

# Electroreduction of CO<sub>2</sub> in Ionic Liquid-Based Electrolytes

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Electroreduction of carbon dioxide ( $CO_2$ ) to value-added chemicals and fuels is a promising approach for sustainable energy conversion and storage. Many electrocatalysts have been designed for this purpose and studied extensively. The role of the electrolyte is particularly interesting and is pivotal for designing electrochemical devices by taking advantage of the synergy between electrolyte and catalyst. Recently, ionic liquids as electrolytes have received much attention due to their high  $CO_2$  adsorption capacity, high selectivity, and low energy consumption. In this review, we present a comprehensive overview of the recent progress in  $CO_2$  electroreduction in ionic liquid-based electrolytes, especially in the performance of different catalysts, the electrolyte effect, as well as mechanism studies to understand the reaction pathway. Perspectives on this interesting area are also discussed for the construction of novel electrochemical systems.

# Introduction

Carbon dioxide (CO<sub>2</sub>) is a major greenhouse gas. It plays a main role in global warming and leads to serious ecological and environmental problems. It is also a cheap, non-toxic, and abundant CI feedstock for the production of alcohols, acids, and other value-added chemicals.<sup>1</sup> Recently, many technologies such as thermal, photochemical, and electrochemical methods have been used for CO<sub>2</sub> reduction. However, most thermal catalytic reactions are thermodynamically unfavorable and/or need harsh reaction conditions because CO<sub>2</sub> is thermodynamically stable and kinetically inert.<sup>2</sup> In photocatalytic reactions, the photocatalysts need to absorb light to generate electron-hole pairs with low reaction efficiency.<sup>3</sup> Among the numerous approaches, electrochemical reduction represents a promising approach owing to its high efficiency, simple operation, and mild conditions, providing potential opportunities for large-scale practical applications.<sup>4–II</sup>

Electrochemical reduction of  $CO_2$  is a multi-electron/proton transfer process, which usually includes the following four steps: (I)  $CO_2$  dissolution and adsorption on the catalyst surface, (2) one-electron reduction of  $CO_2$  to  $CO_2^{-}$  free radical, (3) further electron/proton transfer for the generation of the target product, and (4) desorption of the product into the electrolyte or gaseous product escape from the electrolyte. Therefore, the electrochemical reduction products can be controlled via changing reaction parameters such as the electrolyte, electrocatalyst, and applied voltage.<sup>12–15</sup> However, an efficient and selective  $CO_2$  reduction reaction is not trivial because of the chemical inertness of  $CO_2$  molecules, and a large overpotential is often needed to improve the kinetically sluggish

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### Figure 1 Typical Electrochemical Cells for CO<sub>2</sub> Reduction in IL-Based Electrolytes

(A) H-type and (B) flow cell. Reproduced with permission from Vedharathinam et al.<sup>34</sup> Copyright 2019, ACS Publishers.

reduction process. One resolution is to explore efficient electrochemical systems, including the catalyst and electrolyte, to boost the catalytic performance of CO<sub>2</sub> reduction.16-27

Accordingly, the selection of the electrolyte is important in designing efficient electrochemical devices.<sup>28–34</sup> The electrolyte provides a medium for the reduction process, including interactions among the electrode surface, reactants, and intermediates, which in turn influence the reaction pathway.<sup>28</sup> Therefore, the type and composition of the electrolytes play important roles in the reduction reaction. So far, various electrolytes, such as aqueous electrolytes, organic electrolytes, and ionic liquids (ILs) have been applied in CO<sub>2</sub> reduction.<sup>26,28</sup> Among them, ILs have attracted much attention as an electrolyte, and many catalytic reactions have been successfully carried out in this medium for green chemistry.<sup>32</sup>

ILs are composed of cations and anions and have been proven to be a promising new class of environmentally benign solvents.<sup>32</sup> They have also attracted extensive interest owing to their unique properties, such as nearly zero vapor pressure, high electrical conductivity, high electrical and thermal stability, and high gas solubility. In particular, their negligible vapor pressure, high ionic conductivity, and wide electrochemical windows make them excellent alternatives to conventional electrolytes in electrochemical applications.33 Moreover, ILs also exhibit excellent activity in the electroreduction of CO<sub>2</sub>. They provide a medium for CO<sub>2</sub> reduction, and their strong absorption capacity for CO<sub>2</sub> promotes the CO<sub>2</sub> reduction reaction effectively. More importantly,

the selectivity of CO<sub>2</sub> reduction can be significantly increased, and the hydrogen evolution reaction (HER) is suppressed in the presence of ILs.<sup>32</sup> In recent years, electrochemical reduction of CO<sub>2</sub> has undergone significant progress in IL-based electrolytes.

In this review, we introduce the current progress of  $CO_2$ electrocatalytic reduction in IL-based electrolytes. Various types of catalysts for producing the target products and the main factors for determining the efficiency are discussed. Moreover, some interesting results associated with the electrolyte effect and mechanism studies in understanding the reaction pathway are also described. Finally, the perspectives in this area are proposed for further study.

# Fundamentals of CO<sub>2</sub> **Electroreduction in IL-Based Electrolytes Typical Cell**

Typical CO<sub>2</sub> reduction cells in IL-based electrolytes are presented in Figure I, including H-type cells and flow cells. In an H-type cell (Figure 1A), the cathode and anode are separated by a proton exchange membrane that only allows the transfer of corresponding ions. The membrane takes advantage of independent variation and prevents further oxidation of the products formed from CO<sub>2</sub> reduction. The oxygen evolution reaction and CO<sub>2</sub> reduction occur at the anode and cathode, respectively. In a flow cell (Figure 1B),<sup>34</sup> the electrolyte is in a flow-through configuration to maximize the solubility of CO<sub>2</sub>, to overcome mass transport limitations, and to suppress the HER in flow electrolyte.

Table 1. Selected  $CO_2$  Reduction Process in IL-Based Electrolyte and the Corresponding Standard Potentials  $E^{\circ}$  (pH 7 in Aqueous Solution versus SHE at 25°C, o.1 MPa, and 1 M Concentration of Other Solutes)

Electrochemical Reduction	$E^{\rm o}$ (V versus SHE)				
$\operatorname{CO}_2(\mathbf{g}) + \mathbf{e}^- \rightleftharpoons \operatorname{CO}_2^{\blacksquare^-}$	-1.90				
$\text{CO}_2(\mathbf{g}) + 2\text{H}^+ + 2\text{e}^- \rightleftharpoons \text{HCOOH}(\mathbf{l})$	-0.61				
$\text{CO}_2(\text{g}) + 2\text{H}^+ + 2\text{e}^- \rightleftharpoons \text{CO}(\text{g}) + 2\text{OH}^-$	-0.52				
$\text{CO}_2$ (g) + 6H <sup>+</sup> + 6e <sup>-</sup> $\rightleftharpoons$ CH <sub>3</sub> OH (l) + H <sub>2</sub> O (l)	-0.38				
$\text{CO}_2(\text{g}) + 8\text{H}^+ + 8\text{e}^- \rightleftharpoons \text{CH}_4(\text{g}) + 2\text{H}_2\text{O}(\text{l})$	-0.24				
$2\mathrm{H}^{+} + 2\mathrm{e}^{-} \rightleftharpoons \mathrm{H}_{2}(\mathrm{g})$	-0.42				
Reproduced with permission from Zhang et al. $^{35}$ Copyright 2017, Wiley Publishers.					

#### **Proposed Pathways for CO<sub>2</sub> Electroreduction**

So far, the electroreduction of CO<sub>2</sub> can proceed via two-, six-, and eight-electron reduction pathways in IL-based electrolytes. CO<sub>2</sub> can reduce to species including carbon monoxide (CO), formic acid/formate (HCOOH/  $HCOO^{-}$ ), methanol (CH<sub>3</sub>OH), methane (CH<sub>4</sub>), and acetic acid (CH<sub>3</sub>COOH). From a thermodynamic perspective, the equilibrium potentials  $(E^{\circ})$  of CO<sub>2</sub> reduction and HER are illustrated in Table 1.35 In CO2 reduction, the rearrangement of a linear molecule to a bent radical anion  $(CO_2^{-})$  requires enormous energy, which occurs at -1.90 V versus the standard hydrogen electrode (SHE). Therefore, it is difficult to convert CO<sub>2</sub> to the desired product with high efficiency and selectivity by commonly used electrode materials in aqueous electrolytes, although the  $CO_2$ .<sup>-</sup> radical obtained is highly reactive and can form target products after several proton and electron transfer approaches. A more negative potential than  $E^{o}$  is often needed to drive this reaction. In other words, the large overpotential is mainly attributed to the first step of CO<sub>2</sub> electroreduction.

#### ILs for CO<sub>2</sub> Electroreduction

The structures of typical ILs for electrochemical reduction of  $CO_2$  are depicted in Table 2. In  $CO_2$  reduction, the structure of ILs allows them to coordinate with  $CO_2$ , which promotes  $CO_2$  adsorption on the catalyst surface and reduces the energy barrier for  $CO_2$  activation. Hence, the current density and reaction selectivity can be improved. Rosen et al.<sup>36</sup> found that in the presence of 1-ethyl-3-methylimidazolium tetrafluoroborate ([Emim]BF<sub>4</sub>), the cell overpotential of CO formation from  $CO_2$  electroreduction could be reduced to 0.17 V on a bulk Ag electrode. To date, many imidazoliumbased ILs such as  $[\text{Emim}]BF_4$ , I-butyl-3-methylimidazolium tetrafluoroborate ( $[\text{Bmim}]BF_4$ ), and I-butyl-3-methylimidazolium hexafluorophosphate ( $[\text{Bmim}]PF_6$ ) have exhibited excellent performance in CO<sub>2</sub> electroreduction.<sup>32,37,38</sup> So far, many achievements have been realized in CO<sub>2</sub> electroreduction with IL-based electrolytes. The major merits of IL as an electrolyte and co-catalyst for CO<sub>2</sub> electroreduction not only reflect its strong absorption capacity of CO<sub>2</sub> but also demonstrate that the IL can (I) suppress the competing HER, (2) lower the reduction overpotential, and (3) increase the selectivity for target products.

# Catalysts for CO<sub>2</sub> Electroreduction in IL-Based Electrolytes

Various catalysts have been used in CO<sub>2</sub> reduction in ILbased electrolytes, ranging from homogeneous to heterogeneous catalysts. The interactions of CO<sub>2</sub> and/or imidazolium with catalysts play important roles in the efficiency of CO<sub>2</sub> reduction. The electrocatalysts and the applied potentials can significantly affect the current density and the selectivity of the target products. In general, different reduction products, such as CO, HCOOH/ HCOO<sup>-</sup>, CH<sub>3</sub>OH, CH<sub>4</sub>, and CH<sub>3</sub>COOH can be obtained by controlling the reaction conditions of CO<sub>2</sub> electroreduction.

#### Homogeneous Catalysts

The homogeneous catalysts are generally organic or organometallic compounds, which have intrinsic molecular structures. Therefore, they dissolve in the electrolytes to facilitate the electron and proton transformation during  $CO_2$  reduction. Kubiak et al.<sup>39</sup> summarized the mechanism of homogeneous electrocatalysts used for electroreduction of  $CO_2$  in various electrolytes and elaborated on the electron sources of catalysts (Figure 2). In this case, the reduction of  $CO_2$  and the homogeneous catalyst can occur simultaneously. Therefore,  $CO_2$  reduction usually exhibits favorable kinetics with low overpotentials.



Owing to the unique properties of IL, homogeneous catalysts have been studied in various IL-based electrolytes. As an example, fac-ReCl (2,2'-bipyridine) (CO)<sub>3</sub> was initially used as a homogeneous catalyst for electroreduction of CO<sub>2</sub> to CO in 1-ethyl-3-methylimidazolium tetracyanoborate ([Emim]TCB) at a lower overpotential.<sup>40</sup> The rate constant of the apparent CO<sub>2</sub> reduction  $(k_{app})$  in [Emim]TCB was up to 4,000 M<sup>-1</sup> s<sup>-1</sup> at 25 ± 3°C. The authors proposed that the interaction between catalysts and [Emim]<sup>+</sup> cations accelerated the dissociation of chloride and reduced the activation energy of CO<sub>2</sub> reduction. In another study, the addition of [Bmim]BF<sub>4</sub> to the aprotic electrolyte could serve as a proton source and promote in situ formation of Fe Porphyrin (FeTPP) conversion to [Fe<sup>o</sup>TPP]<sup>2-</sup> homogeneous catalyst at a less negative potential.<sup>41</sup> Co-catalysis coupling of the IL and homogeneous catalyst for CO<sub>2</sub> reduction exhibited a high faradaic efficiency (FE) of CO (93%) at low overpotential (670 mV) (Figure 3A).

Compared with the electrolytes without IL, the turnover number and turnover frequency (TOF) were both increased 4-fold in this system. Isaacs et al.42 investigated the catalytic activity of  $[M^{n+}(cyclam)Cl_n]$  (M = Ni<sup>2+</sup> and  $Co^{3+}$ , cyclam = 1,4,8,11-tetraazacyclotetradecane) homogeneous catalyst in [Bmim]BF4 and I-butyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide ([Bmim]  $NTF_2$ ) electrolytes. Interestingly, they observed that the diffusion coefficient and heterogeneous electron transfer rate of the complexes mainly depended on the anion of IL, which had excellent catalytic performance for CO formation in [Bmim]BF<sub>4</sub>. In addition, [Ni(cyclam)Cl<sub>2</sub>] was proved to be an active catalyst (Figure 3B). When the applied potential was -1.4 V versus Ag/AgCl, only CO could be detected, and the TOF could reach 0.73  $h^{-1}$ . After 4 h electrolysis, the nuclear magnetic resonance (NMR) spectra of the electrolyte showed that the electrolysis reactions did not change the chemical structure of  $[Bmim]BF_4$ , suggesting that  $[Bmim]BF_4$ 

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Figure 2 Homogeneous Electrocatalysis with Electron Source

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was stable during the reaction (Figure 3C). In addition, *in situ* infrared (IR) spectroscopy electrochemical experiments demonstrated that the existence of intermediary Ni(I) from the [Ni(cyclam)Cl<sub>2</sub>] catalyst can form a [Ni(cyclam)CO]<sup>+</sup> complex and the by-product [Ni(CO)<sub>4</sub>], which may hinder the generation of CO (Figure 3D).

#### Heterogeneous Electrocatalysts

In contrast to the above-mentioned homogeneous electrocatalysts, heterogeneous electrocatalysts are low cost and easily recyclable for large-scale applications. The main mechanism of heterogeneous electrocatalysts for electroreduction  $CO_2$  in IL-based electrolytes is shown in Figure 4. In this case,  $CO_2$  reduction mainly occurs at the interface of the electrolytes and heterogeneous electrocatalysts because the electrocatalysts are usually solid and the electrolytes are solvents saturated with  $CO_2$ . To date, many catalysts have been exploited, including metal catalysts, metal oxides, metal chalcogenides, and metal-free catalysts.

**Metal Catalysts.** Metal catalysts, such as Ag, Au, Bi, Cu, etc., have been studied extensively for  $CO_2$  electroreduction in IL-based electrolytes. In the  $CO_2$  reduction reaction, the binding energy between the intermediate and the catalyst surface plays a crucial role in the product distribution.<sup>12,32,35</sup> Generally, some metals (e.g., Sn, Hg, Pb, In) can produce HCOO<sup>-</sup> due to their weaker binding energy of  $CO_2^{\cdot-}$  intermediate; and some metals (e.g., Au, Ag, Zn, Pd) can bind \*COOH tightly, whereas the capability to bind \*CO intermediate is weak, and thus CO is the main product with these metals. Among them, Cu has moderate binding energy of \*CO intermediate, which provides an opportunity to convert  $CO_2$  to more value-added chemicals with two or more carbon atoms. Cu and Cu-based catalysts as a special category are also be highlighted in this section.

Noble Metal Catalysts. Table 3 provides some results for CO<sub>2</sub> electroreduction on noble metal catalysts in IL-based electrolytes. Rosen et al.<sup>36</sup> reported the use of Ag catalyst for CO<sub>2</sub> reduction in [Emim]BF<sub>4</sub> aqueous solution. They found that IL can act as a homogeneous cocatalyst that improved the catalytic rate, which is ascribed to the extra stabilization of \*COOH intermediate. The imidazolium cation can potentially form a complex with CO<sub>2</sub> on the catalyst surface, which may minimize the free energy for the initial electron transfer to CO<sub>2</sub> (Figure 5A). In their following work, they also explored the possible mechanism on a Pt catalyst via sum frequency generation (SFG).43 The results indicated that a layer of [Emim]<sup>+</sup> on the catalyst surface is beneficial to form [CO<sub>2</sub>-Emim]<sup>+</sup> complex by hindering the HER. By using nonresonant (NR) SFG measurements, they found that little CO was absorbed on the surface of Ag at a threshold potential of -1.33 V versus Ag/ AgCl (Figure 5B).<sup>44</sup> When the applied potential shifted negatively, the increase in curvature suggested structural transition of IL driven by the variation of the potential within the double layer (Figure 5C). This suggests that the structural transition of IL and the low overpotential of CO<sub>2</sub> reduction were closely related. Later, Dyson et al.45 investigated the effect of different imidazoliumbased ILs for CO<sub>2</sub> reduction (Figure 5D). In particular, their results showed that the C4 and C5 protons on the imidazolium ring were crucial for enhancing the reaction activity. In another study, trihexyltetradecylphosphonium 1,2,4-triazolide ([P66614]124Triz) was also used as a strongly basic tetraalkyl phosphonium IL to enhance the solubility of CO<sub>2</sub> (Figure 5E).<sup>46</sup> The promotion effect of the IL on CO<sub>2</sub> reduction was also explored. In the reaction, CO<sub>2</sub> could bind to a 1,2,4-triazole anion and was then reduced to HCOO<sup>-</sup> at a low overpotential (0.17 V).

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Figure 3 The Performances of Different Homogeneous Catalysts in Various IL-Based Electrolytes

(A) FEs for CO (red bar)/ $H_2$  (black bar) and CO (blue line) evolution rates at various applied potentials under a CO<sub>2</sub> atmosphere. (I) 0.5 mM Fe<sup>III</sup> PPCl +I M TFE; (2) 0.5 mM Fe<sup>III</sup> TPPCl +I M TFE + 0.3 M [Bmim]BF<sub>4</sub>. Reproduced with permission from Choi et al.<sup>41</sup> Copyright 2014, Wiley Publishers.

(B) Electrochemical behavior of the system in  $[Bmim]BF_4$  (I and 2), and in  $[Bmim]NTF_2$  (3 and 4),  $[Ni(cyclam)Cl_2]$  and  $[Co(cyclam)Cl_2]Cl$  at 9.7 mM and 2 mM respectively, both saturated with N<sub>2</sub> (black line) and CO<sub>2</sub> (red line), at 100 mV/s. (C) H<sup>I</sup>-NMR (I) and (2) F<sup>I9</sup>NMR spectra of  $[Bmim]BF_4$  after 4 h of potential-controlled electrolysis at -I.4 V versus Ag/AgCl. (D) Infrared *in situ* spectroelectrochemical behavior of the  $[Ni(cyclam)Cl_2]$  complex in  $[Bmim]BF_4$  saturated with N<sub>2</sub> (insert) and CO<sub>2</sub> at open circuit potential (solid line) and after 10 min of electrolysis at -I.4 V (dashed line). Reproduced with permission from Honores et al.<sup>42</sup> Copyright 2017, RSC Publishers.

Au has also attracted wide attention because of the excellent performance of  $CO_2$  conversion in IL-based electrolytes. An early report from Zhu et al.<sup>47</sup> explored the catalytic activity of  $CO_2$  reduction over Au nanoparticles in [Bmim]PF<sub>6</sub>-based electrolyte. In the presence of IL, the intermediate COOH\* could be stabilized efficiently on the Au catalyst. In a later study, electrochemical impedance spectroscopy was applied to determine the difference in interface character between I-butyl-3-methylimidazolium trifluoromethanesulfonate ([Bmim]CF<sub>3</sub>SO<sub>3</sub>)/ propylene carbonate (PC) and tetrabutylammonium trifluoromethanesulfonate ( $[Bu_4N]CF_3SO_3$ )/PC over Au catalyst.<sup>48</sup> The authors considered that  $[Bmim]^+$  would be absorbed on the surface of the catalyst, resulting in the generation of IL film. During the reaction, the formation of  $[Bmim-CO_2]_{(ad)}$  could be a benefit for decreasing the activation energy and overpotential of  $CO_2$  electroreduction. Cuesta et al.<sup>49</sup> combined *in situ* surfaceenhanced infrared absorption spectroscopy in attenuated total reflection mode (ATR-SEIRAS) with cyclic

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voltammetry (CV) to study the reason for the decreasing reduction potential of CO<sub>2</sub> in IL (Figure 6A). They attributed this to the lower coverage of the adsorbed layer formed upon CO<sub>2</sub> reduction, which led to a lower degree of dipole-dipole coupling. Then, the CO bands started decreasing at more positive potentials due to CO desorption from the surface. The catalytic ability of CO<sub>2</sub> was also studied on low-index Au(hkl) single crystal catalysts in eight ILs.<sup>50</sup> The Au(II0) catalyst exhibited higher activity than Au(III) and Au(I00) catalysts. The authors observed that the deactivation of Au(II0) catalyst mainly originated from surface reconstruction by *in situ* scanning tunneling microscopy (STM) (Figure 6B).

Pt is another active catalyst for  $CO_2$  reduction. As an example, Compton et al.<sup>51</sup> found electrochemical conversion of  $CO_2$  to HCOOH can occur over anodized Pt wire in I-ethyl-3-methylimidazolium bis(trifluoromethylsulfonyl)imide ([Emim]NTF<sub>2</sub>). The performance of ILs with cyano (–CN) or methoxy (–OCH<sub>3</sub>) functionalized imidazolium cations was also evaluated as electrolytes for electrochemical reduction of  $CO_2$  on Pt catalyst.<sup>52</sup> The results indicated that the addition of the functional groups in ILs can reduce the activated energy for the formation of  $CO_2^{--}$  intermediate. Consistently, the Pt(IIO) single crystal catalyst also efficiently promoted electrochemical synthesis of HCOOH from  $CO_2$  in [Emim]NTF<sub>2</sub> electrolyte.<sup>53</sup>

*Post-transition Metal Catalysts.* Some examples of CO<sub>2</sub> electroreduction on post-transition metal catalysts in IL-based electrolytes are given in Table 3. Typically, Bi is an

abundant, inexpensive, and non-toxic post-transition metal. It is widely probed in electrochemical conversion CO<sub>2</sub> to CO or HCOO<sup>-</sup> with IL-based electrolytes. Rosenthal et al.<sup>64</sup> reported pioneering work that utilized Bi film as the cathode for CO<sub>2</sub> reduction in acetonitrile containing TBAPF<sub>6</sub> and [Bmim]PF<sub>6</sub> as supporting electrolyte. In this system, the FE of CO could reach approximately 95% at a very low overpotential. In their following work, they also found ILs containing different cations as electrolytes affected the selectivity for CO<sub>2</sub> reduction over Bi cathodes (Figure 6C).<sup>66</sup> Recently, Zhu et al.<sup>67</sup> designed surface-activated Bi nanoparticles (NPs) for electrochemical reduction of CO<sub>2</sub> to CO in [Bmim]OTF/acetonitrile electrolyte. The FE of CO can reach 96.1%, and the mass activity for CO evolution  $(MA_{CO})$  can achieve 15.6 mA mg<sup>-1</sup> over activated 36nm Bi NPs (Figure 6D). Furthermore, the structure of Bi was studied during cathodic polarization in acetonitrile solution containing [Bmim]+-based ILs.75 The authors observed that the Bi<sub>2</sub>O<sub>3</sub> layer on the Bi (001) films was reduced during the first CV scan, and Bi could gradually dissolve in lateral size in the CV scans between -1.5 V to -1.9 V versus Ag/AgCl (Figure 6E). The authors also found that the generation of a  $Bi \cdots [Im]^+$  complex was beneficial for CO<sub>2</sub> reduction.

CO<sub>2</sub> electroreduction on other post-transition metals, such as In, Sn, Pb, have also been studied. Rosenthal et al.<sup>69</sup> investigated the catalytic activity of Sn, Pb, Bi, and Sb, which were fabricated by the electrodeposition method. In their study, the electrochemical reduction

Table 3. Selected Exam	mples of CO <sub>2</sub> Electroreduction	on Metal Catalysts in IL-	Based Electrolytes				
Catalysts	Electrolytes	Potential	Current Density (mA cm <sup>-2</sup> )	Main Products	FE for Main Products (%)	References	
Noble Metal Catalysts							
Ag	18 mol % [Emim]BF <sub>4</sub> /H <sub>2</sub> O	1.5 V <sup>a</sup>	-	СО	96	Rosen et al. <sup>36</sup>	
Ag	75 μM H <sub>2</sub> O/[Emim]BF <sub>4</sub>	3.25 V <sup>a</sup>	~4	СО	-	Salehi-Khojin et al. <sup>54</sup>	
Ag	0.1 mol $L^{-1}$ [P <sub>66614</sub> ] 124Triz/acetonitrile	-0.7 V versus Ag/AgNO <sub>3</sub>	-	HCOOH (little amount HCHO)	63	Hollingsworth et al. <sup>46</sup>	
Ag	0.02 M 1,3-dimethyl-2- phenyl-imidazolium tetrafluoroborate/0.1 M TBAPF6 <sup>b</sup> /7 mL acetonitrile	~ $-1.4$ V versus Fc <sup>+</sup> /Fc <sup>c</sup>	4.2	СО	~100	Lau et al. <sup>45</sup>	
Ag	50 mol % [Emim]TFO <sup>d</sup> / 10 × 10 <sup>-3</sup> M KHCO <sub>3</sub> /H <sub>2</sub> O	−1.80 V versus Ag/AgCl	~10	СО	95.6 ± 6.8	Neubauer et al. <sup>55</sup>	
Ag	0.1 M n-Bu <sub>4</sub> NPF <sub>6</sub> <sup>e</sup> / 2.0 mM [C <sub>1</sub> , min]BF $_{1}^{f}$ +	-2.3V versus Fc <sup>+</sup> /Fc <sup>c</sup>	-	H <sub>2</sub>	1.8	Zhao et al. <sup>56</sup>	
	1.0% H <sub>2</sub> O/acetonitrile			$CO^{2^{-}}$	70.4		
				$C_2O_4$	27.1		
4~	$[\mathbf{P}_{mim}]\mathbf{P}\mathbf{E}/\mathbf{U} \cap (\langle \mathbf{z}_{0} 0 \rangle)$		-	HCOO	0.4	Dudney at al 57	
Ag	$[Bmim]BF_4/H_2O (\leq 70\%)$ $[Bmim]BF_4/20\% = 0$	-	-1	CO	>90	Rudnev et al. <sup>58</sup>	
Ag	[bmm]br <sub>4</sub> /20% п <sub>2</sub> О	Ag/AgCl	-	0	>94	Ruunev et al.	
Ag	ı M [EmimOH]Cl <sup>g</sup> /2 M EG/PC <sup>h</sup>	−1.7 V versus Ag/AgCl	~4	CO	~100	Vasilyev et al. <sup>59</sup>	
Rough Ag	8 mM [POHmim]BF <sub>4</sub> <sup>i</sup> / acetonitrile	-2.5 versus Fc <sup>+</sup> /Fc <sup>c</sup>	16.4	СО	92	Zhang et al. <sup>60</sup>	
Ag nanoflowers (flow cell with electrolyte flow-through rates of 100 mL min <sup>-1</sup> )	[Emim]BF <sub>4</sub> /H <sub>2</sub> O (92/8 v/v %)	−1.8 V versus Pt	36.6 (j <sub>CO<sup>j</sup>)</sub>	со	75	Vedharathinam et al. <sup>34</sup>	
Ag, Au, or Pt	0.1 mol L <sup>-1</sup> [P <sub>66614</sub> ] 124Triz/acetonitrile/ 0.7 mol L <sup>-1</sup> H <sub>2</sub> O	–0.7 V versus Ag/AgNO <sub>3</sub>	-	HCOO <sup>-</sup> (on Ag catalysts) Syngas (on Ag, Au, and Pt)	95 (HCOO <sup>-</sup> on Ag catalysts)	Hollingsworth et al. <sup>61</sup>	
Au(110)	[Bmim]BF <sub>4</sub>	−1.82 V versus Ag/AgCl	~I	СО	95	Fu et al. <sup>50</sup>	
Au	0.1 M [Bmim]BF <sub>4</sub> / acetonitrile	−1.73 to −1.93 V versus NHE <sup>k</sup>	-	СО	95	Koh et al. <sup>62</sup>	
Au	0.1 mol dm <sup>-3</sup> [Bmim] OAc <sup>1</sup> /dimethyl sulfoxide/0.2 vol % H <sub>2</sub> O	−1.80 V versus Ag/AgCl	8.6	СО	98	Gonçalves et al. <sup>63</sup>	
Pt	50 mM H[NTF₂] <sup>m</sup> / [Emim]NTF₂	-	-	HCOO <sup>-</sup>	-	Martindale et al. <sup>51</sup>	
Post-transition Metal C	Catalysts						
Bi	20 mM [Emim]BF <sub>4</sub> / acetonitrile/0.1 M TBAPF <sub>6</sub>	−1.95 V versus SCE <sup>n</sup>	5.51 ± 1.2	СО	95 ± 6	DiMeglio et al. <sup>64</sup>	
Bi	300 mM [Bmim]OTF°/ acetonitrile	-2.0 V versus SCE <sup>n</sup>	25 ± 2	СО	87 ± 8	Medina-Ramos et al. <sup>65</sup>	
Bi	250 mM [Bmim]PF <sub>6</sub> /	-1.95 V versus SCE <sup>n</sup>	15 ± 2	СО	84 ± 3	Atifi et al. <sup>66</sup>	
	acetonitrile/0.1 M TBAPF <sub>6</sub>			HCOO <sup>-</sup>	$IO \pm 2$		
	250 mM [DBU-H]PF <sub>6</sub> <sup>p</sup> / acetonitrile/0.1 M TBAPF <sub>6</sub>		27 ± 3	HCOO <sup>-</sup>	77 ± 5		
Activated 36-nm BiNPs	100 mM [Bmim]OTF/	-2.0 V versus Ag/AgCl	15.6 mA mg <sup>-1</sup>	со	96.I	Zhang et al. <sup>67</sup>	
Sn power	0.5 M [Emim]N(CN). <sup>9</sup> /H O	-L2 V versus RHE <sup>r</sup>	~0.3 mA	HCOO <sup>-</sup>	81.9	Zhang et al. <sup>68</sup>	
Bi	100 mM [Bmim]OTF/	-1.95 V versus SCE <sup>n</sup>	$10.1 \pm 2.1$	CO	78 ± 5	Medina-Ramos	
Sn	acetonitrile	-1.95 V versus SCE <sup>n</sup>	$7.2 \pm 1.9$		. 77 ± 5	et al. <sup>69</sup>	
Pb		-2.05 V versus SCE <sup>n</sup>	5.0 ± 1.0		81 ± 5		
						(C	

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Table 3.	Contin

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Table 3. Continued						
Catalysts	Electrolytes	Potential	Current Density (mA cm <sup>-2</sup> )	Main Products	FE for Main Products (%)	References
Sn	30 wt % [Bmim]PF <sub>6</sub> / acetonitrile/5wt %H <sub>2</sub> O	-2.3 V versus Ag/Ag <sup>+</sup>	32.1 (j <sub>HCOO-</sub> <sup>\$</sup> )	HCOO <sup>-</sup>	92	Zhu et al. <sup>70</sup>
Pb			37.6 (j <sub>HCOO-</sub> <sup>s</sup> )		91.6	
Pb	0.1 M [Emim]TNF₂/ 0.1 M TEAP <sup>t</sup> /acetonitrile	–2.34V versus Ag/AgNO <sub>3</sub>	-	CO carboxylate	-	Sun et al. <sup>71</sup>
РЬ	700 mM [Bmim] 124Triz <sup>u</sup> /acetonitrile/ 5 wt % H <sub>2</sub> O	−2.4V versus Ag/Ag <sup>+</sup>	24.5	HCOO <sup>-</sup>	95.2	Feng et al. <sup>72</sup>
Pb phytate	12.8 wt % [Bzmim] $BF_4^{V/}$ 9.9 wt % H <sub>2</sub> O/acetonitrile	– 2.25 V versus Ag/Ag+	30.5	HCOO <sup>-</sup>	92.7	Wu et al. <sup>73</sup>
In	Dimcarb <sup>w</sup>	–1.34 V versus Cc <sup>+/ox</sup>	-	СО	45	Chen et al. <sup>74</sup>
				HCOO <sup>-</sup>	40	
In	[Bmim]PF <sub>6</sub> /acetonitrile/ I mM In(acac) $_3^{y}$	−1.9 V versus SCE <sup>n</sup>	~15	СО	99	Ding et al. <sup>14</sup>

<sup>a</sup>Cell voltage.

<sup>b</sup>Tetrabutylammonium hexafluorophosphate.

<sup>c</sup>Ferrocene/ferrocenium.

<sup>d</sup>I-Ethyl-3-methylimidazolium trifluoromethanesulfonate.

<sup>e</sup>Tetrabutylammonium hexafluorophosphate.

<sup>f</sup>I-Decyl-3-methylimidazolium tetrafluoroborate.

<sup>g</sup>I-Ethyl-3-methylimidazoliumhydroxide chloride.

<sup>h</sup>Propylene carbonate.

<sup>i</sup>I-(3-Hydroxypropyl)-3-methylimidazolium tetrafluoroboride.

<sup>j</sup>CO partial current density.

<sup>k</sup>Normal hydrogen electrode.

<sup>1</sup>I-Butyl-2,3-dimethylimidazolium acetate.

<sup>m</sup>bis(Trifluoromethane)-sulfonimide. <sup>n</sup>Saturated calomel electrode.

°I-Butyl-3-methylimidazolium trifluoromethanesulfonate.

<sup>p</sup>[DBU] is 1,8-diazabicyclo[5.4.0]undec-7-ene.

<sup>q</sup>I-Ethyl-3-methylimidazolium dicyanamide.

<sup>r</sup>Reversible hydrogen electrode.

<sup>s</sup>HCOO<sup>-</sup> partial current density.

<sup>t</sup>Tetraethylammonium perchlorate.

<sup>u</sup>I-Butyl-3-methylimidazolium I,2,4-triazolide.

<sup>v</sup>I-Benzyl-3-methylimidazolium tetrafluoroborate. <sup>w</sup>Dimethylammonium dimethylcarbamate.

<sup>x</sup>Cc<sup>+</sup> is cobaltocenium.

<sup>y</sup>Indium acetylacetonate.

of CO<sub>2</sub> was performed in acetonitrile/[Bmim]OTF electrolyte. Sn and Bi can efficiently catalyze CO<sub>2</sub> to CO with current densities of 5–8 mA cm<sup>-2</sup>. In contrast, Pb and Sb cannot favor CO formation. They demonstrated that the IL can enhance the generation of CO by combining with an appropriate catalyst. In addition, Li et al.<sup>14</sup> also found that in situ prepared In nanocrystals can efficiently catalyze CO<sub>2</sub> conversion to CO in ILbased electrolytes. Ha et al.<sup>68</sup> reported on [Emim] N(CN)<sub>2</sub> aqueous solution as the electrolyte to improve the solubility of CO<sub>2</sub> and inhibit the HER for efficient electroreduction of CO<sub>2</sub> to HCOOH over Sn powder catalyst. The maximum FE of HCOOH can reach 81.9% at -1.2 V versus RHE. In addition, acetonitrile and

[Emim]TNF<sub>2</sub> solutions were used as the electrolyte for CO formation from CO<sub>2</sub> electroreduction using Pb as a catalyst.<sup>71</sup> The authors also found that the ratio of acetonitrile and [Emim]TNF<sub>2</sub> changed the pathway of the reaction, reducing the formation of oxalate anion and enhancing CO generation. In addition, electroreduction of CO<sub>2</sub> over Pb or Sn cathodes was reported in ternary mixture electrolytes ([Bmim]PF<sub>6</sub> [30 wt %]/acetonitrile- $H_2O$ ) with a partial current density of 37.6 mA cm<sup>-2</sup> and FE of 91.6% for HCOO<sup>-</sup>.<sup>70</sup> Interestingly, the authors found that the existence of a small amount of H<sub>2</sub>O can significantly enhance the efficiency of the reaction. In another example, In, Sn, and Pb catalysts were also applied in the electroreduction of CO<sub>2</sub> to HCOO<sup>-</sup> in

9



# Figure 5 The Results of Different ILs Used as Electrolytes over Ag Catalysts for Electroreduction of CO<sub>2</sub>

(A) A schematic illustration of how the free energy of the system changes during the reaction  $CO_2 + 2H^+ + 2e^- \rightleftharpoons CO + H_2O$  in H<sub>2</sub>O or acetonitrile (solid line) or [Emim]  $BF_{4}$  (dashed line). Reproduced with permission from Rosen et al.<sup>36</sup> Copyright 2011, AAAS Publishers.

(B) SFG spectra of CO adsorbed on Ag as the potential was scanned from -0.36 to -1.86 V for two cycles. Each major division along the potential axis is equal to 0.5 V. The arrows indicate the threshold potential for  $CO_2$  reduction, -1.33 V.

(C) (Top) SFG nonresonant (NR) signals when IL electrolyte was saturated with Ar or CO<sub>2</sub>. (Bottom) Meniscus cyclic voltammetry (CV). The circles denote the threshold potential for CO<sub>2</sub> reduction and the NR intensity minimum. There was a close association between the onset of CO<sub>2</sub> reduction and the nonresonant intensity minimum. (I) First forward (reduction) scan. (2) First reverse (oxidation) scan. Reproduced with permission from García Rey et al.<sup>44</sup> Copyright 2015, ACS Publishers.

(D) Structures of imidazolium salts studied. Reproduced with permission from Lau et al.<sup>45</sup> Copyright 2015, ACS Publishers.

(E) Addition of CO<sub>2</sub> to [P<sub>66614</sub>]124Triz, showing binding of CO2 to the triazolide anion. Reproduced with permission from Hollingsworth et al.<sup>46</sup> Copyright 2015, Wiley Publishers.

I-ethyl-3-methylimidazolium trifluoroacetate ([Emim] TFA) aqueous solution.<sup>76</sup> The excellent performance was attributed to the high CO<sub>2</sub> solubility in IL and the capacity of IL to stabilize the reaction intermediate.

Cu-Based Catalysts. Different hydrocarbons and alcohols have been obtained from direct conversion of CO<sub>2</sub> on Cu-based catalysts.<sup>35</sup> Dendritic Cu nanomaterials were prepared for CO<sub>2</sub> electroreduction to HCOOH in IL-based electrolyte.<sup>77,78</sup> It was discovered that the synergetic interaction between IL and the structure of the catalyst favors the generation of HCOO<sup>-</sup>. Bimetallic nanomaterials have also been investigated to improve the catalytic performance by altering the degree of stabilization of key intermediates. On bimetallic Zn-Cu film,

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#### Figure 6 The Preformances of Different ILs for Electroreduction of CO<sub>2</sub>

(A) ATR-SEIRA spectra of an Au catalyst in CO<sub>2</sub>-saturated [Emim]BF<sub>4</sub>/H<sub>2</sub>O (18% mol/mol) acquired during the negative-going (I) and positive-going (2) sweeps of a cyclic voltammogram at  $5 \times 10^{-4} \text{ V s}^{-1}$ . The reference spectrum was taken at -0.60 V just before starting the potential sweep in the negative direction. The highlighted bands correspond to vasym (CO<sub>2</sub>), magenta star; v(COL), blue star; and v(COB), green star. The red lines correspond to the ATR infrared spectrum of the [Emim]BF<sub>4</sub>/H<sub>2</sub>O mixture (18% mol/mol) and are included for the sake of comparison. Reproduced with permission from Papasizza et al.<sup>49</sup> Copyright 2018, ACS Publishers.

(B) *In situ* STM images of Au(110) in CO<sub>2</sub>-saturated [Bmim]BF<sub>4</sub> (1 and 2) at 0.3 V at the beginning of the experiment, (3 and 4) at -1.7 V and 0.3 V after 1 h exposure of the catalyst at -1.7 V. (5) Cross-sectional profile along the white line in panel (6). (7) Scheme of the missing row reconstruction of Au(110), where every third row is missing. Reproduced with permission from Fu et al.<sup>50</sup> Copyright 2018, Wiley Publishers.

(C) Adjusting the production of  $CO_2$  reduction over bicathodes using varied ILs as electrolytes. Reproduced with permission from Atifi et al.<sup>66</sup> Copyright 2018, ACS Publishers.

(D)  $FE_{CO}$  and  $MA_{CO}$  on electrodeposited Bi films (Bi-ED), 36-nm and 7-nm freshly reduced Bi/C. Reproduced with permission from Zhang et al.<sup>67</sup> Copyright 2016, ACS Publishers.

(E) Change in lateral size of Bi (001) domains and reflectivity as a function of the applied potential for bismuth thin film cathodes in  $CO_2$ -saturated acetonitrile containing 100 mM [Bmim]OTF (1–3). (1) The potential function applied during voltammetry; (2) the Bi (001) lateral domain size change (open red diamonds); (3) the total reflectivity (open blue circles) as a function of time. Reproduced with permission from Medina-Ramos et al.<sup>75</sup> Copyright 2018, ACS Publishers.

the rate of syngas generation can reach 85 N  $\mu$ L (normal microliter) cm<sup>-2</sup> C<sup>-1</sup>/170 N  $\mu$ L cm<sup>-2</sup> h<sup>-1</sup>.<sup>79</sup> In a recent study, Pd-Cu bimetallic aerogel was used as a catalyst for electrochemical conversion of CO<sub>2</sub> to CH<sub>3</sub>OH in electrolytes composed of 25 mol % [Bmim]BF<sub>4</sub> and 75 mol % H<sub>2</sub>O.<sup>80</sup> The excellent performance of Pd-Cu aerogels can be attributed to the high porosity of aerogel and the special valence states of the two metals (Figures 7A–7D). The IL-based electrolyte can also adsorb and stabilize CO<sub>2</sub><sup>--</sup>,

which is favorable for  $CO_2$  reduction. CuSn alloys can also efficiently reduce  $CO_2$  in an IL-based electrolyte at low overpotential<sup>81</sup> due to the synergistic effect between two metals.

In addition, Cu-doped catalysts have been explored in the reaction to enhance energy efficiency. For this purpose, Roy et al.<sup>82</sup> investigated CO<sub>2</sub> electroreduction to CO on Cu-modified boron-doped diamond (BDD) in The Innovation



## Figure 7 The Results of Different Cu-Based Catalysts with Various IL-Based Electrolytes

(A and B) X-ray photoelectron spectroscopy of (A) Cu 2p and (B) Pd 3d levels of catalysts. (C and D) The relative intensity ratios of (C)  $Pd^{o}/Pd^{II}$  and (D)  $Cu^{I} + Cu^{o}/Cu^{II}$  in catalysts. Reproduced with permission from Lu et al.<sup>80</sup> Copyright 2018, Wiley Publishers.

(E and F) Various gaseous and liquid electrochemical reduction products obtained by using (E) the Cu catalyst and (F) the Cumodified BDD catalyst in the presence of 100 mM [Emim]BF<sub>4</sub> IL at -I.2 V versus SHE. Reproduced with permission from Roy et al.<sup>82</sup> Copyright 2016, Wiley Publishers.

100 mM [Emim]BF<sub>4</sub> aqueous solution. Compared with bare Cu, the Cu-modified BDD catalysts can inhibit the HER and enhance product selectivity (Figures 7E and 7F). N-based Cu(I)/C-doped boron nitride (BN-C) composites were also designed for electroreduction of  $CO_2$  in [Emim]BF<sub>4</sub>-LiI-H<sub>2</sub>O electrolyte.<sup>83</sup> The authors found that the current density could reach 13.9 mA cm<sup>-2</sup> with a high FE for acetic acid of 80.3%. The synergistic effect of Cu complex, substrate, and electrolyte favor the production of the desired product.

Other Transition Metal-Based Catalysts. Besides Cu, other transition metal (Mo, Co, Zn)-based catalysts have been tested in IL-based electrolytes. Xie et al.<sup>84</sup> carried out electroreduction of  $CO_2$  on single Mo atoms loaded on N-doped graphene in 4 mol % [Emim]BF<sub>4</sub> aqueous solution, which can favor production of HCOO<sup>-</sup>. Zhang et al.<sup>85</sup> reported that the electrochemical reduction of  $CO_2$  can be performed on a Cd catalyst

derived from Cd(OH)<sub>2</sub> in [Bmim]PF<sub>6</sub>/acetonitrile electrolyte. The FE for CO can reach 99.2% with a partial current density of 59.0 mA cm<sup>-2</sup>. A Zn metal-organic framework (Zn-MOF) was also used as the cathode in [Bmim]BF<sub>4</sub> electrolyte for CO<sub>2</sub> reduction.<sup>86</sup> The FE of CH<sub>4</sub> could reach 80% at a low overpotential of 0.14 V. Furthermore, electroreduction of CO<sub>2</sub> was studied over an indium tin oxide modified by cobalt 5,10,15,20 tetra-kis(4-aminophenyl)porphyrin (Co-TAPP) in [Bmim] BF<sub>4</sub>.<sup>87</sup> The results indicated that Co(I) porphyrin species, which promoted the reaction, were detected in an inert atmosphere rather than in the CO<sub>2</sub>-saturated medium.

**Metal Oxides and Metal Chalcogenides.** So far, some attention have been given to  $CO_2$  reduction on metal oxides and metal chalcogenides, such as  $MoO_2$ ,  $SnO_2$ , and  $MoS_2$ . Chu et al.<sup>88</sup> synthesized low-density polyethylene from  $CO_2$  electrochemical reduction over

a nanostructured TiO<sub>2</sub> catalyst in [Emim]BF<sub>4</sub> aqueous solution. The current efficiency of low-density polyethylene was about 8%-14% at an applied potential of -1.50 Vversus standard calomel electrode (SCE). Electroreduction of CO<sub>2</sub> was carried out over MoO<sub>2</sub> with [Bmim] PF<sub>6</sub>/acetonitrile as electrolyte.<sup>89</sup> The addition of IL in the electrolytes led to lower overpotential and improved the FE of CO. The electrocatalytic performance of commercial PbO<sub>2</sub> was carried out in various catholytes composed of IL, H<sub>2</sub>O, and acetonitrile.<sup>90</sup> The [Bzmim]BF<sub>4</sub> was considered to be the best IL for improving the FE of HCOOH. SnO<sub>2</sub> nanosheets on N-doped porous carbon (SnO<sub>2</sub>@N-PC) were prepared for CO<sub>2</sub> electroreduction to HCOOH in 0.5 M [Bmim]PF<sub>6</sub> acetonitrile solution.<sup>91</sup> The current density was 28.4 mA cm<sup>-2</sup> with HCOOH FE of 94.1% at an overpotential of 0.31 V.

Metal chalcogenides can exist in many forms of stoichiometries and structures, therefore they have been widely studied in many fields including CO<sub>2</sub> electrolysis.<sup>35,92–94</sup> For example, titanium disulfide (TiS<sub>2</sub>) planes were synthesized for CO<sub>2</sub> electroreduction to CO in IL-H<sub>2</sub>Oacetonitrile.95 The results revealed that cathodic energy efficiencies can be as high as 64% with a current density of 5 mA cm<sup>-2</sup>. Asadi et al.<sup>96</sup> prepared molybdenum disulfide (MoS<sub>2</sub>) for CO<sub>2</sub> electrochemical reduction. The high current density and low overpotential were obtained in 96 mol % H<sub>2</sub>O and 4 mol % [Emim]BF<sub>4</sub> solution. In the same electrolyte, N-doped MoS<sub>2</sub> nanosheets and N-doped carbon nanodots (N-MoS2@NCDs) composite electrocatalyst were synthesized for CO<sub>2</sub> reduction to CO.97 The good electrical conductivity provided by NCDs on the  $MoS_2$  surface can enhance electron transport. A series of Mo-Bi bimetallic chalcogenides (BMCs) were fabricated for CO<sub>2</sub> electroreduction in [Bmim]BF<sub>4</sub>/acetonitrile.<sup>98</sup> The FE of CH<sub>3</sub>OH was up to 71.2% and the total current density reached 12.1 mA  $\text{cm}^{-2}$ . They found that IL played a crucial role in  $\text{CO}_2$ reduction with the stabilization of CO<sub>2</sub><sup>•-</sup>. The synergistic effect of Mo and Bi favors the generation of CH<sub>3</sub>OH (Figure 8A). The flowerlike  $In_2S_3$  was synthesized as an efficient electrocatalyst for CO2 reduction to HCOO<sup>-</sup> in ILbased electrolyte.99 The excellent catalytic activity was attributed to the special structure and large adsorption energy of intermediate COO\* and OCHO\*. In addition, a defective indium selenide on carbon paper ( $\gamma$ -In<sub>2</sub>Se<sub>3</sub>/ CP) was also prepared for syngas synthesis from CO<sub>2</sub> reduction.<sup>100</sup> Variation in the content of [Bmim]PF<sub>6</sub> and H<sub>2</sub>O in the electrolyte can adjust the CO/H<sub>2</sub> ratio in a wide range (Figures 8B and 8C). WSe<sub>2</sub> nanoflakes (NFs) was prepared for CO<sub>2</sub> electroreduction to CO in 50 vol % [Emim]BF<sub>4</sub>/H<sub>2</sub>O solution.<sup>101</sup> Compared with other cathodes, the current density, FE, and TOF of producing CO were all superior at lower overpotentials (Figures 8D-8G). The IL was vital for this reaction because the cations of IL can form a complex with CO<sub>2</sub> to accelerate the transportation of CO<sub>2</sub>. Cu selenide nanocatalysts can convert CO<sub>2</sub> to CH<sub>3</sub>OH at low overpotential in [Bmim]PF<sub>6</sub> (30 wt %)/acetonitrile-H<sub>2</sub>O solution.<sup>102</sup> The outstanding performance mainly comes from the excellent cooperative effect of Cu and Se in the catalysts. In addition, in [Bmim]BF<sub>4</sub>-H<sub>2</sub>O electrolyte, MoTe<sub>2</sub> could also be used as a catalyst for CO2 reduction to CH4 with high FE of 83%.<sup>103</sup>

**Metal-Free Catalysts.** Metal-free catalysts can also act as potential electrocatalysts for CO<sub>2</sub> reduction in IL-based electrolytes. According to a previous report, they have many intrinsic advantages that can enhance the performance of the reaction, such as excellent conductivity, high surface area, outstanding mechanical strength, and remarkable chemical stability. In addition, they are low cost and easily available in huge quantities. Although pure carbon nanocatalysts show low activity, heteroatoms can be easily introduced to adjust the chemical state and structure of the nanocatalysts to manipulate the active sites for  $CO_2$  reduction. Combining with IL, metal-free nanocatalysts are promising electrocatalysts. The catalytic performance of carbon nanofibers (CNFs) was explored in [Emim]BF<sub>4</sub> and H<sub>2</sub>O mixture electrolytes.<sup>104</sup> In this system, CO<sub>2</sub> could be reduced to CO with high current density and low overpotential. The addition of H<sub>2</sub>O can instantly change the pH and viscosity of IL. The decrease in pH mainly originates from the generation of hydroxyl ions due to the hydrolysis of IL, which can promote the The Innovation



#### Figure 8 The Catalystic Performance of Different Metal Chalcogenides in IL-Based Electrolytes

(A) The current density and FE of the products at different applied potentials over Mo-Bi BMC/CP catalyst with a Mo:Bi molar ratio of 1:1. Reproduced with permission from Sun et al.<sup>98</sup> Copyright 2016, Wiley Publishers.

(B and C) FE of CO and H<sub>2</sub> and current density using [Bmim]PF<sub>6</sub>/CH<sub>3</sub>CN/H<sub>2</sub>O electrolyte with different (B) [Bmim]PF<sub>6</sub> and (C) H<sub>2</sub>O contents over  $F-\gamma-In_2Se_3/CP$  catalysts. Electrolysis experiments were carried out at -2.0 V versus SCE for 5 h. Data were obtained at ambient temperature and pressure with CO<sub>2</sub> stream of 5 sccm. Reproduced with permission from Yang et al.<sup>100</sup> Copyright 2020, Wiley Publishers. CO<sub>2</sub> reduction performance of the TMDC catalysts, Ag NPs, and bulk Ag in the [Emim]BF<sub>4</sub> solution.

(D) CV curves for  $WSe_2 NFs$ , bulk  $MoS_2$ , Ag nanoparticles (Ag NPs), and bulk Ag in a  $CO_2$  environment. Inset shows the current densities in low overpotentials.

(E) CO and H<sub>2</sub> overall FE at different applied potentials for WSe<sub>2</sub> NFs. The error bars represent the SD of four measurements. (F) CO formation TOF of WSe<sub>2</sub> NFs, bulk MoS<sub>2</sub>, and Ag NPs in IL-based electrolyte at overpotentials of 54–650 mV. At 54 mV overpotential, the result for Ag NPs is zero.

(G) Overview of the performance of different catalysts at different overpotentials. All TMDC and Ag NP data were obtained from chronoamperometry experiments under identical conditions. Reproduced with permission from Asadi et al.<sup>101</sup> Copyright 2016, AAAS Publishers.

proton concentration and then improve the rate of  $CO_2$  reduction. It was reported that N-doped carbon (graphene-like) catalysts were efficient for the electrochemical reduction of  $CO_2$  when using IL as the promoter.<sup>105</sup> The FE of  $CH_4$  could be as high as 93.5%, and the current density was I.4 mA·cm<sup>-2</sup> in [Bmim]BF<sub>4</sub>/H<sub>2</sub>O electrolyte.

# **Electrolyte Effects** Comparison of IL, Aqueous Electrolytes, and Organic Electrolytes

In aqueous electrolyte, the solubility of  $CO_2$  is only 0.033 mol<sup>-1</sup> under ambient conditions (298 K, 1 atm), which

leads to low conversion efficiency of  $CO_2$  reduction. Therefore, the sluggish kinetics due to the formation of  $CO_2^{--}$  radical is the main energy barrier for the reaction. Consequently, adequate large overpotentials are usually required to drive this reaction.<sup>28,35</sup> The other complicating factor is the HER, which is prevalent in aqueous media. As a competitive reaction, it can reduce the selectivity of the desired product. Moreover, most studies focus on weakly acidic or alkaline  $CO_2$ -saturated aqueous solutions consisting of inorganic salts (e.g., anions,  $HCO_3^{-}$ ,  $SO_4^{2-}$  Cl<sup>-</sup>, Br<sup>-</sup>, I<sup>-</sup>; alkali metal cations, K<sup>+</sup> and Na<sup>+</sup>) and the catalytic activity and product selectivity

Table 4. Products Formed by Bulk Electrolysis of CO <sub>2</sub> at an Ag Cathe	ode in
Acetonitrile (o.I M n-Bu <sub>4</sub> NPF <sub>6</sub> )	

	$E_{\text{applied}}$ (V)		FE (%)			
	versus					
Additives	Fc/Fc <sup>+</sup>	Charge ©	$H_2$	СО	$C_2 O_4^{\ 2-}$	$HCO_2^-$
Without IL <sup>a</sup>	-2.6 <sup>b</sup>	12.5	0.2	53.9	39.3	0.8
2.0 mM [C <sub>10</sub> mim]BF <sub>4</sub> <sup>a</sup>	-2.3	28.5	0	45.I	53.4	0.4
2.0 mM [C <sub>4</sub> mpyrd]BF <sub>4</sub> <sup>a</sup>	-2.3	50.1	0	66.4	28.4	0.8
Without IL + 1.0% H <sub>2</sub> O	-2.3	15.3	87.4	9.5	3.5	
2.0 mM [C <sub>10</sub> mim]BF <sub>4</sub> + 1.0% H <sub>2</sub> O	-2.3	61.8	1.8	70.4	27 <b>.</b> I	0.4
2.0 mM [C <sub>4</sub> mpyrd]BF <sub>4</sub> + 1.0% H <sub>2</sub> O	-2.3	50.2	0.4	58.4	42.6	0.8

Reproduced with permission from Zhu et al.<sup>56</sup> Copyright 2016, ACS Publishers. <sup>a</sup>H,O content: 5.0 mM.

<sup>b</sup>This more negative potential was chosen to achieve a reduction rate that is comparable with that found in the presence of IL additive.

are enhanced even though the exact mechanism is still under debate.<sup>28</sup> Although there are still difficult issues with CO<sub>2</sub> reduction, CO<sub>2</sub> in aqueous electrolyte could undergo C–C coupling and be further reduced to multi-carbon products. Therefore, designing efficient catalysts for CO<sub>2</sub> electroreduction in aqueous electrolytes can enhance the product selectivity and diversity of the product.<sup>28</sup>

In organic electrolytes, the increased solubility of  $CO_2$  is accompanied by the poor conductivity of the electrolyte.<sup>28</sup> At the same time, the volatilization of a large number of organic solvents also causes environmental problems. Therefore, organic solvent systems are mainly used in homogeneous catalysis or in the design of mixed electrolyte systems.

Compared with aqueous and organic electrolytes, ILs exhibit excellent activity in the electroreduction of  $CO_2$ .<sup>28,32</sup> They provide a medium for  $CO_2$  reduction, and their strong absorption capacity of  $CO_2$  promotes the reduction reaction effectively. More importantly, they can significantly increase the selectivity of products and inhibit the HER.<sup>32</sup> However, a large proportion of ILs are expensive and have high viscosity. Therefore, synthesizing functionalized ILs with low viscosity, high  $CO_2$  absorption, and excellent stability is vital for  $CO_2$  reduction. In addition, most of the catalysts currently developed can only reduce  $CO_2$  to CI product in IL-based

electrolytes. This indicates that the reaction pathways in IL-based electrolyte are different from those in aqueous media. Therefore, it is also necessary to further study the mechanisms in IL-based electrolyte and design novel IL-based systems with high activity for multi-carbon products.

## **Cation and Anion Effect of ILs**

Although many ILs are widely used, the promotion effect of the electrolyte remains unclear. To date, only a few studies have reported the electrolyte effect. This section discusses the recent progress in CO<sub>2</sub> reduction systems concerning the cation and anion effect.

Cation Effect. Imidazolium cations have unique properties in CO<sub>2</sub> reduction. In a recent study, Zhang et al.<sup>56</sup> studied the CO<sub>2</sub> reduction performance on an Ag electrode in acetonitrile solutions (0.1 M [Bu<sub>4</sub>N]PF<sub>6</sub> as supporting electrolyte) containing 2.0 mM imidazolium, pyrrolidium, ammonium, phosphonium, or (trimethylamine)-(dimethylethylamine)-dihydroborate cations. They found that all these cations can enhance the kinetics of the reaction, but imidazolium and pyrrolidium are the most effective (Table 4). Rosenthal et al.<sup>66</sup> found that the cation in ILs can change the selectivity of products over a Bi/IL interface (Figure 6C). Selectively, CO was the main product in [Bmim]PF<sub>6</sub>, and the FE for HCOO<sup>-</sup> was higher in [DBU-H]PF<sub>6</sub> (DBU, 1,8-diazobicyclo[5.4.0]undec-7-ene). These results indicated the interaction among the cation, catalyst, and CO<sub>2</sub> plays an important role in the electroreduction of CO<sub>2</sub>. In addition, it was also reported that ILs with different imidazole rings had a vital influence on the catalytic activity of CO<sub>2</sub> electroreduction.<sup>90</sup> The hydrophobicity of ILs, which can be varied by the side cation chain length, was closely related to the solubility of CO<sub>2</sub>. At the same time, the stability of the imidazole ring-CO<sub>2</sub> complex formed during CO<sub>2</sub> reduction may be decreased by the steric bulkiness with increasing side chain length. Recently, Deng et al.<sup>106</sup> used surface tension measurements and SFG spectroscopy to investigate the surface behavior at a liquid-air interface of I-butyl-3-methylimidazolium methylsulfate ([Bmim]MS) aqueous solution.

The Innovation



# Figure 9 CO<sub>2</sub> Electroreduction Performances

(A) Partial current of HCOOH on the Pb catalyst.

(B) Corresponding FE for HCOOH, CO, and  $H_2$  in IL/acetonitrile- $H_2O$  (5 wt %). Reproduced with permission from Feng et al.<sup>72</sup> Copyright 2018 Wiley Publishers. Structural characteristics of the 20:80 [Emim]BF<sub>4</sub>/H<sub>2</sub>O mixed electrolyte surrounding the \*COOH state.

(C) Calculated radial distribution functions between the hydrogen atom in \*COOH and the oxygen atoms in H<sub>2</sub>O under aqueous and mixed electrolyte conditions.

(D) Calculated radial distribution functions between the oxygen atoms in the adsorbed  $H_2O$  molecules on \*COOH and the oxygen, boron, and carbon atoms in  $H_2O$ ,  $BF_4^{-}$ , and [Emim]<sup>+</sup> in the mixed electrolyte.

(E–G) Different constituents of the mixed electrolyte form alternating layers to solvate the \*COOH intermediate. (E) H<sub>2</sub>O specific adsorption; (F) first anionic layer; (G) second cationic layer. Reproduced with permission from Lim et al.<sup>108</sup> Copyright 2018, ACS Publisher.

The results illustrated that the surface tension was mainly affected by the cations in ILs. Consistently, Dyson et al.<sup>45</sup> also pointed out that different imidazolium rings are vital for efficient  $CO_2$  reduction (Figure 5D).

**Anion Effect.** Anions in the imidazolium-based ILs also affect  $CO_2$  reduction. Zhang et al.<sup>72</sup> built an ionic microhabitat composed of an anion-functionalized IL [Bmim]124Triz, acetonitrile, and H<sub>2</sub>O for CO<sub>2</sub> electroreduction. Other ILs with different anions, such as BF<sub>4</sub><sup>-</sup>, PF<sub>6</sub><sup>-</sup>, NO<sub>3</sub><sup>-</sup>, and NTF<sub>2</sub><sup>-</sup>, were used for comparison. The authors found that [Bmim]124Triz promotes the solubility of CO<sub>2</sub> and bending linear CO<sub>2</sub> by forming the [124Triz]-CO<sub>2</sub> adduct. The activated CO<sub>2</sub> can be transferred into the catalyst surface easily, which can increase the generation of the target product (Figures 9A and 9B). They also used computational results to validate the underlying mechanism of the super-basic IL. Interestingly, they found the bond length in [Bmim]  $\cdots$  CO<sub>2</sub>  $\cdots$  124Triz (2.30 Å) was much shorter than that in other imidazolium-based ILs: [Bmim]PF<sub>6</sub> (3.15 Å), [Bmim]BF<sub>4</sub> (2.93 Å), [Bmim]NTF<sub>2</sub> (3.08 Å), and [Bmim]NO<sub>3</sub> (3.29 Å). This indicated that the interaction between CO<sub>2</sub> and [Bmim]124Triz is much stronger than that between the CO<sub>2</sub> and the other ILs. Therefore, the fast transportation feasibility of activated CO<sub>2</sub> to the catalyst surface led to higher FE of HCOOH. The Innovation

The comprehensive effect of cation and anion was also investigated by Compton et al.<sup>107</sup> They pointed out that the cation bound to the Ag surface allowed the  $CO_2$  molecule to access the Ag surface before the process of desorption and an irreversible reduction of  $CO_2$ . In addition, the anions in ILs may affect the local solvent structure other than the solubility of  $CO_2$ . The electric double layer adjacent to the Ag surface can be occupied by cations and anions and allow  $CO_2$  transport to the Ag surface before electron transfer occurs. Based on previous reports, we can summarize that the cations and anions in ILs play important roles in  $CO_2$  electroreduction. They can interact with the reaction intermediates or change the properties of the electric double layer adjacent to the catalyst surface.

# Mechanism

In general, the CO<sub>2</sub> electroreduction process is driven in imidazolium-based ILs. The importance of the effect of ILs on the activity toward CO<sub>2</sub> reduction was investigated by Lim et al.<sup>108</sup>. In this work, the authors presented a combined experimental and theoretical study to investigate the promotion effect of ILs. Contrary to the previous concept, which assumed specific intermolecular coordination by ILs with the reaction intermediate, the authors figured out that the promotion effect was manifested by changing the reaction microenvironment. They found that the local coordinating environment of \*COOH was nearly identical for aqueous and [Emim] BF<sub>4</sub>/H<sub>2</sub>O systems. A single H<sub>2</sub>O molecule bound to \*COOH through a hydrogen bond (Figures 9C and 9E). However, considering that the H<sub>2</sub>O molecule served as a primary proton source, the local atomic geometry was responsible for the facile proton transfer.

In  $[\text{Emim}]BF_4/H_2O$  electrolyte, approximately one or two  $H_2O$  and  $BF_4^-$  molecules were closed to the adsorbed  $H_2O$  molecule. Then, four  $[\text{Emim}]^+$  molecules surrounded an  $H_2O$ - $BF_4^-$  complex via a strong cationanion attraction (Figures 9D, 9F, and 9G). The combination of these complex noncovalent interactions in the mixed electrolytes formed an exotic microenvironment for \*COOH with an alternating solvation shell structure. These three-dimensional atomic arrangements can result in [Emim]<sup>+</sup> being in direct contact with the catalyst surface, surrounded by the key reaction intermediate. This phenomenon results in a significant polarization of the electron density on the catalyst surface. Then, plenty of metal electrons can be polarized toward the \*COOH intermediate, which induces a strong local field effect at the catalyst interface and stabilizes the \*COOH intermediate. Therefore, the electrical doublelayer interface provided a suitable microenvironment for solvating the intermediate, which can be well preserved with the variations in chemical details because the solvation energy is dominated by the nonspecific interaction.

To further understand the CO<sub>2</sub> electroreduction pathway, Nakamura et al.<sup>109</sup> figured out the possible intermediates and the transition states from CO<sub>2</sub> to CO in  $[\text{Emim}]BF_4$  electrolyte. They stressed that the complex [Emim-COOH] generated during the reaction can be decomposed to CO. In the reaction pathway, H<sub>2</sub>O was a cocatalyst to facilitate proton transfer. The pathway to CO was thermodynamically more favored than that to HCOOH in IL-based electrolyte. As shown in Figure 10, there are many reaction pathways from [Emim]BF<sub>4</sub> and  $CO_2$  to the final product CO. The thermodynamically favorable paths are marked by green arrows and unfavorable ones by red arrows. The black arrows represent the electron transfer from the electrodes. Although important progress has been made in electroreduction of CO<sub>2</sub> with IL-based electrolyte, research on the mechanism is still in its infancy, especially on understanding of the interaction between the liquid medium and the catalyst surface, which is important for the systematic design of efficient catalytic systems.

# Perspective

ILs have shown promising applications in electroreduction of  $CO_2$  due to their unique properties. To date, significant progress has been achieved in this interesting area. However, some related issues need to be solved. The Innovation



# Figure 10 A Schematic Flow of Reaction Intermediates

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(I) For IL-based electrolyte, large-scale application of CO<sub>2</sub> electroreduction has not been realized. On the one hand, the current density at high FE of the desired product is still low for industrial applications (a few hundred mA cm<sup>-2</sup> for industrial level<sup>IIO</sup>). On the other hand, the high cost and high viscosity of ILs are also crucial factors to inhibit its large-scale application. Therefore, highly active, selective, and stable catalyst-electrolyte systems should be explored to promote commercial application, especially using renewable electricity. The design of novel electrochemical devices such as flow cells and gas-diffusion electrodes can overcome the poor mass transferability and increase the current density. Moreover, synthesizing functionalized ILs with low viscosity, high CO<sub>2</sub> absorption, and excellent stability can enhance the capacity of activating CO<sub>2</sub> molecules and achieve multiple reuse of the electrolyte.

- (2) Up to now, most of the catalysts that have been developed can only reduce CO<sub>2</sub> to CI products in IL-based electrolytes. The current density and FE for producing various products with two or more carbons are still not satisfactory because C-C coupling is involved. Therefore, it is interesting and important to explore novel catalystelectrolyte systems with high activity for C-C coupling. Excellent catalysts with high potentials for the HER should be designed that can combine with ILs to provide a good three-phase contact interface for enhancing the selectivity toward multi-carbon products. While the electrocatalytic reduction of CO<sub>2</sub> and H<sub>2</sub>O to produce valuable chemicals and fuels is of great importance, much attention should be given to investigations about new electrocatalytic reactions of CO<sub>2</sub> and organic compounds to synthesize more valuable chemicals. IL-based electrolytes may be more advantageous for this kind of reaction because ILs can dissolve both CO<sub>2</sub> and organic substances. Moreover, the interaction among ILs, CO<sub>2</sub>, and organic reactants can be tuned by changing the structure of the IL, which may enhance catalytic activity and FE for a product, and even control the reaction pathways.
- (3) The interfacial properties and the mechanisms in IL-based electrolytes are still unclear. To further understand  $CO_2$  reduction in IL-based electrolytes, comprehensive recognition of the theoretical and experimental mechanisms is needed. An in-depth study should also be carried out on the role of cations and anions in ILs and the microscopic mechanism of proton-electron transport and transfer. It is expected that combining *in situ* techniques with theoretical calculations can be used to address this issue.

Based on the above discussion, CO<sub>2</sub> electroreduction in IL-based electrolytes can be used to produce many value-added chemicals and feedstocks for fuels. The design of functionalized, low-toxicity, and easily prepared ILs will have broad application in CO<sub>2</sub> electrore-

duction. Although exploring efficient catalyst-electrolyte systems for  $CO_2$  electroreduction is challenging, it should be given much attention because it is crucial for the development of this area.

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# **Declaration of interests**

The authors declare no competing interests.

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