fig 2B showed the hysteresis loops obtained by measuring the performance of $Ni_xMn_{(1-x)}Fe_2O_4$ ($x = 0.1–0.9$) MNPs by vibrating sample magnetometer. The saturation magnetization of magnetic

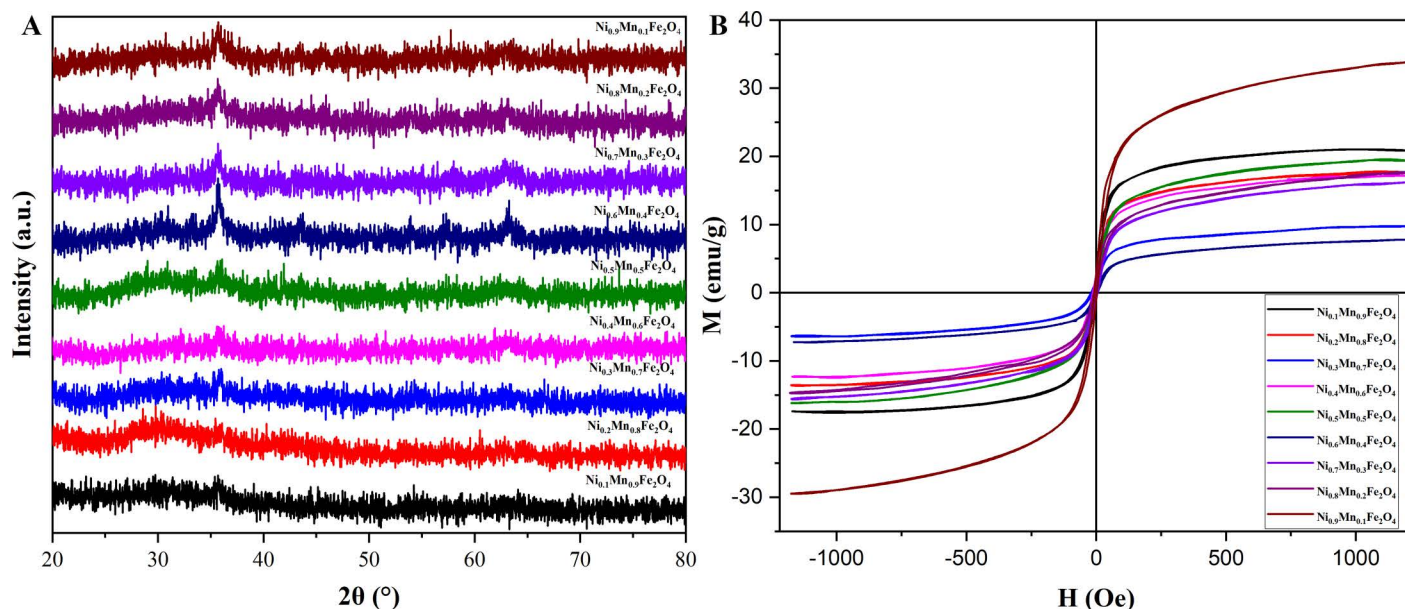


Fig 2. XRD pattern (A) and hysteresis loops (B) of $\text{Ni}_{0.9}\text{Mn}_x\text{Fe}_{2.1-x}\text{O}_4$ ($x = 0.1\text{--}0.9$) MNPs with different element ratios.

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$\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ nanoparticles was the highest of 33.80 emu/g, which provided a guarantee for the separation and recovery of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ nanoparticles.

3.2.2. Effects of calcination temperature and ethanol dosage. Fig 3A revealed the XRD patterns of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs prepared at 400 °C for 2 h with various ethanol volumes for Fe^{3+} concentrations of about 0.85 M, 0.57 M, 0.43 M, 0.34 M, and 0.17 M, respectively. The change of the ethanol dosage would affect the combustion time and the dispersion degree of the preparation process, thus affect the grain size. As was well-known, the long combustion time could increase the degree of crystallinity, and the large dispersion degree of metal ions could reduce the degree of crystallinity. At low doses of ethanol solvent, i.e., large Fe^{3+} concentrations, the combustion time of the ingredient solution was short, and the dispersion degree of metal ions was low, but the combustion time played a mainly larger effect; therefore, with Fe^{3+} concentrations changing from 0.85 M to 0.34 M, the degree of crystallinity increased, and the diffraction peak became narrower and higher. However, with Fe^{3+} concentrations reaching 0.17 M, the dispersion degree of the metal ions began to play the larger effect, resulting in the decrease of the crystallinity degree, therefore, the diffraction peak became shorter and wider, and the average particle size increased. Fig 3B showed the hysteresis loops of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs with different concentrations of ingredient solutions. Obviously, the nanoparticles retained excellent magnetic properties even at low doses (i.e., Fe^{3+} concentration of 0.85 M). With the decrease of Fe^{3+} concentration, the degree of crystallinity increased, M_s of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs increased. When Fe^{3+} concentration reached 0.17 M, the degree of crystallinity decreased, M_s of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs also decreased [34]. Based on the above analysis, to obtain the nanoparticles with larger adsorption performance, the Fe^{3+} concentration of the raw material solution for the preparation of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs was selected as 0.85 M.

Fig 3C displayed the XRD patterns of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs calcined at 400 °C, 500 °C, 600 °C, and 700 °C for 2 h with Fe^{3+} concentration of 0.85 M. The diagram indicated that the characteristic peaks were more prominent with the rise of calcination temperature. When the calcination temperature was 400 °C, the characteristic peaks were the widest and the lowest. Too high temperature would cause the material to agglomerate and increase the particle size, resulting in the decreases of the specific surface area owing to the decrease of inner pore, and finally a descent of the adsorbance. Moreover, with the increase of calcination temperature, the pores inside the nanoparticles would collapse, which would

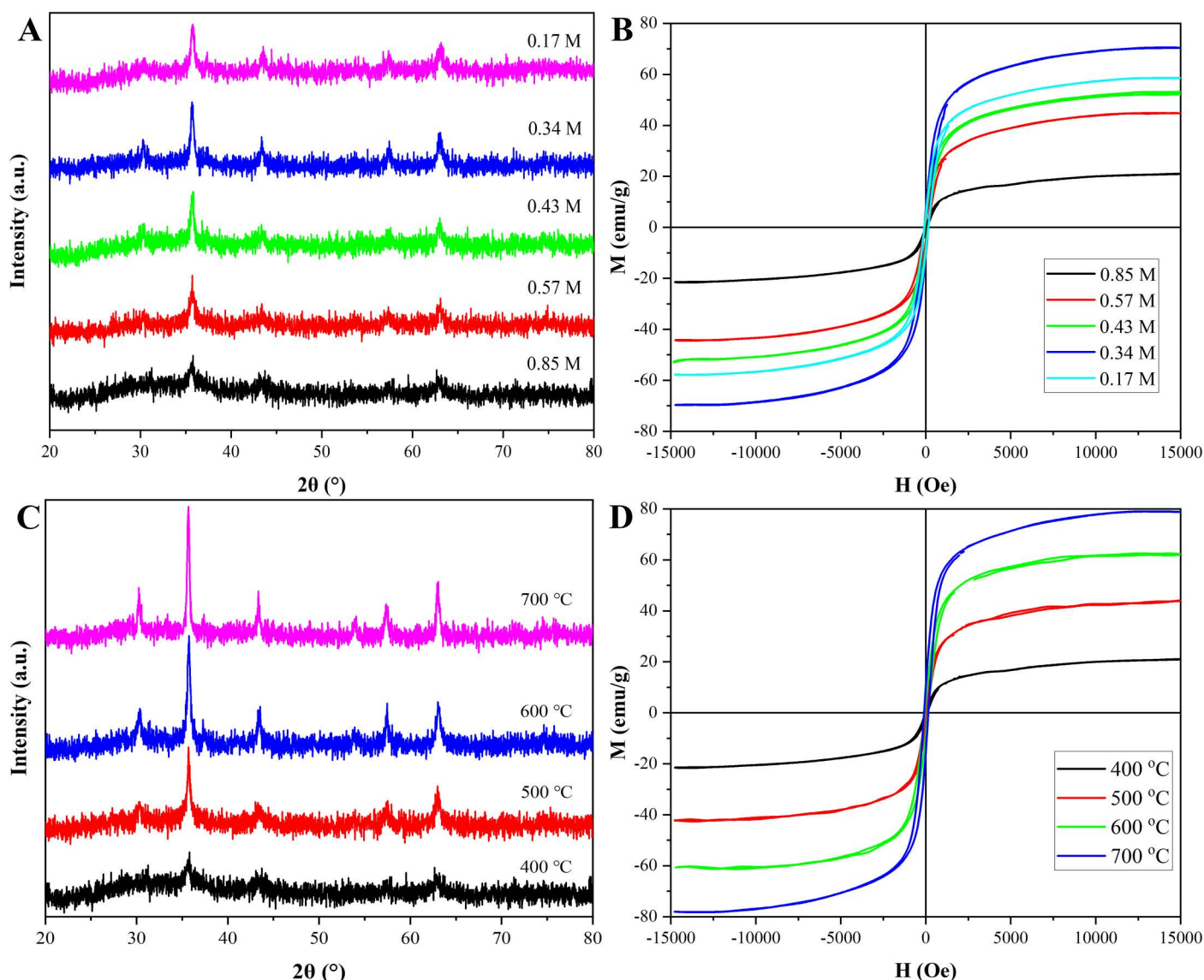


Fig 3. XRD patterns (A, B) and hysteresis loops (C, D) of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs prepared with different Fe^{3+} concentrations and at various temperatures.

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also lead to poor adsorption performance. Fig 3D displayed the hysteresis loops of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs calcined at different temperatures, and the saturation magnetization strength of the nanoparticles similarly increased with the rise of calcination temperature. Although higher temperatures led to better magnetic properties, they also led to too large nanoparticle size, which made adsorption capacity decrease. Considering comprehensively, the sample calcined at 400 °C should be selected for the next experiments.

3.3. Adsorption of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs

3.3.1. Adsorption kinetics. To explore the adsorption mechanism, different models were employed to fit the adsorption data, and the adsorbance of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs with time was investigated by fitting the curve and

kinetics parameters. For this assessment, the pseudo-first-order, pseudo-second-order and intraparticle diffusion models as expressed in Eq. (2) [35], Eq. (3) [18] and Eq. (4) [36] were applied.

$$q_t = q_e(1 - e^{-k_1 t}) \quad (2)$$

$$q_t = \frac{q_e^2 k_2 t}{1 + q_e k_2 t} \quad (3)$$

$$q_t = x_i + k_i t^{1/2} \quad (4)$$

Wherein, q_e and q_t were the adsorbances of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs at equilibrium time and a given time; k_1 , k_2 and k_i were the rate constants for three models; x_i was associated to the thickness of boundary layer.

The experimental curves for the adsorption of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs with various initial MB concentrations at room temperature with time were revealed in Fig 4. The adsorbances of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs rose with the increase of the initial MB concentration. Under the same concentration, the adsorption rate was fast followed by slow until

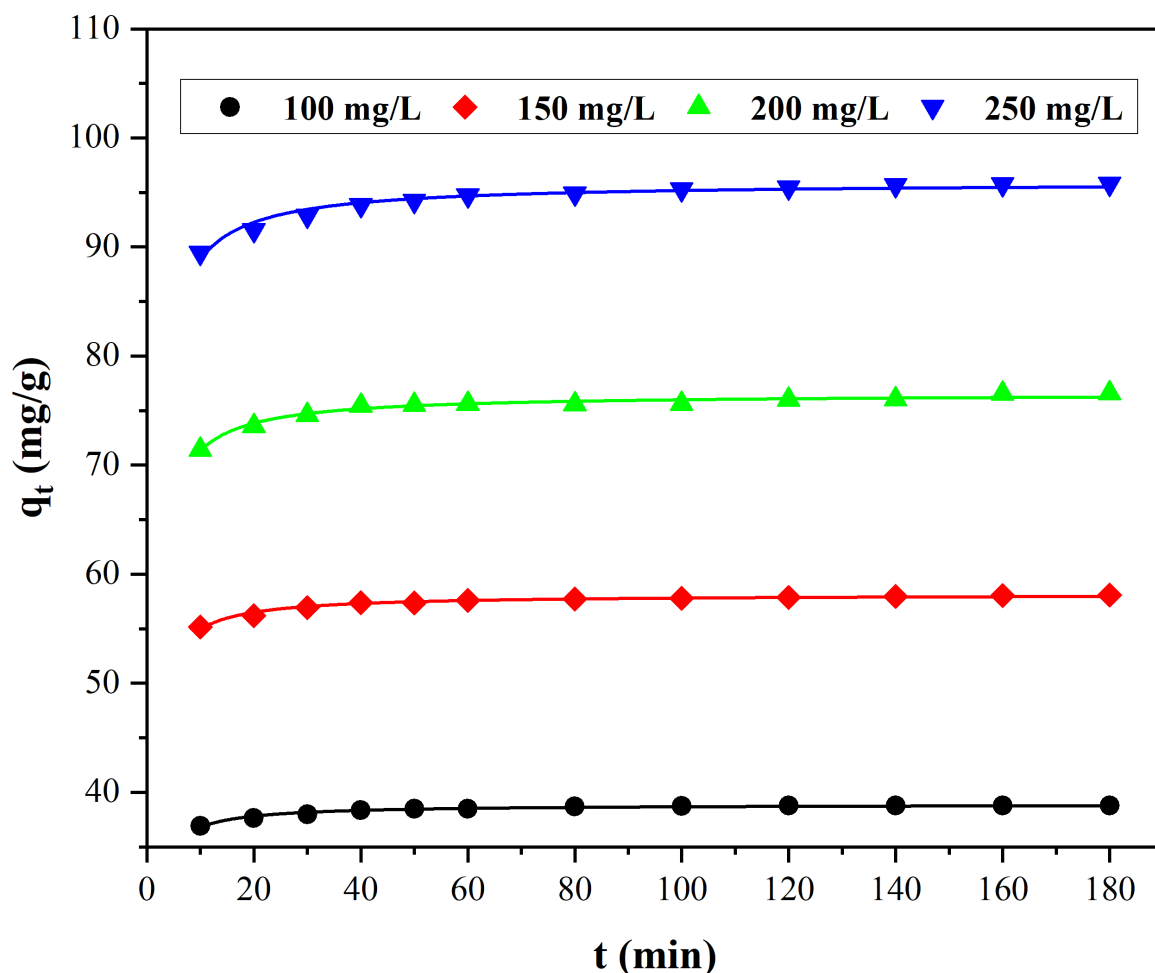


Fig 4. Adsorption process of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs for various initial MB concentrations at room temperature.

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the equilibrium was reached. The fitted curves with three kinetic models for MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs were presented in Fig 5, and all the fitted kinetic parameters were listed in Table 1. The pseudo-second-order kinetics model showed the best fitting based on the variances (R^2) for three models, and their variances were larger than 0.96, and the line relationships of the pseudo second-order adsorption kinetic model for the adsorption of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs with various MB initial concentrations were displayed in Fig 6, which revealed better line correlations, all the results suggested that the adsorption of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs might be a chemical adsorption involving electron sharing or electron transfer.

3.3.2. Adsorption isotherms. The adsorption isotherm could provide the interaction relationship of MB molecules and the state of MB on the surfaces of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs. Therefore, Langmuir, Freundlich, and Temkin adsorption isotherm models were employed to simulate the adsorption equilibrium curves.

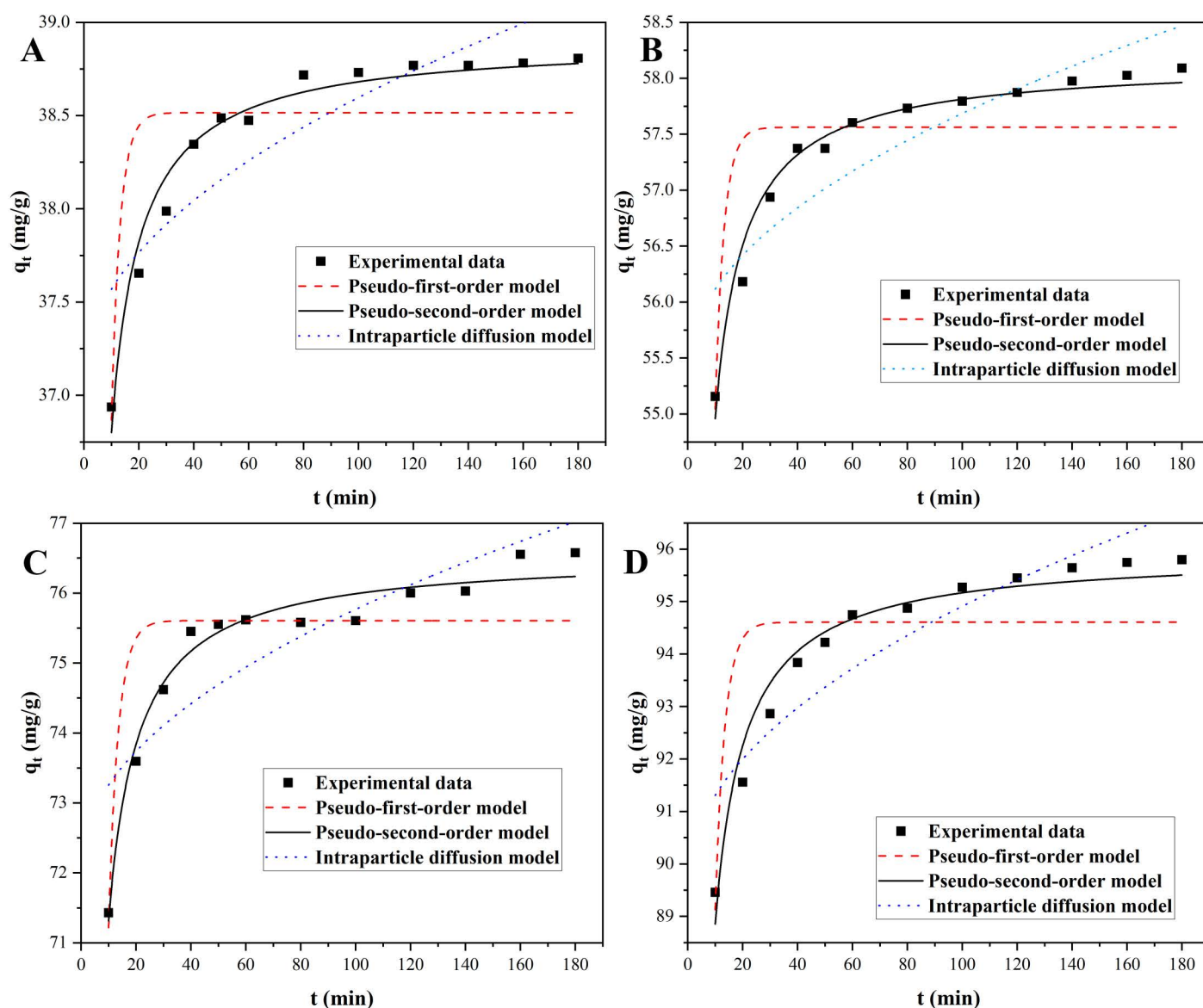


Fig 5. The fitting curves for three kinetics models with initial MB concentrations of 100 mg/L (A), 150 mg/L (B), 200 mg/L (C), and 250 mg/L (D).

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Table 1. The simulative adsorption kinetics parameters for MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs at room temperature.

Adsorption kinetics model	parameter	initial concentrations of MB (mg/L)			
		100	150	200	250
pseudo-first-order kinetics	R^2	0.6432	0.6523	0.7252	0.6097
	K_1	0.3151	0.3129	0.2846	0.2848
	Adj. R^2	0.6076	0.6176	0.6977	0.5707
pseudo-second-order kinetics	R^2	0.9776	0.9760	0.9710	0.9625
	K_2	0.0450	0.0296	0.0178	0.0131
	Adj. R^2	0.9695	0.9737	0.9682	0.9587
internal diffusion	R^2	0.7521	0.7638	0.7212	0.8120
	K_1	0.1502	0.2295	0.3674	0.5272
	Adj. R^2	0.7274	0.7402	0.6933	0.7932

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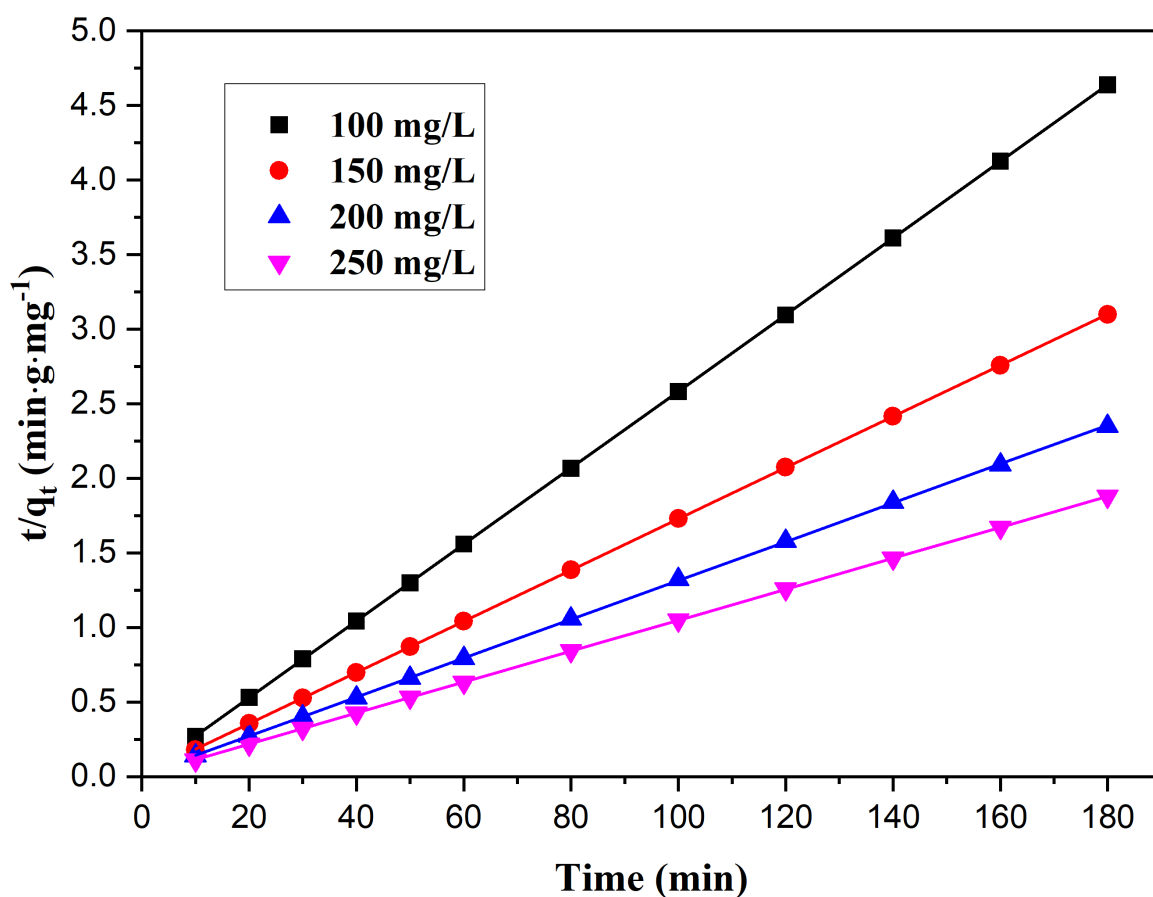


Fig 6. Plots of t/q_t versus t for adsorption of MB onto magnetic $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs with the various initial concentrations at room temperature.

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Langmuir model could be described by the Eq. (5) [37].

$$q_e = \frac{q_{\max} K_L C_e}{1 + K_L C_e} \quad (5)$$

wherein q_e and q_{\max} were the equilibrium and the maximum adsorbances of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs, C_e was the equilibrium concentration of MB, and K_L was the rate of adsorption.

Freundlich model assumed that the adsorption of adsorbate onto adsorbent was bistratal, and its equation was described by Eq. (6) [30].

$$q_e = K_F C_e^{\frac{1}{n}} \quad (6)$$

Whereas K_F was a constant for Freundlich model. $1/n$ was a dimensionless factor that reflected the adsorption intensity or surface heterogeneity.

Temkin model assumed that the adsorption of adsorbate onto adsorbent was tanglesome, and its expression was shown as Eq. (7) [38].

$$q_e = B \ln(A_T C_e) \quad (7)$$

Wherein, B and A_T were the constant for Temkin and the equilibrium binding constant, respectively.

Nonlinear regression methods were utilized to fit the equilibrium data and evaluate the parameters associated with these models, and the fitting curves were displayed in Fig 7, and the simulative parameters were demonstrated in Table 2. Comparing their R^2 , Temkin model acquired the best fitting, and its R^2 value reached 0.9865, which indicated that Temkin model was most suitable for explain the adsorption state of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs. According to the theory of Temkin isothermal model, the adsorption of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs should belong to multi-molecular layer chemical adsorption mechanism [39].

3.3.3. Effect of pH on adsorbance and regeneration study. The pH of MB solution had significant impact on the adsorption, because pH not only affected the surface charge of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs, but also affected the property of the dye itself [40]. To reveal the influence of pH on the adsorbance of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs, the experiments were carried out with various pH of MB solution and the initial MB concentration of 200 mg/L, and the effect of pH on the adsorption was displayed in Fig 8A. When the pH exceeded 5, the adsorption capacity of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs remained a large value. However, once the pH was less than 5, the adsorption capacity decreased sharply. The reason for this phenomenon was that the surface of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs was positively charged owing to MB isoelectric point of about 5. When the pH was less than 5, the surface of MB was positively charged, and there was an electrostatic repulsion between MB and $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs, which gradually decreased with the increase of pH value. As the pH was greater than 5, MB was negatively charged, the dissimilar electrostatics resulted in combination of MB and $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs, and the adsorption capacity reached the maximum, and did not change, suggesting that the saturated adsorption state had been reached at this time. In short, the nanoparticles could maintain a large adsorption capacity for MB in a large pH range from 5 to 13.

The regeneration of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs was shown in Fig 8B. With the increase in reuse frequency of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs, the adsorbance of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs gradually reduced. This might be attributed to the fact that the repeated calcination process increased the sintering degree of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs and the proportion of pore collapse, resulting in a decrease of their specific surface area. Importantly, after 6 rounds of regeneration, the adsorbance of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs still maintained about 90% of the first adsorption capacity, indicating that $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs had excellent recycling performance.

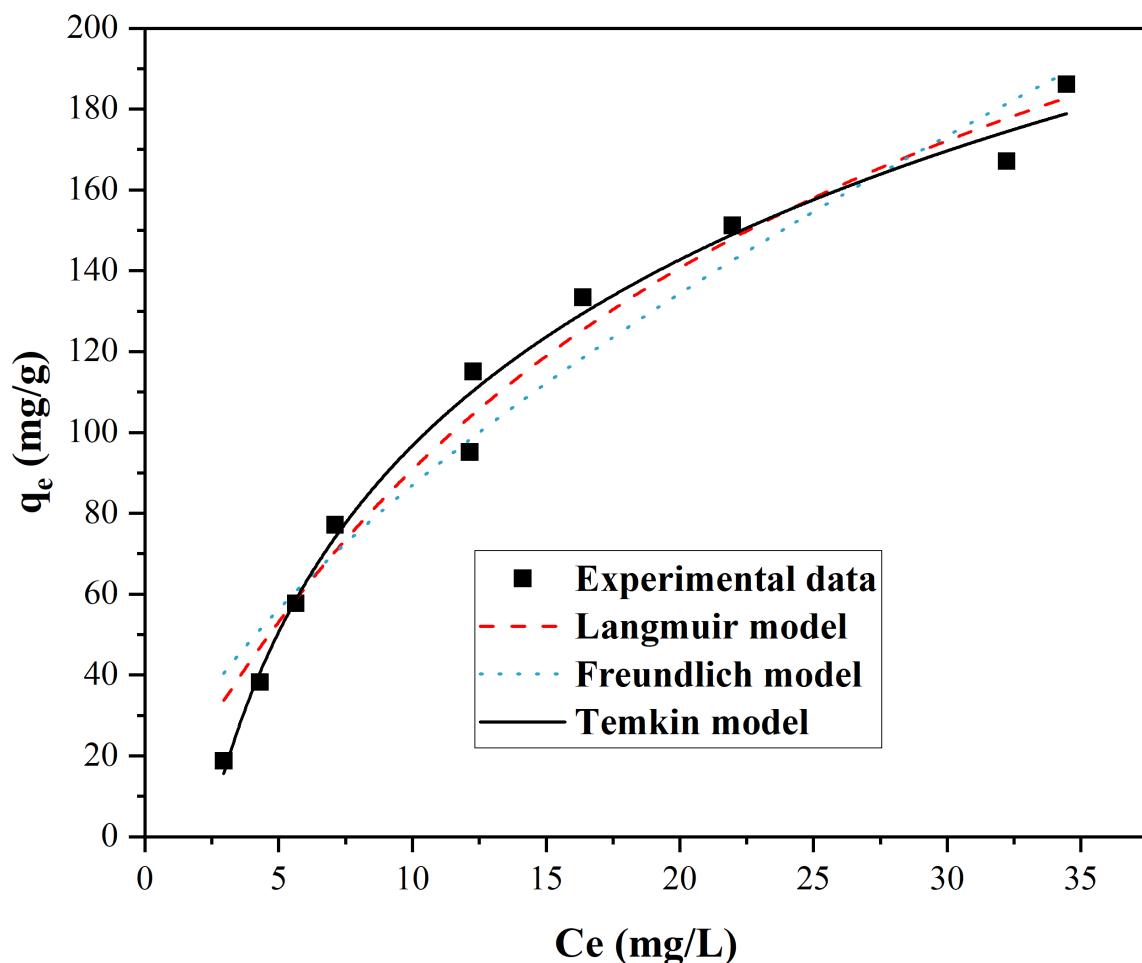


Fig 7. Adsorption isotherm of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs at ambient temperature.

<https://doi.org/10.1371/journal.pone.0321741.g007>

Table 2. Simulative parameters of adsorption isotherms for MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs at room temperature.

adsorption isotherm model	R ²	fitting result	parameter	parameter value
Langmuir	0.9746	0.9714	q_{max}	312.0523
			K_L	0.0400
Freundlich	0.9484	0.9419	K_F	20.4684
			$1/n$	0.6281
Temkin	0.9865	0.9848	B_T	66.4165
			A_T	0.4287

<https://doi.org/10.1371/journal.pone.0321741.t002>

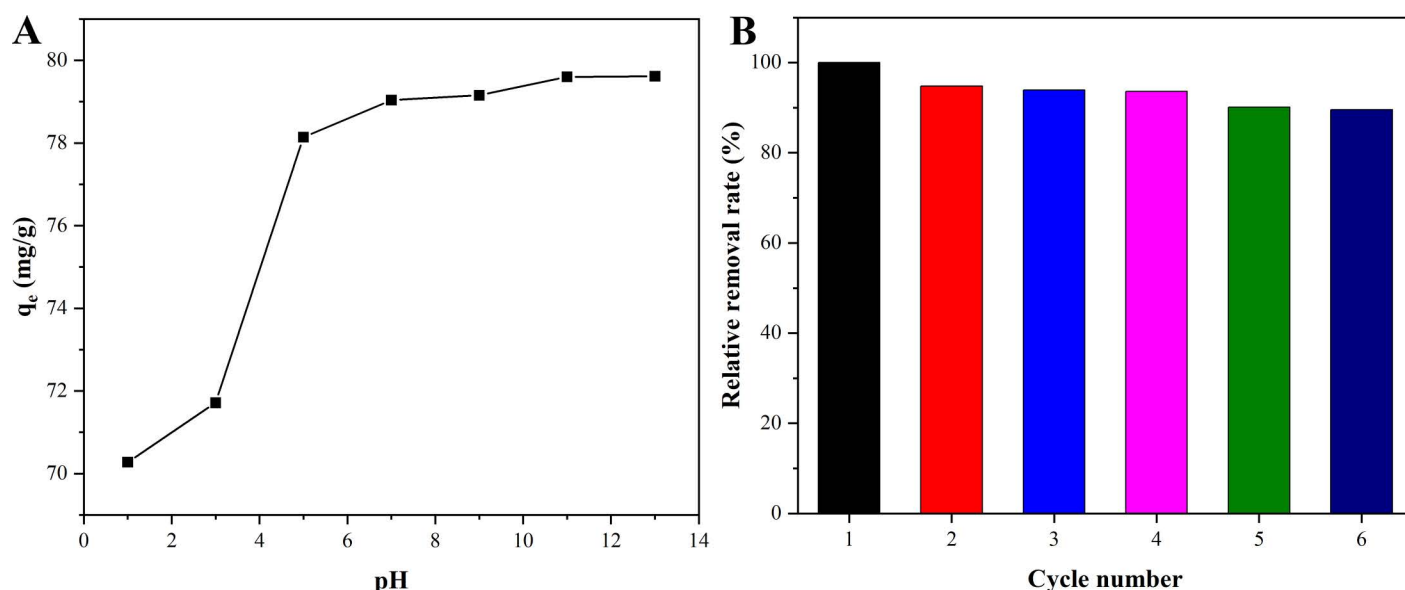


Fig 8. Influence of pH on the adsorbance of MB onto $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNP at room temperature (A) and the regeneration of $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs (B).

<https://doi.org/10.1371/journal.pone.0321741.g008>

Table 3. Comparison of the congeneric adsorbents for MB adsorptions.

Adsorbent	Adsorption capacity (mg/g)	Reference
$Co_{0.5}Zn_{0.5}Fe_2O_4$ MNPs	189.1	[41]
$MnFe_2O_4$ MNRs	102.3	[42]
$Co_{0.8}Cu_{0.2}Fe_2O_4$ MNPs	174.2	[43]
$Co_{0.4}Cu_{0.2}Zn_{0.4}Fe_2O_4$ MNPs	140.4	[44]
$Mg_{0.5}Cu_{0.5}Fe_2O_4$ MNPs	123.8	[45]
$Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs	312.1	This work

<https://doi.org/10.1371/journal.pone.0321741.t003>

The congeneric adsorbents related for MB adsorptions were summarized and were listed in Table 3. Compared with the congeneric adsorbents, including $Co_{0.5}Zn_{0.5}Fe_2O_4$ MNPs, $MnFe_2O_4$ MNRs, $Co_{0.8}Cu_{0.2}Fe_2O_4$ MNPs, $Co_{0.4}Cu_{0.2}Zn_{0.4}Fe_2O_4$ MNPs, $Mg_{0.5}Cu_{0.5}Fe_2O_4$ MNPs, the adsorption capacity of MB onto $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs was almost 1.65–3.05 times of ones for the congeneric adsorbents, suggesting the promising application of $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs for the removal of MB.

3.3.4. FTIR spectrum. FTIR spectroscopy was used to indicate the reproductive property of $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs. The infrared spectra of MB (Fig 9A), $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs (Fig 9B), $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs after adsorption of MB (Fig 9C), and $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs recalcined at 400 °C for 2 h after adsorption (Fig 9D) were analyzed. As shown in the figure, there are five obvious characteristic peaks of 1032 cm^{-1} , 1122 cm^{-1} , 1170 cm^{-1} , 1340 cm^{-1} , and 1575 cm^{-1} on the infrared spectrum of MB. Compared with $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs unadsorbed MB, the infrared spectrum of the adsorbed $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs showed five characteristic peaks corresponding to MB in addition to the Fe-O characteristic peak at 590 cm^{-1} , which verified that MB was successfully adsorbed onto $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs. When $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs adsorbed MB were calcined at 400 °C for 2 h, the characteristic peak of MB in the infrared spectrum basically disappeared and meanwhile the characteristic peak of $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs reappeared, demonstrating that the regeneration of $Ni_{0.9}Mn_{0.1}Fe_2O_4$ MNPs could be realized after calcination.

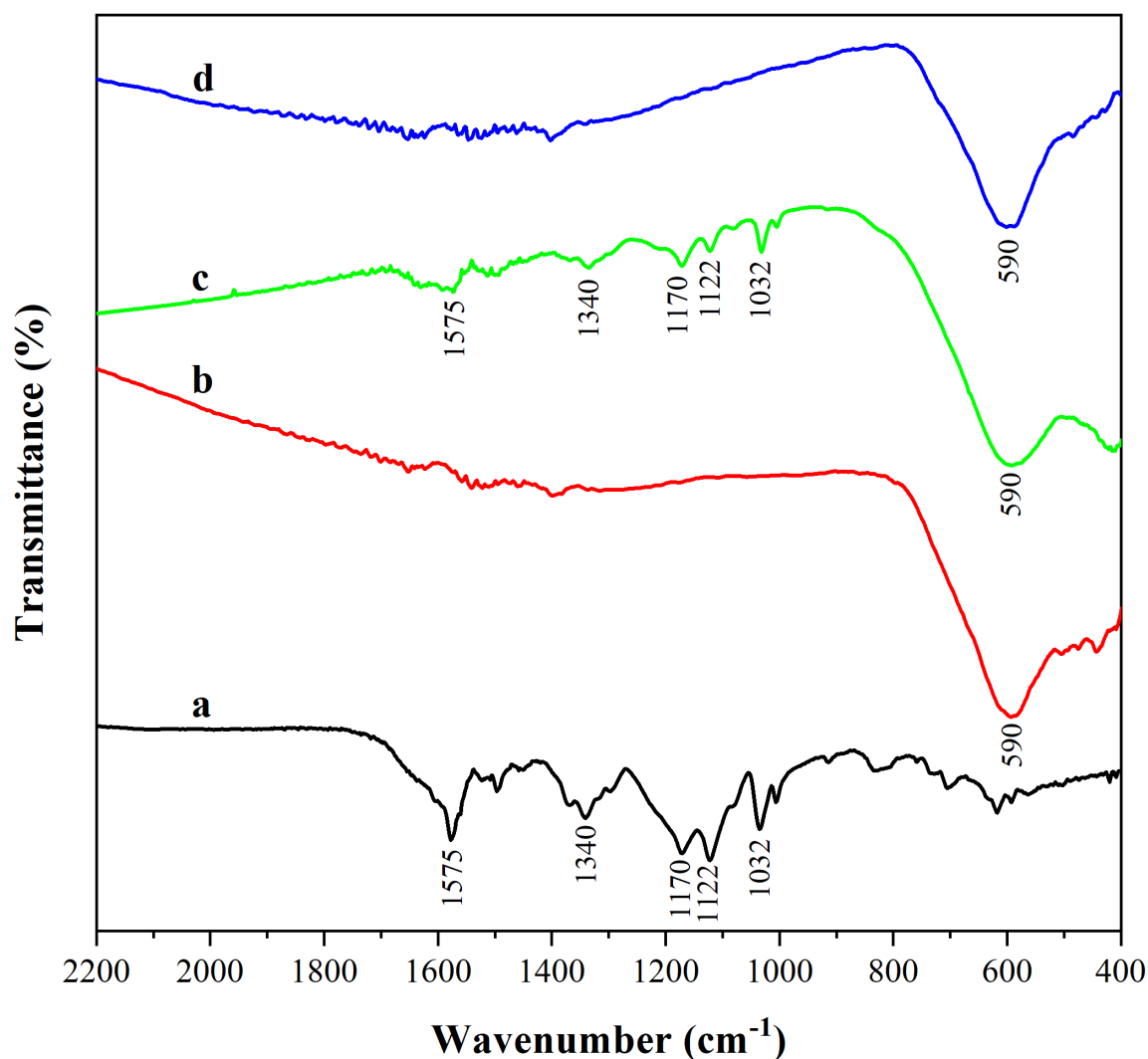


Fig 9. FTIR spectrum of MB (A), $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs (B), $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ -MB (C) and $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs recalcined at 400 °C for 2 h after adsorption (D).

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4. Conclusions

- (1) $\text{Ni}_x\text{Mn}_{(1-x)}\text{Fe}_2\text{O}_4$ MNPs were prepared through the ethanol solution combustion-calcination process, and the as-prepared $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs under optimum preparation conditions (Fe^{3+} concentrations of approximately 0.85 M, the calcination temperature of 400 °C, calcination time of 2 h) with average diameter of about 35 nm, M_s of 21.66 emu/g, and the specific surface area of 136.5 m^2/g were selected for the removal of MB.
- (2) Pseudo-second-order kinetic and Temkin models were the best fittings for the adsorption data of MB onto $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs at ambient temperature, indicating that the multi-molecular layer chemisorption process involving electron sharing or electron transfer was more likely to be the principal underlying mechanism for the removal of MB.
- (3) The influence of pH on the adsorbance showed that the adsorption of MB on $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs could maintain a large adsorption capacity for MB in a range of $\text{pH} > 5$. The FTIR spectroscopy and regeneration performance proved

that $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs could be regenerated by calcination, and still maintain a high adsorption capacity even regenerated for 6 times, exhibiting the excellent reusability and stability of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs.

Supporting information

S1 Fig. SEM morphology of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs calcined at 400 °C with 20 mL ethanol and Fe^{3+} concentrations of 0.85 M.

(TIF)

S2 Fig. TEM image of $\text{Ni}_{0.9}\text{Mn}_{0.1}\text{Fe}_2\text{O}_4$ MNPs calcined at 400 °C with 20 mL ethanol and Fe^{3+} concentrations of 0.85 M.

(BMP)

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