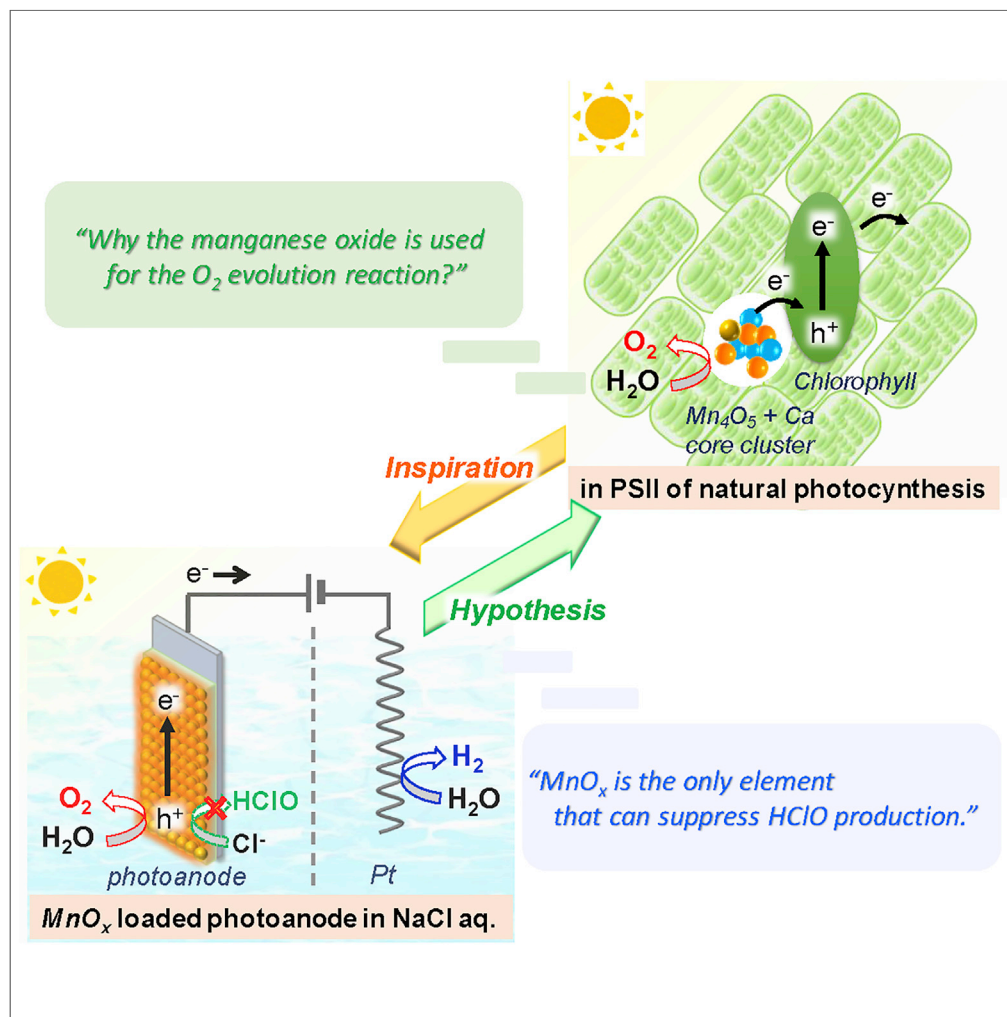


Article

# Functions of $MnO_x$ in NaCl Aqueous Solution for Artificial Photosynthesis



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**HIGHLIGHTS**

Selectivity of  $O_2/HClO$  production in NaCl aq. sol. on photoanodes was investigated

$MnO_x$  modification promoted  $O_2$  evolution specifically without  $HClO$  production

The results are useful for practical application of artificial photosynthesis

A hypothesis about the evolution in natural photosynthesis was proposed



## Article

Functions of  $\text{MnO}_x$  in NaCl Aqueous Solution for Artificial PhotosynthesisSayuri Okunaka,<sup>1</sup> Yugo Miseki,<sup>1</sup> and Kazuhiro Sayama<sup>1,2,\*</sup>

## SUMMARY

Photoelectrochemical water splitting has been intensively investigated as artificial photosynthesis technology to convert solar energy into chemical energy. The use of seawater and salted water has advantages for minimum environmental burden; however, the oxidation of  $\text{Cl}^-$  ion to hypochlorous acid (HClO), which has toxicity and heavy corrosiveness, should occur at the anode, along with the oxygen evolution. Here,  $\text{O}_2$  and HClO production in aqueous solution containing  $\text{Cl}^-$  on photoanodes modified with various metal oxides was investigated. The modification of  $\text{MnO}_x$  resulted in the promotion of the  $\text{O}_2$  evolution reaction (OER) specifically without HClO production over a wide range of conditions. The results will contribute not only to the practical application of artificial photosynthesis using salted water but also to the elucidation of substantial function of manganese as the element for OER center in natural photosynthesis.

## INTRODUCTION

Various photoanodes composed of oxide semiconductors on conducting glass substrate have been widely studied for artificial photosynthesis technology with water oxidation into  $\text{O}_2$  under simulated solar light and low applied bias in aqueous electrolyte solution (Fujishima and Honda, 1972; Hisatomi et al., 2014; Kang et al., 2015; Sivula and van de Krol, 2016; Roger et al., 2017), whereby the efficiency was determined to be improved by loading with metal oxides ( $\text{MO}_x$ ) such as  $\text{FeO}_x$ ,  $\text{NiO}_x$ , and  $\text{CoO}_x$  (Zhong et al., 2015; Chemelewski et al., 2014). The ability of  $\text{O}_2$  evolution reaction (OER) of  $\text{MO}_x$  has been further improved by modification with phosphate, borate, and carbonate ions (Kim and Choi, 2014; Bediako et al., 2012; Li et al., 2016). Moreover, the use of seawater and salted water for electrolyte solution has been investigated because of some significant advantages to minimize the environmental burden and provide cost reduction on electrochemical systems using photoanodes (Desilvestro and Grätzel, 1987; Luo et al., 2011; Barczuk et al., 2013; Fukuzumi et al., 2017; Iguchi et al., 2018) as well as metal anodes (Bennet., 1980; El-Moneim et al., 2009; Vos et al., 2018; Ibrahim and Canan, 2015; Gidon et al., 2018). However, in seawater containing  $\text{Cl}^-$  anions, hypochlorous acid (HClO, neutral form of  $\text{Cl}_2$ ) production reaction (abbreviated as CPR) by  $\text{Cl}^-$  oxidation proceeds concurrently with the OER by water oxidation (Figure 1). Although HClO is a valuable chemical for disinfection and bleaching to some extent (Sayama, 2018), control of the selectivity and the suppression of CPR on photoanodes are important requirements for  $\text{H}_2$  production in large-scale water-splitting systems because of the toxicity and corrosiveness of HClO (Fujimura et al., 1999). The CPR via 2-electron reaction proceeds easily compared with the OER via 4-electron reaction, whereas the OER is more preferable to the CPR with respect to the redox potential ( $\text{HClO}/\text{Cl}^- = \text{ca. } +1.28 \text{ V}$  and  $\text{O}_2/\text{H}_2\text{O} = +0.83 \text{ V}$  versus SHE,  $\text{pH} = 7$ ). There have been some reports that the CPR on metal anodes is effectively suppressed by the use of cation-exchange membranes or entirely coating the anode with  $\text{MnO}_x$  as  $\text{Cl}^-$ -impermeable layers (El-Moneim et al., 2009; Vos et al., 2018; Balaji et al., 2009), and by buffered conditions to maintain an alkaline pH (Dionigi et al., 2016). However, it is more difficult to suppress the CPR in unbuffered NaCl solution because the anode is subjected to partially acidic conditions. Here, we systematically investigated the effect of loading various simple metal oxide species ( $\text{MO}_x$ ), including precious metals, on the selectivity toward HClO/ $\text{O}_2$  production from unbuffered NaCl aqueous solution over a  $\text{BiVO}_4$  photoanode, which is one of the most popular visible-light responsible photoanodes for efficient water splitting (Hong et al., 2011; Saito et al., 2012; Fuku et al., 2017), and found that  $\text{MnO}_x$  loading could specifically suppress the CPR on the photoanode under a wide range of conditions. Finally, we could advocate a new hypothesis why manganese is selected as the element for OER center of natural photosynthesis (Barber., 1998; Yano et al., 2006; Umena et al., 2011). (Figure 1)

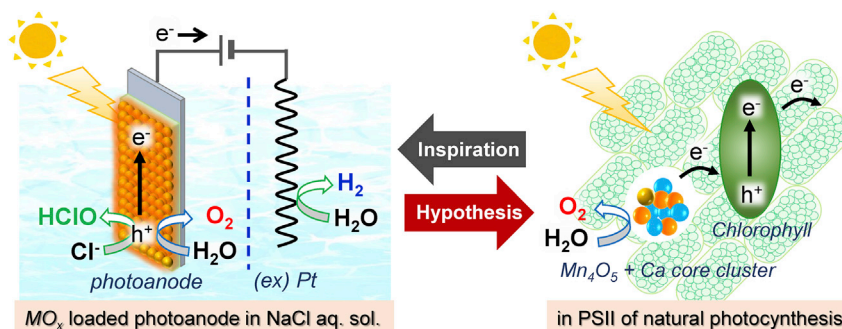
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**Figure 1. Reaction Images of the Artificial/Natural Photosynthesis Systems**

Reaction images of the artificial photosynthesis system using  $MO_x$ -loaded  $BiVO_4/WO_3/FTO$  photoanode (left) and  $Mn_4O_5 + Ca$  core cluster for OER and chlorophyll in PSII of natural photosynthesis (right).

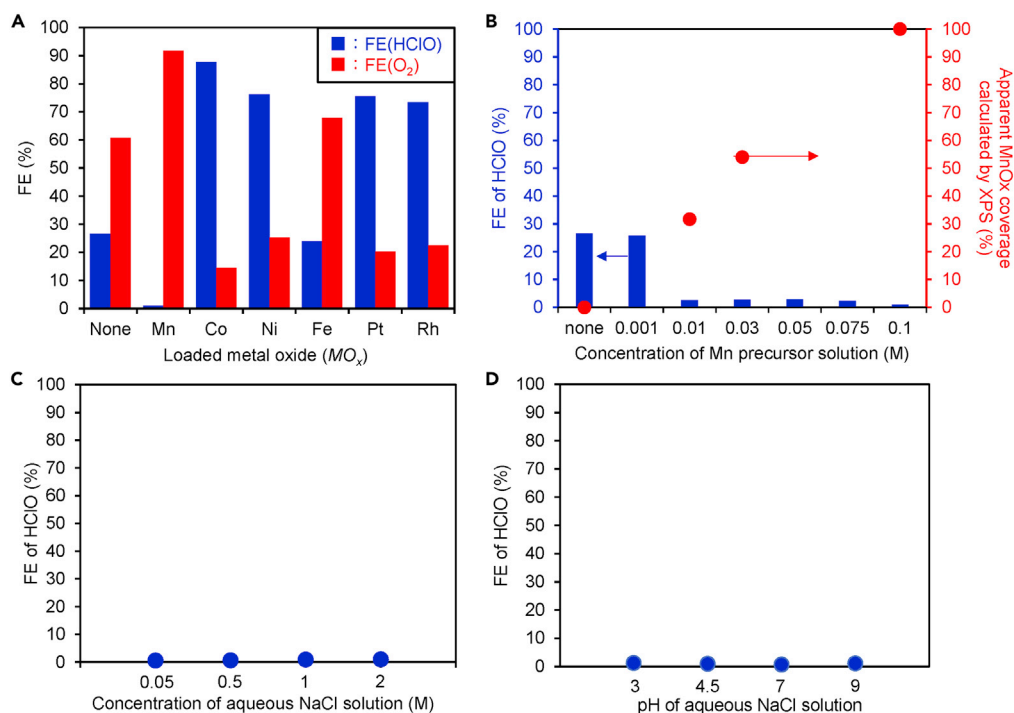
## RESULTS AND DISCUSSION

### Properties of $MO_x/BiVO_4/WO_3/FTO$ under Simulated Solar Light

A multilayer photoanode of  $BiVO_4/WO_3/FTO$  ( $FTO = F$ -doped  $SnO_2$  conducting glass), which has excellent performance for water splitting into  $H_2$  and  $O_2$  under low applied bias (Hong et al., 2011; Saito et al., 2012; Fuku et al., 2017), was used in this work. Figure 2A shows the faradaic efficiencies (FE) for  $O_2$  and  $HClO$  generation ( $FE(O_2)$  and  $FE(HClO)$ ) from aqueous  $NaCl$  solution on a  $BiVO_4/WO_3/FTO$  photoanode loaded with/without  $MO_x$  under simulated solar light (AM 1.5, 1 SUN). The potential required for the photo-electrolysis for steady current (2 mA) using these photoelectrodes was listed in Table S1. The bare photoanode produced both  $HClO$  and  $O_2$ , and other oxidative by-products ( $Cl_2$ ,  $HClO_2$ ,  $HClO_3$  etc.) were not generated, as we recently reported (Iguchi et al., 2018). For the all photoanodes, the sum of FE for the oxidative products ( $O_2$  and  $HClO$ ) became around 100% considering the measurement error (ca. 15%), which suggested the main products were  $O_2$  and  $HClO$ .  $O_2$  production with a high  $FE(O_2)$  of >90% was observed on the  $MnO_x/BiVO_4/WO_3/FTO$  photoanode, and no significant amount of  $HClO$  was detected with  $MnO_x$  loading.  $FE(HClO)$  with a  $CoO_x$ -loaded photoanode was increased to ca. 88%. The dependence of  $FE(HClO)$  on the concentration of the Mn precursor solution and the concentration or pH of aqueous  $NaCl$  electrolyte solution were also investigated (Figures 2B–2D), and the CPR was effectively suppressed when the Mn precursor concentration was  $\geq 0.01$  M, the  $NaCl$  concentration was between 0.05 M–2 M, or the pH was between 3 and 9, respectively. Figure S1A shows current-potential ( $I$ - $V$ ) curves for the  $MnO_x/BiVO_4/WO_3/FTO$  photoanodes under simulated solar light though a light chopper. The photocurrent could be observed on the photoanodes with or without  $MnO_x$  at much less than +0.88 V versus SHE, pH = 7. The optimum preparation temperature for  $MnO_x$  loading was 400°C for the best photocurrent among all  $MnO_x$ -loaded photoanodes (Figure S1B). The photocurrent could be kept at almost 80% after  $MnO_x$  loading compared with that of the bare photoanode, because the color of the photoanode became brown and the photoabsorption might be inhibited by  $MnO_x$  loading (Figure S1C). Another possibility of decreased photocurrent could be considered to be producing some doped layers to accelerate charge recombination at the interface of  $MnO_x/BiVO_4$  during the calcination process. We also examined the photoelectrochemical CPR in artificial seawater rather than in pure  $NaCl$  solution (Figure S2). The behavior of  $HClO$  selectivity in artificial seawater was very similar to that in pure  $NaCl$  solution (Figure 2A), and only the  $MnO_x$ -loaded photoanode suppressed the CPR efficiently. The results suggest no significant effect of various anions and cations contained in the artificial seawater, such as  $SO_4^{2-}$  and  $Mg^{2+}$ , on the selectivity due to the low concentrations of these ions compared with  $Na^+$  and  $Cl^-$  (Desilvestro and Grätzel, 1987; Luo et al., 2011; Barczuk et al., 2013; Fukuzumi et al., 2017; Iguchi et al., 2018). It was also confirmed that  $H_2$  was produced on a Pt cathode in artificial seawater with a high  $FE(H_2)$  (ca. 100%).

### Characterizations of $MO_x/BiVO_4/WO_3/FTO$

The amounts of  $MO_x$  loading on the  $BiVO_4/WO_3/FTO$  photoanodes calculated from X-ray fluorescence (XRF) measurements are summarized in Table S2. The amount of  $MnO_x$  was  $0.02 \mu mol/cm^2$ , and those of other  $MO_x$  were in a similar range between 0.01 and  $0.024 \mu mol/cm^2$ . Surface scanning electron microscopic (SEM) observations of bare  $BiVO_4/WO_3/FTO$  (Figure 3A-(i)) confirmed a nanostructure with particle networks that consist of primary particles with diameters of ca. 100 nm. In contrast, the edge of the particles on the photoelectrode was not clear for  $MnO_x(0.1 M)/BiVO_4/WO_3/FTO$  (Figure 3A-(ii)), which suggests the loaded  $MnO_x$  covered the entire



**Figure 2. Photoelectrochemical Properties of MO<sub>x</sub>-Loaded Photoanodes**

(A) FEs for O<sub>2</sub> and HClO generation on photoanodes (MO<sub>x</sub>/BiVO<sub>4</sub>/WO<sub>3</sub>/FTO) modified with and without various metal oxides. The concentrations of loaded metal precursor solution were 0.1 M for Mn, Co, Ni, and Fe and 0.03 M for Rh and Pt. The calcination temperature for loading was 400°C, at an electric charge of 2 C (1,000 s and a steady photocurrent of 2 mA) in a 0.5 M NaCl aqueous electrolyte (35 mL) under simulated solar light (AM-1.5, 1 SUN).

(B) FE (HClO) and apparent MnO<sub>x</sub>-coverage calculated from XPS results for bare BiVO<sub>4</sub>/WO<sub>3</sub>/FTO and MnO<sub>x</sub>/BiVO<sub>4</sub>/WO<sub>3</sub>/FTO photoanodes, which were prepared by coating the manganese precursor solution with different concentrations (0.001–0.1 M) to change the MnO<sub>x</sub> loading amount.

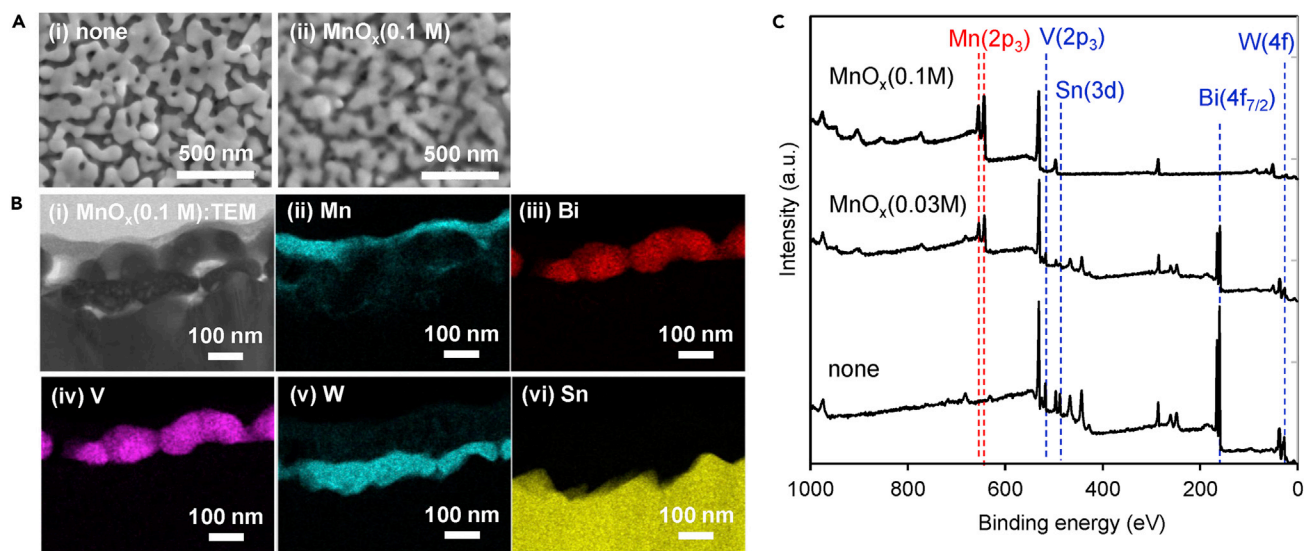
(C) FE (HClO) on MnO<sub>x</sub> (0.1 M)/BiVO<sub>4</sub>/WO<sub>3</sub>/FTO in aqueous NaCl solution with various concentrations (0.05–2 M).

(D) FE (HClO) on MnO<sub>x</sub> (0.1 M)/BiVO<sub>4</sub>/WO<sub>3</sub>/FTO anode in 0.5 M aqueous NaCl solution with various pH (pH 3–9).

surface of the photoanode. Transmission electron microscopic-energy dispersive X-ray spectroscopic (TEM-EDX) cross-sectional images of the photoanode loaded with MnO<sub>x</sub> (0.1 M, Figure 3B) showed that a thin layer (ca. 10–30 nm thick) of MnO<sub>x</sub> was present over the surface of the BiVO<sub>4</sub>/WO<sub>3</sub>/FTO photoanode. No electron diffraction pattern was obtained at the MnO<sub>x</sub> part, which indicates that MnO<sub>x</sub> was not crystalline. The apparent surface coverage of MO<sub>x</sub> layers calculated from the peak area of X-ray photoelectron spectroscopy (XPS; Figure 3C) measurements are summarized in Table S3. In the case of the MnO<sub>x</sub> (0.1 M)-coated sample, the peaks attributed to Bi, V, W, and Sn of the photoanode were not observed, whereas the peak attributed to Mn 2p<sub>3</sub> was clear, which suggested the surface coverage of MnO<sub>x</sub> was almost 100%. In contrast, for the MnO<sub>x</sub> (0.03 M)-coated sample, the peaks attributed to Mn 2p<sub>3</sub> decreased and peaks attributed to V 2p<sub>3</sub>, Bi 4f<sub>7/2</sub>, W 4f, and Sn 3d were observed, which indicates that MnO<sub>x</sub> (0.03 M) was not completely covering the photoanode surface, unlike that prepared with 0.1 M precursor solution. The dependence of the apparent surface coverage of MnO<sub>x</sub> on the concentration of manganese precursor solution is shown by the right-hand axis in Figure 2B. The coverage of MnO<sub>x</sub> decreased on decreasing the concentration of the manganese precursor solution. Although the apparent surface coverage of MnO<sub>x</sub> (0.01 M)-loaded BiVO<sub>4</sub>/WO<sub>3</sub>/FTO photoanode was only 30%, the selectivity toward the CPR was very low. Therefore, it is concluded that entire coverage of MnO<sub>x</sub> on the BiVO<sub>4</sub>/WO<sub>3</sub>/FTO surface was not necessary to suppress the CPR. The results indicate that the selectivity toward HClO/O<sub>2</sub> production could be controlled by this simple coating method using metal precursor solutions, and the CPR could be suppressed in aqueous solution containing Cl<sup>-</sup> ions with a photoanode surface partially loaded with MnO<sub>x</sub>.

### Properties of MO<sub>x</sub>/FTO under Dark Conditions

The electrochemical properties of the simple structured-MO<sub>x</sub>/FTO anodes without semiconductor layers were also evaluated under dark conditions (Figure S3). We checked the product amount of HClO/O<sub>2</sub>



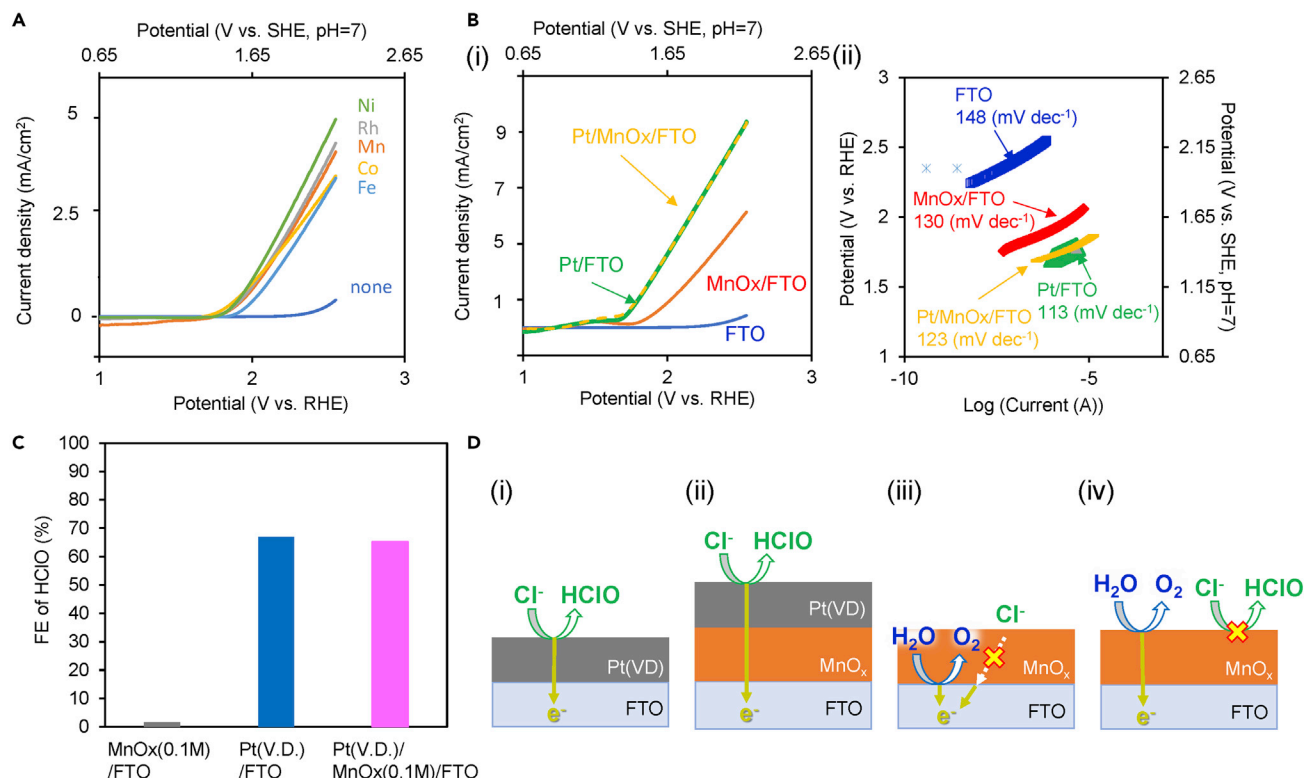
**Figure 3. Characterization of  $\text{BiVO}_4/\text{WO}_3/\text{FTO}$  Photoanodes with and without Loading  $\text{MnO}_x$**   
(A–C) (A) Surface SEM images, (B) cross-sectional TEM-EDX images, and (C) XPS spectra of  $\text{BiVO}_4/\text{WO}_3/\text{FTO}$  photoanodes with and without  $\text{MnO}_x$ . (A (ii) and B) The concentration of the  $\text{MnO}_x$  precursor solution was 0.1 M. (B) (i) TEM image and (ii–vi) EDX mapping images for each element.

and calculated the values of  $\text{FE}(\text{HClO})$ ,  $\text{FE}(\text{O}_2)$  on bare FTO, and  $\text{MO}_x/\text{FTO}$ , confirming that the sum of the  $\text{FE}(\text{HClO})$  and  $\text{FE}(\text{O}_2)$  became almost 100% within variation of measurement errors in each electrode.  $\text{FE}(\text{HClO})$  for various  $\text{MO}_x/\text{FTO}$  anodes (Figure S3A) had a similar tendency to that for the  $\text{MO}_x/\text{BiVO}_4/\text{WO}_3/\text{FTO}$  photoanodes (Figure 2A). It was also confirmed that  $\text{MnO}_x$  loading of the anodes effectively suppressed the CPR in aqueous NaCl solution under a wide range of conditions, regardless of the Mn precursor solution concentration (0.01–0.1 M), the NaCl concentration (0.005–2 M), pH (3–9), applied bias (1.5–1.8 V versus SHE, pH = 7), the valence or structure of  $\text{MnO}_x$  (amorphous,  $\text{Mn}_2\text{O}_3$  and  $\text{Mn}_3\text{O}_4$ ), preparation methods of  $\text{MnO}_x$  such as calcination temperature (300–550°C), and the kinds of manganese salt dissolving the precursor solution, as shown in Figures S3B–S3I. SEM images,  $\text{MnO}_x$  coverages, and  $\text{FE}(\text{HClO})$  of  $\text{MnO}_x/\text{FTO}$  anodes are shown in Figure S4. In the case of the  $\text{MnO}_x$  (0.03 M)/FTO with very low  $\text{FE}(\text{HClO})$ , SEM observations indicated that  $\text{MnO}_x$  did not entirely coat the surface of FTO, and the apparent coverage of  $\text{MnO}_x$  (0.03 M) calculated from the XPS spectrum was only 65%. It is suggested that complete coating of  $\text{MnO}_x$  on FTO anodes was not needed to suppress the CPR, as well as photoanodes.

### Mechanism of Selective $\text{O}_2$ Production on $\text{MnO}_x$ -Loaded Photoanode

There are two possibilities why the  $\text{MnO}_x$  loaded on the photoanodes or anodes could suppress the CPR; direct  $\text{O}_2$  production on  $\text{MnO}_x$  and indirect  $\text{O}_2$  production through the decomposition of HClO as an intermediate. The HClO initially added to the NaCl aqueous solution was not decomposed on a  $\text{MnO}_x/\text{FTO}$  anode under dark conditions (Figure S5). This suggests that indirect  $\text{O}_2$  production on  $\text{MnO}_x/\text{FTO}$  by HClO decomposition on the  $\text{MnO}_x$  surface can be denied and that  $\text{O}_2$  was directly produced on  $\text{MnO}_x/\text{FTO}$  in NaCl aqueous solution.

In the case of noble metal anodes such as  $\text{IrO}_2$ , selective OER from an aqueous solution containing  $\text{Cl}^-$  ions can be realized by coating an  $\text{MnO}_x$  layer on the entire surface of the anode (Bennet, 1980; El-Moneim et al., 2009; Vos et al., 2018; Ibrahim and Canan, 2015; Gidon et al., 2018). In the field of water electrolysis, this selective OER has been explained by a “ $\text{Cl}^-$ -impermeable mechanism,” where  $\text{Cl}^-$  ions cannot reach the surface of the noble metal through the  $\text{MnO}_x$  layer, rather than by a “catalytic mechanism” where  $\text{MnO}_x$  itself functions as an electrocatalyst for  $\text{O}_2$  production (Vos et al., 2018). In this  $\text{Cl}^-$ -impermeable mechanism, the  $\text{MnO}_x$  layer must completely cover the entire surface of the noble metal, and no oxidation reaction should occur on the  $\text{MnO}_x$  but rather on the noble metal catalyst, which indicates that the reaction sites are completely different with each mechanism. However, in this study, much data that cannot be explained by the  $\text{Cl}^-$ -impermeable mechanism was obtained. First, current-voltage (*I*-*V*) curves for the  $\text{MnO}_x/\text{FTO}$  anode showed that the onset potential was significantly shifted to lower potential compared with that for bare FTO (Figures 4A and 4B). Second, complete coating of  $\text{MnO}_x$  on FTO anode was not necessary

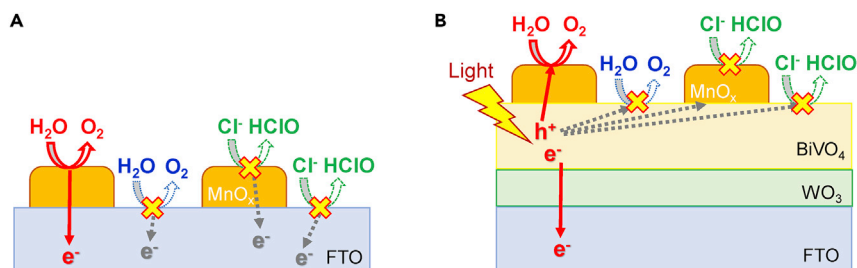


**Figure 4. Evaluation of Electrochemical Properties and Schematic Diagrams on O<sub>2</sub>/HClO Production on MO<sub>x</sub>/FTO Anodes**

(A) *I*-*V* characteristics for bare FTO and various MO<sub>x</sub> (0.1 M)/FTO anodes measured in 0.5 M NaCl aqueous solution (sweeping in the cathodic direction). (B) (i) *I*-*V* characteristics and (ii) Tafel plots for various anodes (FTO, MnO<sub>x</sub> (0.1 M)/FTO, Pt(VD)/FTO, and Pt(VD)/MnO<sub>x</sub> (0.1 M)/FTO) measured in 0.5 M NaCl aqueous solution. The Pt (VD) layer was prepared using the vapor deposition method. (C) FE (HClO) for various anodes at an electric charge of 2 C (1,000 s) at a steady current of 2 mA in a 0.5 M aqueous NaCl solution. (D) Schematic diagrams of (i) Pt (VD)/FTO and (ii) Pt (VD)/MnO<sub>x</sub> (0.1 M)/FTO anodes. (iii) Cl<sup>-</sup>-impermeable mechanism and (iv) catalytic mechanism for MnO<sub>x</sub> (0.1 M)/FTO anodes.

to suppress the CPR (Figures S3B and S4). Third, it was confirmed whether or not the oxidation reaction occurred on MnO<sub>x</sub> (Figures 4C and 4D). A thick MnO<sub>x</sub> (0.1 M) layer that covered the entire FTO surface was prepared, and then it was coated with Pt by vapor deposition method (Pt (VD)/MnO<sub>x</sub>/FTO). The *I*-*V* properties and Tafel slope were improved by Pt (VD) loading (Figure 4B-(ii)). The FE (HClO) on the Pt (VD)/MnO<sub>x</sub>/FTO anode (65.2%) was almost same as that on the Pt (VD)/FTO anode (66.9%) and was completely different from that on MnO<sub>x</sub>/FTO (<1.6%), as shown in Figure 4C, which indicates that the selectivity and *I*-*V* properties could be controlled by modification of the top surface. These results suggest that the oxidation reaction occurred on the top surface of MnO<sub>x</sub> on the MnO<sub>x</sub> (0.1 M)/FTO anode, and not on the surface of FTO (Figure 4D). Furthermore, the Cl<sup>-</sup> adsorption characteristics of MO<sub>x</sub> were compared using XPS, and Cl<sup>-</sup> ions were found not to be adsorbed by CoO<sub>x</sub>, FeO<sub>x</sub>, NiO<sub>x</sub>, or MnO<sub>x</sub> (Table S4, Cl coverage <1%). Therefore, it was difficult to explain MnO<sub>x</sub> peculiarity by the difference of the adsorption characteristics of Cl<sup>-</sup>. From all these results, we can conclude that the mechanism for the selectivity toward the OER/CPR on MnO<sub>x</sub>/FTO from an aqueous solution containing Cl<sup>-</sup> ions can be explained not by the Cl<sup>-</sup>-impermeable mechanism but rather by the catalytic mechanism (Figure 4D-(iii and iv)).

The special OER selectivity on the MnO<sub>x</sub> catalyst-loaded anodes might be explained by the difference or the ratio of the overpotential with the OER and CPR reactions in each electrolyte solution. The potentials required for steady current electrolysis on various MO<sub>x</sub>/FTO were listed in Table S5. The behaviors of potential on each anode were similar in NaCl and NaH<sub>2</sub>PO<sub>4</sub> aqueous solutions except for unstable anodes; the precious metals showed the lowest potential level, and CoO<sub>x</sub>, FeO<sub>x</sub>, NiO<sub>x</sub>, and MnO<sub>x</sub> showed the second lowest level. On the other hand, the evaluation of each specific overpotential in NaCl aqueous solution is difficult because both the OER and CPR occur. It should be emphasized again that the FE (HClO) was very low even when MnO<sub>x</sub> was not fully coated on FTO; therefore, it is surmised that the overpotential for the



**Figure 5. Schematic Diagrams on O<sub>2</sub>/HClO Production over Partially Loaded MnO<sub>x</sub> Catalyst**

(A and B) The OER and CPR on (A) FTO anode and (B) BiVO<sub>4</sub>/WO<sub>3</sub>/FTO photoanode partially loaded with MnO<sub>x</sub> catalyst. The selectivity is controlled by the relative relationship of the overpotentials for each reaction. The overpotential for the OER on MnO<sub>x</sub> might be much lower than those of other reactions such as the CPR on MnO<sub>x</sub>, and the OER and CPR on BiVO<sub>4</sub>.

OER on MnO<sub>x</sub> was much lower than those of the other reactions such as the CPR on MnO<sub>x</sub>, and the OER and CPR on FTO relatively in NaCl solution (Figure 5A). As for the photoanode reactions using MO<sub>x</sub>/BiVO<sub>4</sub>/WO<sub>3</sub>/FTO, the specificity of MnO<sub>x</sub> could not be explained by the decomposition of HClO produced into O<sub>2</sub> by UV light excitation from solar light as reported (Fukuzumi et al., 2017), because the results in Figure 2A were compared under the same irradiation conditions. It was confirmed that the HClO selectivity was very low, even when the apparent coverage of MnO<sub>x</sub> was only 30%, as shown in Figure 2B. Considering the analogy with the results for the MnO<sub>x</sub>/FTO anode, the Cl<sup>-</sup>-impermeable mechanism for MnO<sub>x</sub> loaded on a photoanode can also be excluded. The turnover number (ca. 154) of e<sup>-</sup> to Mn on the MnO<sub>x</sub>-loaded photoanode was much more than 1. Therefore, it is reasonable to explain the results by the catalytic mechanism, where photoexcited h<sup>+</sup> on BiVO<sub>4</sub> immediately moves to MnO<sub>x</sub> and the preferential oxidation of water on the MnO<sub>x</sub> surface into O<sub>2</sub> occurs without the CPR (Figure 5B). It should be noted that various MnO<sub>x</sub> catalysts such as amorphous Mn<sub>2</sub>O<sub>3</sub>, Mn<sub>3</sub>O<sub>4</sub>, and Ca-MnO<sub>x</sub> could suppress the CPR (Figure S3G), which indicates that manganese oxides themselves may have specificity with a large overpotential ratio for the CPR to the OER in NaCl solution. This catalytic mechanism of MnO<sub>x</sub> is generally that for the OER on Mn<sub>4</sub>O<sub>5</sub> core cluster with Ca in the photosystem II (PSII) of natural photosynthesis (Suga et al., 2017; Zhang et al., 2018; Zaharueva et al., 2011; Najafpour et al., 2010); therefore, it can also be a common mechanism in the fields of electrolysis and artificial photosynthesis using photoanodes. Currently, the intrinsic reason for the specific dependence of the overpotentials on these elements including manganese is not clear, and the comparison of energy barriers of transition state between CPR and OER on a certain model structure of each MO<sub>x</sub> through computational chemistry is under investigation.

### Evolutional Hypothesis for the Mn<sub>4</sub>O<sub>5</sub> Core of Natural Photosynthesis

Natural OER metal centers of cyanobacteria, algae, or plants containing elements other than Mn have not been found to date. Mn has many advantages such as a low overpotential for OER and earth-abundant transition metal element with various valence states (Zhang et al., 2018; Armstrong, 2008; Sauer and Yachandra, 2002; Raveau and Seikh, 2012; Bryan et al., 2016). On the other hand, some metal oxides such as Fe, Ni, and Co also basically satisfy all these requirements (Zaharueva et al., 2011; Raveau and Shiek, 2012; Bryan et al., 2016). Therefore, there is no hypothesis to explain why Fe, Ni, or Co is not used as the OER center in PSII so far. Based on our specific results that MnO<sub>x</sub> catalyzes the OER selectively from NaCl aqueous solution under a wide range of conditions, even at low pH and low Cl<sup>-</sup> concentration compared with those for natural photosynthesis *in vivo* (ca. 100 mM of Cl<sup>-</sup> in chloroplasts) (Robinson and Downton, 1984; Baranov and Haddy, 2017; Jagendorf and Uribe, 1966; Beebo et al., 2013), it is possible to advocate a new hypothesis as to why MnO<sub>x</sub> is selected as the OER center of PSII that appeared on the ancient earth. It is because HClO is significantly toxic to organisms, and Mn is the only element that can produce only O<sub>2</sub> without the generation of HClO in aqueous solution containing Cl<sup>-</sup> ions under various conditions *in vivo*. Considering that HClO has extremely strong bactericidal properties compared with H<sub>2</sub>O<sub>2</sub> (McKenna and Davies, 1988), and that it should be necessary to avoid the generation of even a small amount of HClO *in vivo*, the specialty of natural Mn<sub>4</sub>O<sub>5</sub> can be comprehensively explained by the results of this study.

### Limitation of the Study

We investigated the O<sub>2</sub>/HClO production in aqueous solution containing Cl<sup>-</sup> on BiVO<sub>4</sub>/WO<sub>3</sub>/FTO photoanodes and FTO anodes modified with various MO<sub>x</sub>. It is emphasized that the modification of partially

loaded  $\text{MnO}_x$  resulted in specifically catalyzing the OER without HClO production over a wide range of conditions. These results will not only provide some insight into the practical application of artificial photosynthesis technologies using salted water and solar energy but also facilitate the elucidation of the function of  $\text{Mn}_4\text{O}_5$  core cluster with Ca in natural photosynthesis. Considering our results, one hypothesis about the evolutionary process of  $\text{Mn}_4\text{O}_5$  core cluster in natural PSII can be proposed; HClO is toxic to bacteria, so that manganese element might be selected by nature due to the unique catalysis on  $\text{MnO}_x$ , where HClO production is fully suppressed. Complete elucidation of evolutionary hypothesis is difficult generally; however, our hypothesis will be elucidated by various ways. For example, we have some plans about the investigation on the effect of coordination of organic compounds with carboxyl and amino groups, mimicking the atmosphere in the protein of PSII, on various nano-size  $\text{MO}_x$  and multinuclear metal complexes as electrocatalysts systematically, as well as investigation through computational chemistry in the future.

### Resource Availability

#### Lead Contact

Further information and requests for resources should be directed to the Lead Contact, Kazuhiro Sayama ([k.sayama@aist.go.jp](mailto:k.sayama@aist.go.jp)).

#### Materials Availability

This study did not generate new unique reagents.

#### Data and Code Availability

This study did not generate/analyze datasets/code.

## METHODS

All methods can be found in the accompanying [Transparent Methods supplemental file](#).

## SUPPLEMENTAL INFORMATION

Supplemental Information can be found online at <https://doi.org/10.1016/j.isci.2020.101540>.

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## AUTHOR CONTRIBUTIONS

S.O. and K.S. designed the experiments. S.O. performed all sample preparation, characterization, and (photo)electrochemical property experiments. All authors discussed the results and commented on the manuscript.

## DECLARATION OF INTERESTS

The authors declare no competing interests.

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**Supplemental Information**

**Functions of  $\text{MnO}_x$  in NaCl**

**Aqueous Solution**

**for Artificial Photosynthesis**

**Sayuri Okunaka, Yugo Miseki, and Kazuhiro Sayama**

## Supplemental Information

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**References**

## Transparent Methods

### Materials

Metal organic solutions of Mn, Co, Fe, Ni were purchased from Symetrix Co., USA (purchased from Koujundo Chemical. Co., Japan).  $\text{H}_2\text{PtCl}_6 \cdot 6\text{H}_2\text{O}$  and  $\text{Rh}(\text{NO}_3)_3$ ,  $\text{IrCl}_3$ ,  $\text{AgNO}_3$ ,  $\text{NaCl}$ ,  $\text{NaH}_2\text{PO}_4$  were purchased from Wako Pure Chemical, Japan.  $\text{Pd}(\text{NO}_3)_2$ ,  $\text{RuCl}$  were purchased from Nakalai Tesque. All reagents were used as received, and all the experiments were carried out under ambient condition without eliminating the moisture from the atmosphere.

### Preparation of $\text{BiVO}_4/\text{WO}_3/\text{FTO}$ photoanode

$\text{BiVO}_4/\text{WO}_3/\text{FTO}$  photoanodes were prepared as follows. Precursor solutions of each oxide semiconductor were coated on F-doped  $\text{SnO}_2$  conductive glass substrate (FTO;  $10 \Omega \text{ sq}^{-1}$ , Nippon Sheet Glass Co.) by spin-coating and then calcination for each coating. A  $\text{WO}_3$  underlayer was coated on the FTO substrate by spin-coating (1500 rpm, 15 s) aqueous peroxy-tungstic acid solution (1.4 M) containing W ions, followed by calcination at  $500^\circ\text{C}$  for 30 min in air. The  $\text{BiVO}_4$  layer on  $\text{WO}_3/\text{FTO}$  was also fabricated by spin-coating (1000 rpm, 15 s) using a Bi and V precursor solution, followed by calcination at  $550^\circ\text{C}$  for 30 min in air. The  $\text{BiVO}_4$  precursor solutions was a mixed solution of 0.2 M  $\text{Bi}^{3+}$  and 0.2 M  $\text{V}^{5+}$  in a 1:1 volume ratio diluted with butyl acetate.

### Preparation of $\text{MO}_x/\text{BiVO}_4/\text{WO}_3/\text{FTO}$ photoanodes and $\text{MO}_x/\text{FTO}$ anodes

The  $\text{MO}_x$  (where M = Mn, Co, Fe, Ni, Pt, Rh) layers on the  $\text{BiVO}_4/\text{WO}_3/\text{FTO}$  photoanodes (denoted as  $\text{MO}_x/\text{BiVO}_4/\text{WO}_3/\text{FTO}$ ) or FTO anodes (denoted as  $\text{MO}_x/\text{FTO}$ ) were prepared by spin-coating (1500 rpm, 15 s) metal organic solutions in butyl acetate on the  $\text{BiVO}_4/\text{WO}_3/\text{FTO}$  and calcination at  $400^\circ\text{C}$  in air for 1 h. In the case of loading the non-noble metals, metal organic solutions (Symetrix Co., USA, purchased from Koujundo Chemical. Co., Japan) in butyl acetate (0.1 M) were used. In the cases of loading with noble metals, aqueous solutions of  $\text{H}_2\text{PtCl}_6 \cdot 6\text{H}_2\text{O}$  (Wako),  $\text{Rh}(\text{NO}_3)_3$  (Wako) were prepared. It is difficult to prepare high concentration solutions of these noble metal precursor salts; therefore, the concentration of these solutions was adjusted to 0.03 M.

The expression  $\text{MO}_x$  was used, regardless the valence of the metal. To evaluate the reaction sites, Pt (VD) was coated onto FTO or  $\text{MnO}_x$  (0.1 M)/FTO by vapor deposition method under vacuum (JFC-1600, JEOL, emission current: 40 mA, emission time: 7 min, sample distance: 30 mm).

For the electrodes used in the electrolysis system under dark conditions, FTO anode electrodes modified with various metal oxides ( $\text{MO}_x/\text{FTO}$ , where M = Mn, Co, Fe, Ni, Cu, Ag, Pt, Pd, Rh, Ru) were prepared. In the case of loading the non-noble metals, metal organic solutions in butyl acetate (0.03 or 0.1 M) were used. In the cases of loading with noble metals, aqueous solutions of  $\text{H}_2\text{PtCl}_6 \cdot 6\text{H}_2\text{O}$ ,  $\text{Rh}(\text{NO}_3)_3$ ,  $\text{Pd}(\text{NO}_3)_2$ ,  $\text{RuCl}$ ,  $\text{AgNO}_3$  and  $\text{IrCl}_3$  were prepared. It is difficult to prepare high concentration solutions of these noble metal precursor salts; therefore, the concentration of these solutions was adjusted to 0.03 M. The  $\text{MO}_x$  layers on the FTO electrodes (denoted as  $\text{MO}_x/\text{FTO}$ ) were prepared by spin-coating (1500 rpm, 15 s) metal organic solutions in butyl acetate on the FTO and calcination at  $400^\circ\text{C}$  in air for 1 h.

To examine the effect of manganese species on FE ( $\text{HClO}$ ),  $\text{Mn}_2\text{O}_3/\text{FTO}$ ,  $\text{Mn}_3\text{O}_4/\text{FTO}$ ,

and Ca-MnO<sub>x</sub>/FTO anodes were prepared as follows. A Mn<sub>2</sub>O<sub>3</sub>/FTO anode was prepared by electrochemical deposition (ED-S) in a solution of 0.25 M MnSO<sub>4</sub> and 0.25 M Na<sub>2</sub>SO<sub>4</sub> (1:1 v/v) for 10 min. The films were rinsed with water and dried, followed by calcination at 400 °C for 1 h in air (Ramírez. et al. 2014). The Mn<sub>3</sub>O<sub>4</sub>/FTO anode was prepared by electrochemical deposition (ED-N) in a solution of 0.25 M Mn(NO<sub>3</sub>)<sub>2</sub> and 0.25 M Na<sub>2</sub>SO<sub>4</sub> (1:1 v/v) for 10 min at 70 °C. (Qi. et al. 2016) The films were rinsed with water and dried at 80 °C for 1 h in air. A Ca-MnO<sub>x</sub>(Mn/Ca=4) anode was prepared by spin-coating (1500 rpm, 15 s) metal organic solutions (0.1 M, Ca:Mn = 1:4 molar ratio, Symetrix Co., USA, purchased from Koujundo Chemical. Co., Japan) in butyl acetate on the FTO and calcination at 400 °C in air for 1 h.

### Characterization

The anode samples obtained were characterized using X-ray diffraction (XRD; PANalytical, EMPYREAN, rotating anode diffractometer, 40 kV, 10 mA) with Cu *K*α radiation ( $\lambda_{K\alpha} = 1.5406\text{\AA}$ ), X-ray fluorescence (XRF; Rigaku, Supermini200), X-ray photoelectron spectroscopy (XPS; Ulvac Co., XPS-1800), scanning electron microscopy (SEM; HITACHI, S-4100), and transmission electron microscopy (TEM; Hitachi High-Technologies Co., Ltd., HD2700) with energy dispersive X-ray spectroscopy (EDX) mapping. The MnO<sub>x</sub> coverage was calculated using the spectrum area obtained from XPS spectrum and intensity factor of Mn to the sum of those of Mn, Bi, V, W and Sn.

### Photoelectrochemical and electrochemical production of HClO and O<sub>2</sub>

#### Photoelectrochemical properties

The photoelectrochemical performance of the photoanodes was measured using an electrochemical analyzer (BAS. Inc., ALS 760E) and a solar simulator (SAN-EI ELECTRIC Co., XES-151S) calibrated to AM-1.5 (1 SUN, 100 mW cm<sup>-2</sup>) with a spectroradiometer (SOMA Optics, Ltd., Model S-2440). The irradiation area (0.28 cm<sup>2</sup>) was defined using a black mask. The simulated solar light was irradiated from the semiconductor side. The current–voltage (*I*–*V*) characteristics were measured using a two-compartment cell (Pyrex-made) with an ion-exchange membrane (SELEMION, AGC Engineering), and a photoanode equipped with a back-reflection plate as the working electrode, an Ag/AgCl electrode as the reference electrode, and a Pt wire as the counter electrode. The scan rate was 50 mV s<sup>-1</sup>. The measured potentials vs. Ag/AgCl were converted to the standard hydrogen electrode (SHE) and the reversible hydrogen electrode (RHE) scale according to:

$$E_{SHE} = E_{Ag/AgCl} + 0.206 \quad (S1)$$

$$E_{RHE} = E_{Ag/AgCl} + 0.059pH + E^{\circ}_{Ag/AgCl} \quad (S2)$$

where  $E_{SHE}$  and  $E_{RHE}$  are the converted potential vs. SHE or RHE,  $E^{\circ}_{Ag/AgCl} = 0.1976$  at 25 °C, and  $E_{Ag/AgCl}$  is the experimentally measured potential against the Ag/AgCl reference. An aqueous solution of 0.5 M NaCl (35 mL, pH = 5.9) was used as the electrolyte.

### Electrochemical properties

The current–voltage ( $I$ – $V$ ) characteristics on the FTO and  $MO_x$ /FTO anodes were measured using a two-compartment cell (Pyrex-made) with an ion-exchange membrane (SELEMION, AGC Engineering), and an anode as the working electrode, an Ag/AgCl electrode as the reference electrode, and a Pt wire as the counter electrode. The scan rate was  $50 \text{ mV s}^{-1}$ . The measured potentials vs. Ag/AgCl were converted to the SHE and the RHE. An aqueous solution of 0.5 M NaCl (35 mL, pH = 5.9) was used as the electrolyte.

### Simultaneous production of HClO and O<sub>2</sub>

The simultaneous production of HClO and O<sub>2</sub> on the photoanodes was measured using an electrochemical analyzer (BAS. Inc., ALS 760E) and a solar simulator (SAN-EI ELECTRIC Co., XES-151S) calibrated to AM-1.5 (1 SUN,  $100 \text{ mW cm}^{-2}$ ) with a spectroradiometer (SOMA Optics, Ltd., Model S-2440). The simulated solar light was irradiated from the semiconductor side. The reaction on the obtained photoanodes was performed under solar light irradiation using a two-compartment cell, equipped with an ion-exchange membrane (SELEMION, AGC Engineering) between the anode and cathode. Pt wire was used as a counter electrode to effectively reduce water to H<sub>2</sub>. An aqueous solution (anode: 35 mL; cathode: 35 mL) of NaCl (0.5 M) was used as the electrolyte. In the photoelectrochemical reaction, photoanodes (1.5×5 cm) were used. Each solution was stirred by magnetic stirring at ca. 400 rpm. In the case of the FTO and  $MO_x$ /FTO anodes, the production of HClO in the dark was conducted by the same method.

The concentration of HClO produced was measured with a UV-vis spectrometer (JASCO, Y-730) using the *N,N*-diethyl-*p*-phenylenediamine (DPD) method. The faradaic efficiencies (FEs) of HClO (FE (HClO)) can be calculated as:

$$FE(HClO) = \frac{(\text{amount of generated HClO})}{(\text{theoretical amount of HClO})} \times 100 = \frac{(\text{amount of generated HClO})}{(\text{amount of generated electrons}/2)} \times 100 \quad (S3)$$

The amount of O<sub>2</sub> evolved in both the liquid and gas phases were determined using an O<sub>2</sub> sensor (Optical Oxygen Meter, Pyro Science and FireStingO<sub>2</sub>) and combining each value. These HClO/O<sub>2</sub> production reactions of the main part were measured 3 times, and the reproducibility of the data was confirmed with the variation of experimental errors within 10%. The amount of hydrogen evolved from Pt electrode was determined with a gas chromatograph equipped with a TCD detector. The faradaic efficiency of H<sub>2</sub> (FE (H<sub>2</sub>)) can be calculated as:

$$FE(HClO) = \frac{(\text{amount of generated H}_2)}{(\text{theoretical amount of H}_2)} \times 100 = \frac{(\text{amount of generated H}_2)}{(\text{amount of generated electrons}/2)} \times 100 \quad (S4)$$

## Results

**Table S1.** Potential required for photo-electrolysis for steady current (2 mA) using various  $MO_x$ /BiVO<sub>4</sub>/WO<sub>3</sub>/FTO photoelectrodes. Related to Figure 2.

$MO_x$ /BiVO <sub>4</sub> /WO <sub>3</sub> /FTO	Potential (V vs. SHE, pH=7)
None	0.74
Mn	0.83
Co	0.68
Ni	0.70
Fe	0.78
Pt	0.65
Rh	0.80

Potential required for electrolysis with an electric charge of 2 C in 0.5 M aqueous NaCl solution using various  $MO_x$ /BiVO<sub>4</sub>/WO<sub>3</sub>/FTO electrodes (1.5 cm x 5 cm). The concentration of loaded metal precursor solution was 0.03 M.

**Table S2.** Amount of  $MO_x$  loading on the BiVO<sub>4</sub>/WO<sub>3</sub>/FTO photoanodes. Related to Figure 2.

$MO_x$	$MO_x$ loading ( $\mu\text{mol}/\text{cm}^2$ )
None	0
Mn	0.020
Co	0.014
Fe	0.017
Ni	0.024
Rh	0.016
Pt	0.010

Amount of  $MO_x$  loading on the BiVO<sub>4</sub>/WO<sub>3</sub>/FTO photoanodes was calculated using XRF spectra. The concentrations of loaded metal precursor solutions were (a) 0.1 M for Mn, Co, Ni, and Fe, and (b) 0.03 M for Rh and Pt.

**Table S3.** Apparent  $MO_x$ -coverage (%) for the BiVO<sub>4</sub>/WO<sub>3</sub>/FTO photoanodes. Related to Figure 2.

$MO_x$	Coverage (%)	
	(A) 0.03 M	(B) 0.1 M
Mn	54.0	100.0
Co	51.6	79.9
Ni	77.6	91.9
Fe	79.3	87.4
Rh	32.1	-
Pt	38.5	-

Apparent  $MO_x$ -coverage (%) calculated from XPS spectra for BiVO<sub>4</sub>/WO<sub>3</sub>/FTO photoanodes modified with various metal oxides ( $MO_x$ ). The concentrations of the coated metal precursor solutions were (A) 0.03 M for Mn, Co, Ni, Fe, Rh and Pt, and (B) 0.1 M for Mn, Co, Ni, and Fe. The MnO<sub>x</sub> coverage was calculated using the spectrum area and intensity factor of Mn to

the sum of those of Mn, Bi, V, W and Sn.

**Table S4.** Amounts of adsorbed Cl<sup>-</sup> ions on the  $MO_x/FTO$  after dipped in NaCl aq. Related to Figure 4.

$MO_x$	Amount of Cl (%) after immersion in NaCl aq.
None	0.2
Mn	0.2
Co	< 0.1
Ni	0.5
Fe	0.6
Pt	3.2
Rh	3.5

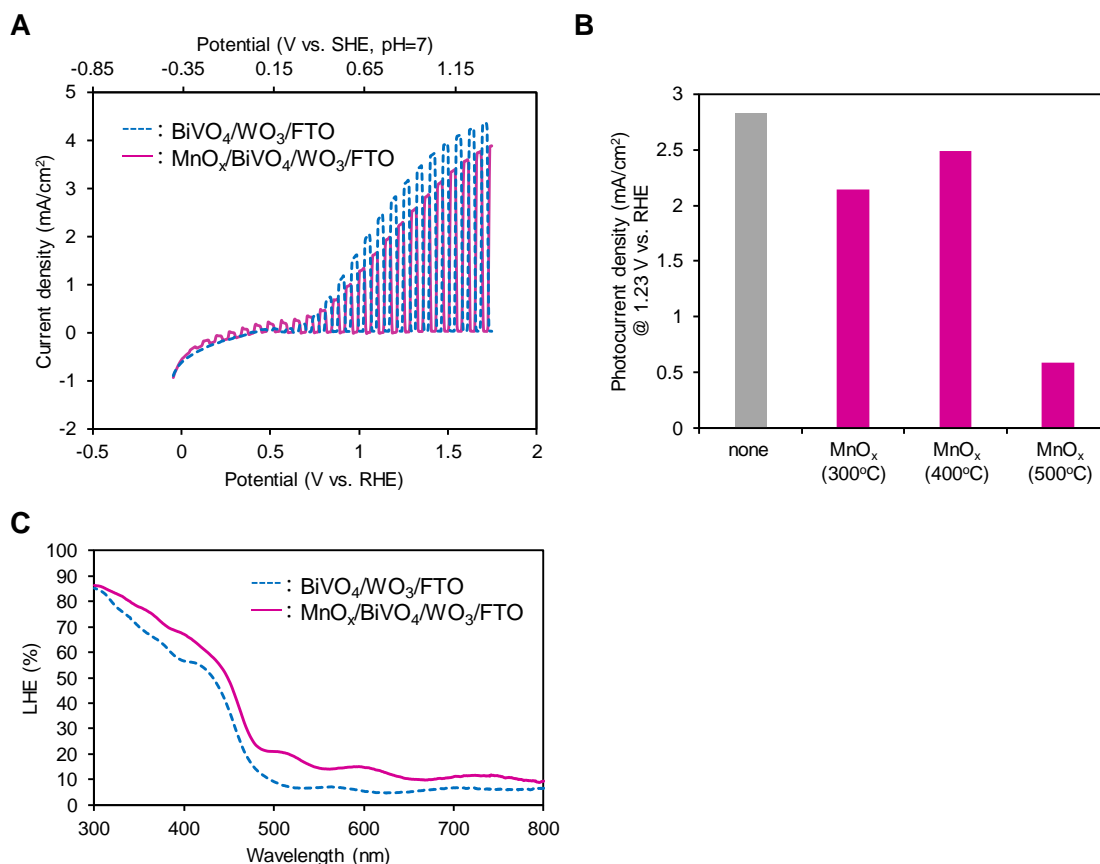
Amounts of adsorbed Cl<sup>-</sup> ions on the  $MO_x/FTO$  anode after immersion in 10 mL of 0.5 M aqueous NaCl solution for 3 h, determined from XPS measurements. Although the amount of Cl<sup>-</sup> adsorption on Pt and RhO<sub>x</sub> on the FTO was slightly larger than that of other typical metals, this is because the precursor solutions of Pt and Rh contain Cl<sup>-</sup> ions.

**Table S5.** Potential required for electrolysis for steady current (2 mA) using various  $MO_x/FTO$  electrodes. Related to Figure 4.

$MO_x/FTO$	(A) Potential (V vs. SHE) in NaCl aq.	(B) Potential (V vs. SHE) in NaH <sub>2</sub> PO <sub>4</sub> aq.
None	2.43	2.45
Mn	1.62	1.40
Co	1.50	1.38
Ni	1.61	1.50*
Fe	1.67	1.44
Cu	1.95*	2.23*
Cr	1.95*	2.19*
Ag	1.74	1.86
Pt	1.23	1.34
Pd	2.04*	1.50
Rh	1.38	1.37
Ru	1.35	1.36
Ir	1.30	1.36

Potential after the electrolysis with an electric charge of 2 C (1000 s, in a steady current of 2 mA) in (A) 0.5 M aqueous NaCl solution (pH 5.9) and (B) 0.5 M aqueous NaH<sub>2</sub>PO<sub>4</sub> solution (pH 4.3) using various  $MO_x/FTO$  electrodes (1.5 cm x 4 cm). The concentration of loaded metal precursor solution was 0.03 M. \*Elution was observed during the reaction.

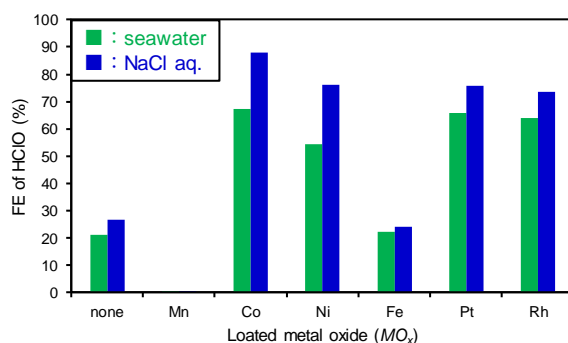




**Figure S1.** Photoelectrochemical performance and optical property of photoanode. Related to Figure 2.

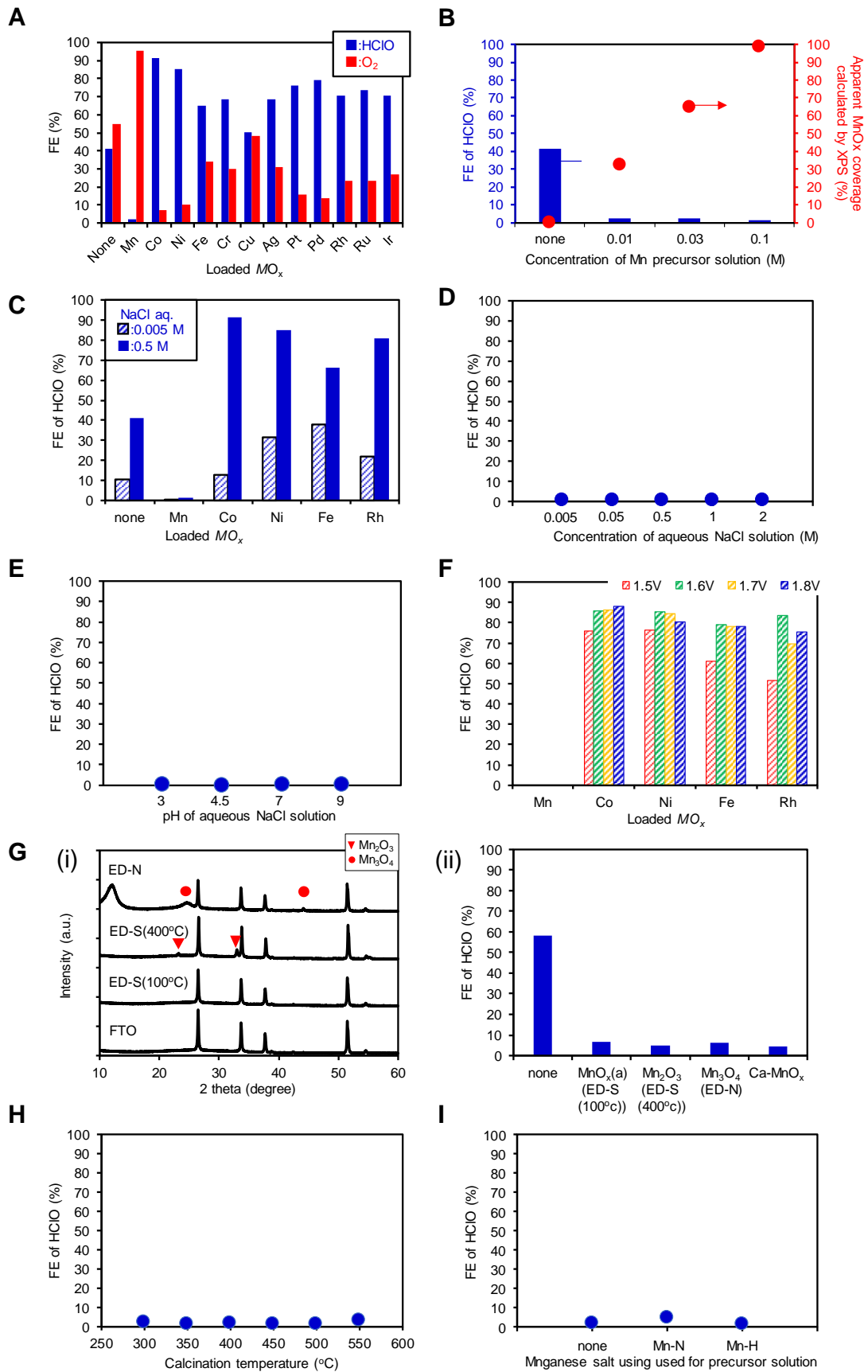
(A)  $I$ - $V$  characteristics for bare  $\text{BiVO}_4/\text{WO}_3/\text{FTO}$  and  $\text{MnO}_x(0.1\text{M})/\text{BiVO}_4/\text{WO}_3/\text{FTO}$  photoanodes measured in 0.5 M NaCl aqueous solution under simulated solar light (AM-1.5, 1 SUN, irradiation area:  $0.28 \text{ cm}^2$ , irradiated from the semiconductor side) with a light chopper.  $\text{MnO}_x$  was prepared using 0.1 M-Mn precursor solution and by calcination at  $400 \text{ }^\circ\text{C}$ . (B) Photocurrent at + 0.88 V vs. SHE at pH=7 of the bare  $\text{BiVO}_4/\text{WO}_3/\text{FTO}$  and  $\text{MnO}_x(0.1\text{M})/\text{BiVO}_4/\text{WO}_3/\text{FTO}$  photoanodes, which were calcined at different temperatures (300 – 500  $^\circ\text{C}$ ) after coating of the manganese precursor solution, measured in 0.5 M NaCl aqueous solution under simulated solar light. (C) Light harvesting efficiency (LHE) spectra for the bare  $\text{BiVO}_4/\text{WO}_3/\text{FTO}$  and  $\text{MnO}_x(0.1\text{M})/\text{BiVO}_4/\text{WO}_3/\text{FTO}$  photoanodes calcined at  $400 \text{ }^\circ\text{C}$  after coating with the manganese precursor solution. LHE was calculated from transmittance ( $T$ , %) and reflectance ( $R$ , %) using the following formula:

$$LHE(\%) = 100 - T - R \quad (\text{S5})$$



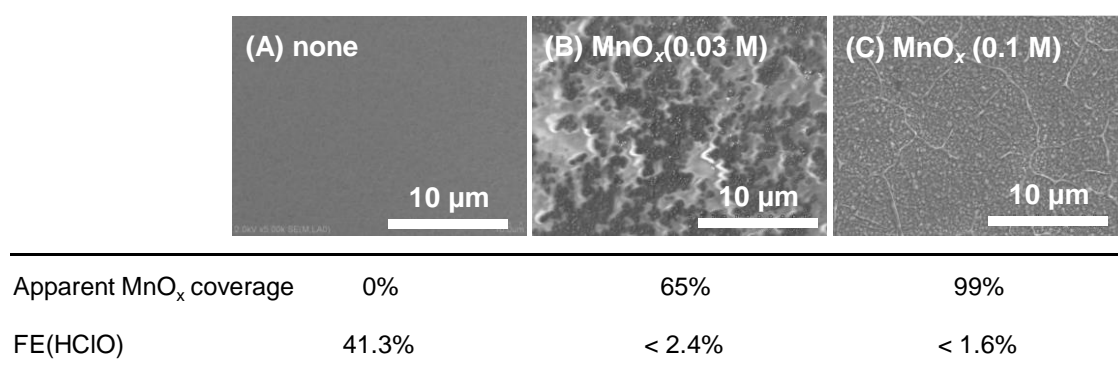
**Figure S2.** FE(HClO) on photoanodes in 0.5 M of NaCl aq. and artificial seawater. Related to Figure 2.

FEs for oxidative HClO generation on photoanodes ( $MO_x/BiVO_4/WO_3/FTO$ ) modified with and without various metal oxides at an electric charge of 2 C (1000 s at steady photocurrent of 2 mA) in 0.5 M of NaCl aq. and artificial seawater (35 mL) under simulated solar light (AM-1.5, 1 SUN). The concentrations of coated metal precursor solutions were 0.1 M for Mn, Co, Ni, and Fe, and 0.03 M for Rh and Pt. The artificial seawater (MARINE ART SF-1) was purchased from Osaka Yakken. Co. Ltd., Japan (Iguchi. et al. 2018).



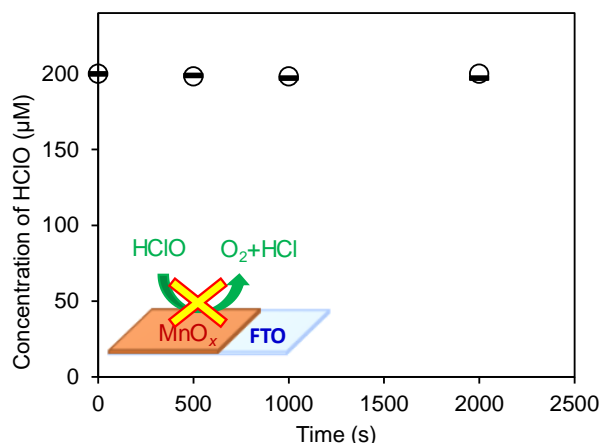
**Figure S3.** FEs for HClO generation on  $MO_x$ /FTO under dark conditions. Related to Figure 2.

The electric charge was 2 C (1000 s at a steady photocurrent of 2 mA) under various conditions. (A) FE (HClO) and  $FE(O_2)$  on  $MO_x$  (0.03 M)/FTO in 0.5 M aqueous NaCl solution. (B) FE (HClO) and apparent  $MnO_x$ -coverage calculated from XPS results for bare FTO and  $MnO_x$ /FTO photoanodes, which were prepared by coating the manganese precursor solution with different concentrations (0.01–0.1 M) to change the  $MnO_x$  loading amount. (C) FE (HClO) on bare FTO and  $MO_x$ /FTO in 0.005 M or 0.5 M aqueous NaCl solution. (D) FE (HClO) on  $MnO_x$  (0.1 M)/FTO in aqueous NaCl solution with various concentrations (0.005–2 M). (E) FE (HClO) on  $MnO_x$  (0.1 M)/FTO anode in 0.5 M aqueous NaCl solution with various pH (pH 3–9). (F) FE (HClO) on various  $MO_x$ /FTO anode at steady potentials (1.5–1.8 V vs. SHE, pH=7) in 0.5 M aqueous NaCl solution. pH was adjusted by using NaOH and HCl. For the  $MO_x$ /FTO electrodes (1.5 cm x 4 cm) used in the experiments of (B), (C) and (D), the concentrations of the coated metal precursor solution were 0.1 M for Mn, Co, Ni, and Fe, and 0.03 M for Rh. (G-i) XRD patterns of the various  $MnO_x$ /FTO anodes prepared by electrochemical deposition and followed by calcination at various temperatures. In the XRD pattern of  $MnO_x$ (ED-S(100°C))/FTO anode, no diffraction peak originated from the coating metal oxide, indicative of their amorphicity. (G-ii) FE (HClO) for  $MnO_x$ /FTO anodes prepared by electrochemical deposition followed by calcination at various temperatures, and that for the Ca- $MnO_x$  anode in a 0.5 M aqueous NaCl solution. (H) FE (HClO) on  $MnO_x$ /FTO electrodes prepared by changing different calcination temperatures (300–550°C) in 0.5 M aqueous NaCl solution. (I) FE (HClO) on  $MnO_x$ /FTO electrodes prepared by using different manganese precursor salt ( $Mn(NO_3)_2 \cdot 6H_2O$  and manganese bis(2-ethylhexanoate)) The obtained electrodes are denoted that Mn-N, Mn-H, respectively.



**Figure S4.** SEM images and  $MnO_x$  coverages of (A) FTO substrate and (B)(C)  $MnO_x$ /FTO anodes. Related to Figure 3.

Manganese precursor solutions with different concentrations ((B) 0.03 M and (C) 0.1 M) were spin-coated on FTO, and calcined at 400 °C. The apparent  $MnO_x$  coverage was evaluated by using XPS spectra of Mn 2p to Sn 3d and these counts per seconds (cps) coefficients.



**Figure S5.** HClO degradation behavior for MnO<sub>x</sub> (0.1 M)/FTO under dark conditions. Related to Figure 4, 5.

HClO degradation reactions were performed by using MnO<sub>x</sub> (0.1 M)/FTO under dark conditions in 0.5 M aqueous NaCl solution (35 mL) with initial addition of 200 µM of NaClO; (i) without current flow (-), and (ii) at a steady current of 2 mA (○).

#### References:

- Ramírez, A. et al. (2014) Evaluation of MnO<sub>x</sub>, Mn<sub>2</sub>O<sub>3</sub>, and Mn<sub>3</sub>O<sub>4</sub> Electrodeposited Films for the Oxygen Evolution Reaction of Water. *J. Phys. Chem. C* 118, 14073–14081.
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