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## Molecular simulation of the effect of water content on CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> adsorption characteristics of coal

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The objective of this work was to investigate the sorption behavior of gases, namely CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub>, by molecules of coal sampled from Linglu mine under different water inclusion rates. To this end, the adsorption, diffusion, adsorption heat, and potential energy distribution characteristics of the gases in the coal pores at different water inclusion rates were analyzed using molecular dynamics and grand canonical ensemble Monte Carlo methods. The results showed that the adsorption relationship of the coal molecules on CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> exhibited a downtrend followed by an uptrend when the water content was increased from 0 to 3.6%. The adsorption amount of CO<sub>2</sub> was approximately twice as much as those of CH<sub>4</sub> and N<sub>2</sub>, indicating that the competitive adsorption advantage of CO<sub>2</sub> compared with those of CH<sub>4</sub> and N<sub>2</sub> was unaffected by the water content. The trend in the average heat of adsorption was generally consistent with the trend in the density of coal molecules under different moisture contents. Under the same conditions, the diffusion coefficient within a coal molecule (2.875 Å) was greater than the liquid–water layer spacing, indicating the formation of a water molecule layer at this point, which inhibited gas adsorption. This study lays a theoretical foundation for further investigating the microscopic mechanism of coal–water interaction.

**Keywords** Molecular dynamics, Grand canonical ensemble Monte Carlo, Radial distribution function, Diffusion, Energy distribution

The adsorption process of water molecules by coal is relatively complex and is a combined result of intermolecular electrostatic forces and hydrogen bonding<sup>1,2</sup>. Several studies have reported that the adsorption of CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> by coal macromolecules decreases with the increase in the number of water molecules<sup>3–5</sup>. However, there is literature confirming the role of water molecules in facilitating the adsorption of methane<sup>6</sup>.

In an attempt to study the sorption characteristics and thermodynamic properties of  $CO_2$ ,  $CH_4$ , and  $N_2$  on coal under different water contents, scholars at home and abroad have conducted a series of experiments<sup>7–9</sup> and simulations<sup>10,11</sup>. Li et al.<sup>12–14</sup> simulated the sorption properties of coal on  $CO_2$  and  $CH_4$  at various water inclusion rates and pore sizes using the grand canonical ensemble Monte Carlo (GCMC) method and verified that the sorption of  $CH_4$  and  $CO_2$  by coal molecules is negatively correlated with the water inclusion rate. Zhang et al.<sup>15–17</sup> analyzed the effects of the temperature and content of moisture on the isotherms and thermodynamic properties of  $CH_4$  adsorption through simulations. Gao et al.<sup>18,19</sup> verified that the greater the amount of water injection, the lower the desorption of the gas. Thus, water injection can decrease the risk of coal and gas protrusion. Wang et al.<sup>20,21</sup> quantitatively characterized the effects of adsorbed water and water vapor on coal gas sorption by nuclear magnetic resonance (NMR) spectroscopy. The results showed that water vapor preferred to adsorb in the coal micropores, while liquid water filled the extensive network of pores and cracks. Xing et al.<sup>22</sup> verified that water competes with  $CH_4$  for specific sorption sites, resulting in a reduced  $CH_4$  sorption capacity for shales containing water. Environmental factors, such as the pressure, temperature, and other external factors, can also vary the water distribution and endowment in shale, thus affecting the  $CH_4$  sorption capacity of shale

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to a certain extent<sup>23</sup>. Zhang et al.<sup>24</sup> used a combination of X-ray photoelectron spectroscopy (XPS), mercury intrusion porosimetry (MIP), and high-pressure volumetric method to quantitatively analyze the adsorption behavior of  $CH_4$  in tectonic coals under the influence of moisture. They further verified that the sorption capacity of  $CH_4$  decreases with an increase in the water content. Guo et al.<sup>25</sup> tested coal samples with different water contents by developing a new type of device for water injection gas adsorption. Some foreign scholars have studied the adsorption characteristics and thermodynamic analysis of coal containing different amounts of water. Chattaraj et al.<sup>26</sup> discussed the adsorption behavior of coalbed methane and showed that the adsorption process can be better explained in terms of thermodynamics and its molecular dynamics (MD). Men'shchikov et al.<sup>27</sup> studied the porous structure, phases, and chemical properties of activated carbon through experimental methods such as nitrogen adsorption, X-ray diffraction, and scanning electron microscopy. The sorption of CH<sub>4</sub> and the thermodynamic properties of the sorption system were analyzed. Gensterblum et al.<sup>28</sup> measured the sorption isotherms of CH<sub>4</sub> and CO<sub>2</sub> for coal samples of various coal grades at dry and moisture equilibriums and investigated the variation in the sorption capacities of CH<sub>4</sub> and CO<sub>2</sub> by coals of different grades, as well as the effect of water on the sorption characteristics. Muangthong-On et al.<sup>29</sup> measured the heat of sorption/desorption of water on coal using thermogravimetric analysis and differential scanning calorimetry (TG-DSC) at temperatures exceeding 100 °C. They demonstrated that the adsorption of water vapor plays an important role in the self-heating of coal. These studies have provided a basis to study the sorption/desorption characteristics of coal on gas under different water contents.

Most studies on the effect of water addition on coal sorption/desorption characteristics have focused on macroscopic phenomena, while studies on microscopic mechanisms are fewer and less in-depth. Therefore, in this work, the adsorption/desorption characteristics and thermodynamic properties of  $CO_2$ ,  $CH_4$ , and  $N_2$  by molecules in the Linglu mine coal with different water contents were quantitatively analyzed by simulating the injection of different amounts of water molecules into the coal seam, which is crucial for the suppression of coal–gas protrusion.

#### Methodology

#### Coal model building and optimization

The adsorption of coal on gas can be categorized as a physical adsorption process<sup>30,31</sup>. In response to this paper, based on the test results of coal samples from Linglu coal mine, the molecular structure model of coal  $(C_{216}H_{169}O_{12}N_4)$  was established to study the adsorption characteristics of  $CO_2$ ,  $CH_4$ , and  $N_2$  on coal with different moisture contents taken from the Linglu mine. The established 2D model was imported into the Materials Studio software, and the structure was subjected to geometric optimization, energy optimization, and simulated annealing with a minimum value of annealed energy. The simulation parameters are shown in Table 1. Table 2 presents the optimized energy parameters. Figure 1 shows the optimized molecular models of the Linglu mine coal, where 10, 20, and 30 molecules of water are added to the computational cell using the amorphous cell module. Figure 2 shows the ultracrystalline cell model of this coal constructed under different water content conditions.

#### Parameter settings for adsorption kinetics simulation

The adsorption laws and influencing characteristics of  $CO_2$ ,  $CH_4$ , and  $N_2$  adsorption by the molecules of the Linglu mine coal at different temperatures (273.15, 283.15, 293.15, 303.15, and 313.15 K) and water contents were analyzed based on the GCMC simulation method. A geometry optimization of the coal molecular fragments was performed using the Forcite module with the simulation parameters listed in Table 3. The MD method was then applied to analyze the diffusion and flow ability of the water molecules, and the NVT system with a constant number of molecules (*N*), constant volume (*V*), and constant temperature (*T*) was selected to run the MD simulations. The temperature was fixed using the Berendsen thermostat. In the MD operation, the simulation

Setting	Parameter		
Summation method	Atom based		
Truncation	Cubic spline		
Spline width	1 Å		
Buffer width	0.5 Å		

Table 1. Optimized parameter settings for coal molecular modeling at Linglu mine.

	E <sub>v</sub> (kcal/mol)				<i>E</i> <sub>N</sub> (kcal/mol)		
E <sub>total</sub> (kcal/mol)	E <sub>B</sub>	EA	E <sub>T</sub>	EI	E <sub>VAN</sub>	E <sub>E</sub>	E <sub>H</sub>
14,452.484	5439.979	1189.461	1471.321	191.326	4028.284	5.50	- 2.320

**Table 2.** Energetic parameters for the optimization of the molecular structure of Linglu mine coal.  $E_V$  valence energy,  $E_B$  bond energy,  $E_A$  angle energy,  $E_T$  torsion energy,  $E_I$  inversion energy,  $E_N$  nonbond energy,  $E_{VAN}$  van der Waals energy,  $E_E$  electrostatic energy,  $E_H$  hydrogen bond energy.



Figure 1. Pore structure model of the coal from Linglu mine with different water contents.



Figure 2. Ultracrystalline cell structure of Linglu mine coal with different water contents.

Setting	Parameter
Force field	Dreiding
Quality	Fine
Electrostatic	Atom based
van der Waals	Atom based
Cutoff distance	15.5 Å
Charges	QEq
Maximum iteration steps	20,000
Energy convergence values	0.0001 kcal/mol

 Table 3.
 Simulation parameter settings.

step size was 1 fs, and the total simulation time was 500 ps, of which the first 60 ps were used to bring the system to equilibrium and the middle 60–100 ps to determine its diffusion properties.

#### **Results and discussion**

### Influence of water content on $CO_2$ , $CH_4$ , and $N_2$ sorption and adsorption heat trends Adsorption capacity

The sorption of  $CO_2$ ,  $CH_4$ , and  $N_2$  using the structural model of the Linglu mine coal was calculated at different temperatures (273.15, 283.15, 293.15, 303.15, and 313.15 K), pressures (0.1–10 MPa), and moisture contents (0%, 1.2%, 2.4%, and 3.6%), as shown in Fig. 1. The coal molecules were modeled with 0, 10, 20, and 30 water molecules.

The formula for calculating the water content<sup>32</sup> is as follows:

$$W = \frac{M_{H_2O}}{M_{coal} + M_{H_2O}} \times 100\%$$
(1)

where  $M_{\rm H2O}$  is the molecular weight of water, g/mol;  $M_{\rm coal}$  is the molecular weight of coal, g/mol; and W is the water content, %.

As can be seen from Fig. 3, when the pressure in the system is from 0.1 to 1 MPa, the rising trend of the adsorption amount of CO<sub>2</sub>, CH<sub>4</sub> and N<sub>2</sub> rises rapidly with the increase of pressure, and the rising trend of the adsorption amount of the three kinds of gases is gradually smooth when the pressure is from 1 to 10 MPa, which indicates that the adsorption rate of the gases is more rapid in the low-pressure stage. The adsorption of the three gases decreases rapidly with increasing temperature. Clearly, increasing the pressure and decreasing the temperature were favorable to the adsorption of these gases. As shown in Fig. 3, the rise and fall trends of CO<sub>2</sub>,  $CH_4$ , and  $N_2$  adsorption by coal with different water contents were investigated at a pressure of 10 MPa and a temperature of 293.15 K as an example. A comparison of Fig. 3a-d shows that CO<sub>2</sub> adsorption decreases from 6.87 to 6.57 mmol/g, from 6.57 to 7.88 mmol/g, and from 7.88 to 4.23 mmol/g, respectively, when the water content in the system is increased from 0 to 1.2%, 2.4%, and 3.6%. Similarly, a comparison between Fig. 3e-l shows that the rise and fall trends of  $CH_4$  and  $N_2$  adsorption are the same as that of  $CO_2$  adsorption. As shown in Fig. 4, the rise and fall trends of  $CO_2$ ,  $CH_4$ , and  $N_2$  adsorption in the system appears to be decreasing, then increasing, and finally decreasing. The reason for this phenomenon may be that the adsorption of coal on water molecules belongs to multilayer adsorption<sup>33</sup>, and initially the water molecules are easy to form hydrogen bonding with the oxygen-containing functional groups in the coal molecules<sup>34,35</sup>, but the hydrogen bonding belongs to the weak intermolecular interactions, and the interaction energies of the water molecules adsorbed on hydroxyl groups are much larger than the interaction energies adsorbed on the other reactive groups<sup>36</sup>. With the increase in the number of water molecules in coal, the oxygen-containing functional groups in the system will promote the competition between water molecules and  $\dot{CO_2}$ ,  $CH_4$ , and  $N_2$  adsorption, resulting in a regional increase in the adsorption of the three gases,  $CO_2$ ,  $CH_4$ , and  $N_2^{37}$ . Finally, after all the oxygenated functional groups in the coal were occupied, the excess water molecules began to adsorb on the pore surface of the coal in the form of free water, and they continuously condensed, eventually forming a water condensation film on the pore surface, which inhibited the sorption of  $CO_2$ ,  $CH_4$ , and  $N_2$  by the coal. Ultimately, the adsorption amount reduced.

#### Adsorption heat

Adsorption heat is one of the important parameters to characterize thermodynamics in order to respond to the thermic effect generated by the sorption process of water molecules on  $CO_2$ ,  $CH_4$ , and  $N_2$ . During the sorption process, the gas molecules move to the surface of the coal, where the speed of molecular motion is significantly reduced, thus releasing a large amount of heat. Table 4 shows the average sorption heat of  $CO_2$ ,  $CH_4$ , and  $N_2$ .



Figure 3. Isothermal sorption curves of  $CO_2$ ,  $CH_4$ , and  $N_2$  adsorbed by coal molecules with different water contents.



**Figure 4.** Rise and fall trends of  $CO_2$ ,  $CH_4$ , and  $N_2$  adsorption at a pressure of 10 MPa and a temperature of 293.15 K.

		Average heat of adsorption/(kcal/mol)				
Moisture content/%	Gas	273.15 K	283.15 K	293.15 K	303.15 K	313.15 K
	CO <sub>2</sub>	7.703	7.430	7.236	7.129	7.072
0%	$CH_4$	4.552	4.495	4.443	4.419	4.388
	N <sub>2</sub>	3.755	3.740	3.730	3.713	3.701
	CO <sub>2</sub>	7.485	7.148	7.011	6.896	6.855
1.2%	$CH_4$	4.394	4.376	4.354	4.339	4.322
	N <sub>2</sub>	3.686	3.678	3.668	3.664	3.655
	CO <sub>2</sub>	7.538	7.185	7.034	6.928	6.897
2.4%	$CH_4$	4.400	4.385	4.370	4.343	4.329
	N <sub>2</sub>	3.739	3.726	3.711	3.698	3.688
	CO <sub>2</sub>	7.808	7.522	7.293	7.197	7.165
3.6%	$CH_4$	4.819	4.803	4.792	4.785	4.772
	N <sub>2</sub>	4.038	4.030	4.024	4.019	4.012

**Table 4.** Average sorption heat of  $CO_2$ ,  $CH_4$ , and  $N_2$  at various temperatures and water content conditions.

adsorbed by coal molecules of various water contents at various temperatures and pressure ranging from 0.1 to

adsorbed by coal molecules of various water contents at various temperatures and pressure ranging from 0.1 to 10 MPa.

As shown in Fig. 5, at a temperature of 273.15 K, as the water content in the system is increased from 0 to 1.2%, the average sorption heats of CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> decrease, respectively, from 7.70 to 7.48 kcal/mol, from 4.55 to 4.39 kcal/mol, and from 3.75 to 3.69 kcal/mol. When the water content in the system is increased from 1.2 to 2.4%, the average sorption heats of CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> increase from 7.48 to 7.54 kcal/mol, from 4.39 to 4.40 kcal/mol, and from 3.69 to 3.74 kcal/mol, respectively. When the water content is increased from 2.4 to 3.6%, the average sorption heats of CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> increase from 7.54 to 7.81 kcal/mol, from 4.40 to 4.82 kcal/mol, and from 3.74 to 4.04 kcal/mol, respectively.

Clearly, the average sorption heats of  $CO_2$ ,  $CH_4$ , and  $N_2$  showed a decreasing trend with increasing temperature. However, the average heat of adsorption showed an increasing trend with an increase in the water content in the system from 1.2 to 3.6%. From a thermodynamic viewpoint, this phenomenon can be attributed to increase in the density of the water molecules in the system, and their values gradually stabilized as the optimization process approached 500 ps, as shown in Fig. 6, in which the densities converged to 0.855, 0.873, and 0.948 g/ cm<sup>3</sup>, respectively, for water contents of 1.2%, 2.4%, and 3.6%. Therefore, the trend in the average sorption heat was consistent with the trend in the density of the H<sub>2</sub>O molecules in the system, indicating that the average sorption heat of the molecules in the Linglu mine coal with different water contents increases with the increase in the density of the system.







Figure 6. Density distribution of the coal molecules in the Linglu mine with different water contents.

#### Radial distribution function (RDF) and diffusive behavior (MSD)

#### Radial distribution function

The RDF is a physical quantity that characterizes the microstructural features of particles, and its physical meaning is the probability that other particles would appear at a distance *r* around an arbitrarily specified central particle, which can be interpreted as the ratio of the local density of the system to its mean bulk density. The radial distribution function g(r) is given by Eq.<sup>38</sup>:

$$g(r) = \frac{dN}{4\pi \rho r^2 dr} \tag{2}$$

where dN corresponds to the range *r* to r + dr:

$$dN = 4\pi r^2 \rho g(r) dr \tag{3}$$

where  $\rho$  is the density of the particle.

As shown in Fig. 7, with the addition of different amounts of water (1.2%, 2.4%, and 3.6%) to the system, the  $H_2O$  molecules showed the first peak at 0.975 Å, with the peaks being 1200.31, 638.13, and 371.65, respectively. A second peak occurred at 1.525 Å with peaks of 132.94, 73.45, and 41.78, respectively. From these two peaks, it can be seen that the  $H_2O$  molecules exhibited the highest peak when the water content in the system was 1.2%, followed by that when the water contents were 2.4% and 3.6%. The difference in the peaks indicates that, the fewer the  $H_2O$  molecules added to the molecular model of the Linglu mine coal (10–30 molecules), the tighter the arrangement of the  $H_2O$  molecules in the pores. The  $H_2O$  molecules showed a third peak at 2.875 Å with peaks of 10.07, 18.35, and 7.71, marking the formation of a layer of  $H_2O$  molecules with a layer spacing greater





than the liquid–water layer spacing at 2.86 Å<sup>39</sup>. When the water contents in the system were 1.2%, 2.4%, and 3.6%, the  $H_2O$  molecules competed for adsorption with  $CO_2$ ,  $CH_4$ , and  $N_2$  in the preliminary stage due to the lack of formation of the water molecule layer, resulting in an elevated adsorption of the three gases in the system. The sorption of  $CO_2$ ,  $CH_4$ , and  $N_2$  by the Linglu mine coal reduced in the later stage due to the formation of the  $H_2O$  molecular layer. This conclusion is consistent with that arrived at in Sect "Adsorption capacity".

#### Diffusion coefficients

The diffusion behavior of a substance in a pore is proportional to the mean-square displacement of the center of mass of its molecules, and the corresponding diffusion coefficient is the rate of change in the mean-square displacement of all the molecules of the substance over a long duration<sup>40</sup>, and the MSD is calculated using the equation:

$$MSD = \frac{1}{N} \sum_{i=1}^{N} [r_i(t) - r_i(0)]^2$$
(4)

where N is the number of molecules;  $r_i(0)$  is the initial site vector of the molecule; and  $r_i(t)$  is the molecular site vector at time t.

The diffusion coefficient of a gas, Eq.<sup>41</sup>, is given below:

$$D = \frac{1}{6N} \lim_{t \to \infty} \frac{d}{dt} \sum_{i=1}^{N} [r_i(t) - r_i(0)]^2$$
(5)

$$D = \lim_{t \to \infty} \left(\frac{MSD}{6t}\right) = \frac{1}{6} k_{MSD} \tag{6}$$

where D is the diffusion coefficient of the gas;  $k_{MSD}$  is the slope of the MSD curve.

Diffusion coefficient is a physical quantity that describes the process of diffusion of a substance in space, and is the amount of substance per unit time, per unit area, that diffuses in the direction of lower concentration. Figure 8 shows the MSD versus time curves for  $CO_2$ ,  $CH_4$ , and  $N_2$  after water injection. It can be seen that the diffusion coefficient of  $N_2$  in the system is obviously larger than that of  $CH_4$  and  $CO_2$ , and the increase of water content did not inhibit the diffusion rate of  $N_2$ . The trend of the curves shows that water content has a more significant effect on the diffusion capacity of  $N_2$ , followed by  $CH_4$  and  $CO_2$ .

The diffusion coefficients of  $CO_2$ ,  $CH_4$ , and  $N_2$  in coal molecules under the conditions of different water content are shown in Table 5. When the water content is 1.2%, the diffusion coefficients of  $CO_2$ ,  $CH_4$ , and  $N_2$  are  $6.38 \times 10^{-7}$ ,  $2.26 \times 10^{-6}$ , and  $7.47 \times 10^{-6}$  cm<sup>2</sup>·s<sup>-1</sup>, respectively; when the water content is 3.6%, the diffusion coefficients of  $CO_2$ ,  $CH_4$ , and  $N_2$  were  $2.77 \times 10^{-7}$ ,  $3.83 \times 10^{-7}$ , and  $3.53 \times 10^{-6}$  cm<sup>2</sup>·s<sup>-1</sup>, respectively. This is because with the increase of water content, the collision efficiency between the molecules increases, and the interaction force between them is strengthened, resulting in the inhibition of the diffusion of  $CO_2$ ,  $CH_4$ , and  $N_2$  in the pores, leading to a low diffusion coefficient.



Figure 8. MSD vs. time for  $CO_2$ ,  $CH_4$ , and  $N_2$ .

	D/cm <sup>2</sup> ·s <sup>-1</sup>				
Moisture content	CO <sub>2</sub>	CH <sub>4</sub>	N <sub>2</sub>		
0%	$6.47  imes 10^{-7}$	$2.30  imes 10^{-6}$	$7.52  imes 10^{-6}$		
1.2%	$6.38  imes 10^{-7}$	$2.26\times10^{-6}$	$7.47\times10^{-6}$		
2.4%	$4.17  imes 10^{-7}$	$2.08  imes 10^{-6}$	$4.51\times10^{-6}$		
3.6%	$2.77  imes 10^{-7}$	$3.83  imes 10^{-7}$	$3.53 imes10^{-6}$		

Table 5. Diffusion coefficients of CO<sub>2</sub>, CH<sub>4</sub> and N<sub>2</sub> in coal molecules.

#### Potential energy distribution

The potential energy distribution of  $CO_2$ ,  $CH_4$ , and  $N_2$  adsorbed by the coal molecules in the Linglu mine was simulated at a temperature of 293.15 K and a pressure of 10 MPa, as shown in Fig. 9. The effect of the water content in the coal molecules on the preferential adsorption potential of  $CO_2$ ,  $CH_4$ , and  $N_2$  was analyzed.

Figure 9 shows that the absolute value of the potential energy peak exhibits a trend of increasing and then decreasing in systems with water contents of 1.2%, 2.4%, and 3.6%. This is mainly because of the formation of ionic and covalent bonds between the adsorbed particles and atoms during the adsorption process, forming an ordered covering layer on the surface of molecules<sup>42,43</sup>. When an adsorbed particle is close to the surface, it is subjected to an adsorption potential, and the adsorbed particle releases energy and adsorbs at the position where the potential energy of the molecule's surface has a minimum value. Interactions between its adsorbed atoms change the potential energy distribution on the surface. This is the main reason why the potential energy





distribution graph shows a rise and then a fall. With the increase in the water content, the peak potential energies of the optimal adsorption sites of CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> in the system were compared, and the peak potential energies of CO<sub>2</sub> were – 8.15, – 8.95, and – 8.05 kcal/mol, respectively, under the different water contents. The peak potential energies of CH<sub>4</sub> were – 3.95, – 4.45, and – 4.25 kcal/mol, respectively. The peak potential energies of N<sub>2</sub> were – 2.75, – 2.85, and – 2.35 kcal/mol, respectively. The sorption advantage of CO<sub>2</sub> was significantly greater than those of CH<sub>4</sub> and N<sub>2</sub>. Therefore, it can be concluded that the presence of water does not inhibit the CO<sub>2</sub> adsorption advantage.

#### Conclusions

- (1) With the increase in the water content from 0 to 3.6% in the system, with the adsorption amount of  $CO_2$  being approximately twice as much as those of  $CH_4$  and  $N_2$ . This indicates that the presence of water had almost no effect on the sorption advantage of  $CO_2$ .
- (2) The average sorption heat in the system was negatively correlated with the density of the water molecules,  $CO_2$  emitted more heat during adsorption, resulting in its average heat of adsorption being significantly greater than those of  $CH_4$  and  $N_2$ .
- (3) The effect of water content on the diffusion ability of N<sub>2</sub> is more significant, followed by CH<sub>4</sub> and CO<sub>2</sub>. The diffusion coefficients of these three gases decreased gradually with the increase of water molecules. Based on the radial distribution function, the molecular layer spacing of the H<sub>2</sub>O molecules (2.875 Å) was greater than the liquid–water layer spacing of 2.86 Å. Therefore, the adsorption of CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> was inhibited by the formation of the water molecule layer.
- (4) At the same temperature and pressure, and water contents of 1.2%, 2.4%, 3.6%, in terms of the sorption potential, the absolute values of the potential energy peaks of CO<sub>2</sub>, CH<sub>4</sub>, and N<sub>2</sub> increased and then decreased, with the same trend as its adsorption amount.

#### Data availability

All data supporting the findings of this study are available from the corresponding author Jiaxing Lin upon request.

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#### **Author contributions**

The data were analyzed by H.L. and G. D., Z. D., W. W. analyzed the images, and L.J. wrote the manuscript.

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#### **Competing interests**

The authors declare no competing interests.

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