

Research Paper

## Concentration, characterization and application of lipases from *Sporidiobolus pararoseus* strain

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### Abstract

Lipases produced by a newly isolated *Sporidiobolus pararoseus* strain have potential catalytic ability for esterification reactions. After production, the enzymatic extracts (conventional crude and precipitated, 'CC' and 'CP', and industrial crude and precipitated, 'IC' e 'IP') were partially characterized. The enzymes presented, in general, higher specificity for short chain alcohols and fatty acids. The precipitated extract showed a good thermal stability, higher than that for crude enzymatic extracts. The 'CC' and 'CP' enzymes presented high activities after exposure to pH 6.5 and 40 °C. On the other hand, the 'IC' and 'IP' extracts kept their activities in a wide range of pH memory but presented preference for higher reaction temperatures. Preliminary studies of application of the crude lipase extract in the enzymatic production of geranyl propionate using geraniol and propionic acid as substrates in solvent-free system led to a reaction conversion of  $42 \pm 1.5\%$ .

**Key words:** *Sporidiobolus pararoseus*, 'synthetic lipase', submerged fermentation, enzyme characterization.

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### Introduction

Lipases are ubiquitous in all types of living organisms and can be obtained from different sources such as microorganisms, animals and plants (Lotti and Alberguina, 2007; Bon *et al.*, 2008; Reis *et al.*, 2009). The enzymes of bacteria and fungi have the greatest potential as industrial biocatalysts, as they present high reaction rates, high-yield conversion of substrate to product, great versatility and simplicity in environmental and genetic manipulation of its productive capacity and easy recovery from fermentation broth (Lotti and Alberguina, 2007; Bon *et al.*, 2008).

Microbial lipases are produced mainly by submerged culture (Sharma *et al.*, 2001) and a wide variety of culture conditions that stimulate or suppress the production of mi-

crobial lipases is described in the literature. However, there is no general procedure to improve lipase production (Kademi *et al.*, 2004). The so-called 'industrial medium' for production of lipases commonly uses agroindustrial wastes or byproducts in its formulation, while the conventional medium is based on ingredients with a definite composition like salts, aminoacids, vitamins, growth factors, or costly complex ingredients like yeast extract, peptones and malt extract, among others. The main advantage of the industrial medium over the conventional one is its reduced costs, which may impact on the final product price. Over the recent years, research on the selection of suitable substrates for fermentative processes has mainly focused on agro-industrial residues, due to their potential advantages. Utili-

zation of agroindustrial wastes provides alternative substrates and may help solving pollution problems, which otherwise might be caused by their disposal. The choice of the substrate depends upon several factors, mainly related to cost and availability (Treichel *et al.*, 2010).

After the fermentation step, the enzyme is contained in a medium together with a series of other compounds of no interest. Precipitation is normally used as the first step in the purification procedure and the ammonium sulfate fractionation is the method most widely used (Martins *et al.*, 2008).

The effects of some variables on the activity of crude and purified lipases have been studied by some researchers. Factors such as pH, temperature, metallic ions, organic solvents, among others, can increase or decrease lipase activity. Besides, lipases can present different specificity to substrates. So, biochemical characterization can determine the adequacy of each enzyme to industrial processes (Hasan *et al.*, 2006).

Lipases that present esterification activity are gaining more attention nowadays because of their potential to catalyze the production of biodiesel, bioaromas and pharmaceuticals, reducing the operational costs associated with the conventional process, as well as overcoming problems related with chemical catalysis. As the production cost of the lipase is a major obstacle to the commercialization of the enzyme catalyzed process, various attempts have been made to develop cheaper systems. Many other applications of lipase with synthetic activity have been proposed, such as enantioselective reactions, synthesis of various esters and kinetic resolutions of chiral compounds (Treichel *et al.*, 2010).

In this context, this work aimed at characterization of crude and precipitated lipase extracts from conventional and industrial media in terms of stability at high and low temperatures, esterification substrate specificity (different fatty acids and alcohols) and acting ranges of memory of pH and temperature. A preliminary investigation of the potential application of the crude lipase extract on the enzymatic production of geranyl propionate using geraniol and propionic acid as substrates in solvent-free system was also carried out.

## Materials and Methods

### Cell production

The yeast used in the present study was previously isolated from soybean meal (9) and identified as *Sporidiobolus pararoseus* (Smaniotto *et al.*, 2012). It was maintained in glycerol at -80 °C and potato dextrose agar slants under refrigeration. The propagation was carried out for 3 days at 30 °C in Petri dishes containing a medium constituted by potato dextrose agar (PDA) 3.9 wt% and distilled water. The pre-inoculum was prepared by transferring the microorganism from the Petris dish to test

tubes containing 10 mL of PC medium (0.5, 0.25 and 0.1 wt% of tryptone, yeast extract and dextrose, respectively) sterilized at 121 °C for 15 min. The mixture was incubated at 30 °C for 24 h. The inoculum was prepared by mixing the pre-inoculum with 90 mL of sterilized PC medium in 250 mL Erlenmeyer flasks covered with cotton plugs. Flasks were incubated in a rotary shaker at 30 °C and 150 for 24 h.

### Culture conditions

Lipase was produced in conventional and industrial media. The conventional medium consisted of 5.0, 6.8, 7.0 and 1.0 wt% of peptone, yeast extract, NaCl and olive oil, respectively. The industrial medium consisted of corn steep liquor (5.0 wt%), hydrolyzed yeast extract (6.8 wt%), waste frying oil (1.0 wt%) and NaCl (7.0 wt%). Residual frying oil consisted of refined soybean oil, submitted to three successive frying batches of potatoes at 180 °C (Juaréz *et al.*, 2011). Cultivation was carried out in 250 mL Erlenmeyer flasks covered with cotton plugs in rotary shaker at 30 °C and 150 rpm. The media (in 90 mL aliquots) were sterilized at 121 °C for 15 min, cooled and inoculated with the inoculum solution (10%). After fermentation, samples were collected and filtered through Whatmann qualitative paper. The filtrate was frozen at -80 °C for 24 h and then lyophilized for 48 h. The resultant solid was considered as the crude enzymatic extract and used for analytical assays.

### Concentration of crude enzymatic extract

Ammonium sulfate was added to 150 mL of extract until the desired degree of saturation. The precipitation was carried out in single steps (using 40 and 60% of the saturation concentration) and in two sequential steps. The first step was carried out with addition of ammonium sulfate until 20% of saturation was reached. After the separation of the precipitated material, the supernatant was then further precipitated adding ammonium sulfate up to 40% of saturation.

The mixture was kept at 4 °C in an ice bath with constant agitation, with the pH maintained at 7.0 through the addition of NaOH 20%. The mixture was then transferred to centrifuge tubes, maintained at -10 °C for 5 h and then centrifuged at 4 °C and 5400 g for 30 min. The supernatant was discarded and the precipitate removed with a minimum amount of sodium phosphate buffer 100 mM pH 7.0 (8, 10). Samples were frozen at -80 °C and lyophilized for 48 h. The enzymes obtained in conventional and in industrial media in the crude (CC and IC) and precipitated (CP and IP) forms were partially characterized as described below. Protein was determined in all extracts as described by Fernandes *et al.* (2004).

### Esterification activity

Lipase synthetic activity was assayed by alkali titration using oleic acid and ethanol as substrates. An amount

of 0.1 g sample of lyophilized enzyme was added to a 1:2 mixture of oleic acid and ethanol. After incubation in shaker for 40 min at 40 °C and 150 rpm, the reaction was interrupted and the products were extracted by the addition of 20 mL of an acetone/ethanol solution (1:1v/v). The residual oleic acid was titrated with 0.02 M NaOH until pH 11. Reaction blanks were run in the same way, but adding the sample after addition of acetone/ethanol solution. The assays were carried out in duplicates. A unit of lipase activity was defined as the amount of enzyme that consumes 1  $\mu$ mol of oleic acid per minute under the assay conditions.

#### Specificity of the crude and precipitated enzymatic extract

The crude and precipitated lyophilized enzymatic extracts were characterized based on their esterification activity in different alcohols (methanol, ethanol, n-propanol and n-butanol) and fatty acids (lauric (12:0), oleic (18:1) and butyric (4:0)) (4, 5, 31).

#### Stability of the crude and precipitated enzymatic extract at low and high temperatures

The stability of lyophilized crude and precipitated enzymatic extracts at low temperatures was studied at 4 and -10 °C by measuring the esterification activities each 5 days during storage. The evaluation of stability at high temperatures was carried out by incubation at 30, 45 and 60 °C. The esterification activity was monitored every 24 h until total loss of activity.

#### Effect of temperature and pH memory on the crude and precipitated extracts

The pH memory was assessed by incubating the crude and precipitated enzymes ('CC', 'CP', 'IC' and 'IP') in different buffers (pH varying from 3.0 to 10.0) for 20 min at 4 °C. The extracts were then lyophilized, according to Sun *et al.* (2009) and the esterification activity was measured at different temperatures (11.8-68.2 °C) following the method described below.

These ranges of pH and temperature were evaluated according to a composite central rotatable design (DCCR)  $2^2$ , which was carried out for each extract.

#### Enzymatic esterification for production of geranyl esters

The esterification reactions were carried out by preparing a reactional mixture of geraniol, propionic acid (at molar ratios optimized previously by our research group using commercial lipases) and molecular sieves (20 mg/mL of substrates) in a 50 mL Erlenmeyer. After complete dissolution of the substrates, the enzymatic extract was added to the mixture. All experiments were carried out in an orbital shaker at constant agitation of 150 rpm. After the reaction time completion, the samples were kept at 5 °C for further

determination of reaction conversion, following a previously established method (Sun and Xu, 2008).

Quantitative analyses of geranyl esters produced were carried out in a gas chromatograph (Shimadzu GC-2010), using a capillar column of fused silica INOWAX (30 m length x 250  $\mu$ m i.d. x 0.25  $\mu$ m thickness), flame ionization detector, with the following temperature program: 40-180 °C (3 °C/min), 180-230 °C (20 °C/min), 230 °C (20 min), injector temperature 250 °C, detector at 275 °C, injection in the mode split, ratio of split 1:100. Hydrogen (56 KPa) was used as carrier gas and a volume of 0.4  $\mu$ L of sample diluted in n-hexane (1:10) was injected. Reaction conversion was calculated based on the reduction of area of limitant reagent on the basis of reaction stoichiometry (Sun and Xu, 2008).

## Results and Discussion

### Lipase production

The yeast *Sporodiobolus pararoseus* isolated and identified by our research group was previously presented as good synthetic lipase producer. Using the conventional optimized medium as substrate (Smaniotto *et al.*, 2012) the esterification activity was 26.9 U/mL of fermented medium in 72 h of fermentation. This yield is higher than those reported in literature for good lipase producer strains. Teng and Xu (Teng and Xu, 2008) obtained 13.9 U/mL of a lipase produced by *Rhizopus chinensis* at optimal conditions.

In the present study, the *Sporodiobolus pararoseus* was used to produce lipase using a low-cost substrate based on corn steep liquor, hydrolyzed yeast extract, waste frying oil and NaCl. The crude enzymatic extract obtained after 72 h of fermentation presented 12.3 U/mL of esterification activity. Although the lipase activity with this medium was lower than that obtained from conventional one, the lower costs of the residues may justify the study of the precipitation and characterization of the enzyme extract from industrial media.

It is important to mention that the corn steep liquor and the yeast hydrolysate presents a complex composition and both are sources of nitrogen, carbon, mineral salts and vitamins. The industrial medium contains a rich mixture of nutrients that might repress lipase production (Wang *et al.*, 2008). Pinheiro *et al.* (2008), studying the conventional and industrial media for lipase production by submerged fermentation from *Penicillium verrucosum*, observed that the lipase hydrolytic activity was 1.2 times higher in the conventional compared to the industrial medium. Immanuel *et al.* (2008) also discuss the importance of the use of industrial medium for enzyme production. They evaluated the substitution of the tryptone by casein in the production of an extracellular lipase from *Serratia rubidaea*, which caused an increase from 4.0 to 6.5 U/mL. Bapiraju *et al.* (2005), in an optimization study of lipase production by a

mutant *Rhizopus* sp., concluded that the potato starch, corn steep liquor and olive oil were the most promising sources of carbon, nitrogen and lipids, respectively.

### Concentration of the crude enzymatic extracts

Table 1 presents the results obtained for the concentration using ammonium sulfate in terms of esterification activity (U/g lyophilized extract), protein content (mg/mL) and specific esterification activity (U/mg<sub>protein</sub>). The first step of the fractional precipitation (20% of ammonium sulfate saturation) resulted in higher purification folds for the lipase produced both in conventional and industrial media (1.2 and 0.5-fold, respectively). These precipitated extracts presented the highest synthesis activity (154.6 and 120.9 U/g lyophilized extract, respectively) and the lowest protein content.

Specific lipase activity and purification folds presented in the literature vary a lot according to fermentation and precipitation condition, as well as the microorganism. The literature points out that the purification folds by precipitation with ammonium sulfate are usually low, but can reach up to 10, when optimized conditions are applied (Bradoo *et al.*, 2002; Stanburry *et al.*, 2003; Bapiraju *et al.*, 2005; Bon *et al.*, 2008).

### Characterization of the lipases

#### *Specificity of the crude and precipitated enzymatic extracts*

The esterification activity of the crude extracts using butyric and oleic acids as substrates and different alcohols is presented in Figure 1 (a) and (b), respectively. In general, the use of butyric acid as acil donor affords higher esterification activities. The IC extract presented the highest

esterification activity using methanol, independent from the acid used.

It is interesting to note that higher specificities for methanol and butanol can be observed when butyric acid is used. The same behavior can be seen using oleic acid when the enzymes from industrial medium (IC and IP) were evaluated. The alcohol specificity, towards oleic acid esterification, of the lipase produced with conventional medium presented a distinct behavior from that described above, since higher activities were obtained using methanol, ethanol and propanol with the enzymes CC and CP, respectively. When lauric acid was used as the acil donor, only the enzymes from the industrial medium (IC and IP) presented esterification activities, using methanol as substrate.

The produced enzymes showed higher apparent specificities for short chain fatty acids (butyric acid) and short chain alcohols (methanol). Sun *et al.* (2009) and Wang *et al.* (1995) cite that lipases commonly present higher specificity to fatty acids with 8 to 16 carbons. Usually, short chain fatty acids are known as inhibitors of the catalytic activity of the lipases. However, Abbas and Comeau (2003) showed that a lipase from *Mucor* sp. was able to catalyze esterification reaction using different alcohols and acids.

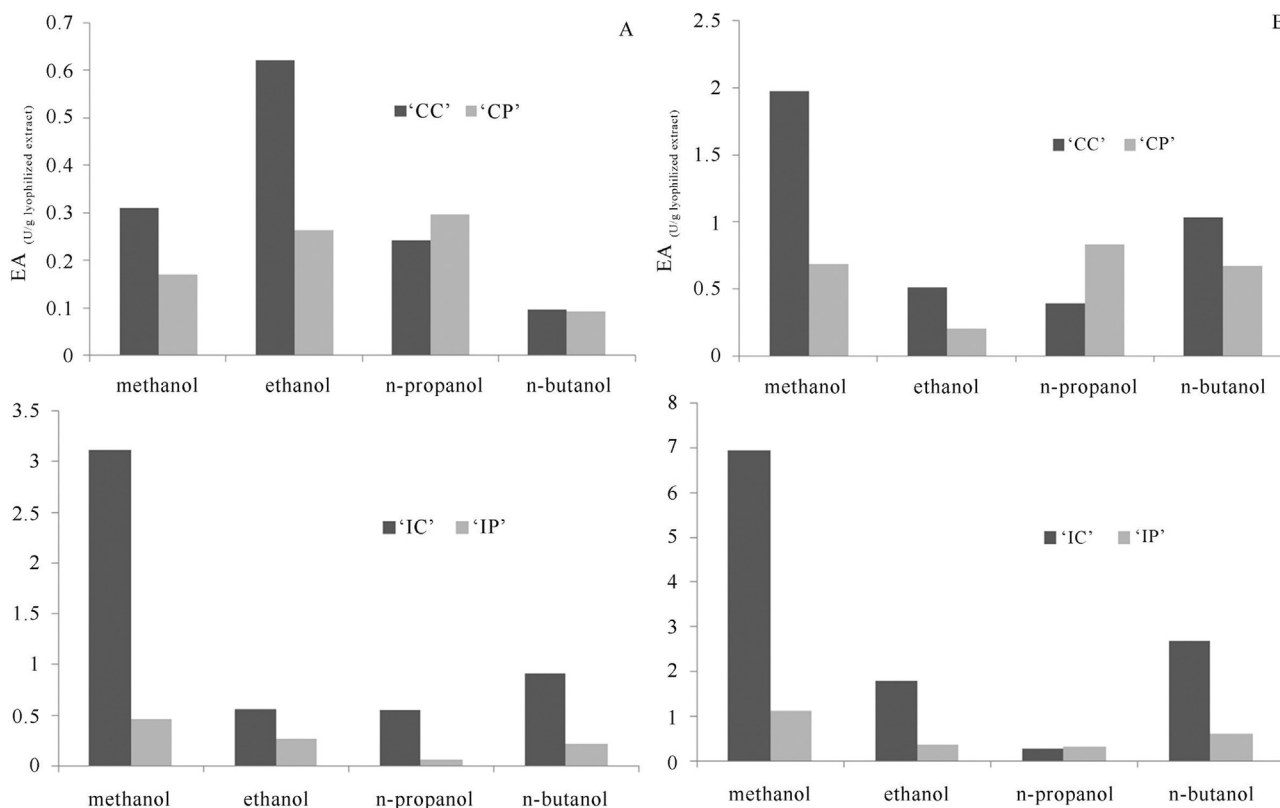
The lipase evaluated by Abbas and Comeau (2003) presented a particular specificity to short chains alcohols such as methanol, ethanol, 2-propen-1-ol and butanol. These results are in agreement with the studies carried out by Langrand *et al.* (1998) and Sun *et al.* (2009), where the yields decreased with the increase of the number of carbons. According to Ghandi *et al.* (1995) and Abbas and Comeau (2003) differences in lipase specificities to different alcohols can be explained in terms of the binding energy that is liberated when the substrate binds to the active site.

**Table 1** - Concentration of lipase extract using ammonium sulfate.

Extract <sup>a</sup>	Esterification activity (U/g <sub>lyophilized extract</sub> )	Protein content (mg/g <sub>lyophilized extract</sub> )	Specific esterification activity (U/mg <sub>protein</sub> )	Purification factor
Conventional				
Crude	127.31	0.26	489.65	1
D40	115.69	4.12	28.07	0.06
D60	119.31	3.76	31.74	0.06
F20	154.57	0.26	594.5	1.21
F40	103.10	1.03	100.09	0.20
Industrial				
Crude	58.31	0.11	530.10	1
D40	86.65	2.33	37.18	0.07
D60	77.56	3.02	25.68	0.05
F20	120.96	0.44	274.91	0.52
F40	95.63	2.20	43.47	0.08

<sup>a</sup>D40 and D60 refer to the extract precipitated by direct addition of ammonium sulfate at 40% and 60% of saturation. F20 and F40 refer to the extracts obtained by fractional precipitation in the first and second steps, respectively.





**Figure 1** - Esterification activities (EA) of the crude extracts using oleic (a) and butyric (b) acids as substrates and different alcohols.

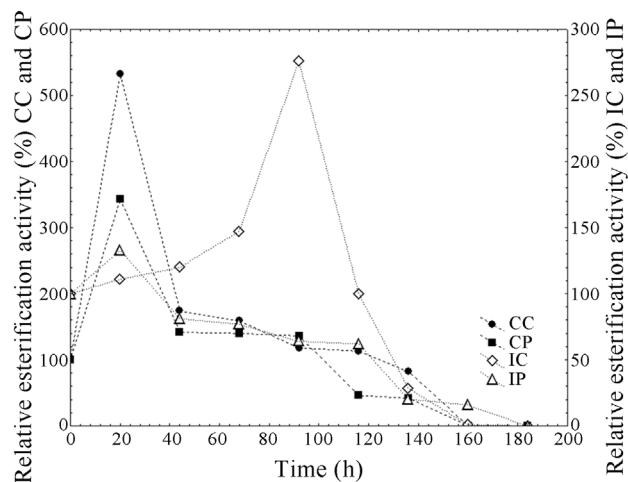
Short chain ethyl esters synthesized from acids are an important group of flavor and fragrances widely employed in food and beverages' industries (Kashmiri *et al.*, 2006). The market value of such compounds obtained by enzymatic reactions is usually higher than those produced by the conventional chemical path. Few studies can be found in the literature showing the specificity of non-commercial lipases to short-chain substrates, since these compounds can cause inhibitory effects (Peter and Preda; 2002; Shu *et al.*, 2006). So, the lipases presented here can find potential application in the production of flavours.

#### *Stability of the crude and precipitated enzymatic extracts to low and high temperatures*

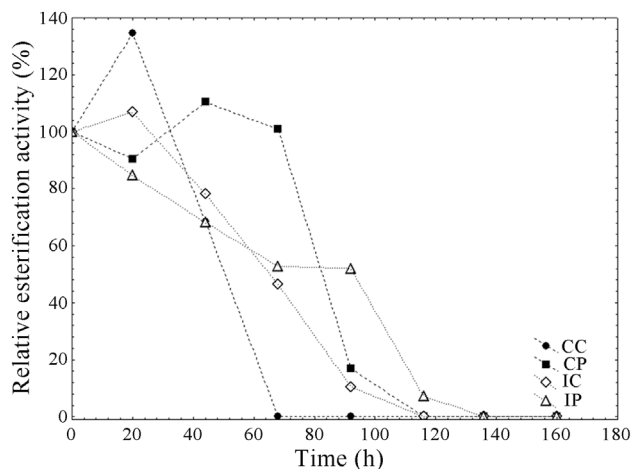
Figures 2, 3 and 4 present the evolution of lipase activities with time of incubation at 30, 45 and 60 °C, respectively. From Fig. 2 it is possible to observe the activation of the enzymes when incubated at 30 °C. The enzymes from conventional medium presented a maximum esterification activity after 20 h of incubation, at this time an increase of 5.3 and 3.4-fold in the activity was observed for the CC and CP, respectively. The extracts IC and IP showed the highest esterification activity after 92 and 20 h of incubation (2.8 and 1.3 times), respectively. The crude extracts presented a more marked activation. However, after 160 h of incubation, almost complete deactivation of all the extracts occurred. The activation of lipases at 30 °C was also observed

by Fernandes *et al.* (2004) studying hydrolysis reactions catalyzed by lipases from *Thermomyces lanuginosa*.

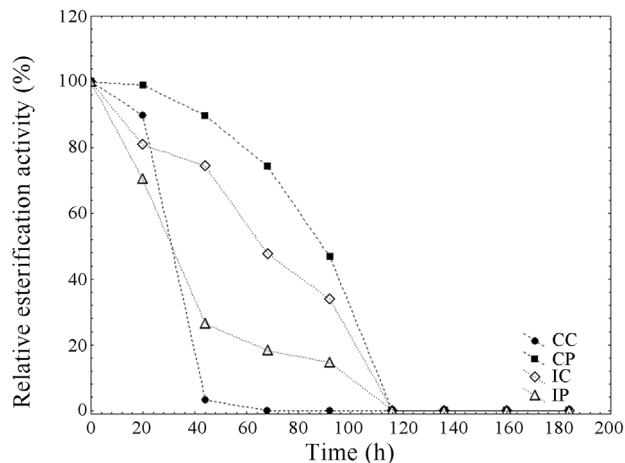
Figure 3 shows that at 45 °C the enzyme IP did not present an initial activation, but this extract kept the enzyme activity until 116 h of incubation. At 60 °C (Figure 4), all extracts lost the esterification activity during the incubation time (92 h) and the CC was the most heat sensitive (loss of all activity after 44 h of incubation).



**Figure 2** - Lipase activities during incubation at 30 °C. Initial activities: CC = 127.3 U/g, CP = 154.6 U/g, IC = 58.3 U/g, IP = 121.0 U/g.



**Figure 3** - Lipase activities during incubation at 45 °C. Initial activities: CC = 127.3 U/g, CP = 154.6 U/g, IC = 58.3 U/g, IP = 121.0 U/g.



**Figure 4** - Lipase activities during incubation at 60 °C. Initial activities: CC = 127.3 U/g, CP = 154.6 U/g, IC = 58.3 U/g, IP = 121.0 U/g.

The evaluation of low temperature stability showed that the precipitated enzymes CP and IP presented higher stabilities. Both kept 100% of their esterification activity until 60 days of storage at 4 and -10 °C. These results are in agreement with the work of Menoncin *et al.* (2010). The study of these authors showed that a concentrated lipase extract from *Penicillium verrucosum* kept its activity until 90 days of storage at the same low temperatures. Thus, the precipitation step is advantageous when considering the lipase stability. Although the esterification activity did not improve when the extracts were precipitated, the increase in the stability could be considered a promising result in terms of future application of these extracts.

#### *Effect of temperature and memory of pH on the crude and precipitated extracts*

According to Sun *et al.* (2009) and Sun and Xu (2008), lyophilized enzymes present a “memory of pH” ef-

fect. This can be explained by the fact that the esterification activity in organic solvents is extremely dependent on the pH of the aqueous solution before the lyophilization. This “memory of pH” effect probably occurs due to the ionic fixation of the catalytic site. Thus, after freeze-drying of the enzyme, the biocatalyst keeps the same state as in non-aqueous medium.

To evaluate the behavior of the extracts at different temperatures and pH memories, one CCRD 2<sup>2</sup> was carried out for each extract. Table 2 presents the matrix of the experimental design and the respective responses in terms of esterification activity for each extract.

The highest activity was obtained for the CC extract (around 145 U/g<sub>lyophilized extract</sub>), at a pH memory of 6.5 and 40 °C. High activity values for the CP were obtained at the central points (around de 64 U/g<sub>lyophilized extract</sub>), and these values show that the enzymes from conventional medium

**Table 2** - Effect of the temperature and pH memory on the crude and precipitated extract: Matrix of the experimental design (coded and real values) and the respective responses in terms of esterification activity for each extract.

Run	pH	T (°C)	Esterification activity (U/g <sub>lyophilized extract</sub> )			
			CC	CP	IC	IP
1	-1(4.0)	-1(20)	26.87	4.65	18.42	9.09
2	+1(9.0)	-1(20)	22.54	4.61	32.56	0.00
3	-1(4.0)	+1(60)	52.55	8.96	92.41	50.96
4	+1(9.0)	+1(60)	114.51	42.47	39.92	42.80
5	0(6.5)	0(40)	143.57	64.78	32.90	8.52
6	0(6.5)	0(40)	159.20	59.86	38.10	9.26
7	0(6.5)	0(40)	132.44	66.66	44.21	8.44
8	0(6.5)	-1.41(11.8)	0.00	0.00	0.00	0.00
9	0(6.5)	+1.41(68.2)	0.00	0.00	85.9	48.46
10	-1.41(3.0)	0(40)	56.62	52.54	0.00	0.00
11	+1.41(10.0)	0(40)	7.44	0.00	0.00	0.00

presented higher activities at pH memory of about 7 and near ambient temperatures.

High activities were also obtained with lipase produced with industrial medium, in runs 3 (pH 4.0 and 60 °C) and 9 (pH 6.5 and 68.2 °C), showing that the enzymes present activity in a wide range of pH memory and high temperatures.

Table 3 presents the empirical models that predict the lipase activity as a function of pH and temperature. All of them were validated ( $F_{\text{calculated}} > F_{\text{listed}}$ ) by analysis of variance (Table 4) at 90% of confidence level. The determination coefficients were 81, 80, 85 and 90% for the extracts CC, CP, IC and IP, respectively.

#### Preliminary studies for the application of the lipase extract

Preliminary studies of application of the conventional crude lipase extract in the enzymatic production of geranyl

propionate using geraniol and propionic acid as substrates, in solvent-free system, showed that in optimized operating conditions for propionate production using commercial lipases (geraniol to propionic acid molar ratio of 3:1, 40 °C, 150 rpm and 10 wt% of enzyme, conversions of about 95% (Sun and Xu, 2008)), a reaction conversion of  $42 \pm 1.5\%$  was achieved. This result is very promising, since it was obtained using optimized conditions for a commercial lipase. Probably, after optimization of operation parameters for the lipase of *Sporidiobolus pararoseus*, higher conversions could be obtained.

#### Conclusions

The yeast *Sporidiobolus pararoseus* is a promising synthetic lipase producer using conventional (13.9 U/mL) and industrial (12.3 U/mL) media. The enzymatic extracts presented, in general, higher specificity for short chain al-

**Table 3** - Empiric models for the esterification activity in function of pH and temperature for each studied extract.

Extract	Coded model
CC	$144.92 - 1.47pH(L) - 47.00pH(Q) + 14.75T(L) - 63.12T(Q) + 16.57pH(L)T(L)$
CP	$63.75 - 5.09pH(L) - 18.27pH(Q) + 5.29T(L) - 31.48T(Q) + 8.39pH(L)T(L)$
IC	$153.27 - 12.87pH(L) + 99.38T(L) - 19.84pH(L)T(L)$
IP	$8.69 - 2.16pH(L) - 0.96pH(Q) + 10.18T(L) + 11.23T(Q) + 0.23pH(L)T(L)$

**Table 4** - Analysis of variance for each model presented in Table 3.

Extract		Sum of squares	Degress of freedom	Mean of squares	F calculated
CC	Regression	30,178.05	5	6,035.61	4.24
	Residues	7,113.31	5	1,422.661	
	Lack of fit	361.42	3		
	Pure Error	6,751.88	2		
	Total	37,291.36	10		
CP	Regression	6,768.35	5	1,353.67	3.96
	Residues	1,710.69	5	342.14	
	Lack of fit	24.66	3		
	Pure Error	1686.03	2		
	Total	8479.04	10		
IC	Regression	42,119.73	3	14,039.91	5.73
	Residues	7,356.25	3	2,452.08	
	Lack of fit	64.10	2		
	Pure Error	7,292.16	1		
	Total	49,475.98	6		
IP	Regression	3,788.41	5	757.68	8.70
	Residues	435.61	5	87.12	
	Lack of fit	0.41	3		
	Pure Error	435.20	2		
	Total	4,224.01	10		

cohols and fatty acids. So, the use of the lipase extract presented here in the production of flavours could be considered an interesting application.

The concentrated extracts presented a good thermal stability, and are more stable than the crude enzymes. The CC and CP enzymes presented higher activities at pH memories around neutrality (6.5) and 40 °C. On the other hand, the IC and IP enzymes kept the activity in a wide range of memories of pH.

Preliminary studies of application of the produced lipase showed promising results. The enzymatic production of geranyl propionate using geraniol and propionic acid as substrates in solvent-free system yielded a reaction conversion of  $42 \pm 1.5\%$

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