

# Inhibition Effect of $\text{KHCO}_3$ and $\text{KH}_2\text{PO}_4$ on Ethylene Explosion

Yang Wang, JingJing Yang, Jia He, XiaoPing Wen, WenTao Ji,\* and Yan Wang\*

Cite This: *ACS Omega* 2023, 8, 7566–7574

Read Online

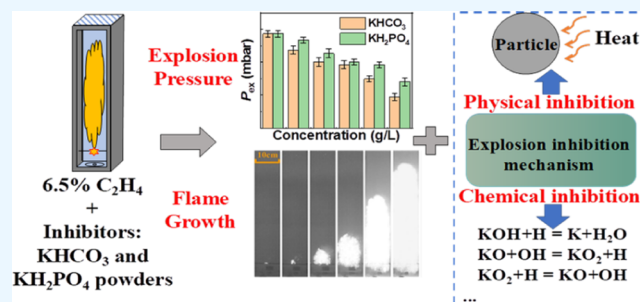
ACCESS |

Metrics &amp; More

Article Recommendations

Supporting Information

**ABSTRACT:** The explosion risk of ethylene ( $\text{C}_2\text{H}_4$ ) seriously hinders safe development of its production and processing. To reduce the harm caused by  $\text{C}_2\text{H}_4$  explosion, an experimental study was conducted to assess the explosion inhibition characteristics of  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powders. The experiments were conducted based on the explosion overpressure and flame propagation of the 6.5%  $\text{C}_2\text{H}_4$ –air mixture in a 5 L semi-closed explosion duct. Both the physical and chemical inhibition characteristics of the inhibitors were mechanistically assessed. The results showed that the 6.5%  $\text{C}_2\text{H}_4$  explosion pressure ( $P_{\text{ex}}$ ) decreases by increasing the concentration of  $\text{KHCO}_3$  or  $\text{KH}_2\text{PO}_4$  powder. The inhibition effect of  $\text{KHCO}_3$  powder on the  $\text{C}_2\text{H}_4$  system explosion pressure was better than that of the  $\text{KH}_2\text{PO}_4$  powder under similar concentration conditions. Both powders significantly affected the flame propagation of the  $\text{C}_2\text{H}_4$  explosion. Compared with  $\text{KH}_2\text{PO}_4$  powder,  $\text{KHCO}_3$  powder had a better inhibition effect on the flame propagation speed, but its ability to reduce the flame luminance was less than  $\text{KH}_2\text{PO}_4$  powder. Finally, the inhibition mechanism(s) of  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powders were revealed based on the powders' thermal characteristics and gas-phase reaction.



## 1. INTRODUCTION

$\text{C}_2\text{H}_4$  is the primary raw material for most of the chemical and petroleum industry applications. Therefore, its output, production scale, and production technology level become critical indicators to assess the developments in the chemical and petroleum processes.<sup>1,2</sup> Due to the high explosion sensitivity of  $\text{C}_2\text{H}_4$ , it is very easy to cause fire and even explosion accidents during its production and utilization. For example, the explosions of EVAL Plant in the United States in 2018 and that of the Sinopec Maoming Petrochemical Company in 2022 were caused by  $\text{C}_2\text{H}_4$ .<sup>3,4</sup> The explosion risk of  $\text{C}_2\text{H}_4$  has seriously hindered the development of some specific processes in the chemical and petroleum industries. Therefore, it is imperative to study the inhibition of  $\text{C}_2\text{H}_4$  explosion to reduce/control personnel and property loss.

According to the wealth of literature on explosion prevention and control, it is clear that explosion inhibitors not only result in a more safe and reliable operation involving certain chemicals but also effectively reduce the explosion intensity and generation of toxic and harmful gases.<sup>5</sup> The commonly used inhibitors include inert gas, powder inhibitors, and water mist.<sup>6</sup> Among them, inert gas mainly inhibits explosions through a physical process, and its application scope is limited.<sup>7</sup> Although the water mist significantly suppresses the explosion and does not cause secondary pollution, its practical application is difficult due to its immature technology.<sup>8</sup> In contrast, powder inhibitors are favored in the chemical industry due to their low price, strong environmental adaptability, and physical and chemical inhibition.<sup>9</sup>

With the improvement of environmental protection policies, there are other characteristics to select appropriate powder inhibitors besides their explosion hindering performance such as their impact on the ecological environment. For instance, halon inhibitors with good fire extinguishing and explosion suppression characteristics have been gradually abandoned, and instead, efficient alkali metal compounds with environmentally friendly characteristics have been utilized over the years.<sup>10</sup> Two alkali metal compounds of  $\text{KHCO}_3$  and  $\text{NaHCO}_3$  have been widely studied in the literature.<sup>11,12</sup> Using a modeling approach, Babushok<sup>13</sup> demonstrated that  $\text{KHCO}_3$  and  $\text{NaHCO}_3$  particles exhibit better inhibition effects than  $\text{CF}_3\text{Br}$  (halon-1301) under ideal conditions.

The effects of alkali metals on methane explosion inhibition under various factors (i.e., concentration, inhibitor type, and oxygen concentration) have been extensively studied.<sup>14–16</sup> Some studies on flammable gas explosion showed that explosion intensity of olefin gas is often greater than that of alkane gas, with a more complicated explosion process.<sup>17–19</sup> To better ensure safe development of the  $\text{C}_2\text{H}_4$  industry, it is necessary to study the inhibition mechanisms associated with  $\text{C}_2\text{H}_4$  explosion. Even though various concentrations of

Received: October 26, 2022

Accepted: November 28, 2022

Published: February 14, 2023



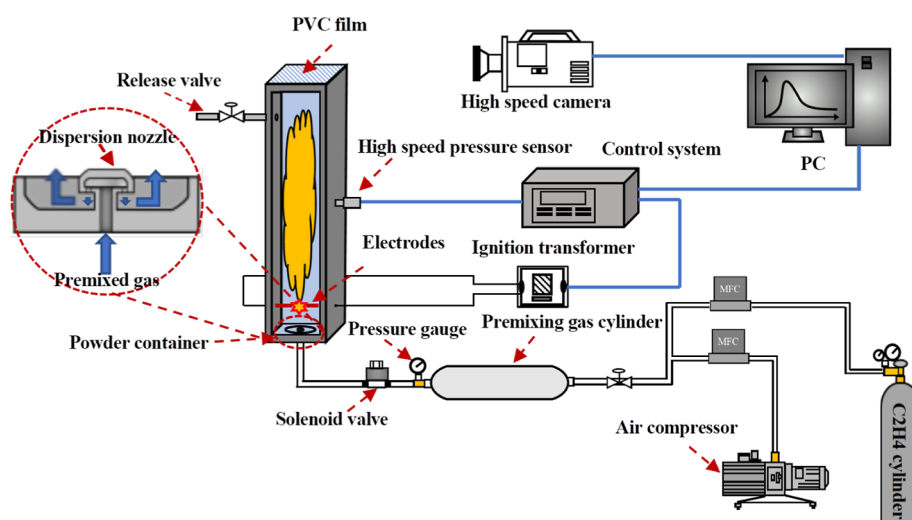


Figure 1. Schematic representation of the experimental apparatus.

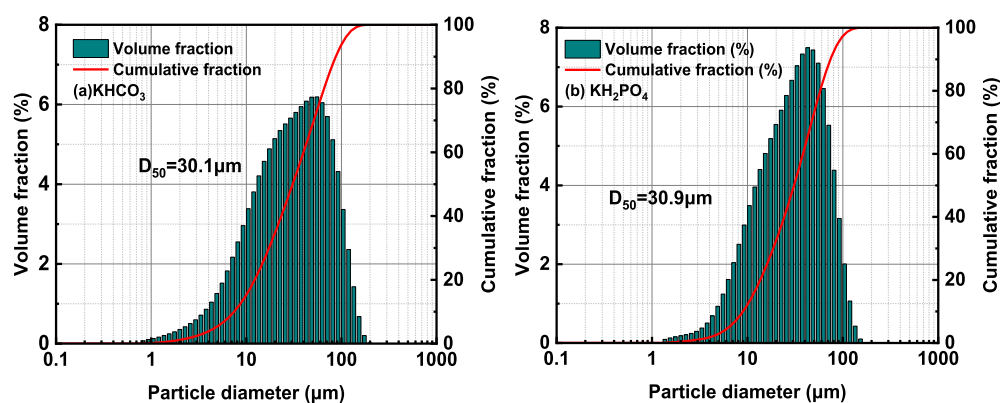


Figure 2. Particle size distribution of two inhibitors: (a)  $\text{KHCO}_3$  powder and (b)  $\text{KH}_2\text{PO}_4$  powder.

$\text{KH}_2\text{PO}_4$  powder proved to be the best explosion inhibitor for the  $\text{C}_2\text{H}_4$  system,<sup>20</sup> its performances against other traditional alkali metal inhibitors (i.e.,  $\text{KHCO}_3$  or  $\text{NaHCO}_3$ ) have not been studied yet. Since the explosion inhibition characteristics of  $\text{KHCO}_3$  in the flammable gas systems are generally better than those of  $\text{NaHCO}_3$ ,<sup>21</sup> we selected  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powder inhibitors in this study in order to explore more ideal  $\text{C}_2\text{H}_4$  explosion inhibitors.

In the experiments involving  $\text{C}_2\text{H}_4$  explosion inhibitors, the explosion overpressure and explosion index are mostly used to assess explosion inhibition performance.<sup>22,23</sup> However, the use of the explosion characteristic parameters only cannot reveal the inhibition mechanisms for the  $\text{C}_2\text{H}_4$  system. Analysis of the explosion inhibition mechanism is generally based on the explosion flame propagation.<sup>24</sup>

In this study,  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powder inhibitors were used in  $\text{C}_2\text{H}_4$  explosion experiments with an equivalent  $\text{C}_2\text{H}_4$  concentration of 6.5% in a 5 L semi-closed transparent explosion duct. By analyzing the effect of these two explosion inhibitors on the overpressure and flame propagation characteristics of the  $\text{C}_2\text{H}_4$  system at different concentrations, the explosion inhibition mechanisms of  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  were revealed considering the combined thermal characteristics of the two inhibitors and the kinetic mechanism of the gas-phase reaction kinetics. The experimental results obtained in this study can be applied to the explosion suppression of

$\text{C}_2\text{H}_4$  and also provide a theoretical basis for the explosion prevention of the  $\text{C}_2\text{H}_4$  industry.

## 2. EXPERIMENTAL SECTION

**2.1. Experimental Apparatus.** The explosion system used in this study is shown in Figure 1. The explosion system included a 5 L semi-closed explosion duct, an ignition system, a powder dispersion system, a data acquisition system, a high-speed camera, and a time control system. For a detailed description of the experimental apparatus and methodology, please refer to our previous research work.<sup>25</sup>

For the  $\text{C}_2\text{H}_4$  explosion inhibition experiments, a camera with higher photo-capture frequency and more precise capture quality was used to record the dynamic nature of the process due to rapid propagation of the gas explosion flame. A VEO710 model camera, manufactured by Dantec Dynamics, was used in this study, with 6000 fps and a maximum resolution of  $1280 \times 800$  pixels. To make the powder uniformly dispersed in the duct, a powder dispersion pressure of 0.4 MPa was used in this study, along with an ignition delay time of 600 ms after a series of preliminary tests. The ignition system consisted of a 6 kV high-voltage transformer and ignition electrodes. The ignition electrodes were a pair of tungsten electrode rods set 50 mm above the powder container, with a gap of 4 mm between the two electrodes. The high-voltage transformer was able to generate 30 J sparks.

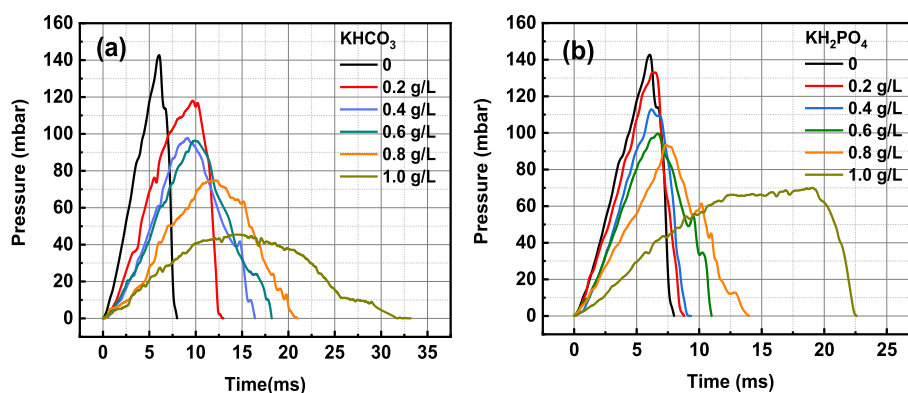


Figure 3. Pressure curves for  $C_2H_4$  explosion in the presence of two inhibitors: (a)  $KHCO_3$  powder and (b)  $KH_2PO_4$  powder.

**2.2. Experimental Materials.** The purity of  $C_2H_4$  used in the experiment was 99.99%.  $KHCO_3$  and  $KH_2PO_4$  powders were analytically pure. To avoid the effect of particle humidity and particle size difference on the experiments, the inhibitor powders were placed in a vacuum drying oven at  $60\text{ }^\circ\text{C}$  for 24 h before the experiments began, and the dried powders were tested using a Malvern laser particle size meter. The results are shown in Figure 2. According to the results, the median particle sizes of  $KHCO_3$  and  $KH_2PO_4$  powders were 30.1 and  $30.9\text{ }\mu\text{m}$ , respectively, that is, the particle size of the two inhibitor powder types was not much different and can be regarded as the same particle size.

### 3. RESULTS AND DISCUSSION

**3.1. Overpressure Variation of  $C_2H_4$  Explosion in the Presence of Inhibitors.** Six different concentrations of inhibitors (i.e., 0.0, 0.2, 0.4, 0.6, 0.8, and 1.0 g/L) were selected, and the effect of inhibitor concentration change on  $P_{ex}$  associated with the 6.5%  $C_2H_4$  system was studied. In Figure 3a,b, the pressure curves for  $C_2H_4$  explosion in the presence of two inhibitors are shown, in which the peak value is  $P_{ex}$ . It is clear that  $P_{ex}$  of  $C_2H_4$  gradually decreased by increasing the inhibitor concentration, that is, both  $KHCO_3$  and  $KH_2PO_4$  powders had an excellent inhibition effect on  $C_2H_4$  explosion. The pressure rise phase can also be used to assess the explosion risk.<sup>6</sup> The steeper the rising curve, the greater the explosion risk. In this study, the pressure rise curve gradually became flat with increasing inhibitor concentration, that is, the increasing rate of explosion pressure associated with the  $C_2H_4$  system gradually decreased under the action of two inhibitors.

For precise comparison of the inhibitor effect, the  $P_{ex}$  variations under the action of  $KHCO_3$  and  $KH_2PO_4$  powders at different concentrations were summarized (Figure 4).  $P_{ex}$  associated with  $C_2H_4$  explosion with no inhibitor was 143 mbar. At various  $KHCO_3$  powder concentrations,  $P_{ex}$  was decreased to 118.4, 100.3, 96.1, 74.8, and 47.2 mbar. The effect of  $KH_2PO_4$  powder on  $P_{ex}$  values was weaker, leading to 133.6, 113.4, 100.2, 95.8, and 70.1 mbar values, respectively. It is concluded that  $KHCO_3$  powder had a stronger impact on reducing  $P_{ex}$ , leading to more effective explosion overpressure inhibition.

**3.2. Flame Propagation Behavior of  $C_2H_4$  Explosion in the Presence of Inhibitors.** Through analysis of images captured during the tests, it was found that the explosion flame brightness in the presence of  $KHCO_3$  was greater than that of  $KH_2PO_4$  at similar concentrations, which makes it impossible

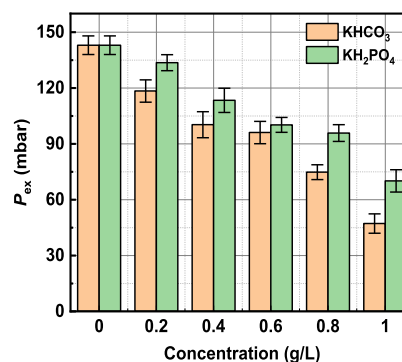


Figure 4. Effect of various inhibitor concentrations on  $P_{ex}$  of  $C_2H_4$ .

to clearly observe the effect of  $KHCO_3$  on the  $C_2H_4$  explosion reaction zone. The reason for this experimental phenomenon is that the content of potassium and its compounds produced by pyrolysis of  $KHCO_3$  particles under the same conditions is slightly larger than that of  $KH_2PO_4$  particles, resulting in enhanced flame emissivity and higher brightness.<sup>26,27</sup> Therefore, we selected  $KH_2PO_4$  powder to analyze the flame behavior under various experimental conditions. The flame images associated with various  $KHCO_3$  powder concentrations in the  $C_2H_4$  explosion system can be found in the Supporting Information.

In Figure 5, the flame propagation of the 6.5%  $C_2H_4$  explosion system is shown. Clearly, the explosion flame brightness is strong after  $C_2H_4$  was ignited, which is consistent with previous research results.<sup>28,29</sup> The flame propagation process can be divided into two stages: flame growth stage,

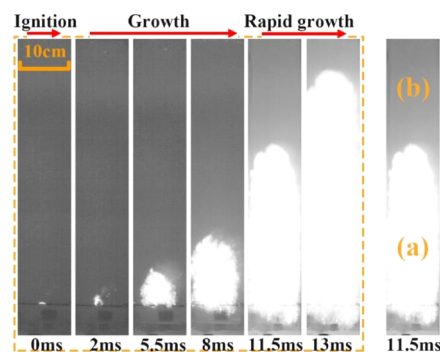
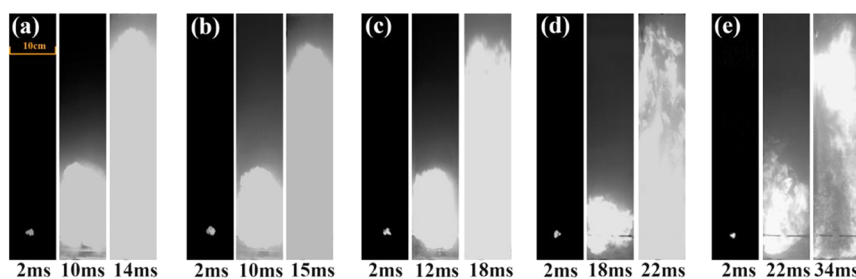
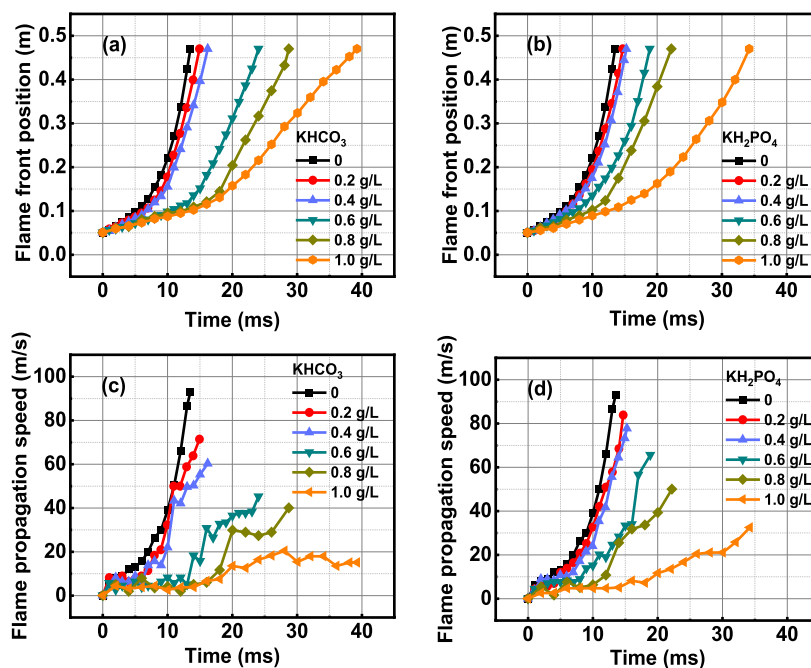


Figure 5. 6.5%  $C_2H_4$  explosion flame propagation: (a) explosion reaction zone and (b) unreacted zone.



**Figure 6.** Flame propagation behavior associated with  $C_2H_4$  explosion under different  $KH_2PO_4$  inhibitor concentrations of (a) 0.2, (b) 0.4, (c) 0.6, (d) 0.8, and (e) 1.0 g/L.



**Figure 7.** Effects of two different inhibitor concentrations on  $C_2H_4$  explosion flame: (a,b) effects of inhibitors on flame front position and (c,d) effects of inhibitors on flame propagation speed.

during which the flame slowly grew upward and approached the duct wall. The second is the rapid growth stage of the flame during which the flame propagated upward in a finger shape after coming into contact with the duct wall, and the propagation speed was gradually accelerated. During the propagation of the entire explosion flame, we divided the explosion area into an explosion reaction zone and an unreacted zone based on previous research results.<sup>28</sup> The bright flame area in the duct is the explosion reaction area, that is, the (a) area in the figure. The remaining (b) area is unreacted zones. In this study, the effects of different concentrations of inhibitors on the  $C_2H_4$  explosion flame considering these two stages were studied. During the flame propagation process, the irregular shape of the flame front may be caused by factors such as turbulent fields and thermal diffusion instability.<sup>24,30</sup>

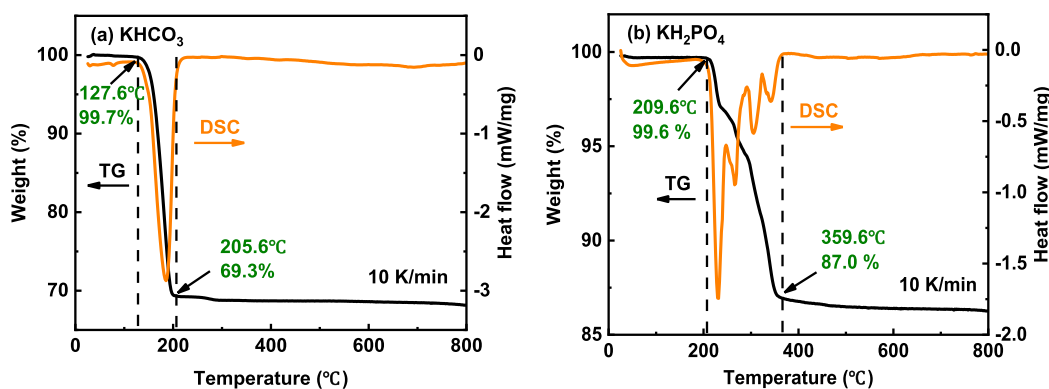
In Figure 6, the  $C_2H_4$  explosion flame during two flame propagation stages is displayed after the addition of various  $KH_2PO_4$  concentrations. The first two flame images of each group belong to the first stage. According to this figure, adding a small amount of  $KH_2PO_4$  powder enhanced the flame brightness, resulting in the local changes in the flame that cannot be visually displayed. By increasing the inhibitor concentration, the flame became irregular. At this time, the

explosion reaction zone began to appear as a local area with weak brightness. After adding 0.8 g/L  $KH_2PO_4$  powder, the distribution of this area became more obvious in the second stage of the flame, which led to a discrete flame state. When the  $KH_2PO_4$  powder concentration was 1.0 g/L, the flame in the first stage showed an apparent discrete state, and as the flame propagated to the second stage, a large area of weak brightness appeared in the explosion reaction zone. It is generally believed that these areas with weak brightness are originated from inhibition of the explosion flame.<sup>31</sup> From Figure 6, it is observed that the suppression effect of the  $KH_2PO_4$  inhibitor was increased with its concentration.

It is difficult to discuss the effect of  $KHCO_3$  powder on  $C_2H_4$  explosion flame behavior, but this does not mean that  $KHCO_3$  powder has a weak inhibitory effect on  $C_2H_4$  explosion flame propagation. Since many scholars' research on explosion flame propagation is mainly based on the analysis of flame propagation speed,<sup>32,33</sup> this study mainly compares the effects of two different concentrations of inhibitors on  $C_2H_4$  explosion flame through flame propagation speed.

**3.3. Flame Propagation Speed Associated with  $C_2H_4$  Explosion in the Presence of Inhibitors.** The effects of  $KHCO_3$  and  $KH_2PO_4$  inhibitors on the flame front position and propagation speed of the  $C_2H_4$  explosion flame are





**Figure 8.** Thermal decomposition characteristics of two inhibitors: (a)  $\text{KHCO}_3$  powder and (b)  $\text{KH}_2\text{PO}_4$  powder.

presented in Figure 7. The flame front position is defined as the distance between the highest point of the upward propagating flame and the base of the explosion duct. The flame propagation speed is the ratio of the flame front propagation distance to the propagation time. During explosion flame propagation, the pressure generated by the explosion reaction zone causes the concentrations of  $\text{C}_2\text{H}_4$  and inhibitors to decrease or close to zero at the proximity of the upper-end opening of the duct. To analyze the variations associated with the flame front position and propagation speed, the 470 mm area above the bottom of the duct was selected. According to Figure 7a,b, the flame generated by  $\text{C}_2\text{H}_4$  explosion reached the set position in the duct for the shortest time in the absence of any inhibitor, indicating that the average speed associated with  $\text{C}_2\text{H}_4$  flame propagation was the fastest in this case. With the addition of two different inhibitor concentrations, the average propagation speed associated with  $\text{C}_2\text{H}_4$  explosion flame was decreased with increasing inhibitor concentration. In Figure 7c,d, the effects of different inhibitors on the flame propagation speed associated with  $\text{C}_2\text{H}_4$  explosion at different times are displayed. From these figures, it is clear that the relations between the maximum propagation speed associated with  $\text{C}_2\text{H}_4$  explosion flame and powder concentration also show similar variations. According to the literature, high-quality inhibitors often significantly inhibit the propagation speed associated with explosion flames.<sup>34–37</sup> Clearly, high concentrations of  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powders are expected to be influential in inhibiting  $\text{C}_2\text{H}_4$  explosions.

From Figure 7, it is also observed that the flame propagation time associated with the explosion system in the presence of  $\text{KHCO}_3$  is longer under similar inhibitor concentration compared to the other inhibitor. This indicates that  $\text{KHCO}_3$  powder inhibited the  $\text{C}_2\text{H}_4$  explosion flame better than  $\text{KH}_2\text{PO}_4$  powder.

#### 4. MECHANISTIC ANALYSIS OF THE $\text{C}_2\text{H}_4$ EXPLOSION INHIBITION

It is known that alkali metal compounds inhibit explosions through physical and chemical mechanisms. The physical and chemical reactions are mainly heat absorption and gas-phase reaction, respectively.<sup>38</sup> The inhibition characteristics of  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powders were also mechanistically investigated in this research work.

**4.1. Physical Inhibition.** Physical inhibition is mainly achieved through heat absorption. In this study, the endothermic mechanism of the two powders was investigated by thermal analysis (Figure 8). From the TG curve presented

in Figure 8, it is clear that both  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powders had a mass loss stage that occurred in a temperature range of 127.6–205.6 and 209.6–359.6 °C, respectively. The temperature at which  $\text{KHCO}_3$  powder began to lose mass was less, indicating that the endothermic decomposition temperature of  $\text{KHCO}_3$  powder was less. The end temperature associated with  $\text{KH}_2\text{PO}_4$  weight loss was greater, indicating that the end of thermal decomposition for  $\text{KH}_2\text{PO}_4$  powder required a greater temperature.

As shown in Figure 8, there is an apparent differential scanning calorimetry front curve in the mass loss stage of both inhibitors, which is their endothermic peak. Previous studies have shown that the  $\text{KHCO}_3$  heat absorption in this stage was mainly decomposed into  $\text{KOH}$  and  $\text{CO}_2$ , and then part of  $\text{KOH}$  reacted with  $\text{HCO}_3^-$  to form  $\text{K}_2\text{CO}_3$  and  $\text{H}_2\text{O}$ .<sup>39</sup> Similarly,  $\text{KH}_2\text{PO}_4$  powder in this stage was mainly decomposed into  $\text{KPO}_3$  and  $\text{H}_2\text{O}$  after absorbing the heat.<sup>40</sup>  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  heat absorption values were 603.4 and 436.2 J/g, respectively. Clearly,  $\text{KHCO}_3$  powder had better heat absorption characteristics.

The key to explosion inhibition technology is reducing heat transfer from the explosion reaction zone to the unreacted zone.<sup>25</sup> According to the thermal characteristic results of these two inhibitors, the physical inhibition characteristics of  $\text{KHCO}_3$  for the  $\text{C}_2\text{H}_4$  explosion were stronger due to its lower trigger thermal decomposition temperature and greater endothermic characteristics. In addition, the  $\text{H}_2\text{O}$  produced by the two inhibitors and the additional  $\text{CO}_2$  produced by  $\text{KHCO}_3$  diluted the oxygen concentration in the explosion system. Other researchers believe that this method has little effect on the explosion;<sup>41,42</sup> therefore, it will not also be discussed in this paper.

**4.2. Chemical Inhibition.** Although the physical heat absorption mechanism of the two inhibitors reveals their physical inhibition characteristics, many scholars believe that  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powders inhibit gas explosion mainly through gas-phase reaction.<sup>43</sup> In this section, we look further into the explosion inhibition mechanism associated with these two powders through their chemical mechanism.

It is known that the explosion intensity of hydrocarbon fuels depends on how much H and OH radicals participate in the chain reaction during the combustion and explosion processes. One of the main reasons why  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powders are effective explosion inhibitors is that the  $\text{KOH}$  produced by their thermal decomposition can react with these free radicals to form other products, further blocking the explosive chain reaction containing hydrocarbon gases.<sup>9,44</sup> For the case of

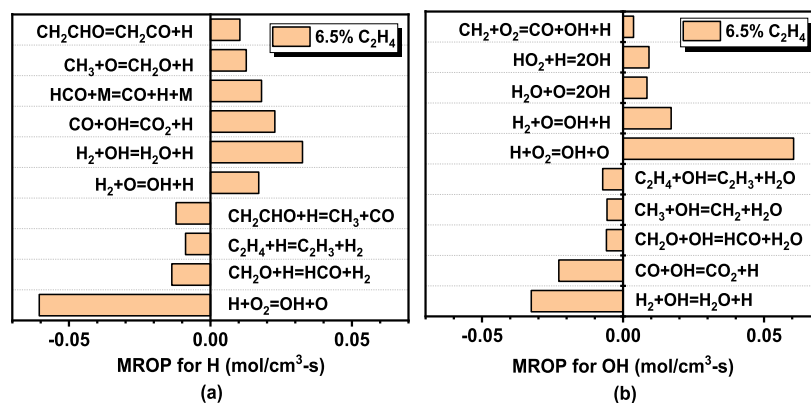


Figure 9. MROP for H (a) and OH (b) radicals of 6.5%  $C_2H_4$  explosion.

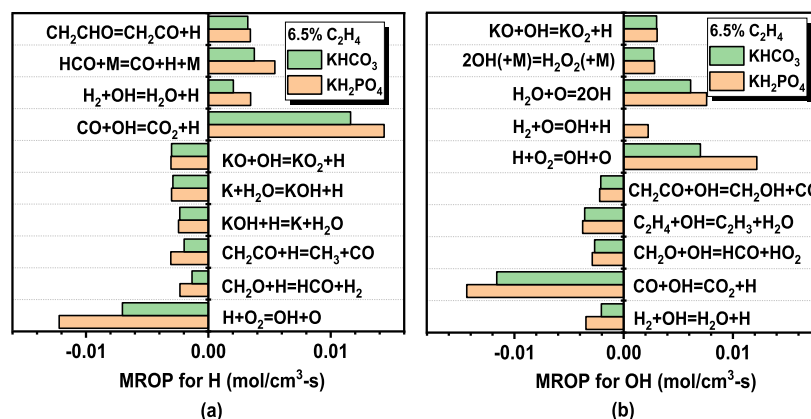


Figure 10. Effect of 1 g/L inhibitors on MROP of H (a) and OH (b).

$KH_2PO_4$  powder under high-temperature conditions, formation of a large concentrations of  $KPO_3$  does not exhibit any explosion inhibition characteristic.<sup>45</sup>  $KH_2PO_4$  powder can suppress the explosion through pyrolysis by producing a small amount of KOH.<sup>45,46</sup> Previous studies often use reaction kinetics to analyze the flame/explosion inhibition mechanism(s) of alkali metal compounds.<sup>15,38</sup> Constructing complex kinetic models for alkali metal compounds is computationally expensive. Therefore, metal hydroxides have been used as the main kinetic module for simplified calculation, which has proved to have a small effect on the results.<sup>38</sup> Therefore, in our study, only some of the mechanisms of KOH were considered in order to study the inhibition characteristics/mechanisms of  $KHCO_3$  and  $KH_2PO_4$ .

To reveal the chemical mechanism associated with these two inhibitors, the effect of KOH on H and OH radicals produced by  $C_2H_4$  explosion was considered through reaction kinetics, which has been proven to be a feasible approach in the literature.<sup>44,47,48</sup>

In this study, the effect of KOH on  $C_2H_4$  explosion was investigated using the zero-dimensional homogeneous reactor in CHEMKIN software package. The KOH kinetic module adopts a relatively high degree of recognition between all the kinetic models associated with the K-containing compounds.<sup>49</sup> The  $C_2H_4$  kinetic model uses the San Diego (UCSD) mechanism,<sup>50</sup> which is often used in studying  $C_2H_4$  combustion and explosion in the air medium. All the thermodynamic parameters in this model were from the JANAF thermodynamic database provided by Burcat<sup>51</sup> and the NIST database. The initial temperature and pressure of the

numerical simulation were set to 1300 K and 1 atm, respectively. This parameter setting refers to the initial boundary conditions of Wang's<sup>52</sup> numerical simulation model for explosion characteristics of 6.5%  $C_2H_4$ .

In addition, it was assumed that the K-compound produced by the rapid pyrolysis of  $KHCO_3$  and  $KH_2PO_4$  powders in an ideal high-temperature environment was KOH. It should be noted that in reality, the main product of  $KHCO_3$  rapid pyrolysis is KOH, while the rapid pyrolysis of  $KH_2PO_4$  produces less KOH. Therefore, the pyrolysis product in this study was artificially enhanced compared with the real case of application of  $KH_2PO_4$  for  $C_2H_4$  explosion inhibition. To more significantly analyze the effect of KOH on H and OH radicals during  $C_2H_4$  explosion, we selected 1 g/L concentration of  $KHCO_3$  and  $KH_2PO_4$  powders in this study.

In the complex reaction system of hydrocarbon fuel, analysis of the maximum rate of production (MROP) is often used to reveal the effect of essential reaction on the formation and consumption of components.<sup>47,48</sup> In this study, the chemical inhibition of the two inhibitors is assessed through their effect on MROP of H and OH radicals. In Figures 9 and 10, variations of the explosion system without and with inhibitors are shown, respectively. From the variations in H and OH radicals in the two figures, the effectiveness of inhibitors is proven. For example, the main reactions of H radical formation and consumption without adding explosion inhibitors are  $H_2 + OH = H_2O + H$  and  $H + O_2 = OH + O$ , and their MROP values are approximately 0.03 and  $-0.06 \text{ mol/cm}^3 \text{ s}$ , respectively (Figure 9). The MROP of these two reactions are about 0.003 and  $-0.01 \text{ mol/cm}^3 \text{ s}$  after adding the

inhibitors. Similar variations can also be found for the OH radicals. Therefore,  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powders are able to inhibit the chain reaction of H and OH radicals during the  $\text{C}_2\text{H}_4$  explosion, resulting in reduction of the explosion intensity.

As shown in Figure 10,  $\text{KHCO}_3$  powder has a significant effect on the MROP of H and OH radical inhibition, which is related to the KOH content. For  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powders with the same mass, the thermal decomposition of  $\text{KHCO}_3$  powder produces more KOH because the relative molecular mass of  $\text{KHCO}_3$  was smaller than that of  $\text{KH}_2\text{PO}_4$ . In addition, previous experimental results showed that KOH was difficult to produce from  $\text{KH}_2\text{PO}_4$  powder,<sup>42</sup> so the MROP inhibition effect of  $\text{KH}_2\text{PO}_4$  powder on H and OH radicals is less than the simulation results. However, according to the macroscopic results of overpressure and flame propagation for  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$ , the difference in their inhibition performances is not particularly significant. This suggests that during the pyrolysis process of  $\text{KH}_2\text{PO}_4$ , other components except  $\text{KPO}_3$  also participated in the chain reaction process. Since P-containing compounds have been also found useful as flame inhibition products, we speculate that a small amount of P-containing components may have been involved in the reaction process. According to the literature, the inhibition effect of  $\text{KHCO}_3$  is greater than that of  $\text{KH}_2\text{PO}_4$ ,<sup>21</sup> which indicates that the P-containing components have no significant explosion inhibition effect. Due to the lack of detailed  $\text{KH}_2\text{PO}_4$  reaction kinetic equations and thermodynamic parameters, the chemical inhibition mechanism of the two powders should be further studied in the future.

## 5. CONCLUSIONS

In this study,  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powders were used to inhibit the explosion process of 6.5%  $\text{C}_2\text{H}_4$  in a 5 L semi-closed duct system. The explosion inhibition mechanism of these two powders was studied from both physical and chemical perspectives. The following conclusions are drawn from this study:

- (1) After  $\text{KHCO}_3$  and  $\text{KH}_2\text{PO}_4$  powders were added to the  $\text{C}_2\text{H}_4$  explosion system, the  $P_{\text{ex}}$  of 6.5%  $\text{C}_2\text{H}_4$  decreased with the inhibitor concentrations, and the inhibition effect of  $\text{KHCO}_3$  powder on the  $P_{\text{ex}}$  of  $\text{C}_2\text{H}_4$  was better than that of  $\text{KH}_2\text{PO}_4$  powder at similar concentrations.
- (2) The average and maximum flame propagation speeds associated with  $\text{C}_2\text{H}_4$  explosion were decreased by increasing the inhibitor concentration. When the inhibitor concentrations were the same,  $\text{KH}_2\text{PO}_4$  powder was weaker than  $\text{KHCO}_3$  powder in reducing the propagation speed of  $\text{C}_2\text{H}_4$  explosion, but its ability to reduce the luminous brightness of  $\text{C}_2\text{H}_4$  flame was better than  $\text{KHCO}_3$  powder.
- (3) Compared with  $\text{KH}_2\text{PO}_4$  powder,  $\text{KHCO}_3$  powder was superior in physical flame/explosion inhibition due to its lower initial pyrolysis temperature and higher heat absorption.
- (4) According to the reaction kinetic model, the chemical inhibition characteristics of  $\text{KHCO}_3$  powder were better than those of  $\text{KH}_2\text{PO}_4$  powder. This is due to the production of greater values of KOH from rapid pyrolysis of  $\text{KHCO}_3$  than  $\text{KH}_2\text{PO}_4$ . Therefore,  $\text{KHCO}_3$  powder seemed to be a more efficient additive in inhibiting the chain reaction of H and OH radicals.

## ■ ASSOCIATED CONTENT

### Supporting Information

The Supporting Information is available free of charge at <https://pubs.acs.org/doi/10.1021/acsomega.2c06894>.

Flame propagation behavior associated with  $\text{C}_2\text{H}_4$  explosion under different  $\text{KHCO}_3$  inhibitor concentrations, change in species fraction during 6.5%  $\text{C}_2\text{H}_4$  explosion, and effects of two inhibitors on the  $\text{C}_2\text{H}_4$  explosion process (PDF)

## ■ AUTHOR INFORMATION

### Corresponding Authors

**WenTao Ji** – State Key Laboratory Cultivation Bases for Gas Geology and Gas Control, College of Safety Science and Engineering, Henan Polytechnic University, Jiaozuo 454003, China; The Collaboration Innovation Center of Coal Safety Production of Henan Province, Henan Polytechnic University, Jiaozuo 454003, China; [orcid.org/0000-0002-2085-7007](https://orcid.org/0000-0002-2085-7007); Email: [jwentao@hpu.edu.cn](mailto:jwentao@hpu.edu.cn)

**Yan Wang** – State Key Laboratory Cultivation Bases for Gas Geology and Gas Control, College of Safety Science and Engineering, Henan Polytechnic University, Jiaozuo 454003, China; The Collaboration Innovation Center of Coal Safety Production of Henan Province, Henan Polytechnic University, Jiaozuo 454003, China; [orcid.org/0000-0001-6671-4661](https://orcid.org/0000-0001-6671-4661); Email: [yanwang@hpu.edu.cn](mailto:yanwang@hpu.edu.cn)

### Authors

**Yang Wang** – State Key Laboratory Cultivation Bases for Gas Geology and Gas Control, College of Safety Science and Engineering, Henan Polytechnic University, Jiaozuo 454003, China; The Collaboration Innovation Center of Coal Safety Production of Henan Province, Henan Polytechnic University, Jiaozuo 454003, China

**JingJing Yang** – State Key Laboratory Cultivation Bases for Gas Geology and Gas Control, College of Safety Science and Engineering, Henan Polytechnic University, Jiaozuo 454003, China; The Collaboration Innovation Center of Coal Safety Production of Henan Province, Henan Polytechnic University, Jiaozuo 454003, China

**Jia He** – State Key Laboratory Cultivation Bases for Gas Geology and Gas Control, College of Safety Science and Engineering, Henan Polytechnic University, Jiaozuo 454003, China; The Collaboration Innovation Center of Coal Safety Production of Henan Province, Henan Polytechnic University, Jiaozuo 454003, China

**XiaoPing Wen** – School of Mechanical and Power Engineering, Henan Polytechnic University, Jiaozuo 454003, China; [orcid.org/0000-0002-5821-5130](https://orcid.org/0000-0002-5821-5130)

Complete contact information is available at: <https://pubs.acs.org/10.1021/acsomega.2c06894>

### Notes

The authors declare no competing financial interest.

## ■ ACKNOWLEDGMENTS

This study was supported by the National Natural Science Foundation of China (51904094, 51874120, and 51974107).

## ■ REFERENCES

- (1) Ding, Q.; Zhang, Z.; Zhang, P.; Yu, C.; He, C.-H.; Cui, X.; Xing, H. One-step ethylene purification from ternary mixture by synergetic



- molecular shape and size matching in a honeycomb-like ultra-microporous material. *J. Chem. Eng. Mater. Sci.* **2022**, *450*, 138272.
- (2) Yao, L.; King, J.; Wu, D.; Ma, J.; Li, J.; Xie, R.; Chuang, S. S. C.; Miyoshi, T.; Peng, Z. Non-Thermal Plasma-Assisted Rapid Hydrogenolysis of Polystyrene to High Yield Ethylene. *Nat. Commun.* **2022**, *13*, 885.
- (3) <https://www.csb.gov/csb-investigators-deploying-to-incident-at-the-kuraray-america-eval-facility-in-pasadena-texas/> (accessed November 10, 2022).
- (4) <https://www.119.gov.cn/xw/mtbd/tpbd/2022/29746.shtml> (accessed November 11, 2022).
- (5) Cao, X.; Wei, H.; Wang, Z.; Fan, L.; Zhou, Y.; Wang, Z. Experimental Research on the Inhibition of Methane/Coal Dust Hybrid Explosions by the Ultrafine Water Mist. *Fuel* **2023**, *331*, 125937.
- (6) Yu, M.; Wang, X.; Zheng, K.; Han, S.; Chen, C.; Si, R.; Wang, L. Investigation of Methane/Air Explosion Suppression by Modified Montmorillonite Inhibitor. *Process Saf. Environ. Prot.* **2020**, *144*, 337–348.
- (7) Zheng, K.; Yang, X.; Yu, M.; Si, R.; Wang, L. Effect of N<sub>2</sub> and CO<sub>2</sub> on Explosion Behavior of Syngas/Air Mixtures in a Closed Duct. *Int. J. Hydrogen Energy* **2019**, *44*, 28044–28055.
- (8) Song, Y.; Zhang, Q. Quantitative Research on Gas Explosion Inhibition by Water Mist. *J. Hazard. Mater.* **2019**, *363*, 16–25.
- (9) Ji, W.-T.; Yang, J.-J.; He, J.; Wang, Y.; Wen, X.-P.; Wang, Y. Preparation and Characterization of Flower-like Mg-Al Hydrotalcite Powder for Suppressing Methane Explosion. *J. Loss Prev. Process. Ind.* **2022**, *80*, 104858.
- (10) Dounia, O.; Vermorel, O.; Jaravel, T.; Poinot, T. Time Scale Analysis of the Homogeneous Flame Inhibition by Alkali Metals. *Proc. Combust. Inst.* **2021**, *38*, 2371–2378.
- (11) Liu, Z.; Zhong, X.; Zhang, Q.; Lu, C. Experimental Study on Using Water Mist Containing Potassium Compounds to Suppress Methane/Air Explosions. *J. Hazard. Mater.* **2020**, *394*, 122561.
- (12) Mitani, T.; Niioka, T. Extinction Phenomenon of Premixed Flames with Alkali Metal Compounds. *Combust. Flame* **1984**, *55*, 13–21.
- (13) Babushok, V. I.; Linteris, G. T.; Hoorelbeke, P.; Roosendans, D.; van Wingerden, K. Flame Inhibition by Potassium-Containing Compounds. *Combust. Sci. Technol.* **2017**, *189*, 2039–2055.
- (14) Wang, Y.; Cheng, Y.; Yu, M.; Li, Y.; Cao, J.; Zheng, L.; Yi, H. Methane Explosion Suppression Characteristics Based on the NaHCO<sub>3</sub>/Red-Mud Composite Powders with Core-Shell Structure. *J. Hazard. Mater.* **2017**, *335*, 84–91.
- (15) Shi, Z.; Zheng, L.; Zhang, J.; Miao, Y.; Wang, X.; Wang, Y.; Tang, S. Effect of Initial Pressure on Methane/Air Deflagrations in the Presence of NaHCO<sub>3</sub> Particles. *Fuel* **2022**, *325*, 124910.
- (16) Cao, X.; Bi, M.; Ren, J.; Chen, B. Experimental Research on Explosion Suppression Affected by Ultrafine Water Mist Containing Different Additives. *J. Hazard. Mater.* **2019**, *368*, 613–620.
- (17) Wang, T.; Luo, Z.; Wen, H.; Cheng, F.; Liu, L.; Su, Y.; Liu, C.; Zhao, J.; Deng, J.; Yu, M. The Explosion Enhancement of Methane-Air Mixtures by Ethylene in a Confined Chamber. *Energy* **2021**, *214*, 119042.
- (18) Wang, K.; Su, M.; Wei, L.; Chen, S.; Kong, X.; Fang, Y. Effect of Initial Turbulence on Explosion Behavior of Stoichiometric Methane-Ethylene-Air Mixtures in Confined Space. *Process Saf. Environ. Prot.* **2022**, *161*, 583–593.
- (19) Razus, D.; Mitu, M.; Giurcan, V.; Movileanu, C.; Oancea, D. Additive Influence on Maximum Experimental Safe Gap of Ethylene-Air Mixtures. *Fuel* **2019**, *237*, 888–894.
- (20) Wang, Y.; Li, Z.; Zhang, Y.; Wang, Y.; Yang, J.; Ji, W. Suppression characteristics and mechanism of different hydrogen phosphates on ethylene explosion. *China Saf. Sci. J.* **2022**, *32*, 48–54.
- (21) Badhuk, P.; Ravikrishna, R. V. Flame Inhibition by Aqueous Solution of Alkali Salts in Methane and LPG Laminar Diffusion Flames. *Fire Saf. J.* **2022**, *130*, 103586.
- (22) Cao, Y.; Li, B.; Gao, K. Pressure Characteristics during Vented Explosion of Ethylene-Air Mixtures in a Square Vessel. *Energy* **2018**, *151*, 26–32.
- (23) Movileanu, C.; Gosa, V.; Razus, D. Explosion of gaseous ethylene-air mixtures in closed cylindrical vessels with central ignition. *J. Hazard. Mater.* **2012**, *235–236*, 108–115.
- (24) Dorofeev, S. B. Flame Acceleration and Explosion Safety Applications. *Proc. Combust. Inst.* **2011**, *33*, 2161–2175.
- (25) Ji, W.; Wang, Y.; Yang, J.; He, J.; Lu, C.; Wen, X.; Wang, Y. Explosion Overpressure Behavior and Flame Propagation Characteristics in Hybrid Explosions of Hydrogen and Magnesium Dust. *Fuel* **2023**, *332*, 125801.
- (26) Lu, G.; Yan, Y.; Cornwell, S.; Whitehouse, M.; Riley, G. Impact of Co-Firing Coal and Biomass on Flame Characteristics and Stability. *Fuel* **2008**, *87*, 1133–1140.
- (27) Fan, R.; Jiang, Y.; Qiu, R. A Compound Silica-Trifluoroacetyl Powder for Fire Suppressant: Preparation, Characterization and Suppression Mechanism Discussion. *Fire Saf. J.* **2020**, *115*, 103158.
- (28) Li, J.; Zhang, P.; Yuan, L.; Pan, Z.; Zhu, Y. Flame Propagation and Detonation Initiation Distance of Ethylene/Oxygen in Narrow Gap. *Appl. Therm. Eng.* **2017**, *110*, 1274–1282.
- (29) Wu, M.-H.; Wang, C.-Y. Reaction Propagation Modes in Millimeter-Scale Tubes for Ethylene/Oxygen Mixtures. *Proc. Combust. Inst.* **2011**, *33*, 2287–2293.
- (30) Oppong, F.; Luo, Z.; Li, X.; Song, Y.; Xu, C. Intrinsic Instability of Different Fuels Spherically Expanding Flames: A Review. *Fuel Process. Technol.* **2022**, *234*, 107325.
- (31) Zhao, Q.; Liu, J.; Chen, X.; Li, Y.; Yin, H.; Dai, H.; Huang, C. Hindrance and Suppression Characteristics of Local Whole-Inerting Zone on Flame Propagation of Methane/Coal Dust Deflagration. *Fuel* **2021**, *305*, 121483.
- (32) Zhu, C.; Gao, Z.; Lu, X.; Lin, B.; Guo, C.; Sun, Y. Experimental Study on the Effect of Bifurcations on the Flame Speed of Premixed Methane/Air Explosions in Ducts. *J. Loss Prev. Process. Ind.* **2017**, *49*, 545–550.
- (33) Cammarota, F.; Di Sarli, V.; Salzano, E.; Di Benedetto, A. Measurements of pressure and flame speed during explosions of CH<sub>4</sub>/O<sub>2</sub>/N<sub>2</sub>/CO<sub>2</sub> mixtures. *J. Loss Prev. Process. Ind.* **2016**, *44*, 771–774.
- (34) Cao, X.; Zhou, Y.; Wang, Z.; Fan, L.; Wang, Z. Experimental Research on Hydrogen/Air Explosion Inhibition by the Ultrafine Water Mist. *Int. J. Hydrogen Energy* **2022**, *47*, 23898–23908.
- (35) Zhang, S.; Bi, M.; Jiang, H.; Gao, W. Synergistic inhibition of aluminum dust explosion by gas-solid inhibitors. *J. Loss Prev. Process. Ind.* **2021**, *71*, 104511.
- (36) Liu, J.; Meng, X.; Yan, K.; Wang, Z.; Dai, W.; Wang, Z.; Li, F.; Yang, P.; Liu, Y. Study on the Effect and Mechanism of Ca(H<sub>2</sub>PO<sub>4</sub>)<sub>2</sub> and CaCO<sub>3</sub> Powders on Inhibiting the Explosion of Titanium Powder. *Powder Technol.* **2022**, *395*, 158–167.
- (37) Pei, B.; Li, S.; Yang, S.; Yu, M.; Chen, L.; Pan, R. Flame Propagation Inhibition Study on Methane/Air Explosion Using CO<sub>2</sub> Twin-Fluid Water Mist Containing Potassium Salt Additives. *J. Loss Prev. Process. Ind.* **2022**, *78*, 104817.
- (38) Jiang, H.; Bi, M.; Li, B.; Ma, D.; Gao, W. Flame Inhibition of Aluminum Dust Explosion by NaHCO<sub>3</sub> and NH<sub>4</sub>H<sub>2</sub>PO<sub>4</sub>. *Combust. Flame* **2019**, *200*, 97–114.
- (39) Zhao, W.; Wu, Y.; Cai, T.; Zhang, W.; Chen, X.; Liu, D. Density Functional Theory and Reactive Dynamics Study of Catalytic Performance of TiO<sub>2</sub> on CO<sub>2</sub> Desorption Process with KHCO<sub>3</sub>/TiO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> Sorbent. *Mol. Catal.* **2017**, *439*, 143–154.
- (40) Borges, R.; Soares Giroto, A.; Klatic, R.; Wypych, F.; Ribeiro, C. Mechanochemical Synthesis of Eco-Friendly Fertilizer from Eggshell (Calcite) and KH<sub>2</sub>PO<sub>4</sub>. *Adv. Powder Technol.* **2021**, *32*, 4070–4077.
- (41) Wei, S.; Yu, M.; Pei, B.; Xu, M.; Guo, J.; Hu, Z. Experimental and Numerical Study on the Explosion Suppression of Hydrogen/Dimethyl Ether/Methane/Air Mixtures by Water Mist Containing NaHCO<sub>3</sub>. *Fuel* **2022**, *328*, 125235.
- (42) Wang, Q.; Sun, Y.; Jiang, J.; Deng, J.; Shu, C.-M.; Luo, Z.; Wang, Q. Inhibiting effects of gas-particle mixtures containing CO<sub>2</sub>,



Mg(OH)<sub>2</sub> particles, and NH<sub>4</sub>H<sub>2</sub>PO<sub>4</sub> particles on methane explosion in a 20-L closed vessel. *J. Loss Prev. Process. Ind.* **2020**, *64*, 104082.

(43) Fan, R.; Jiang, Y.; Li, W.; Xiong, C.; Qiu, R. Investigation of the Physical and Chemical Effects of Fire Suppression Powder NaHCO<sub>3</sub> Addition on Methane-Air Flames. *Fuel* **2019**, *257*, 116048.

(44) Dong, Z.; Liu, L.; Chu, Y.; Su, Z.; Cai, C.; Chen, X.; Huang, C. Explosion Suppression Range and the Minimum Amount for Complete Suppression on Methane-Air Explosion by Heptafluoropropane. *Fuel* **2022**, *328*, 125331.

(45) Zhang, T. Fire-Extinguishing Performance and Mechanism Study on Water Mist with Potassium Additives. Ph.D. Thesis, Beijing Institute of Technology, China, 2020.

(46) Liu, B.; Xu, K.; Zhang, Y.; Ge, J. Gas-Liquid Dual Phase Inhibition Method for Explosion Accident of Wet Al Dust Collection System Based on KH<sub>2</sub>PO<sub>4</sub>. *Adv. Powder Technol.* **2022**, *33*, 103516.

(47) Zhou, S.; Luo, Z.; Gao, J.; Wang, T.; Li, R.; Hu, S.; Wang, L. Experimental and Chemical Kinetic Behaviors at the Explosion Reaction of Typical C<sub>6</sub> Hydrocarbons. *Fuel* **2022**, *322*, 124258.

(48) Zhou, J.; Jiang, H.; Zhou, Y.; Gao, W. Flame Suppression of 100 Nm PMMA Dust Explosion by KHCO<sub>3</sub> with Different Particle Size. *Process Saf. Environ. Prot.* **2019**, *132*, 303–312.

(49) Slack, M.; Cox, J. W.; Grillo, A.; Ryan, R.; Smith, O. Potassium Kinetics in Heavily Seeded Atmospheric Pressure Laminar Methane Flames. *Combust. Flame* **1989**, *77*, 311–320.

(50) <http://web.eng.ucsd.edu/mae/groups/combustion/mechanism.html> (accessed November 11, 2022).

(51) Burcat, A. Third Millennium Ideal Gas and Condensed Phase Thermochemical Database for Combustion With Updates From Active Thermochemical Tables. <http://garfield.chem.elte.hu/Burcat/burcat.html> (accessed September 2005).

(52) Wang, L.; Gao, J.; Pan, R.; Hu, S.; Zhou, S.; Yang, X.; Liu, Y. Effect and Mechanism Analysis of Wires Explosion-Proof Material on Ethylene-Air Explosion. *J. Loss Prev. Process. Ind.* **2022**, *80*, 104881.